

# Numerical study of melting effect with entropy generation minimization in flow of carbon nanotubes

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# Abstract

Optimization of entropy generation in squeezing flow of carbon nanotubes is addressed. Nanoparticles consist of singleand multiple-walled carbon nanotubes. Heat transfer subject to melting effect is employed. Shooting technique along with the fifth-order Runge–Kutta algorithm (bvp4c) is employed for the simulation. Bejan number, entropy generation rate, velocity and temperature are studied. Nusselt number and skin friction are also discussed. Velocity intensifies for higher estimations of squeezing parameter, nanoparticle volume fraction and melting parameter, while it reduces the temperature of fluid. Nusselt number enhances with an increment in estimations of squeezing parameter, nanoparticle volume fraction and melting parameter. Rate of entropy production decays with higher nanoparticle volume fraction and squeezing parameter. Bejan number is an increasing function of squeezing parameter, while it decays with an increment in melting parameter and nanoparticle volume fraction. Furthermore, prominent behavior is shown by multiple-walled CNTs.

Keywords Entropy generation · Bejan number · Melting effect · Carbon nanotubes (single- and multi-walled) · Squeezed flow

## List of symbols



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- $\Omega$  Non-dimensional temperature difference
- $P_1$  Pressure
- T Temperature of nanoliquid
- $T<sub>m</sub>$  Melting surface temperature
- $T<sub>h</sub>$  Upper wall temperature
- $\mu_{\rm nf}$  Nanofluid dynamic viscosity
- $S_{\text{G}_0}$  Characteristic entropy generation
- $\alpha_f$  Thermal diffusivity of base fluid
- $c_{\text{pf}}$  Specific heat of base fluid
- $k<sub>nf</sub>$  Nanofluids thermal conductivity
- $(c_p)_{\text{nf}}$  Specific heat of nanofluid
- $\alpha_{\text{nf}}$  Thermal diffusivity of nanofluid
- Pr Prandtl number
- $k_{\text{CNT}}$  Thermal conductivity of CNTs
- CNTs Carbon nanotubes
- $\phi$  Nanoparticle volume fraction
- $Ec_1$  Local Eckert number
- $\tau_{w}$  Shear stress
- Sq Squeezing parameter
- M Melting parameter
- $T_0$  Solid surface temperature
- $c_s$  Solid surface heat capacity
- Ec Eckert number

## <span id="page-1-0"></span>Introduction

Nanoliquids, a novel thermo-fluids class engineered through stable adjournment of nanosized metallic/nonmetallic objects (droplets, tubes, fibers, particles) in base materials with improved conductivity, exhibit the effective thermal management advantages with compactness. Nonetheless the intensification of thermal conductivity is not the main component accountable for nanofluids developed thermal efficiency, other aspects like sedimentation, gravity, inter-phase resistive force, dispersion, gravity, airborne phonon advection, invariable shear rate, migration of nanoparticles persuaded via layering and viscosity gradient at solid–liquid boundary also have a noteworthy contribution. The hydrothermal features of nanoliquids are revealed through the net impact of relative alterations in nanofluids thermophysical characteristics which are sympathetic regarding multiple factors comprising particle morphology (shape and size), pH value and base liquid characteristics, material temperature and additives. No doubt the amalgamation of disseminated solid elements in base liquid demonstrates extraordinary rise in thermophysical characteristics and maintains vast utilizations for illustration functioning of heat exchanger, thermal defiance, nuclear reactors cooling, etc. Choi [[1\]](#page-7-0) elaborates that nanoparticles size ought to be under 50 nm to convalesce heat transportation of ordinary materials. Later, with an innovation of technology in contemporary industry the nanoliquids with size under 100 nm have been established for distinct engineering functionalities. Various nanoliquid models (single-phase, two-phase, CNTs, Tiwari and Das) are reported to investigate nanotechnology [\[2–7](#page-7-0)]. Some recent works in this direction can be seen in Refs. [\[8–19](#page-7-0)].

Investigation regarding entropy generation and utilization of energy introduces a significant methodology in the thermal design and turns out to be the prime concern in numerous engineering demands for illustration (microelectronics, nuclear reactors chilling, heat exchangers, boiler and solar collectors). Precision estimation regarding entropy generation elucidates energy dissipation of a system effectively and consequently is a trustworthy device to acquire an optimum design in several industries. No doubt heat transportation intimate links with the thermodynamics first relation which is the only thermodynamic principle utilized in traditional heat transportation analysis. Thermodynamics second relation delivers an amount regarding rate of entropy generation or irreversibility in a system or procedure and accordingly influences the effectiveness of heat transportation process. Recently, increasing interest about irreversibility influence on energy interactions is noted. Initial analysis about entropy generation is elaborated by Bejan  $[20-22]$ . He revealed that entropy in convective liquid flow is owing to shear stresses and heat transportation. Numerous investigators employed entropy concept to minimize irreversibility of heat transport problems like boiling phenomenon and steam turbines [\[23](#page-7-0)]. Further, recent investigations covering entropy generation concept can be consulted through the Refs. [[24–](#page-7-0)[32\]](#page-8-0).

The researchers at present have considerable concern about improvement for energy storage and heating/cooling rate in various modern and advanced technologies. In this direction, numerous flow problems have been formulated considering different kinds of distributions (wall to ambient temperature) utilizing various fluid models. Nonetheless, major problem for researchers is to introduce extraordinary storing of energy through minimal price. Some advanced technologies like waste heat retrieval, solar energy and simultaneous heat/power plants necessitate economically more apposite and effectual approach to store energy. In general, three approaches are utilized regarding energy storing, that is sensible heat, latent heat and chemical/thermal energy. Among these approaches, the latent heat is regarded more apposite and well organized (by altering the materials phase). Consequently, thermal energy in a material is stowed via latent heat through melting procedure. Melting process is extremely vital in processes comprising soil melting, the soil freezing around heat exchanger loops of a field-based pump, permafrost melting, magma solidification, frozen grounds thawing, freeze cure of sewage, semiconductor material preparation, welding and molding of an industrial process [\[33](#page-8-0)]. Various researches have elaborated melting aspect under different flow configurations (see Refs. [[34–39](#page-8-0)]).

In this paper, we have studied entropy generation in dissipative flow of carbon nanotubes. Melting heat is accounted. Analysis is carried out between two infinite plates. Systems of differential equations are obtained via implementing suitable variables. Shooting method (bvp4c) is used for solutions development. Physical quantities are discussed.

# Formulation

Unsteady squeezed flow of carbon nanomaterial is assumed between two parallel plates. Both plates are distant  $h(t)$ apart. Lower plate (at  $y = 0$ ) is stretched with velocity  $U_w = \frac{ax}{1 - ct}$ , while the plate at  $y = h(t)$  is set in motion toward the plate at  $y = 0$  with a squeezing velocity  $v_h = \frac{dh}{dt} = \sqrt{\frac{v_f(1-ct)}{a}}$ . Melting heat is considered for heat transfer. Entropy generation effect is considered. Flow is parallel to  $x$  axis, while  $y$  axis is normal to it. Expressions under interest are [\[11\]](#page-7-0):

$$
\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0,\tag{1}
$$

$$
\rho_{\rm nf} \left( \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = -\frac{\partial p_1}{\partial x} + \mu_{\rm nf} \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right), \qquad (2)
$$

$$
\rho_{\rm nf} \left( \frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = -\frac{\partial p_1}{\partial y} + \mu_{\rm nf} \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right), \tag{3}
$$

$$
\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha_{\text{nf}} \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) \n+ \frac{\mu_{\text{nf}}}{(\rho c_p)_{\text{nf}}} \left[ 4 \left( \frac{\partial u}{\partial x} \right)^2 + \left( \frac{\partial v}{\partial x} + \frac{\partial u}{\partial y} \right)^2 \right],
$$
\n(4)

with boundary conditions

$$
u = U_{w}(x) = \frac{ax}{1 - ct}, \quad T = T_{m} \text{ at } y = 0, \quad u = 0,
$$
  

$$
v = v_{h} = \frac{dh}{dt}, \quad T = T_{h} \text{ at } y = h(t).
$$
 (5)

Melting condition is [[5\]](#page-7-0):

$$
k_{\rm nf}\left(\frac{\partial T}{\partial y}\right) = \rho_{\rm nf}(\lambda_1 + c_{\rm s}(T_{\rm m} - T_0))v \, \,at \, y = 0. \tag{6}
$$

The expressions used in theoretical model proposed by Xue [\[40](#page-8-0)] are

$$
\mu_{\rm nf} = \frac{\mu_{\rm f}}{(1 - \phi)^{2.5}}, \quad \nu_{\rm nf} = \frac{\mu_{\rm nf}}{\rho_{\rm nf}}, \quad \rho_{\rm nf} = (1 - \phi) \rho_{\rm f} + \phi \rho_{\rm CNT},
$$
\n
$$
\alpha_{\rm nf} = \frac{k_{\rm nf}}{\rho_{\rm nf}(c_{\rm p})_{\rm nf}}, \quad \frac{k_{\rm nf}}{k_{\rm f}} = \frac{(1 - \phi) + 2\phi \frac{k_{\rm CNT} - k_{\rm f}}{k_{\rm CNT} - k_{\rm f}} \ln \frac{k_{\rm CNT} + k_{\rm f}}{2k_{\rm f}}}{(1 - \phi) + 2\phi \frac{k_{\rm f}}{k_{\rm CNT} - k_{\rm f}} \ln \frac{k_{\rm CNT} + k_{\rm f}}{2k_{\rm f}}},\tag{7}
$$

We use the transformations [\[38](#page-8-0)]:

$$
\eta = \frac{y}{h(t)}, \quad u = \left(\frac{ax}{(1 - ct)}\right) f'(\eta), \quad v = -\sqrt{\frac{av_f}{1 - ct}} f(\eta),
$$

$$
\theta(\eta) = \frac{T - T_m}{T_f - T_m},
$$
(8)

where

$$
h(t) = \sqrt{\frac{v_f(1 - ct)}{a}}.\tag{9}
$$

Equation [\(1](#page-1-0)) is verified, while the other equations reduced to

$$
\left(\frac{1}{(1-\phi)^{2.5}(1-\phi+\phi^{\text{ccstr}})^{}}\right) f^{(iv)} - f'f'' + ff''' - \frac{Sq}{2}(3f'' + \eta f''') = 0,
$$
\n(10)

$$
\begin{aligned}\n&\left(\frac{k_{\rm nf}/k_{\rm f}}{(1-\phi+\phi\frac{(\rho c_{\rm p})_{\rm CN}}{(\rho c_{\rm p})_{\rm f}})}\right)\theta'' + Pr(f\theta' - \frac{Sq}{2}\eta\theta') \\
&+ \frac{Pr}{(1-\phi)^{2.5}(1-\phi+\phi\frac{(\rho c_{\rm p})_{\rm CN}}{(\rho c_{\rm p})_{\rm f}})}(4Ecf'^{2} + Ec_{\rm 1}f''^{2}) \\
&= 0.\n\end{aligned} \tag{11}
$$

$$
f'(0) = 1, \quad \theta(0) = 0,
$$
  
\n
$$
\left(\frac{k_{\text{nf}}}{k_{\text{f}}}\right) M \theta'(0) + Pr(1 - \phi + \phi \frac{\rho_{\text{CNT}}}{\rho_{\text{f}}}) f(0) = 0,
$$
 (12)  
\n
$$
f'(1) = 0, \quad f(1) = 1, \quad \theta(1) = 1.
$$

The involved dimensionless parameters are

$$
Sq = \frac{c}{a}, \quad Pr = \frac{v}{\alpha}, \quad Ec = \frac{v_f^2}{h^2(c_p)_f(T_m - T_h)},
$$
  
\n
$$
Ec_1 = \frac{U_w^2}{(c_p)_f(T_m - T_h)},
$$
  
\n
$$
M = \frac{c_{pf}(T_{\infty} - T_m)}{\lambda + c_s(T_m - T_0)}, \quad \eta = \frac{y}{h(t)}.
$$
\n(13)

Expressions of skin friction coefficient ( $C_f\sqrt{Re_\mathbf{x}}$ ) and Nusselt number  $(\frac{Nu_x}{\sqrt{Re_x}})$ 

Expressions for  $C_f \sqrt{Re_x}$  and  $\left(\frac{Nu_x}{\sqrt{Re_x}}\right)$  in dimensional and nondimensional forms are [[11\]](#page-7-0):

$$
C_{\rm f} = \frac{(\tau_{xy})_{y=0}}{\rho_{\rm f} U_{\rm w}^2}, \quad Nu_{x} = \frac{x \mathbf{q}_{\rm w}}{k_{\rm nf}(T_{\rm f} - T_{\rm h})},\tag{14}
$$

where

$$
\tau_{xy} = \mu_{nf} \left(\frac{\partial u}{\partial y}\right)_{y=0}, \quad \mathbf{q}_w = -k_{nf} \left(\frac{\partial T}{\partial y}\right)_{y=0}
$$
(15)

$$
or C_f \sqrt{Re_x} = \frac{1}{(1 - \phi_1)^{2.5} (1 - \phi_2)^{2.5}} f''(0),
$$
  

$$
\frac{Nu_x}{\sqrt{Re_x}} = -\frac{k_{\text{nf}}}{k_f} \theta'(0),
$$
 (16)

where  $Re_x = \sqrt{\frac{(1-ct)v_f}{a}}$  represents local Reynolds number.

# Entropy analysis

Entropy generation rate is [\[32\]](#page-8-0):

$$
S_G = S_H(entropy \text{ via heat transfer}) + S_F(entropy \text{ via fluid friction}).
$$
 (17)

Or

$$
S_{\rm G} = \frac{k_{\rm nf}}{T_{\rm h}^2} \left( \left( \frac{\partial T}{\partial x} \right)^2 + \left( \frac{\partial T}{\partial y} \right)^2 \right) + \frac{\mu_{\rm nf}}{T_{\rm h}} \left( 4 \left( \frac{\partial u}{\partial x} \right)^2 + \left( \frac{\partial v}{\partial x} + \frac{\partial u}{\partial y} \right)^2 \right).
$$
 (18)

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Non-dimensional entropy generation is

$$
Ns = N_{\rm H}(entropy \text{ via heat transfer}) + N_{\rm F}(entropy \text{ via fluid friction}), \qquad (19)
$$

$$
Ns = \frac{S_{\rm G}}{S_{\rm G_0}} = \theta^{\prime 2} + \frac{Pr}{\Omega(k_{\rm nf}/k_{\rm f})(1-\phi)^{2.5}}(4Ecf^{\prime 2} + Ec_1f^{\prime\prime 2})\tag{20}
$$

where 
$$
S_{G_0} = \frac{k_{\rm nf}(T_{\rm m} - T_{\rm h})}{T_{\rm h}^2 h^2}
$$
. (21)

Bejan number is [\[32](#page-8-0)]:

$$
Be = \frac{N_{\rm H}(entropy \text{ via heat transfer})}{N_{\rm G}(Total \text{ entropy})},
$$
\n(22)

$$
Be = \frac{\theta'^2}{\theta'^2 + \frac{P_r}{\Omega(k_{\rm inf}/k_l)(1-\phi)^{25}}(4Ecf'^2 + Ec_1f''^2)}.
$$
\n(23)

Note that Bejan number ( $Be$ ) lies between 0 and 1.  $N_{\rm H}$ dominates over  $N_F$  when  $0.5 < Be \le 1.0$ , and  $N_F$  overrides  $N_{\rm H}$  for  $0 \leq Be \lt 0.5$ , while for  $Be = 1.0$  both  $N_{\rm H}$  and  $N_{\rm F}$  are equal.

#### Solution via shooting method

Governing equations for flow are solved via shooting method using the fifth-order Runge–Kutta algorithm (bvp4c). First, we have an interest to write the first-order initial value problem as follows [[4,](#page-7-0) [38,](#page-8-0) [41](#page-8-0), [42](#page-8-0)]:

$$
f = s_1,\tag{24}
$$

$$
f'=s_2,\tag{25}
$$

$$
f'' = s_3,\tag{26}
$$

$$
f''' = s_4,\tag{27}
$$

$$
s_4' = f^{(iv)} = (1 - \phi)^{2.5} \left( 1 - \phi + \phi \frac{\rho_{CNT}}{\rho_f} \right) \left( \frac{Sq}{2} (\eta s_4 + 3 s_3) - s_2 s_3 + s_{1s_4} \right),\tag{28}
$$

$$
\theta = s_5,\tag{29}
$$

$$
\theta' = s_6,\tag{30}
$$

$$
s'_{6} = \frac{\left(1 - \phi + \phi \frac{(\rho c_{p})_{\text{cstr}}}{(\rho c_{p})_{t}}\right)}{\left(\left(k_{\text{nf}}/k_{\text{f}}\right)\right)} \left(-\Pr(s_{1} s_{6} - \frac{Sq}{2} \eta s_{6})\right) - \frac{Pr}{\left(1 - \phi\right)^{2.5}}\left(Ec_{1} s_{3}^{2} + 4Ec_{2}^{2}\right). \tag{31}
$$

along with

$$
s_2(0) = 1,
$$
  
\n
$$
\left(\frac{k_{\rm nf}}{k_{\rm f}}\right)Ms_6(0) + Pr\left(1 - \phi + \phi \frac{\rho_{\rm CNT}}{\rho_{\rm f}}\right)s_1(0) = 0,
$$
  
\n
$$
s_5(0) = 0,
$$
  
\n
$$
s_2(1) = 1, s_1(1) = 1, s'_5(1) = 1.
$$
\n(32)

### Analysis

#### Analysis for flow and temperature

In this subsection, influences of involved parameters on flow and temperature are analyzed graphically. Figures 1[–3](#page-4-0) are plotted in order to study variations of flow under Sq,  $\phi$ and M. Intensification in flow is seen for larger Sq. Variation in flow via Sq can be studied in two cases: (1)  $Sq > 0$ , (2) Sq < 0. Here, Sq > 0 is associated with motion of the squeezing plate (upper plate) toward stretchable plate (lower plate), while  $Sq<0$  corresponds to motion of the squeezing plate (upper plate) away from stretchable plate (lower plate). For higher Sq  $(Sq > 0)$ , the velocity of fluid increases due to influence of a force (squeezing force) felt by fluid particles. Also the increments in  $\phi$  and M lead to an enhancement in flow. Physically, an increment in M is associated with more rapid flow of heated fluid toward melting surface which intensifies flow. Interestingly, single-walled CNTs show overriding trends when compared with multiple-walled CNTs. Variations in temperature via Sq,  $\phi$  and M are labeled in Figs. [4–](#page-4-0)[6.](#page-5-0) Reduction in temperature is observed for an increment in Sq  $(Sq > 0)$ .



Fig. 1  $f'(\eta)$  via Sq

<span id="page-4-0"></span>

Fig. 2  $f'(\eta)$  via  $\phi$ 





Higher Sq leads to small collision among the fluid particles. Hence, temperature decays while the associated penetration depth rises. Decay in temperature is noted with the variations in  $\phi$  and M, while opposite trend is seen for associated penetration depth. Physically, higher M leads to more flow from hot fluid toward the melting surface. Hence, fluid temperature decays. Furthermore, overriding impact is observed for single-walled CNTs.



Fig. 4  $\theta(\eta)$  via Sq





# Analysis for entropy generation and Bejan number

Variations in Ns and Be via Sq,  $\phi$  and M are depicted in this subsection. Figures [7](#page-5-0), [9](#page-5-0) and [11](#page-5-0) illustrate variations in Ns via Sq,  $\phi$  and M, respectively. It is noticed that Ns reduces with an increment in Sq. Furthermore, production of entropy is maximum at the both walls, while it is minimum at the center of channel. Higher  $\phi$  leads to smaller Ns, while Ns intensifies for larger M. At both walls, production of entropy is maximum, while at center, the entropy production is minimum. Further, single-walled

<span id="page-5-0"></span>

Fig. 6  $\theta(\eta)$  via M



Fig. 7 Be via Sq

behavior (Figs. 9–[12\)](#page-6-0).

Tables [2](#page-6-0) and [3](#page-7-0).

CNTs show overriding trend comparatively with multiplewalled CNTs. In order to analyze the dominance of entropy due to fluid friction over entropy due to heat transfer or vice versa, Be is labeled via  $\eta$  in Figs. 8, [10](#page-6-0) and [12.](#page-6-0) Intensification in Be is noted with an increment in Sq. It is observed that at the lower wall the entropy due to fluid friction is prominent for higher Sq. Reduction in Be is noted for higher  $\phi$ . It is also observed that entropy via fluid friction shows overriding behavior at both walls. Be decays with an increment in  $M$ , and dominance in entropy via fluid



friction is noticed at both walls over entropy via heat transfer. Furthermore, single-walled CNTs show prominent

Table [1](#page-6-0) presents constructed thermophysical features of nanoparticles and base liquid, while numerical values of  $C_f$  and  $Nu_x$  under Sq,  $\phi$  and M are presented in



Fig. 8 Be via Sq



<span id="page-6-0"></span>



Fig. 10 Be via  $\phi$ 



Fig. 11 Ns via  $M$ 

# Final remarks

The key points of the presented analysis are

- Intensification in flow is observed with the increment in Sq,  $\phi$  and M.
- Decay in temperature is noted against Sq,  $\phi$  and M.
- Single-walled CNTs show overriding behavior than multiple-walled CNTs in terms of both flow and temperature.
- Intensification in heat transfer rate is analyzed for larger Sq,  $\phi$  and M.

Table 1 Thermophysical features of base liquid and CNTs [[40](#page-8-0)]

Physical features	Base liquid	Physical features	
	Water	<b>SWCNT</b>	<b>MWCNT</b>
$\rho$ /kg m <sup>-3</sup>	997	2600	1600
$c_p/J$ kg <sup>-1</sup> K <sup>-1</sup>	4179	425	796
$k/W$ m <sup>-1</sup> K <sup>-1</sup>	0.613	6600	3000

Table 2 Analysis of  $C_f$  via Sq,  $\phi$  and M

Fig. 12 Be via M



<b>Table 5</b> Allarysis of <i>IVII<sub>X</sub></i> via Sq. $\varphi$ and <i>M</i> when $EC = EC_1 = 0.2$ .					
Sq	$\phi$	M	$Nu_{x}$ (SWCNTS)	$Nu_{x}$ ( <i>MWCNTs</i> )	
$-1.0$	0.5	0.7	24.3	9.7	
0.0			24.5	9.8	
1.0			24.7	9.9	
2.0			24.9	10.0	
3.0			25.1	10.1	
1.0	0.1	0.7	11.4	9.3	
	0.2		12.0	9.4	
	0.3		14.0	9.5	
	0.4		16.5	9.6	
	0.5		19.2	9.7	
1.0	0.1	0.1	7.0	7.4	
		0.2	9.6	10.3	
		0.3	12.7	13.9	
		0.4	16.7	18.7	
		0.5	21.9	29.9	

<span id="page-7-0"></span>**Table 3** Analysis of  $Nu_x$  via Sq, $\phi$  and M when  $Ec = Ec_1 = 0.2$ .

- Entropy production rate decays with an increment in Sq and  $\phi$ .
- Bejan number is an increasing function of Sq, while it reduces for  $\phi$  and M.
- Role of multiple-walled CNTs is prominent than singlewalled CNTs for both entropy generation and Bejan number.

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