

Comparison of adsorption of U(VI) by magnetic MCM‑41, MCM‑48 and SBA‑15 mesoporous silicas

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Abstract

Three types of magnetic mesoporous silicas (MMSs), namely, MMCM-41, MMCM-48 and MSBA-15 were prepared by a hydrothermal method using CTAB and P123 as templates. The structure and physicochemical properties of MMSs were characterized by small angle XRD, VSM, ζ potential analyzer, contact angle measurer, and XPS, etc. The potential applications of MMSs in U(VI) recovery were thoroughly investigated. The adsorptive kinetics, thermodynamics, and selectivity of MMCM-41, MMCM-48 and MSBA-15 were compared. The results show that MSBA-15 revealed a high capacity for U(VI) $(341.94 \text{ mg} \cdot \text{g}^{-1})$ and a superior selectivity than MMCM-41 and MMCM-48. The adsorption mechanism was explored by using the relevant adsorption models and XPS. The results indicated that MSBA-15 could be considered a strong candidate for the adsorption and recovery of U(VI) from radioactive wastewater.

Keywords Uranium · Adsorption · Magnetic mesoporous silicas

Introduction

Uranium is a primary and valuable constituent of nuclear fuel of pressurized water reactor $[1]$ $[1]$ $[1]$. Additionally, $U(VI)$ is a highly toxic and radioactive metal ion [[2\]](#page-12-1), even in trace amounts, can harm organs such as the kidneys, liver, and bones [[3\]](#page-12-2), etc. Uranium-containing wastewater may have generated during nuclear fuel fabrication including mining, hydrometallurgy, and conversion. Therefore, there is an urgent need to efficiently eliminate and reuse uranium from contaminated water [[4](#page-12-3)].

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Among numerous techniques for U(VI) capture, adsorption is considered the most favorable owing to its high efectiveness, simple operation, and lack of secondary pollution. Moreover, fostering a high efficient adsorbent is the key for this certain objective. Mesoporous silicas (MSs) has attracted increasing attentions for their excellent properties, such as remarkable stability, controllable pore diameter, high specific area $[2]$ $[2]$, rich in porosity $[5]$ $[5]$. Many MSs adsorbents have been applied into recovery of U(VI) from wastewater, including MSs functionalized with phosphonate [\[6\]](#page-12-5), amidoxime [[7](#page-12-6)], and amino groups [\[8\]](#page-12-7).

As a kind of nano-adsorbent, the MMs are found to be difficult to recovery from aqueous solution $[9]$ $[9]$. With strong magnetic responsivity [[10\]](#page-12-9), magnetic mesoporous silicas (MMSs) have tremendous potential in the felds of U(VI) adsorption $[10-12]$ $[10-12]$, which can easily separation from water by an external magnetic feld. But, the MMSs matrix applied in removal of U(VI) were diferent, such as magnetic MCM-41 [[2](#page-12-1)], and magnetic SBA-15 [\[13](#page-12-11)].

Herein, the adsorptive performances for U(VI) at MMSs were compared. Firstly, magnetic MCM-41, MCM-48 and SBA-15 were synthesized using a hydrothermal method. The structure and physicochemical properties of three kinds of MMSs were characterized by small angle XRD, VSM, ζ potential analyzer, contact angle measurer, and XPS, etc.

The adsorption mechanism was clarifed by using the relevant adsorption models, FT-IR and, XPS.

Experimental

Reagents and instruments

Ferric chloride hexahydrate (AR), chloroacetic acid (AR), sodium fuoride (AR), and anhydrous sodium acetate (AR) were obtained from Shanghai Macklin Biochemical Technology Co., Ltd. P123 (MW 5800) was acquired from Sigma Aldrich (Shanghai) Trading Co., Ltd. Cetyltrimethylammonium bromide (CTAB, AR), Arsenazo III (AR), and TEOS (AR) were sourced from Shanghai Aladdin Biochemical Technology Co., Ltd.

The equipment used in the study included centrifuge (TG12-WS, Shanghai Spectral, China), XRD instrument (D8 ADVANCE, Bruke, Germany), FT-IR spectrometer (Nicolet iS5, Thermo Fisher, USA), FEI-TEM (Tecnai F20, FEI, USA), XPS (K-alpha, Thermo Fisher, USA), Vibrating sample magnetometer (VSM) (7404 type, Lakeshore, China), Particle potential titration analyzer (Stabino, PMX, Germany), and an automatic gas adsorption system (ASAP2020, Micromeritics, USA).

Preparation of magnetic mesoporous silica

Preparation of Fe₃O₄@ SiO₂ (MNPS)

The Fe₃O₄@SiO₂ composite was synthesized using a sol–gel method. 0.30 g of $Fe₃O₄$ was dispersed in a 70.0 mL ethanol–water solution ($V_{\text{ethanol}}/V_{\text{water}}=6/1$). After ultrasonic treatment for 10 min, 2.0 mL of TEOS and 1.0 mL of ammonia solution were introduced. The solution was mechanically stirred at 25 °C for 10 h. Then, wash it with water and ethanol for three times, separate the product with external magnetic feld, and dry it at 60 °C.

Preparation of MMSs

The preparation route for the MMSs is illustrated in Fig. [1.](#page-1-0) Initially, a mixture comprising 1.50 g of MNPS, 50.0 mL of H_2O , and 5.0 mL of $NH_3·H_2O$ was subjected to oscillation using an ultrasonic cleaner for 30 min. After adding 10 mL of TEOS, 0.90 g of NaOH, and 0.19 g of NaF, the resulting mixture was then mechanically blended at 25 °C for 2 h. Subsequently, 3.00 g of CTAB was introduced, and the stirring process was continued for an additional 2 h. After thorough mixing, the resulting solution was transferred to a reaction kettle and aged at 100 °C for 48 h. The obtained product was subjected to washing and dried at 60 °C for 12 h. Finally, the product underwent calcination at 300 °C for 3 h to yield the ultimate product MMCM-41. The preparation of MMCM-48 followed the same procedure, with the only diference being the use of 7.0 g of CTAB.

In a separate process, 4.00 g of P123 and 0.05 g of NH_4F were dissolved in 138.0 mL $H₂O$ and 1.2 mL concentrated hydrochloric acid within a three-neck fask. The solution underwent ultrasonication for 10 min after the addition of 0.60 g of $Fe₃O₄@SiO₂$. Afterthat, 9.0 mL of TEOS was introduced into the fask, and the solution was stirred at 40 °C and then at 100 °C for 24 h each. The resulting flter residue was obtained after washing with H_2O and subsequent dehydration at 60 °C for 24 h. The fnal product, MSBA-15, was achieved through calcination at 550 °C for 6 h.

U(VI) adsorption experiment

The adsorption properties of the MMSs for U(VI) were investigated using a batch experiment. In a conventional adsorption procedure, 50 mL of U(VI) solution was introduced into a 150 mL conical fask and adjusted to a fxed

Fig. 1 Schematic synthesis diagram of magnetic mesoporous silicas

pH value with NaOH and $HNO₃$ solutions. The conical flask with 50 mL solution and 10.0 mg of adsorbent was shaken for a certain time. Then, the U(VI) concentration of supernatant was determined by an Arsenazo III spectrophotometry. Finally, the amount of U(VI) adsorbed [\[14](#page-12-12), [15\]](#page-12-13) $(q, mg·g^{-1})$ and the distribution coefficient $[16]$ $[16]$ (K_d , mg·mL⁻¹) were calculated by the Eq. S1 and S2, respectively.

Selective experiment

Weighed amounts of $Zn(NO_3)$ ²·6H₂O, Co(NO₃)²·6H₂O, $Sr(NO₃)₂$, $Pb(NO₃)₂$, $Ni(NO₃)₂·6H₂O$, $Ce(NO₃)₃·6H₂O$, $Gd(NO₃)₃·6H₂O$, and $La(NO₃)₃·6H₂O$ were ultrasonically dissolved in a beaker. And, the mixture with 10 mL of 5 g·L−1 U(VI) solution was diluted to 1 L volume by deionized water. The concentration of these ions in the prepared solution was 50 mg·L−1. After shaking for 240 min, 10 mL of supernatant was taken and added with 2.5 mL of $HNO₃$ solution (2 mol⋅L⁻¹). Finally, the residual concentrations of the aforementioned ions were measured using an ICP-AES (ICAP-6300, Thermo Fisher, USA).

Results and discussion

Characterization

The micro morphology and ordered structure of the MMSs were examined using TEM and small angle XRD, respectively. The TEM images of MSBA-15 is shown in Fig. [2a](#page-2-0) and b. Fe₃O₄ is covered with an ordered SiO₂ layer, whose pore wall is approximately 5.13 nm. The small-angle XRD patterns of three types of MMSs are presented in Fig. [2](#page-2-0)c. Concerning MSBA-15, the peaks at 0.9° , 1.7° and 2.1° correspond to the (100), (110), and (200) crystal planes, revealing that it has hexagonal structure [[17](#page-12-15)]. The peak of MMCM-48 at 2.4° corresponds to the (100) crystal plane, and the characteristic peak of MMCM-41 and MMCM-48 at 2.1° corresponds to the (200) crystal plane, has a good mesoporous structure [\[18\]](#page-12-16). The small-angle XRD results indicate that the structure of MMSs is both mesoporous and ordered.

The surface functional groups of MMSs were analyzed using FT-IR, and the fndings are illustrated in Fig. [2](#page-2-0)d. In the infrared spectra of MMSs, there are typical characteristic peaks of mesoporous silica. The bands at 1041 and 804 cm−1are Si–O–Si stretching vibration peaks [[19](#page-12-17), [20](#page-12-18)]. The stretching and bending vibration of the hydroxyl group connected to the silica atom appears at 1647 and 3750 cm−1

Fig. 2 TEM images of MSBA-15 (**a**) \times 8 \times 10⁵, (**b**) \times 1.6 \times 10.⁶, (**c**) small-angle XRD patterns of MSBA-15, MMCM-41 and MMCM-48, (**d**) FT-IR spectra of MSBA-15, MMCM-41 and MMCM-48

[\[21,](#page-12-19) [22](#page-12-20)].The weak absorption peak at about 593 cm⁻¹ can be attributed to the vibration of Fe–O bond [\[23](#page-12-21)]. The FT-IR results indicate the successful synthesis of three distinct MMSs.

The adsorption–desorption plots were obtained under a N_2 atmosphere. MSBA-15, MMCM-41, and MMCM-48 were degassed at 373.15 K for more than 15 h before the determination. The specific surface of the sample $(S_{BET}$, $m^2 \cdot g^{-1}$) is calculated from the BET equation [\[24](#page-12-22)] at a relative pressure (P/P_0) between 0.05 and 0.25. Pore distribution is calculated by BJH model $[25]$ $[25]$. In Fig. [3a](#page-3-0), the N₂ adsorption–desorption isotherms of MMSs at 77 K. It can be seen from the Fig. that their adsorption isotherms all show the characteristics of type IV curves, indicating that they all conform to the characteristics of mesopores [\[26\]](#page-12-24). MSBA-15's type hysteresis ring is a typical H2 type [[27\]](#page-13-0), suggesting that it has a narrow mesoporous structure. The N_2 desorption adsorption curves of MMCM-41 and MMCM-48 are H4 type hysteresis loops, showing micro-mesoporous structure. Figure [3b](#page-3-0) illustrates the BJH pore size distribution of MMSs. The pore size distribution of MMSs is relatively narrow. The most probable pore diameters of MSBA-15, MMCM-41, and MMCM-48 is 8.36, 3.79, and 2.75 nm, respectively. The pore structure data are itemized in Table [1](#page-4-0). The S_{BET} and average pore diameter values of MSBA-15, MMCM-41 and MMCM-48 was 675.50, 605.38 and 638.70 m²·g⁻¹; 6.69 nm, 3.60 nm and 3.56 nm, respectively.

Magnetic properties of MMSs are measured by VSM (Fig. [3](#page-3-0)c). The magnetic symmetrical hysteresis curves of MSBA-15, MMCM-41 and MMCM-48 all show an S-shape. And, the saturation magnetization is 6.29, 13.66 and 16.17 emu·g−1, respectively. Upon the removal of the template from the as-synthesized MSBA-15 at high temperatures, there is a consequential partial oxidation of ferric oxide. It's noteworthy that MSBA-15 can swiftly aggregate using a magnet, as depicted in the inset of Fig. [2](#page-2-0)c. This property proves beneficial for the recovery of $U(VI)$ through magnetic means.

The ζ potential at different pH values is illustrated in Fig. [3d](#page-3-0). The surface potential of the three materials declined with the increasing pH values. Specifcally, the surface potential of MSBA-15, MMCM-41, and MMCM-48 decreases from -1.32, 1.53, and 19.83 mV to −48.59, −38.49, and −31.45 mV, respectively, when the pH value is

Fig. 3 MSBA-15, MMCM-41 and MMCM-48, (**a**) N2 adsorption and desorption curves, (**b**) BJH pore size distribution, (**c**) VSM plots, (**d**) ζ potential

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Table 1 Pore structure parameters of MSBA-15, MMCM-41 and MMCM-48

a Specifc surface area calculated by BET method

b Total pore volume

c BJH desorption volume

^dAverage aperture, $D_A = 4V_t/S_{BET}$

e BJH desorption average pore size

f The most probable aperture

within the range of 2.0–8.0. The pH values of the zero potential points (pH_{IZE}) of MMCM-41 and MMCM-48 is 2.6 and 5.6, respectively. When the pH value of the external system exceeds the pH_{IZE} of the material, the surface potential of the material becomes negative. This negative surface potential contribute to the adsorption of U(VI) through electrostatic attraction.

The hydrophilicity of materials was explored through contact angle. Contact angle of MMSs after dropping liquid for 5 s is illustrated in Fig. [4](#page-4-1). The contact angles of MSBA-15, MMCM-41, and MMCM-48 was 22.5°, 24.5°, and 31.5°, indicating that MSBA-15 has best hydrophilicity [\[28\]](#page-13-1). Excellent hydrophilicity of MSBA-15 facilitates the contact with aqueous solution and improves the separation ability of U(VI) [[29\]](#page-13-2).

The XPS was employed to characterize the element composition and chemical form of the prepared MSBA-15 material. The corresponding spectra are shown in Fig. [5.](#page-5-0) The peaks of Fe, O, C and Si appear in the full spectrum, indicating $Fe₃O₄$ and mesoporous silica combined together closely. The spectrum peak of Fe 2p shows that Fe $2p_{1/2}$ and $2P_{3/2}$ is located at 708.9 and 714.1 eV, respectively [\[30](#page-13-3)]. It signposted that $Fe₃O₄$ exists in MSBA-15, showing a good match with the results of TEM and FT-IR. The C 1 s peak separation that the synthesized magnetic mesoporous silica material contains two peaks of C–C and C–Si, locating at 284.1 and 282.6 eV, respectively. It noted that the synthesized MSBA-15 also contained a small amount of template that has not been removed completely. Figure [5d](#page-5-0) is the spectrum of Si 2p, with Si–OH at 102.1 eV and Si–C at 101.4 eV [[31\]](#page-13-4). In the O 1 s spectrum, the peak at 531.3 and 530.5 eV corresponds to Si–OH and O–H. In summary, the XPS analysis corroborates the presence of $Fe₃O₄$ in MSBA-15. The characterization indicates a substantial presence of silica hydroxide groups on the material's surface.

pH value

The impact of pH value on the adsorption of $U(VI)$ by MSBA-15, MMCM-41 and MMCM-48 was studied in the range of pH 2.0–7.0 (C_0 =50 mg·L⁻¹, m = 10 mg, V =50 mL, $T=298.15$ K, $t=240$ min). The results are displayed in Fig. [6.](#page-6-0) Under acidic conditions, U(VI) predominantly exists in the form of UO_2^{2+} . And, the competition of H^+ with U(VI) for the active sites on the MMSs resulted in lower adsorption [[32](#page-13-5)]. With the increasing of pH values, the ζ potential of MMSs decreased according to the Fig. [3d](#page-3-0). Consequently, the values of *q* increased accordingly. At a pH value of 6.0, the adsorption performance of the three types of MMSs for U(VI) reached its peak, with adsorption capacities of 158.18, 126.74, and 125.38 mg⋅g⁻¹. The best adsorption ability of MSBA-15 may be due to highest pore volume, biggest pore diameter (Table [1](#page-4-0)) as well as smallest contact angle (Fig. [4](#page-4-1)). When pH was over 6.0, the anions of $UO_2CO_3(OH)_3^{3-}$ and $UO_2(CO_3)_3^{4-}$ were major components [\[33](#page-13-6)]. Thus, the electrostatic repulsion weakened the removal

Fig. 4 Contact angle of MSBA-15, MMCM-41 and MMCM-48

Fig. 5 XPS spectra of MSBA-15: (**a**) survey, (**b**) C 1 s, (**c**) Fe 2p, (**d**) Si 2p, (**e**) O 1 s

capacity for U(VI). As a result, during the subsequent batch experiments, the solution's pH was adjusted to 6.0.

Adsorption kinetics

The effect of contact time on U(VI) adsorption by MMSs (*C*0= 50 mg·L−1, *m* = 10 mg, *V* = 50 mL, *T* = 298.15 K, pH=6.0) was explored. In Fig. [7a](#page-6-1), U(VI) rapidly enriched on the surface of MMSs in the initial 90 min. Notably, MSBA-15, MMCM-41, and MMCM-48 achieved adsorption equilibrium at 120, 120, and 240 min, respectively.

Quasi-frst order [\[34,](#page-13-7) [35\]](#page-13-8), quasi-second order [[34](#page-13-7)] and intra-particle difusion model [\[36,](#page-13-9) [37\]](#page-13-10) were employed to analyze the experimental data and the process of adsorption

Fig. 6 Effect of pH on the adsorption of U(VI) by MSBA-15, MMCM-41, and MMCM-48 (C_0 =50 mg·L⁻¹, m =10 mg, V =50 mL, *T*=298.15 K, *t*=240 min)

of U(VI) by MMSs. The formulas of them are shown in form of S3, S4, and S5. The sorption kinetics of U(VI) by MSBA-15, MMCM-41, and MMCM-48 are depicted in Fig. [7a](#page-6-1). The ftting parameters are detailed in Table [2](#page-6-2). The correlation coefficient (R^2) of the quasi-second order kinetic model for three kinds of MMSs is closer to 1.0. Furthermore, the theoretical adsorption capacity (176.23, 154.86, and 144.33 mg·g⁻¹) is closer to the experimental value (172.40, 152.86, and 140.85 mg·g⁻¹). Consequently, the U(VI) adsorption processes of on MMSs align more closely with the quasi-second-order equation, suggesting that chemical action predominantly governs the adsorption process.

The intra-particle difusion model [[38\]](#page-13-11) of MMSs for U(VI) sorption by MMSs is illustrated in Fig. [7](#page-6-1)b. The ftting results can be found in Table [3](#page-6-3). The internal difusion rate constants (k_{id}) for the three kinds of MMSs consistently follow the order $k_{id,1} > k_{id,2} > k_{id,3}$, indicating that the adsorption process occurs in three distinct steps.

Fig. 7 Fitted curves of (**a**) quasi-primary and quasi-secondary kinetic models for MSBA-15, MMCM-41 and MMCM-48 adsorbed U(VI), (**b**) fitted curves of internal diffusion model (C_0 =50 mg·L.⁻¹, m = 10 mg, V =50 mL, T =298.15 K, pH=6.0)

Table 2 Kinetic parameters of

MMCM-41 and MMCM-48

During the initial phase of rapid adsorption, U(VI) in the solution comes into contact with the surface of MMSs and swiftly difuses towards the material surface. Subsequently, in the slower adsorption process, U(VI) penetrates the inner surface and binds to active sites within. Upon reaching adsorption equilibrium, the difusion rate approaches 0.

Adsorption isotherm

Figure [8](#page-7-0) illustrates the impact of varying equilibrium concentrations of U(VI) (C_e , mg·L⁻¹) on the adsorption efficiency of MMS for U(VI). In the lower concentration range, the adsorption capacity of U(VI) shows a rapid increase. Conversely, at higher concentrations, MSBA-15 demonstrates a gradual attainment of adsorption satiation, reaching a capacity of 319.55 mg·g−1. The saturated adsorption capacities for MMCM-41 and MMCM-48 are 217.88 and 190.54 mg·g−1, respectively.

To further analyze the adsorption processes, Langmuir [\[39,](#page-13-12) [40\]](#page-13-13), Freundlich [[41\]](#page-13-14), and Sips [[42](#page-13-15), [43](#page-13-16)] isotherm models were used. The formula is presented as Eqs. S6, S7, and S8. The fitting results including the values of the R^2 and relevant parameters are revealed in Fig. [8](#page-7-0) and Table [4.](#page-7-1) As shown from Table [7](#page-9-0), MSBA-15 exhibit a greater consistency with the Sips adsorption isotherm model with a higher R^2 values (0.99) than Freundlich ($R^2 = 0.87$) and Langmuir models $(R^2 = 0.98)$. Furthermore, the saturated adsorption capacity (341.94 mg·g⁻¹) obtained by ftting the Sips adsorption isotherm model of MSBA-15 is near to the actual value (319.55 mg·g⁻¹). However, the saturated adsorption capacities of Langmuir adsorption isotherm models for MMCM-41 and MMCM-48

Fig. 8 Langmuir, Freundlich and Sips models for MSBA-15, MMCM-41 and MMCM-48 adsorption U(VI) (*m*=10 mg, *V*=50 mL, *T*=298.15 K, pH=6.0, *t*=240 min)

Table 4 Adsorption isotherm model parameters for U(VI) adsorption by MSBA-15, MMCM-41 and MMCM-48

Model	Parameter	Adsorbents		
		MSBA-15	MMCM-41	MMCM-48
Langmuir	q_e (mg·g ⁻¹)	362.80	250.60	232.88
	K_L	0.09	0.05	0.05
	R^2	0.99	0.98	0.96
Freundlich	K_F	90.28	49.03	41.31
	1/n	0.28	0.31	0.33
	R^2	0.87	0.92	0.93
Sips	q_s (mg·g ⁻¹)	341.94	256.72	259.95
	Ks	0.05	0.06	0.07
	\overline{c}	0.27	0.06	0.20
	R^2	0.99	0.98	0.97
D-R	q_d (mol·g ⁻¹)		1.49×10^{-3} 1.08×10^{-3} 0.92×10^{-3}	
	β		-3.97×10^{-3} -3.61×10^{-3} -3.52×10^{-3}	
	E (kJ·mol ⁻¹)	11.18	11.78	11.95
	R^2	0.98	0.97	0.96
Temkin	B (J·mol ⁻¹)	71.68	46.72	41.86
	K_T	0.70	0.87	0.91
	R^2	0.90	0.96	0.93

 $(250.60 \text{ mg} \cdot \text{g}^{-1}, 232.88 \text{ mg} \cdot \text{g}^{-1})$ are closer to the actual values (217.88 mg·g⁻¹, 190.54 mg·g⁻¹), indicating a single molecular layer adsorption dominated by a chemical process.

To investigate the impact of the initial U(VI) concentration on MSBA-15, MMCM-41, and MMCM-48, the Dubin-Radushkevich (D-R) [\[44](#page-13-17)], and the Temkin [[45](#page-13-18)] adsorption isotherm models were employed to compute the binding energy (*E*, kJ·mol⁻¹) and the constant (*B*, J·mol⁻¹). The calculation formula for the D-R adsorption isotherm model is represented by Eqs. S9, S10, and S11.

The D-R and Temkin adsorption isotherm models are illustrated in Fig. [9a](#page-8-0) and b, respectively. The relevant parameters are displayed in Table [4.](#page-7-1) The values of D-R adsorption isotherm models' R^2 (0.98, 0.97, 0.96) of MSBA-15, MMCM-41, and MMCM-48 are closer to 1. The results are higher than the Temkin adsorption isotherm models $(0.90, 0.96, 0.93)$, presenting that the enrichment of U(VI) by MMSs is more consistent with the D-R adsorption isotherm model. Furthermore, the binding energies of the three kinds of MMSs (11.18, 11.78, 11.95 kJ·mol⁻¹) are all over 8.0 kJ·mol−1. And again, it indicated that adsorption is dominated by chemical reaction [[46](#page-13-19)].

The adsorption capacity of MSBA-15 for U(VI) was compared with that of other adsorbents, and the relevant results are presented in Table [5](#page-8-1). Observing the table, it becomes apparent that of MSBA-15 shows a greater saturated adsorption capacity for U(VI) than that of the studied functionalized Fe₃O₄, SBA/SA, MCM-41, and MCM-48, etc.

Table 5 Comparison of the adsorption performance of diferent mesoporous material adsorbents on U(VI) at

298.15 K

Fig. 9 MSBA-15, MMCM-41 and MMCM-48 adsorption U(VI) isothermal models: (**a**) D-R model; (**b**) Temkin model

Fig. 10 (**a**) Efect of temperature on the adsorption of U(VI) by MSBA-15, MMCM-41 and MMCM-48, (**b**) thermodynamic curves (*C*0=50 mg·L.−1, *m*=10 mg, *V*=50 mL, *t*=240 min, pH=6.0)

Table 6 Thermodynamic parameters of adsorbed U(VI) for MSBA-15, MMCM-41 and MMCM-48

MSBA-15 20.60 144.33 −20.99 −22.43 −23.87 −25.32 −26.76 MMCM-41 13.67 177.21 −37.39 −39.16 −40.94 −42.71 −44.48 MMCM-48 13.13 114.55 −19.88 −21.02 −22.17 −23.31 −24.46

Adsorbents Δ*H* (kJ·mol−1) Δ*S* (J·K−1·mol−1) Δ*G* (kJ·mol−1)

Fig. 11 Selectivity of MSBA-15, MMCM-41 and MMCM-48 for different ions (pH=6.0, C_0 =50 mg·L.⁻¹, m =10 mg, V =50 mL, *T*=298.15 K, *t*=240 min)

Adsorption thermodynamics

The effect of temperature on the adsorption of $U(VI)$ by MMSs is depicted in Fig. [10](#page-8-2)a. The equilibrium adsorption capacity of U(VI) increases with rising temperature, suggesting that adsorption of U(VI) is an endothermic process.

To further explore the infuence of temperature, the corresponding thermodynamic functions [[52\]](#page-13-25) of Δ*H*, Δ*S,* and Δ*G* are calculated by using formulas S13 and S14. Thermodynamic ftting plots are presented in Fig. [10](#page-8-2)b. Accord-ing to the results presented in Table [6](#page-9-1), $\Delta H > 0$ and $\Delta G < 0$ indicate that the adsorption processes are endothermic and spontaneous.

Adsorption selectivity

The adsorption selectivity of MMSs for U(VI) was studied in the solution with coexisting ions. In Fig. [11](#page-9-2), the adsorption capacity of MSBA-15, MMCM-41 and MMCM-48 for U(VI) in the presence of eight ions is 49.03, 44.82 and 52.48 mg·g−1, respectively, accounting for 50.81, 42.89 and 44.47% of the total adsorption capacity. Among them, U(VI) accounts for the largest proportion of MSBA-15 adsorption, thanks to the excellent mesoporous structure and abundant Si–OH of MSBA-15.

To further theoretically evaluate the adsorption selectivity of MMSs for U(VI), the selectivity coefficient (S) [\[53](#page-13-26)] is calculated. In Table [7](#page-9-0), comparing with the other eight ions, the three MMSs have higher partition coefficients for $U(VI)$, and the selectivity coefficient S is greater than 1, indicating that they can selectively adsorb U(VI) in an aqueous solution.

Table 7 Distribution ratios and selectivity coefficients of MSBA-15、MMCM-41and MMCM-48

Fig. 12 (**a**) Elution efect of diferent hydrochloric acid concentrations on MSBA-15, (**b**) reproducibility of MSBA-15

Repetitive experiment

HCl solutions (0–0.50 mol⋅L⁻¹) are chosen as the desorption solution. Then the reusability experiments of MSBA-15 were carried out (Fig. [12a](#page-10-0)). The elution rate $(D, \%)$ is determined by the formula S16 [\[54\]](#page-13-27). The U(VI) adsorbed on MSBA-15 can be eluted with 0.30 mol⋅L⁻¹HCl with the best elution rate of 99.4%. Thus, 0.30 mol⋅L⁻¹ HCl solution was selected as the eluent for MSBA-15 in subsequent repeated experiments.

Adsorption–desorption-regeneration cycles were repeated for 5 times, as shown in Fig. [12](#page-10-0)b. After repeating the experiment for 4 times, the adsorption capacity of MSBA-15 for U(VI) decreased to 80.7% of the initial value. It may be related to the destruction of the adsorption active site on MSBA-15. The above results show that MSBA-15 can be reused in recovery of U(VI) from an aqueous solution.

Adsorption mechanism

The potential mechanism of U(VI) adsorption on MSBA-15 was assessed through FT-IR and XPS analyses. In the FT-IR spectrum following the adsorption of $U(VI)$ (Fig. [13](#page-11-0)a), an asymmetric vibration absorption peak of UO_2^{2+} emerged at 911 cm⁻¹. Furthermore, the stretching and bending vibration peaks (3750 and 1647 cm⁻¹) of the hydroxyl group were intensifed.

The XPS spectra of MSBA-15 before and after U(VI) uptake are shown in Fig. [13b](#page-11-0). Apart from the Fe 2p, O 1 s, C 1 s and Si 2p peaks, the U 4f peak (Fig. [13c](#page-11-0)) also manifested in the spectrum after adsorption. It indicated that $U(VI)$ was successfully adsorbed by MSBA-15. Additionally, in the Si 2p spectrum (Fig. [13](#page-11-0)d), the Si–OH at 102.1 eV shifted to 102.5 eV after adsorption, indicating that there was an interaction between the Si–OH groups and U(VI). In the spectrum of O 1 s (Fig. 13 (e)), the Si-OH peak shifted to 531.3 eV, and the O–H peak at 530.5 eV did not change signifcantly. In addition, the spectral diagram at C 1 s (Fig. [13](#page-11-0)f, the C–C peak at 284.1 eV exhibited no change, whereas the C-Si peak at 282.6 eV has shifted. These fndings indicate that U(VI) coordinates with the silica hydroxide group on the surface of MSBA-15.

Conclusion

Magnetic mesoporous silicas, MMCM-41, MMCM-48, and MSBA-15, were successfully synthesized. The ordered-mesoporous structure of MSBA-15 was identified by TEM, small angle XRD and N_2 adsorption–desorption curves. The BET specifc surface areas of MSBA-15, MMCM-41 and MMCM-48 is 675.50, 605.38 and 638.70 $m^2 \cdot g^{-1}$, respectively. The optimal adsorption pH values of MMSs were all 6.0, and reached adsorption equilibrium within 240 min. MSBA-15 has a higher saturated adsorption capacity (341.94 mg·g⁻¹) and superior selectivity for U(VI) than MMCM-41 and MMCM-48. The adsorption capacity of MSBA-15 for U(VI) decreased to 80.7% of the initial value after 4 recycles. The adsorption of U(VI) on MSBA-15 is mainly the coordination of Si–O–H group with U(VI). In conclusion, MSBA-15 has outstanding performance for U(VI) and is expected to be used in treatment and recovery of U(VI) from radioactive waste water.

Fig. 13 (a) FT-IR spectrum of MSBA-15 after adsorption, XPS spectra of MSBA-15 before and after adsorption: (**a**) total spectrum, (**b**) U 4f, (**c**) Si 2p, (**d**) O 1 s, (**e**) C 1 s

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Authors' contribution DB wrote the entire draft of the manuscript. The core conceptual idea and study design were all provided by YL and YW. The preparation and adsorptive experiments were conducted out with WC and QL. Material preparation and data analysis were completed by XC and LX. The characterization analysis of the adsorbents was worked out through ZZ and LX. WC has revised most of the content of the manuscript according to the comment of reviewers.

Data availability All data generated or analyzed during this study are included in the manuscript.

Declarations

Competing interests The authors declare that they have no competing interests.

Consent to participate Not applicable consent to participate the authors have consent to participate.

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