Study on modification of Cu-based oxygen carrier for chemical looping combustion

Hou-yin Zhao • Yan Cao • William Orndorff • Wei-ping Pan

Received: 30 September 2012 / Accepted: 11 December 2012 / Published online: 23 December 2012 © Akadémiai Kiadó, Budapest, Hungary 2012

Abstract Chemical looping combustion (CLC) is a promising technology for segregation of carbon dioxide. CLC uses a metal oxide as an oxygen carrier, which transfers oxygen from the air to the fuel avoiding direct contact between them, thus separating the carbon dioxide and nitrogen. Cu-based oxygen carriers are excellent mediums due to high reactivity, environmental friendliness, and favorable thermodynamics. However, there are agglomeration issues due to low melting point of Cu. To solve this issue, a new preparation method as well as a dispersion reagent and a thermal durability-enhanced reagent were applied simultaneously to the oxygen carrier. The carriers were synthesized using both wet and dry impregnation methods. Based on the initial oxygen loading capability tests, the dry impregnation method received additional investigation. The characterizations of the oxygen carriers were evaluated using thermogravimetric analyzer (TG), X-ray diffraction (XRD), scanning electron microscopy (SEM), and surface area analyzer. TG results demonstrate that the enhanced dry impregnation was an effective preparation method, where the mass loss of the oxygen carrier was typically 3.4 %, correlating to almost 17 % loaded CuO. XRD results indicate a new phase, $CuAl₂O₄$ spinel, formed after the first few redox cycles, which is responsible for promoting the thermal stability of the oxygen carriers. SEM results show that the addition of the dispersants decreased the agglomeration and the enhanced reagent chemicals greatly improved the strength of the carriers. However, the surface area of the

H. Zhao \cdot Y. Cao \cdot W. Orndorff \cdot W. Pan (\boxtimes)

Institute for Combustion Science & Environmental Technology, Western Kentucky University, Bowling Green, KY 42101, USA e-mail: Wei-ping.pan@wku.edu

H. Zhao e-mail: Hou-yin.zhao@wku.edu oxygen carriers decreased with the addition of the additives. In addition, with the increasing redox cycles, the surface area also decreased while the pore size increased, indicating that small pores were crushed, but the reactivity of the oxygen carriers did not decrease. In conclusion, the oxygen carriers produced in this manner are suitable for multi-cycle tests, and a major hurdle toward reducing greenhouse gases has been achieved.

Keywords Modified Cu-based oxygen carrier · TG · SEM - XRD - Surface area

Introduction

The increasing concentration of carbon dioxide has added to the greenhouse gas effect. Carbon dioxide capture and sequestration (CCS) technology has been pursued to reduce greenhouse gases. Chemical looping combustion (CLC) is one of the most promising CCS technologies with inherent separation of carbon dioxide and nitrogen [\[1–7\]](#page-5-0). CLC is carried out by cyclic reduction and oxidation of a metallic oxide, which acts as an oxygen carrier that is exchanged between two interconnected reactors [[3\]](#page-5-0). In the fuel reactor, the oxygen carrier is reduced by the fuel, and in the air reactor, the oxygen carrier is oxidized by the air. With this system, there is no direct contact between fuel and air $[1-5]$. The exit gas from the fuel reactor contains $CO₂$ and $H₂O$. If the water is condensed, concentrated $CO₂$ streams can be obtained with little energy lost for component separation, thus making CLC systems pivotal in the sequestration of CO2. During the reduction–oxidation cycles, the oxygen carrier plays a significant role, which needs high oxygentransfer capacity, reactivity, and favorable thermodynamics [\[1–10](#page-5-0)]. Many different metal-based oxides have been tested in the literature as potential candidates for CLC systems, for example, NiO, CuO, $Fe₂O₃$, and MnO, which are supported on different inert materials, such as Al_2O_3 , SiO_2 , yttrium stabilized zirconia (YSZ) or TiO₂ $[1-8]$. These supporting materials not only provide high surface area but also act as a binder for increasing mechanical strength and attrition resistance [[1,](#page-5-0) [5\]](#page-5-0). Different metal oxides, substrates, and preparation methods significantly influence the characterization of the oxygen carriers. Among these metal oxides, copper oxide has been chosen because of high reactivity and favorable thermodynamic behavior [[8–10\]](#page-5-0). In addition, γ -Al₂O₃ is used as the substrate due to its good fluidization properties and thermal stability [[11\]](#page-5-0). Many preparation methods, such as mechanical mixing [[1,](#page-5-0) [5](#page-5-0)], precipitation [\[12](#page-5-0)], spray drying $[13, 14]$ $[13, 14]$ $[13, 14]$, freeze granulation $[2, 4]$ $[2, 4]$ $[2, 4]$ $[2, 4]$ $[2, 4]$, impregnation [\[1](#page-5-0), [7](#page-5-0), [11](#page-5-0), [15–17](#page-5-0)], and sol–gel [\[18](#page-5-0), [19](#page-5-0)] have been used to prepare the oxygen carriers. Research shows that the impregnation method is one of the best methods for preparing the Cu-based oxygen carriers [[1,](#page-5-0) [15,](#page-5-0) [16](#page-5-0)]. In this method, the metal oxide is evenly dispersed on the supporting material, which enabled the oxygen carrier to exhibit high reactivity [\[1](#page-5-0), [15](#page-5-0), [16](#page-5-0)]. However, the copper-based oxygen carrier still faces the problem of a low melting point, which may cause agglomeration and accumulative thermal sintering problems after multi-cycle tests [[8–10\]](#page-5-0). Hence, solving these issues is an important step for widespread usage of Cu-based oxygen carriers. The addition of a dispersant agent and a thermal durability-enhanced reagent is necessary, which will reduce the agglomeration and enhance the thermal durability. In this paper, the dispersant reagent and thermal durability-enhanced reagent were added to the copper-based oxygen carrier during preparation and the characterization of the modified oxygen carrier, such as enhanced as well as used, were evaluated using TG, XRD, SEM, and surface area analyzer for determination of suitable in a CLC system.

Experimental

Oxygen carrier preparation

The oxygen carriers were prepared from γ -Al₂O₃ (Puralox NWa-155 Sasol Germany GmbH) and $Cu(NO₃)₂$ (Acros, USA). The effective method for preparing oxygen carriers is impregnation, including dry impregnation and wet impregnation [\[1](#page-5-0)]. For the wet impregnation method, the substrate γ -Al₂O₃ was immersed in a saturated solution of Cu(NO₃)₂ for 12 h, rinsed with DI water, and dried in an oven at 150 \degree C for 2 h. These procedures were followed by calcination at $500 \degree C$ in the oven for 5 h to assure the loaded copper compound was copper oxide (CuO). In the dry impregnation method, a solution of saturated $Cu(NO₃)₂$ and a small amount of thermal durability-enhanced reagent (lanthanum nitrate) and dispersant (citric acid) are mixed in a special ratio by mass for 12 h. Following mixing, the solution is applied to the substrate γ -Al₂O₃ until fully wetted, which took approximately 1 h. Then ethanol was continuously applied to the oxygen carrier for roughly 30 min and dried in the oven at 150 \degree C for 2 h. After removing from the oven, the oxygen carrier was treated again with the saturated $Cu(NO₃)₂$ solution followed by the ethanol treatment and 2 more hours at 150 \degree C. Subsequently, the oxygen carrier was calcinated in the oven at 500 \degree C for 5 h. The major difference between ''wet'' and ''dry'' methods is removal of moisture occupied inside the pore structure of supporting materials prior to doping procedures. In our process, ethanol was used to facilitate the removal of the moisture.

This study involved three types of oxygen carriers that were prepared according to the wet and dry impregnation methods. Based on the outcome of initial tests, a more complete analysis was performed on the dry impregnation method. The first type oxygen carrier labeled as CW was prepared using the wet method. The second type oxygen carrier labeled as CD was prepared using the dry method, without any additives. The third type oxygen carrier labeled as CD-en is prepared with the dry method, but is also augmented with enhanced reagents and dispersants.

Characterization

The amount of loaded CuO and the thermal stability of the modified oxygen carriers were performed on a TG (TA 2950, US). A 20 mg of sample was placed in a platinum pan and heated to 800 \degree C in nitrogen flow, and then exposed in a cyclic manner to a reducing gas of 10 $%$ H₂ for the reduction period and to air for the oxidation period. The temperature was kept at 800 °C during both reduction and oxidation periods, which were 300 s, respectively. N_2 was introduced for 600 s between periods to avoid mixing between H_2 and $O₂$. The total flow of the gas into the furnace was 100 mL min⁻¹ and a 10 % portion of the total gas flow, i.e., 10 mL min⁻¹ purge N_2 was introduced from the head of TG to keep the balance parts from any corrosive gas. The specific surface area and the pore size distribution of the oxygen carriers were obtained from a Micromeritics ASAP 2020 (Micromeritics Instruments Inc.), where the surface area was evaluated by BET equation in the relative pressure range of 0.05–0.35. The pore size and the pore size distribution were determined by BJH and DFT methods, respectively. The crystalline structures of the oxygen carriers were identified by a SCINTAG X'TRA AA85516 (ThermoARL) X-ray diffractometer equipped with a Peltier-cooled Si solid detector. Monochromatized Cu K_{α} (0.154 nm) was used as the radiation source. Diffraction patterns were collected at 45 kV–40 mA over 5° –90° (2 θ) at a step scan rate of

 1.20° min⁻¹. The microstructure of the oxygen carrier was determined by a JEOL JSM 5400-LV scanning electron microscope. The copper distribution in the cross-section was also determined by embedding the particle in resin, polishing to reveal cross-section, and then analysis by SEM.

Results and discussion

TG results

From Figs. 1, 2, and 3, it can be seen that the mass losses of CW, CD, and CD-en were 1.1, 3.8, and 3.4 %, respectively, which correlates to loaded CuO amount of 5.5, 19, and 17 %. Based on the threefold difference in oxygen carrying capacities, the rest of our studies were fully devoted to the dry impregnation method. The CuO content

Fig. 1 TG curves for the CW oxygen carrier

Fig. 2 TG curves for CD oxygen carrier

in CD was higher than that of CD-en, suggesting greater oxygen-transfer capacity. However, higher CuO content will lead to agglomeration issues [\[15](#page-5-0)]. The typical CuO amount was 17 % for CD-en. After 20 redox cycles of CD and 30 redox cycles of CD-en, both demonstrated good thermal stability, i.e., no further thermal degradation. However, there were small compositional differences between the CD and CD-en oxygen carriers after the multicycle tests. The original CD and CD-en oxygen carriers were both composed of CuO and γ -Al₂O₃; however, after the first few redox cycles, a new phase, $CuAl₂O₄$ spinel, formed (Fig. 4), which promoted the thermal stability of the oxygen carrier [\[1](#page-5-0), [15](#page-5-0)]. In addition, in CD oxygen carrier, another new phase was also formed, $Cu₂O$. This is probably because there were no dispersant reagents, and parts of the Cu agglomerated and emitted large amounts of

Fig. 3 TG curve for the CD-en oxygen carrier

Fig. 4 XRD spectrum for the oxygen carriers of CD and CD-en

Fig. 5 SEM image for CD and CD-en samples. a CD; b CD after 20 redox cycles-oxidation; c CD-en; d CD-en after 20 redox cycles-oxidation; e CD-en after 30 redox cycles-reduction; f cross section of CD-en; g cross section of CD-en after 20 redox cycles-oxidation

heat when reacted, which accelerated the decomposition of CuO (Fig. [4\)](#page-2-0). Moreover, the reduction of the oxygen carrier was an exothermic process, as a result, the temperature increased and CuO decomposed to $Cu₂O$. In the reduction process, even after 30 redox cycles, the product was only Cu, indicating that not only CuO but also $CuAl₂O₄$ were completely reduced by H_2 .

SEM results

The morphology change and the element distribution of the oxygen carrier were studied by SEM. It can be seen that the particle sizes were $\langle 10 \mu m$, and there were many holes on the surface of the oxygen carrier, indicating a higher surface area for the CD and CD-en (Fig. 5a–g). For the CD oxygen carrier, after 20 redox cycles, there was clear agglomeration on the surface of Al_2O_3 , which is exhibited by the dark spots (Fig. 5b). This further explains the compositional difference between CD and CD-en after 20 redox cycles. Based on the agglomeration problem for CD with\20 redox cycles further redox cycles were not attempted. For the CD-en carrier, the agglomeration decreased and the CuO particles were evenly distributed on the surface of the Al_2O_3 (Fig. 5c, d). After 30 reduction cycles, the copper was evenly distributed on the surface of Al_2O_3 (Fig. 5e). The images of the crosssection of the original CD-en and CD-en after 20 redox cycles were shown in Fig. 5f and g. It is noted that most of the CuO formed an outer layer on the surface of the Al_2O_3 and a small amount of CuO migrated into the center of the Al_2O_3 . After 20 redox cycles, the outer layer of the CuO attenuated, moreover, more CuO transferred into the pores of Al_2O_3 . This may be due in part to a chemical reaction or thermal displacement [[18\]](#page-5-0). However, even after 20 redox cycles, the holes can still be observed, indicating that the oxygen carrier was still porous and the reactivity of the oxygen carrier did not decrease even when there was some agglomeration.

Surface area results

The surface area and pore size also influence the reactivity of the oxygen carrier. After redox cycles, not only the surface area but also the pore size changed. Table [1](#page-4-0) shows that the surface area of the original γ -Al₂O₃ was $150 \text{ m}^2 \text{ g}^{-1}$, and original CD and CD-en were 116 and 105 m² g^{-1} , respectively, demonstrating that with the addition of additives, the surface area decreased. Moreover, with increasing redox cycles, the surface area of CD and CD-en both further decreased from 116 to 42 and 105 to

Table 1 Summarized surface area results for CD and CD-en oxygen carriers

Sample ID	Surface area/m ² g^{-1}	Pore size/nm	Pore volume/ $\rm cm^3~g^{-1}$
γ -Al ₂ O ₃	150	8.9	0.41
CD	116	8.9	0.30
CD 20th oxidation	42	17.7	0.20
CDen	105	9.4	0.30
CD-en 20th oxidation	42	18.8	0.19
CD-en 30th reduction	42	192	0.18

Fig. 6 Pore size distribution of CD and CD-en carriers

 $42 \text{ m}^2 \text{ g}^{-1}$, respectively. But, the average pore size of CD and CD-en increased from 9.0 nm to 17.7 and 18.8 nm, respectively, after 20 redox cycles, implying that some smaller pores were crushed, which may be due to thermal displacement or reactions [[18\]](#page-5-0). As a consequence, pore volume decreased. However, the decreased surface area

and increased pore size did not influence the reactivity of the oxygen carrier, which is confirmed by the TG results, Figs. [2](#page-2-0), [3](#page-2-0) refer. Actually, the pore size has a close relationship with the reactivity of the oxygen carrier. The pore size controls molecular diffusion, which contributes to the reactivity of the carriers. Large pore size promotes the diffusion of molecules to improve the reactivity of the oxygen carrier, but decreases the surface area. Thus, it reduces availability of active sites to reaction and decreases reactivity. So, there is a threshold for the pore size, where the pore size cannot be too large or small. This needs to be further studied. Figure 6a shows that the pore size distribution of both CD and CD-en shifted to the larger pore range. The pore size of CD and CD-en was initially distributed in 2–50 nm. However, after 20 redox cycles, the pore size of both carriers was shifted to 12–50 nm, further confirming that the micropores were crushed. Nevertheless, these pores were still in the mesopore size range, which may be attributed to the oxygen carrier's long lasting good reactivity. After 30 reduction cycles, the average pore size was 192 nm because of the reduction of copper oxide to Cu. Figure 6b also shows that in the reduction process, the pore size distribution was mainly in 130–500 nm, which is attributed to Cu.

Conclusions

The preparations of Cu-based oxygen carriers were compared using dry and wet impregnation methods. The characterizations of the modified oxygen carriers were evaluated using TG, XRD, SEM, and surface area analyzer. TG results show that enhanced dry impregnation was an effective preparation method, where the loaded CuO amount could reach up to 17 %. Moreover, even after 20 redox multi-cycles, the CD and CD-en demonstrated good thermal stability. XRD results exhibit the formation of a new phase, $CuAl₂O₄$ spinel, which promoted the thermal stability of the oxygen carrier. However, in the CD carrier, $Cu₂O$ was formed, which may be due in part to a deficiency of dispersant reagents. In the reduction process, the oxygen carriers were completely reduced to Cu. SEM results confirm that the deficiency of dispersant additives led to the agglomeration of the oxygen carriers. BET results point out that with the addition of the enhancers, the surface area of the oxygen carriers decreased. With increasing redox cycles, the surface area of the oxygen carrier decreased but the pore size increased, indicating that the small pores were crushed. The pore size distribution of the CD and CD-en both shifted from 2–50 to 12–50 nm after 20 redox cycles. However, the reactivity of the carriers did not decrease. In conclusion, CD-en is a good oxygen carrier that is suitable for multi-cycle tests.

Acknowledgements We gratefully acknowledge financial supports through projects by Cenovus, Canada and the United State Department of Energy (DE-FC26-FE0001808).

References

- 1. de Diego LF, Garcia-babiano F, Adanez J, Gayan P, Abad A, Corbella BM, Palacios JM. Development of Cu-based oxygen carriers for chemical-looping combustion. Fuel. 2004;83:1749–57.
- 2. Zafar Q, Abad A, Mattisson T, Gevert B. Reaction kinetics of freeze-granulated NiO/MgAl₂O₄ oxygen carrier particles for chemical-looping combustion. Energy Fuels. 2007;21:610–8.
- 3. Moghtaderi B, Song H. Reduction properties of physically mixed metallic oxide oxygen carriers in chemical looping combustion. Energy Fuels. 2010;24:5359–68.
- 4. Cho P, Mattisson T, Lyngfelt A. Comparison of iron-, nickel-, copper- and manganese-based oxygen carriers for chemicallooping combustion. Fuel. 2004;3:1215–25.
- 5. Adanez J, de Diego LF, Garcia-labiano F, Gayan P, Abad A. Selection of oxygen carriers for chemical-looping combustion. Energy Fuels. 2004;18:371–7.
- 6. Gu H, Shen LH, Xiao J, Zhang SW, Song T. Chemical looping combustion of biomass/coal with natural iron ore as oxygen carrier in a continuous reactor. Energy Fuels. 2011;25:446–55.
- 7. Mattisson T, Jardnas A, Lyngfelt A. Reactivity of some metal oxides supported on alumina with alternating methane and oxygen-application of chemical-looping combustion. Energy Fuels. 2003;17:643–51.
- 8. Cao Y, Pan WP. Investigation of chemical looping combustion by solid fuels. 1. Process analysis. Energy Fuels. 2006;20:1836–44.
- 9. Cao Y, Casenas B, Pan WP. Investigation of chemical looping combustion by solid fuels. 2. Redox reaction kinetics and product characterization with coal, biomass, and solid waste as solid fuels and CuO as an oxygen carrier. Energy Fuels. 2006;20:1845–54.
- 10. Cao Y, Li B, Zhao HY, Lin CW, Sit SP, Pan WP. Investigation of asphalt (bitumen)-fuelled chemical looping combustion using durable copper-based oxygen carrier. Energy Procedia. 2011;4: 457–64.
- 11. Dueso C, Aba A, Garci-labiano F, Diego LF, Gayan P, Adanez J, Lyngfelt A. Reactivity of a $NiO/Al₂O₃$ oxygen carrier prepared by impregnation for chemical-looping combustion. Fuel. 2010; 89:3399–409.
- 12. Gayan P, Dueso C, Aba A, Adanez J, Diego L, Garcia-labiano F. $NiO/Al₂O₃$ oxygen carriers for chemical-looping combustion prepared by impregnation and deposition–precipitation methods. Fuel. 2009;88:1016–23.
- 13. Moldenhauer P, Ryden M, Mattisson T, Lyngfelt A. Chemicallooping combustion and chemical-looping with oxygen uncoupling of kerosene with Mn- and Cu-based oxygen carriers in a circulating fluidized-bed 300 W laboratory reactor. Fuel Process Technol. 2012;104:378–89.
- 14. Jernadl E, Mattisson T, Thijs I, Snijkers F, Lyngfelt A. NiO particles with Ca and Mg based additives produced by spraydrying as oxygen carriers for chemical-looping combustion. Energy Procedia. 2009;1:479–86.
- 15. Diego LF, Gayan P, Garacia-Labiano F, Celaya J, Abad A, Adanez J. Impregnated $CuO/Al₂O₃$ oxygen carriers for chemicallooping combustion: avoiding fluidizing be agglomeration. Energy Fuels. 2005;19:1850–6.
- 16. Dennis JS, Muller CR, Scott SA. In situ gasification and $CO₂$ separation using chemical looping with a Cu-based oxygen carrier: performance with bituminous coals. Fuel. 2010;89:2353–64.
- 17. Zhao HY, Cao Y, Kang ZZ, Wang YB, Pan WP. Thermal characteristics of Cu-based oxygen carriers. J Therm Anal Calorim. 2012;109:1105–9.
- 18. Zhao HB, Liu LM, Xu D, Zheng CG, Liu GJ, Jiang LL. NiO/ NiAl2O4 oxygen carriers prepared by sol–gel for chemical-looping combustion fueled by gas. J Fuel Chem Technol. 2008;36:261–6.
- 19. Wang BW, Zhao HB, Zheng Y, Liu ZH, Yan R, Zheng CG. Chemical looping combustion of a Chinese anthracite with $Fe₂O₃$ based and CuO-based oxygen carriers. Fuel Process Technol. 2012;96:104–15.