



Synthesis of silver decorated silica nanoparticles with rough surfaces as adsorbent and catalyst for methylene blue removal

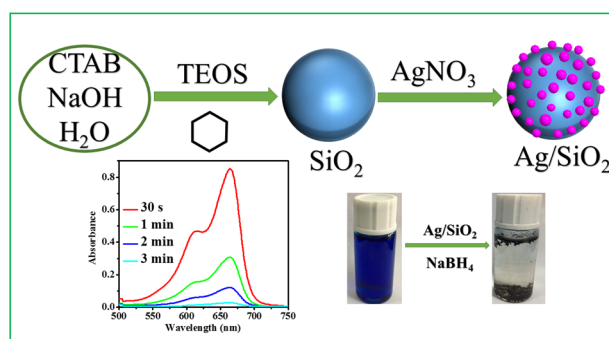
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Received: 3 September 2018 / Accepted: 29 October 2018 / Published online: 9 November 2018
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Abstract

The discharge of dyes from industries to water reservoirs has attracted extensive attention worldwide, and it is of great importance to remove them efficiently. In this study, a series of silica nanoparticles with rough surfaces was prepared, and highly dispersed silver nanoparticles were loaded on its surface through a simple wet-impregnation method. The adsorption performance and catalytic activity of the as-prepared Ag/SiO₂ for methylene blue (MB) removal was investigated. The results demonstrated that the Ag/SiO₂ with smaller particle size and higher Ag loading amount shows high adsorption capacity and catalytic activity for MB. The maximum adsorption capacity was found to be ~55 mg/g, which is more than two times of pure silica nanoparticles. Besides, MB could be degraded by more than 99% of the initial concentration (40 mg/L) within 3 min and rate constant of the catalytic reduction achieved as high as 2.128 min⁻¹. Moreover, the as-prepared Ag/SiO₂ shows good stability in acidic environment and excellent reusability for at least eight successive cycles of adsorption and four cycles of catalytic reduction.

Graphical Abstract



Highlights

- Highly dispersed Ag nanoparticles on rough surface of silica spheres were prepared.
- Ag decorated silica shows good adsorption and catalytic capability for MB removal.
- MB could be catalytically degraded to < 1% of the initial concentration within 3 min.

Electronic supplementary material The online version of this article (<https://doi.org/10.1007/s10971-018-4871-z>) contains supplementary material, which is available to authorized users.

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Keywords Silver decorated SiO₂ · Catalyst · Adsorption · Reduction · Methylene blue

1 Introduction

Water pollution caused by organic contaminants has posed a great threat to human life and health. Among many organic pollutants, organic dyes are receiving extensive attention because large numbers of industrial produced wastewater containing organic dyes were discharged into water body directly [1, 2]. Therefore, it is imperative to seek some ways to remove organic dye from water.

At present, various technologies have been exploited to remove organic dyes from water, such as adsorption [3, 4], catalytic oxidation [5–7], photocatalytic degradation [8, 9], membrane filtration [10], electrochemical method [11], and biological method [12]. Among them, adsorption and catalytic degradation are considered as the most effective and reliable technique for treatment of wastewater, due to its high efficiency, easy operation and relatively low cost etc. [13, 14]. Therefore, various adsorbents and catalysts are designed and developed to remove dyes from water, such as porous carbon [15], metal oxides [16], graphene oxide [17], Mg–Al layered double hydroxide [18], and mesoporous silica [19].

Recently, reduction of dyes into biodegradable pollutants in the presence of NaBH₄ was developed as a new and efficient technique for wastewater treatment [20–22]. And silver nanoparticles were found to be a good catalyst with excellent performance [23–25]. However, direct use of silver nanoparticle often suffer from their susceptibility to coagulation and agglomeration, moreover, silver is a precious metal and reducing the amount of silver used is one of the most effective ways to cut the cost. To overcome these shortbacks, immobilization of silver onto different support materials was developed as novel adsorbent or catalyst to remove organic dyes from water. Zhu et al. synthesized [26] silver-doped mesoporous silica fiber for methylene blue reduction; Lee et al. reported [27] the fabrication of silver nanoparticles decorated graphene–carbon sphere hybrid aerogel for adsorption of MB from water. Nasrollahzadeh et al. used [28, 29] seashell and perlite as the support for silver nanoparticles and investigated their catalytic activity for reduction of organic dyes. However, most of the reported composites are limited by relatively long degradation time or poor cyclic stability, which makes it challenging to recycle and reuse the adsorbents efficiently, further affecting their decontamination efficiencies in dye removal.

In this work, a series of silica spheres with rough surface were synthesized by controlling the formation time of silica. Then, silver nanoparticles were loaded onto the surface of

silica sphere through a wet-impregnation method. The above obtained Ag/SiO₂ composites were further used as adsorbent for MB removal from water, besides, its catalytic activity was studied by monitoring the reduction of MB by an excess of NaBH₄. The results showed that the Ag/SiO₂ composite exhibited good catalytic and adsorption properties for MB removal. In addition, it maintains good catalytic performance in a wide range of solution pH and exhibits good recycle stability.

2 Experimental details

2.1 Materials

All reagents used were of analytical grade and were purchased from Sinoreagent Company (Shanghai, China), including hexadecyltrimethylammonium bromide (CTAB), tetraethoxysilane (TEOS), cyclohexane, silver nitrate (AgNO₃), sodium borohydride (NaBH₄), NaOH, aqueous ammonia, ethanol, and Methylene blue (MB).

2.2 Synthesis of silica nanoparticles with rough surfaces

A series of silica nanoparticles with rough surfaces were synthesized according to Zhao et al. [30]. Typically, 1.0 g of CTAB and 0.8 mL of NaOH (0.1 M) were added into 50 mL of deionized water under stirring, and the solution was continuously stirred at 60 °C for 2 h. Then 20 mL of TEOS and 1 mL of cyclohexane mixture solution was added to the above solution and kept at 60 °C with stirring for 6, 12, 24, and 48 h, respectively. After that, the products were collected by centrifuging and washed by ethanol for three times. Then, the samples were dispersed in 50 mL of ethanol and refluxed at 70 °C for 12 h to remove CTAB. Finally, the products were washed with ethanol and dried in vacuum at 45 °C for 12 h. The as-prepared samples were marked as SiO₂-6, SiO₂-12, SiO₂-24, and SiO₂-48, respectively.

2.3 Synthesis of Ag/SiO₂ composites

The Ag decorated SiO₂ nanoparticles were synthesized by using wet-impregnation method. Typically, 100 mg of as-prepared SiO₂-6, SiO₂-12, SiO₂-24, or SiO₂-48 were dispersed in a mixed solution of 100 mL ethanol and 5 mL ammonia under stirring for 5 min, respectively, and then the solution was ultrasonication for 10 min. Afterwards, a

solution of 0.4 g of AgNO_3 dispersed in 20 mL ethanol was rapidly poured into the above mixture under continuous ultrasonication for 40 min. Finally, the obtained Ag/SiO_2 was washed three times with water and ethanol. The products were collected by centrifugation, and dried in vacuum for 12 h at 90 °C. The obtained samples were marked as Ag/SiO_2 -6, Ag/SiO_2 -12, Ag/SiO_2 -24, and Ag/SiO_2 -48, respectively.

2.4 Characterization

Powder X-ray diffraction patterns (XRD) were recorded by a Bruker D8 ADVANCE diffractometer with Cu K- α radiation (40 KV, 30 mA). The morphology of the samples was examined using scanning electron microscope (SEM) (FEI Quanta 400 FEG) and transmission electron microscope (TEM) (FEI Tecnai G2 F20). N_2 adsorption–desorption experiments were performed in a Quantachrome iQ2 porosimeter after degassing the samples at 100 °C for 12 h. The Brunauer–Emmet–Teller (BET) method was used to calculate the specific surface area. Content of silver in the composite materials were analyzed by using inductively coupled plasma optical emission spectrometry (ICP-MS, Agilent 7900). X-ray photoelectron spectrum (XPS) measurements were performed on a Thermo Scientific Escalab 250Xi instrument equipped with Al K α radiation. Thermogravimetric analysis (TGA, Netzsch STA 449 F5) was performed under Ar gas at a flow rate of 100 cm^3/min . The sample was heated from 30 to 800 °C with a temperature ramp rate of 10 °C/min. FT-IR spectra were collected by a Thermo Nicolet iS5 spectrometer in transmission mode over the range of 4000–400 cm^{-1} . The zeta potential of the sample at different solution pH was determined by a Brookhaven Zeta-PALS instrument.

2.5 Adsorption experiment

The MB adsorption isotherms were acquired by the adsorption measurements performed with 5 mg of solid samples dispersed in a series of 25 mL of solutions with different MB concentrations (10 mg/L–50 mg/L) under stirring for 12 h at 25 °C. At the end of adsorption, the solution was collected by filtration, and the concentration of MB was measured with an UV–Vis spectrophotometer (TU-1810, Persee Co., China). The capacity of MB adsorbed onto the samples was calculated using the following equation:

$$q_e = \frac{(C_0 - C_e)V}{M}$$

where q_e is the capacity of MB adsorbed at equilibrium; C_0 and C_e are the initial and equilibrium concentration of

MB, respectively; V is the volume (L) of solution; and M is the sample weight used.

2.6 Catalytic reduction of MB

Catalytic reduction of MB was conducted in a beaker containing 10 mg of sample dispersed in 20 mL of MB aqueous solution (40 mg/L) with 1 mL of fresh NaBH_4 aqueous solution (0.1 mol/L) injected under stirring. The concentration of MB in solution was monitored by measuring the absorbance values at 665 nm using a UV–Vis spectrophotometer.

The catalytic degradation fraction of the dyes can be expressed in the following equation:

$$\text{Dye removal (\%)} = \frac{A_0 - A_t}{A_0}$$

where A_0 is the absorbance of MB solution before reaction and A_t is the absorbance of MB at time t of the catalytic reaction. The reaction rate constant k_{app} was calculated using the pseudo-first-order kinetics equation:

$$\ln \frac{A_t}{A_0} = -k_{\text{app}}t$$

3 Results and discussion

3.1 Characterization of materials

Figure 1 shows the XRD patterns of Ag/SiO_2 composites. A wide diffraction peak at $\sim 22.8^\circ$ (2θ) corresponding to the amorphous SiO_2 could be observed for all samples [31]. Moreover, four diffraction peaks located at $2\theta = 38.36^\circ$, 44.32° , 64.58° , and 77.51° can be ascribed to (111), (200), (220), and (311) planes of silver crystals, respectively,

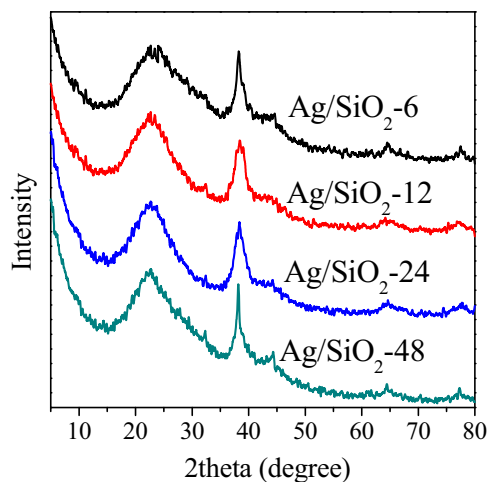


Fig. 1 XRD patterns of Ag/SiO_2 samples

indicating the existence of silver crystals with face centered cubic structure in the composites [32, 33]. The Ag content in Ag/SiO₂ composites analyzed by ICP were 3.5 wt%, 4.9 wt%, 6.7 wt%, and 6.0 wt% for Ag/SiO₂-6, Ag/SiO₂-12, Ag/SiO₂-24, and Ag/SiO₂-48 samples, respectively (Table 1).

The morphology of different SiO₂ and Ag modified SiO₂ was characterized by TEM and SEM. For pure SiO₂, particles with rough surfaces could be seen for all samples (Fig. S1). With increasing hydrothermal time from 6 to 48 h during the synthesis, the diameter of SiO₂ particles increased. However, the particle size barely changed with further increase of hydrothermal time. For Ag decorated silica (Fig. 2), the morphology was not much different from their parent silica, except the appearance of small black dots, which could be convinced that these dots are silver particles. With the increase of hydrothermal time of silica from 6 to 48 h, the content of silver in the Ag/silica composite slightly increased, and the particle size increased from ~25 to ~101 nm, while the size of silver particle in all Ag/silica were found to be ~10 to ~13 nm. According to the

high-resolution TEM picture and energy-dispersive X-ray spectroscopy (EDX) results (Fig. 2e, f), detectable Ag in Ag/SiO₂-48 sample further confirmed that silver was loaded onto silica successfully. (Note that Cu peaks came from the TEM grid.) Furthermore, SEM (Fig. 3a–d) images show that all samples have similar sphere-like shapes with rough surfaces. Among these samples, Ag/SiO₂-24 was selected for further analysis by using EDX elemental mapping (Fig. 3e–h). The result shown in Fig. 3h reveals that silver atoms are homogeneously dispersed on the surface of SiO₂ matrix.

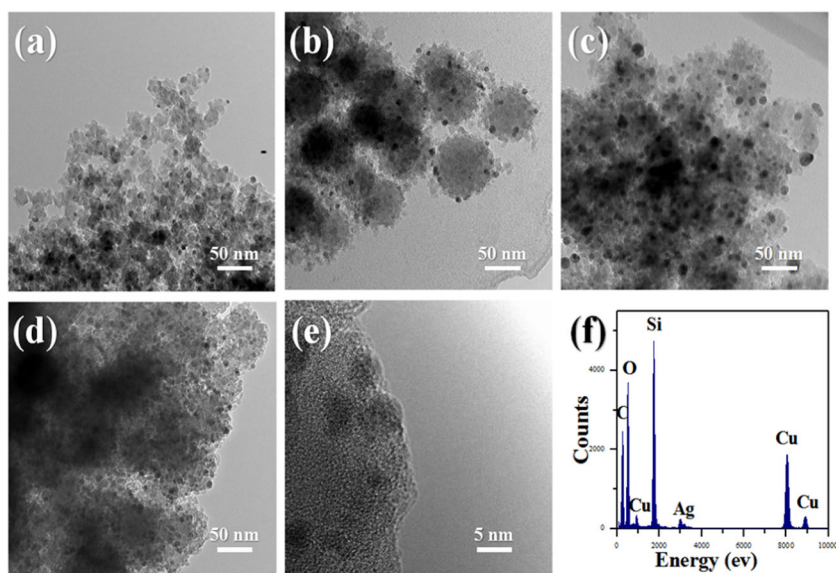
Figure 4a and S2a displayed N₂ adsorption–desorption isotherms of Ag/SiO₂ and SiO₂ samples. Clearly, all Ag/SiO₂ and SiO₂ samples exhibited type IV isotherm, which is characteristic of mesoporous material [34, 35]. There is a decrease of surface area and pore volume for all composites after silver impregnation as revealed in Table 1. The pore size distributions of different Ag/SiO₂ and SiO₂ materials were analyzed by NLDFT method. All the Ag/SiO₂ samples showed similar pore size distributions compared with their parent silica (Fig. S2b and Fig. 4b). It can also be seen that pore size of the Ag/SiO₂ composites decreased slightly with increased formation time of silica. The pore size distribution of Ag/SiO₂-6 sample is much different with other Ag/SiO₂ samples. It has mesopores with a size centered at around 43 nm. The relatively large pore size may cause the easy pour of the Ag precursor, thus, the Ag content in the resulting samples are relatively low.

To further investigate the valence state of different species on SiO₂ samples, XPS analysis was conducted and the results are shown in Fig. 5. All of the peaks on the survey spectrum of Ag/SiO₂-24 composite can be assigned to Ag, O, and Si elements, which is well consistent with the EDX analysis. Two peaks at ~368 eV and ~374 eV in the high-resolution XPS spectrum of Ag 3d region can be assigned to

Table 1 Surface area, porosity data and Ag content of Ag/SiO₂ samples

Samples	S _{BET} (m ² /g)	V _t (cm ³ /g)	W _{Ag} /W _{sample} (wt%)
Ag/SiO ₂ -6	216	0.80	3.5
Ag/SiO ₂ -12	210	0.77	4.9
Ag/SiO ₂ -24	208	0.76	6.7
Ag/SiO ₂ -48	199	0.66	6.0
SiO ₂ -6	292	1.09	0
SiO ₂ -12	218	0.81	0
SiO ₂ -24	262	0.91	0
SiO ₂ -48	261	0.76	0

Fig. 2 TEM images of **a** Ag/SiO₂-6, **b** Ag/SiO₂-12, **c** Ag/SiO₂-24, **d–e** Ag/SiO₂-48, and **f** EDX analysis of the Ag/SiO₂-48



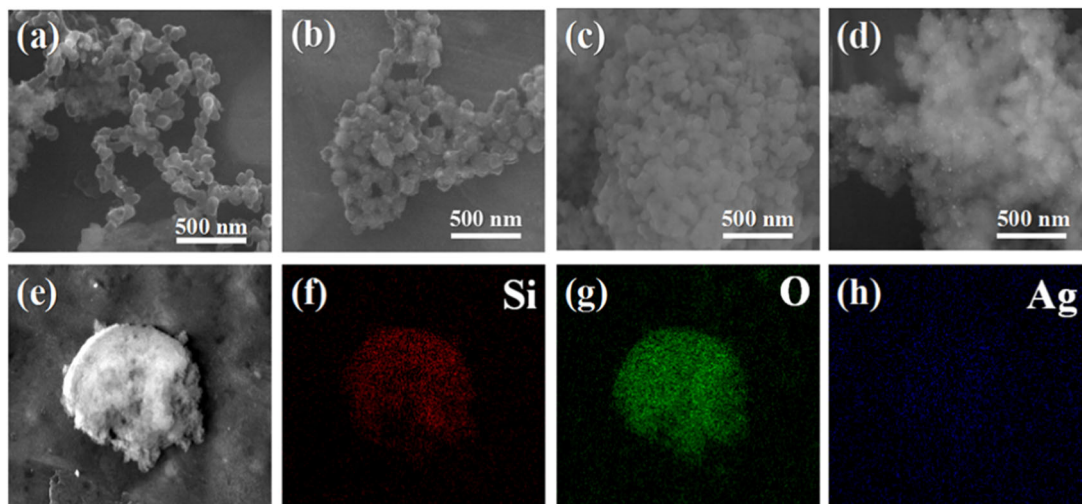


Fig. 3 SEM images of **a** Ag/SiO₂-6, **b** Ag/SiO₂-12, **c** Ag/SiO₂-24, **d** Ag/SiO₂-48, and **e–h** elemental mapping images (9223× magnification) of the Ag/SiO₂-24

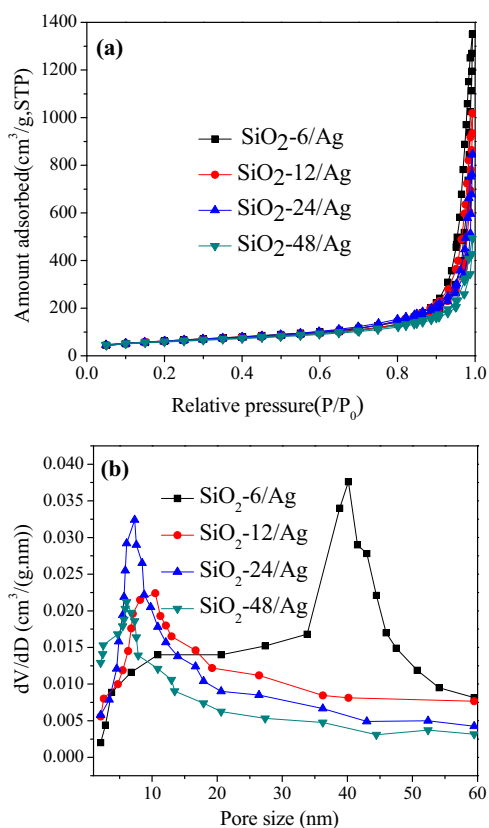


Fig. 4 **a** Nitrogen adsorption–desorption isotherms and **b** pore size distributions of Ag/SiO₂ samples (NLDFT method)

Ag 3d_{5/2} and Ag 3d_{3/2}, indicating the formation of metallic Ag⁰ at surface of Ag/SiO₂-24 sample [24].

TG curves of SiO₂ and Ag/SiO₂-24 samples were shown in Fig. S3, little weight change caused by desorption of

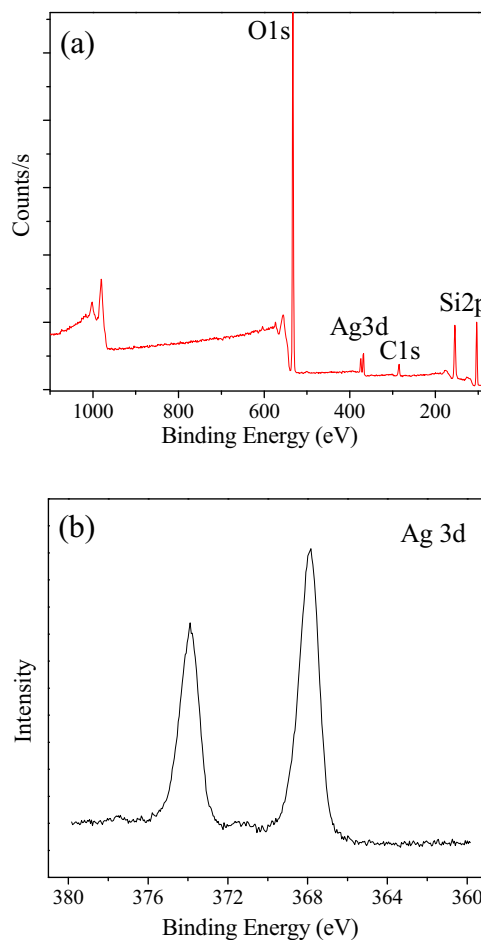


Fig. 5 XPS survey **a** and high-resolution Ag 3d spectra **b** of Ag/SiO₂-24 sample

moisture can be seen for both samples, which indicates the high thermal stability of the samples.

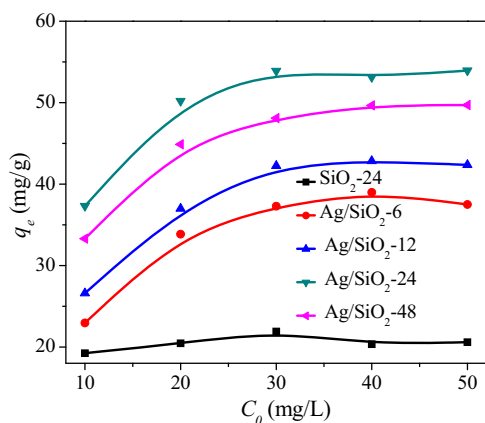


Fig. 6 Adsorption isotherms of MB onto different samples. (MB concentration = 10–50 mg/L, solution volume = 25 mL, Ag/SiO₂ = 5 mg, $T = 25\text{ }^{\circ}\text{C}$)

Table 2 Comparison of adsorption capacity for MB with different silver composites

samples	MB volume (mL)	adsorbent (g/L)	Ag content (g/L)	adsorption capacity (mg/g)
Ag/SiO ₂ -6	25	0.2	0.007	37
Ag/SiO ₂ -12	25	0.2	0.0098	42
Ag/SiO ₂ -24	25	0.2	0.013	55
Ag/SiO ₂ -48	25	0.2	0.012	49
SiO ₂ -24	25	0.2	0	20

3.2 Adsorption of MB

The adsorption capacities of the as-synthesized composites at different MB concentration were tested and the results are shown in Fig. 6. With the increase of MB concentration in solution, the adsorption capacity of all samples increased at first and then gradually achieved a constant value finally. Only tiny amount of MB (~20 mg/L) was adsorbed by pure SiO₂-24. With the decoration of Ag, adsorption capacity of all the composites increased significantly. Among all the composites, Ag/SiO₂-24 exhibited the highest adsorption capacity with a value of ~55 mg/g, which is more than two times of pure SiO₂. The high adsorption capacity should be contributed by its high Ag loading (Table 2), which provides more adsorption sites for MB [24].

The effect of pH values on the adsorption of MB onto Ag/SiO₂-24 samples was further conducted. The removal efficiency at different pH as a function of adsorption time is shown in Fig. 7 and the corresponding successive UV–Vis spectra can be seen in Fig. S4. With the increase of solution pH from 3 to 11, the removal efficiency of Ag/SiO₂-24 increased gradually. This behavior could be associated with the electrostatic interaction between Ag/SiO₂-24 and MB. According to the results shown in Fig. S5, Ag/SiO₂-24 is

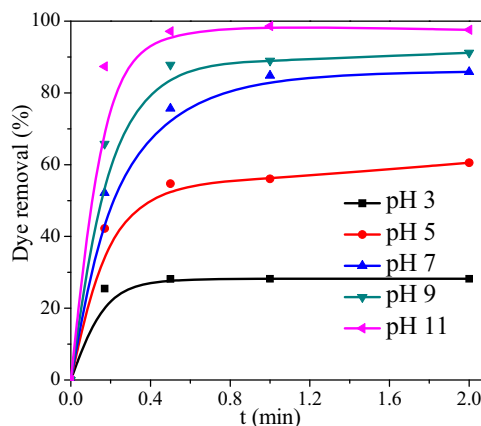


Fig. 7 Fraction of degraded dye for adsorption of MB by Ag/SiO₂-24 sample under various pH conditions. (MB = 10 mg/L, solution volume = 20 mL, Ag/SiO₂-24 = 10 mg, $T = 25\text{ }^{\circ}\text{C}$)

negatively charged in the solution with pH value >3, moreover, absolute value of the negative zeta potential of Ag/SiO₂-24 improved with increasing pH value of the solution. Consequently, more electronegative charges were formed on the surface of Ag/SiO₂-24, meanwhile, there were less competition between H⁺ and positively charged MB cations during adsorption as the solution PH increased. As a result of this, the adsorption capacity of Ag/SiO₂-24 increased [36, 37].

The recyclability of Ag/SiO₂-24 for MB adsorption was also evaluated. After adsorption, Ag/SiO₂-24 was collected by centrifugation, washed with fresh NaBH₄ solution (1.5 mmol/L) and ethanol solution several times. It can be seen from Fig. S6 that the Ag/SiO₂-24 material still maintained high MB removal efficiency with more than 99% of MB removed even after eight cycles of adsorption–desorption.

3.3 Catalytic reduction of MB

The catalytic reduction of MB with an excess amount of NaBH₄ was selected as a model reaction to test the catalytic performance of different Ag/SiO₂ samples. The reaction can be easily monitored by the color change of MB solution after addition of composite sample and NaBH₄. Figure 8a shows that all the Ag decorated samples exhibit good catalytic reduction activity for MB, with much higher removal efficiency than that of pure SiO₂ sample. Among those silver containing samples, Ag/SiO₂-24 shows the fastest reduction kinetics, i.e. a completed catalytic reduction of MB within 3 mins (Fig. 9b, c) and removal efficiency > 99%. Comparatively, the time used for complete catalytic reduction using Ag/SiO₂-6, Ag/SiO₂-12, and Ag/SiO₂-48 were 18, 13, and 7 min under the same conditions (Fig. 8a and S7). The catalytic activity based on the Ag content was calculated and listed in Table 3. It could be seen that the higher content of silver, the faster reaction rate was obtained

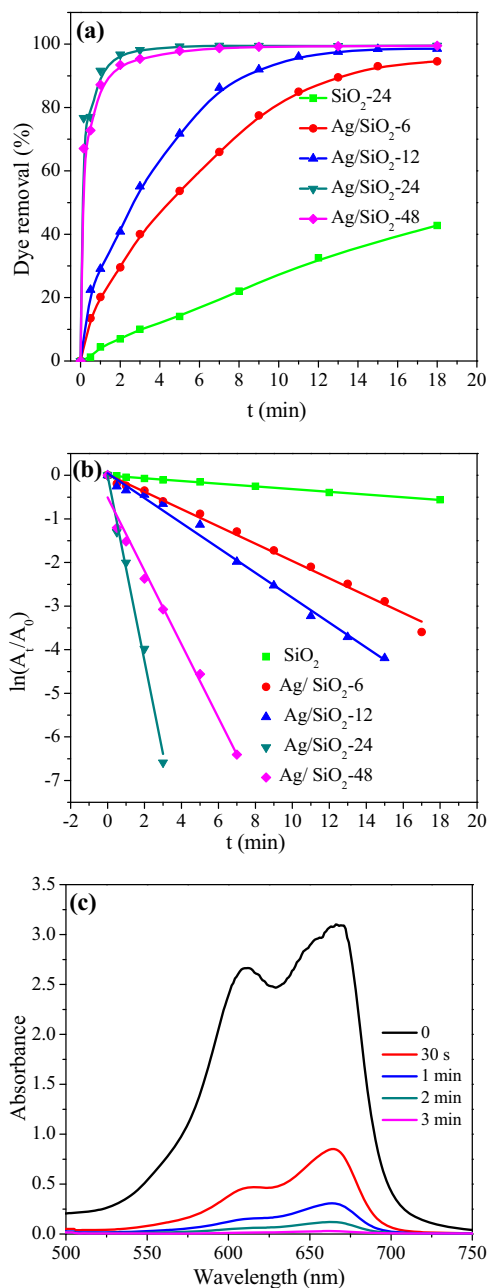


Fig. 8 **a** Fraction of dye degradation during the catalytic reduction of MB. **b** First-order kinetic plot of catalytic MB reduction in the presence of SiO₂-24 and various Ag/SiO₂ samples. **c** Successive UV-Vis spectra for MB reduction with Ag/SiO₂-24 sample. (MB = 40 mg/L, NaBH₄ = 0.1 mol/L, solution volume = 20 mL, sample mass = 10 mg, *T* = 25 °C)

over the corresponding sample, since the silver nanoparticles act as the catalytic sites in the reaction, consequently more active sites were present on the sample with higher Ag content (the particle size of Ag on those samples are very close).

For further analyze the reaction mechanism, pseudo-first-order kinetics model was attempted for simulation for the

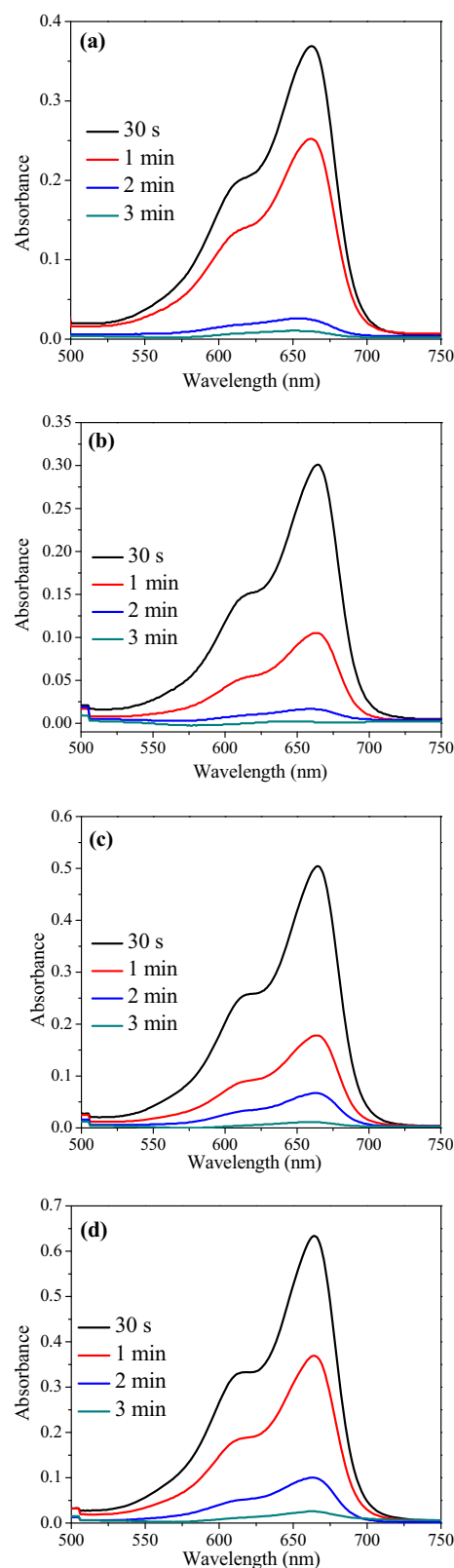
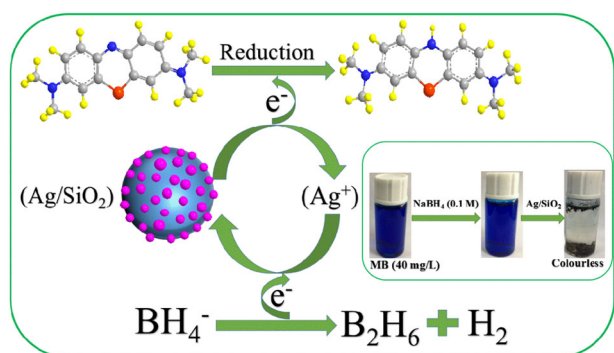


Fig. 9 Successive UV-Vis spectra for catalytic reduction of MB by NaBH₄ and Ag/SiO₂-24 sample at **a** pH 3, **b** pH 7, **c** pH 9, and **d** pH 11. (MB = 40 mg/L, NaBH₄ = 0.1 mol/L, solution volume = 20 mL, Ag/SiO₂-24 = 10 mg, *T* = 25 °C)

Table 3 Comparison of rate constants for degradation of MB with different silver composites

Samples	MB/NaBH ₄ (mol/mol)	Catalyst (g/L)	Ag content (g/L)	Rate constant (k_{app}/min^{-1})	R^2	References
Ag/Tr-SBA-15	1/40	0.5	–	0.858	–	[21]
Ag/AMT-SBA-15	1/40	0.5	–	0.564	–	[21]
Fe ₃ O ₄ @PDA-Ag	1/40	0.5	–	0.430	0.987	[24]
Ag/SiO ₂ -6	1/40	0.5	0.018	0.199	0.993	This work
Ag/SiO ₂ -12	1/40	0.5	0.025	0.285	0.993	This work
Ag/SiO ₂ -24	1/40	0.5	0.034	2.128	0.990	This work
Ag/SiO ₂ -48	1/40	0.5	0.030	0.843	0.982	This work
SiO ₂ -24	1/40	0.5	0	0.032	0.995	This work

**Fig. 10** Mechanism of the catalytic reduction of MB by NaBH₄ and Ag/SiO₂ samples

constant concentration and excessive amount of NaBH₄ presented. A linear relationship could be observed between $\ln(A_t/A_0)$ vs. time plots for all samples in Fig. 8b. The rate constants of MB catalytic reduction were calculated to be 0.199, 0.285, 2.128, and 0.842 min^{-1} at 25 °C for Ag/SiO₂-6, Ag/SiO₂-12, Ag/SiO₂-24, and Ag/SiO₂-48 samples, respectively (Table 3). Obviously, k_{app} value of Ag/SiO₂-24 was much higher than other samples, possibly owing to a higher Ag content in Ag/SiO₂-24. Moreover, a comparison of the values (Table 3) reveals that Ag/SiO₂-24 shows significant higher k_{app} value compared with the catalyst reported in literature. Thus, Ag/SiO₂-24 sample was selected for further analysis because of its superior catalytic activity.

To explore the effect of solution pH on catalytic degradation of MB with Ag/SiO₂-24 sample, MB solutions with four different pH values (pH = 3, 7, 9, 11) were prepared for the study. It could be clearly seen (Fig. 9) that there is little change in catalytic activity of Ag/SiO₂-24 in the solution with pH range of 3–11, with removal efficiency for MB up to >99% within 3 min, indicating that Ag/SiO₂-24 can maintain high catalytic activity in a wide range of solution pHs.

The electron transfer effect can be used to explain the catalytic reduction of dye by Ag/SiO₂ composites [38–41]. Silver is a good conductor and can transfer electrons

between donors and receptors. Therefore, this catalytic process can be mediated by silver nanoparticles through redox mechanism, and electrons can be transferred from donor (BH₄[−]) to the acceptor (MB) [24, 42]. Figure 10 displays the illustration of general reduction of MB in the presence of Ag/SiO₂ and NaBH₄. Firstly, NaBH₄ and MB were adsorbed onto the surface of Ag/SiO₂. Then, electrons can be transferred from BH₄[−] to MB with the help of Ag catalyst, resulting in the reduction of MB into LMB (leucomethylene blue) (Fig S8). Finally, LMB spontaneously desorbed from the surface of Ag/SiO₂ and diffused into the solution due to weaker electrostatic action between Ag/SiO₂ and LMB [33, 38].

3.4 Catalyst stability

The recyclability of catalytic materials is an important standard for practical application. Figure 11a shows that the Ag/SiO₂-24 sample displays good recycle performance with extremely high removal efficiency for MB even after four cycles of catalytic reduction. Moreover, there is little change in XRD diffraction patterns before and after reaction (Fig. 11b), demonstrating that structure of the materials was well reserved after catalytic runs. FT-IR spectra were collected to further explore the surface functional groups of Ag/SiO₂-24 before and after reaction (Fig. 11c). The peaks at 800 cm^{-1} (Si-O-Si), 959 cm^{-1} (Si-OH), and 1098 cm^{-1} (Si-O-Si) remained unchanged, indicating the stable surface functional groups of the materials.

This study also evaluated the stability of Ag/SiO₂ in strong acidic environment. After 24 h of continuous stirring of 10 mg of Ag/SiO₂-24 dispersed in 20 ml of deionized water with pH values of 2 or 3, the concentrations of silver ion in the solution were measured by inductively coupled plasma mass spectrometry (ICP-MS, Agilent 7900). The data shown in Table 4 revealed that only about 1.3% and 0.6% of silver in Ag/SiO₂-24 composite was leached out in the environment of pH = 2 and pH = 3, respectively. This result suggested that Ag/SiO₂ can possibly be applied in strong acidic environment owing to its high stability.

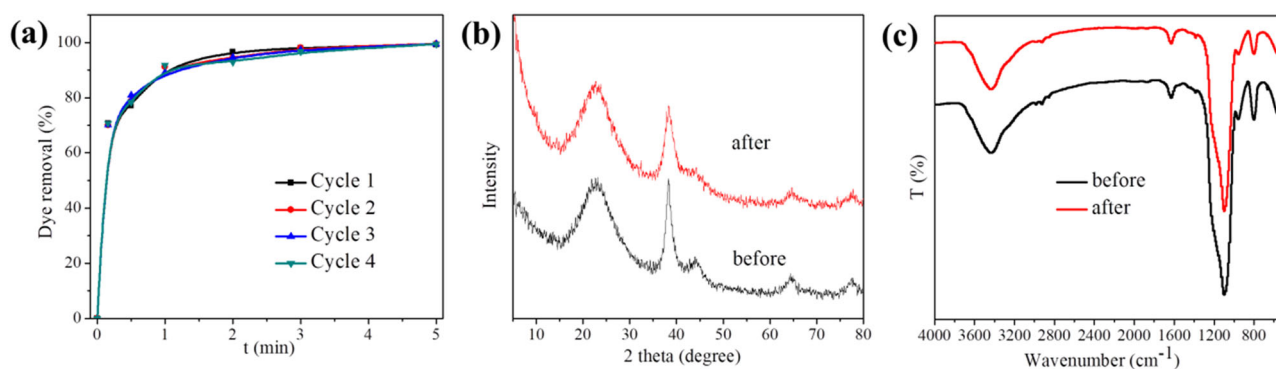


Fig. 11 **a** Recyclability of Ag/SiO₂-24 sample during the catalytic reduction of MB with NaBH₄ (MB = 40 mg/L, NaBH₄ = 0.1 M, sample = 0.5 g/L, T = 25 °C), **b** XRD patterns, and **c** FT-IR spectra of Ag/SiO₂-24 before and after catalytic reduction of MB

Table 4 Silver precipitation of Ag/SiO₂-24 composite under acid conditions

Sample	pH	C _{Ag+} (mg/L)	W _{Ag+} /W _{Ag in sample} (%)
Ag/SiO ₂ -24	2	0.44	1.3
Ag/SiO ₂ -24	3	0.21	0.6

4 Conclusions

In summary, highly dispersed silver nanoparticles on rough surface of silica spheres were prepared through simple sol-gel and wet-impregnation methods. These Ag decorated silica shows good adsorption and catalytic capability for MB removal. Among these composites, Ag/SiO₂-24 nanoparticles showed highest MB adsorption capacity of ~55 mg/g and catalytic activity for the reduction of MB with an excess of NaBH₄. MB could be catalytically degraded to <1% of the initial concentration within 3 min and the rate constant could be as high as 2.128 min⁻¹. The Ag/SiO₂-24 nanoparticle can also be used in environment with wild range of pH values. Moreover, the as-prepared Ag/SiO₂-24 exhibited excellent reusability for at least 8 cycles of adsorption and 4 cycles of catalytic reduction.

Acknowledgements This work was supported by the Fundamental Research Funds for the Central Universities (No. 2018XKQYMS18) and the Priority Academic Program Development of Jiangsu Higher Education Institutions.

Compliance with ethical standards

Conflict of interest The authors declare that they have no conflict of interest.

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