

# Optimized synthesis of hydroxypropyl cellulose-*g*-poly( $\epsilon$ -caprolactone) network

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**Abstract** The objective of this study was the synthesis of copolymer networks based on poly ( $\epsilon$ -caprolactone) (PCL), hydroxypropyl cellulose (HPC) and hexamethylene diisocyanate (HDI) via bulk graft copolymerization followed by crosslinking (using routes I and II), and subsequent optimization of the process by response surface methodology (RSM). The studied reaction parameters were: (i) monomer content (weight ratio of CL/HPC), (ii) amount of catalyst, and (iii) amount of crosslinker. FT-IR and <sup>1</sup>H NMR results confirmed that the grafting of PCL onto HPC and subsequent crosslinking through terminal hydroxyl groups of PCL grafts by HDI were performed successfully. Through differential scanning calorimetry (DSC) and X-ray diffraction analysis (XRD), it was found that the crystallinity of grafted polymers depended on the amount of grafted PCL and degree of crosslinking. In modeling of the process using RSM, the coefficient of determination ( $R^2$ ) for the models (97.3 and 93.3 % for two routes) as well as the probability ( $p < 0.0001$ ) revealed high significance of the regression models. Also it was found that the obtained systems possessed  $T_m$ s between 42.94 and 54.57 °C (route I) and 32.49–46.30 °C (route II) that were tunable by the monomer content, catalyst and crosslinker amounts. RSM provided a useful tool to select in a fast way the proper experimental conditions to synthesize

crosslinked HPC-*g*-PCL copolymer as a novel biocompatible and biodegradable shape memory polymer with adjustable switching temperature and potential biomedical applications, which would be further studied in the future.

**Keywords** Poly ( $\epsilon$ -caprolactone) · Hydroxypropyl cellulose · Graft copolymer · Optimization · Response surface methodology

## Introduction

Recently, chemical modification of biodegradable polymers has become an important method to generate valuable materials with improved properties and expand their applications especially in biomedical fields. Poly ( $\epsilon$ -caprolactone) (PCL) as a semicrystalline biodegradable polymer, is one of the most important polymer with relatively low melting temperature and good mechanical properties. For biomedical applications, the biodegradability nature of the polymers and adjustment of their  $T_m$  around the human body temperature (37–39 °C) are the essential key factors and a challenging field for researchers [1, 2]. From this aspect, PCL is a good choice as a biocompatible and biodegradable polymer with a sharp  $T_m$  around 60 °C which could be adjusted ranging from 19 to 62 °C by modifying the PCL chain length [3, 4].

Typically, polymerization of  $\epsilon$ -caprolactone (CL) is started by ring-opening polymerization (ROP) method. To date, in several investigations on the modification of PCL melting point, it has been observed that by introducing the hydroxyl rich initiators as backbone, available hydroxyl groups are much enough to short the PCL chain length and modulate its  $T_m$ . Therefore, a branched architecture was used in PCL system, and relatively short PCL segments were employed as another means of lowering  $T_m$  [5]. Liang and co-workers [6]

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reported three-arm polymers as thermally induced biodegradable polymers based on glycerol and PCL. The star shape design was critical in achieving a  $T_m$  near biologically relevant temperatures. Nagahama et al. [7] developed novel biodegradable consisting of star shape branched oligo( $\epsilon$ -caprolactone). Recently, Bai and co-workers [8] demonstrated that introducing of ethyl cellulose as backbone to polymer network can modulate the  $T_m$  and mechanical strength of PCL materials.

In this study, we report on the synthesis and characterization of hydroxypropyl cellulose (HPC) and CL graft copolymers (HPC-*g*-PCL) with well-defined structure, controlled molecular weight, and desired thermal properties, which were prepared via “grafting from” method using opening polymerization (ROP). HPC is one of the most important nontoxic, biodegradable, and biocompatible cellulose derivatives which is extensively used in producing the smart materials, in biomedicine [9–12]. Structurally, HPC has three hydroxyl groups per each monomeric unit. Therefore, it was selected as initiator due to the adequate number of hydroxyl groups and its bioactive feature [13]. HPC is essential to lowering the crystallinity so that a reduced  $T_m$  could be observed for HPC-*g*-PCL copolymer. The hexamethylene diisocyanate (HDI) was applied to prepare crosslinked HPC-*g*-PCL (X(HPC-*g*-PCL)) as a biocompatible and biodegradable polymer at body temperature.

Most optimization studies during the development of a novel polymeric system involve variation of one factor at a time, keeping all other factors constant. This traditional optimization method is time-consuming and expensive. Today, a statistical-based technique of response surface methodology (RSM) is used extensively to elucidate the interaction between reaction parameters for optimization. RSM is a technique where by reaction parameters are varied simultaneously in a suitable manner to generate data for development of empirical models. It is a faster and more economical analytical approach than the traditional ones. RSM has been commonly used for designing and optimization of different polymeric systems prepared via ROP, such as grafted PCL to cellulose nanocrystals [14], copolymers of polylactide and polyglycolide (PLGA) as tissue scaffold and drug release device [15], and copolyester involving  $\delta$ -gluconolactone as a new bio-based product [16]. However, there is not any published information about the optimization of graft polymerization of CL in the presence of HPC and crosslinking reaction of the obtained copolymer.

The current study aims to model and optimize the synthesis of X(HPC-*g*-PCL) and predicting the  $T_m$  in various operating conditions using RSM approach. RSM was used to investigate the effect of reaction parameters (variables) including the monomer content (weight ratio of CL/HPC), catalyst concentration and crosslinker amount on the  $T_m$  of X(HPC-*g*-PCL). Therefore, the novelty of the present study is the use of the RSM approach for optimization of the resultant copolymer X(HPC-*g*-PCL) in order to get the best option for its use as a new bio-based SMP. Further, we will investigate the shape

memory behaviors of the X(HPC-*g*-PCL) films with appropriate  $T_m$  in continue.

## Experimental

### Materials

Hydroxypropyl cellulose (HPC) was purchased from Aldrich (Milwaukee, WI, USA;  $M_n=100,000 \text{ gmol}^{-1}$  according to the manufacturer) and dried under vacuum at room temperature for 24 h before use. The molar substitution of propoxy groups ( $MS_{\text{HPC}}$ ) was approximated 1.25 using  $^1\text{H}$  NMR spectrum of HPC [17].  $\epsilon$ -Caprolactone (CL) was purchased from Merck (Germany) and dried over freshly powdered  $\text{CaH}_2$  for 24 h and then purified by twice distillation under reduced pressure [13]. Tin (II) bis (2-ethylhexanoate) ( $\text{Sn}(\text{Oct})_2$ , 96 %) was purchased from Alfa Aker. Hexamethylene diisocyanate (HDI) was purchased from Fluka and was used without further purification. *N,N'*-Dimethylformamid (DMF) was dried with 4 Å molecular sieves and distilled under reduced pressure before use. Chloroform ( $\text{CHCl}_3$ ) and *n*-hexane were used without further purification.

### Synthesis

#### *Synthesis of HPC-g-PCL graft copolymers*

A series of HPC-*g*-PCL graft copolymers having different chain lengths of graft PCL were prepared by ROP of CL in bulk condition. The recipes for preparing the series of HPC-*g*-PCL (with 85–93 wt.% of CL) are summarized in Table 1. All the polymers were prepared in a similar manner. Therefore, HPC and CL at appropriate weight ratio were charged into a dry flask, mixed thoroughly, and left at room temperature for 12 h until HPC was completely swelled by CL. The mixture was placed in an oil bath at 130 °C under argon atmosphere, then a certain amount of  $\text{Sn}(\text{Oct})_2$  (Table 1) was dissolved in dry toluene (250  $\mu\text{L}$ ) and added immediately into the mixture and was stirred for 24 h at the same temperature. For removing PCL homopolymer as the main by-product during the reaction, it was cooled to room temperature; the resulting polymer was dissolved in THF at a concentration of 5 % (*w/v*) and then precipitated in equal volume of cold *n*-hexane. The purification procedure was repeated three times and the pure resultant polymer was dried in vacuum at room temperature to a constant mass.

#### *Preparation of X(HPC-g-PCL) films*

The films of X(HPC-*g*-PCL) were prepared using two different routes.

In route (I), HPC-*g*-PCL (0.1 g) was dissolved in 4 mL of anhydrous DMF by vigorous stirring until a homogenous solution was obtained. Then enough amount of HDI (Table 2)

**Table 1** DSC results for HPC-g-PCL copolymers

HPC-g-PCL	CL:HPC:Sn(Oct) <sub>2</sub> (wt/wt/wt)	T <sub>m</sub> (°C)	T <sub>c</sub> (°C)	X <sub>c</sub> <sup>(a)</sup> (%)	ΔH <sub>m</sub> (J/g)
HPC-g-PCL-85 (A)	100:17.65:1.47	47.72	11.24	18.21	-24.58
HPC-g-PCL-87 (B)	100:14.90:0.76	48.08	11.12	27.18	-36.70
HPC-g-PCL-87 (C)	100:14.90:2.11	51.90	16.13	25.94	-35.02
HPC-g-PCL-90 (D)	100:11.11:0.28	56.15	24.24	30.32	-34.40
HPC-g-PCL-90 (E)	100:11.11:1.39	50.67	15.50	33.04	-44.61
HPC-g-PCL-90 (F)	100:11.11:2.50	51.22	11.27	29.99	-40.49
HPC-g-PCL-93 (G)	100:7.56:0.699	52.34	22.55	32.87	-44.37
HPC-g-PCL-93 (H)	100:7.56:1.98	54.70	23.34	32.47	-43.83
HPC-g-PCL-93 (I)	100:5.26:1.32	56.07	25.15	32.98	-44.52

<sup>(a)</sup> X<sub>c</sub> =  $\frac{\Delta H_m}{\Delta H_{100\%}} \times 100$ , where the melting enthalpy for 100 % crystallized PCL was considered 135 J/g [8]

was added and before pouring into a Teflon dish, was stirred at 80 °C under argon for about 2 h. After casting the solution, to complete the reaction, the mixture was cured and dried in an oven at 80 °C for 24 h.

In route (II), after dissolving the same amount of HPC-g-PCL in 5 mL of anhydrous CHCl<sub>3</sub>, enough amount of HDI (Table 2) was added to the stirred solution. The mixture was poured into a Teflon dish and left at room temperature for 12 h. For more drying and curing, the casted film was heated in an oven at 80 °C for about 24 h.

**Determination of molar substitution (MS<sub>CL</sub>)**

Molar substitution of CL (MS<sub>CL</sub>) in HPC-g-PCL molecules, which is the average number of CL molecules reacted with each anhydroglucose unit, was determined with a gravimetric method [13]. The calculation is given as follows:

$$MS_{CL} = [(W_{graft} - W_{HPC})/114]/(W_{HPC}/234)$$

where W<sub>graft</sub> is the weight of HPC-g-PCL after purification, W<sub>HPC</sub> is the initial weight of HPC, 114 is the molecular weight of a repeating unit of PCL, and 234 is the average molecular weight of a repeating unit of HPC. In this calculation, HPC was assumed to be 100 % converted to HPC-g-PCL Fig. 1.

**Determination of side-chain length and distribution**

Various graft lengths of HPC-g-PCL copolymers were obtained by adjusting the molar ratios of CL monomer to HPC. The average length of the PCL side chains (L) on each HPC repeating unit could be estimated from end-group analysis by <sup>1</sup>H NMR spectroscopy. The intensity of the a and e protons at 2.3 and 4.6 ppm, respectively (see Fig. 2) was used for this purpose. The calculation is given as follows:

$$L = I_{Ha}/(I_{Ha} - I_{He})$$

where I<sub>He</sub> is the peak intensity of the e protons that are not at the chain end and I<sub>Ha</sub> is the peak intensity of the e and e' protons (peaks overlapped).

The average number of PCL chains on each HPC repeating unit (N) was then calculated by

$$N = MS_{CL}/L$$

**RSM experimental design and model development for optimized synthesis of HPC-g-PCL**

In synthesis process, some parameters such as CL/HPC weight ratio, and catalyst and crosslinker amounts affect the T<sub>m</sub>. The influence of operational parameters in the conventional methods has been investigated by systematically varying a parameter and keeping constant the others. This should be repeated for all the influencing parameters, resulting in a large number of experiments. To model the process, using the experimental design methodologies such as RSM can be useful.

The design procedure for RSM is as follows [18]: (i) Performing a series of experiments for adequate and reliable measurement of the response of interest; (ii) developing a mathematical model of the second-order response surface with the best fit; (iii) determining the optimal set of experimental parameters that produce a maximum or minimum value of response; (iv) representing the direct and interactive effects of process parameters through two and three-dimensional (3D) plots. Using RSM, it is possible to estimate linear, interaction and quadratic effects of the factors and a prediction model for the response. In this way, RSM designs could be used to find improved process settings in an efficient use of resources.

In this paper, modeling of the synthesis process was studied using central composite design (CCD) under RSM. In CCD, the response surface is modeled by fitting a second-order polynomial with the number of experiments equal to 2<sup>f</sup>+2f+n<sub>c</sub>, where f and n<sub>c</sub> are the number

**Table 2** DSC results for X(HPC-g-PCL) copolymers

Route I						Route II					
X(HPC-g-PCL)	HDI %W/W	$T_m$ (°C)	$T_c$ (°C)	$X_c$ (%)	$\Delta H_m$ (J/g)	X(HPC-g-PCL)	HDI %w/w	$T_m$ (°C)	$T_c$ (°C)	$X_c$ (%)	$\Delta H_m$ (J/g)
A'	25.0	42.94	6.72	15.05	-20.32	A''	15.0	32.88	-	-	-
B <sub>1</sub> '	16.1	46.58	15.28	20.25	-27.34	B <sub>1</sub> ''	9.10	37.67	-	0.52	-0.70
B <sub>2</sub> '	33.9	44.60	7.58	16.53	-22.34	B <sub>2</sub> ''	21.9	32.49	-	-	-
C <sub>1</sub> '	16.1	48.11	15.24	17.34	-23.41	C <sub>1</sub> ''	9.10	41.63	2.37	15.69	-21.18
C <sub>2</sub> '	33.9	46.62	15.05	12.87	-17.37	C <sub>2</sub> ''	21.9	38.82	-	0.34	-0.46
D'	25.0	48.26	16.74	14.38	-19.41	D''	15.0	35.76	-	-	-
E <sub>1</sub> '	40.0	47.79	21.23	22.29	-30.09	E <sub>1</sub> ''	25.0	36.32	-	0.79	-1.07
E <sub>2</sub> '	25.0	49.73	18.44	22.75	-30.71	E <sub>2</sub> ''	15.0	38.91	0.69	2.05	-2.77
E <sub>3</sub> '	25.0	48.93	17.35	21.58	-29.13	E <sub>3</sub> ''	15.0	40.11	2.07	2.84	-2.78
E <sub>4</sub> '	25.0	48.11	17.56	21.06	-28.43	E''	15.0	38.02	-	1.55	-2.09
E <sub>5</sub> '	25.0	50.00	19.01	23.72	-32.02	E <sub>5</sub> ''	15.0	39.35	1.18	2.93	-3.95
E <sub>6</sub> '	25.0	49.05	17.69	21.88	-29.54	E <sub>6</sub> ''	15.0	37.47	-	-	-
E <sub>7</sub> '	25.0	49.34	18.04	22.23	-30.01	E''	15.0	38.55	0.35	1.83	-2.47
E <sub>8</sub> '	10.0	50.04	19.32	26.48	-35.64	E <sub>8</sub> ''	5.00	46.30	15.41	26.34	-35.56
F'	25.0	49.23	15.77	23.15	-35.64	F''	15.0	44.29	8.55	8.65	-11.68
G <sub>1</sub> '	16.1	52.74	23.13	24.41	-31.25	G <sub>1</sub> ''	9.10	40.53	0.55	13.90	-18.77
G <sub>2</sub> '	33.9	53.22	20.31	26.91	-32.95	G <sub>2</sub> ''	21.9	33.32	-	0.11	-0.15
H <sub>1</sub> '	16.1	53.22	22.63	24.98	-36.33	H <sub>1</sub> ''	9.10	43.80	12.71	18.26	-24.85
H <sub>2</sub> '	33.9	50.80	15.09	19.57	-33.73	H <sub>2</sub> ''	21.9	37.64	-	3.09	-4.18
I'	25.0	54.57	25.63	24.78	-26.42	I''	15.0	40.03	3.74	16.71	-22.56

of design factors and center runs, respectively. The CCD consists of three distinct portions: (1st)  $2^f$  fractional points where the factor levels are coded to the usual low and high values (-1, +1); (2nd)  $2f$  axial points or "star" points on the axis of each variable at a distance  $\alpha$  from the designed center where  $\alpha=(2^f)^{1/4}$ ; and (3rd)  $n_c$  center points that can be replicated to provide an estimate of experimental error variance. Therefore, each independent variable was varied at five levels (denoted as coded values  $-\alpha$ ,  $-1$ ,  $0$ ,  $+1$ ,  $+\alpha$ ) [19]. In this study,  $\alpha$  value was fixed at 1.68. The variables studied were HPC/CL ratio ( $X_1$ ), amount of catalyst ( $X_2$ ), and amount of crosslinker ( $X_3$ ). Thus, for synthesis process having three independent parameters, the total number of experiments required was calculated as Eq. (1):

$$N = 2^f + 2f + n_c = 2^3 + (2 \times 3) + 6 = 20 \quad (1)$$

Minitab software was used for both the design and statistical analysis of the experimental data. An analysis of variance (ANOVA) was used to estimate the statistical parameters. The experimental design runs generated by software is shown in Table 3. The setup consist of 20 runs in random order allows modeling of all parameter effects on response.

In Table 3, process factors and their investigated levels are given in coded and actual values. The relationship between the

coded (x) and actual (X) values of the variables is according to Eq. (2):

$$\text{coded value} = \frac{\text{actule value} - \frac{(\text{high value} + \text{low value})}{2}}{\frac{(\text{high value} - \text{low value})}{2}} \quad (2)$$

The outcome of each experimental run is analyzed and the response is correlated with three input factors through an empirical second degree polynomial equation as given by the Eq. (3) [20]:

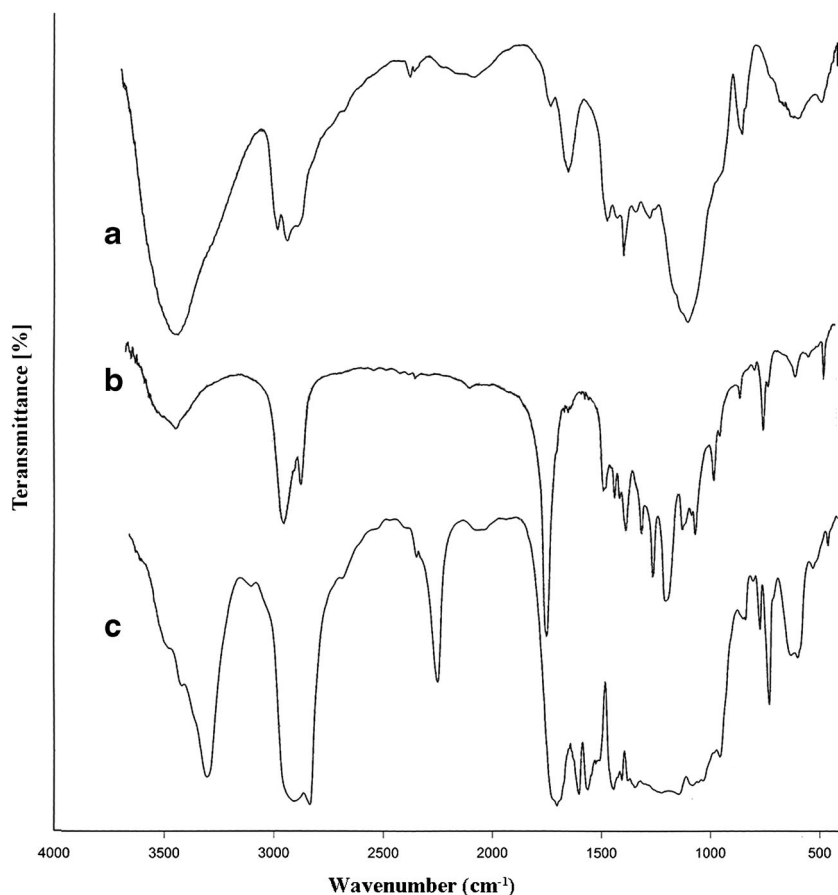
$$Y = b_0 + \sum_{i=1}^n b_i x_i + \sum_{i=1}^n b_{ii} x_i^2 + \sum_{i=1}^n \sum_{j=1}^{n-1} b_{ij} x_i x_j \quad (3)$$

where,  $Y$  is the predicted response ( $T_m$ , °C),  $b_0$  the constant coefficient,  $b_i$  the linear coefficients,  $b_{ij}$  the interaction coefficients and  $b_{ii}$  the quadratic coefficients of the factors.

## Instrumental

FT-IR spectra were recorded on a Bruker PS-15 spectrometer (Bruker Optics, Ettlingen, Germany) at wave numbers ranging from 400 to 4000  $\text{cm}^{-1}$ .  $^1\text{H}$  NMR spectra were taken on a 400 MHz Bruker SP-400 Avance spectrometer (Bruker Biospin, Rheinstetten, Germany) using chloroform as solvent

**Fig. 1** FT-IR spectra of **a** HPC, **b** HPC-g-PCL, and **c** X(HPC-g-PCL)



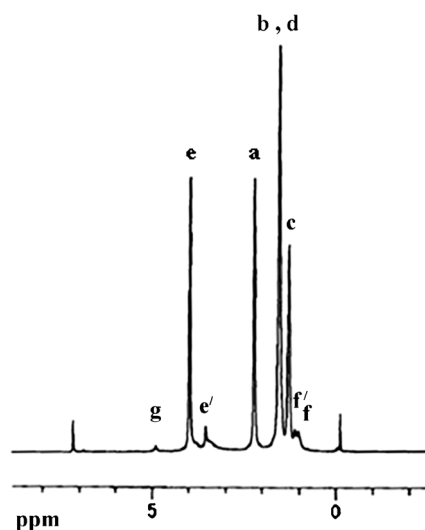
with tetramethylsilane as the internal standard. A Mettler-Toledo model 822 differential scanning calorimeter (Columbus, OH, USA) was used to determine phase transition temperatures at heating and cooling rates of 10 °C/min. The instrument was calibrated with indium regarding temperature and enthalpy. Enthalpy change ( $\Delta H_m$ ), melting temperature ( $T_m$ ) and crystallinity ( $X_c$ ) were obtained from the second

heating curves. The crystalline structure of the products were analyzed using X-ray diffraction (XRD) patterns by a Bruker AXS model D8 advanced diffractometer for Cu K $\alpha$  radiation ( $\lambda=1.54187 \text{ \AA}$ ) at 40 kV and 35 mA with Bragg angle ranging from 3 to 70°.

## Results and discussion

### Synthesis and structural analysis of HPC and PCL based copolymers

The synthetic routes for the HPC-g-PCL and its crosslinked copolymers are shown in Schemes 1. In this study, the graft copolymerization of CL was initiated by a hydroxyl-group-rich HPC in the presence of Sn(Oct)<sub>2</sub> catalyst in a bulk condition. ROP method was chosen since it is well-known for CL to form either a homopolymer or copolymers [13]. Therefore, a series of HPC-g-PCL copolymer with different CL/HPC ratios and catalyst amounts were prepared and named as HPC-g-PCL-N (N is related to the weight percent of CL in HPC-g-PCL synthesis). Then the corresponding X(HPC-g-PCL) were obtained by crosslinking with different amounts of HDI through two different routes (route I and route II). We



**Fig. 2** <sup>1</sup>H NMR spectrum of HPC-g-PCL

**Table 3** Experimental design matrix and response matrix for route I and route II

Run	Coded value			Actual value						T <sub>m</sub> <sup>*</sup> (°C)	
	x <sub>1</sub>	x <sub>2</sub>	x <sub>3</sub>	Route I			Route II			Route I	Route II
				X <sub>1</sub>	X <sub>2</sub>	X <sub>3</sub>	X <sub>1</sub>	X <sub>2</sub>	X <sub>3</sub>		
1	0.00	0.00	0.00	90.00	1.25	25.00	90.00	1.25	15.00	49.73	38.91
2	0.00	0.00	+1.68	90.00	1.25	40.00	90.00	1.25	25.00	47.79	36.32
3	0.00	0.00	0.00	90.00	1.25	25.00	90.00	1.25	15.00	48.94	40.11
4	-1.00	-1.00	-1.00	87.03	0.66	16.08	87.03	0.66	9.05	45.58	37.67
5	0.00	0.00	-1.68	90.00	1.25	10.00	90.00	1.25	5.00	50.04	46.30
6	0.00	0.00	0.00	90.00	1.25	25.00	90.00	1.25	15.00	48.11	38.02
7	+1.00	+1.00	-1.00	92.97	1.84	16.08	92.97	1.84	9.05	53.22	43.80
8	-1.00	+1.00	-1.00	87.03	1.84	16.08	87.03	1.84	9.05	48.11	41.63
9	-1.00	+1.00	+1.00	87.03	1.84	33.92	87.03	1.84	20.95	46.62	38.32
10	-1.00	-1.00	+1.00	87.03	0.66	33.92	87.03	0.66	20.95	44.60	32.49
11	+1.68	0.00	0.00	95.00	1.25	25.00	95.00	1.25	15.00	54.57	40.03
12	0.00	0.00	0.00	90.00	1.25	25.00	90.00	1.25	15.00	50.00	39.35
13	0.00	0.00	0.00	90.00	1.25	25.00	90.00	1.25	15.00	49.05	37.47
14	0.00	0.00	0.00	90.00	1.25	25.00	90.00	1.25	15.00	49.34	38.55
15	+1.00	+1.00	+1.00	92.97	1.84	33.92	92.97	1.84	20.95	50.80	37.64
16	0.00	+1.68	0.00	90.00	2.25	25.00	90.00	2.25	15.00	49.23	44.29
17	+1.00	-1.00	+1.00	92.97	0.66	33.92	92.97	0.66	20.95	53.22	33.32
18	0.00	-1.68	0.00	90.00	0.25	25.00	90.00	0.25	15.00	48.26	35.76
19	-1.68	0.00	0.00	85.00	1.25	25.00	85.00	1.25	15.00	42.94	32.88
20	+1.00	-1.00	-1.00	92.97	0.66	16.08	92.97	0.66	9.05	52.74	40.53

\* Each run was repeated 3 times and the average value was taken to ensure the results

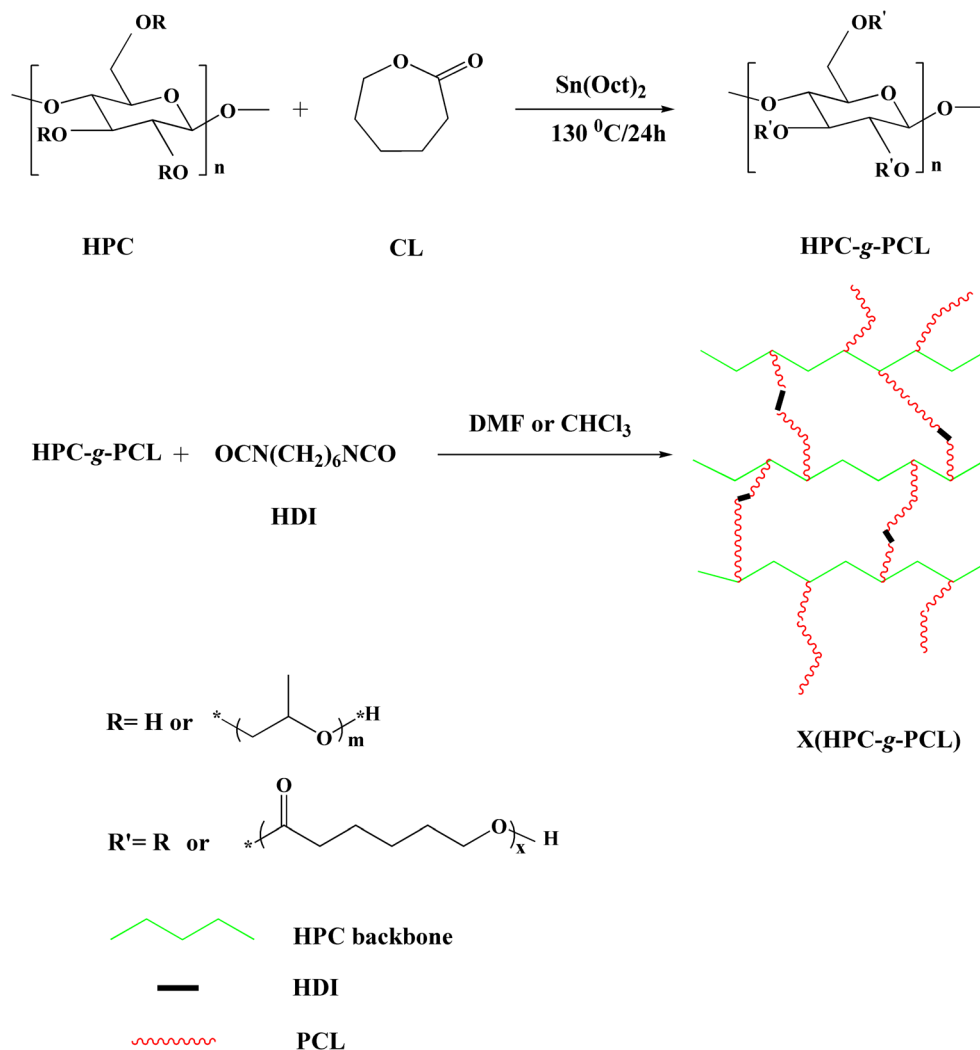
first attempted to synthesize X(HPC-g-PCL) by reacting terminal hydroxyl functional groups of PCL grafts with HDI in DMF at 80 °C for 2 h, as shown in Scheme 1, route I. However, the mild condition for the synthetic approach (Scheme 1, route II) was the second route to crosslink the HPC-g-PCL with the same crosslinker in the chloroform at room temperature for 12 h.

The structures of HPC-g-PCL and the crosslinked product were characterized with FT-IR and <sup>1</sup>H NMR spectroscopies. The FT-IR spectra of HPC, HPC-g-PCL and X(HPC-g-PCL) are depicted in Fig. 1. As shown in HPC-g-PCL spectrum (Fig. 1b), in comparison with the HPC spectrum (Fig. 1a), a new peak appearing at 1732 cm<sup>-1</sup> can be attributed to the C=O stretching of the PCL segment in HPC-g-PCL [21]. In Fig. 1c, a clear evidence for cross-linking the copolymer resulted from the stronger and wider absorption peak of C=O in cross-linked film in comparison with HPC-g-PCL due to the presence of carbamate and ester peaks. The spectrum of crosslinked HPC-g-PCL shows a new sharp absorption band at 3329 cm<sup>-1</sup>, which was ascribed to the N-H stretching vibration of the urethane bonds [7, 8]. Another variation associated with the crosslinks in the copolymer is an enhancement in the intensity of C-H stretching resonances from the

methylene groups which resonate at 2926 and 2854 cm<sup>-1</sup> (Fig. 1c). These results confirmed that the grafting of PCL onto HPC and subsequent crosslinking through terminal hydroxyl groups of PCL grafts by HDI was performed successfully [22, 23].

The <sup>1</sup>H NMR spectra of HPC-g-PCL are displayed in Fig. 2. The spectra were recorded in CDCl<sub>3</sub> at 25 °C. The signals at 2.12 and 1.21 ppm (f, f') arise through the splitting of the signal due to methyl protons in the hydroxypropyl groups by the ester groups formed during the graft reaction. It is apparent that besides the dominant HPC signals, there is new very small peak (g) at 5.0 ppm in HPC-g-PCL spectrum which was assigned to the methine protons in the hydroxypropyl groups bonded directly to the PCL chains [13]. Due to the low content of HPC in the copolymers, the HPC signals were not observed in spectrum.

On the basis of the gravimetric method and assignment and integration of the <sup>1</sup>H NMR spectrum of HPC-g-PCL, the average number of CL molecules reacted with each anhydroglucose unit (MS<sub>CL</sub>), the average length of the PCL side chains (L) and the number of the side chains on each HPC repeating unit (N) could be estimated (see Experimental section). The results of MS<sub>CL</sub> for copolymers HPC-g-PCL-85

**Scheme 1** Synthetic route of HPC-g-PCL and X(HPC-g-PCL)

and HPC-g-PCL-95 (with lowest and highest amount of CL/HPC) are 4.8 and 26.6, respectively. The errors were considered from  $\text{MS}_{\text{CL}}$  estimation with the  $^1\text{H}$  NMR spectroscopy method as reported earlier [13]. The  $L$  and  $N$  values for synthesized HPC-g-PCL copolymers varied from 20.2 to 24.0 and 0.2 to 1.1, respectively, with increasing of CL content (85 to 95 %). Hence, on average, for HPC-g-PCL-85 and HPC-g-PCL-95, there were 2 and 11 PCL side chains attached to 10 HPC repeating units with length of 20 and 24, respectively.

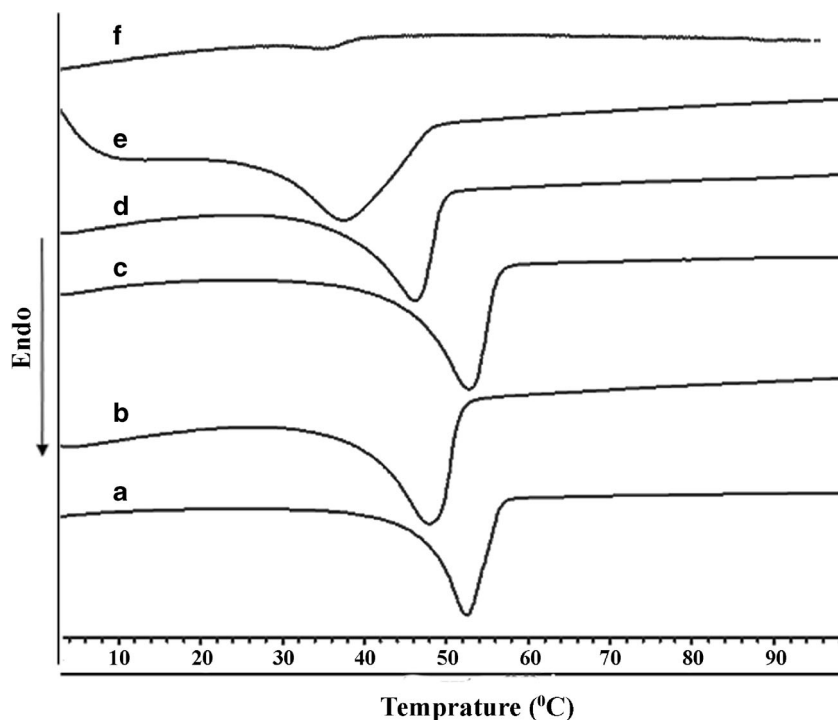
### Thermal analysis

The thermal properties of HPC-g-PCL and X(HPC-g-PCL) copolymers were characterized using DSC. The curves from the second heating run are shown in Fig. 3. Their main thermal characteristic are summarized on Tables 1 and 2, in terms of melting and crystallization temperature,  $T_m$  and  $T_c$ , respectively, as well as melting enthalpy,  $\Delta H_m$ . HPC is an amorphous polymer without any sharp melting peak. However, as shown in Table 1, HPC-g-PCL, depending on the CL/HPC ratio (85–

93 %) exhibits a sharp melting peak ranging from 47.7 to 56.1 °C. The  $T_m$  and  $X_c$  of HPC-g-PCL increased with increasing PCL content [8] which could be easily concluded from Table 1 and Fig. 3a and b. Generally,  $T_m$  of HPC-g-PCL is lower than that of PCL due to the decreased crystallinity of PCL grafts which in turn has resulted from the inhibited crystal formation via the incorporation of amorphous HPC backbone. In a way that the resulted HPC-g-PCL which contains well shortened side chains (graft copolymer synthesized without using the catalyst) did not show any  $T_m$  from DSC thermogram.

As seen in Table 1,  $T_m$  is also dependent on the content of  $\text{Sn}(\text{Oct})_2$  catalyst on the ROP of CL. Using the same CL/HPC ratio (i.e., samples D and E; Table 1), decreased in  $T_m$ , and in the corresponding  $\Delta H_m$  and  $X_c$  values, were observed for HPC-g-PCL by using higher amount of catalyst ( $T_m = 56.1$  °C and 50.7 °C for D and E, respectively). Indeed, enhancement of the initial concentration of catalyst essentially increased the overall number of active chain ends in the melt, resulting in lower length of side chain. The contrary, using higher amount of catalyst (i. e. sample F; Table 1) increasing

**Fig. 3** DSC curves of recorded on the second heating run of **a** HPC-g-PCL-93 (G), **b** HPC-g-PCL-87 (B), **c** X(HPC-g-PCL-93) ( $G_1'$ ), **d** X(HPC-g-PCL-87) ( $B_1'$ ), and **e** X(HPC-g-PCL-93) ( $G_1''$ ), and **f** X(HPC-g-PCL-87) ( $B_1''$ )



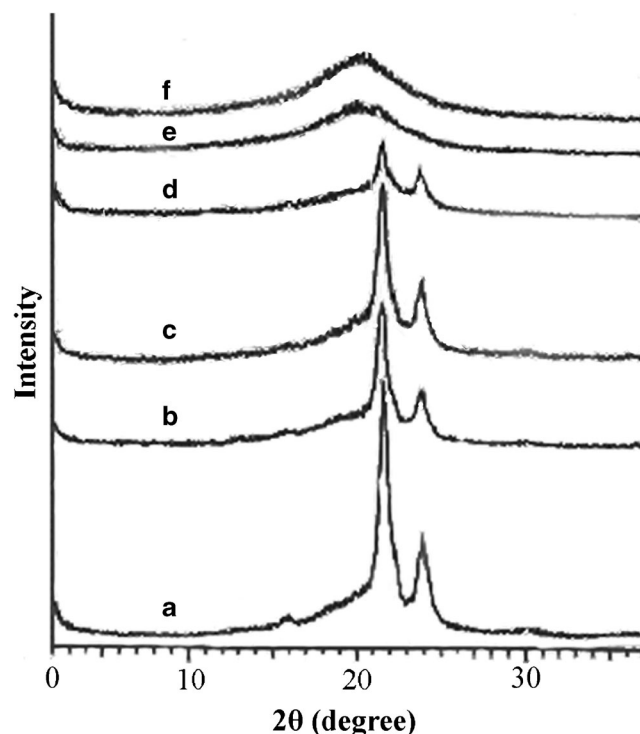
the  $T_m$  was observed. This dependence can be explained obviously based on activation of all hydroxyl groups on the HPC, resulting in higher rates of monomer consumption [24].

In our study, X(HPC-g-PCL) by using different amount of HDI and HPC-g-PCL was synthesized through two crosslinking routes. As shown in Fig. 3c to f, melting is observed for X(HPC-g-PCL), confirming the presence of crystalline phases in the films. The crosslinked films also showed a decreased  $\Delta H_m$  and  $X_c$  compared to those of the corresponding HPC-g-PCL due to the decreased quantity of crystalline phase in X(HPC-g-PCL) (Table 2).

As listed in Table 2, notable decrease in  $T_m$  are observed upon network formation indicating that network formation had a strong influence on the degree of crystallinity via more limitation in movement of PCL chains [7, 8, 25]. The melting temperature of X(HPC-g-PCL-85) decreased with increasing of HDI content and it declined to 42.9 °C and 32.9 °C at 25.0 and 15.0 % of HDI via route I and route II, respectively ( $A'$  and  $A''$ , Table 2). As the resulted X(HPC-g-PCL) (containing 85–95 % CL) via route II by using higher than 22 % HDI did not show any  $T_m$  from DSC thermogram (Table 2). When the crosslinking route II was used, both  $X_c$  and  $T_m$  dropped largely, which might result from the mild reaction conditions of route II and increasing of crosslinking efficiency.

The variation of crystallinity can also be confirmed by XRD analysis. As shown in Fig. 4a and b, spectra of HPC-g-PCL with different PCL contents displays well defined crystalline diffraction peaks at  $2\theta = 21.56$  and  $23.84^\circ$ , in agreement with those reported for PCL in the literature [26], with increased of crystalline diffraction with the former due to its

greater  $MS_{CL}$ . These results suggest that the partially crystalline phase in the HPC-g-PCL originated from the PCL side chains. On the other hand, there were significant crystallinity



**Fig. 4** Wide-angle X-ray diffraction patterns of **a** HPC-g-PCL-93 (G), **b** HPC-g-PCL-87 (B), **c** X(HPC-g-PCL-93) ( $G_1'$ ), **d** X(HPC-g-PCL-87) ( $B_1'$ ), and **e** X(HPC-g-PCL-93) ( $G_1''$ ), and X(HPC-g-PCL-87) ( $B_1''$ ) recorded at 25 °C



differences in crosslinked films (Fig. 6c to f). Similar to the results obtained from DSC analysis, the intensity of crystalline diffraction peaks of PCL also decreased in crosslinked films, especially for prepared film via route II, while it increased at  $2\theta=20.24^\circ$  (Fig. 4e and f). According to the DSC and XRD results, the crystallinity of these grafted copolymers and crosslinked films were mostly changed from a semicrystalline to an amorphous material depending on the amount of grafting PCL and degree of crosslinking.

**RSM results**

*Model design and statistical analysis*

To obtain the polynomial model representing the  $T_m$  (response) as a function of HPC/CL weight ratio, catalyst, and crosslinker amounts (factors), the data for two routes, shown in Table 3, were used. The data were analyzed using Minitab software to provide analysis of variance (ANOVA), regression coefficients, and regression. A regression equation for different factors was obtained after ANOVA. All terms regardless of their significance are included in the following fitted second-order polynomial equations in terms of the coded variables for route I (Eq. 4) and route II (Eq. 5):

$$q = 49.1763 + 3.2679x_1 + 0.3106x_2 - 0.6000x_3 - 0.0332x_1^2 - 0.0367x_2^2 + 0.0234x_3^2 - 0.8112x_1x_2 + 0.0662x_1x_3 - 0.4263x_2x_3 \tag{4}$$

$$q = 38.7692 + 1.2232x_1 + 2.3597x_2 - 2.7931x_3 - 1.0293x_1^2 + 0.2328x_2^2 + 0.6872x_3^2 - 0.3375x_1x_2 - 0.6725x_1x_3 + 0.4275x_2x_3 \tag{5}$$

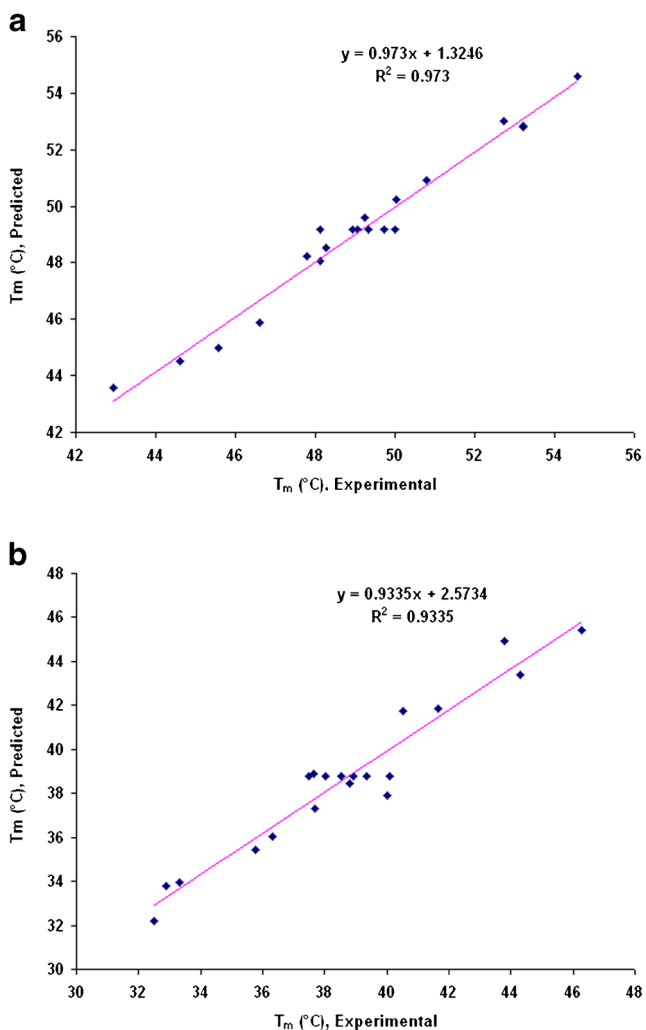
The adequacy of the regression models for explaining the experimental data at a 95 % confidence level was tested by analysis of variance (ANOVA) results. The ANOVA includes some statistic factors such as lack of fit,  $R^2$ , and adjusted  $R^2$ . From ANOVA results (Table 4) it is found that the fit of models for two routes were very satisfactory, as  $P$ -values for both

routes were 0.000 ( $P$ -value<0.05). Also, the coefficients of determination ( $R^2$ ) and adjusted coefficients of determination ( $R_{Adj}^2$ ) were 97.3, 94.9 % for route I and 93.3, 87.4 % for route II. These indicated only 2.7 % in route I and 6.7 % in route II of the total variability were not explained by the repressors in the models. The high  $R^2$  value indicated that the obtained model gives a good estimate of response of the system in the studied range. Joglekar and May suggested that for a good fit of a model,  $R^2$  should be at least 80 % [27]. The insignificance “lack of fit” with  $P$ -values of 0.506 for route I and 0.145 for route II ( $P$ -value>0.05) indicated that the models satisfactorily fitted the data. A comparison between calculated and experimental values of the  $T_m$  in two routes by using the resulted second-order polynomial Eqs. (4) and (5) were shown in Fig. 5. These plots confirm that the experimental values are in good agreement with the predicted values.

All terms in the regression model are not equally important. The significance of each term was determined by student’s  $T$ -test and  $P$ -values data (Table 5). The  $T$ -values represent the ratio of the estimated parameter effect to the estimated parameter standard deviation. The larger the magnitude of the  $T$ -value and smaller the  $P$ -value of the coefficients represent the more significance [28]. In route I results of the  $T$ -value and  $P$ -value imply that the linear effects of monomer content (ratio of CL/HPC) and crosslinker amount are more significant. Also the interactive effect of monomer-crosslinker is important whereas catalyst amount, square effect of monomer, square effect of catalyst, square effect of crosslinker, interactive effect of monomer-crosslinker and interactive effect of catalyst-crosslinker have no significant influence on the  $T_m$ . In route II the results indicate that the linear effects of monomer, catalyst, and crosslinker are more significant. Also the square effect of monomer is important whereas square effect of catalyst, square effect of crosslinker, interactive effect of monomer-catalyst, interactive effect of monomer-crosslinker and interactive effect of catalyst-crosslinker have no significant influence on the  $T_m$ .

**Table 4** Analysis of variance for route I and route II

Source	Degree of freedom		Sum of squares		Mean square		F-value		P-value	
	M 1	M 2	M 1	M 2	M 1	M 2	M 1	M 2	M 1	M 2
Regression	9	9	158.876	234.365	17.6529	26.0405	40.08	15.60	0.000	0.000
Linear	3	3	152.078	203.014	50.6925	67.6714	115.08	40.53	0.000	0.000
Square	3	3	0.045	25.359	0.0150	8.4531	0.03	5.06	0.991	0.022
Interaction	3	3	6.754	5.991	2.2512	1.9971	5.11	1.20	0.021	0.360
Residual error	10	10	4.405	16.696	0.4405	1.6696				
Lack of fit	5	5	2.186	12.251	0.4373	2.4501	0.99	2.76	0.506	0.145
Pure error	5	5	2.219	4.445	0.4437	0.8890				
Total	19	19	163.281	251.060						

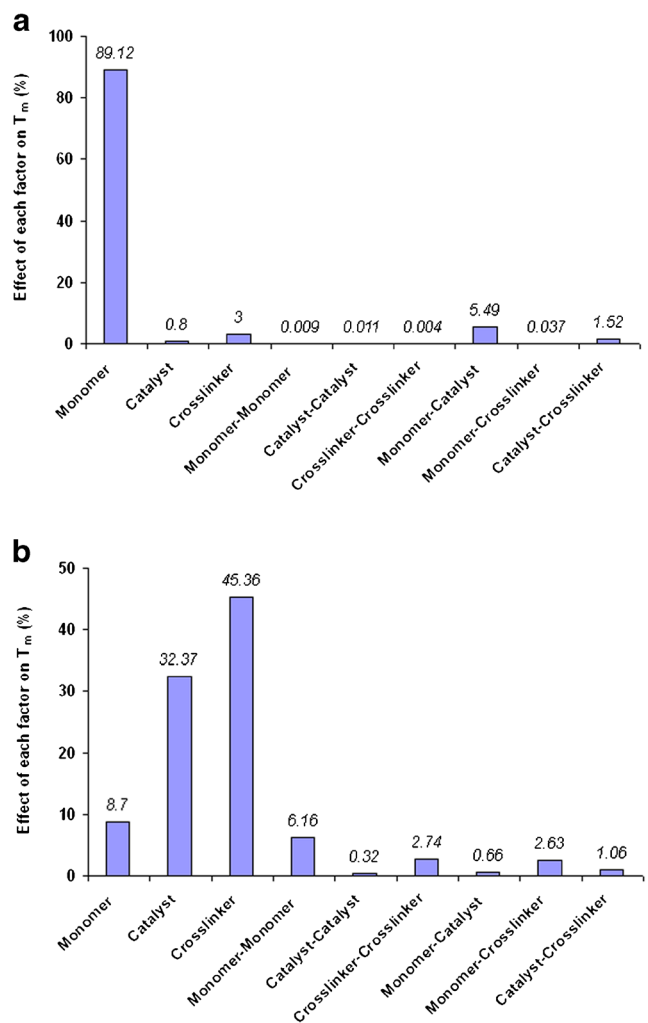


**Fig. 5** Plot of predicted results of  $T_m$  versus experimental values **a** route I and **b** route II

The probability value less than 0.05 calls for the rejection of the null hypothesis indicating that the particular term significantly affects the measured response of the system. The insignificant terms with  $P$ -values higher than 0.05 were

**Table 5** Estimated regression coefficients and corresponding  $T$ -values and  $P$ -values from the data of central composite design experiments for method 1 (M 1) and method 2 (M 2)

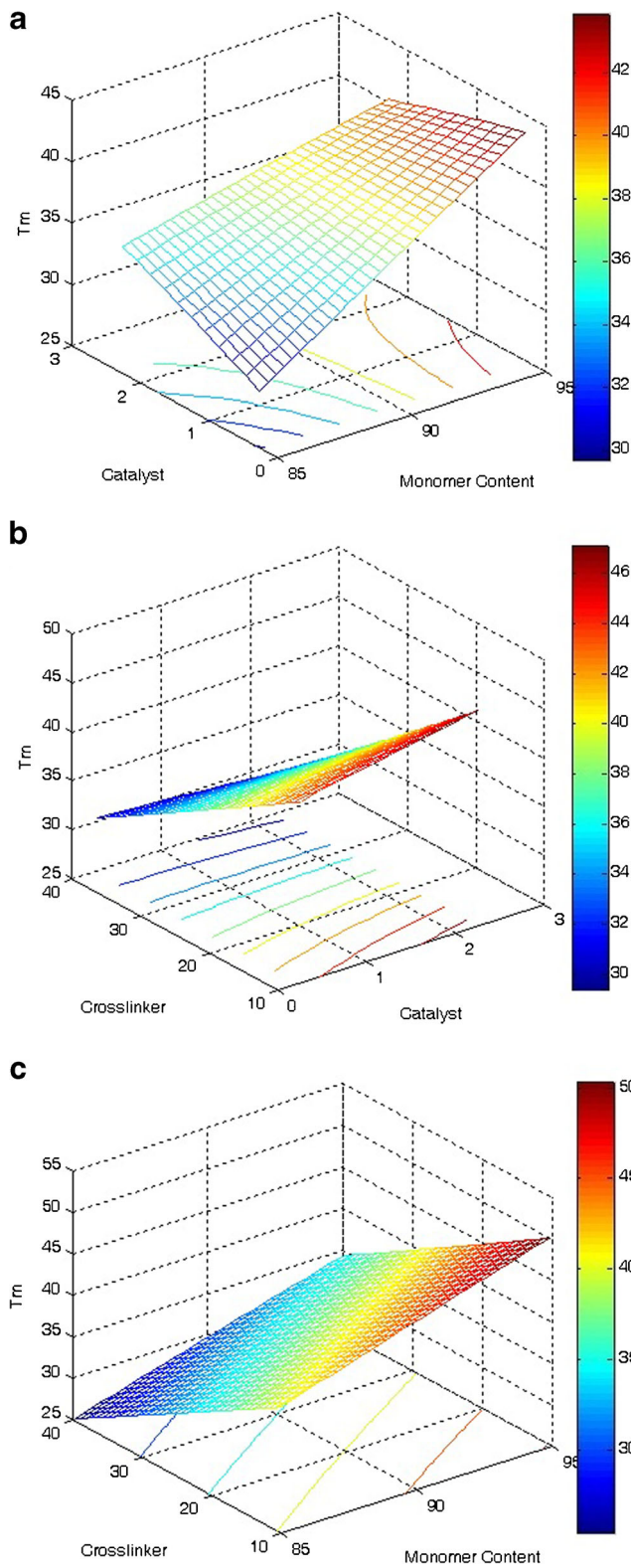
Coefficient	Parameter estimated		Standard error		$T$ -value		$P$ -value	
	M 1	M 2	M 1	M 2	M 1	M 2	M 1	M 2
$b_0$	49.1763	38.7692	0.2707	0.5270	181.674	73.567	0.000	0.000
$b_1$	3.2679	1.2232	0.1796	0.3496	18.196	3.498	0.000	0.006
$b_2$	0.3106	2.3597	0.1796	0.3496	1.729	6.749	0.114	0.000
$b_3$	-0.6000	-2.7931	0.1796	0.3496	-3.341	-7.988	0.007	0.000
$b_{11}$	-0.0322	-1.0293	0.1748	0.3404	-0.190	-3.024	0.853	0.013
$b_{22}$	-0.0367	0.2328	0.1748	0.3404	-0.210	0.684	0.838	0.509
$b_{33}$	0.0234	0.6872	0.1748	0.3404	0.134	2.019	0.896	0.071
$b_{12}$	-0.8112	-0.3375	0.2346	0.4568	-3.457	-0.739	0.006	0.477
$b_{13}$	0.0662	-0.6725	0.2346	0.4568	0.282	-1.472	0.783	0.172
$b_{23}$	-0.4263	0.4275	0.2346	0.4568	-1.817	0.936	0.099	0.371



**Fig. 6** Pareto graph for  $T_m$  **a** route I and **b** route II

removed from final expressions of the two models. The final predictive models in terms of the coded variables are presented for route I (Eq. 6) and route II (Eq. 7):

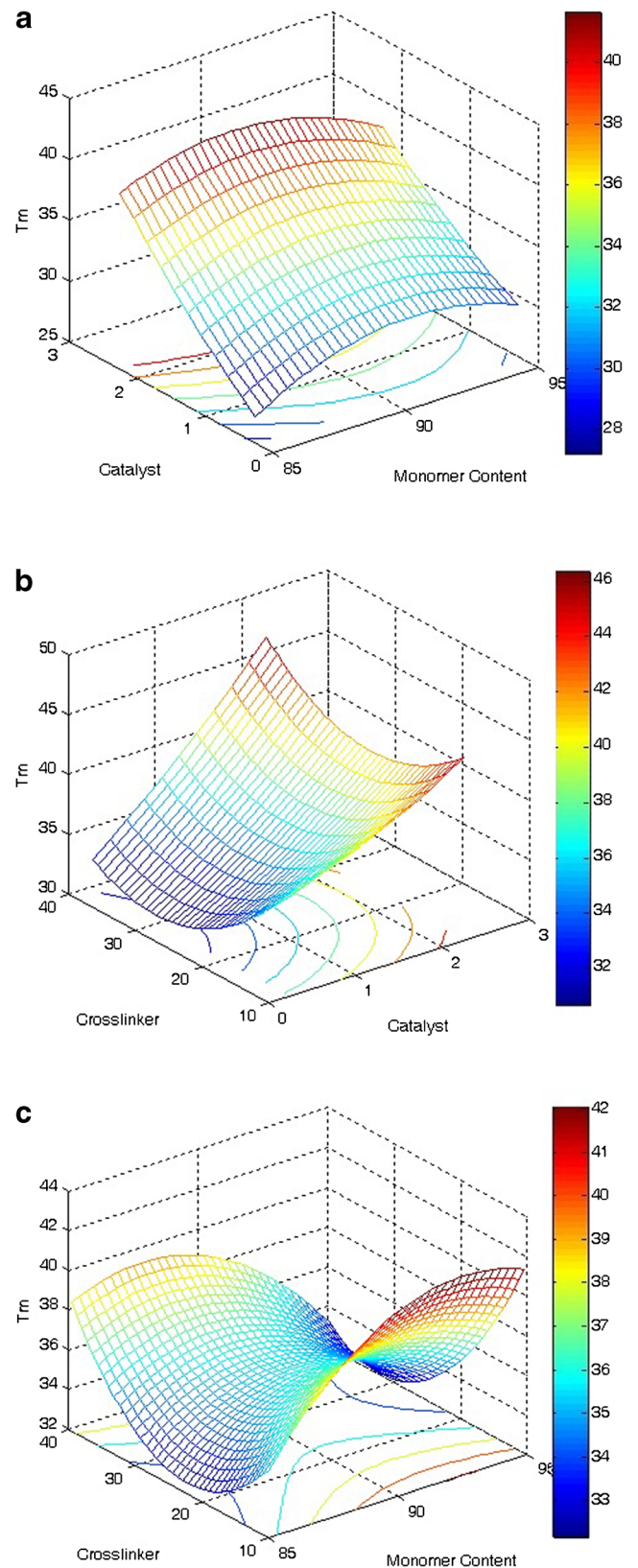
$$q = 49.1763 + 3.2679x_1 - 0.6000x_3 - 0.8112x_1x_2 \quad (6)$$



**Fig. 7** Response surface and contour plots of  $T_m$  (route I)

$$q = 38.7692 + 1.2232x_1 + 2.3597x_2 - 2.7931x_3 - 1.0293x_1^2 \quad (7)$$

The pareto analysis is used primarily to identify those factors that have the greatest cumulative effect on the



**Fig. 8** Response surface and contour plots of  $T_m$  (route II)

system, and has screen out the less significant factors. In fact, this analysis calculates the percentage effect of

each factor on the response, according to the Eq. (8) [19]:

$$P_i = \left( \frac{b_i^2}{\sum b_i^2} \right) \times 100 \quad (i \neq 0) \quad (8)$$

The results presented in Fig. 6 indicated that the important factors are different in two routes. In route I, monomer content and interactive effect of monomer-catalyst were more important. But in route II, monomer content, catalyst amount, crosslinker amount and square effect of monomer content had more influence on  $T_m$ .

#### Response surface and contour plots

The graphical explanation of the factors effects in obtained models are shown using 3D (response surface) and 2D (contour) plots. These plots predict responses by holding one factor at fixed level (normally at the zero level) and the others varying within the experimental ranges using the Minitab software. Response surface plots are helpful to predict the response for different levels of tested factors. Contour plots that give a geometric representation of the underlying response function are useful in understanding both the main and the interaction effects of factors. A circular contour of response surface indicates that the interaction between the corresponding factors is negligible. In contrast, an elliptical or saddle nature of the contour plots indicates that the interaction between the corresponding factors is significant [19].

In the present study the plots of two routes and the determined relationships between the process factors and  $T_m$  have shown in Fig. 7(a to c) and Fig. 8(a to c). In accordance with the DSC and XRD results, the RSM results showed that the  $T_m$  increased with increasing the ratio of CL/HPC. Also,  $T_m$  decreased with increase of crosslinker amount. Furthermore, from results, it can be concluded that the  $T_m$  increased with increasing the catalyst amount.

#### Optimization and verification

The optimum values of selected factors for model were obtained by solving the regression equations. In this work, the value of temperature was the most important constraint because of the biomedical application of the synthesized X(HPC-g-PCL) copolymer. The target value for  $T_m$  was selected as 38 °C. The condition for closer value to target temperature in route I was obtained with these factor values: monomer content=85.00, catalyst=0.25 and crosslinker=10.00. The optimum condition for  $T_m$  with target value of 38 °C in route II were found to be as follow: monomer content=85.32, catalyst=0.92 and crosslinker=5.00. Under these conditions, the values of  $T_m$  in route I and route II predicted by using the optimum values of the factors and model equations

were 36.15 °C and 37.70 °C, respectively. A verification of the predicted results was accomplished by performing experiments using the set of optimized factors. The values of  $T_m$  in optimum conditions obtained through the experiments were 36.50 °C and 37.65 °C. Therefore, the experimental results were in close agreement with the model predictions. Meanwhile, it was further confirmed that the optimized conditions described in this study would be helpful for the application of synthesized X(HPC-g-CL) copolymer in biomedical applications.

#### Conclusion

Well-defined HPC-g-PCL copolymers were synthesized by grafting PCL from HPC via ring opening polymerization of CL in the presence of HPC as an initiator and a catalytic amount of Sn(Oct)<sub>2</sub>. The graft copolymers were crosslinked by HDI under two different routes to prepare chemically crosslinked polymeric network (X(HPC-g-PCL)). Response surface methodology (RSM) was successfully used to optimize the process by using a factorial design approach on three experimental parameters: monomer content, amount of catalyst and crosslinker. In accordance with the DSC and XRD results, the RSM results showed that the  $T_m$  increased with increasing the ratio of CL/HPC and catalyst amount and with decreasing the crosslinker amount. Based on the fitted models, the optimum content for the biomedical application of crosslinked HPC-g-PCL films is over 85 wt.% monomer, below 1 wt.% catalyst and 10 wt.% crosslinker. The target value for  $T_m$  was selected as 38 °C. These results should be relevant and important for the developments of a novel biodegradable shape-memory materials.

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