

# Analysis of the relationship between MCC and thermal analysis results in evaluating flammability of EPS foam

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**Abstract** The thermal properties of EPS foam were tested by simultaneous thermal analysis in a nitrogen environment, using a Netzsch STA 449C TG-DSC. Pyrolysis products were characterized using mass spectrometry and Fourier transform infrared spectroscopy. The flammability of EPS foam was examined using microscale combustion calorimetry. Heat release rate, peak heat release rate, heat release capacity, and some typical temperatures were obtained. The relationships between thermal analysis and MCC were derived from above test results. This could become a significant methodology in establishing the parameters contributing to flammability of polymers.

**Keywords** Microscale combustion calorimetry (MCC) · Flammability · Expanded polystyrene foam · Simultaneous thermal analysis · Decomposition

## Introduction

The essential characteristics that describe quantitatively “how big is the fire” is the heat release rate (*HRR*) [1]. It is widely used flammability assessment and for describing the

fire behavior of material [2]. *HRR* can be measured using the technique of “oxygen consumption” calorimetry. This can be determined using different scale calorimeters, such as the ISO 9705 room scale test, the ISO5660 bench scale cone calorimeter, and the microscale combustion calorimeter (MCC) ASTM D7309-07 [3], in which *HRR* can be obtained using the conversion factor  $13.1 \text{ kJ g}^{-1}$  of oxygen consumed. Prediction of *HRR* by modeling of the pyrolysis process has drawn great interest in flammability research. This is often described as creating a pyrolysis model because the degradation of material when it is exposed to heat is known as pyrolysis. When a material heats up, it may degrade to generate fuel fragments which ignite and burn. Complicated physical and chemical phenomena take place [1].

To discover the effect of material properties and composition on burning behavior, a quantitative analytical laboratory test that correlates fire behavior or flame test performance with material properties has been developed to relate the results of thermogravimetric analysis to flammability [4]. Microscale combustion calorimetry (MCC) or pyrolysis-combustion flow calorimetry (PCFC) has been developed for this purpose. Unlike thermogravimetric investigations of flammability which have relied on a single thermal stability parameter, in MCC, the pyrolysis products generated from a controlled pyrolysis in an inert gas stream are mixed with excess oxygen and combusted (oxidized) at high temperature, and the instantaneous heat of combustion of the flowing gas stream is measured by oxygen consumption calorimetry [4]. Results from MCC are not dependent on ignition source, sample thickness and orientation, ventilation, or edge condition in bench, and room scale tests [4]. The correlation of MCC parameters with conventional flammability tests such as LOI, UL 94, and cone calorimetry has been investigated [5]. Results from MCC have been compared with those from TG-gas chromatography/mass

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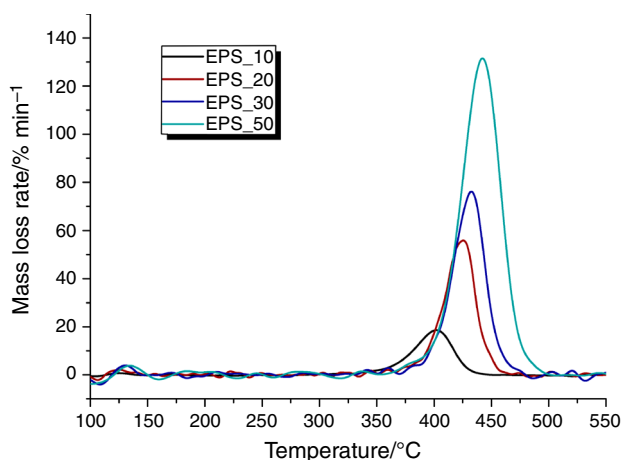
spectrometry, oxygen bomb calorimetry, and cone calorimetry for selected polymers [4]. MCC was established as an international standard test method in 2007 [3] [6]. Since then MCC has been used in material flammability research, especially in fire retardant research [7–10].

EPS foam panel is one end-use product of expandable polystyrene. Foam products typically are more sensitive to heat than their solid equivalents [11]. EPS is flammable; thus, the principal safety hazard of EPS foam panel is fire. Many large scale tests have been utilized to characterize the fire behavior of EPS [12–15]. The flammability of EPS has been evaluated using multi-scale methods [16]. In this approach, TG, DSC, cone calorimetry, and real-scale fire testing were used. MCC was adopted for further study. Results from MCC may be correlated with results from previous simultaneous thermal analysis. With the aid of mass spectrometry and Fourier transform infrared spectroscopy, the process from pyrolysis to combustion may be better understood.

## Test descriptions

### Test facilities

The experiments were carried out by means of STA (Simultaneous Thermal Analysis, using a Netzsch STA



**Fig. 1** DTG curves

**Table 1** Typical data obtained from TG curve

Sample label	$T_5/^\circ\text{C}$	$T_{50}/^\circ\text{C}$	$T_{95}/^\circ\text{C}$	$TR_{\max}/^\circ\text{C}$	Conversion/%	Peak conversion rate vs. Time/ $\% \text{ min}^{-1}$
EPS_10	351	397	422	402	61.3	23.0
EPS_20	381	421	447	427	65.3	55.7
EPS_30	393	429	455	432	57.7	79.4
EPS_50	407	441	464	443	57.1	140.2

$T_5$  temperature of 5 % sample mass loss,  $T_{50}$  temperature of 50 % sample mass loss,  $T_{95}$  temperature of 95 % sample mass loss,  $TR_{\max}$  temperature of sample thermal decomposition maximum rate

449C TG-DSC) which applies thermogravimetry (TG) and differential scanning calorimetry (DSC) to EPS foam samples under a nitrogen atmosphere. A heating rate of 10, 20, 30, and 50  $^\circ\text{C min}^{-1}$  from 50  $^\circ\text{C}$  to a maximum temperature of 600  $^\circ\text{C}$  was used with a gas flow rate of 75  $\text{mL min}^{-1}$ . Samples were contained in  $\text{Al}_2\text{O}_3$  crucibles without lids.

Coupled techniques, such as STA-FTIR-MS, that enable the identification of the gases that are evolved during EPS pyrolysis were used in this research. The STA was coupled to evolved gas analysis (EGA) detectors. The pyrolysis products from STA were examined using mass spectrometry (MS), using a type QMS403C unit from Netzsch, and Fourier transform infrared spectroscopy (FTIR), using a type 5700 instrument from Nicolet Instrument Company. For FTIR, the wavenumber range was set as 4,000–400  $\text{cm}^{-1}$ . MS and FTIR measurement were coupled with STA at heating rate of 10 and 50  $^\circ\text{C min}^{-1}$ .

MCC tests were conducted on Type MCC-2, from Govmark Organization, Inc., Farmingdale, NY, USA, according to the ASTM standard test method D7309-2007, using ‘Method A’ [3]. The heating rate was 10, 20, 30, 50, and 100  $^\circ\text{C min}^{-1}$ .

EPS foam was from Jiangsu Sanyou Plastics Co., Ltd. The foam has a density of 8.033  $\text{kg m}^{-3}$  and a normal level of fusion. A molecular mass determination for the foam was not performed. A LOI test carried out according to ASTM D2863 provided a value of 22.2.

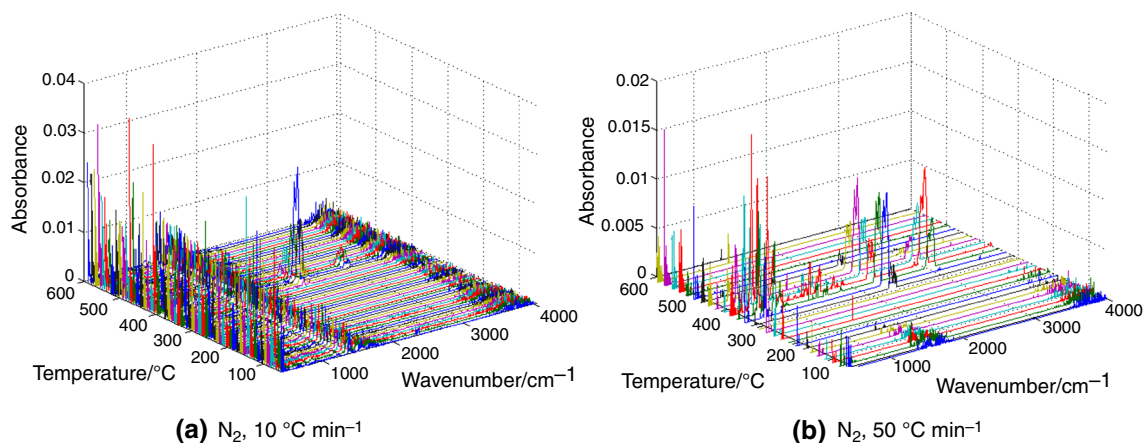
## Test results

### STA, FTIR, and MS test results

Illustrative DTG curves are presented in Fig. 1. There is only one degradation stage for EPS. A delay in degradation and a shift of the curves to higher temperatures with increasing heating rate were observed in agreement with previous observations [17], [18]. At lower heating rates, the sample spends a longer time at a certain temperature; thus, more degradation will occur before the sample reaches the next temperature zone [18]. The conversion reaches its

**Table 2** Typical data obtained from DSC

Sample label	Inflection temperature of glass transition/ $^{\circ}\text{C}$	Peak temperature for a endothermic event/ $^{\circ}\text{C}$	Temperature range for the of endothermic effect/ $^{\circ}\text{C}$	Enthalpy/ $\text{J g}^{-1}$
EPS_10	132.4	404	361–423	2407
EPS_20	122.2	426	376–474	1476
EPS_30	132.3	438	378–484	728
EPS_50	135.0	450	391–521	602

**Fig. 2** FTIR spectra of degradation products evolved from TG

peak rate between 57.1 and 65.3 %. The conversion rate is greater for 50–90 % conversion than for 5–50 % conversion as shown in Table 1. In DTG curves, there is a small fluctuation at different heating rates at around 125  $^{\circ}\text{C}$ . This is due to air which escapes from the foam cell when it breaks.

Only one main endothermic event is observed in the DSC curve for each sample. This event occurs at temperature greater than 350  $^{\circ}\text{C}$ . The peak temperature for the endothermic event shifts to higher temperature as the heating rate increases. This behavior, in an inert environment, is similar to that previously described [19]. Typical data obtained from DSC are listed in Table 2.

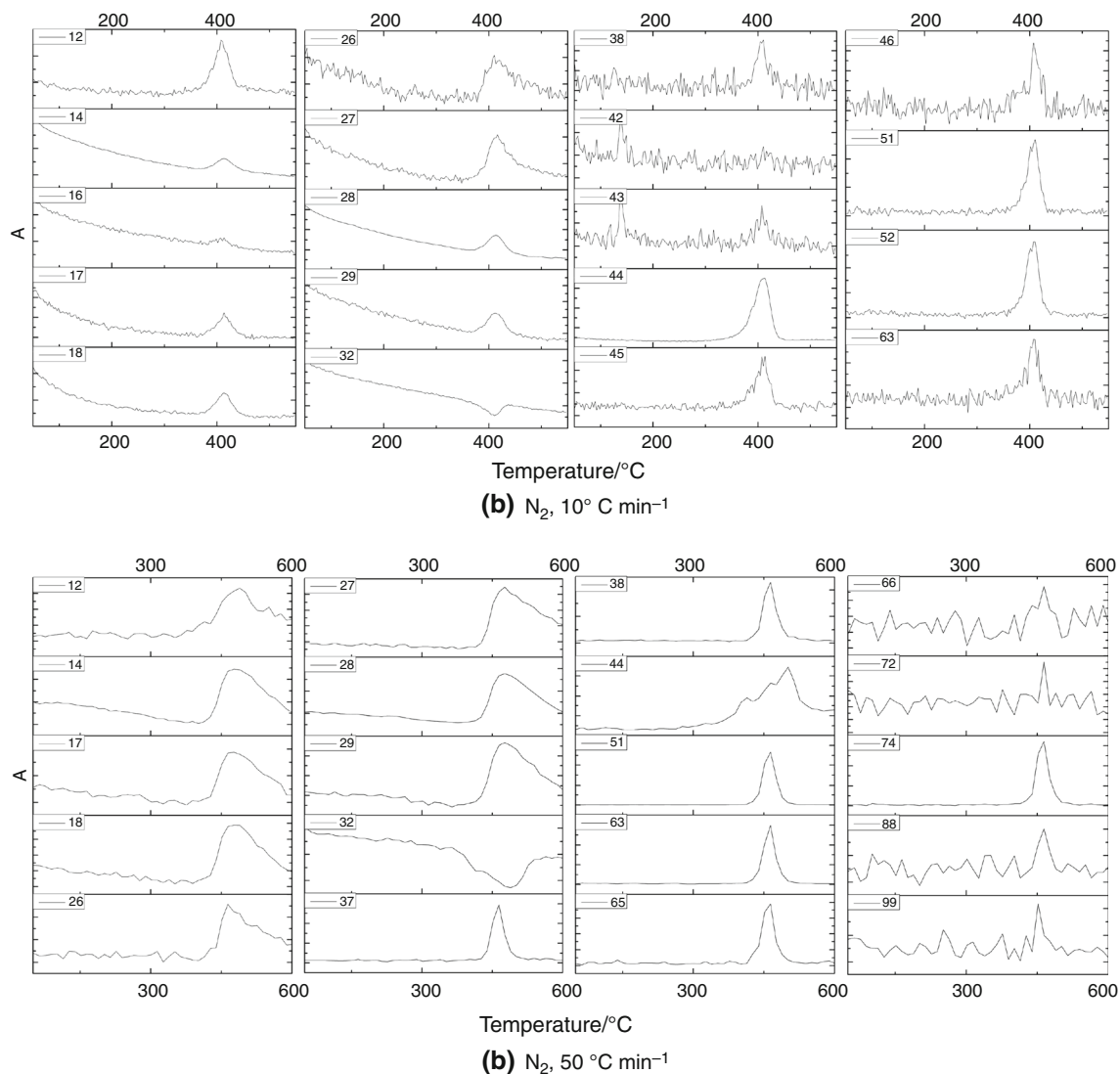
The 3D FTIR spectra of degradation products obtained from thermal degradation at 10 and 50  $^{\circ}\text{C min}^{-1}$  heating rates in a nitrogen atmosphere are shown in Fig. 2. A detailed analysis of the spectra suggests the following results.

At 372.5  $^{\circ}\text{C}$ , it begins to produce  $\text{CO}_2$  (fundamental frequency absorption peak at 669 and 2,349  $\text{cm}^{-1}$ ), single substituted benzene (out-of-plane ring bend vibrations at 669 and 2,349  $\text{cm}^{-1}$ , planar aromatic skeleton vibrations ranging from 1,430 to 1,600  $\text{cm}^{-1}$ ), m-di-substitution benzene (three absorption peaks located at 695, 771 and 900  $\text{cm}^{-1}$ ), alkynes ( $\text{C}\equiv\text{C}$  symmetric stretching vibration nearby 2,309 and 2,380  $\text{cm}^{-1}$ ),  $\text{H}_2\text{O}$  (from 3,500 to 4,000  $\text{cm}^{-1}$ ). There may be some acids, esters, and ethanol

(CO stretching vibration nearby 1,217  $\text{cm}^{-1}$ , carbonyl stretch vibration at 1,650 to 1,900  $\text{cm}^{-1}$ ). With the temperature increasing, more substances are generated. When it reaches the maximum mass loss velocity temperature at 404.2  $^{\circ}\text{C}$ , the amount of resultant reached maximum. In addition to above compounds, it produces terminal olefins (the out-of-plane of CH bending mode nearby 910 and 990  $\text{cm}^{-1}$ , CH stretching vibration at 3,072  $\text{cm}^{-1}$ ,  $\text{C}=\text{C}$  symmetric stretching vibration at 1,500 to 1,680  $\text{cm}^{-1}$ ). Then, considering the absorption peaks centering at 695 and 719  $\text{cm}^{-1}$ , this kind of terminal olefins can be adjudged to be styrene.

With further increase of temperature, the amount of resultant decreases and eventually stops generating. Although terminal olefins increase very slowly in early stage, it has a sharp decrease in the latter period. Above all, at initial period of degradation, it mainly produces some styrene polymers, whereas the generation of other resultant is caused for oxidation. As temperature further increased, the amount of styrene reaches maximum at maximum mass loss velocity. In conclusion, during pyrolysis of EPS at nitrogen atmosphere, weak bond begins to break randomly, then polymers further degrades after initial pyrolysis until all polymers degrades to styrene monomer; thus, the pyrolysis mechanism of EPS is mainly random degradation.

Figure 3a is the variation diagram that ion current density varies with temperature with heating rate of



**Fig. 3** MS results

$10^\circ C \text{ min}^{-1}$  at a nitrogen atmosphere.  $m/z$  detected by MS and the temperature range are listed in Table 3.  $m/z$  42 was detected from 125 to  $150^\circ C$ , which accorded with glass-transition temperature measured by DSC. Meanwhile, an absorption peak from  $2300$  to  $2,500 \text{ cm}^{-1}$  is found in 3D infrared spectra (Fig. 2); thus, it can be judged as propylene, which may be produced after the foaming agent rupture. The ion current density of  $m/z$  32 decreases from  $375$  to  $445^\circ C$ , which may be caused by the reduction of oxygen mingled in a nitrogen atmosphere.

According to the above infrared spectra, it can be defined that  $m/z$  14, 16, 26, 27, 29, 38, 43, 51, 52, 63 are some alkane, olefin hydrocarbons, and alkyne. The maximum ion current density accords with maximum mass loss velocity.  $m/z$  28 may be CO, which is the resultant of EPS and oxygen impurity.

$m/z$  18 is  $H_2O$ , which can be verified from  $3,500$  to  $4,000 \text{ cm}^{-1}$  on the infrared spectra.  $m/z$  44 may be  $CO_2$  or  $C_3H_8$ , and then we can identify, it is  $CO_2$  by the absorption peak at  $669$  and  $2,349 \text{ cm}^{-1}$  in infrared spectra.  $m/z$  12 is C, and  $m/z$  45 is  $C_2H_5O$ , then we can deduce, it is  $CH_2CH_2OH$  by the IR spectra.  $m/z$  46 is  $C_2H_6O$  or  $CH_2O_2$ , and it may be  $CH_3CH_2OH$  (HO stretching vibration at  $3,000$  to  $3,750 \text{ cm}^{-1}$ ) or  $HCOOH$  (CO stretching vibration at  $1,217 \text{ cm}^{-1}$ , carbonyl stretching vibration nearby  $1,650$  to  $1,900 \text{ cm}^{-1}$ ).

From the above analysis, a conclusion could be drawn that the pyrolysis products of EPS in nitrogen atmosphere mainly contain some micromolecules, such as single substituted, m-di-substitution benzene, alkane, olefin hydrocarbons, alkyne, CO,  $H_2O$ , C,  $CO_2$ , and ethyl alcohol.

When the temperature rises up to  $443^\circ C$ , it also generates m-di-substitution benzene and terminal olefins in

**Table 3** MS results

$m/z$ ( $\beta = 10\text{ }^{\circ}\text{C min}^{-1}$ )	$T/^{\circ}\text{C}$ ( $\beta = 10\text{ }^{\circ}\text{C min}^{-1}$ )	$m/z$ ( $\beta = 50\text{ }^{\circ}\text{C min}^{-1}$ )	$T/^{\circ}\text{C}$ ( $\beta = 50\text{ }^{\circ}\text{C min}^{-1}$ )	Possible ions
12	375–445	12	420–600	C
14	375–445	14	420–600	CH <sub>2</sub> , N
16	375–445	–	–	CH <sub>4</sub> , O
17	375–445	17	420–600	OH
18	375–445	18	420–600	H <sub>2</sub> O
26	375–445	26	420–600	C <sub>2</sub> H <sub>2</sub>
27	375–445	27	420–600	C <sub>2</sub> H <sub>3</sub>
28	375–445	28	420–600	C <sub>2</sub> H <sub>4</sub> , CO, N <sub>2</sub>
29	375–445	29	420–600	C <sub>2</sub> H <sub>5</sub>
32	375–445	32	375–550	O <sub>2</sub>
–	–	37	420–500	C <sub>3</sub> H
38	375–445	38	420–500	C <sub>3</sub> H <sub>2</sub>
42	125–150	–	–	C <sub>3</sub> H <sub>6</sub> , C <sub>2</sub> H <sub>2</sub> O
43	125–150, 375–445	–	–	C <sub>3</sub> H <sub>7</sub> , C <sub>2</sub> H <sub>3</sub> O
44	350–445	44	400–550	CO <sub>2</sub> , C <sub>3</sub> H <sub>8</sub> , C <sub>2</sub> H <sub>4</sub> O
45	375–445	–	–	C <sub>2</sub> H <sub>5</sub> O, CHO <sub>2</sub>
46	375–445	–	–	C <sub>2</sub> H <sub>6</sub> O, CH <sub>2</sub> O <sub>2</sub>
51	375–445	51	420–500	C <sub>4</sub> H <sub>3</sub>
52	375–445	–	–	C <sub>4</sub> H <sub>4</sub>
63	375–445	63	420–500	CH <sub>3</sub> O <sub>3</sub> , C <sub>5</sub> H <sub>3</sub>
–	–	65	420–500	C <sub>4</sub> HO, C <sub>5</sub> H <sub>5</sub>
–	–	66	420–500	C <sub>4</sub> H <sub>2</sub> O, C <sub>5</sub> H <sub>6</sub>
–	–	72	420–500	C <sub>4</sub> H <sub>8</sub> O, C <sub>5</sub> H <sub>12</sub>
–	–	74	420–500	C <sub>2</sub> H <sub>2</sub> O <sub>3</sub> , C <sub>3</sub> H <sub>6</sub> O <sub>2</sub> , C <sub>6</sub> H <sub>2</sub>
–	–	88	420–500	C <sub>4</sub> H <sub>8</sub> O <sub>2</sub> , C <sub>5</sub> H <sub>12</sub> O, C <sub>7</sub> H <sub>4</sub>
–	–	99	420–500	C <sub>5</sub> H <sub>7</sub> O <sub>2</sub> , C <sub>6</sub> H <sub>11</sub> O

addition to above substance. As the temperature increases, these products disappear gradually, this tendency is similar to the situation at  $10\text{ }^{\circ}\text{C min}^{-1}$ . However, there are some differences at the m-di-substitution benzene generated temperature between both heating rates.

Figure 3b is the mass spectra at the heating rate of  $50\text{ }^{\circ}\text{C min}^{-1}$ . Details of temperature range and possible ions are also listed in Table 3. According to Table 3 and above infrared analysis, we can obtain that  $m/z$  12, 14, 17, 18, 26, 27, 29 are C, alkane, olefin hydrocarbons, and alkyne, respectively.

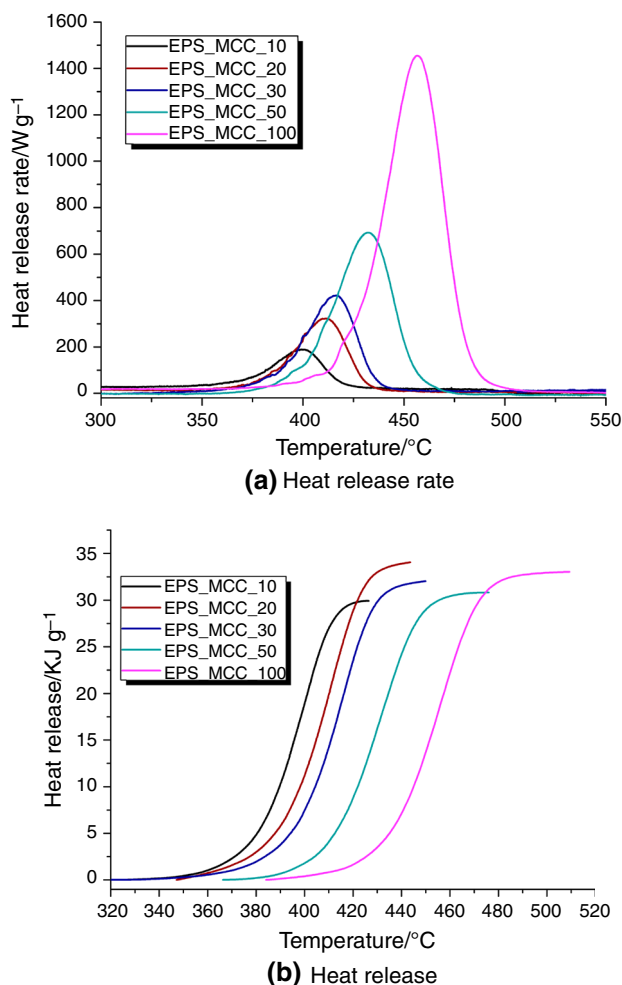
These micromolecules can be detected ranging from 420 to  $600\text{ }^{\circ}\text{C}$ , which indicated that these fragments ions are generated even at the end stage of pyrolysis.  $m/z$  28 is CO detected from 420 to  $600\text{ }^{\circ}\text{C}$  through the whole pyrolysis process, and  $m/z$  44 is CO<sub>2</sub>, whereas its detected temperature range is 420 to  $550\text{ }^{\circ}\text{C}$ , which is narrower than the former. O<sub>2</sub> ( $m/z = 32$ ) is detected ranging from 375 to  $550\text{ }^{\circ}\text{C}$  at the heating rate of  $50\text{ }^{\circ}\text{C min}^{-1}$ , which is the same with the mass spectra of  $10\text{ }^{\circ}\text{C min}^{-1}$ .

This phenomenon means that oxygen participates in reaction at the initial phase of pyrolysis.  $m/z$  37, 38, 51, 63,

65, 66 are fragment ions of alkane, olefin hydrocarbons, and alkyne. And its temperature range is 420 to  $500\text{ }^{\circ}\text{C}$ , which is shorter than those small mass charge ratio ions. So, it can be deduced that these small mass charge ratio ions come from further degradation of large mass charge ratio ions. As to even larger mass charge ratio ions, for example,  $m/z$  72, 74, 88, 89, all these may be the fragment ions of alkane, olefin hydrocarbons, and alkyne, of course, it also may be of alcohol or acid.

By FTIR and MS analysis at different heating rates ( $10$  and  $50\text{ }^{\circ}\text{C min}^{-1}$ ), we can conclude that the pyrolysis mechanism of EPS in nitrogen atmosphere is random pyrolysis, and the degradation products at two different heating rates are similar, including single substituted (styrene), m-di-substitution benzene, alkane, olefin hydrocarbons, alkyne, acid, CO, O, CO<sub>2</sub>, and alcohol.

Main generated products were accordance with respective mass loss temperature. The mass spectra of  $50\text{ }^{\circ}\text{C min}^{-1}$  can detect both small and large mass charge ratio ions, whereas  $10\text{ }^{\circ}\text{C min}^{-1}$  mass spectra only showed the small mass charge ratio ions. This difference is explained by the fact that it is too short for large ions to

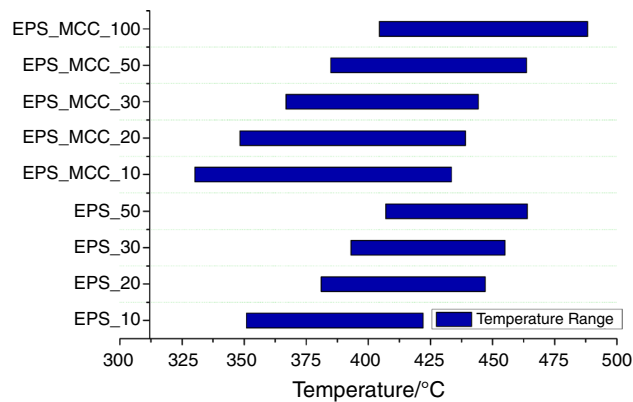


**Fig. 4** MCC results

break into small ions, on the contrary, for the case of 10 °C min<sup>-1</sup>, large ions have enough time to break into small ones.

#### MCC test results

The parameters used to characterize flammability can be examined using MCC are heat release capacity ( $HRC$ , J g<sup>-1</sup> °C<sup>-1</sup>), heat, release rate ( $HRR$ , W g<sup>-1</sup>) at different temperatures, peak heat release rate ( $pHRR$ , W g<sup>-1</sup>), temperature at  $pHRR$  ( $T_{pHRR}$ , °C), and total heat release ( $THR$ , kJ g<sup>-1</sup>).  $HRC$ , which is obtained by dividing the maximum value of the specific heat release rate ( $SHRR$ ) with the heating rate (°C s<sup>-1</sup>) in the test, is a material property [4]. It appears to be a good predictor of flammability and propensity for ignition, and it is related to the decomposition kinetics and combustion parameters of the sample [4]. Swelling and dripping of thermoplastics influence flame fire tests, such as cone calorimeter test, but do not affect  $HRC$ .



**Fig. 5** Temperature ranges of mass loss and non-flame combustion

**Table 4** Typical data obtained from MCC

Sample label	$HRC$ / J g <sup>-1</sup> °C <sup>-1</sup>	$pHRR$ / W g <sup>-1</sup>	$THR$ / kJ g <sup>-1</sup>	$T_{pHRR}$ / °C	$T_{up5}$ / °C	$T_{down5}$ / °C
EPS_MCC_10	1136.4	189.4	29.9	399.2	330.1	433.5
EPS_MCC_20	968.4	322.8	34.0	411.6	348.3	439.1
EPS_MCC_30	844.8	422.4	32.1	415.6	366.9	444.3
EPS_MCC_50	831.7	693.1	30.8	432.2	384.8	463.7
EPS_MCC_100	873.0	1454.9	33.0	457.0	404.5	488.3

$T_{pHRR}$  temperature of peak heat release rate,  $T_{up5}$  temperature of 5 % peak heat release rate in rising stage,  $T_{down5}$  temperature of 5 % of peak heat release rate in declining stage

$HRR$  versus time curves are shown in Fig. 4a,  $T_{pHRR}$  shifts to higher temperature with increasing heating rate as the DTG curves. The groups of  $HRR$  curves have the same shape and tendency as TG and DTG (shown in Fig. 1a, b). Typical parameters are listed in Table 4.  $HRC$  decreases with increase of heating rate generally, except for 100 °C min<sup>-1</sup>.  $pHRR$  increases with increase of heating rate. The range of  $THR$  is from 29.9 to 34.0 kJ g<sup>-1</sup>, shown in Fig. 4b and Table 4. Temperature ranges of  $HRR$  in MCC and mass loss in STA are shown in Fig. 5.

#### Conclusions

The more pyrolyzate produced per unit of time, the more heat release rate generated in forced combustion. This is the main reason account for high  $pHRR$  appearing at high heating rate.

This suggests that  $HRR$  depends on heating rate in MCC tests. MCC can be used to characterize the fundamental performance of materials in forced combustion condition. The forced combustion condition is quite different from real fire scenario; thus, results from MCC cannot be used to modeling or predicting fire behavior of materials directly. High heating rate MCC test would be more helpful in



understanding material's combustion performance, while in STA test low heating rate would be helpful in analyzing pyrolyzate.

*HRC* decreases with the increase of heating rate, while the total heat release is independent of heating rate. It is the sum of heat release from all combustibles when forced to combust in MCC, and it assumed to have the same value even at different heating rates. It could be used as a measure of combustion potential of materials and used to compare fire hazard potential among materials.

There is no direct corresponding relationship between MCC and DSC data, such as the *pHRR* in MCC and endothermic peak in DSC, except for typical temperature ranges are the same. In the tests presented above, the temperature of *pHRR* in MCC is lower than peak temperature in DTG and DSC at every heating rate, but the differences are not significant, within systematic errors of both equipments.

From the comparison of typical temperature ranges from MCC to DTG, the temperature at which *HRR* reaches 5 % of *pHRR* in MCC is lower than the temperature at which mass loss reaches 5 % in DTG. It partly implies that the pyrolyzate in early stage contributes more to *HRR*.

From MS and FTIR results at 10 and 50 °C min<sup>-1</sup> heating rate, EPS decomposes more sufficiently at low heating rate. At low heating rate, the amount of pyrolyzate swept into combustion furnace is less than that at high heating rate, and almost of pyrolyzates are smaller fragment than those at high heating rate. At high heating rate, bigger fragments in combustion chamber further decompose and combust, more oxygen is consumed than at low heating rate, it will cause a higher *pHRR*. It is the main reason that *HRR* depends on heating rate in MCC tests.

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