

## A Study of the Excess Properties of Aliphatic Chlorinated Compounds with Benzylalcohol at Various Temperatures

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**Abstract** Densities ( $\rho$ ) have been measured from 298.15 to 313.15 K at atmospheric pressure over the entire composition range for binary mixtures of benzyl alcohol with 1,2-dichloroethane, 1,1,1-trichloroethane, 1,1,2,2-tetrachloroethane, trichloroethylene and tetrachloroethylene. Further, the speeds of sound in these mixtures were also measured from 303.15 to 313.15 K. The experimental density data were used to compute excess molar volumes ( $V^E$ ) which were compared with the Redlich–Kister and Hwang equations. Excess speeds of sound ( $u^E$ ), isentropic compressibilities ( $\kappa_S$ ) and excess isentropic compressibilities ( $\kappa_S^E$ ) were evaluated from experimental speed of sound and density data. Moreover, the experimental speeds of sound were compared in terms of theoretical models proposed by Schaaff's collision factor theory and Jacobson's free length theory. The experimental and derived properties are discussed in terms of intermolecular interactions between component molecules.

**Keywords** Density · Excess volume · Sound velocity · Theoretical analysis · Molecular interaction

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## 1 Introduction

Thermodynamic properties of non electrolyte solutions have proved to be a useful tool in elucidating the structural interactions among component molecules [1]. For example, excess volume and density data can be used to study solvent–solvent specific interactions as a function of temperature, while the composition dependence provides valuable un-substitutable information about the presence and the stoichiometry of complex adducts. The intermolecular interactions influence the structural arrangement along with the shape of the molecules. The sign and magnitude of these properties guide us to understand possible interactions between the component molecules. The knowledge of physicochemical properties of non-aqueous binary liquid mixtures has relevance in theoretical and applied areas of research, and such results are frequently used in the design process (flow, mass transfer or heat transfer calculations) in many chemical and industrial processes. The excess properties derived from these physical property data reflect the physicochemical behavior of the liquid mixtures with respect to the solution structure and intermolecular interactions between the component molecules of the mixture [2, 3]. In continuation of our studies of acoustic and volumetric properties of non-electrolyte liquid mixtures [4], the present study reports densities ( $\rho$ ) at 298.15, 303.15, 308.15 and 313.15 K and speed of sound data at 303.15 and 313.15 K for binary mixtures of benzylalcohol with 1,2-dichloroethane, 1,1,1-trichloroethane, 1,1,2,2-tetrachloroethane, trichloroethylene and tetrachloroethylene over the entire composition range. From these data, excess molar volumes ( $V^E$ ), excess speed of sound ( $u^E$ ) and excess isentropic compressibility ( $\kappa_S^E$ ) were calculated. Further, the experimental speed of sound data were compared with Schaaff's collision factor theory (CFT) and Jacobson's free length theory (FLT).

Liquids that were chosen in the present investigation are of much interest due to their various industrial and consumer applications. Aromatic alcohols show a large variety of relevant technical applications including as an antimicrobial agent. In addition, they are good solvents for gelatin, cellulose acetate and shellac, encountered in perfumery, veterinary science, or in microscopy as an embedding material. Benzylalcohol is also used as an additive for synthetic fuels, derived from the Fischer–Tropsch process for usage in ground and air vehicles. Further, it significantly retards the thermal degradation of jet fuels at high temperatures and is used as a dielectric solvent for the dielectrophoretic reconfiguration of nano wires [5]. Chloroalkanes and alkenes have many industrial application [6, 7], the most common use of 1,2-dichloroethane is in the production of vinyl chloride and vinyl products including polyvinyl chloride (PVC); it is also used as a solvent that is added to leaded gasoline to remove lead. 1,1,2,2-tetrachloroethane and trichloroethylene are nonflammable solvents, traditionally used in fats, waxes, resins, oils, rubber, paints, varnishes, natural resins, and alkaloids. The applications of tetrachloroethylene are in dry cleaning, textile processing, degreasing metals, insulating fluid, and cooling gas in electrical transformers.

A survey literature of binary mixtures containing benzylalcohol shows that excess volume data of benzylalcohol with benzene and substituted benzenes [8], benzylalcohol with ethanol [9], chloroalkanes and chloroalkenes with alcohol [10], benzylalcohol with 1-alcohols [11] and enthalpy data of benzylalcohol with 1-alkanols [12] and benzylalcohol with chloroalkanes and chloroalkenes [13] were reported. To the best of our knowledge, acoustic and volumetric properties of binary mixtures of benzylalcohol with the chloroalkanes and alkenes considered in this work are not reported in literature.

## 2 Experimental Section

### 2.1 Chemicals Used

All the chemicals used in the present work were of analytical reagent grade procured from S.D. Fine chemicals Ltd., India and Merck and their purities were as follows: benzylalcohol (99.5 %), 1,2-dichloroethane (99.0 %), 1,1,1-trichloroethane (99.0 %), 1,1,2,2-tetrachloroethane (99.5 %), trichloroethylene (99.0 %) and tetrachloroethylene (99.0 %) Prior to experimental measurements, all the liquids were purified as described in the literature [7, 14, 15].

### 2.2 Analysis of Water Content in Chemicals

The water content of solvents used in this work was measured using an Analab (Micro Aqua Cal 100) Karl Fischer Titrator and Karl Fisher reagent from Merck. It can detect water content from less than 10 ppm to 100 % by conductometric titration with dual platinum electrodes.

The water contents are given in Table 1 along with their CAS number, supplier and manufacturer's stated purities.

The purities of chemicals, after distillation, were checked by comparing the measured densities and speeds of sound, which are in good agreement with literature values [4, 6, 10, 16–21] and these are given in Table 2.

### 2.3 Measurements

All binary liquid mixtures were prepared by weighing appropriate amounts of pure liquids on an electronic balance (Afoset, ER-120A, India) with a precision of  $\pm 0.1$  mg, by syringing each component into airtight stopper bottles to minimize evaporation losses. The uncertainty of the mole fraction was  $\pm 1 \times 10^{-4}$ . After mixing, a bubble free homogenous sample was transferred into the U-tube of the densimeter through a syringe. The density measurements were performed with a Rudolph Research Analytical digital densimeter (Model DDM-2911), equipped with a built-in solid state thermostat and a resident program, with an accuracy of temperature of  $\pm 0.03$  K. The uncertainty in the density

**Table 1** List of chemicals with details of supplier, CAS number and purity

Chemical	Supplier	CAS number	Purity in mole fraction (as received from supplier)	Purity in mole fraction (after purification)	Water content (%)
Benzylalcohol	Merck	100-51-6	0.995	0.995	0.048
1,2-Dichloroethane	Merck	107-06-2	0.990	0.995	0.017
1,1,1-Trichloroethane	Merck	71-55-6	0.990	0.995	0.008
1,1,2,2-Tetrachloroethane	Merck	79-34-5	0.995	0.995	0.007
Trichloroethylene	S.D. Fine Chemicals Ltd.	79-01-6	0.990	0.995	0.018
Tetrachloroethylene	S.D. Fine Chemicals Ltd.	127-18-4	0.990	0.995	0.012

**Table 2** Densities ( $\rho$ ) speed of sound ( $u$ ) thermal expansion coefficient ( $\alpha$ ) and heat capacity ( $C_p$ ) of pure components at 303.15 K

Compound	Density ( $\text{g}\cdot\text{cm}^{-3}$ )		Speed of sound ( $\text{m}\cdot\text{s}^{-1}$ )		$\alpha$ ( $10^{-3} \text{ K}^{-1}$ )	$C_p$ ( $\text{J}\cdot\text{K}^{-1}\cdot\text{mol}^{-1}$ )
	Exp.	Lit.	Exp.	Lit.		
Benzylalcohol	1.03767	1.03700 [4] 1.04144 [4] <sup>a</sup> 1.03375 [4] <sup>b</sup>	1514	1511 [4] 1485 [4] <sup>b</sup>	0.740 [4]	224.4 [4]
1,2-Dichloroethane	1.23879	1.23870 [6] 1.24682 [10] <sup>a</sup> 1.23080 [18] <sup>b</sup>	1175	1176 [18] 1165 [18] <sup>b</sup>	1.138 [19]	129.5 [19]
1,1,1-Trichloroethane	1.32079	1.32070 [16] 1.32950 [10] <sup>a</sup>	944	943 [17]	1.254 [19]	169.8 [19]
1,1,1,2-Tetrachloroethane	1.57963	1.57960 [6] 1.58666 [10] <sup>a</sup> 1.57043 [18] <sup>b</sup>	1128	1132 [18] 1135 [18] <sup>b</sup>	0.964 [19]	169.8 [19]
Trichloroethylene	1.44756	1.44750 [6] 1.45537 [10] <sup>a</sup> 1.43850 [18] <sup>b</sup>	1015	1011 [18] 994 [18] <sup>b</sup>	1.121 [19]	122.4 [20]
Tetrachloroethylene	1.60724	1.60720 [6] 1.61470 [21] <sup>a</sup> 1.59724 [18] <sup>b</sup>	1028	1028 [18] 1038 [21] <sup>b</sup>	1.295 [20]	149.7 [20]

<sup>a</sup> 298.15 K<sup>b</sup> 308.15 K

measurements is  $\pm 2 \times 10^{-5} \text{ g}\cdot\text{cm}^{-3}$ . Calibration of the densimeter, at each temperature, was with doubly distilled, deionized water and with air as standards. The ultrasonic speeds in the pure liquids and in their mixtures were measured by using a multi frequency ultrasonic interferometer (M-82 Model, Mittal Enterprise, New Delhi, India) single-crystal variable-path at 303.15 and 313.15 K. The uncertainty in the measurement of ultrasonic sound velocity is  $\pm 0.3\%$ . The temperature stability is maintained within  $\pm 0.01$  K by a circulating thermostatic water bath around the cell with a circulating pump. The present investigation has been devoted to the study of densities, speed of sounds of binary liquid mixtures at different temperatures and at a pressure of 0.1 MPa.

### 3 Results and Discussion

The measured densities ( $\rho$ ) and excess volume data of the binary liquid mixtures of benzylalcohol with 1,2-dichloroethane, 1,1,1-trichloroethane, 1,1,2-tetrachloroethane, trichloroethylene and tetrachloroethylene at the temperature range from 298.15 to 313.15 K are given in Table 3 along with graphical representation in Figs. 1, 2, 3, 4 and 5. The excess molar volume ( $V^E$ ) of all the binary mixtures were calculated from the measured densities by using the following equation:

**Table 3** Mole fraction of benzylalcohol ( $x_1$ ) densities ( $\rho$ ) excess molar volumes ( $V^E$ ) and predicted excess mole volumes (Redlich–Kister and Hwang) at  $T = 298.15$ – $313.15$  K for the binary mixtures of benzylalcohol with chloroalkanes and chloroalkenes

$x_1$	$\rho$ ( $\text{g}\cdot\text{cm}^{-3}$ )	$V^E$ (experimental) ( $\text{cm}^3\cdot\text{mol}^{-1}$ )	$V^E$ (Redlich–Kister) ( $\text{cm}^3\cdot\text{mol}^{-1}$ )	$V^E$ (Hwang) ( $\text{cm}^3\cdot\text{mol}^{-1}$ )
Benzylalcohol (1) + 1,2-dichloroethane (2)				
$T = 298.15$ K				
0.0000	1.24674	0.000	0.000	0.000
0.0499	1.23564	0.054	0.054	0.053
0.1278	1.22009	0.127	0.128	0.127
0.1967	1.20584	0.183	0.183	0.182
0.2388	1.19569	0.210	0.203	0.204
0.3173	1.18128	0.253	0.252	0.254
0.3973	1.16392	0.280	0.284	0.285
0.4763	1.14722	0.305	0.307	0.304
0.5382	1.13330	0.308	0.308	0.309
0.6182	1.11938	0.300	0.296	0.294
0.6950	1.10235	0.275	0.278	0.276
0.7372	1.09334	0.257	0.257	0.258
0.7948	1.08237	0.216	0.219	0.219
0.8503	1.07041	0.174	0.175	0.177
0.9133	1.05699	0.114	0.115	0.117
0.9853	1.04471	0.021	0.021	0.021
1.0000	1.04156	0.000	0.000	0.000
$T = 303.15$ K				
0.0000	1.23879	0.000	0.000	0.000
0.0499	1.22787	0.062	0.061	0.060
0.1278	1.21406	0.140	0.143	0.141
0.1967	1.19874	0.204	0.203	0.203
0.2388	1.18944	0.238	0.237	0.238
0.3173	1.17518	0.283	0.282	0.285
0.3973	1.15837	0.323	0.323	0.325
0.4763	1.14335	0.344	0.342	0.343
0.5382	1.12954	0.354	0.355	0.354
0.6182	1.11408	0.350	0.355	0.353
0.6950	1.09787	0.325	0.321	0.323
0.7372	1.08901	0.299	0.301	0.303
0.7948	1.07776	0.262	0.264	0.263
0.8503	1.06680	0.210	0.210	0.211
0.9133	1.05419	0.139	0.137	0.135
0.9853	1.03930	0.027	0.027	0.027
1.0000	1.03767	0.000	0.000	0.000
$T = 308.15$ K				
0.0000	1.23049	0.000	0.000	0.000
0.0499	1.21807	0.067	0.067	0.065
0.1278	1.20319	0.158	0.159	0.160

**Table 3** continued

$x_1$	$\rho$ (g·cm <sup>-3</sup> )	$V^E$ (experimental) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Redlich–Kister) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Hwang) (cm <sup>3</sup> ·mol <sup>-1</sup> )
0.1967	1.18900	0.230	0.233	0.233
0.2388	1.18245	0.271	0.272	0.273
0.3173	1.16608	0.319	0.316	0.318
0.3973	1.15066	0.365	0.369	0.361
0.4763	1.13578	0.392	0.393	0.394
0.5382	1.12377	0.400	0.396	0.395
0.6182	1.10958	0.395	0.381	0.379
0.6950	1.09498	0.369	0.371	0.369
0.7372	1.08433	0.346	0.346	0.344
0.7948	1.07396	0.293	0.295	0.296
0.8503	1.06236	0.234	0.230	0.231
0.9133	1.05213	0.157	0.153	0.156
0.9853	1.03603	0.029	0.029	0.030
1.0000	1.03330	0.000	0.000	0.000
$T = 313.15$ K				
0.0000	1.22378	0.000	0.000	0.000
0.0499	1.21261	0.081	0.080	0.079
0.1278	1.19951	0.190	0.193	0.195
0.1967	1.18532	0.269	0.268	0.268
0.2388	1.17767	0.305	0.301	0.302
0.3173	1.16239	0.367	0.367	0.368
0.3973	1.14602	0.414	0.415	0.415
0.4763	1.13128	0.445	0.448	0.447
0.5382	1.11736	0.454	0.456	0.458
0.6182	1.10207	0.447	0.449	0.446
0.6950	1.08679	0.422	0.428	0.424
0.7372	1.07697	0.398	0.397	0.396
0.7948	1.06632	0.344	0.345	0.348
0.8503	1.05540	0.273	0.278	0.276
0.9133	1.04244	0.175	0.174	0.175
0.9853	1.03084	0.032	0.033	0.034
1.0000	1.02912	0.000	0.000	0.000
Benzylalcohol (1) + 1,1,1-trichloroethane (2)				
$T = 298.15$ K				
0.0000	1.32955	0.000	0.000	0.000
0.0446	1.31482	0.033	0.035	0.029
0.0921	1.29865	0.073	0.071	0.071
0.1492	1.28616	0.113	0.111	0.108
0.1700	1.27838	0.129	0.124	0.121
0.2207	1.26344	0.155	0.154	0.152
0.2954	1.24338	0.189	0.191	0.179
0.3525	1.22660	0.207	0.211	0.209
0.4090	1.21063	0.220	0.224	0.219

**Table 3** continued

$x_1$	$\rho$ (g·cm <sup>-3</sup> )	$V^E$ (experimental) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Redlich–Kister) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Hwang) (cm <sup>3</sup> ·mol <sup>-1</sup> )
0.4928	1.18750	0.225	0.227	0.230
0.6454	1.14247	0.202	0.203	0.201
0.7500	1.11361	0.162	0.159	0.158
0.8370	1.08802	0.114	0.117	0.119
0.8636	1.07922	0.090	0.091	0.093
0.9266	1.06366	0.048	0.049	0.047
0.9565	1.05240	0.028	0.029	0.031
1.0000	1.04156	0.000	0.000	0.000
$T = 303.15$ K				
0.0000	1.32079	0.000	0.000	0.000
0.0446	1.30549	0.050	0.049	0.045
0.0921	1.29154	0.099	0.096	0.092
0.1492	1.27492	0.144	0.146	0.145
0.1700	1.26938	0.161	0.162	0.160
0.2207	1.25390	0.189	0.192	0.194
0.2954	1.23384	0.230	0.235	0.227
0.3525	1.21779	0.252	0.255	0.254
0.4090	1.20175	0.266	0.267	0.263
0.4928	1.17882	0.268	0.270	0.269
0.6454	1.13564	0.240	0.244	0.245
0.7500	1.10603	0.190	0.192	0.194
0.8370	1.08272	0.131	0.134	0.137
0.8636	1.07432	0.108	0.107	0.106
0.9266	1.05693	0.056	0.059	0.059
0.9565	1.04929	0.034	0.035	0.039
1.0000	1.03767	0.000	0.000	0.000
$T = 308.15$ K				
0.0000	1.31568	0.000	0.000	0.000
0.0446	1.30033	0.063	0.059	0.060
0.0921	1.28600	0.113	0.114	0.112
0.1492	1.26880	0.166	0.170	0.169
0.1700	1.26097	0.185	0.188	0.186
0.2207	1.24836	0.220	0.223	0.223
0.2954	1.22849	0.254	0.256	0.259
0.3525	1.21283	0.279	0.277	0.278
0.4090	1.19697	0.295	0.298	0.299
0.4928	1.17462	0.301	0.299	0.297
0.6454	1.13221	0.268	0.268	0.266
0.7500	1.10297	0.214	0.212	0.213
0.8370	1.07776	0.150	0.151	0.153
0.8636	1.06954	0.122	0.120	0.129
0.9266	1.05368	0.067	0.067	0.065

**Table 3** continued

$x_1$	$\rho$ (g·cm <sup>-3</sup> )	$V^E$ (experimental) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Redlich–Kister) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Hwang) (cm <sup>3</sup> ·mol <sup>-1</sup> )
0.9565	1.04413	0.036	0.040	0.038
1.0000	1.03330	0.000	0.000	0.000
$T = 313.15$ K				
0.0000	1.30887	0.000	0.000	0.000
0.0446	1.29727	0.071	0.075	0.074
0.0921	1.28352	0.128	0.126	0.129
0.1492	1.26766	0.179	0.178	0.176
0.1700	1.26116	0.202	0.205	0.206
0.2207	1.24741	0.240	0.242	0.241
0.2954	1.22716	0.281	0.283	0.281
0.3525	1.21034	0.307	0.305	0.307
0.4090	1.19372	0.325	0.327	0.325
0.4928	1.17080	0.331	0.329	0.325
0.6454	1.12781	0.293	0.292	0.394
0.7500	1.09782	0.237	0.238	0.239
0.8370	1.07413	0.164	0.164	0.167
0.8636	1.06496	0.136	0.132	0.176
0.9266	1.04834	0.069	0.072	0.074
0.9565	1.04012	0.041	0.044	0.045
1.0000	1.02912	0.000	0.000	0.000
Benzylalcohol (1) + 1,1,2,2-tetrachloroethane (2)				
$T = 298.15$ K				
0.0000	1.58686	0.000	0.000	0.000
0.0505	1.55958	0.043	0.042	0.042
0.1012	1.53092	0.081	0.081	0.081
0.1524	1.50963	0.111	0.115	0.114
0.1908	1.48507	0.135	0.137	0.137
0.2388	1.45969	0.162	0.161	0.161
0.3157	1.41588	0.193	0.192	0.192
0.3551	1.39501	0.206	0.204	0.204
0.4234	1.35325	0.220	0.217	0.217
0.5163	1.30003	0.225	0.223	0.222
0.6337	1.23698	0.208	0.207	0.207
0.7292	1.18540	0.174	0.177	0.177
0.7980	1.14978	0.143	0.145	0.145
0.8418	1.12727	0.119	0.120	0.119
0.8972	1.09288	0.082	0.083	0.083
0.9687	1.05276	0.027	0.027	0.027
1.0000	1.04156	0.000	0.000	0.000
$T = 303.15$ K				
0.0000	1.57963	0.000	0.000	0.000
0.0505	1.55175	0.048	0.049	0.051
0.1012	1.52031	0.091	0.096	0.096



**Table 3** continued

$x_1$	$\rho$ (g·cm <sup>-3</sup> )	$V^E$ (experimental) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Redlich–Kister) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Hwang) (cm <sup>3</sup> ·mol <sup>-1</sup> )
0.1524	1.49192	0.133	0.135	0.135
0.1908	1.47009	0.155	0.160	0.159
0.2388	1.44301	0.186	0.186	0.186
0.3157	1.40502	0.220	0.218	0.217
0.3551	1.38450	0.233	0.230	0.229
0.4234	1.34607	0.246	0.242	0.242
0.5163	1.29323	0.248	0.244	0.245
0.6337	1.22904	0.227	0.224	0.225
0.7292	1.17271	0.191	0.189	0.189
0.7980	1.13646	0.151	0.154	0.154
0.8418	1.11681	0.122	0.127	0.167
0.8972	1.08537	0.086	0.088	0.087
0.9687	1.05087	0.029	0.029	0.030
1.0000	1.03767	0.000	0.000	0.000
$T = 308.15$ K				
0.0000	1.57058	0.000	0.000	0.000
0.0505	1.54148	0.059	0.059	0.065
0.1012	1.50977	0.117	0.117	0.118
0.1524	1.48417	0.155	0.161	0.162
0.1908	1.46086	0.182	0.189	0.189
0.2388	1.43297	0.211	0.216	0.216
0.3157	1.39476	0.250	0.248	0.247
0.3551	1.37527	0.262	0.259	0.257
0.4234	1.33668	0.273	0.269	0.268
0.5163	1.28510	0.277	0.269	0.269
0.6337	1.22014	0.254	0.247	0.248
0.7292	1.17429	0.214	0.211	0.212
0.7980	1.13723	0.169	0.174	0.174
0.8418	1.11468	0.141	0.145	0.145
0.8972	1.08259	0.099	0.102	0.102
0.9687	1.04345	0.033	0.033	0.034
1.0000	1.03330	0.000	0.000	0.000
$T = 313.15$ K				
0.0000	1.56374	0.000	0.000	0.000
0.0505	1.54187	0.067	0.068	0.068
0.1012	1.51359	0.137	0.138	0.139
0.1524	1.48684	0.183	0.188	0.189
0.1908	1.46086	0.214	0.218	0.218
0.2388	1.43603	0.249	0.248	0.247
0.3157	1.39438	0.282	0.280	0.279
0.3551	1.37183	0.296	0.294	0.293
0.4234	1.33553	0.310	0.309	0.308

**Table 3** continued

$x_1$	$\rho$ (g·cm <sup>-3</sup> )	$V^E$ (experimental) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Redlich–Kister) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Hwang) (cm <sup>3</sup> ·mol <sup>-1</sup> )
0.5163	1.28663	0.308	0.307	0.307
0.6337	1.22549	0.276	0.272	0.273
0.7292	1.17314	0.231	0.233	0.234
0.7980	1.13493	0.185	0.184	0.184
0.8418	1.11010	0.153	0.153	0.152
0.8972	1.07838	0.107	0.106	0.105
0.9687	1.04094	0.035	0.035	0.034
1.0000	1.02912	0.000	0.000	0.000
Benzylalcohol (1) + trichloroethylene (2)				
$T = 298.15$ K				
0.0000	1.45597	0.000	0.000	0.000
0.0537	1.43892	-0.010	-0.010	-0.010
0.1241	1.40559	-0.027	-0.026	-0.026
0.1807	1.38338	-0.041	-0.039	-0.039
0.2351	1.35906	-0.052	-0.051	-0.052
0.3066	1.32724	-0.067	-0.066	-0.066
0.3749	1.30082	-0.075	-0.077	-0.077
0.4378	1.27230	-0.081	-0.084	-0.084
0.5483	1.22456	-0.085	-0.088	-0.088
0.6075	1.20085	-0.085	-0.086	-0.085
0.6796	1.17142	-0.078	-0.078	-0.078
0.7393	1.14621	-0.070	-0.069	-0.069
0.7857	1.12489	-0.062	-0.059	-0.059
0.8498	1.10027	-0.047	-0.044	-0.044
0.9004	1.07926	-0.030	-0.030	-0.030
0.9570	1.05494	-0.012	-0.013	-0.013
1.0000	1.04156	0.000	0.000	0.000
$T = 303.15$ K				
0.0000	1.44756	0.000	0.000	0.000
0.0537	1.42675	-0.018	-0.017	-0.017
0.1241	1.39891	-0.041	-0.040	-0.039
0.1807	1.37598	-0.056	-0.057	-0.056
0.2351	1.35273	-0.069	-0.071	-0.071
0.3066	1.32391	-0.087	-0.088	-0.088
0.3749	1.29345	-0.099	-0.100	-0.099
0.4378	1.26561	-0.104	-0.107	-0.107
0.5483	1.22172	-0.108	-0.111	-0.110
0.6075	1.19683	-0.107	-0.107	-0.107
0.6796	1.16475	-0.098	-0.098	-0.098
0.7393	1.14028	-0.089	-0.087	-0.087
0.7857	1.12153	-0.079	-0.076	-0.075
0.8498	1.09601	-0.062	-0.057	-0.057
0.9004	1.07602	-0.039	-0.039	-0.039

**Table 3** continued

$x_1$	$\rho$ (g·cm <sup>-3</sup> )	$V^E$ (experimental) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Redlich–Kister) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Hwang) (cm <sup>3</sup> ·mol <sup>-1</sup> )
0.9570	1.05207	-0.016	-0.018	-0.018
1.0000	1.03767	0.000	0.000	0.000
$T = 308.15$ K				
0.0000	1.43778	0.000	0.000	0.000
0.0537	1.41949	-0.022	-0.024	-0.023
0.1241	1.39028	-0.050	-0.050	-0.049
0.1807	1.36736	-0.070	-0.068	-0.067
0.2351	1.34225	-0.087	-0.082	-0.082
0.3066	1.31277	-0.104	-0.097	-0.097
0.3749	1.28684	-0.113	-0.108	-0.109
0.4378	1.25901	-0.118	-0.116	-0.116
0.5483	1.21370	-0.123	-0.123	-0.123
0.6075	1.19078	-0.123	-0.123	-0.123
0.6796	1.16048	-0.114	-0.119	-0.117
0.7393	1.13592	-0.107	-0.110	-0.109
0.7857	1.11736	-0.096	-0.100	-0.099
0.8498	1.09279	-0.077	-0.080	-0.081
0.9004	1.07151	-0.054	-0.059	-0.060
0.9570	1.04694	-0.033	-0.029	-0.029
1.0000	1.03330	0.000	0.000	0.000
$T = 313.15$ K				
0.0000	1.43047	0.000	0.000	0.000
0.0537	1.41023	-0.026	-0.026	-0.026
0.1241	1.37841	-0.059	-0.057	-0.057
0.1807	1.35710	-0.079	-0.079	-0.079
0.2351	1.33458	-0.098	-0.097	-0.093
0.3066	1.30606	-0.116	-0.117	-0.117
0.3749	1.27814	-0.129	-0.131	-0.131
0.4378	1.25142	-0.139	-0.140	-0.139
0.5483	1.20549	-0.144	-0.145	-0.144
0.6075	1.18327	-0.140	-0.141	-0.141
0.6796	1.15595	-0.132	-0.132	-0.131
0.7393	1.12983	-0.121	-0.118	-0.118
0.7857	1.11182	-0.106	-0.105	-0.105
0.8498	1.08390	-0.082	-0.081	-0.081
0.9004	1.06498	-0.060	-0.058	-0.059
0.9570	1.04277	-0.026	-0.027	-0.027
1.0000	1.02912	0.000	0.000	0.000
Benzylalcohol (1) + tetrachloroethylene (2)				
$T = 298.15$ K				
0.0000	1.61476	0.000	0.000	0.000
0.0473	1.58886	-0.016	-0.017	-0.016
0.0772	1.56965	-0.026	-0.025	-0.025

**Table 3** continued

$x_1$	$\rho$ (g·cm <sup>-3</sup> )	$V^E$ (experimental) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Redlich–Kister) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Hwang) (cm <sup>3</sup> ·mol <sup>-1</sup> )
0.1102	1.55044	-0.037	-0.035	-0.035
0.1759	1.51463	-0.058	-0.054	-0.054
0.2330	1.48231	-0.071	-0.069	-0.069
0.3365	1.42205	-0.090	-0.090	-0.089
0.4282	1.36703	-0.099	-0.100	-0.100
0.5173	1.31769	-0.100	-0.103	-0.103
0.5702	1.28668	-0.098	-0.101	-0.101
0.6363	1.25175	-0.092	-0.094	-0.094
0.7377	1.19061	-0.076	-0.076	-0.076
0.7991	1.15480	-0.062	-0.062	-0.062
0.8562	1.12162	-0.047	-0.046	-0.046
0.9026	1.09236	-0.033	-0.032	-0.032
0.9591	1.05961	-0.015	-0.015	-0.014
1.0000	1.04156	0.000	0.000	0.000
<i>T</i> = 303.15 K				
0.0000	1.60724	0.000	0.000	0.000
0.0473	1.57776	-0.022	-0.022	-0.023
0.0772	1.55966	-0.034	-0.036	-0.036
0.1102	1.54203	-0.052	-0.049	-0.049
0.1759	1.50166	-0.072	-0.073	-0.073
0.2330	1.47151	-0.089	-0.089	-0.089
0.3365	1.41073	-0.110	-0.111	-0.110
0.4282	1.35876	-0.119	-0.120	-0.120
0.5173	1.30540	-0.120	-0.121	-0.121
0.5702	1.27989	-0.116	-0.118	-0.118
0.6363	1.24416	-0.110	-0.109	-0.109
0.7377	1.18063	-0.090	-0.089	-0.089
0.7991	1.14727	-0.074	-0.073	-0.073
0.8562	1.11618	-0.057	-0.055	-0.055
0.9026	1.09084	-0.039	-0.039	-0.038
0.9591	1.05994	-0.017	-0.017	-0.017
1.0000	1.03767	0.000	0.000	0.000
<i>T</i> = 308.15 K				
0.0000	1.59798	0.000	0.000	0.000
0.0473	1.56785	-0.024	-0.026	-0.025
0.0772	1.55027	-0.040	-0.039	-0.040
0.1102	1.52888	-0.054	-0.054	-0.055
0.1759	1.49334	-0.082	-0.084	-0.083
0.2330	1.46354	-0.102	-0.103	-0.103
0.3365	1.40546	-0.127	-0.127	-0.127
0.4282	1.35235	-0.137	-0.138	-0.138
0.5173	1.30191	-0.138	-0.139	-0.139
0.5702	1.27287	-0.135	-0.135	-0.135

**Table 3** continued

$x_1$	$\rho$ (g·cm <sup>-3</sup> )	$V^E$ (experimental) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Redlich–Kister) (cm <sup>3</sup> ·mol <sup>-1</sup> )	$V^E$ (Hwang) (cm <sup>3</sup> ·mol <sup>-1</sup> )
0.6363	1.23963	-0.126	-0.126	-0.126
0.7377	1.17964	-0.104	-0.103	-0.103
0.7991	1.14334	-0.084	-0.084	-0.084
0.8562	1.11354	-0.063	-0.064	-0.063
0.9026	1.08641	-0.044	-0.045	-0.044
0.9591	1.05622	-0.020	-0.020	-0.019
1.0000	1.03330	0.000	0.000	0.000
$T = 313.15$ K				
0.0000	1.59053	0.000	0.000	0.000
0.0473	1.56670	-0.031	-0.031	-0.031
0.0772	1.55104	-0.048	-0.048	-0.048
0.1102	1.53002	-0.066	-0.066	-0.067
0.1759	1.49716	-0.097	-0.096	-0.096
0.2330	1.46277	-0.117	-0.118	-0.118
0.3365	1.40202	-0.144	-0.145	-0.145
0.4282	1.35120	-0.155	-0.157	-0.157
0.5173	1.30038	-0.157	-0.158	-0.158
0.5702	1.27402	-0.154	-0.154	-0.154
0.6363	1.23581	-0.144	-0.145	-0.145
0.7377	1.17658	-0.121	-0.120	-0.121
0.7991	1.14487	-0.101	-0.099	-0.099
0.8562	1.11316	-0.077	-0.076	-0.076
0.9026	1.08182	-0.055	-0.054	-0.054
0.9591	1.05317	-0.023	-0.024	-0.024
1.0000	1.02912	0.000	0.000	0.000

$$V^E = \frac{x_1M_1 + x_2M_2}{\rho} - \left( \frac{x_1M_1}{\rho_1} + \frac{x_2M_2}{\rho_2} \right) \tag{1}$$

where  $x_1, x_2, M_1, M_2, \rho_1, \rho_2$  and  $\rho_m$  are the mole fraction, molar mass, and the density of pure components 1 and 2 and mixture, respectively. Moreover, the experimental excess volumes were also analyzed in terms of Redlich–Kister [22] and Hwang et al. [23] equations and these are also included in Table 3.

The empirical relation proposed by Redlich–Kister is given as follows:

$$V^E = x_1x_2 \left\{ a_0 + a_1(x_1 - x_2) - a_2(x_1 - x_2)^2 \right\} \tag{2}$$

where  $a_i$  are adjustable parameters and  $x_1$  is the mole fraction of benzylalcohol. The values of these parameters were obtained by the least-squares method.

The Hwang et al. equation takes the following form:

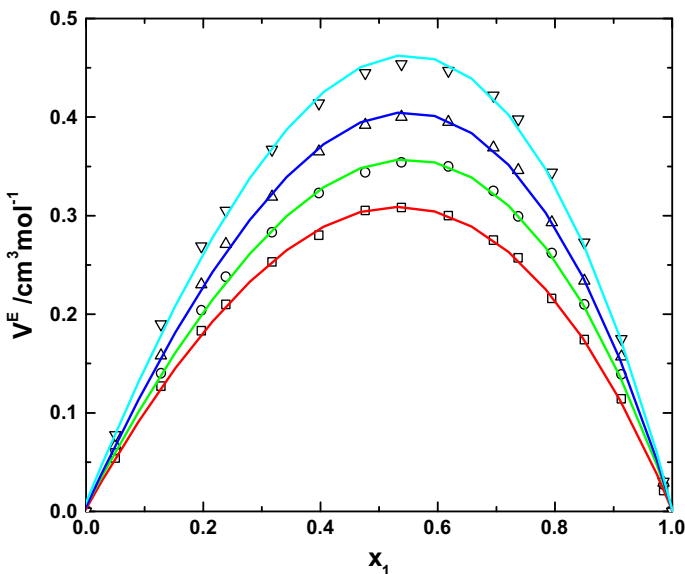
$$V^E = x_1x_2(b_0 + b_1x_1^3 + b_2x_2^3) \tag{3}$$

where  $x_1$  and  $x_2$  represent the mole fractions of benzylalcohol and chloroalkanes and alkenes, respectively, and the  $b_i$  are constants. The computation of  $b_i$  coefficients in the

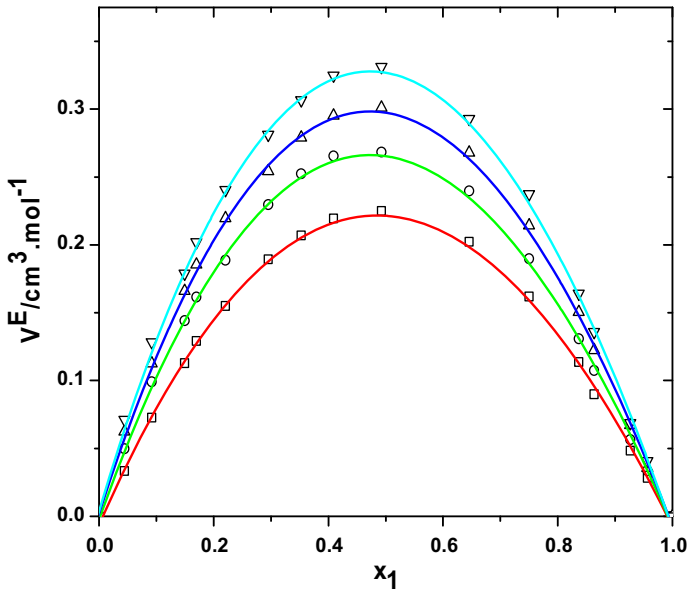
above equation was described earlier [24, 25]. The values of the two sets of constants are given in Tables 4 and 5 along with standard deviation ( $\sigma V^E$ ) and these values point out that equations of Redlich–Kister and Hwang et al. also precisely represent the experimental excess volume data.

An examination of  $V^E$  data in Figs. 1, 2, 3, 4 and 5 for the binary mixtures of benzylalcohol with 1,2-dichloroethane, 1,1,1-trichloroethane, 1,1,2,2-tetrachloroethane are positive, while for trichloroethylene and tetrachloroethylene systems they are negative, over the entire mole fraction range at all temperatures. Desnoyers and Perron [26] suggested that representing the nonideality as excess quantities can be quite misleading, specifically for mixtures having strong interactions at low concentrations, and it is better to plot  $V^E/x_2(1-x_2)$  against  $x_2$ , which gives nearly straight line for binary liquid mixtures of similar size and polarity. This function  $V^E/x_2(1-x_2)$  is equivalent to an apparent molar quantity over the whole mole fraction range, and its extrapolation to  $x_2 = 0$  and  $x_2 = 1$  will give the two excess partial molar quantities, which are important to understand the solute–solvent interactions. For the binary mixtures of benzylalcohol with 1,2-dichloroethane, 1,1,1-trichloroethane, 1,1,2,2-tetrachloroethane, the plots of  $V^E/x_2(1-x_2)$  against  $x_2$  are shown in supporting information (Figs. S1–S5). Comparisons of Figs. 1, 2, 3, 4 and 5 with Figs. S1–S5, show that  $V^E/x_2(1-x_2)$  is more sensitive than  $V^E$  to interactions which occur at low concentrations.

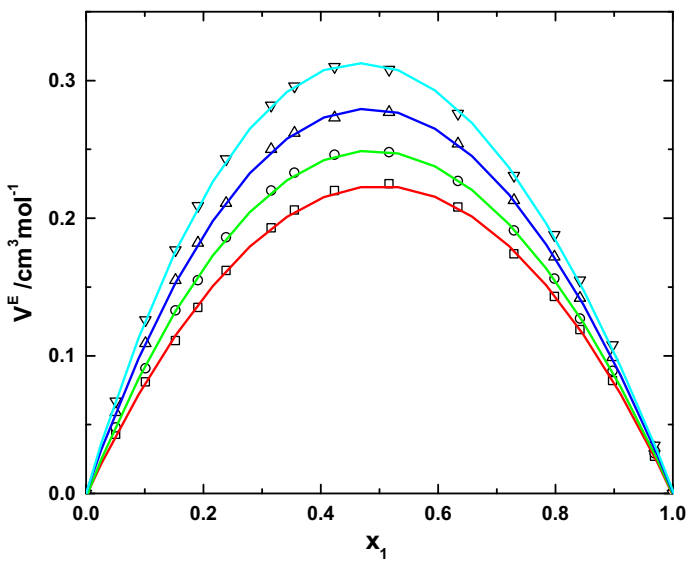
The variation of excess volume with mole fraction, for all the binary mixtures under the present investigation, may be explained by the following factors: (i) contraction of volume due to dipole–dipole and dipole-induced dipole interactions; (ii) complex formation between benzylalcohol with chloroethanes [27]. A perusal of the  $V^E$  data in Figs. 1, 2, and 3



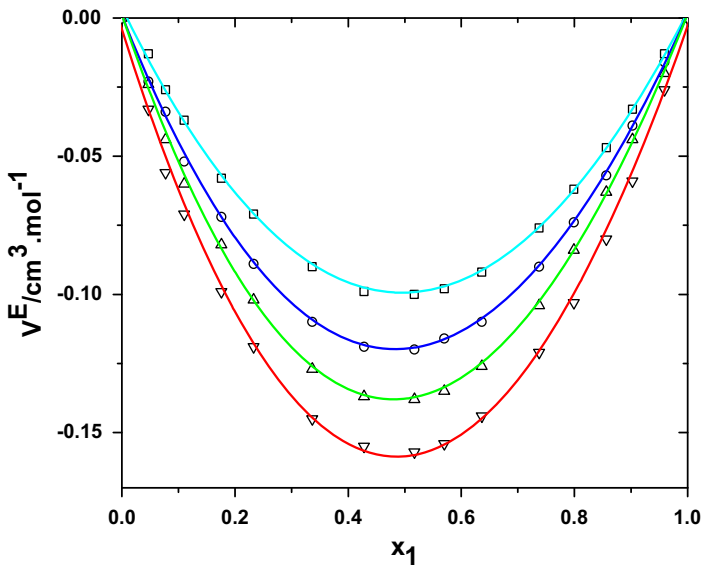
**Fig. 1** Variation of the excess volume ( $V^E$ ) of the binary liquid mixtures of benzylalcohol (1) with 1,2-dichloroethane (2) at 298.15 K (square), 303.15 K (circle), 308.15 K (triangle) and 313.15 K (inverted triangle)



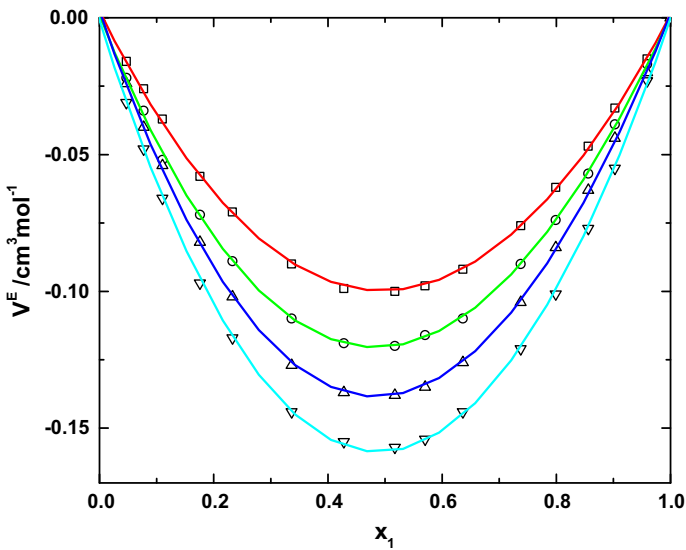
**Fig. 2** Variation of the excess volume ( $V^E$ ) of the binary liquid mixtures of benzylalcohol (1) with 1,1,1-trichloroethane (2) at 298.15 K (square), 303.15 K (circle), 308.15 K (triangle) and 313.15 K (inverted triangle)



**Fig. 3** Variation of the excess volume ( $V^E$ ) of the binary liquid mixtures of benzylalcohol (1) with 1,1,2,2-tetrachloroethane (2) at 298.15 K (square), 303.15 K (circle), 308.15 K (triangle) and 313.15 K (inverted triangle)



**Fig. 4** Variation of the excess volume ( $V^E$ ) of the binary liquid mixtures of benzylalcohol (1) with trichloroethylene (2) at 298.15 K (square), 303.15 K (circle), 308.15 K (triangle) and 313.15 K (inverted triangle)



**Fig. 5** Variation of the excess volume ( $V^E$ ) of the binary liquid mixtures of benzylalcohol (1) with tetrachloroethylene (2) at 298.15 K (square), 303.15 K (circle), 308.15 K (triangle) and 313.15 K (inverted triangle)

reveals that the former factor, which contributes to positive excess volumes is dominant in the binary mixtures of benzylalcohol and chloroalkanes(1,2-dichloroethane, 1,1,1-trichloroethane, 1,1,2,2-tetrachloroethane).



**Table 4** Constants ( $a_i$ ) and corresponding standard deviation  $\sigma(V^E)$  values obtained from the Redlich–Kister equation, Eq. 2

Temperature	$a_0$ (cm <sup>3</sup> ·mol <sup>-1</sup> )	$a_1$ (cm <sup>3</sup> ·mol <sup>-1</sup> )	$a_2$ (cm <sup>3</sup> ·mol <sup>-1</sup> )	$\sigma(V^E)$ (cm <sup>3</sup> ·mol <sup>-1</sup> )
Benzylalcohol (1) + 1,2-dichloroethane (2)				
298.15 K	1.2201	0.1659	0.0826	0.002
303.15 K	1.3892	0.2788	0.1920	0.003
308.15 K	1.5888	0.3122	0.1319	0.003
313.15 K	1.8174	0.3107	0.1783	0.006
Benzylalcohol (1) + 1,1,1-trichloroethane (2)				
298.15 K	0.9227	-0.0670	-0.1993	0.004
303.15 K	1.0779	-0.1661	-0.0972	0.004
308.15 K	1.1924	-0.2215	-0.0209	0.004
313.15 K	1.3048	-0.2550	-0.0039	0.003
Benzylalcohol (1) + 1,1,2,2-tetrachloroethane (2)				
298.15 K	0.8938	0.0033	-0.0112	0.002
303.15 K	0.9994	-0.0353	0.0236	0.002
308.15 K	1.1085	-0.0846	0.0530	0.001
313.15 K	1.2393	-0.1447	0.0526	0.002
Benzylalcohol (1) + trichloroethylene (2)				
298.15 K	-0.3510	-0.0648	0.1096	0.002
303.15 K	-0.4422	-0.0497	0.0679	0.003
308.15 K	-0.4844	-0.1224	-0.1231	0.004
313.15 K	-0.5764	-0.0742	-0.0121	0.001
Benzylalcohol (1) + tetrachloroethylene (2)				
298.15 K	-0.4040	-0.0027	0.0426	0.001
303.15 K	-0.4849	0.0317	0.0206	0.001
308.15 K	-0.5581	0.0284	0.0421	0.001
313.15 K	-0.6342	0.0378	-0.0152	0.001

The excess volumes for mixtures of chloroalkanes show the following order: 1,2-dichloroethane > 1,1,1-trichloroethane > 1,1,2,2-tetrachloroethane

This order suggests an absence of H-bonding in these systems, since the interactions are maximum in the system of 1,1,2,2-tetrachloroethane. Further, the presence of one more chlorine atom in 1,1,1-trichloroethane increases its electron accepting capacity and therefore it reacts more strongly towards a benzylalcohol molecule when compared to 1,2-dichloroethane, making less positive values for benzylalcohol with 1,1,1-trichloroethane than for benzylalcohol with 1,2-dichloroethane. Similarly, in the case of the benzylalcohol with 1,1,2,2-tetrachloroethane system, less positive values are observed when compared to benzylalcohol with the 1,2-dichloroethane and 1,1,1-trichloroethane systems. This suggests that as the number of chlorine atoms in an alkane molecule increases, the intermolecular interactions increase, thereby less positive  $V^E$  values are observed in the system of 1,1,2,2-tetrachloroethane than in the cases of 1,2-dichloroethane and 1,1,1-trichloroethane, molecules containing two and three chlorine atoms, respectively. Thus, the fewer chlorine atoms in the alkane molecule, the more positive is the observed value of  $V^E$  [28].

The  $V^E$  data of the system containing tetrachloroethylene are more negative than for the benzylalcohol with trichloroethylene mixtures. This result likely reflects the double bond

**Table 5** Constants ( $b_i$ ) and corresponding standard deviation values  $\sigma(V^E)$  obtained from the Hwang equation, Eq. 3

Temperature	$b_0$ (cm <sup>3</sup> ·mol <sup>-1</sup> )	$b_1$ (cm <sup>3</sup> ·mol <sup>-1</sup> )	$b_2$ (cm <sup>3</sup> ·mol <sup>-1</sup> )	$\sigma(V^E)$ (cm <sup>3</sup> ·mol <sup>-1</sup> )
Benzylalcohol (1) + 1,2-dichloroethane (2)				
298.15 K	1.1926	0.3076	-0.0874	0.006
303.15 K	1.3252	0.5879	-0.0759	0.006
308.15 K	1.5448	0.5475	-0.1958	0.005
313.15 K	1.7579	0.6076	-0.1321	0.005
Benzylalcohol (1) + 1,1,1-trichloroethane (2)				
298.15 K	0.9891	-0.3455	-0.1859	0.002
303.15 K	1.1103	-0.3273	0.0681	0.006
308.15 K	1.1993	-0.2915	0.2358	0.005
313.15 K	1.3061	-0.3088	0.2983	0.004
Benzylalcohol (1) + 1,1,2,2-tetrachloroethane (2)				
298.15 K	0.8975	-0.011	-0.0189	0.001
303.15 K	0.9915	-0.0106	0.0735	0.003
308.15 K	1.0908	-0.0301	0.1714	0.001
313.15 K	1.2218	-0.1021	0.2424	0.002
Benzylalcohol (1) + trichloroethylene (2)				
298.15 K	-0.3875	0.0690	0.2232	0.001
303.15 K	-0.4648	0.0314	0.1496	0.002
308.15 K	-0.4433	-0.3099	-0.0184	0.001
313.15 K	-0.5724	-0.1045	0.0721	0.002
Benzylalcohol (1) + tetrachloroethylene (2)				
298.15 K	-0.4182	0.0536	0.0601	0.001
303.15 K	-0.4918	0.0652	-0.0103	0.001
308.15 K	-0.5721	0.0899	0.0223	0.001
313.15 K	-0.6291	0.0247	-0.0653	0.001

character of chloroethylenes, shielding of the ethylenic double bond by chlorine atoms and partial saturation of the electron accepting nature of chlorine atoms by  $\pi$ -electrons of the ethylenic double bond [6, 17, 29].

The excess volume data for mixtures of chloroalkanes and chloroalkenes shows the following order: tetrachloroethylene > trichloroethylene

The more negative  $V^E$  data for the system of benzylalcohol with tetrachloroethylene may be ascribed to  $\pi$ - $\pi$  interactions between the unlike molecules, but  $\pi$ -electrons of the tetrachloroethylene donor are involved because of partial shielding by the chlorine atoms [30]; also, the shielding capacity of double bond character is observed to a greater extent in tetrachloroethylene, because of the presence of four chlorine atoms, when compared with trichloroethylene.

Data for mole fraction ( $x_1$ ) of benzylalcohol, density ( $\rho$ ) of pure liquids and their liquid mixtures, and experimental sound velocities ( $u$ ), isentropic compressibilities ( $\kappa_S$ ) and excess isentropic compressibilities ( $\kappa_S^E$ ) data are presented Table 6. The excess isentropic compressibility data are also represented graphically in Figs. 6 and 7.

From the result of speed of sound ( $u$ ), densities ( $\rho$ ), excess isentropic compressibilities ( $\kappa_S^E$ ) was calculated as [31]:

**Table 6** Mole fraction ( $x_1$ ) of benzylalcohol, densities ( $\rho$ ), speed of sound ( $w$ ), isentropic compressibilities ( $\kappa_S$ ), excess isentropic compressibilities ( $\kappa_S^E$ ), theoretical speed of sound, and excess speed of sound ( $w^E$ ) values of benzylalcohol (1) with chloroalkanes and chloroalkenes (2) at 303.15 and 313.15 K

$x_1$	$w$ (m·s <sup>-1</sup> )	$\kappa_S$ (TPa <sup>-1</sup> )	$w_{FLT}$ (m·s <sup>-1</sup> )	$w_{CFT}$ (m·s <sup>-1</sup> )	$\kappa_S^E$ (Exp) (TPa <sup>-1</sup> )	$\kappa_S^E$ (Redlich–Kister) (TPa <sup>-1</sup> )	$\kappa_S^E$ (Hwang) (TPa <sup>-1</sup> )	$w^E$ (Exp) (m·s <sup>-1</sup> )	$w^E$ (Redlich–Kister) (m·s <sup>-1</sup> )	$w^E$ (Hwang) (m·s <sup>-1</sup> )
Benzylalcohol (1) + 1,2-dichloroethane (2)										
$T = 303.15$ K										
0.0000	1175	585	–	–	0.0	0.0	0.0	0.0	0.0	0.0
0.0499	1190	576	1208	1205	-5.9	-5.7	-5.6	3.4	3.9	3.7
0.1278	1216	561	1225	1227	-10.6	-12.0	-11.9	7.9	8.4	8.2
0.1967	1238	548	1244	1241	-14.9	-15.7	-15.6	11.2	11.2	11.2
0.2388	1253	540	1258	1255	-16.9	-17.2	-17.3	13.6	12.7	12.8
0.3173	1282	523	1289	1287	-19.6	-19.3	-19.3	16.0	14.9	15.1
0.3973	1309	509	1304	1308	-22.4	-20.4	-20.5	19.4	16.9	17.1
0.4763	1338	494	1228	1330	-23.4	-21.0	-21.0	20.8	18.7	18.7
0.5382	1360	484	1365	1358	-24.1	-21.2	-21.2	22.4	19.9	19.8
0.6182	1388	471	1389	1883	-23.7	-20.9	-20.9	22.9	21.0	20.8
0.6950	1414	460	1412	1418	-21.1	-20.0	-19.9	21.7	21.2	21.0
0.7372	1428	454	1428	1420	-17.3	-19.1	-19.1	18.7	20.7	20.6
0.7948	1447	446	1451	1455	-13.9	-17.2	-17.2	15.2	19.2	19.2
0.8503	1468	437	1467	1469	-11.6	-14.4	-14.2	13.1	16.5	16.6
0.9133	1491	428	1504	1502	-7.8	-9.8	-9.8	9.4	11.4	11.7
0.9853	1511	421	1516	1515	-2.6	-2.0	-2	3.1	2.4	2.5
1.0000	1514	420	–	–	0.0	0.0	0.0	0.0	0.0	0.0
$T = 313.15$ K										
0.0000	1155	613	–	–	0.0	0.0	0.0	0.0	0.0	0.0
0.0499	1168	605	1163	1165	-5.4	-5.1	-5.0	1.7	2.0	2.0
0.1278	1194	588	1204	1202	-9.2	-10.5	-10.4	4.3	4.4	4.4
0.1967	1218	573	1216	1218	-12.3	-13.4	-13.4	6.3	6.0	6.0

Table 6 continued

$x_1$	$u$ ( $\text{m}\cdot\text{s}^{-1}$ )	$\kappa_S$ ( $\text{TPa}^{-1}$ )	$u_{\text{FLT}}$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u_{\text{CFT}}$ ( $\text{m}\cdot\text{s}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Exp})$ ( $\text{TPa}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Redlich-Kister})$ ( $\text{TPa}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Hwang})$ ( $\text{TPa}^{-1}$ )	$u^{\text{E}}(\text{Exp})$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u^{\text{E}}(\text{Redlich-Kister})$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u^{\text{E}}(\text{Hwang})$ ( $\text{m}\cdot\text{s}^{-1}$ )
0.2388	1231	565	1230	1235	-14.0	-14.5	-14.6	7.3	6.7	6.8
0.3173	1255	552	1258	1262	-16.5	-15.9	-16.0	8.5	7.8	7.8
0.3973	1284	535	1289	1286	-18.9	-16.8	-16.9	9.5	8.5	8.5
0.4763	1310	521	1305	1307	-20.1	-17.6	-17.6	9.8	8.9	8.9
0.5382	1327	513	1337	1338	-21.1	-18.1	-18.1	10.0	9.1	9.0
0.6182	1355	499	1356	1353	-21.2	-18.6	-18.5	9.9	9.0	8.9
0.6950	1379	488	1385	1386	-19.7	-18.6	-18.5	8.5	8.5	8.5
0.7372	1396	479	1389	1397	-16.9	-18.2	-18.2	7.0	8.1	8.1
0.7948	1415	471	1500	1507	-13.4	-14.0	-14.0	5.4	7.2	7.2
0.8503	1432	463	1430	1432	-12.0	-14.7	-14.7	4.4	6.0	6.0
0.9133	1457	452	1461	1465	-8.1	-10.3	-10.4	3.4	4.0	4.0
0.9853	1478	444	1479	1474	-2.8	-2.2	-2.2	1.1	0.8	0.8
1.0000	1485	441	-	-	0.0	0.0	0.0	0.0	0.0	0.0
Benzylalcohol (1) + 1,1,1-trichloroethane (2)										
$T = 303.15 \text{ K}$										
0.0000	944	850	-	-	0.0	0.0	0.0	0.0	0.0	0.0
0.0446	972	823	987	982	-8.2	-7.0	-7.0	10.9	10.2	10.4
0.0921	994	829	998	1004	-12.7	-13.7	-13.7	20.0	20.0	20.3
0.1492	1030	779	1036	1035	-19.5	-20.7	-20.7	28.6	30.3	30.5
0.1700	1044	761	1053	1057	-22.1	-23.0	-23.0	32.1	33.8	33.4
0.2207	1071	729	1080	1085	-26.8	-27.9	-27.9	41.6	41.3	40.3
0.2954	1113	684	1121	1119	-32.7	-33.6	-33.6	51.1	50.5	51.0
0.3525	1148	649	1156	1158	-35.9	-36.7	-36.7	55.3	56.1	56.8
0.4090	1179	621	1184	1185	-38.6	-38.7	-38.6	60.0	60.2	61.4
0.4928	1226	583	1232	1237	-40.1	-39.6	-39.6	64.6	63.8	64.0

**Table 6** continued

$x_1$	$u$ ( $\text{m}\cdot\text{s}^{-1}$ )	$\kappa_S$ ( $\text{TPa}^{-1}$ )	$u_{\text{FLT}}$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u_{\text{CFT}}$ ( $\text{m}\cdot\text{s}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Exp})$ ( $\text{TPa}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Redlich-Kister})$ ( $\text{TPa}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Hwang})$ ( $\text{TPa}^{-1}$ )	$u^{\text{E}}(\text{Exp})$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u^{\text{E}}(\text{Redlich-Kister})$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u^{\text{E}}(\text{Hwang})$ ( $\text{m}\cdot\text{s}^{-1}$ )
0.6454	1315	521	1321	1325	-36.6	-35.4	-35.5	62.8	61.9	63.1
0.7500	1370	489	1375	1374	-29.7	-28.5	-28.5	52.8	53.2	53.5
0.8370	1417	465	1419	1423	-21.7	-20.3	-20.3	41.5	40.5	40.9
0.8636	1433	457	1442	1435	-18.5	-17.4	-17.4	36.4	35.4	36.5
0.9266	1469	440	1472	1475	-10.4	-9.9	-9.8	21.3	21.2	21.4
0.9565	1489	431	1495	1499	-4.9	-6.0	-5.9	12.6	13.2	13.8
1.0000	1514	420	-	-	0.0	0.0	0.0	0.0	0.0	0.0
$T = 313.15 \text{ K}$										
0.0000	915	913	-	-	0.0	0.0	0.0	0.0	0.0	0.0
0.0446	944	826	954	956	-4.0	-4.0	-4.1	7.3	9.9	6.9
0.0921	967	834	975	978	-9.0	-8.0	-8.1	14.5	19.7	14.0
0.1492	997	795	1006	1004	-12.0	-12.5	-12.6	21.3	30.2	22.0
0.1700	1016	769	1025	1031	-13.6	-14.0	-14.0	24.3	33.7	24.7
0.2207	1043	738	1049	1052	-16.6	-17.3	-17.3	30.2	41.4	30.8
0.2954	1087	691	1096	1094	-20.9	-21.1	-21.1	37.5	50.8	38.3
0.3525	1121	659	1133	1135	-22.7	-23.2	-23.0	42.0	56.3	42.6
0.4090	1153	631	1156	1154	-24.0	-24.5	-24.4	45.2	60.4	45.6
0.4928	1198	596	1204	1206	-24.3	-24.9	-24.9	45.4	63.8	47.4
0.6454	1281	541	1287	1289	-21.3	-21.3	-21.4	43.4	61.7	42.9
0.7500	1338	509	1343	1344	-17.3	-16.2	-16.3	35.8	53.1	34.3
0.8370	1391	481	1395	1396	-12.4	-10.8	-10.8	26.2	40.6	24.1
0.8636	1407	474	1409	1405	-9.7	-9.1	-9.0	21.4	35.6	20.6
0.9266	1440	460	1446	1445	-4.4	-4.8	-4.7	13.0	21.5	11.5
0.9565	1457	453	1459	1461	-2.4	-2.8	-2.7	5.2	13.4	6.9
1.0000	1485	441	-	-	0.0	0.0	0.0	0.0	0.0	0.0

Table 6 continued

$x_1$	$u$ (m·s <sup>-1</sup> )	$\kappa_S$ (TPa <sup>-1</sup> )	$u_{FLT}$ (m·s <sup>-1</sup> )	$u_{CFT}$ (m·s <sup>-1</sup> )	$\kappa_S^E$ (Exp) (TPa <sup>-1</sup> )	$\kappa_S^E$ (Redlich–Kister) (TPa <sup>-1</sup> )	$\kappa_S^E$ (Hwang) (TPa <sup>-1</sup> )	$u^E$ (Exp) (m·s <sup>-1</sup> )	$u^E$ (Redlich–Kister) (m·s <sup>-1</sup> )	$u^E$ (Hwang) (m·s <sup>-1</sup> )
Benzylalcohol (1) + 1,1,2,2-tetrachloroethane (2)										
$T = 303.15$ K										
0.0000	1128	498	–	–	0.0	0.0	0.0	0.0	0.0	0.0
0.0505	1149	490	1154	1148	-10.1	-10.8	-11.0	9.2	9.5	9.3
0.1012	1171	482	1167	1169	-21.3	-20.0	-20.3	17.0	17.5	17.3
0.1524	1191	476	1195	1194	-28.1	-27.9	-28.1	23.9	24.3	24.2
0.1908	1204	473	1210	1208	-32.9	-32.9	-32.9	28.1	28.7	28.7
0.2388	1225	467	1232	1236	-38.7	-38.0	-37.8	34.5	33.4	33.5
0.3157	1253	461	1257	1261	-43.8	-43.8	-43.5	41.3	39.4	39.6
0.3551	1271	455	1276	1274	-45.3	-45.7	-45.4	43.8	41.8	42.0
0.4234	1294	452	1298	1296	-47.3	-47.3	-47.1	47.9	45.1	45.2
0.5163	1332	443	1336	1339	-45.6	-46.4	-46.4	49.7	47.7	47.6
0.6337	1376	436	1384	1387	-39.8	-40.8	-41.0	47.5	47.3	47.1
0.7292	1412	431	1415	1418	-32.9	-33.1	-33.3	41.3	43.3	43.1
0.7980	1438	428	1446	1444	-26.4	-26.1	-26.1	34.4	37.5	37.5
0.8418	1455	426	1459	1461	-21.5	-21.0	-20.9	29.3	32.2	32.3
0.8972	1477	423	1486	1481	-14.2	-14.1	-13.9	22.0	23.5	23.7
0.9687	1505	420	1512	1516	-4.4	-4.5	-4.3	9.6	8.3	8.5
1.0000	1514	420	–	–	0.0	0.0	0.0	0.0	0.0	0.0
$T = 313.15$ K										
0.0000	1095	533	–	–	0.0	0.0	0.0	0.0	0.0	0.0
0.0505	1116	524	1123	1118	-6.0	-5.8	-5.9	8.0	7.7	7.4
0.1012	1136	517	1141	1143	-10.2	-10.7	-10.8	14.4	14.4	14.2
0.1524	1156	510	1159	1162	-14.4	-14.7	-14.8	20.2	20.4	20.3
0.1908	1173	504	1175	1176	-17.3	-17.2	-17.2	23.1	24.4	24.4

**Table 6** continued

$x_1$	$u$ (m·s <sup>-1</sup> )	$\kappa_S$ (TPa <sup>-1</sup> )	$u_{FLT}$ (m·s <sup>-1</sup> )	$u_{CFT}$ (m·s <sup>-1</sup> )	$\kappa_S^E$ (Exp) (TPa <sup>-1</sup> )	$\kappa_S^E$ (Redlich–Kister) (TPa <sup>-1</sup> )	$\kappa_S^E$ (Hwang) (TPa <sup>-1</sup> )	$u^E$ (Exp) (m·s <sup>-1</sup> )	$u^E$ (Redlich–Kister) (m·s <sup>-1</sup> )	$u^E$ (Hwang) (m·s <sup>-1</sup> )
0.2388	1190	499	1204	1195	-20.0	-19.8	-19.7	28.7	28.9	28.9
0.3157	1219	491	1224	1226	-23.0	-22.6	-22.6	34.4	34.8	34.9
0.3551	1237	485	1236	1238	-24.3	-23.6	-23.5	37.6	37.2	37.4
0.4234	1262	479	1267	1270	-25.0	-24.5	-24.5	41.3	40.6	40.7
0.5163	1298	471	1305	1298	-24.9	-24.5	-24.5	43.8	43.2	43.2
0.6337	1345	461	1349	1351	-22.4	-22.5	-22.6	43.1	42.8	42.6
0.7292	1382	454	1391	1394	-19.1	-19.2	-19.3	38.5	38.8	38.6
0.7980	1412	448	1416	1415	-15.3	-15.9	-15.9	32.7	33.2	33.2
0.8418	1429	445	1434	1437	-12.7	-13.3	-13.2	28.6	28.4	28.5
0.8972	1451	442	1456	1454	-9.0	-9.3	-9.3	21.0	20.5	20.7
0.9687	1474	441	1482	1485	-3.4	-3.2	-3.1	7.0	7.1	7.3
1.0000	1485	441	-	-	0.0	0.0	0.0	0.0	0.0	0.0
Benzylalcohol (1) + trichloroethylene (2)										
$T = 303.15$ K										
0.0000	1015	671	-	-	0.0	0.0	0.0	0.0	0.0	0.0
0.0537	1045	644	1052	1055	-20.3	-18.8	-19.3	15.9	14.4	14.3
0.1241	1079	618	1083	1082	-35.3	-37.4	-37.9	29.3	30.7	30.6
0.1807	1108	596	1114	1109	-45.9	-48.2	-48.3	39.9	41.7	41.7
0.2351	1141	572	1146	1152	-54.6	-55.5	-55.3	49.2	50.6	50.6
0.3066	1172	555	1176	1176	-59.8	-61.3	-60.9	57.9	59.9	60.0
0.3749	1209	534	1213	1214	-64.5	-63.6	-63.1	65.7	66.2	66.3
0.4378	1239	519	1243	1245	-63.9	-63.3	-63.0	69.2	69.8	69.9
0.5483	1293	494	1295	1302	-60.2	-58.5	-58.7	71.6	71.2	71.1
0.6075	1322	482	1326	1328	-55.9	-54.2	-54.6	70.2	69.2	69.1
0.6796	1358	468	1362	1366	-47.6	-47.5	-48.0	65.2	64.0	63.9

Table 6 continued

$x_1$	$u$ ( $\text{m}\cdot\text{s}^{-1}$ )	$\kappa_S$ ( $\text{TPa}^{-1}$ )	$u_{\text{FLT}}$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u_{\text{CFT}}$ ( $\text{m}\cdot\text{s}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Exp})$ ( $\text{TPa}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Redlich-Kister})$ ( $\text{TPa}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Hwang})$ ( $\text{TPa}^{-1}$ )	$u^{\text{E}}(\text{Exp})$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u^{\text{E}}(\text{Redlich-Kister})$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u^{\text{E}}(\text{Hwang})$ ( $\text{m}\cdot\text{s}^{-1}$ )
0.7393	1389	457	1396	1397	-41.7	-40.9	-41.2	58.8	57.4	57.3
0.7857	1410	450	1419	1420	-34.5	-35.2	-35.2	52.3	50.7	50.7
0.8498	1449	436	1454	1458	-26.6	-26.2	-25.9	40.6	39.0	39.1
0.9004	1473	429	1486	1484	-18.3	-18.3	-17.7	27.7	27.8	27.9
0.9570	1494	425	1498	1495	-8.1	-8.4	-7.9	12.1	13.0	13.1
1.0000	1514	420	-	-	0.0	0.0	0.0	0.0	0.0	0.0
$T = 313.15 \text{ K}$										
0.0000	982	725	-	-	0.0	0.0	0.0	0.0	0.0	0.0
0.0537	1018	686	1015	1021	-12.7	-11.6	-12.0	12.2	12.6	12.4
0.1241	1051	658	1058	1054	-22.8	-23.8	-24.1	26.4	26.3	26.1
0.1807	1078	637	1084	1087	-29.3	-31.2	-31.3	35.7	35.2	35.1
0.2351	1105	617	1109	1107	-35.5	-36.6	-36.5	43.0	42.3	42.3
0.3066	1140	593	1148	1152	-41.0	-41.3	-41.0	49.6	49.7	49.8
0.3749	1174	572	1177	1184	-42.6	-43.5	-43.2	54.7	54.8	54.9
0.4378	1207	552	1213	1209	-43.6	-43.8	-43.6	59.4	57.9	58.0
0.5483	1262	524	1265	1268	-41.6	-40.9	-41.0	60.8	59.8	59.7
0.6075	1290	511	1294	1295	-38.8	-37.8	-38.1	59.7	58.8	58.7
0.6796	1328	494	1325	1328	-34.0	-32.8	-33.1	55.3	55.5	55.3
0.7393	1357	483	1359	1361	-28.7	-27.8	-28.0	49.6	50.7	50.6
0.7857	1379	475	1384	1385	-24.0	-23.5	-23.6	43.3	45.5	45.4
0.8498	1413	462	1417	1415	-17.5	-17.0	-16.8	35.8	35.9	36.0
0.9004	1439	453	1441	1443	-11.3	-11.5	-11.2	24.5	26.1	26.3
0.9570	1466	445	1465	1471	-4.7	-5.1	-4.8	13.5	12.5	12.0
1.0000	1485	441	-	-	0.0	0.0	0.0	0.0	0.0	0.0

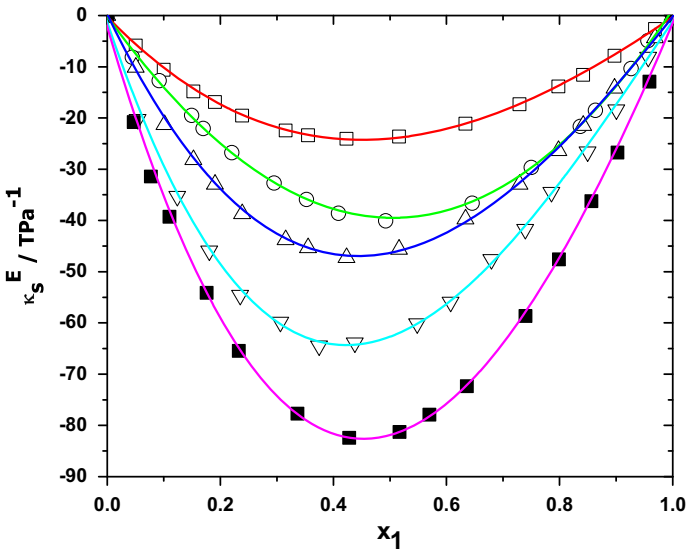


**Table 6** continued

$x_1$	$u$ ( $\text{m}\cdot\text{s}^{-1}$ )	$\kappa_S$ ( $\text{TPa}^{-1}$ )	$u_{\text{FLT}}$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u_{\text{CFT}}$ ( $\text{m}\cdot\text{s}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Exp})$ ( $\text{TPa}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Redlich-Kister})$ ( $\text{TPa}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Hwang})$ ( $\text{TPa}^{-1}$ )	$u^{\text{E}}(\text{Exp})$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u^{\text{E}}(\text{Redlich-Kister})$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u^{\text{E}}(\text{Hwang})$ ( $\text{m}\cdot\text{s}^{-1}$ )
Benzylalcohol (1) + tetrachloroethylene (2)										
$T = 303.15 \text{ K}$										
0.0000	1028	589	–	–	0.0	0.0	0.0	0.0	0.0	0.0
0.0473	1055	569	1065	1056	–20.8	–19.9	–20.3	17.2	17.3	16.8
0.0772	1071	558	1083	1085	–31.4	–30.6	–31.1	27.4	27.1	26.6
0.1102	1086	549	1097	1094	–39.3	–40.9	–41.3	36.9	37.0	36.6
0.1759	1118	531	1125	1123	–54.2	–57.2	–57.3	53.0	54.1	54.0
0.2330	1150	513	1154	1161	–65.5	–67.3	–67.2	66.0	66.4	66.6
0.3365	1199	492	1204	1208	–77.7	–77.9	–77.6	84.8	83.6	84.1
0.4282	1245	474	1250	1249	–82.5	–80.8	–80.6	96.0	93.8	94.1
0.5173	1287	460	1296	1299	–81.3	–79.0	–79.1	101.4	99.0	99.0
0.5702	1314	452	1315	1321	–77.9	–76.1	–76.3	102.0	99.8	99.5
0.6363	1345	445	1351	1356	–72.4	–70.6	–71.1	98.5	97.8	97.4
0.7377	1396	433	1399	1403	–58.7	–58.5	–58.8	85.1	87.6	87.3
0.7991	1423	429	1427	1431	–47.6	–48.8	–48.8	72.9	76.1	76.1
0.8562	1456	422	1459	1464	–36.2	–37.8	–37.5	59.1	61.1	61.4
0.9026	1473	422	1481	1483	–26.8	–27.3	–26.9	44.7	45.4	45.9
0.9591	1499	420	1507	1505	–12.9	–12.5	–12.1	22.5	21.3	21.7
1.0000	1514	420	–	–	0.0	0.0	0.0	0.0	0.0	0.0
$T = 313.15 \text{ K}$										
0.0000	996	634	–	–	0.0	0.0	0.0	0.0	0.0	0.0
0.0473	1018	617	1024	1027	–10.1	–11.5	–11.7	9.8	10.1	9.7
0.0772	1037	601	1042	1045	–18.0	–18.0	–18.2	15.8	15.8	15.4
0.1102	1052	591	1056	1057	–26.5	–24.4	–24.6	21.2	21.7	21.3
0.1759	1084	571	1087	1086	–36.6	–35.2	–35.2	32.4	32.2	32.1

Table 6 continued

$x_1$	$u$ ( $\text{m}\cdot\text{s}^{-1}$ )	$\kappa_S$ ( $\text{TPa}^{-1}$ )	$u_{\text{FLT}}$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u_{\text{GFT}}$ ( $\text{m}\cdot\text{s}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Exp})$ ( $\text{TPa}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Redlich-Kister})$ ( $\text{TPa}^{-1}$ )	$\kappa_S^{\text{E}}(\text{Hwang})$ ( $\text{TPa}^{-1}$ )	$u^{\text{E}}(\text{Exp})$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u^{\text{E}}(\text{Redlich-Kister})$ ( $\text{m}\cdot\text{s}^{-1}$ )	$u^{\text{E}}(\text{Hwang})$ ( $\text{m}\cdot\text{s}^{-1}$ )
0.2330	1112	554	1117	1119	-43.5	-42.4	-42.4	40.4	39.9	40.1
0.3365	1164	527	1171	1184	-52.6	-51.1	-51.1	53.3	51.2	51.7
0.4282	1209	507	1214	1215	-55.3	-54.6	-54.5	61.0	58.4	58.7
0.5173	1252	491	1254	1258	-54.3	-54.5	-54.6	63.6	62.5	62.5
0.5702	1275	485	1278	1284	-53.0	-53.0	-53.1	64.8	63.5	63.2
0.6363	1313	471	1318	1321	-48.7	-49.5	-49.7	62.8	62.8	62.4
0.7377	1360	460	1365	1367	-39.3	-41.0	-41.1	54.7	56.8	56.6
0.7991	1390	454	1398	1396	-32.4	-34.0	-33.9	47.1	49.6	49.6
0.8562	1420	447	1425	1424	-24.9	-26.0	-26.0	37.5	40.0	40.2
0.9026	1444	443	1449	1446	-17.6	-18.6	-18.5	28.3	29.8	30.2
0.9591	1469	441	1474	1478	-9.5	-8.3	-8.2	15.6	14.0	14.4
1.0000	1485	441	-	-	0.0	0.0	0.0	0.0	0.0	0.0



**Fig. 6** Variation of excess isentropic compressibility ( $\kappa_S^E$ ) of the binary liquid mixtures of benzylalcohol (1) with 1,2-dichloroethane (*square*), 1,1,1-trichloroethane (*circle*), 1,1,2-tetrachloroethane (*triangle*), trichloroethylene (*inverted triangle*) and tetrachloroethylene (*filled square*) at 303.15 K

$$\kappa_S^E = \kappa_S - \kappa_S^{id} \tag{4}$$

$$\kappa_S = \frac{1}{u^2 \rho} \tag{5}$$

$$M_m = \sum x_i M_i \tag{6}$$

$$\kappa_S^{id} = \phi_1 \kappa_{S1} + \phi_2 \kappa_{S2} + T \left[ \frac{\phi_1 V_1 \alpha_{p1}^2}{C_{p1}} + \frac{\phi_2 V_2 \alpha_{p2}^2}{C_{p2}} - \frac{V_m^{id} \alpha_{pm}^{id2}}{C_{pm}^{id}} \right] \tag{7}$$

$$\phi_i = \frac{x_i V_i^o}{\sum x_i V_i^o} \tag{8}$$

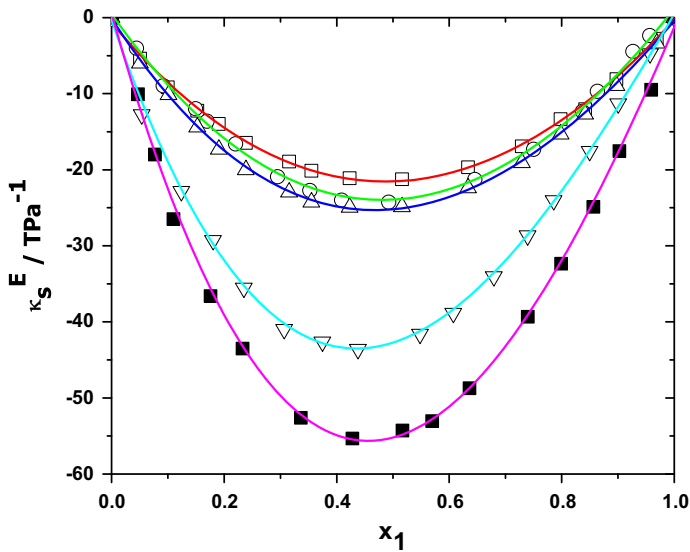
$$V_m^{id} = \sum x_i V_i \tag{9}$$

$$\alpha_p^{id} = \sum \phi_i \alpha_{pi} \tag{10}$$

$$c_p^{id} = \sum x_i C_{pi} \tag{11}$$

Here,  $C_{pi}$  and  $\alpha_i$  are the molar heat capacity and the thermal expansion coefficient of the  $i$ th component respectively. The value of  $C_{pi}$  and  $\alpha_i$  were obtained and evaluated from the literature [4, 19, 20].

The excess speed of sound ( $u^E$ ) data of the binary mixtures under the investigation [31] were calculated from the following equations, and are given in Table 6.



**Fig. 7** Variation of excess isentropic compressibility ( $\kappa_S^E$ ) of the binary liquid mixtures of benzylalcohol (1) with 1,2-dichloroethane (*square*), 1,1,1-trichloroethane (*circle*), 1,1,2,2-tetrachloroethane (*triangle*), trichloroethylene (*inverted triangle*) and tetrachloroethylene (*filled square*) at 313.15 K

$$u^E = u - u^{\text{id}} \quad (12)$$

$$u^{\text{id}} = \frac{1}{\rho^{\text{id}}} \left\{ \frac{1}{M_m} \left[ \sum \frac{x_i m_i}{(\rho_i u_i)^2} \right] \right\}^{-1/2} \quad (13)$$

$$\rho^{\text{id}} = \sum \phi_i \rho_i \quad (14)$$

An examination of  $\kappa_S^E$  data in Table 6, for the mixtures of benzylalcohol with chloroalkanes and chloroalkenes, shows they are negative over the entire composition range at 303.15 and 313.15 K. This may be attributed to the relative strength of effects which influence the free space between component molecules. The negative  $\kappa_S^E$  values arise from changes of free volume in the real mixture and presence of  $\pi$ -electrons in benzylalcohol resulting in the formation of weak intermolecular complexes leading to negative excess isentropic compressibility [32, 33].

Perusal of  $\kappa_S^E$  data in Table 6 suggests that the factors that are responsible for negative  $\kappa_S^E$  are dominate in all the binary mixtures.

The excess volume data for mixtures of chloroalkanes and chloroalkenes follows the order:

1,2-dichloroethane < 1,1,1-trichloroethane < 1,1,2,2-tetrachloroethane < trichloroethylene < tetrachloroethylene

This order suggests that as the number of chlorine atoms in alkane and alkene molecules increase the weak dipolar interactions between unlike molecules, which leads to decreases in free space, thereby an increase in the speed of sound and negative  $\kappa_S^E$  values are observed [34].

The effect of increasing the temperature appears to increase the magnitude of excess volume, suggesting of the existence weak dipolar interactions and complex formation. Further, as the temperature increases,  $\kappa_S^E$  becomes more negative, which may be due to the thermal dissociation of hetero-aggregates in liquid mixtures and more interstitial accommodation of the components [35].

Experimental ultrasonic sound velocities were analyzed in terms of collision factor theory (CFT) [36], free length theory (FLT) [37, 38] and these are also included in Table 6 along with experimental ultrasonic sound velocities. The pure component data namely, the molar volume ( $V_m$ ), molar volume at absolute zero ( $V_0$ ), molar available volume ( $V_a$ ), free length ( $L_f$ ), surface area ( $Y$ ), collision factor ( $S$ ), average molecular radius ( $r_m$ ), actual volume of molecules per mole ( $B$ ) and molecular sound velocity ( $R$ ) that were used in the theoretical calculations were collected from the literature [39]. The methods and details of calculation were discussed earlier [33]; these values are given in Table 6.

**Table 7** Standard deviation  $\sigma$  ( $\kappa_S^E$  or  $u^E$ ) and values of constants from the Redlich–Kister equation

Temperature	Function	$a_0$ [TPa <sup>-1</sup> (m·s <sup>-1</sup> )]	$a_1$ [TPa <sup>-1</sup> (m·s <sup>-1</sup> )]	$a_2$ [TPa <sup>-1</sup> (m·s <sup>-1</sup> )]	$\sigma$ ( $\kappa_S^E/u^E$ )
Benzylalcohol (1) + 1,2-dichloroethane (2)					
303.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-84.461	-6.115	-49.741	2.157
313.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-71.196	-17.464	-65.026	2.191
303.15 K	$u^E$ (m·s <sup>-1</sup> )	76.658	39.740	50.512	2.222
313.15 K	$u^E$ (m·s <sup>-1</sup> )	36.040	5.430	14.214	0.990
Benzylalcohol (1) + 1,1,1-trichloroethane (2)					
303.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-158.194	10.365	4.924	1.124
313.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-99.400	14.571	22.594	0.769
303.15 K	$u^E$ (m·s <sup>-1</sup> )	255.913	42.664	26.366	0.964
313.15 K	$u^E$ (m·s <sup>-1</sup> )	189.793	1.676	-30.911	1.266
Benzylalcohol (1) + 1,1,2,2-tetrachloroethane (2)					
303.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-187.126	42.300	0.588	0.623
313.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-98.586	10.401	-17.393	0.453
303.15 K	$u^E$ (m·s <sup>-1</sup> )	189.450	39.548	54.604	1.996
313.15 K	$u^E$ (m·s <sup>-1</sup> )	171.599	40.054	30.010	0.573
Benzylalcohol (1) + trichloroethylene (2)					
303.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-244.664	92.971	-52.803	1.410
313.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-170.517	58.394	-7.541	1.023
303.15 K	$u^E$ (m·s <sup>-1</sup> )	285.625	17.063	17.133	1.424
313.15 K	$u^E$ (m·s <sup>-1</sup> )	238.234	29.627	45.634	1.093
Benzylalcohol (1) + tetrachloroethylene (2)					
303.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-318.757	69.047	-73.792	1.712
313.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-219.313	23.895	-18.431	1.340
303.15 K	$u^E$ (m·s <sup>-1</sup> )	393.632	85.117	83.106	1.825
313.15 K	$u^E$ (m·s <sup>-1</sup> )	247.973	72.354	49.784	1.712

A comparison between experimental sound velocities and theoretical values suggest that the model proposed by Schaaff's CFT gives better estimation of sound velocity data. The methods of calculation of these theories were described earlier (Tables 7, 8). The merits of these theories were compared in terms of relative root mean deviation by using the following formula [40]:

$$RMSD = \left[ \frac{1}{n} \sum_{i=1}^n \left( \frac{y_{\text{exp}} - y_{\text{pred}}}{y_{\text{exp}}} \right)^2 \right]^{1/2} \quad (15)$$

The *RMSDs* for all the binary systems values, given in Table 9, show that Schaaff's CFT model gives a better estimation in speed of sound for the binary mixtures under the investigation.

The experimental  $V^E$ ,  $u^E$  and  $\kappa_S^E$  data were fitted to the Redlich–Kister Eq. 2 and Hwang Eq. 3 type polynomial equations and the adjustable parameters of the function and are

**Table 8** Standard deviation  $\sigma$  ( $\kappa_S^E$  or  $u^E$ ) and values of constants from the Hwang Eq. 3

Temperature	Function	$b_0$ TPa <sup>-1</sup> (m·s <sup>-1</sup> )	$b_1$	$b_2$	$\sigma$ ( $\kappa_S^E/u^E$ )
Benzylalcohol (1) + 1,2-dichloroethane (2)					
303.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-67.88	-73.60	-59.04	2.138
313.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-49.52	-107.49	-65.91	1.966
303.15 K	$u^E$ (m·s <sup>-1</sup> )	59.82	114.66	20.04	2.245
313.15 K	$u^E$ (m·s <sup>-1</sup> )	31.30	25.42	12.49	1.498
Benzylalcohol (1) + 1,1,1-trichloroethane (2)					
303.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-159.84	18.90	-5.77	1.110
313.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-106.93	47.47	12.78	0.748
303.15 K	$u^E$ (m·s <sup>-1</sup> )	247.12	85.95	-15.64	1.092
313.15 K	$u^E$ (m·s <sup>-1</sup> )	200.10	-39.22	-43.21	1.267
Benzylalcohol (1) + 1,1,2,2-tetrachloroethane (2)					
303.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-187.32	51.14	-49.57	0.680
313.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-92.79	-10.81	-35.57	0.475
303.15 K	$u^E$ (m·s <sup>-1</sup> )	171.25	119.89	25.72	1.947
313.15 K	$u^E$ (m·s <sup>-1</sup> )	161.60	87.70	-7.67	0.566
Benzylalcohol (1) + trichloroethylene (2)					
303.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-227.06	40.28	-181.08	1.406
313.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-168.00	59.46	-79.57	0.929
303.15 K	$u^E$ (m·s <sup>-1</sup> )	279.91	43.16	2.53	1.471
313.15 K	$u^E$ (m·s <sup>-1</sup> )	270.41	81.16	40.53	1.161
Benzylalcohol (1) + tetrachloroethylene (2)					
303.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-294.16	-16.19	-180.59	1.667
313.15 K	$\kappa_S^E$ (TPa <sup>-1</sup> )	-213.17	3.87	-53.02	1.371
303.15 K	$u^E$ (m·s <sup>-1</sup> )	365.93	212.14	9.48	1.871
313.15 K	$u^E$ (m·s <sup>-1</sup> )	231.38	152.51	-19.76	1.692

**Table 9** RMSD of speed of sound ( $u$ ) with theoretical models of benzylalcohol with chloroalkanes and chloroalkenes at  $T = 303.15$  K and  $313.15$  K

RMSD	$u$ (m·s <sup>-1</sup> ) 303.15 K	$u$ (m·s <sup>-1</sup> ) 313.15 K
Benzylalcohol (1) + 1,2-dichloroethane (2)		
CFT	0.0219	0.0219
FLT	0.0922	0.0172
Benzylalcohol (1) + 1,1,1-trichloroethane (2)		
CFT	0.0067	0.0066
FLT	0.0078	0.0080
Benzylalcohol (1) + 1,1,2,2-tetrachloroethane (2)		
CFT	0.0043	0.0050
FLT	0.0048	0.0048
Benzylalcohol (1) + trichloroethylene (2)		
CFT	0.0046	0.0038
FLT	0.0059	0.0049
Benzylalcohol (1) + tetrachloroethylene (2)		
CFT	0.0060	0.0041
FLT	0.0070	0.0069

determined using the least-squares method. The corresponding standard deviations  $\sigma(Y^E)$  have been computed using the relation:

$$\sigma(Y^E) = \left[ \frac{\sum (Y_{\text{exp}}^E - Y_{\text{cal}}^E)^2}{m - n} \right]^{1/2} \quad (16)$$

where  $m$  is the total number of experimental points and  $n$  is the number of coefficients; the standard deviations for all the binary mixtures are presented in Tables 4, 5, 7 and 8.

## 4 Conclusions

In the present work excess volume data of binary mixtures of benzylalcohol with 1,2-dichloroethane, 1,1,1-trichloroethane and 1,1,2,2-tetrachloroethane are positive and trichloroethylene and tetrachloroethylene are negative over the entire composition range at 298.15–313.15 K. Further, negative  $\kappa_S^E$  values in all the binary mixtures arise due to changes of free volume in the real mixtures and presence of  $\pi$ -electrons in benzylalcohol and result in the formation of strong intermolecular complexes leading to negative excess isentropic compressibility.

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