

Adsorption performance and mechanism of g-C₃N₄/UiO-66 composite **for U(VI) from aqueous solution**

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Abstract

The uranium (VI) adsorption performance of $g - C_3N_4/UiO-66$ composite (CNUIO) was evaluated under different solution pH values, adsorbent dosages, coexisting ions, contact times, initial U(VI) concentrations, and temperatures. The surface properties and the interaction mechanism between U(VI) and CNUIO were analyzed via SEM–EDS, BET, FT-IR and XPS. CNUIO exhibited the maximum adsorption rate of 95.01% under the conditions of C_{U(VD}=10 mg/L, pH=6, M/V=0.4 g/L, $t = 120$ min, and $T = 298$ K, which was about 25% and 33.73% higher than that of g-C₃N₄ and UiO-66, respectively. The adsorption process was found to be a spontaneous endothermic process and conformed to the pseudo-second-order kinetic model and the Langmuir isothermal adsorption model. SEM–EDS and BET analysis revealed that increasing the specifc surface area efectively improved the adsorption capacity of CNUIO. FT-IR spectroscopy and XPS indicated that the removal of U(VI) was attributed to the coordination complexation between the nitrogen-containing and the oxygen-containing functional groups of CNUIO and U(VI). Adsorption–desorption experiment demonstrated that CNUIO has a good reusability.

Keywords Uranium (VI) · Adsorption · Performance · $g - C_3N_4/U$ iO-66 · Mechanism

Introduction

With the rapid development of nuclear energy, huge amounts of uranium-containing water are produced by uranium mining and processing and utilization of uranium raw materials [\[1](#page-11-0)]. Untreated uranium-containing water that is directly discharged into aqueous environments can cause serious harm to human health and the ecological environment [[2,](#page-11-1) [3](#page-11-2)]. Therefore, efective treatment of uranium-containing water has become an urgent environmental concern. Various efective treatment techniques, such as adsorption method, chemical precipitation, ion exchange, redox, and biological treatment $[4–7]$ $[4–7]$ $[4–7]$ $[4–7]$, have been developed, among which the adsorption method is widely used because it is a simple and cost-efective operation.

Graphitic carbon nitride $(g - C_3N_4)$ is a low-cost absorbent that contains both amino and imino groups on its surface [[8\]](#page-11-5), and the highly condensed nature of the CN framework endows it with excellent physical and chemical stability [\[9](#page-11-6)]. $g - C_3 N_4$ reportedly has a good removal effect on U(VI) [\[10](#page-11-7)], Pb (II), Ni (II), Cd (II), and Cu (II) in aqueous solutions [[11\]](#page-11-8). However, the adsorption capacity of $g - C_3N_4$ is limited because of its small specifc surface area owing to its layered structure formed by the stacking of nanosheets and insufficient number of functional groups $[12]$ $[12]$ $[12]$. To enhance its adsorption capacity, we used morphology control [[13\]](#page-11-10) and made a $g - C_3 N_4$ composite with other materials. Liu et al. [[14](#page-11-11)] combined polyaniline with oxidation etching $g - C_3 N_4$. They reported that at the adsorption rate of U(VI) was 36.24% higher than that of $g - C_3N_4$. A previous study found that $MnFe₂O₄/PCN$ composites have an improved adsorption capacity of 182.8 mg/g $[15]$ $[15]$. Long et al. $[16]$ $[16]$ also found that $Fe₃O₄@g-C₃N₄$ nano magnetic materials can be used for purifying uranium ion. Wang et al. [\[17](#page-11-14)] reported a β-CD modified g-C₃N₄ nanosheet for the extraction of U(VI) with high selectivity from solution system and simulated seawater.

UiO-66, as a zirconium dicarboxylate (Zr)-based metal organic framework material, not only has a large specifc

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surface area and a high porosity but also has outstanding hydrothermal and chemical stability, which makes it a promising candidate of adsorbent [\[18](#page-11-15)]. Luo et al. [\[19](#page-11-16)] demonstrated that the maximum adsorption capacity of UiO-66 for U(VI) at pH 5.5 is 109.9 mg/g. Chen et al. $[20]$ $[20]$ $[20]$ found that the uranium adsorption capacity was higher for aminemodifed UiO-66. Tripathi et al. [[21](#page-11-18)] prepared a series of functionalized UiO-66 for uranium separation, which exhibit efficient sorption and moderate recyclability to uranium. These works highlight the tremendous potential of UiO-66 in removal of U(VI) from aqueous solution. In order to enhance the adsorption performance of $g - C_3N_4$, UiO-66 was assembled on its surface to increase its specifc surface area and enrich its surface functional groups, which overcame the shortcoming of a single component and improved the capture ability of U (VI). Therefore, in this study, a $g - C_3N_4/$ UiO-66 composite (CNUIO) was synthesized. Its performance in removing U(VI) was evaluated and the underlying mechanism was investigated. This study provides a convenient adsorbent with efficient adsorption performance for the treatment of uranium-containing water.

Experimental section

Materials and chemicals

Melamine, zirconium chloride $(ZrCl₄)$, terephthalic acid (H_2BDC) , N, N-dimethylformamide (DMF), acetic acid glacial, methanol. Uranium stock solution were prepared from GBW04201 U_3O_8 standard. All reagents were of analytical grade, and all solutions were prepared with deionized water.

Synthesis of g-C₃N₄

Typically, 5 g melamine was placed in a covered crucible and calcined in the muffle furnace at 550 °C for 4 h (2 °C/ min). After cooling to room temperature and grinding, the obtained yellow powder was $g - C_3 N_4$.

Synthesis of UiO‑66

UiO-66 Octahedrons were synthesized by solvothermal method:1.059 g $ZrCl₄$ and 0.755 g H₂BDC were dissolved in 100 ml DMF with a continuous stirring for 1 h and then 60 ml acetic acid glacial was added dropwise to adjust the shape of UiO-66. The solution was transferred into a Teflon-lined stainless steel reactor, followed by being heated at 120 °C for 24 h. The product was washed several times with DMF and methanol. Finally, the UiO-66 samples were obtained after dried in oven at 80 °C overnight.

Synthesis of CNUIO

An improved scheme for preparing CNUIO was adopted herein following the method described in a previous study [[22\]](#page-11-19). First, 1 g of $g - C_3N_4$ was dispersed into 10 mL DMF and sonicated for 1 h. Then, 0.053 g of $ZrCl₄$ and 0.034 g of H2BDC were dissolved in 5 mL DMF. Afterward, 6 mL of glacial acetic acid was added dropwise to adjust the shape of UiO-66. The mixture was sonicated at room temperature until the solution became homogeneous. The $g - C_3N_4$ solution was added into the above solution and continuously ultrasonicated for 1 h. The mixture was transferred into a Teflon-lined stainless steel reactor and then heated at 120 °C for 24 h. The subsequent washing and drying operations were the same those performed on UiO-66. The schematic of the synthesis process is shown in Scheme [1.](#page-1-0)

Adsorption performance experiments

Uranium stock solution was diluted to the required concentration, and U(VI) adsorption by CNUIO was conducted through batch experiments. First, the pH of 50 mL U(VI)

tion for synthesis of the CNUIO

solution was regulated to a range of 2–8 by adding negligible amounts of 0.1 M HCl and NaOH solutions. In the uranium adsorption experiment, 20 mg adsorbents were added into the 10 mg/L U(VI) solution. The mixture was shaken at 160 rpm in an air batch shaker. After continuous shaking to reach adsorption equilibrium, the adsorbent was separated from the reaction solution via centrifugation and fltration. The residual concentration of U(VI) in the supernatant was measured via a standard spectrophotometry method (578 nm). It was based on the formation of colored complexes of U(VI) ion with bromine generation ethanol in aqueous medium [\[23](#page-11-20)]. The average values of each experimental result were obtained through three repeated experiments. The % adsorption and adsorption capacity *q* (mg/g) were calculated by the following Eqs. [\(1](#page-2-0)) and [\(2\)](#page-2-1):

% adsorption =
$$
\frac{C_0 - C_e}{C_0} \times 100\%
$$
 (1)

$$
q = \frac{(C_0 - C_e) \times V}{M}
$$
 (2)

where C_0 is the initial U(VI) concentration (mg/L), C_e is the equilibrium concentration (mg/L), *V* is the volume of the solution (L) , M is the mass of the adsorbent (g) .

Adsorption–desorption test

The 20 mg of CNUIO adsorbed by U(VI) was added to 50 mL HCl (0.1 M) and desorbed by shaking for 6 h. A certain volume of the supernatant was centrifuged at 7000 rpm for 10 min. The concentration of U(VI) was measured, and its desorption rate was calculated. Desorbed CNUIO was repeatedly washed with distilled water, dried by a vacuum drying tank, and repeatedly adsorbed fve times under the same conditions to determine the adsorption efficiency. The % desorption was calculated by the following Eqs. ([3\)](#page-2-2):

% desorption =
$$
\frac{q_0}{q} \times 100\%
$$
 (3)

where q_0 is the desorption capacity of U (VI) (mg/g), q is the adsorption capacity of U (VI) (mg/g).

Characterization

The morphology of the adsorbents was observed via scanning electron microscopy (SEM) (JSM–7500F, Japan). The surface area of the adsorbents was determined by Brunauer–Emmett–Teller (BET) analysis, and the pore size and volume were calculated by Barrett–Joyner–Halenda (BJH) model (Micro for Tristar II,USA). The crystal texture of the adsorbents was identifed using an XRD (Bruker D8, Germany). The functional groups of the adsorbents were ascertained via Fourier transform infrared (FTIR) spectroscopy (Nicolet–iS10, USA). The chemical elements of the adsorbents were identifed via X-ray photoelectron spectroscopy (XPS) (ESCALAB250Xi, USA).

Results and discussion

Experiments on adsorption performance of CNUIO

Efects of pH and ionic strength

The effect of the initial pH value $(2–8)$ on U(VI) removal by the three adsorbents were evaluated (Fig. [1](#page-2-3)). When the pH value increased from 2 to 6, the adsorption rate of CNUIO for U(VI) increased from 22.03% to 95.01%. When the pH value increased to 8, the adsorption rate decreased to 88.90%. At pH 6, the adsorption rate of CNUIO for U(VI) was about 25% and 33.73% higher than that of $g - C_3N_4$ and UiO-66, respectively. Furthermore, the removal rate of U(VI) by $g - C_3 N_4$ and UiO-66 was lower than that of CNUIO within the range of pH values studied herein, indicating that the adsorption performance of the composite on U(VI) was better than that of each single component.

The effects of pH may be attributed to the fact that the acid–base of the solution has an important efect on the morphology of uranium, the surface charge distribution of the adsorbent, and the binding sites. The uranyl ion species in natural water has been widely studied [[24\]](#page-11-21). The reason for the changes in the adsorption rate of CNUIO to U(VI) with pH was further explored by simulating uranyl species at diferent pH values by using the Visual

Fig. 1 The effect of the pH on U(VI) adsorption onto $g - C_3N_4$, UiO-66 and CNUIO. (M/V=0.4 g/L, C_{U(VI)}=10 mg/L, T=298 K, *t*=120 min)

MINTEQ software. As shown in Fig. [2,](#page-3-0) at $pH < 4$, U(VI) mainly existed as UO_2^{2+} , and at pH = 5–7, several kinds of uranyl hydroxides, such as $UO_2(OH)^+$, $(UO_2)_3(OH)_5^+$ and $(UO_2)_4(OH)_7^+$, were gradually generated. When pH = 6, the dominating uranyl specie is $(UO₂)₃(OH)₅⁺$ and the adsorption rate reached 95.01%. At $pH > 8$, the predominant species are $UO_2(CO_3)_3^{4-}$ and $UO_2(CO_3)_2^{2-}$.

According to the zeta potential (Fig. [3](#page-3-1)), the point of zero charge of CNUIO was measured at $pH = 6.02$. The surface of the adsorbent was positively charged prior to 6.02 because of the protonation of functional groups on CNUIO by H^+ . At this time, electrostatic repulsion was formed between the protonated adsorbents and the positively charged UO_2^{2+} ; moreover, the high concentration of H^+ completed with UO_2^{2+} for the active sites, thereby restricting uranium adsorption [[25](#page-11-22)]. As pH increased, the surface charge of CNUIO changed from positive to negative. Owing to the electrostatic attraction between CNUIO and UO_2^{2+} , adsorption efficiency gradually improved. After the zero potential, the negatively charged CNUIO repelled each other with various U(VI) complexes, such as $UO_2(CO_3)_3^{4-}$ and $UO_2(CO_3)_2^{2-}$, resulting in a slight decrease in adsorption rate.

The infuence of ionic strength on U(VI) adsorption by CNUIO was assessed (Fig. [4](#page-3-2)). When $Na⁺$ concentration increased from 0 to 0.1 mol/L, U(VI) adsorption was negligibly afected within the specifed pH range, indicating that the adsorption was dominated by inner-sphere surface complexation and electrostatic attraction [[26\]](#page-11-23).

Fig. 3 The zeta potential changes with diferent pH

Efects of adsorbent dosages

The dosage of CNUIO may afect the number of binding sites between CNUIO and U(VI), thus affecting the adsorption capacity of U(VI). The efect of CNUIO dosages on U(VI) adsorption were examined (Fig. [5](#page-4-0)). When the dosage increased from 0.1 to 1.6 g/L , the adsorption efficiency of U(VI) by CNUIO increased from 69.19 to 97.4%, whereas the adsorption capacity decreased from 69.19 to 6.09 mg/g. As the dosage increased, the number of active sites of the adsorbents and the adsorption rate of U(VI) correspondingly increased [[27\]](#page-11-24). However, excessive CNUIO dosages will reduce the unsaturation sites per unit mass adsorption, so the adsorption capacity was decreased. When CNUIO

Fig. 2 The distribution of U(VI) species in aqueous solution with different pH

Fig. 4 The effect of ionic strength on U(VI) adsorption by CNUIO. $(M/V=0.4 \text{ g/L}, C_{U(VI)}=10 \text{ mg/L}, T=298 \text{ K}, t=120 \text{ min})$

Fig. 5 Efect of the adsorbent dosage on U(VI) adsorption to CNUIO. $(pH=6, C_{U(VI)}=10 mg/L, T=298 K, t=120 min)$

Fig. 6 Efects of coexisting-ions on U(VI) adsorption by CNUIO. $(pH=6, M/V=0.4 \text{ g/L}, C_{U(VI)}=10 \text{ mg/L}, T=298 \text{ K}, t=120 \text{ min})$

dosage exceeded 0.4 g/L, U(VI) adsorption tended to remain stable. Therefore, the subsequent dosage of CNUIO in this experiment was 0.4 g/L.

Efects of coexisting ions

The effects of coexisting ions on $U(VI)$ adsorption by CNUIO are illustrated in Fig. [6](#page-4-1). A low concentration of the coexisting ions (10 mg/L) had little efect on CNUIO adsorption. As their concentration increased, SO_4^2 ⁻ and $NO₃⁻$ had little effect on U(VI) adsorption. However, Cu^{2+} , Ca^{2+} , Mg^{2+} , and F⁻ inhibited the adsorption to a certain extent, and the degree of inhibition was positively correlated with the concentration of the coexisting ions. Cu^{2+} , Ca^{2+} , and Mg^{2+} competed with uranyl ions

for CNUIO surface activity adsorption sites during the adsorption process, resulting in a decrease in adsorption rate. The adsorption inhibition of F− on U(VI) was the strongest. When the concentration of F− was 90 mg/L, the adsorption rate was only 60.97%. Owing to the high afnity between fuorine and zirconium, zirconium-based adsorbents usually exhibit ideal F− removal [[28](#page-11-25)]. Therefore, in the presence of interference ions other than F−, the removal rate of U(VI) by CNUIO remained above 80%, indicating that CNUIO had a certain selective adsorption of U(VI) in aqueous solutions.

Efects of contact time and adsorption kinetics

The effect of contact time on adsorption of CNUIO was shown in Fig. [7\(](#page-5-0)a). As can be seen, the adsorption capacity rapidly increased within the frst 20 min, and the adsorption equilibrium was reached within 60 min. This result was attributed to the sufficient active sites on CNUIO and the large concentration gradient at the initial stage. As the adsorption progressed, the active sites on the CNUIO surface became saturated, resulting in almost no increase in adsorption capacity.

The adsorption behavior of U(VI) was simulated by the pseudo-frst-order model (Eq. [\(4\)](#page-4-2)), pseudo-secondorder model (Eq. ([5\)](#page-4-3)), and intraparticle difusion model (Eq. ([6](#page-4-4))):

$$
\ln(q_e - q_t) = \ln q_e - k_1 t \tag{4}
$$

$$
\frac{t}{q_t} = \frac{1}{k_2 \cdot q_e^2} + \frac{t}{q_e} \tag{5}
$$

$$
q_t = k_i \cdot t^{\frac{1}{2}} + C \tag{6}
$$

where q_e is the equilibrium adsorption capacity (mg/g), and q_t (mg/g) is the adsorption capacity at time t (min). k_l (min^{-1}) , k_2 (min⁻¹), and k_i (mg/m·min^{1/2}) are the adsorption rate constants of the pseudo-frst, pseudo-second, and intraparticle difusion models, respectively.

The dynamic model fitting curves are plotted in Fig. $7(b)$ $7(b)$ –(d), and the fitting parameters were listed in Table [1](#page-5-1). The equilibrium adsorption capacity ftted in the pseudo-second-order kinetic model was closer to the U(VI) adsorption capacity obtained from the test, and the correlation coefficient $(R^2 = 0.999)$ was high, indicating that the pseudo-second-order kinetic model could describe the adsorption process better. Thus, the adsorption was mainly based on the chemical adsorption [[29\]](#page-11-26). In addition, as intercept not zero, intraparticle difusion is not the only rate limiting step.

Fig. 7 Efect of contact time on U(VI) adsorption by CNUIO (**a**), pseudo-frstorder model (**b**); pseudosecond-order model (**c**), intra-particle-difusion model (**d**). ($pH = 6$, $M/V = 0.4$ g/L, $C_{U(VI)} = 10$ mg/L, $T = 298$ K)

Adsorption isotherms and thermodynamic analysis

To further explore the adsorption behavior, the experimental data were fitted by the Langmuir model (Eq. ([7](#page-5-2))) and Freundlich isotherm model (Eq. [\(8](#page-5-3))).

$$
\frac{C_e}{q_e} = \frac{1}{b \cdot q_{max}} + \frac{C_e}{q_{max}} \tag{7}
$$

$$
\ln q_e = \ln k_F + \frac{1}{n} \ln C_e \tag{8}
$$

where C_e is the concentration of U(VI) after adsorption equilibrium (mg/L), *b* is Langmuir adsorption equilibrium constant (L/mg), q_{max} is the maximum adsorption capacity

 (mg/g) , k_F is the Freundlich adsorption equilibrium constant, and *n* is a dimensionless constant.

The fitting curves were shown in Fig. [8](#page-6-0), and more fitted parameters were provided in Table [2](#page-6-1). A comparison of the correlation coefficient between the two models revealed that the process of U(VI) adsorption on CNUIO was more consistent with the Langmuir model. The adsorption process was a uniform monolayer adsorption, and the interaction between adjacent uranyl ions could be ignored. The separation factor R_L (R_L=1/(1+bC₀)) [\[30\]](#page-11-27) in the Langmuir model was 0.423, 0.510 and 0.609 in the range of $(0-1)$, thereby demonstrating that the adsorption of U(VI) by CNUIO was favorable. Furthermore, the maximum adsorption capacity was calculated from the Langmuir model was 261.16 mg/g. The comparison of adsorption

Fig. 8 The ftting of adsorption isotherm model. (pH=6, $M/V = 0.4$ g/L, $t = 60$ min)

$$
\Delta G^0 = -RT \cdot \ln K^0 \tag{10}
$$

where K^0 is the distribution coefficient, *R* is the universal gas constant (8.312 J mol⁻¹ K⁻¹), *T* is the temperature (K). The thermodynamic parameters for the adsorption of U(VI) on CNUIO were listed in Table [4.](#page-6-5) The values of ΔH^0 and ΔS^0 were determined from the intercept and slope of $ln K^0$ and 1/T linear curve (Fig. [9](#page-6-6)), and the value of ΔG^0 at the three temperature was calculated according to the above formula.

 ΔG^0 < 0 and ΔH^0 > 0 confirmed that the adsorption was a spontaneous endothermic process. $\Delta S^0 > 0$ indicated an increase in disorder throughout adsorption. Meanwhile, the value of ΔG^0 decreased as temperature increased. This result indicated that the rise in temperature was conducive to the adsorption of U(VI) on CNUIO because this phenomenon can provide more energy for the reaction

Table 2 Parameters of Langmuir and Freundlich model of U(VI) at 293, 303, 313 K	T/K	Langmuir			Freundlich		
		q_{max}		R^2	K_E	n	R^2
	293	225.34	0.017	0.996	5.552	1.384	0.967
	298	235.42	0.012	0.994	7.080	1.542	0.949
	303	261.16	0.008	0.994	9.184	1.770	0.920

Table 3 Comparison of the capacities with other adsorbents for U(VI)

capacities of various uranium adsorbents was provided in Table [3](#page-6-2). CNUIO exhibited superior adsorption performance, which verifed its great potential in the feld of uranium-containing water treatment.

In order to better refect the feasibility of the adsorption process, the thermodynamic parameters entropy change (ΔS^0) , the enthalpy change (ΔH^0) , and the standard free energy charge(ΔG^0) were calculated according to the following Eqs. (9) (9) and (10) (10) (10) .

Fig. 9 The plots of $ln K^0$ versus 1/T for U(VI) adsorption on CNUIO

Table 4 CNUIO absorbs the thermodynamic parameters of U(VI)

ΔG^{0} / (KJ mol ⁻¹)			ΔH^{0} / (KJ mol ⁻¹)	$\Delta S^{0}/(J \text{ mol}^{-1})$	
293 K	298 K	303 K	12.43	54.94	
-3.66	-3.97	-4.20			

process and promote the formation of stable chemical bonds between the surface of adsorbent and uranyl ions, thereby promoting the adsorption [\[36\]](#page-12-0).

Fig. 10 The effect of cycle times on U(VI) adsorption–desorption by CNUIO. (pH = 6, M/V = 0.4 g/L, $C_{U(VI)}$ = 10 mg/L, $T = 298$ K)

Adsorption–desorption experiment of CNUIO

The fve adsorption–desorption cycles of CNUIO using 0.1 mol/L HCl are shown in Fig. [10.](#page-7-0) The initial adsorption rate and desorption rate of CNUIO were 92.55% and 93.27%, respectively. In the frst three experiments, the effective removal of $U(VI)$ could still be maintained (removal rate $> 85\%$). When the desorption experiment was repeated fve times, the adsorption rate decreased to about 80% probably because some adsorption sites on the material surface were not successfully desorbed during the desorption process. In the process of acid desorption, part of H^+ occupied the surface binding site. Although the desorbed adsorbent was washed to neutral several times before the next cycle, the efect of acid treatment was irreversible, resulting in the gradual reduction in removal rate. The fve adsorption–desorption tests demonstrated that CNUIO had a strong renewable capacity within a short time, and multiple cycles reduced its adsorption capacity.

Characterization of the adsorbents

SEM–EDS analysis

The SEM images of $g - C_3N_4$, UiO-66, and CNUIO are given in Fig. [11](#page-7-1). $g - C_3N_4$ was composed of dense, thick-layered block structures, and its surface was relatively smooth

Fig. 11 SEM images of g-C3N4 (**a**), UiO-66 (**b**), CNUIO (**c**), EDS patterns of CNUIO adsorption U(VI) before(**d**), after (**e**)

(Fig. [11](#page-7-1)(a)). UiO-66 had an obvious cubic structure with a smooth surface and a uniform particle size (Fig. $11(b)$ $11(b)$). CNUIO had a rougher and more wrinkled structure than $g - C_3 N_4$ (Fig. [11\(](#page-7-1)c)). Moreover, $g - C_3 N_4$ had a small particle aggregation, indicating that UiO-66 nanoparticles were successfully loaded on the $g - C_3N_4$ layer, and a small amount was intercalated between $g - C_3N_4$ layers. After the introduction of UiO-66, the thickness of block $g - C_3N_4$ became thin, which greatly increased its specifc surface area and promoted U(VI) adsorption.

The EDS elemental energy spectra of CNUIO before and after $U(VI)$ adsorption are shown in Figs. $11(d)$ and (e). The elemental composition of CNUIO before absorption mainly consisted of O, C, N, and Zr (Fig. $11(d)$ $11(d)$). The abundant O and N elements formed oxygen-containing and nitrogencontaining functional groups, thereby providing numerous active sites for U(VI) adsorption. The increase in uranium peak in the Fig. $11(e)$ $11(e)$ proved that U(VI) was successfully adsorbed onto the sample surface. The drastic decrease in weight $(\%)$ of Zr after U(VI) adsorption may be the interaction between the Zr–O bond and U(VI).

XRD analysis

The crystal structure of $g - C_3N_4$ and CNUIO are characterized via XRD. Figure [12](#page-8-0) shows two characteristic peaks at 13.1° and 27.4° in $g - C_3N_4$, corresponding to planar packing of tri-s-triazine units are the (100) peak and interlayer stacking of conjugated aromatic system as the (002) peak, respectively [\[37\]](#page-12-1). The decrease of the (002) peak value in CNUIO indicated that the graphite layer spacing became larger, further confrming the intercalation phenomenon of UiO-66.

Fig. 12 XRD patterns of $g - C_3N_4$ and CNUIO

BET analysis

The N_2 adsorption–desorption isotherms of $g - C_3N_4$ and CNUIO are shown in Fig. [13](#page-8-1). The text parameters are summarized in Table [5.](#page-8-2) The adsorption curves of CNUIO were similar to those of the typical type IV isotherm with obvious H3 hysteresis loops, indicating the presence of mesopores in the materials $[38]$ $[38]$ $[38]$. The smaller pore size of the composite indicated that UiO-66 particles stay in the channel of $g - C_3N_4$, resulting in the increase of specific surface area from 5.92 to 40.03 m^2/g . The incorporation of UiO-66 substantially enlarged the specifc surface area and the pore volume of $g - C_3N_4$, further confirming that the excellent adsorption performance of CNUIO could be attributed to its large specifc surface area.

Mechanisms of U(VI) adsorption on CNUIO

FT‑IR spectroscopy

The FT-IR spectra of CNUIO before and after adsorption only slightly changed (Fig. [14\)](#page-9-0), indicating that the structure and surface functional groups of CNUIO were not destroyed during the adsorption process. This result also indicated that the material had good regeneration properties. After U(VI)

Fig. 13 N_2 adsorption–desorption isotherms of $g - C_3N_4$ and CNUIO

Table 5 BET surface area and pore parameters of the $g - C_3N_4$ and CNUIO

Sample	S_{BET} (m ² /g)	Pore volume $\text{cm}^3\text{/g}$	Pore size (nm)
$g - C_3 N_4$	5.92	0.029	20.17
CNUIO	40.03	0.052	5.22

Fig. 14 FT-IR spectra before and after CNUIO adsorption U(VI)

adsorption, some of the peaks showed the changes of displacement and strength. The increase in the band strength at 923.71 cm⁻¹ was attributed to the O = U = O stretching vibration [[39\]](#page-12-3). The main peak shifted, the broad peak at 3000–3500 cm^{-1} was associated with the stretching vibration of N–H and –OH, resulting from uncondensed amino groups $(-NH₂– or –NH_–)$ and absorbed water. However, the shape and strength of the peak did not remarkably change, which might have been caused by the complexation between N–H and –OH and U(VI) [[40](#page-12-4)]. Several typical vibrations of carbon–nitrogen heterocycles were detected within the 1200–1700 cm^{-1} wavenumber range. The C = N tensile vibration peaks at 1639.22 and 1573.86 cm^{-1} shifted to 1634.57 and 1574.40 cm⁻¹, respectively [[41](#page-12-5)]. The C-N tensile vibration peaks at 1408.87, 1321.65, and 1240.65 cm⁻¹ moved to 1413.37, 1329.43, and 1249.07 cm−1, respectively [[42\]](#page-12-6). The N–H stretching vibration peak at 886.60 cm⁻¹ caused by incomplete condensation of amino moved to 887.76 cm⁻¹ [\[43\]](#page-12-7). These movements may be the formation of complexes between nitrogen-containing functional groups and U(VI) in CNUIO. Furthermore, the Zr–O bond (744.07 cm^{-1}) peak position did not change, but the vibration peak intensity increased, which indicated that Zr–O was also involved in the reaction [[44](#page-12-8)]. On the basis of the changes in FTIR spectra before and after adsorption, $N-H$, $-OH$, $C=N$, $C-N$ and $Zr-O$ are speculated to be the main adsorption sites in the process of U(VI) adsorption by CNUIO.

XPS analysis

in the material were consistent with the EDS results (Fig. [15\(](#page-10-0)a)). The two peaks at the binding energy of 392.70 and 381.93 eV were attributed to U4f $_{5/2}$ and U4f $_{7/2}$ peaks in hexavalent form, respectively (Fig. [15\(](#page-10-0)b)), illustrating that U(VI) was only adsorbed onto the CNUIO surface via oxidation [[45](#page-12-9)].

The typical Zr3d $_{3/2}$ and Zr3d $_{5/2}$ peaks at 185.24 and 182.85 eV revealed the existence of Zr^{4+} (Fig. [15](#page-10-0)(c)) [\[46](#page-12-10)]. After adsorption, the two peaks moved to the low binding energy end probably because of the interaction between the Zr–O bond and U(VI) [\[47](#page-12-11)]. The high-resolution spectrum of C1s is shown in Fig. [15](#page-10-0)(d). The peak at 284.80 eV came from the graphitic carbon or the amorphous carbon of the sp² C–C bond in g-C₃N₄, whereas the peak at 288.19 eV was the sp² hybridized carbon (N–C=N) in the triazine ring structure that was bound to nitrogen atom [\[48](#page-12-12)]. The weak peak at 286.01 eV was attributed to the C–NH_x $(x=1, 2)$ groups at the edge of heptazine [[49](#page-12-13)]. The pre-adsorption N1s spectra at 404.64, 400.42, and 398.63 eV belonged to N–oxide [\[50\]](#page-12-14), the N–H bond, and the C–N = C sp² hybrid nitrogen, respectively (Fig. $15(e)$) [\[51](#page-12-15)]. The binding energy of the three peaks increased after adsorption because the lone pair of electron in the N atom transferred to the unoccupied orbital of U electron, resulting in a decrease in electron cloud density and the positive movement of binding energy [[52](#page-12-16)]. Additionally, the decrease of difraction peak intensity can be attributed to the combination of these functional groups with U(VI), which is consistent with the FTIR results. In the spectrum of O1s, the peak at 532.30 eV corresponded to the surface hydroxyl group of melamine thermal polymerization [\[53](#page-12-17)], whereas the peaks at 531.65 and 530.15 eV represented the $C = O$ and $Zr-O$ bonds, respectively (Fig. $15(f)$ $15(f)$) [[54](#page-12-18)]. After U(VI) adsorption, the binding of O1s peaks shifted to higher, thereby demonstrating that the oxygen-containing functional groups on the surface of CNUIO provided active sites for U(VI) adsorption. To sum up, the above results demonstrated that the nitrogen- and oxygen-containing functional groups were in charge of the interaction between CNUIO and U(VI).

Conclusion

In this work, CNUIO was synthesized and successfully applied to U(VI) adsorption. Tests demonstrated that this composite had good reusability. Under the conditions of pH 6, absorbent dosage = 0.4 g/L, $t = 120$ min, and $C_{U(VI)} = 10$ mg/L, the adsorption rate of U(VI) by CNUIO was 95.01%. U(VI) adsorption onto CNUIO was strongly dependent on pH but independent of ionic strength, indicating that the adsorption process was dominated by inner-sphere surface complexation and electrostatic attraction. The adsorption process ftted well with

the pseudo-second-order kinetic model and the Langmuir isothermal adsorption model, indicating that U(VI) adsorption was mainly monolayer chemical adsorption on the CNUIO surface. The maximum Langmuir adsorption capacity was 261.16 mg/g. Thermodynamic parameters $(\Delta G^0 < 0$ and $\Delta H^0 = 12.427$ kJ mol⁻¹) revealed that U(VI) adsorption by CNUIO was a spontaneous endothermic process. SEM–EDS and BET analysis revealed that the

specifc surface area of CNUIO substantially increased, which promoted U(VI) adsorption. According to the results of FTIR spectroscopy and XPS, the underlying adsorption mechanism was the synergistic complexation of nitrogen-containing and oxygen-containing functional groups. In conclusion, CNUIO can be used as a suitable adsorbent in practical radioactive wastewater treatment.

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Declarations

Conflict of interest The authors declare that they have no known competing fnancial interests or personal relationships that could have appeared to infuence the work reported in this paper. The authors declare the following fnancial interests/personal relationships which may be considered as potential competing interests.

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