REVIEW PAPER

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Recent advancements in manufacturing technologies of microcellular polymers: a review

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Abstract

Significant research efforts are being pursued by numerous plastic foaming industries towards the transformation of macrocellular polymer foam to microcellular and imminent future is trending towards nanocellular polymer foams. These novel foamed plastic possess enhanced properties and easy tunability which could potentially fulfill many of the ever-evolving industrial requirements. These industrial requirements have led to several advancements in the current manufacturing technologies and as a result, new industrial-scale production technologies are being researched upon cellular plastics and its allied composites. The microcellular polymeric foams have huge industrial demand due to their improved properties such as specific strength, energy absorption, and thermal/electrical/acoustic insulation compared to their unfoamed counterparts. This review article aims to summarise the existing manufacturing technologies for producing microcellular polymers and provide an up-to-date report on the recent advancements in these manufacturing technologies.

Keywords Microcellular · Ultrasound-aided foaming · Bimodal foaming · EMI shielding · Wood fiber composites · Porous foam

Introduction

The polymer foaming transforms solid polymers into cellular structured polymeric composites by incorporation of a large number of very small-sized bubbles to reduce the use of material without a significant effect on the mechanical properties of the product. In the 1930s, the first polymer foam with macrocellular structure was reported [1], and since then the research & development is being consistently pursued towards the smaller cell types of cellular structure was reported by Prof. Suh et.al [2] from Massachusetts Institute of Technology and subsequently, in the early 2000s, the nanocellular polymeric structure came into existence. The development in this field of research still continues to endeavour through numerous cutting-edge innovation for several diverse industrial

Rupesh Dugad dugadrupesh23@gmail.com applications [1]. The microcellular plastics are being extensively used in a wide range of applications such as biomedical, automotive, naval, aerospace, safety goods, insulation purpose in construction, packaging, filters, membranes, cushioning owing to its properties like strength to weight ratio, toughness, insulating properties, flexibility, etc. [2–6]. These cellular materials can be classified according to the interconnectivity of cell structure, cell size, cell density, expansion ratio, elastic modulus [1, 7–10]. Figure 1 shows a clear depiction of the classification of foamed polymers.

Mechanism of polymer foaming

The mechanism of polymer foaming typically comprises three distinct stages which are clearly shown in Fig. 2 [1, 3, 11]. The first stage is the dissolution of gas or blowing agent. In this stage, a polymer sample (solid or melt) is loaded with a high-pressure blowing agent such as CO_2 or N_2 . The dissolution of the blowing agent in the polymer matrix occurs over an extended period of time, till full saturation level is achieved. The dissolution process involves the mixing of two different phases (gas & solid) to form a single-phase homogenous solution. The dissolution of gas or blowing agent in polymer also causes plasticization effect which assists in the flow of polymer matrix during the foaming process. Plasticization

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Fig. 1 Classification of foamed polymers

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|---|-----|----|------|--------|-------------|-----|
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| Cell Connectivity | Open – Interconnected cell structure Closed – Isolated cell structure |
|---------------------------------------|--|
| Elastic Modulus (EM) | Soft – EM < 68.6 MPa Semi-rigid – EM between 68.6 - 686 MPa Rigid- EM > 686 MPa |
| Expansion Ratio (ER) | High Density - ER < 4 Medium Density - ER between 4-10 Low Density - ER between 10-40 Ultra-low Density - ER > 40 |
| Cell Size (CS) & Cell Density (CD) | $\label{eq:macro-cellular-CS} \begin{array}{l} \textbf{Wacro-cellular-CS} > 300 \ \mu\text{m} \ \& \ \text{CD} < 10^6 \ cells/cm^3 \\ \hline \textbf{Fine-cellular} - CS \ between \ 10^- \ 300 \ \mu\text{m} \ \& \ \text{CD} \ between \ 10^6 \ - \ 10^9 \ cells/cm^3 \\ \hline \textbf{Micro-cellular} - CS < 10 \ \mu\text{m} \ \& \ \text{CD} \ between \ 10^9 \ - \ 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \text{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \text{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \text{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \text{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \text{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \text{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \text{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \text{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \textbf{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \textbf{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \textbf{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \textbf{CD} > 10^{15} \ cells/\ cm^3 \\ \hline \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \textbf{Nano-cellular} - CS < 1 \ \mu\text{m} \ \& \ \textbf{Nano-cellular} - \ Nano-ce$ |

occurs due to the suppression of glass transition temperature & result in the decrease of stiffness, viscosity and increases the chain mobility of polymer materials which cause the reduction in energy barrier for cell nucleation [12]. The second stage is cell nucleation and cell growth. Thermodynamic instability is the basic principle behind cell nucleation. The thermodynamic instability can be induced either by a sudden rise in temperature or a sudden drop in pressure. Due to this thermodynamic instability, the solubility of CO₂ within the polymer matrix drops instantaneously and the dissolved blowing agent emerges out from the polymer matrix, thereby creating a large number of nuclei. Finally, the third stage is the cell stabilization stage. To preserve the so-developed cell structure, the foamed sample is guenched in water or other suitable cooling media. Even though after quenching, cell growth may continue.

The blowing agent plays an important role in the transformation of solid polymer into the cellular structured polymer. Two types of blowing agents are using generally in foam manufacturing namely,- chemical blowing agent (CBA) and physical blowing agent (PBA) [1, 5, 7, 13]. The foaming with PBA has many advantages over foaming with CBA, such as lesser materials usage, no residues, and lower cost. In foaming with PBA, mostly CO_2 or N_2 are used as blowing agent because of their inertness, easiness to integrate, availability, and notably low cost [14, 15]. The cell density is the function of saturation pressure [16]. The increase in saturation pressure increases the dissolution of the blowing agent within the polymer matrix & leads to higher cell density [17].

Traditional manufacturing technologies of microcellular polymers

The traditional techniques generally used for microcellular polymeric foam manufacturing are; batch solid-state microcellular foaming, extrusion foaming, and injection mould foaming. Out of which mostly extrusion foaming and injection mould foaming are commercially used for foam production and batch solid-state foaming is being used for research purposes.

Batch solid-state microcellular foaming

Batch solid-state foaming is a non-continuous foam formation technique as in this technique a saturation of the polymer sample and the foaming (i.e. cell nucleation and cell growth) occurs individually. The polymer sample to be foamed is in solid-state and is processed in batches/group in a closed vessel at defined saturation parameters, thus named as batch solid-state foaming [1, 3, 9, 12, 18]. The batch solid-state foaming process is further classified as- Pressure-induced (One-step) and Temperature-induced (Two-step). These two techniques are discussed in detail below.

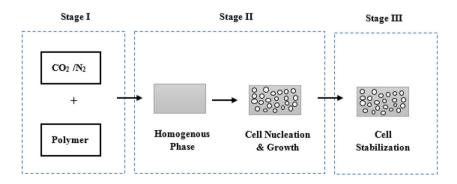


Fig. 2 Mechanism of polymer foaming

Pressure-induced (one-step) technique- In this technique, a solid polymer sample is placed inside an autoclave vessel, which is pressurized with blowing agent at high pressure termed as saturation pressure and at a certain temperature termed as saturation temperature for a defined period of time termed as saturation time. Once the polymer sample is fully saturated, the vessel is depressurized rapidly at a high depressurization rate. This gas saturated polymer at a fully saturated state which is defined as, the state above which no more dissolution or absorption of blowing agent in the polymer sample can occur. In this type of batch foaming method, the induction of thermodynamic instability occurs due to the high pressure gradient $\left(-\frac{\partial P}{\partial t}\right)$ which results in cell nucleation and its subsequent growth. The negative sign indicates the drop in pressure with respect to time. Finally, the sample is cooled in water for stabilization of the microstructure [1, 3, 12, 19]. Figure 3 represents a schematic of the typical pressure-induced batch solid-state microcellular foaming process.

Temperature-induced (two-step) technique- In the temperature-induced technique, the sample saturation is typically done at a temperature lower than the glass transition temperature of the polymer matrix. Immediately after depressurization, the sample is taken out from the vessel and is dipped in a hot oil bath or glycerine/silicon bath [20, 21]. The bath temperature is generally kept above the glass transition temperature of the polymer matrix which is termed as foaming temperature. If the foaming temperature is above that glass transition temperature, stiffness or viscosity of polymer matrix decreases thus dissolved gas diffused out fastly and cause nucleation [22]. The time for which the saturated sample is dipped inside the hot bath is termed as the foaming time. In general, with an increase in the foaming temperature, the cell size also increases because higher temperature reduces the polymer viscosity and in turn reduces the resistance to cell growth [1, 4, 18]. In this type of batch foaming, the thermodynamic instability for cell nucleation and cell growth occurs due to the high temperature gradient $(+\frac{\partial T}{\partial t})$. The positive sign indicates the rise in temperature with respect to time. Figure 4 shows a schematic of the typical temperature-induced batch solid-state microcellular foaming process. Also, Table 1 depicts the comparison between techniques of batch solid-state microcellular foaming [1, 3, 4, 18, 22].

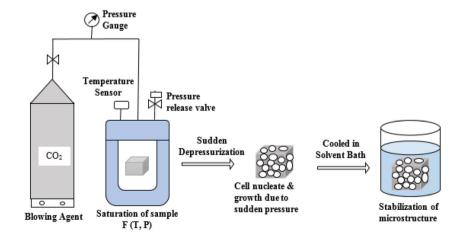
The limitation of batch solid-state microcellular foaming is that it takes a significant amount of processing time for the development of foam and the autoclave vessel capacity also limits its product dimensions. To overcome this drawback, processes like extrusion foaming and injection mould foaming were developed [22], which could manufacture microcellular foamed products at an industrial scale.

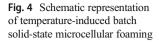
Extrusion microcellular foaming

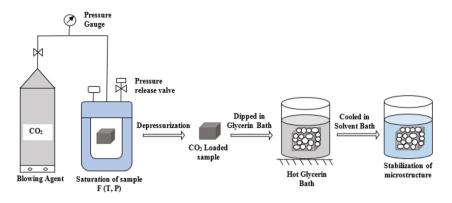
Extrusion microcellular foaming was developed by amalgamating conventional polymer extrusion process and external gas injection system which could disperse the blowing agent within the polymer melt [1]. When compared with the batch foaming process, the extrusion foaming process provides higher productivity, ease of control, versatility in endproduct properties and profiles [22]. In extrusion foaming, the polymer pellets are fed into the barrel through hopper. The pellets get melted inside the barrel due to high temperature and the blowing agent at high pressure from the external gas injection system is injected into polymer melt, typically in the compression zone of the extruder and action of shear forms a homogenous mixture.

Generally, two kinds of extrusion processes are used which are single barrel extrusion and tandem (two-barrel) extrusion. In the single barrel extrusion, melting and cooling polymer matrix occurs in the same barrel while in tandem extrusion, separate barrels are there for melting and cooling [1, 4, 7]. Significantly better results are obtained with tandem extrusion than single barrel extrusion but gas leakage possibility, setup cost & power consumption are more in tandem extrusion

Fig. 3 Schematic representation of pressure-induced batch solid-state microcellular foaming







compared to single barrel extrusion [4, 7]. Figures 5 and 6 depict a typical schematic of single extrusion and tandem extrusion microcellular foaming.

The screw motion passes the molten mixture into the second barrel, here it gets cooled to a temperature lower than temperature in the first barrel. Further cooling provided to reduce the cell coalescence. The melt pump regulates the amount of molten mixture flowing through the extruder. As the molten mixture exits the extruder die head, a large number of cells begin to nucleate and subsequently grows. The primary driving force for this nucleation is thermodynamic instability due to the high pressure gradient $(-\frac{\partial P}{\partial t})$. The cell growth occurs until it stabilizes or ruptures [7, 23]. The dispersion of the blowing agent in polymer melts significantly affects the morphology of the developed foam using extrusion process. The blowing agent injecting location in extrusion barrel affects the residence time of blowing agent which in turn affects the morphology of the developed foam [24].

Injection mould microcellular foaming

In the injection mould microcellular foaming process, the polymer pellets get melted in the barrel and the blowing agent is mixed in the molten polymer to form a homogenous mixture. The screw pushes this single phase molten mixture and is injected in the mould, the pressure drops to the atmospheric pressure and this leads to the microcellular nucleation phenomenon. The nucleated cells grow till they are stabilized. Due to the presence of gas, plasticization of polymer chain occurs due to which the viscosity of melt decreases & it leads to decrease in injection pressure. Also, the lesser clamp force is required [11, 23, 25, 26], when compared with the conventional injection moulding process. Figure 7 shows the typical schematic setup for injection mould microcellular foaming.

The cycle time required for microcellular injection mould foaming is significantly lesser than conventional injection moulding. Approximately 20–50% cycle time can be saved with microcellular injection moulding. Figure 8 shows a comparison between conventional and microcellular injection foaming.

In microcellular injection foaming, the viscosity of polymer matrix reduced due to the presence of blowing agent (i.e. CO_2/N_2) which increases the filling speed and reduced filling time. The packing pressure provided by gas in bubbles thus, holding time is almost eliminated. And as cell nucleation & growth required endothermic variation thus, cooling time is also reduced [13, 27]. Table 2 represents the comparison between traditional manufacturing processes of microcellular polymers [1, 3, 4].

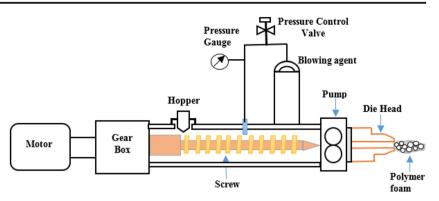
Advanced manufacturing technologies in the microcellular foaming

From the last decade, a number of innovations have occurred in the manufacturing technologies of microcellular foam.

Table 1 Comparison between techniques of batch solid-state microcellular foaming

| Comparative point | Pressure-induced technique | Temperature-induced technique |
|-------------------------------------|---|--|
| Alternate term | One-step or Batch foaming | Two-step |
| Saturation temperature | Typically higher than Tg | Less than Tg |
| Thermodynamic instability | Due to high pressure gradient $\left(-\frac{\partial P}{\partial t}\right)$ | Due to high temperature gradient $\left(+\frac{\partial T}{\partial t}\right)$ |
| Time inclusion for foam preparation | Typically 2–4 h | Typically 16–24 h |
| Crucial processing parameters | Saturation pressure, saturation temperature, depressurisation rate | Saturation time, foaming temperature, foaming time |

Fig. 5 Schematic representation of single barrel extrusion microcellular foaming



These advanced technologies include ultrasound-aided microcellular foaming, bi-modal microcellular foaming, and cyclic microcellular foaming. These advanced technologies are developed either by specific process integration or process modification or variation in the process parameters & their levels to obtain the desired foam structure.

Ultrasound-aided microcellular foaming

Ultrasound-aided microcellular foaming is the advanced foaming technique in which external ultrasound vibration applied within the existing traditional batch foaming process to enhance the cell morphology of the foamed product. This technique is useful to convert the closed cell structure to an open or interconnected cell structure. The main application of this technique could be in the field of tissue engineering scaffold as it is a solvent-free technique and therefore, the new tissue generation ability of biological cells remains unaffected [28–30]. Also, it could be utilized for filters and membrane preparation [31]. The various process parameters such as ultrasound frequency, exposure time of ultrasound, the intensity of ultrasound, temperature of water in the ultrasound aided microcellular foaming technique which significantly affects the cell morphology of polymer foam. Figure 9 shows the schematic representation of for ultrasound aided microcellular foaming setup used by Gandhi et al.

Mechanism of ultrasound aided microcellular foaming

The ultrasonication creates the vibrational sinusoidal wave in an elastic medium. During the positive half of the wave, the distance between the molecules of the medium decreases and during negative half that distance increases. When the wave vibration reaches to threshold or peak, it create bubbles that are termed as cavitation bubbles. With time, the size of cavitation bubbles increased, when it reached the critical size it explodes violently and thus creating the packets of energy called microjets. These microjets start continuously striking on the polymer surface that creates the hot spot. The hot spot is confined to a localized area, experience extreme high temperature and pressure about 5000 °C and 1000 atm [31–33], which induces high thermodynamic instability.

The significant effect of ultrasonication on cell morphology depends on when ultrasonication assists with traditional foaming technique, i.e. either at the beginning of nucleation or after nucleation.

Ultrasonication applied at beginning of nucleation- The ultrasonication creates a number of cavitation bubbles which collapse violently once bubbles reach their critical sizes and thus creates hot spots. The extreme conditions of hot spots generate high thermodynamic instability which leads to the nucleation of a large number of small cells i.e. cell density gets enhanced [33].

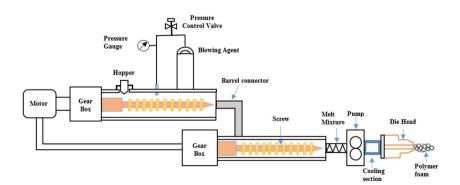
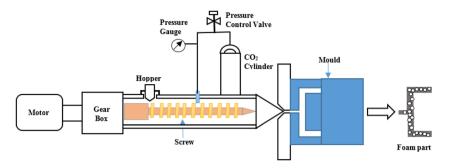


Fig. 6 Schematic representation of tandem extrusion microcellular foaming adapted from Ref [1] with kind permission from Elsevier Fig. 7 Schematic representation of injection mould microcellular foaming adapted from Ref [1] with kind permission from Elsevier



Ultrasonication applied after cell nucleation & growth - The generated microjets continuously strike on the foam surface and break the surface cell walls. Then the water along with cavitation bubbles enters into inner foam. Further, in the same manner, cell walls get rupture and the interconnected or open cell structure achieved [33]. Even if there is heat generation at hot spots, it is consized to the localized area so that the overall temperature is less, and hence the foam shape or structure is not distorted [34]. The schematic representation of the mechanism of ultrasound aided microcellular foaming is shown in Fig.10.

Wang et al. demonstrated that ultrasound irradiation (UI) enhanced the non-uniform cell structure to uniform cell structure of the semi-crystalline or crystalline polymer if UI introduces at the beginning of cell nucleation. The delay in the introduction of UI leads to non-uniformity of structure and if the exposure time of UI increases, it leads to cell uniformity and enhances the cell density [28]. The literature review on ultrasound aided microcellular foaming is given in Table 3.

Bi-modal microcellular foaming

The bi-modal structure also termed as bi-cellular or complex cellular, as it consists of both large sized cells and small ones [40, 41]. The small sized cells provide mechanical strength, thermal insulation, whereas large sized cells provide low bulk density [42]. The bi-modal structured foam has better thermal insulation compared to uni-modal structured foam. The two different nucleating mechanisms are required to develop the bi-modal cell structure [42]. Generally, the bi-modal foam structure is developed by; two-step depressurization technique [43–51], co-blowing technique [40, 42, 52–54], polymer blend technique [55–58]. Along with this, some researchers developed bi-modal structure using ultrasound excitation [33],

multiple soaking technique (MST) [59], temperature rising and depressurization [60], etc.

The schematic of two-step depressurization is shown in Fig. 11. In this technique initially, sample saturated at pressure (P_1) and temperature (T_1) for a defined time (t_1) . Then depressurized the vessel to an intermediate pressure (P_2) and hold it for some time (t_2) . Finally depressurized vessel to atmospheric pressure. This stepped depressurization causes large and small bubbles. The intermediate pressure also termed as holding pressure.

The co-blowing agent with a primary blowing agent also develops bi-modal cell structure. In this case, the different nucleating mechanism is induced by two different blowing agents. Generally, the large cell size is obtained by the coblowing agent and small cell size is obtained by a primary blowing agent which may be due to the diffusion difference of blowing agent in the polymer matrix. The polymer blending technique leads to the formation of the bi-modal structure due to the non-homogeneity of polymer blend and also due to the difference in stiffness. This leads to time inclusion in first cell nucleation and second cell nucleation.

Gandhi et al. [33] shown that bi-modal structure could be created with ultrasound excitation in which the ultrasound frequency is a significant parameter that affects the bi-modal microcellular structure of ABS foam as shown in Fig. 12. The author found that the low ultrasound frequency (25 kHz) led to uniform cell morphology and high ultrasound frequency (45 kHz) led to bi-modal cell morphology. The high ultrasound frequency generated the number of microjets. These microjets continuously hit the polymer surface and formed a number of small cells. But microjets continued to strike the surface and forming new cells around the growing cells eventually which led to bi-modal microcellular morphology.

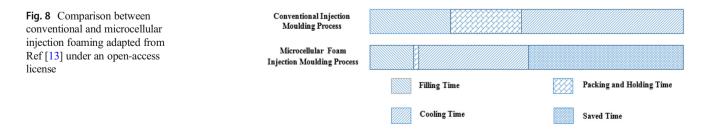


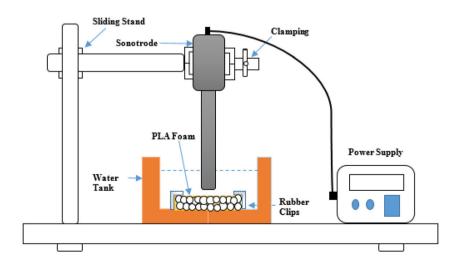
Table 2 Comparison between traditional manufacturing processes of microcellular polymers

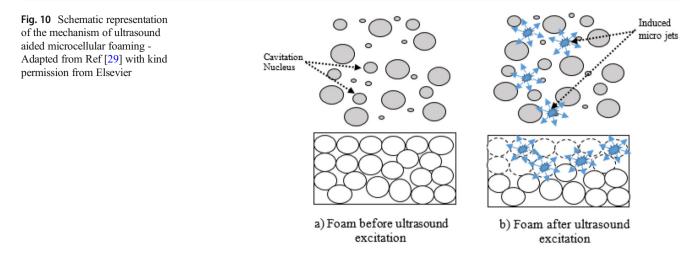
| Comparative point | Batch solid-state microcellular foaming | Extrusion microcellular foaming | Injection molding microcellular foaming |
|------------------------------------|--|--|---|
| Type of process | Non-continuous | Continuous | Semi-continues |
| Sample state | Solid | Molten | Molten |
| Raw material required (amount) | Small | Large | Medium to large |
| Sample composition | Fixed | Variable | Variable |
| Blowing agent amount | More (upto saturation of sample) | As per requirement | As per requirement |
| Gas dissolution rate | Low | High | High |
| Cause of thermodynamic instability | $\left(+\frac{\partial T}{\partial t}\right)$ or $\left(-\frac{\partial P}{\partial t}\right)$ | Only $\left(-\frac{\partial P}{\partial t}\right)$ | Only $\left(-\frac{\partial P}{\partial t}\right)$ |
| Processing time incurred | More | Moderate | Less |
| Size of sample | Small | Large | Moderate (depend on mould) |
| Skin formed | Thin | Medium Thicken | Thicker |
| Sample complexity | Simple | Simple | Both (simple & complex) |
| Variety of products | Moderate | Less | More |
| No. of temperature zones | One | More than one | More than one |
| Post-process | Final part dried | Final part calibrated and cut of the extruded foam | Final part calibrated or cut off the injected foam |
| Productivity | Low | High | High |
| Use | Lab Scale | Commercial | Commercial |
| Cost | Cheap | Expensive (depend on machine & mould standard) | Expensive(depend on machine & mould standard) |

Huang et al. [59] developed another new technique called multiple soaking temperature (MST) to generate a bi-modal structure. In this method, first sample was sealed in the autoclave chamber at room temperature and pressurized with saturation pressure of P₁. Then raised temperature to T₁ which is the first soaking temperature, kept it for time t₁. After that, decreased the temperature to second soaking temperature T₂ kept for time t₂. Again temperature increased to third soaking temperature T₃ kept for time t₃, followed by a reduction in temperature to fourth soaking temperature or foaming temperature T₄ kept for time t₄, later depressurized chamber to ambient pressure. Finally cooled autoclave chamber to room temperature and foamed sample taken out from chamber. Here, soaking temperature array as $T_1 > T_3 > T_4 > T_2$. With this method, the author successfully fabricated porous bi-modal PLA foam with open-cell structure had porosity, open-cell content, average large and small cell size are 87.9%, 82.4%, 150 µm, and 8 µm respectively.

The thermodynamic instability could be generated by sudden pressure drop or sudden temperature rise which results in the cell nucleation and in general foaming process, either one of them is enough for nucleation. But Lin-Qiong Xu et al. [60] used both thermodynamic instability aspects synergistically and successfully created the bi-modal structure in polystyrene foam.

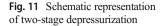
Fig. 9 Schematic of setup for ultrasound aided microcellular foaming- Adapted from Ref [29] with kind permission from Elsevier

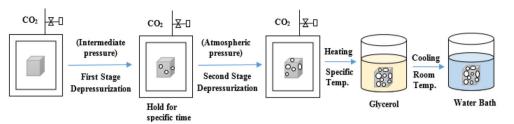




| Table 3 | Literature review | on ultrasound aided | microcellular foaming |
|---------|-------------------|---------------------|-----------------------|
|---------|-------------------|---------------------|-----------------------|

| Author | Material | Foaming process | Ultrasound treatment applied | Ultrasonic processor | Findings | Ref |
|----------------|---|---|--|---|--|------|
| Wang et al. | PLA | Batch Foaming | At very start of cell nucleation and at a time interval (0-20 s) | _ | UI enhanced cell density about 2 orders of magnitude at different foaming temperatures. | [28] |
| Guo et al. | PLA | Batch Foaming | After PLA foam Cell nucleated | Sonics VCX750, Sonics & Materials Inc., USA, 20 kHz | Cell interconnectivity & permeability enhances with an intensity of ultrasound radiation. | [29] |
| Wang et al. | PLA | Batch Foaming | After PLA foam cells nucleated | VC750, Sonics Concept Inc., 20 kHz, 750 W | Ultrasound treatment changes closed cell to interconnected cell of size 30–90 µm. | [34] |
| Youn & H. Park | PU | Reaction Injection Moulding | After the imprignment mixing of two components | Piezo-electric actuator with titanium horn, 20 kHz | Negative pressure field generated by ultrasound which enhanced the nucleation rates. | [35] |
| Zhai et al. | PS | Batch Foaming | At the start of foaming | Ultrasound Irradiation | UI enhanced cell density about 100–1000 times & expansion ratio about 2–4 times | [36] |
| Wei Li et al. | РММА | Selective Ultrasonic Foaming Process | At starting of PMMA foam cell nucleation | HIFU Transducer (H101 Sonic Concept Inc), 1.1 MHz, 200 W | Effect of scanning speed and ultrasound power on cell size were studied and cell size enhanced with the decrease in the scanning speed. | [30] |
| Wang et al. | PLA | Solid-State Foaming | After PLA foam cells nucleated | VC750 (20 kHz) & VC540 (40 kHz) Sonics & Materials, Inc) 750 W | Ultrasound effectiveness affected by pore size. Higher permeability achieved at a bigger pore size. | [31] |
| Byon & Youn | PS with ZnS and blend of PE wax & LDPE | Ultrasonic foaming | At the start of cell nucleation | Sonicor Model UP-400 | Ultrasonic excitation enhanced nucleation with the generation of negative pressure. | [37] |
| Gandhi et al. | ABS | Batch foaming | At very starting of ABS foam cell nucleation | Martin-Walter push-pull transducer 25 and 45 kHz | Bi-modal cell structure at higher and uniform cell structure at lower sonication frequency was obtained. | [33] |
| Gandhi et al. | ABS | Cyclic Batch foaming | After ABS foam cells nucleated (second cycle) | Takashi Ultrasonics, 750 W 20 kHz | Ultra-low density porous ABS foam fabricated with the application of ultra-sound excitation. | [38] |
| Gandhi et al. | ABS | Batch foaming | Before the cell nucleation | Martin-Walter, Crest Ultrasonics MW1000GPI2 25 kHz, 1 kW | Distance of ultrasound transducer to sonication sample affects the cell nucleation. | [39] |





Radhakrishna et al. used a step-wise depressurization technique (Four-step), and each depressurization step induced different nucleation phenomenon led in the development of bimodal and multi-modal ABS foam microstructure [61].

The literature review on bi-modal microcellular foaming by two-step depressurization, co-blowing agent, polymer blend technique is given in Tables 4, 5, and 6 respectively.

Cyclic microcellular foaming

The cyclic foaming is repetitive foaming. In the cyclic foaming first, a neat polymer sample converts into a foamed sample then again foamed sample processed under the required levels of foaming parameters. From literature, it has seen that for cyclic microcellular foaming generally batch foaming process was used as; easy to control processing parameters and repeatability [65]. In the cyclic foaming process, saturation pressure is a crucial parameter; consider primary saturation pressure as P_1 and secondary saturation pressure as P_2 . Also, the sequence of P_1 and P_2 plays a significant role in controlling cell morphology [65, 66]. Gandhi et al. developed a novel technique by applying the ultrasound assistance to cyclic foaming to produce ultralow density foam with interconnected cell structure as shown in Fig. 13. Table 7 shows the literature review on cyclic microcellular foaming.

Manufacturing technologies of advanced microcellular polymers

The microcellular polymers have enhanced properties owing to its micron-sized cell structure and therefore the application range gets widened compared to macron-sized cell structure. The advanced applications of the microcellular polymer such as EMI shielding, microcellular auxetic foam for sports & safety equipment, scaffolds for controlled drug released, wooden foam composites for high strength applications. The manufacturing technologies of advanced microcellular polymers, its properties and applications are discussed in detail.

Electromagnetic interference shielding microcellular polymers

The radiation generated by electronic devices interferes with each other causing the disruption in the functionality of devices is known as Electromagnetic Interference (EMI) [69, 70]. The ringing cellphone near the television causes the fluctuations in video or audio quality of television is one of the examples of EMI. EMI may lead to the adverse effect on the functioning of the important electronic systems/devices in the field of aerospace, defence, intelligence department, significant scientific research and also on human health due to prolonged radiation exposure [69-71]. The term EMI Shielding is referred to as the protection against the interruption of electromagnetic waves. The conductive material possesses good EMI shielding capability thus generally, the metal-based materials are used as EMI shield material but their weight to shielding effect ratio is more. Therefore nowadays, polymer-based conductive materials replaced them owing to their less weight, corrosion resistance, ease of processing, flexibility, and cost [69, 70, 72].

There are two kinds of conductive polymers; intrinsic conductive polymers (ICP) which have good electrical conductivity and extrinsic conductive polymers (ECP) in which electrical conductivity has to generate i.e. by conductive coating or conductive filler addition. There is a large range of conductive fillers are available categorized as; carbon-based and metalbased. Carbon-based fillers comprise as; CNT, CNF, CB, graphene, GR, GO, GNRs, GNPs, etc. And metals based metal nanowires, metal granules metal nanoflakes, etc. [69, 70].

The various structures were reported to enhance the absorption of electromagnetic waves as, segregated structure,

Fig. 12 Schematic representation of the formation of bi-modal ABS foam structure using ultrasound excitation

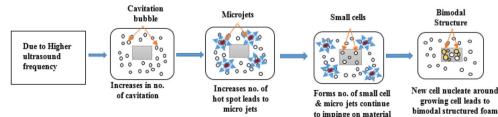


 Table 4
 Literature review on bi-modal microcellular foaming (Two-step depressurization)

| Author | Material | Process Parameter | Findings | Ref |
|-----------------|----------------------------------|--|--|------|
| Bao et al. | PS | $P_1 = 20$ MPa, $T_1 = 100$ °C, $t_1 = 4$ h, $P_2 = 15$ MPa, $t_2 = 0,10,30,45,60$ min | Degree of depressurization and holding time significantly controlled density of large cells and small cells. | [43] |
| Bao et al. | PS | $P_1 = 20$ MPa, $T_1 = 100$ °C, $t_1 = 4$ h, $P_2 = 12,13,15,17$ MPa, $t_2 = 0,10,30,45,60$ min | Tensile and impact strength of bi-modal foam varies with volume fraction of large cell. | [44] |
| Z. Ma et al. | PC | $P_1 = 20$ MPa, $T_1 = 60$ °C, $t_1 = 6$ h, $P_2 = 14$ MPa, $t_2 = 1$ h, $T_2 = 60$ °C | Tensile strength & modulus improved by 28% & 32% respt. For foam having bi-modal structure compared to uni-modal structure due to blunting effect. | [45] |
| Z. Ma et al. | PC | $P_1 = 20$ MPa, $T_1 = 60$ °C, $t_1 = 6$ h, $P_2 = 14$ MPa, $t_2 = 1$ h, $T_2 = 60$ °C | Dielectric properties of the bi-modal structure were similar to a uni-modal structure as it depends on the porosity of foam. | [46] |
| P. Yu et al. | PLA/PBS blends | $P_1 = 20$ MPa, $T_1 = 150$ °C, $t_1 = 1$ h, $P_2 = 16$ MPa, $t_2 = 10$ min, $T_2 = 90,100,110$ °C | PLA/PBS blend in 80/20 ratio at 100 °C has highest cell opening rate of 96% | [47] |
| Wang et al. | PS/PETG blend | $P_1 = 20$ MPa, $t_1 = 4$ h, $P_2 = 17.5$ MPa | Bi-modal structure has a large-cell of diameter is 300 μm or more and small-cell of diameter is 100 μm or less. | [48] |
| C. Li et al. | PS | $P_1 = 16$ MPa, $T_1 = 100$ °C, $t_1 = 2$ h, $P_2 = 12$ MPa, $T_2 = 100$ °C | Density of larger cell & small cell governs by first degree of depressurization & second degree of depressurization respect. | [49] |
| Chen et al. | PCL | $P_1 = 20$ MPa, $T_1 = 40$ °C, $t_1 = 2$ h, $P_2 = 12,10,8,7,6,5$ MPa, $t_2 = 1$ h | Bi-modal porous scaffolds fabricated with a large cell size of 100 µm and smaller with 50 µm. | [50] |
| Arora et al. | PS | $P_1 = 6000 \text{ psi}, T_1 = 100 \text{ °C, hr.}, P_2 = 4000 \text{ psi}, t_2 = 1 \text{ h}$ | Bi-modal foam with an average cell size of the large cells and small cells about 21 µm and 4.8 µm fabricated. | [51] |
| Bernardo et al. | PMMA, PMMA/ MAM, PMMA/ SEP | $P_{1PMMA} = 31 \text{ MPa},$ $P_{1PMMA/MAM} = 10 \text{ MPa},$ $P_{1PMMA/SEP} = 10 \text{ MPa},$ $T_1 = 25 \text{ °C}, t_1 = 24 \text{ h},$ $P_{drPMMA} = 100 \text{ MPa/s},$ $P_{drPMMA/MAM} = 15 \text{ MPa/s},$ $P_{drPMMA/SEP} = 15 \text{ MPa/s},$ $t_2 = 1 \text{ to } 1.5 \text{ min}$ | Proposed a model to predict thermal conductivity with consideration of bi-modal structure which provide more accurate estimation than model with mono-modal structure. | [62] |
| Gandhi et al. | ABS | $P_1 = 5, 4, 3$ MPa, $T_1 = R.T$, $t_1 = 24$ h, $P_2 = 3, 2, 1.5, 1$ MPa, $T_2 = 100, 110, 120, 130, 140$ °C | In bi-modal structure, size of primary bubbles and secondary bubbles influence by initial saturation pressure and holding time & holding pressure respect. | [63] |

multilayer structure, sandwich structure and foam structure [71]. The density of polymer composite is less than metal composite but due to the addition of conductive filler, the density and the viscosity of polymer composite may increase. The researchers strive to further reduce the density of polymer composites by developing a porous structure in the polymer matrix [69, 71]. The reflection, absorption, multiple-reflection, and transmission are the mechanisms that play a significant role in locking the electromagnetic waves in the shielding material [69]. EMI shielding effectiveness (EMI SE) is a measure of the shielding material's performance, which is the sum of losses associated with all the above

mechanisms and given in terms of decibel (dB) [69, 70, 72, 73]. In this study, this section is focussed on EMI shielding of the foam structure. The multiple-reflection mechanism occurs in foamed EMI shielding material because the foamed EMI shielding material has a large interface area and surface area so multiple-reflection possible [69].

Yang et al. [74] integrated hot pressure compression moulding and salt leaching process to develop PS/CNT foamed composite having a density of 0.45 and 0.27 g/cc.

Ling et al. [75] used the water vapour induced phase separation (WVIPS) process shown in Fig. 14 to produce microcellular nanocomposite foams for enhancement of EMI

| Author | Material | Blowing agent | Foaming process | Findings | Ref |
|---------------------|----------|---|-------------------|--|------|
| Lee et al. | PS | Primary- n-butane Co- Water Nucleating agent- Silica particles | Extrusion foaming | Bi-modal structure can be tuned with the variation in co-blowing agent content. With an increase in water content enhanced the expansion ratio. | [40] |
| Zhang et al. | PS | Primary- CO ₂ , Co- Water Additives- GR, AC, CNF | Extrusion foaming | Foaming of PS with 0.5% GR & 0.5% AC with 0.5% water produced bi-modal Structure | [52] |
| Zhang et al. | PS | Primary- CO ₂ Co- Water Additives- GR, AC, Nano Clay 30B | Extrusion foaming | Addition of particulates reduced the difference in foaming time. In PS/GR and PS/AC/GR both show bi-modal structure, in that PS/GR has small cells than PS/AC/GR. | [42] |
| Nistor et al. | PS | Primary- CO ₂ nC5 & cC5 | Batch foaming | Organic agents were used to enhanced foam porosity | [53] |
| Daigneult & Gendron | PS | Blend of CO ₂ & 2-EH | Extrusion foaming | At 8.6 wt% of CO_2 & 1.6 wt% of 2- EH bi-modal cell size distribution was observed with a large cell size of about 250 μ m and a small-cell size of about 25 μ m. | [54] |
| Dugad et al. | ABS | Primary- CO ₂ Co- Water | Batch foaming | Cell size enhanced with introduction of water which enhanced the expansion ratio | [64] |

 Table 5
 Literature review on bi-modal microcellular foaming (Co-blowing agent)

Shielding. Figure 15 depicts microwave transfer across nanocomposite foam that enables composite foam as an excellent microwave absorber. Table 8 represents the literature review on EMI shielding microcellular polymers.

Auxetic foamed polymers

The auxetic polymers are processed materials having negative Poisson's ratio (NPR) by the virtue of which it explores the exceptional properties [89–92]. The material with NPR indicates, the material expands laterally when stretched linearly and vice versa [93–95]. The first polymer auxetic foam was synthesized by Lakes R. in 1987, had Poisson's ratio of -0.7 and Young's Modulus of 72 kPa from open-celled PS foam [89]. The auxetic foam has superior properties over

conventional as; resilience, synclastic, indentation resistance, shear resistance, etc. which leads to the wide range applications in the field of aerospace, military, sports, biomedical, etc. [89, 90, 92, 96–99].

Generally, the thermo-mechanical technique is used for the transformation of conventional polymer foam to auxetic polymer foam. The thermo-mechanical technique is comprised of three steps; first is volumetric compression of conventional foam using a mould of which shape is to be achieved. In this step, the buckling of cell ribs or struts occurs which leads to a re-entrant cell structure. Then second is a heating step, in which compressed foam along with mould heated in a furnace at a temperature above the softening temperature to maintain the buckled cell structure for a defined time. Finally in third step, mould takes out from the furnace, cooled it to room temperature and

 Table 6
 Literature review on bi-modal microcellular foaming (Polymer blend technique)

| Author | Blend Composition | Foaming Process | Process Condition | Findings | Ref |
|------------------|--------------------------|--------------------------|--|---|---------------------|
| Kohlhoff et al. | PMMA & PS | Batch foaming | $P_1 = 8$ MPa, $T_1 = 60$ °C, $t_1 = 4$ h, $T_2 = 100$ °C P2 = 8 MPa, $t_2 = 4$ h | Bi-modal cell structure with diameter range for small cells 10–30 μm and for large cell 200–400 μm were observed in blend ratio of 50:50, 33:67, 15:85 | [57] |
| Lei Jiang et al. | PP/LDPE | Batch foaming | $P_1 = 25$ MPa, $T_f = 100$ °C, 90 °C, & 140 °C, 150 °C R _{dp} = 400 MPa/s | Bi-modal structure generated in pure PP, 90:10 & 75:25 PP: LDPE Blend foam. | [55] |
| Tang et al. | PP and PP/PLA & talc | Batch foaming | $T_f = 82 \text{ °C to } 99 \text{ °C.}$ | Bi-modal structure was observed at a low temperature of 93 °C & 94.5 °C in PP foam. And in PP/PLA blend foam at 90 °C. | [<mark>56</mark>] |
| Wang et al. | PP/ PS blend and clay | Tandem extrusion foaming | First barrel pressure = 7 bar & second barrel pressure = 10.5–18 bar | Bi-modal structure was observed in PP/PS blend in the ratio of 80/20, 70/30, 60/40. Large cell Density increases with an increase in PS concentration. | [58] |



c

A- Neat Sample, B- Primary Foam Sample, C-Secondary Foam

Secondary Foaming

в

X

Primary Foaming

remove the foam from it. Sometimes cell ribs stick to each other which may affect the functionality of final foam (auxetic) thus stretch the foamed sample in the opposite direction of compression [89, 100-103]. It is recommended to lubricate inside the mould or use of wire or tweezers or redesign the mould to avoid the surface wrinkling or surface creasing [97].

A

To eliminate the high temperature processing, Garima et al. [104] developed a novel chemo-mechanical technique. In this technique, the first compression step was similar to as in thermo-mechanical technique. Then compressed foam sample wrapped in filter paper and placed in the organic solvent (acetone) for a defined time. Finally taken out the sample and dried it in the air. The formed foam was auxetic in nature. Also, the researchers successfully re-convert auxetic foamed structure to the original foamed structure using the same organic solvent through the re-expansion of the auxetic foamed sample in the solvent.

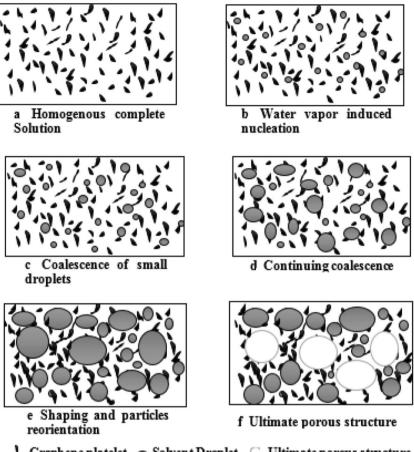
The simple geometry auxetic foams are easy to manufacture than complex and curved geometry auxetic foams using above mentioned conventional techniques. As the solution for this, Binachi et al. [105] developed a new method called half mould manufacturing process. In this method, the author used an open curved mould instead of a closed mould. The conventional foamed sample placed in mould on which layer of non-porous fluorinated ethylene propylene (FEP) film and over that the medium weighs polyester nonwoven breather blanket placed such a that it covers foamed sample with mould. The assembly closed in the flexible membrane and sealed it properly then using a vacuum pump reduced internal pressure to 0.7 Bar. Due to vacuum, cell ribs get bucked and re-entrant structure was formed. To preserve the cell structure, all assembly was kept in a furnace of temperature 200 °C by maintaining inside vacuum. After a definite heating time of half-hour, assembly was taken out and immersed in water. Once the temperature reached to room temperature foamed sample outstretched orthogonally to relive cell sticking. The resultant foam was in auxetic nature.

Ultrasound excitation applied to secondary foam

The transformation of closed cell conventional foam to auxetic foam is difficult than open cell conventional foam to auxetic foam which may be due to isolated cell or thick cell walls. Fan et al. [106] proposed a new technique using water steam called steam penetration and condensation (SPC). In this technique, the foamed sample of defined shaped placed in water steam environment which maintains at a specific temperature for a defined time. Due to steam, all cells contracted inside leads to cell bucking, re-entrant structure.

| Table 7 Literature review on cyclic microcellular foaming | Author | Material | Foaming process | Findings | Ref. |
|---|---------------------|----------|-----------------|--|---------------------|
| | Gandhi et. al | ABS | Batch foaming | Developed 0.02 g/cc low density foam with the cell size enhancement using cyclic foaming. | [38] |
| | Seo et al. | PC | Batch foaming | If $P_1 > P_2$ then cell density increased & if $P_2 > P_1$ cell size enhanced. | [<mark>66</mark>] |
| | Cho et al. | PC | Batch foaming | P ₁ significantly affects cell morphology than P ₂ . Also, the sequence of processing affects both cell morphology and foaming ratio. | [65] |
| | Nawaby &. Handa | PMMA | Batch foaming | The foam density of secondary foam significantly reduced up to 6 days aging after that plateau occurs. Also the density of secondary foam with N ₂ nearly the same to primary foam. | [67] |
| | Radhakrishna et. al | PMMA | Batch foaming | Cell buckling phenomenon was observed which resulted in star-like microstructure and low-density PMMA foam developed using cyclic foaming. | [68] |

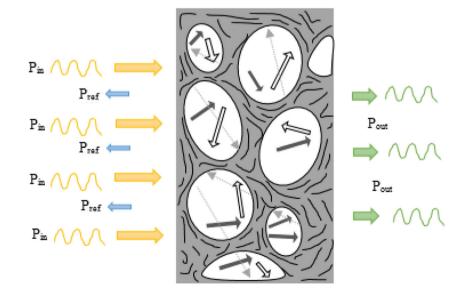
Fig. 14 Schematic representation of WVIPS process to prepare nanocomposite foam- adapted from Ref [75] with kind permission from American Chemical Society



🕴 Graphene platelet 💿 Solvent Droplet 🛛 Ultimate porous structure

Then the sample was taken out and cooled to room temperature. The foam structure resulting from this technique has NPR i.e. showing uniform auxetic nature due to the pressure difference. In order to enhance the mechanical performance of auxetic foam compared to the performance of auxetic foam produced from the thermo-mechanical technique, the new technique was developed by Quadrini et al.

Fig. 15 Schematic representation of the microwave transfer across nanocomposite foam- adapted from Ref [75] with kind permission from American Chemical Society



| | | , - , - | | | | |
|-----------------|--------------------------|---------------|---|---|---|------|
| Author | Filler | Material | Composite preparation technique | Foaming process | Finding | Ref |
| Thomassin et al | MWCNT | PMMA | Precipitation polymerization Melt-blending, Co-precipitation | Batch-foaming | Compared to neat polymer sample foamed sample absorbed more than 90% of incoming nower | [76] |
| X-B Xu et al. | CNT | PU | Static casting | Polymerization between nolvol and isocvanate | Lightest PU/CNT composite with 0.05 ø/cc fahricated. | [77] |
| Wang et al. | Graphite | PLA | Twin Screw extruder | Mould opening foam injection molding | PLA/graphene nanocomposite foam exhibits EMI SE upto 45 dB (i.e 99% radiation blocked) | [78] |
| Yang et al. | MWCNT | Sd | Surfactant with ultrasonication | 1 | Foam composite with 7% CNT generated EMI SE about 20 dB | [79] |
| L Xu et al. | CNT | HDPE | Solution mixing & mechanical pulverization | Compression molding plus salt-leaching | Specific EMI SE of CNT/HDPE foam composite about 2.2 times of solid composite | [74] |
| D-X Yan et al. | FGS | PS | Solution mixing & mechanical pulverization | Compression molding plus salt-leaching | Porous, low-density FGS/PS composite foam exhibited EMI SE of 29 dB. | [80] |
| Zhang et al. | GS | PMMA | Solution Blending & melt compounding | Batch foaming | PMMA/ graphene composite foam with 1.8 vol% graphene shows an EMI SE of 13–19 dB | [81] |
| Shen et al. | G@Fe3O4 Hybrid | PEI | Solution Blending | SdIVW | Composite foam showed EMI SE of ~14.3–18.2 dB at a frequency range of 8–12 GHz | [82] |
| Shen et al. | GO | PU Sponge | 1 | Dip coating | PU/Graphene foam fabricated with a density range of 0.027-0.03 ø/cc | [83] |
| Ling et al. | GNC | PEI | Solution Blending | SdIAM | Microcellular PEl/graphene foams at 7 & 10 wt% exhibits EMI SE of 36.1 & 44.1 dB/ (g/cm3) respect. | [75] |
| Zeng et al. | MWCNT | WPU | 1 | Freeze drying | Porous, anistropic MWCNT/WPU foam exhibits SE above 20 dB | [84] |
| Ameli et al. | CF | ЬР | Ι | Injection molding machine MuCell technology | PP/CF composite density reduced by 25% & EMI SE increased to 65% | [85] |
| Bernal et al | MWCNT, f- MWCNT & FGS | Dd | Ultrasound-assisted the dispersion of (polyol & filler) | Open cylinder moluding | FGS/PU composite exhibited EMI SE of 15.15 dB cc/g. And for MWCNT & FMWCNT it showed nearly the same | [86] |
| Ameli et al. | SSF | ЬР | I | Injection molding machine MuCell technology | PP/SSF composites showed EMI SE of 75 dB·g – 1 at 1.1 vol% SSF | [87] |
| Yu Xu et al. | MWCNT | Melamine foam | Solution blending and then ground in cone mill | Electroless silver plating | Epoxy composite with multiple conductive showed SE of 88 dB. | [88] |

[107] called solid-state foaming for auxetic foam. In this method, first the epoxy resin powder tablets of re-entrant hexagonal shape were prepared by cold compaction. Here the number of small tablets were arranged in an ordered manner with defined space between them because the large size tablet leads to poor foaming. After that foaming of tablets was done using the oven at 320 °C for 8 min in the presence of air. Then the foamed samples were taken out and cooled in the air which showed auxetic behaviour.

For the manufacturing of large auxetic foam blocks, Chan et al. [108] proposed a multi-stage thermo-mechanical technique in which volumetric compression and heating occurred in stages. The advantage of this multistage method is that the surface ceasing is eliminated. Table 9 shows the literature review on auxetic foamed polymer.

Porous microcellular polymers

The large surface area, interconnected cell structure, small and uniform cell size increased demand of the porous microcellular polymer preferably for tissue engineering scaffolds, separation membranes, cushioning, etc. The scaffolds used for the transformation of nutrients, the excretion of cell wastes, cell interaction, tissue formation which required porous structure [109, 110]. The various techniques used for the fabrication of porous structure for scaffold as; solvent casting/ particulate leaching, thermally induced phase separation, freeze-drying, etc. [110, 111]. These are conventional solvent-based techniques which may affect the ability of the biological cell to generate new cells [31], less pore-interconnectivity, uneven pore distribution, less porosity, etc. [109]. These problems are resolved by the gas foaming technique as it is a solvent-free technique [109, 110, 112].

 Table 9
 Literature review on Auxetic foamed polymers

| Author | Material | Foaming process | Findings | Ref. |
|-----------------|--|--|--|-------|
| Lakes | Low-density PS-Open cell polymer foam | Thermo-mechanical | Successfully synthesized man-made auxetic foam with poison's ratio of -0.7 with properties like synclastic, high shear modulus. | [89] |
| Fan et al. | PE –Closed Cell foam | SPC | Auxetic foam with SPC successfully prepared and conclude that pressure difference due to steam condensation main reason for conversion of auxetic structure. | [106] |
| Grima et al. | PU foam – Open cell (30 pores per inch) foam | Chemo-mechanical | Auxetic foam with poison's ratio ranges from -0.32 to -0.36 obtained with new technique compare to thermo-mechanical technique it is more. | [104] |
| Bianchi et al. | PU foam – Open cell foam | Vacuum based assembly system | With novel technique curved auxetic foam with poison's ratio of $-1.26 \& -0.96$ in yx and xy direction respectively at 5% tensile strain manufactured. | [105] |
| Bianchi et al. | PU-PE - Open cell foam | Thermo-mechanical | It reported that the foam density depends on the time delay to remove from the mould. More time delay leads to higher density. | [100] |
| Chan & Evans | Polyether urethane- open cell foam | Multi stage-thermo-mechanical | Poison's ratio can be controlled by the volumetric compression. The heating time, temperature and compression load required more for large sample compared with the small one. | [108] |
| Quadrini et al. | Commercial Epoxy Resin- powder | Solid-State foaming | New solid-state foaming without any additives directly results in foam with auxetic structure. | [107] |
| Wang & Lakes | PU- open cell foam | Thermo-mechanical | The study suggests that with auxetic effect reduces with a decrease in cell size. As poison's ratio of -0.8 , -0.5 , -0.4 for cell size of 20, 65,100 ppi respectively obtained at optimal heating temperature and time. | [101] |
| Yao et al. | PU foam as matrix & shape memory epoxy resin as functional phase | Thermo-mechanical | The auxetic effects enhance with the rise in the volume compression ratio. At a compression ratio of 0.79 maximum Poisson ratio (-0.43 ± 0.05) obtained. | [102] |
| Alderson et al. | PU- open cell foam | Thermo-mechanical Uniaxial compression within a specially designed rig | For the curved foams and flat sheets, Poisson's ratio values reported as -3 and -0.3 . | [103] |

Presently, advanced techniques such as electrospinning and 3D printing or rapid prototyping are using to achieve better specific structure properties with ease of processing at economical cost. Electrospinning is used to fabricate a porous scaffold using fibers, it's a simple and cost-effective fiber production technique. In this technique, the high voltage supply applied to polymer droplet held at tip of needle, which charges the droplet & formed repulsive force. The charged jet of polymer solution erupts and reaches to a collector, solvent evaporates and jet solidified into thin fibers [111, 113–115]. Another technique called, 3D printing or rapid prototyping technique is used to fabricate complex scaffold structures precisely from biodegradable materials [110, 116–121]. Also, some researchers modified or integrated two or more techniques to achieve the advance structure [122–126]. This section focused on porous microcellular plastics using a gas foaming technique.

To fabricate the porous or open interconnected structure, the ultrasound assistance was also used by various researchers such as Gandhi et al. [38], Wang et al. [31], H Wang et al. [34], X Wang et al. [36] for different applications. Table 10 contains the literature review on porous microcellular plastic.

Wood fiber reinforced microcellular polymer composites

Wood fillers or flour as reinforcement in polymer matrix led to the new branch of composites termed as wood fiber reinforced polymer composite (WFRP). At present, WFRP composites are the most demandable composites in different fields like construction for interior decoration & furniture, automotive for decking, window, and door lineals, railing, auto parts, etc. due to its mechanical properties [135-139]. The WFRP composites are generally manufactured by injection moulding, extrusion and compression moulding [135, 137]. The reason behind the huge demand of WFRP composite is, readily available wood filler at low cost, has specific strength and biodegradability [135–137]. The various wood fillers, with different aspect ratio are available in the form of fiber or flour [137]. There are some constraints for the utilization of wood fibers such as; thermal degradation, fiber breakage, and moisture content which limits the selection of processing parameters [135, 137, 140]. The WFRP composites possess good strength and stiffness so it could be utilized for static applications but also has low impact strength, brittleness, and high bulk density which limits its utilization in dynamic applications [140-143]. Therefore to advance its utilization in dynamic applications, the mechanical properties have to be enhanced (impact strength & ductility has to enhance with a reduction in bulk density), which could be achieved by the creation of microcellular structure in composites [136, 141, 144, 145].

The microcellular structure could be generated in wood composites by foaming processes such as; batch foaming, injection mould foaming, extrusion foaming, compound Moulding [136, 141, 145]. Some advancement is still going on to develop a new process or modify the existing ones as; co-extrusion, foaming during extrusion, and inline coating technologies, etc. [138]. The advantages of foamed wood composite over the unfoamed wood composite are low processing temperature, high production speed which in turn reduced manufacturing cost also better surface smoothness, sharp counters, and corners, etc. [136, 144, 146].

The process of WFRP composite foaming is similar to the general foaming process comprised of three stages; gas dissolution & saturation, cell nucleation, and cell growth & stabilization. In wood-composite foaming, blowing agent is not dissolved in wood fillers thus only polymer matrix gets plasticized. Subsequently, due to the generation of thermodynamic instability, cell nucleation occurs. In this case, both types of nucleation occur; homogenous as well as heterogeneous. The homogenous nucleation due to the gas diffusion from the composite whereas heterogeneous nucleation due to the entrapped gas at micro-voids near polymer-filler interfaces. The percentage of heterogeneous nucleation is more than the homogenous nucleation because of the more filler content, the number of interfaces available and restricted the gas dissolution to the polymer matrix. The continue cell growth may lead to cell coalescence and cell collapse, [136, 141]. To avoid this, the cells are stabilized using a cooling medium.

A wide variety of additives are used to form wood composites such as coupling agents to improve the dispersion of fillers, chemical surfactants to enhance the bonding or adhesion between filler and polymer matrix, flame retardants to enhance resistance to the outbreak of fire, etc. [139–141, 144, 145, 147–150].

Some researchers fabricated wood composites from the wastes; PS foam as polymer matrix and agricultural waste as a wood filler. Koay et al. [151] prepared novel wood composite from recycled PS foam and durian husk fiber. In this, first PS foam sample was dissolved in acetone to remove air from it. Later it was dried at 70 °C using oven followed by filtration; subsequently recycled PS was cut into small samples for further process. For wood fiber, durian husks were collected, cleaned and cut into small pieces then dried it in an oven at the same 70 °C and prepared short fiber with the grinder. The fibers dried again to avoid high moisture content. Subsequently, WPC compound formed using torque rheomix and moulded into sheets using hot press. Similarly, Tawfik et al. [152] formed a wood composite with recycled PS and rice straw. The tensile strength, water absorption, and acoustic resistance test were performed. The tensile strength decreased with an increase in rice straw content above 30%. Chun et al. [153] used agricultural waste to formed wood composite with PS foam. The tensile, thermal and morphological evaluation

 Table 10
 Literature review on Porous microcellular polymers

| Author | Material | Process | Findings | Ref |
|----------------------|---|---|--|-------|
| Mancuso et al. | AW & two silicate-based novel glasses | Binder jetting 3D printing and sintering | Structure with the accuracy of ± 0.25 mm created | [119] |
| Seleznev et al. | • | Combination of 2D nano imprint & 3D printing (SLA) | Polymer bone scaffold fabricated with a hybrid technique | [118] |
| Mohanty et al. | PVA | Combined 3D printing and salt leaching | Double pore scaffold with uniform cell distribution, high cell density fabricated with a combined technique | [117] |
| Jakus et al. | Graphene & PLGA | 3D printing | Graphene-based scaffold fabricated with filaments of diameter ranges from 100 to 1000 µm | [120] |
| Zein et al. | PCL | Fused deposition modelling (FDM) | PCL scaffold with the porosity of 48–77%, range of yield strength 0.4–3.6 MPa & strain yield 4% -28% | [121] |
| Huang et al. | PLA | Electrospinning | Electrospin fibers with 100 nm sized pores fabricated using chloroform solvent as a volatile solvent | [113] |
| Qin et al. | 5 wt% PLA dissolved in DMF/ CH ₂ Cl ₂ | Electrospinning | Durable, uniform, flexible white-light-emitting fi- brous membrane fabricated with coaxial electrospinning | [114] |
| T Xu et al. | PCL, cellulose acetate | Electrospinning | Interconnect structure scaffold with the porosity about 95% & pore size from submicron to 100 μm fabricated | [115] |
| Jaganathan et al. | PU, Corn oil, Neem oil, DMF | Electrospinning | Addition of corn oil & corn/neem oil reduced fiber diameter from 890 ± 116.911 nm to 845 ± 117.86 nm & 735 ± 126.49 nm respt. | [127] |
| Thakare et al. | PCL, ZrO ₂ | Electrospinning | Scaffold with ZrO ₂ enhanced the cell adhesion and proliferation. | [128] |
| Wang et al. | PCL, CBA- SB, PBA- CO ₂ | Chemical injection mould foaming combined with particulate leaching | Scaffolds with porosities of 68.2%, 73.8%, and 70.9% for different samples; A, B, and C respect. Fabricated | [122] |
| Kramschuster et al. | PLA, PVOH, Particulate- NaCl, PBA- CO ₂ | Physical injection molding combined with particulate leaching | Interconnected pores structure about 200 μ m in diameter and porosities of about 75% fabricated. | [120] |
| Huang et al. | PCL, PEO, PBA- N ₂ | Combined injection mould foaming and polymer leaching | Blend of PCL/PEO (50%/50%) enhanced porosity to 89.5% & compression modulus decrease to 46.7 MPa from 68.2 MPa | [124] |
| Matuana et al. | PLA, PBA- CO ₂ , NA- Montmorillonite clay, quater- nary bis (2-hydroxy ethyl) am- monium salt | Continuous-extrusion foaming | Higher porosity obtained by high gas flow rate and high-pressure drop | [129] |
| Gomes et al. | Starch, PBA- CO ₂ | Extrusion foaming, compression moulding & particle leaching, and solvent casting & particle leaching | Higher porosity about 60–70% reported with solvent casting & particle leaching | [130] |
| Jing et al. | PCL & CSNF | Combined extrusion foaming, water-soluble phase leaching, and freeze-drying. | Compressive modulus & water uptake capacity of scaffold enhance by 35% with utilization CSNF | [125] |
| Gandhi et al. | LDPE, CBA- N ₂ | Extrusion foaming process by rapid surface quenching technique | High blowing agent content induced open cell structure and at lower chill roll speed & temperature open cell with interconnected structure was observed | [126] |
| Sierraa et al. | PCL, PBA- CO ₂ , THF, & EtOAc | ScCO ₂ foaming | Membrane with the larger pore of 300–500 µm surrounded by smaller pore of 15–50 µm prepared | [131] |
| Cue'noud et al. | Blend of PLLA, PLDLA, PEG flakes | Batch foaming | Open-cell structure with cell dia. 200 µm –700 µm & porosity more than 75% generated | [132] |
| Floren et al | PDLLA | Batch foaming | Mechanical anisotropy and performance of foamed specimen depends on processing parameters | [133] |
| Singh et al. | PLGA | Batch foaming | Interconnected structure with 89% porosity and pore size ranges from 30 to 100 µm generated | [134] |

| Table 11 Literature revie | Literature review on wood fibre reinforced microcellular | orced microcellular polymer composite | ite | | | |
|---------------------------|--|--|--|-------------------------------|--|-------|
| Author | Material | Filler and additives | Mixture process | Foaming process | Finding | Ref |
| Rachtanapun et al. | Blend of HDPE/PP | Wood fiber | Twin-screw extruder | Batch foaming | Gas solubility and void fraction decrease due to high filler crystallinity and increased etitinese | [154] |
| Fatih M. et al | PVC | Wood flour, and CBA- azodicarbon- amide & SB | High-intensity Mixer | Extrusion foaming | CBA contract sumess. CBA contra and type has no effect on the density reduction of the foamed commosite | [155] |
| Zhang et al. | dd | Wood fiber, Flame retardants- APP & silica | Twin-screw extruder | Batch foaming | Smaller cell size and high relative density in case of silica and in APP density first decreases and then increases with enhanced cell size | [139] |
| Zhang et al. | PP | Wood Flour, CA- MAPP CBA-Foamazol R71 Antioxidant & stabilizer- Irganox B215 | Twin-screw extruder | Extrusion foaming | Composite form with average cell size less than 100 µm obtained and coupling agent enhance bonding between PP & wood flour. | [140] |
| Bledzki et al. | ЪР | Hardwood fiber, CA- MAPP, CBA- Hydrocerol 530, Hydrocerol AB40E, Hydrocerol BIH20 | High-speed mixer | Injection moulding | Nearly 70% of surface roughness decreases using an endothermic foaming agent and physico-mechanical properties enhanced up to 80%. | [144] |
| Zhang et al. | dd | Wood Fiber, compatibilizers- SEBS-g-MA, PP-g-MA, Silica (aerogel 150) | Twin-screw extruder | Batch-foaming | Cell Density increases and cell size decreases with silica content due to heterogeneous nucleation | [150] |
| Q Li et al. | HDPE | Wood flour, CBA - SB, Celogen-OT, Celogen-AZNP & EX210, CA- MA-g-HDPE | High-intensity mixer | Extrusion foaming | Void fraction depends on CBA content than CBA type. (1% for neat HDPE and 0.5% for HDPE/wood-flour composites | [142] |
| B Xie et al. | Recycled PP | Wood Fiber, CBA- azodicarbonamide, CA- MAPP | Single-screw extruder | Injection molding | Density reduction by 24.5% and impact strength enhancement by 53% of the composite. | [145] |
| Lee et al. | HDPE | Wood Fiber, CA- MA-g-HDPE, Nano clay- Cloisite 20A (intercalated and exfoliated) | Masterbatch and direct melt blending | Extrusion foaming | At low wood fiber content 1% clay significantly affects cell morphology. | [143] |
| Choe et al. | PU | Chemically treated wood fiber, CS- NaOH & y-aminopropyltriethoxysilane | Stirred Mixer | One-shot polymerization | Chemical treatment enhanced the open porosity which increases sound absorption | [147] |
| Feng et al. | PVC | Wood Fiber CS- NaOH & 3-triethxysilyl- 1-propanamine (KH-550) | Tank-ball mill mixed | One-step compression moulding | Compared to both chemical surfactants NaOH treated gave the best result. The tensile strength more for small particle-sized wood fiber composite. | [148] |
| Yeh et al. | ЬР | Rice husk, CA- SEBS-g-MA & PP-g-MA, CS- NaOH, silane, NaOH + HCI + silane | Brabender plasticorder (PLE-331) internal mixer | Batch foaming | Fiber surface treatment and coupling agent significantly enhance the cell morphology and reduce the density. | [149] |
| Khoshnoud & Abu-Zahra | PVC | Mica, glass fiber, and fly ash | High shear mixer | Extrusion foaming | The glass fiber composite has better flexural and impact strength than mica and fly ash composite. | [156] |

was done to analyze the performance of composites. Table 11 represents the literature review on wood fiber reinforced microcellular polymer composite.

Conclusions and future direction

- The manufacturing of customized polymer foam with controlled cell morphology using general microcellular foaming is quite difficult. Therefore, the integration of advancement to traditional methods has been made more convenient and effective.
- The advancement in the microcellular foaming process such as ultrasonication has been found to be much effective in enhancing both nucleation rate as well as interconnected open-cell structure. It depends on the time of application of the ultrasonication (i.e. at the beginning of nucleation or after nucleation)
- The microcellular polymer composites exhibit a better EMI Shielding effect than neat polymer composites with a reduction in weight density too.
- Carbon-based fillers are the most suitable fillers to enhance the electrical conductivity of polymer foam in EMI shielding applications due to their wide range of properties.
- In wood fiber reinforced polymer foaming, the cell nucleates by homogenous nucleation as well as heterogeneous nucleation. Homogenous nucleation occurs due to gas diffusion from polymer matrix whereas, heterogeneous nucleation takes place at polymer-filler interface due to entrapped gas at micro-voids.
- The buckling of cells governs the auxetic behaviour and the performance of auxetic foam polymer is independent of the cell size of the foam structure.
- The bi-modal cell structure provides superior properties compared to the uni-modal cell structure. Moreover, the tri-modal cell structure may add more value to properties governed by the bi-modal structure. Hence, there is scope to further develop the polymeric foam with tri-modal or multi-modal cell structure.
- Few literatures are available on the cyclic foam manufacturing process which builds up research focus to explore more and more on the cyclic foaming technique to manufacture ultralow density foam with desired properties.

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Abbreviations CBA, Chemical blowing agent; PBA, Physical blowing agent; CA, Coupling agent; NA, Nucleating agent; CS, Chemical surfactants; CO2, Carbon dioxide; ScCO2-, Supercritical CO2; N2, Nitrogen; ABS, Acrylonitrile-Butadiene-Styrene; PS, Polystyrene; PE, Polyethylene; PC, Polycarbonate; PP, Polypropylene; PMMA, Polymethyl methacrylate; LDPE, Low-Density Polyethylene; HDPE, High-Density Polyethylene; PVOH, Polyvinyl alcohol; PEG, Polyethylene glycol; PLA, Poly (lactic acid); PLLA, Poly-L-lactide; PLDLA, Poly-L-lactide-co-D, L-lactide; PDLLA, Poly (D, L lactic acid); PVC, Poly (vinyl chloride); PLGA, Polylactide-co-glycolide; PVOH, Polyvinyl alcohol; PEO, Poly (ethylene oxide); PBS, Poly (butylenes succinate); PETG, Poly (ethylene terephthalate glycol); PCL, Poly (Ecaprolactone); PVA, Polyvinyl alcohol; PVDF, Polyvinylidene fluoride; PEI, Polyethyleneimine; PANI, Polyaniline; MAM, Poly (methyl methacrylate)-poly (butyl acrylate)-poly (methyl methacrylate); PU, Polyurethane; WPU, Water-borne polyurethane; ZnS, Zinc stearate; SEP, Sepiolites,; nC5, Co-n-pentane; cC5, Cyclopentane; 2-EH, 2-ethyl hexanol; AW, Apatite-wollastonite; DMF, Dimethylformamide; CSNF, Chitosan nanofibers; THF, Tetrahydrofurane; EtOAc, Ethylacetate; SEBS-g-MA, Maleic anhydride- grafted styrene-ethylene-butylene-styrene; PP-g-MA, Maleic anhydride-grafted polypropylene; APP, Ammonium polyphosphate; MAPP, Maleated PP; SB, Sodium bicarbonate; NaCl, Sodium chloride; HCL, Hydrochloric Acid; NaOH, Sodium Hydroxide; CB, Carbon black; AC, Activated carbon; CNT, Carbon nanotubes; CNF, Carbon nanofibers; GR, Graphite; GO, Graphene oxide; GNC, Graphene Nano composite; GNRs, Graphene nanoribbons; GNPs, Graphene nanoplatelets; GS, Graphene sheets; FGS, Functionalized graphene sheets; MWCNT, Multi-wall carbon nanotube; f-MWCNT, Functionalized MWCNT; SSF, Stainless-steel fiber; ZrO₂, Zirconia

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