

Synthesis of the *p*-tert-butyl calix[4] arene symmetrical sulfide derivatives and its extraction properties towards U(VI) from aqueous solution

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Abstract The *p*-tert-butyl calix[4]arene symmetrical sulfide derivatives (**3a** and **3b**) were successfully synthesized using *p*-tert-butyl calix[4]arene as the raw material and were characterized by FT-IR. The effects of pH value, temperature, and contact time on the U(VI) extraction with compounds **3a** and **3b** from aqueous solution were systematically investigated. The results showed that the optimum pH value for uranium extraction was 4.0 and the extraction equilibration time was 90 min. It is also found that the pseudo-second-order kinetic model ($R^2 > 0.999$) was better fitted to the extraction process. The thermodynamic parameters of the enthalpy (ΔH^θ) were all negative, indicating that the extraction reaction were exothermic reaction.

Keywords *p*-Tert-butyl calix[4]arene · Extraction properties · Chemical modifying · U(VI)

Introduction

In recent years, nuclear energy as a clean and efficient energy has been accelerated development and utilization, and widely used in military, aerospace, the chemical energy and other fields [1]. The demand for uranium as an important raw material for nuclear industry is increasing, and the pollution of water caused by uranium is more and more [2]. Uranium is one of the most important heavy metals with chemical toxicity and radioactivity. And uranium is through inhalation and ingestion or penetrating wound, soluble uranium compounds can also enter the body through the skin without injury, resulting in the internal irradiation and chemical toxicity [3–5], will produce damage to human nervous system, immune system, kidney, and fertility, and may lead to gene mutation and cancer [6–8]. Therefore, development of efficient and economically viable methods for removal of uranium from waste water is a very urgent and formidable task.

At present, the methods for separating heavy metals include solid-phase separation [9, 10], cloud-point separation [11], liquid–liquid extraction [12], ion exchange [13] and liquid-phase microextraction [14], etc. Among them, Solvent extraction has been widely used in the removal because of its advantages of high efficiency, easy operation, and high selectivity. And it has also some advantages in the separation and purification of heavy metals and waste water treatment [15]. Thus, the further research on suitable and ideal extractant and its industrial application has become a hot topic of research [16, 17].

The calix[n] arene is made up of the phenol unit by the ortho connection of methylene in the phenol hydroxyl group [18], and its upper and lower rims are easy to be chemical modified [19, 20].

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The cesium and strontium in the material are separated by the modified calixarene [21]. Because they have higher complexing ability and is easier to be used as extractant [22, 23]. The modification of the lower rim of calixarene is mainly based on the intermolecular hydrogen bond between phenolic hydroxyl groups of calixarene [24], by controlling the reaction conditions, the phenolic hydroxyl groups will be converted into ethers, esters, amides and other groups, and the calixarene derivatives, which have certain selectivity to heavy metal ions are obtained [25–27]. However, there are few reports about the calixarene modified by heteroatom containing groups with such strong ligands as heavy metal groups, such as alkoxy groups.

In this work, the *p*-tert-butyl calix[4]arene symmetrical sulfide derivatives (**3a** or **3b**) were successfully synthesized for the extraction of U(VI) from aqueous solution by chemical modifying of calix[4]arene as raw material. The different factors affecting the extraction behavior such as the effects of pH value, the temperature and the contact time were investigated. The extraction kinetics, isotherms and thermodynamic properties of the extraction process for U(VI) were evaluated. The parameters are important for scaling up of the process before investigating the extraction properties in continuous systems.

Experimental

Reagents

The aqueous solution containing U(VI) ions was prepared by dissolving an appropriate amount of $\text{UO}_2(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$, which was provided by the Key Discipline Laboratory for National Defence for Biotechnology in Uranium Mining and Hydrometallurgy, University of South China. All the solvents, 4-tert-butylphenol, formalin, sodium hydroxide, ethyl acetate, acetic acid, diphenyl ether, 1,3-dibromopropane, potassium carbonate, acetonitrile, dichloromethane, tetrabutylammonium iodide, sodium sulfide nonahydrate, ethanol, magnesium sulphate, methanol, arsenazo III, were obtained from Tianjin Damao Chemical Reagent Co. Ltd., China, which are of analytical grade.

Apparatus

UV–Vis 8500 (Shanghai sky Scientific Instrument Co., Ltd.) was used to determine the concentration of UO_2^{2+} in the aqueous solution containing uranium ions. PHS-3C Model pH meter (Shanghai Peng Shun Scientific Instrument Co., Ltd.) was used for measuring the pH of the aqueous solutions containing uranium ions. The extraction experiments were conducted in a THZ-82 thermostated

shaker bath (Jintan Analytical Instrument Co., Ltd.). Fourier transform infrared (FT-IR) spectroscopy was recorded on a IR Prestige-21 (Shimadzu, Japan) spectrometer using KBr pellets.

Synthesis experiment

The experimental procedure for preparation of **3a** or **3b** was described as follows (as shown in Scheme 1).

Firstly, 1.25 g of *p*-tert-butyl calix[4]arene, 4 mL 1,2-dibromomethane, 0.7231 g of K_2CO_3 (dry and weight) and 20 mL absolute acetonitrile were added into the 50 mL flask and stirred for 48 h at 70 °C. After the reaction, rotary evaporation to eliminate solvent and unreacted 1,2-dibromomethane, and the hydrochloric acid and CHCl_3 were added into residue. Then washing the organic layer to neutral, adding MgSO_4 to dry, filtering, and white crystalline powder (**2a** or **2b**) was obtained by adding methanol.

Afterward, 0.1033 g of **2a** or **2b**, 0.1373 g of four butyl ammonium iodide and 0.0855 g sodium sulfide (dry weight) were dissolved in 5 mL water and 25 mL absolute ethanol, and then stirred for 12 h at 55 °C.

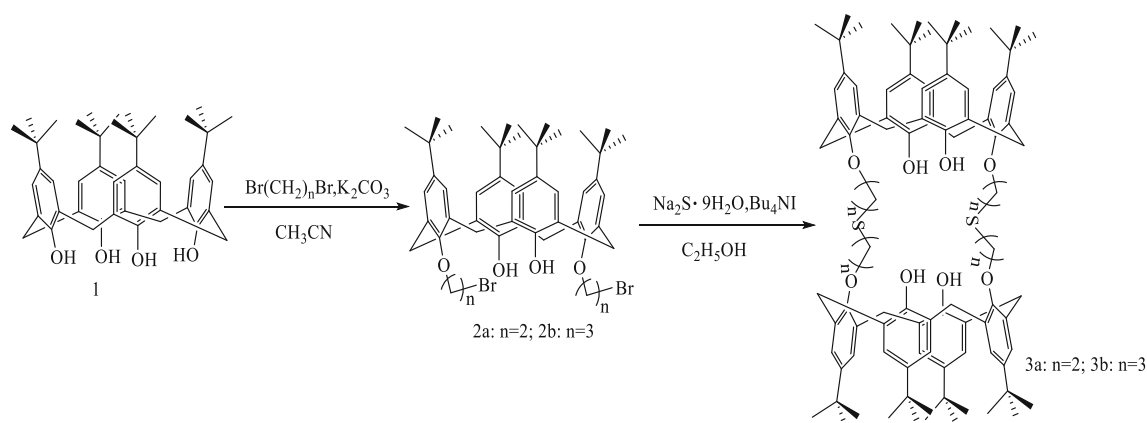
Finally, the organic layer was obtained by rotating evaporation and adding saturated sodium chloride and ethyl acetate. Then, adding MgSO_4 to dry, filtering, and the product (**3a** or **3b**) was extracted by adding methanol.

Characterization of the samples

The *p*-tert-butyl calix[4]arene symmetrical sulfide derivatives (**3a** or **3b**) were analyzed by FT-IR (IR Prestige-21, Shimadzu, Japan) using KBr pellets in the 4000–500 cm^{-1} region.

Extraction experiment

The chloroform solution of **3a** or **3b** was used as extractant of U(VI), and the standard solution of 2×10^{-4} mol L^{-1} was used. The solution of 5 mg L^{-1} U(VI) was distilled with two distilled water. According to the experimental requirements, the chloroform solution of **3a** or **3b** of the 10 mL ligand was removed in the 50 mL conical flask and U(VI) solutions with different concentrations (0.05, 0.01, 0.1 mol L^{-1}) of HCl and NaOH have been adjusted for pH of the solution, then it was placed at constant temperature (298 K) in the water bath shaker and subjected to constant temperature oscillation of 90 min. After the shaking was stopped, the appropriate pipette tip was selected to remove a certain volume of aqueous phase. The absorbance was measured by UV–Vis spectrophotometer, and the extraction rate ($E\%$) was calculated as.



Scheme. 1 Synthesis route of the p-tert-butyl calix [4] arene symmetrical sulfide derivatives (**3a** and **3b**)

$$E(\%) = \frac{C_0 - C_e}{C_0} \times 100\% \quad (1)$$

where C_0 and C_e are the initial and the final concentration of U(VI) in solution phase, respectively.

Effect of pH

At the temperature of 25 °C, the initial concentration of the chloroform solution of **3a** or **3b** was 2×10^{-4} mol L⁻¹, and the initial concentration of U(VI) was 2.1×10^{-5} mol L⁻¹, and the contact time was 90 min, the effect of the extraction of U(VI) on the chloroform solution of **3a** or **3b** was discussed when the initial pH value of the aqueous solution containing U(VI) ions was 2–8.

Effect of temperature

The complete extraction isotherms of U(VI) was obtained by placing 10 mL the chloroform solution of **3a** or **3b** chloroform solution into a series of conical flasks containing 50 mL of the aqueous solution containing U(VI) ions with the initial concentration of 2.1×10^{-5} mol L⁻¹ and pH 4.0 [28]. The flasks were agitated for 90 min, while keeping the temperature at 25, 30, 35, 40 or 45 °C. After the equilibration, the residual concentration of U(VI) was determined.

Effect of contact time

The chloroform solution of **3a** or **3b** was added to the aqueous solution containing U(VI) ions with the initial concentration of 2.1×10^{-5} mol L⁻¹, adjusted pH 4.0 under the experimental conditions. At the constant temperature of 25 °C, controlling the shaker oscillation time were 5, 10, 20, 30, 60, 90, 120, 180 min, and the residual concentration of U(VI) ions was measured.

Results and discussion

Characterization

The results are shown in Fig. 1. From the spectra in Fig. 1(**3a**), it can be seen that antisymmetric stretching vibration peaks at 1234.4 cm⁻¹ for the –C–O–C and skeleton vibration peaks at 1581.6 and 1479.4 cm⁻¹ for the aromatic ring. It also can be found that antisymmetric stretching vibration absorption peaks (wide and strong) at 2951.1 and 2862.4 cm⁻¹ for the –CH₃, the antisymmetric bending vibration peaks at 1361.7 cm⁻¹ for the C–H in the tertiary butyl group, and the symmetric stretching vibration absorption peaks at 1020.3 cm⁻¹ for the C–S. In Fig. 1(**3a**), the characteristic peaks for the –(CH₂)₃– appeared at 728.9 cm⁻¹ and the peaks at 742.6 cm⁻¹ for the –(CH₂)₂– in Fig. 1(**3b**), which implies two target compounds in Scheme 1.

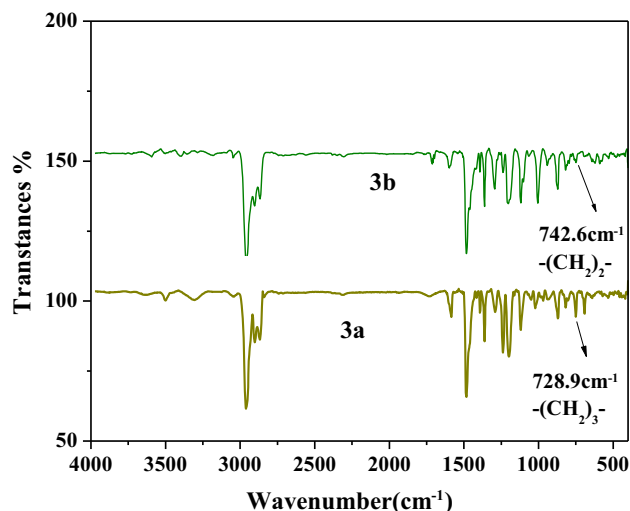


Fig. 1 FT-IR spectra of **3a** or **3b**

Effect of pH

Figure 2 shows the relationship between pH and extraction rate. In this extraction experiment, it is clear that pH has a great effect on the extraction of U(VI) by the chloroform solution of **3a** or **3b**. As pH increases (2.0 < pH < 4.0), the extraction percentage of U(VI) increased greatly from 2.0 to 4.0, which could be due to at low pH, the protonation affect the binding ability of –OH or –S– functional groups. When pH from 5.0 to 8.0, the extraction rate was reversed, which was due to at high pH, the hydrolysis may be the reason of decreasing the extraction properties [29]. It was

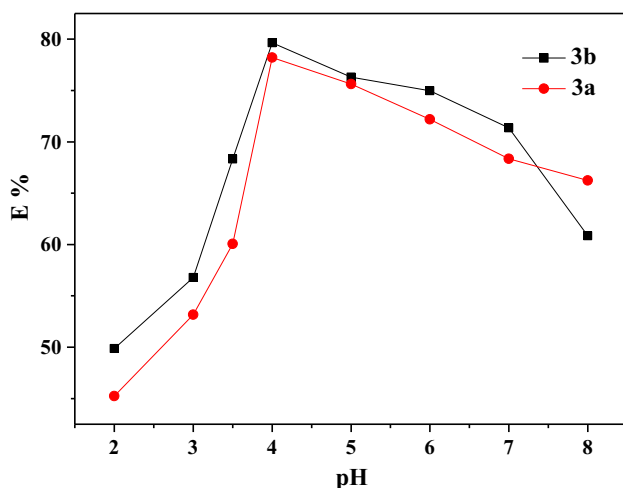


Fig. 2 Effect of pH on the extraction of U(VI) on **3a** or **3b**; $C_{U(VI)} = 2.1 \times 10^{-5} \text{ mol L}^{-1}$; contact time = 90 min; temperature = 25 °C

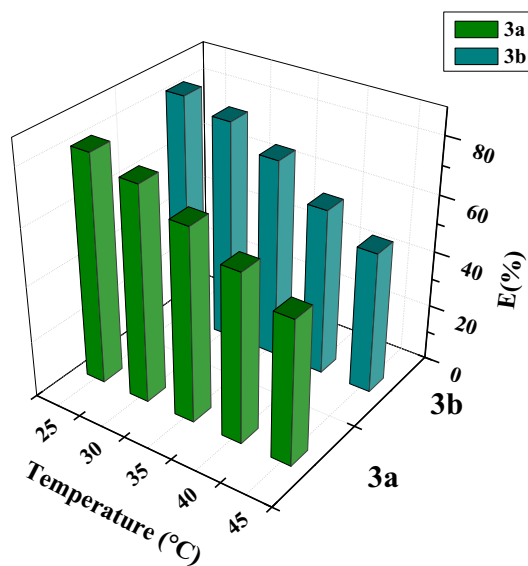


Fig. 3 Effect of temperature on the extraction of U(VI) on the chloroform solution of **3a** or **3b**; $C_{U(VI)} = 2.1 \times 10^{-5} \text{ mol L}^{-1}$; pH 4.0; contact time = 90 min

unfavorable for the extraction of metal ions by **3a** or **3b**. It was clear that the highest uptake value was observed at pH 4.0 for both **3a** or **3b**. Therefore, pH 4.0 was chosen for extraction of U(VI) in the experiment.

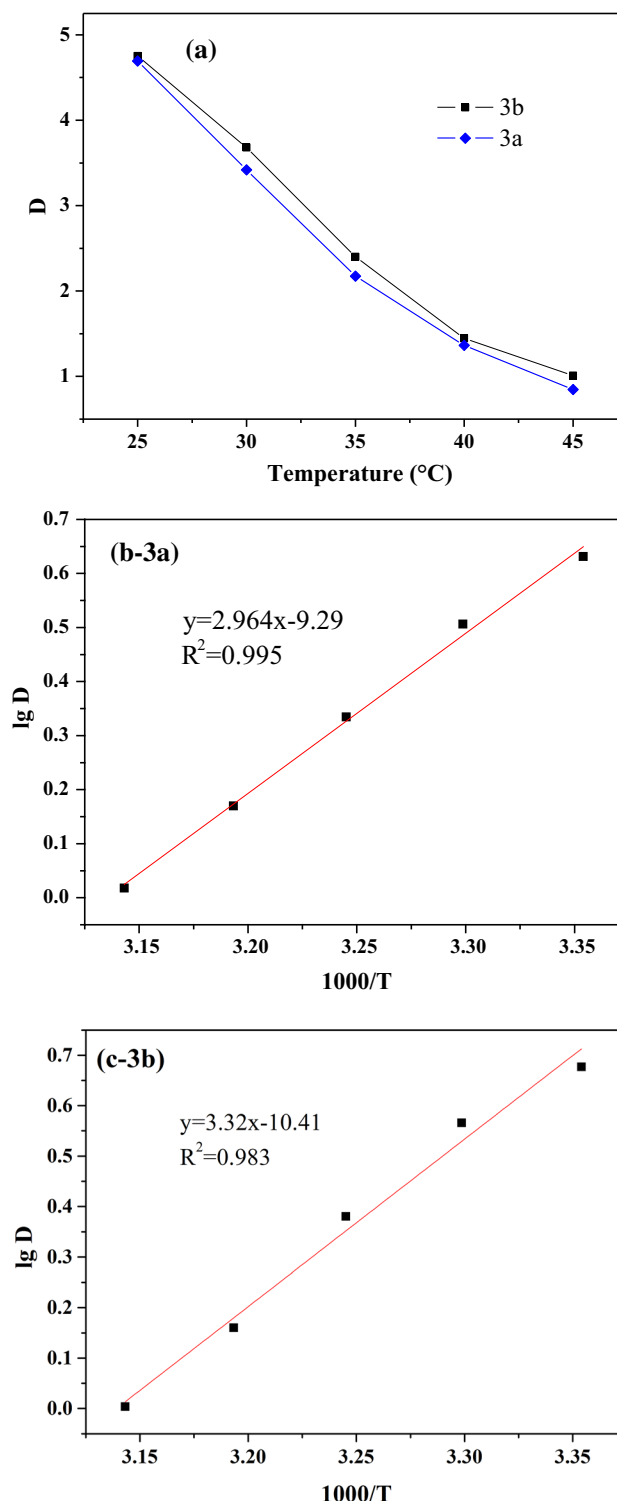


Fig. 4 Effect of temperature on the extraction of U(VI) on the chloroform solution of **3a** or **3b**

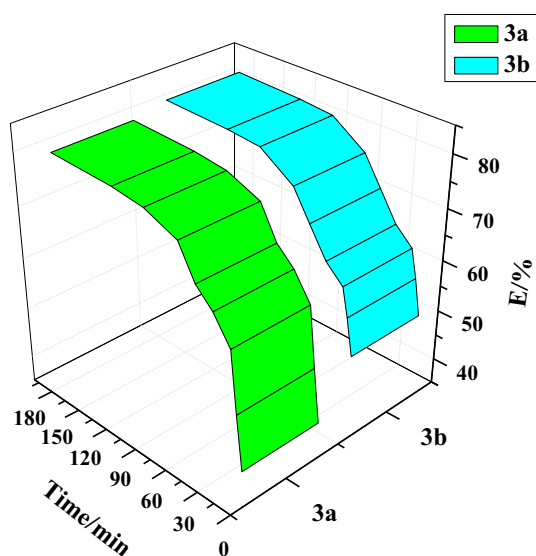


Fig. 5 Effect of contact time on the extraction of U(VI) on the chloroform solution of **3a** or **3b**; $C_{U(VI)} = 2.1 \times 10^{-5} \text{ mol L}^{-1}$; pH 4.0; temperature = 25 °C

Extraction thermodynamics

From the spectra in Fig. 3, it can be seen that with the temperature increased, the extraction rate of U(VI) were decreased by the chloroform solution of **3a** or **3b**. As can be seen from Fig. 4a, the extraction rate of U(VI) decreased with the increase of temperature, indicating that the extraction reaction is an exothermic reaction, and the increase of temperature is unfavorable to the extraction [16].

After drawing a linear fit $\lg D$ versus $1000/T$ (Fig. 4b, c), we obtained a straight slope for calculating the enthalpy change (ΔH^θ). The results shown that ΔH^θ for the extraction of U(VI) with the chloroform solution of **3a** or **3b** are

– 56.75 and – 63.57 kJ/mol^{-1} , respectively, which means the extraction process is exothermic.

Extraction kinetics

The extraction kinetics were studied for describing the rate of extraction process, and the removal of U(VI) ions changing with contact time is shown in Fig. 5. The results show that as the shaking time increased, the extraction rate of extractant U(VI) increased with the increase of time and the concentrations remained relatively unchanged after 90 min, which indicated that the process of extraction had reached equilibrium. Therefore, the best extraction time of the chloroform solution of **3a** or **3b** in this experiment was 90 min. This may be due to the hydroxyl functional groups and the sulfur groups in the extractant were in contact with U(VI), and the binding sites were many and the rate was fast.

With the contact time prolonged, the binding site on the extractant functional groups was close to saturation, and the change of extraction amount was not obvious. In order to further study the relationship between the extraction amount and time of extractant U(VI), the experimental data were fitted by pseudo-first-order kinetic model and pseudo-second-order kinetic model. The fitting parameters of the model were shown in Table 1.

As can be seen from Table 1, the pseudo-second-order kinetic equation was more relevant than the pseudo-first-order kinetic equation, so the extraction process of U(VI) is in line with the pseudo-second-order kinetic equation. The formulas for the pseudo-first-order kinetic equation and the pseudo-second-order kinetic equation were (2) and (3),

$$\lg(q_e - q_t) = \lg q_e - \frac{k_1}{2.303} t \tag{2}$$

Table 1 Kinetics parameters of U(VI) extraction

Temperature (°C)	Compound	Pseudo-first-order kinetic equation $\ln(q_e - q_t) = \ln q_e - k_1 t$			Pseudo-second-order kinetic equation $t/q_t = 1/k_2 q_e^2 + t/q_e$		
		K_1 (min^{-1})	Q_e (mg g^{-1})	R^2	K_2 ($\text{g mg}^{-1} \text{min}$)	Q_e (mg g^{-1})	R^2
25	3a	0.024	2.361	0.631	0.021	18.331	0.9993
	3b	0.029	3.891	0.575	0.020	18.523	0.9994
30	3a	0.036	6.217	0.734	0.0183	18.209	0.9994
	3b	0.031	5.693	0.803	0.0179	18.461	0.9993
35	3a	0.068	62.302	0.615	0.0138	18.210	0.9992
	3b	0.071	68.591	0.713	0.0135	18.445	0.9993
40	3a	0.056	50.746	0.723	0.0132	17.316	0.9991
	3b	0.045	42.562	0.785	0.0129	17.462	0.9992
45	3a	0.025	3.213	0.896	0.009	16.869	0.9990
	3b	0.022	2.863	0.833	0.009	16.913	0.9991

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} t \quad (3)$$

where q_e represents the equilibrium extraction capacity (mg L^{-1}), q_t represents the extraction capacity at t moments (mg L^{-1}), k_1 represents the pseudo-first-order extraction rate constant (min^{-1}), k_2 represents the pseudo-second-order extraction rate constant [$\text{g}(\text{mg min})^{-1}$], t (min).

Conclusion

- (1) By means of the infrared spectroscopy analysis of the *p*-tert-butyl calix [4] arene symmetrical sulfide derivatives (**3a** or **3b**), it was found that **3a** or **3b** provided a large surface area and more extraction sites for the extraction of U(VI).
- (2) The chloroform solution of **3a** or **3b** all have a better extraction effect on U(VI). When the optimum pH value is 4.0, the temperature is 25 °C, and the initial concentration of U(VI) is $2.1 \times 10^{-5} \text{ mol L}^{-1}$. The extraction process has the characteristics of stage extraction, which is characterized by rapid surface extraction. At 60 min, the extraction rates of U(VI) on **3a** or **3b** was respectively 76.39 and 76.29%, and reached equilibrium at 90 min.
- (3) The extraction of U(VI) from the aqueous solution containing U(VI) ions on the chloroform solution of **3a** or **3b** is consistent with the pseudo-second order kinetic model. The process of extraction U(VI) is consistent with the pseudo-second order kinetic model ($R^2 > 0.999$), and the process of extraction is chemical extraction. The enthalpy of extraction reaction is less than zero, indicating that it is an exothermic reaction.

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