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Ion Imprinted Sodium Alginate Hydrogel Beads Enhanced with Carboxymethyl Cellulose and β -Cyclodextrin to Improve Adsorption for Cu²⁺

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Abstract

To achieve efficient adsorption and recycling of Cu^{2+} in wastewater, using Cu^{2+} as template ion, glutaraldehyde as crosslinker, three sodium alginate hydrogel beads including SA, SAC, and SAB beads were prepared by imprinting sol–gel method using sodium alginate (SA) with carboxymethyl cellulose (CMC) and β -cyclodextrin (β -CD) as different precursors, respectively. Scanning electron microscopy and Fourier transform infrared spectroscopy were used to characterize and analyze morphology and composition change of the hydrogel beads, respectively. When the mass ratio of SA to CMC or SA to β -CD reach 1:1, the SAC beads or SAB beads are nearly homogeneous sphere. Then the effects of pH, adsorption time, initial concentration of Cu^{2+} , adsorbent dosage, and coexisting ions on the adsorption efficiency of three hydrogel beads increased the toughness of the beads and improved the adsorption capacity of Cu^{2+} . Compared to the saturated adsorption capacity 510 mg/g of Cu^{2+} on SA, the saturated adsorption capacity of Cu^{2+} on SAB and SAC reached 817 mg/g and 822 mg/g, respectively. And their adsorption efficiency for Cu^{2+} are over 95% at 25 °C with pH of 7, contact time within 350 min, adsorbent dosage of 4 mg/50 mL, and initial concentration of 5 mg/L. Thus, SAC and SAB beads could be used as adsorption material for detecting and removing Cu^{2+} from wastewater.

Keywords Sodium alginate · Carboxymethyl cellulose · β -Cyclodextrin · Copper ions · Ion imprinted hydrogel beads · Specific adsorption

Introduction

With the development of modern industry, wastewater polluted by heavy metals from the manufacture of pesticides, fertilizers and metals has become an important field of environmental treatment [1-3]. The non-degradability of heavy metals in soil and water makes them accumulate in organisms, which leads to organism damage and finally

Lianwu Xie xielianwu@csuft.edu.cn endangers human life and health [4]. Therefore, the efficient treatment of heavy metals has always been the key point of national environmental protection [5]. China has established a series of discharge standards for heavy metals in aquatic ecosystem. For example, the comprehensive sewage discharge standard GB 8978-1996 stipulates that the maximum acceptable emission concentration of Cu²⁺ is 0.5 mg/L. Copper is an essential trace element for human body. However, excess accumulation of Cu²⁺ in human body through food chain will cause damage to liver, heart, lung, and brain, and threaten the safety of human life. Various ecological problems caused by copper pollution have also received great attention from relevant environmental protection departments. Therefore, effective removal of copper from polluted water bodies has always been an important topic for scientific researchers and governors.

The treatment methods for heavy metals including Cu²⁺ in wastewater include: chemical method [6], adsorption [7, 8], electro-dialysis [9, 10], ion exchange method [7, 11],

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photocatalysis methods [12, 13]. Various chemical method such as chemical precipitation are being used for the treatment of wastewater containing Cu²⁺, but still are limited in their efficiencies, residues, cost, and versatility [14]. Electrodialysis method has been recognized as an efficient treatment for the wastewater, but it is unsuitable for distressed area lack of electric power [15]. The ion-exchanger with good ion exchange capacity, chemical stability, and thermal stability [16], would inevitably bring another ion into wastewater after treatment. Photocatalysis has been an interesting issue for the degradation of organic contaminants and heavy metals for quite a few years. However, many photocatalysis materials hold the disadvantage of photo-corrosion which decline the photoactivity and stability [17]. With the adsorption method's advantages such as economical, simple and easy to handle, and wide scope of application [18], the research and development of green adsorption materials with good performance and specific selectivity is becoming an important trend of controlling pollution and recycling of heavy metals [19-22].

The ion-imprinted polymer is regarded as one type of green adsorption materials with specific selectivity [23]. Ion imprinting technology is the technique that creating threedimensional cavity structures in a polymer matrix, i.e., ion imprinting polymers by the copolymerization of functional monomers and cross-linkers in the presence of target ion as template ion based on coordination or electrostatic interactions. After removal of the template ion with acidic reagent, recognition cavities complementary to the template ion were formed in the highly cross-linked polymer matrix [24]. Except for inorganic reagent such as 3-aminopropyltriethoxysilane, some natural raw materials such as chitosan and sodium alginate were used as the functional monomer to prepare ion-imprinted polymer. When using sodium alginate as functional monomer, ion-imprinted hydrogel beads could be easily obtained owing to its good film forming property [25]. The hydrogel beads have the advantages of degradable, good biocompatibility, high load, high specific surface area, convenient operation and transportation, etc. However, ionimprinted sodium alginate hydrogel beads are rarely studied.

Sodium alginate (SA) is a natural macromolecular polysaccharide extracted from brown algae and composed of α -L-glucuronic acid and β -D-mannouronic acid. It is watersoluble and contains a large number of free carboxyl groups that can interact with heavy metal ions. Thus, it can be used as an excellent adsorption material for heavy metals [26, 27]. And β -cyclodextrin (β -CD) with a circular structure formed by the α -1,4-glycosidic bond connecting seven D-glucopyranose basic units, contains a cavity structure that can encapsulate ions and organics, etc., and its molecular surface contains a large number of hydroxyl groups that can chelate with heavy metal ions to form complexes [28–30]. Carboxymethyl cellulose (CMC) is a renewable natural cellulose ether compound, which contains abundant hydroxyl and carboxyl groups and can form hydrogels through physical or chemical methods [23, 31].

In this paper, to achieve efficient adsorption of Cu^{2+} from wastewater, using Cu^{2+} as template ion, glutaraldehyde as crosslinker, three kinds of sodium alginate hydrogel beads were prepared by imprinting sol–gel method using SA with CMC and β -CD as different precursors, respectively. Two of them were enhanced with CMC and β -CD to improve adsorption for Cu^{2+} . Scanning electron microscopy (SEM) and Fourier transform infrared spectroscopy (FT-IR) were used to characterize and analyze the sodium alginate hydrogel beads, and the influence of different factors on adsorption performance of the hydrogel beads was also investigated. Some adsorption experiments and different adsorption kinetics models were used to analyze the adsorption mechanism of Cu^{2+} on the hydrogel beads.

Materials and Methods

Chemicals and Apparatus

Sodium alginate (Chemically Pure, C.P.), carboxymethyl cellulose (C.P.), β -cyclodextrin (C.P.), glutaraldehyde (25%, Biochemical Reagent, B.R.), hydrochloric acid (38%, A.R.), and sodium hydroxide (A.R.) were all purchased from Sinopharm Chemical Reagents Co., Ltd. Anhydrous copper chloride (99.99%) was purchased from Shanghai Aladdin Biochemical Technology Co., Ltd. Triple distilled water was used in the experiment.

The instruments and equipment used in this paper mainly included QUANTA FEG 250 field emission environmental scanning electron microscope (FEI Co., OR, USA), Nicolet iS5 Fourier transform infrared spectrometer (Thermo Fisher Scientific, MA, USA), Optima 8000 inductive coupled plasma (ICP) emission spectrometer (Perkin-Elmer, MA, USA), SZ-97 automatic triple water distiller (Yarong Biochemical Instrument Co., Shanghai, China), PXSJ-226 pH meter (INESA Instrument Co., Shanghai, China), AL204 electronic analytical balance (Mettler Toledo Instrument Co., Zurich, Switzerland), TL-F6 micro injection pump (Tongli Weina Co., Shenzhen, China), and HYG-A shaker (Taicang Equipment Co., Jiangsu, China).

Preparation of Sodium Alginate Hydrogel Beads

The structural stability and the adsorption effect of sodium alginate hydrogel beads on Cu^{2+} were improved by adding different precursors. The effects of concentrations of precursors and concentration of template Cu^{2+} on the pellet formation of hydrogel beads were investigated in the preliminary stage, and Cu^{2+} pre-adsorption experiments were conducted to obtain the optimal conditions for the preparation of sodium alginate hydrogel beads by imprinting sol-gel method.

Preparation of SA Hydrogel Beads

The SA hydrogel beads were synthesized by the following procedure. SA (2.0 g) was added into 200 mL distilled water with a magnetic stirrer for 6 h at 25 °C. Then, 4 mL glutaraldehyde solution (as crosslinker) in $H_2O(25\%, w/w)$ was added into above solution and reacted at 25 °C for 12 h under sealing and stirring to prepare sol solution. The prepared sol solution was dropped into 200 mL 0.2 mol/L Cu²⁺ aqueous solution by a micro-injection pump at a constant rate to obtain hydrogel beads, and the hydrogel beads were stabilized by Cu^{2+} ion imprinting for 10 h. After washing the hydrogel beads with distilled water for 5 times (50 mL each time), SA hydrogel beads (abbr. as SA beads) were obtained by eluting Cu^{2+} in the hydrogel beads with 100 mL 0.5 mol/L HCl for 5 times and washing with 50 mL distilled water for 5 times. The proposed reaction was shown in Scheme 1a.

Preparation of SAC Hydrogel Beads

The mass ratio of SA to CMC is an important factor in the preparation of SA + CMC hydrogel beads (abbr. as SAC beads). At preliminary experiment, we investigate the effect of mass ratio of SA to CMC (from 4:1 to 1:4) on morphology of hydrogel beads. The hydrogel beads are nearly homogeneous sphere once the mass ratio of SA to CMC reach 1:1. Then, the SAC hydrogel beads were synthesized by the following procedure. SA (3.0 g) and CMC (3.0 g) were added into 200 mL distilled water with a magnetic stirrer for 6 h at 25 °C. After the same subsequent treatment as the "Preparation of SA Hydrogel Beads" section, the SAC beads were obtained. The proposed reaction was shown in Scheme 1b.

Preparation of SAB Hydrogel Beads

As "Preparation of SAC Hydrogel Beads" section, when the mass ratio of SA to β -CD reach 1:1, the SA + β -CD hydrogel beads (abbr. as SAB beads) are nearly homogeneous sphere. Then, the SAB hydrogel beads were synthesized by the following procedure. SA (3.0 g) and β -CD (3.0 g) were added into 200 mL distilled water with a magnetic stirrer for 6 h at 25 °C. After the same subsequent treatment as the "Preparation of SA Hydrogel Beads" section, the SAB beads were obtained. The proposed reaction was shown in Scheme 1c.

Structure Characterization for Hydrogel Beads

All sodium alginate hydrogel beads were freeze-dried (- 80 °C) before structure characterization in order to avoid damaging the structure by drying in normal oven. SEM was used to characterize the morphology of the hydrogel beads, and FT-IR was used to characterize the composition change of the hydrogel beads.

Adsorption Experiment

Adsorption experiment was conducted to investigate the effects of different experimental parameters on the adsorption of Cu^{2+} on the hydrogel beads. A fixed amount of the sodium alginate hydrogel beads was added into a series of Cu^{2+} solution with different concentration, respectively. Then the solution was oscillated for adsorbing 12 h at 120 r/min in a shaker under different temperature. After that, the concentration of Cu^{2+} in the solution reaching equilibrium adsorption was determined by the inductive coupled plasma emission spectrometer (ICP). All the adsorption experiments were repeated for three times and the mean values were recorded. The adsorption capacity and adsorption efficiency of the sodium alginate hydrogel beads were calculated according to Eqs. (1) and (2), respectively.

$$q = \frac{(C_0 - C_1) \times V}{m} \tag{1}$$

where q is the adsorption capacity (mg/g) of Cu^{2+} on hydrogel beads, C_0 is the initial concentration of Cu^{2+} (mg/L) in the solution, C_1 is the concentration of Cu^{2+} (mg/L) after adsorption, V is the volume of Cu^{2+} solution (L), and m is the weight of the dry hydrogel beads (g).

$$Q = \frac{C_0 - C_1}{C_0} \times 100\%$$
(2)

where Q is the adsorption efficiency (%), C_0 is the initial concentration of Cu²⁺ (mg/L) in the solution, C_1 is the concentration of Cu²⁺ (mg/L) after adsorption.

Effect of pH on Adsorption

The dry hydrogel beads (4 mg) were added into 50 mL Cu^{2+} solution (5 mg/L) with different pH ranging 1–8. In a shaker, the adsorption was carried out under 25 °C at 120 r/min for 10 h to study the effect of pH on the adsorption.

Effect of Hydrogel Beads Dosage on Adsorption

The dry hydrogel beads with different weight (0.4–10 mg) were added into 50 mL Cu^{2+} solution (5 mg/L) with pH



 $\label{eq:scheme1} Scheme 1 \ \ \ The proposed preparation reaction of SA (a), SAC (b), SAB (c) \ sodium \ alginate \ hydrogel \ beads$

7, respectively. In a shaker, the adsorption was carried out under 25 $^{\circ}$ C at 120 r/min for 10 h to study the effect of hydrogel beads dosage on the adsorption.

Effect of Initial Concentration on Adsorption

A series of Cu^{2+} solution with different concentration ranging 1 mg/L to 700 mg/L was prepared firstly. The dry hydrogel beads (4 mg) were added into above all Cu^{2+} solutions (50 mL for each one) after adjusting pH to 7, respectively. In a shaker, the adsorption was carried out under 25 °C at 120 r/min for 10 h to investigate the effect of initial concentration of Cu^{2+} on the adsorption.

Adsorption Kinetics Experiment

The dry hydrogel beads (40 mg) were added into a 50 mL Cu^{2+} solution (5 mg/L) with pH 7. In a shaker, the adsorption was carried out under 25 °C at 120 r/min. The concentration of Cu^{2+} in the adsorbing solution was measured at a certain time interval, and the adsorption effect of hydrogel beads along with different treatment time was investigated. The pseudo-first-order kinetic model and the pseudo-second-order kinetic model were used to fit the dynamic adsorption data to explore the adsorption mechanism.

The pseudo-first-order kinetic equation and the pseudosecond-order kinetic equation are shown as Eqs. (3) and (4), respectively.

$$ln(\mathbf{q}_{\mathrm{e}} - \mathbf{q}_{\mathrm{t}}) = ln\mathbf{q}_{\mathrm{e}} - \mathbf{k}_{\mathrm{1}}\mathbf{t}$$
(3)

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e}$$
(4)

where q_t is the adsorption capacity (mg/g) at time t, q_e is the saturated adsorption capacity at equilibrium (mg/g), t is the adsorption time (h), k_1 is the pseudo-first-order adsorption rate constant (1/h), k_2 is the pseudo-second-order adsorption rate constant [g/(mg/h)].

Adsorption Thermodynamic Experiment

For better understanding the interaction mechanism between hydrogel beads and Cu^{2+} after evaluating their adsorption capacity, both Langmuir model and Freundlich model were used to fit the experimental results. In general, the Langmuir adsorption isotherm equation is used to describe the adsorption process of monolayer adsorption. The Freundlich adsorption isotherm equation is commonly used to describe the multilayer adsorption process.

The Langmuir adsorption isotherm equation and the Freundlich adsorption isotherm equation are shown as Eqs. (5) and (6), respectively.

$$\frac{1}{q_e} = \frac{1}{K_L q_m C_e} + \frac{1}{q_m}$$
(5)

$$\ln q_e = m \ln C_e + \ln K_f \tag{6}$$

where q_e is the equilibrium adsorption amount of Cu²⁺ on hydrogel beads at adsorption equilibrium (mg/g), q_m is the saturation adsorption amount of Cu²⁺ on hydrogel beads (mg/g), C_e is the adsorption equilibrium concentration of Cu²⁺ (mg/L), K_L is the parameter of Langmuir isotherm equation, which is related to the strength of adsorption capacity, and its magnitude mainly depends on the nature of adsorbent, adsorbent mass and temperature; K_f is the adsorption equilibrium constant of Freundlich isotherm equation, which indicates the adsorption amount at *C* per unit concentration; m is the Freundlich characteristic adsorption parameter.

Effect of Coexisting lons on Adsorption

A mixed solution of Cu^{2+} and 15 coexisting ions $(A1^{3+}, Ag^+, Ba^{2+}, Ca^{2+}, Cd^{2+}, Co^{2+}, Cr^{3+}, Fe^{2+}, Fe^{3+}, Li^+, Mg^{2+}, Mn^{2+}, Ni^{2+}, Pb^{2+}$ and Zn²⁺) was prepared with the same concentration of 5 mg/L, and 50 mL mixed solution was taken to adjust pH to 7 before 4 mg dried hydrogel beads were added. In a shaker, the adsorption was carried out under 25 °C at 120 r/min for 10 h. After that, the concentration of Cu²⁺ and other coexisting ions in the adsorbing solution was measured by the ICP and the effect of coexisting ions on the adsorption of Cu²⁺ was analyzed.

The separation factors (β) were calculated according to Eq. (7).

$$\beta = \frac{Q(Cu2 +)}{Q(other ion)}$$
(7)

where $Q(Cu^{2+})$ is the adsorption efficiency of Cu^{2+} on hydrogel beads, and Q(other ions) is the adsorption efficiency of other coexisting ion on hydrogel beads.

Regeneration and Recycling

The dried sodium alginate hydrogel beads (4 mg) with adsorbed Cu^{2+} were added into 50 mL HCl solution (0.5 mol/L) for desorption for 5 h, then the beads were washed with 50 mL distilled water for 5 times. The desorbed hydrogel beads were placed into 50 mL Cu^{2+} aqueous solution (5 mg/L) again for another adsorption for 10 h, and the adsorption–desorption-adsorption process was repeated to investigate the reutilization of the hydrogel beads.

Results and Discussion

Structure Characteristics of Sodium Alginate Hydrogel Beads

SEM Morphological Characteristics

In fact, there is nearly no difference of the morphology between hydrogel beads in the presence of Cu²⁺ as ion template and hydrogel beads on the absent of Cu^{2+} (data not shown). Thus, we focused on difference of the morphology between SA hydrogel beads and SAC or SAB hydrogel beads. The SEM images of SA, SAC, and SAB sodium alginate hydrogel beads were shown in Fig. 1. Although the newly prepared sodium alginate hydrogel beads were basically spherical with diameter of 3-5 mm (Fig. 1g), the freeze-dried sodium alginate hydrogel beads were ellipsoid with particle size of 1.2-2.0 mm, and with layered and fish scale-like folds on the surface (Fig. 1a, c, e) as the reported by Ding et al. [32], indicating the existence of internal cavity. Figure 1b, d, and f showed that more fold structures appeared after adding CMC and β -CD than that of SA beads, leading to a significant increase in the specific surface area of the hydrogel beads, thus enhancing the adsorption capacity of Cu^{2+} by the SAC and SAB beads.

FT-IR Spectral Characteristics

The FT-IR spectra of SA, SAC and SAB hydrogel beads before and after adsorption were shown in Fig. 2. The absorption peaks at 3427 cm^{-1} , 3440 cm^{-1} and 3466 cm^{-1} were O–H stretching vibration peaks [33, 34]. At 3440 cm⁻¹, O-H of both sodium alginate and sodium carboxymethyl cellulose produced stretching vibration peak. The broad peak of 3466 cm⁻¹ was the stretching vibration peak generated by hydrogen bond between sodium alginate and hydroxyl group on cyclodextrin. The peaks of 1740 cm^{-1} and 1370 cm^{-1} were the characteristic absorption peaks of the symmetric and asymmetric stretching vibration of COO- of sodium alginate and the C=O superimposed on sodium carboxymethyl cellulose, respectively [35, 36]. The absorption peaks at 1370 cm⁻¹ and 1366 cm⁻¹ were related to the C–O stretching vibration and O-H bending vibration of sodium alginate and sodium carboxymethyl cellulose [37, 38]. The absorption peak of the C=O double bond at 1738 or 1740 cm^{-1} indicated that the crosslinking agent glutaraldehyde was successfully polymerized with sodium alginate. And the peak of 2904 cm⁻¹ was the C-H stretching vibration of methylene of sodium alginate [39], and the absorption peak of C-H stretching vibration at 2904 cm⁻¹ was weakened by the chelation of carboxylic acid group with Cu²⁺.

The absorption peaks' wavenumber of sodium alginate hydrogel beads did not change significantly before and after adsorption, but the intensity of absorption peaks increased or decreased slightly, which indicated that the main structure of sodium alginate hydrogel beads did not change before and after adsorption of Cu^{2+} , and perhaps treating Cu^{2+} by hydrogel beads existed not only physical adsorption but also chemical adsorption which is dominated by coordination reaction.

Evaluation on Adsorption Properties

Effect of pH on Adsorption

Batch adsorption experiments were conducted to examine the effects of solution pH, initial concentration, adsorbent dosage, and contact time (adsorption kinetics) on Cu²⁺ adsorption using SA, SAC, and SAB, respectively. The effect of pH in initial solution on the adsorption efficiency of Cu²⁺ on the three sodium alginate hydrogels was shown in Fig. 3. The adsorption efficiency of SA and SAB beads was lower than 20% at pH 1-3 while that of SAC beads reached about 40%, then the adsorption efficiency of SA and SAB beads increased sharply within pH 3-4 until more than 80% within pH 4-7, and reached the maximum values at pH 7. However, the adsorption efficiency of SA hydrogel beads reached the maximum value at pH 8. These might be caused by the positive charge on the adsorbent surface, which decreased with increasing of pH in solution [40]. Considering that Cu^{2+} will generate $Cu(OH)_2$ precipitation under alkaline conditions, the optimal pH for the adsorption of the three hydrogel beads is confined to 7.

Effect of the Dosage of Hydrogel Beads on Adsorption

In addition to initial pH, adsorbent dosage is one of the most significant parameters affecting the adsorption [41]. The influence of the dosage of SA, SAC, and SAB hydrogel beads on the adsorption was shown in Fig. 4. The initial concentration of Cu^{2+} in the solution was 5 mg/L, and the adsorption efficiency of Cu^{2+} in the solution gradually increased with the increase of the dosage of three kinds of hydrogel beads. When the dosage of hydrogel beads reached 4 mg in dry, the adsorption capacity of Cu^{2+} in the solution reached the maximum. Thus, when treating 50 mL wastewater containing Cu^{2+} with a concentration of 5 mg/L, the dosage of hydrogel beads should be used at least 4 mg in dry to achieve adsorption equilibrium, and the adsorption efficiency exceeded 95% under this condition.



Fig.1 SEM images of SA (**a**–**b**), SAC (**c**–**d**), SAB (**e**–**f**) and photo (**g**) of sodium alginate hydrogel beads. SA = Cu^{2+} imprinted hydrogel beads prepared with sodium alginate, SAC= Cu^{2+} imprinted hydrogel

beads prepared with sodium alginate and carboxymethyl cellulose, SAB= Cu^{2+} imprinted hydrogel beads prepared with sodium alginate and β -cyclodextrin



Fig. 2 FT-IR spectra of SA (a), SAC (b), and SAB (c) sodium alginate hydrogel beads before and after adsorption of Cu^{2+}



Fig. 3 The effect of pH on the adsorption efficiency of three kinds of hydrogel beads



Fig. 4 The effect of the dosage of hydrogel beads on the adsorption



Fig. 5 The effect of initial concentration of Cu^{2+} on adsorption of three hydrogel beads

Effect of Initial Concentration on Adsorption

The adsorption capacity of SA, SAC, and SAB hydrogel beads was also affected by the initial concentration of Cu²⁺ in the solution (Fig. 5). When the concentration of Cu^{2+} was 600 mg/L, the three kinds of hydrogel beads reached the saturated adsorption capacity. The saturated adsorption capacity of sodium alginate hydrogel beads with CMC and β -CD increased significantly with 817 mg/g for SAC beads and 822 mg/g for SAB beads, respectively, which was more than 1.5 times of that of SA beads (510 mg/g). This suggested that the hydrogel beads formed by crosslinking CMC or β -CD with sodium argent alginate play a very important role in metal ion adsorption [29, 31]. More importantly, these values were much higher than the literature reported values for other polymeric hydrogels (Table 1). Thus, the synthesized hydrogel beads with strong adsorption capacity could be a good adsorbent for removing Cu²⁺ from waste water.

Tab	le 1	Saturated	adsorptic	on capacities	s for Cu ^{2*}	+ in compariso	n with previous	work
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Sample	Saturated adsorption capacity (mg/g)	References
Carboxymethyl cellulose/epichlorohydrin hydrogel	415	[36]
Chitosan entrapped carboxymethylated cellulose hydrogel	45	[46]
Cellulose/gelatin composite hydrogel	52	[47]
Cellulose-graft-polyacrylamide/hydroxyapatite composite hydrogel	175	[48]
Carboxymethyl cellulose/polyacrylamide composite hydrogel	227	[49]
Nanofibrillated cellulose/polyethyleneimine composite hydrogels	175	[50]
Carboxymethyl cellulose-graft-sodium alginate hydrogel imprinted with Cu ²⁺	817	This work
β -cyclodextrin-graft-sodium alginate hydrogel imprinted with Cu ²⁺	822	This work

Adsorption Kinetic Model

Adsorption kinetics controls the rate of adsorption, which determines the time required for reaching equilibrium for the adsorption process. The time to reach equilibrium is also an important data for the development of the process and the adsorption system design [42]. The adsorption kinetics curves of the three kinds of hydrogel beads at 308 K were shown in Fig. 6, the inserted image presented the effect of Cu²⁺ adsorption on the hydrogel beads (Cu²⁺ solution on the left and Cu^{2+} adsorption on the bottom right). The adsorption capacity of Cu²⁺ on the hydrogel beads increased with the increase of adsorption time firstly. The adsorption of SA beads reached equilibrium at about 500 min, SAC beads reached equilibrium at about 250 min, and SAB beads reached equilibrium at about 350 min. It could be concluded that adding CMC and β -CD would shorten the equilibrium time of sodium alginate hydrogel beads.

Kinetic models can give information regarding adsorption pathways and probable mechanism involved [42]. The firstorder equation and the second-order equation were used to determine the mass transfer mechanisms and rate-control. Table 2 showed the fitting parameters of quasi-first-order and pseudo-second-order kinetic equations at 308 K. The pseudo-first-order kinetic model for SA beads had higher correlation coefficient than those for SAC and SAB beads, and the calculated q_e of Cu²⁺ on SA beads was very close to that of experimental $q_e(exptl.)$ in three kinds of hydrogel beads, which demonstrated that the adsorption behavior of Cu²⁺ on SA beads could be consistent with the pseudofirst-order kinetic equation, and the adsorption rate of on SA beads was positively correlated to the Cu²⁺ concentration in a certain concentration range.

However, the pseudo-second-order kinetic models for SAC and SAB beads had higher correlation coefficient than that for SA beads, and the calculated q_e of Cu²⁺ on SAC or SAB beads was very close to that of experimental $q_e(\text{exptl.})$, which demonstrated that the adsorption behavior of Cu²⁺ on SAC or SAB beads could be confirmed to the

pseudo-second-order kinetic equation, and the adsorption rate of Cu^{2+} on SAC or SAB beads was not only positively correlated with the concentration of adsorbate, but also positively correlated with the amount of adsorbate [43].

Adsorption Isotherm Model

The Langmuir adsorption equation represented the monolayer adsorption process, while Freundlich's adsorption equation introduced the intermolecular force, which represented the multilayer adsorption process [44]. The adsorption isotherm curves of the three kinds of hydrogel beads at 308 K were shown in Fig. 7. And the fitting parameters of Langmuir and Freundlich for adsorption isotherm equations at 308 K were shown in Table 3. The correlation coefficients of the Freundlich adsorption isotherm equation for the three kinds of hydrogel beads are higher than those of Langmuir isotherm equation, and all of $q_{\rm m}$, the adsorption amounts of the three kinds of hydrogel beads calculated by the Langmuir adsorption isotherm equation, were tremendously different from the experimental $q_e(exptl)$. The adsorption behavior of Cu²⁺ on gel spherical beads is consistent with the Freundlich adsorption isotherm equation, which indicates that the adsorption of Cu²⁺ by gel spherical beads is a multilayer adsorption process in a certain concentration range.

The Freundlich adsorption isotherm equations of SAC and SAB hydrogel beads had higher correlation coefficients, and it was known that the addition of CMC and β -CD could improve the adsorption capacity of hydrogel beads.

The Adsorptive Selectivity of Cu²⁺ on Hydrogel Beads

For studying the adsorption selectivity of SA, SAC, and SAB hydrogel beads, Cu^{2+} was mixed with 15 coexisting ions $(Al^{3+}, Ag^+, Ba^{2+}, Ca^{2+}, Cd^{2+}, Co^{2+}, Cr^{3+}, Fe^{2+}, Fe^{3+}, Li^+, Mg^{2+}, Mn^{2+}, Ni^{2+}, Pb^{2+}$ and Zn^{2+}) in the same concentration of 5 mg/L before the adsorption experiment, respectively. The adsorption efficiency of Cu^{2+} [Q(Cu^{2+})%] on SA, SAC, and SAB hydrogel beads were the maximum ones, reaching



Fig. 6 Adsorption kinetics curve of SA (a), SAC (b), and SAB (c) hydrogel beads

Table 2 Simulation parameters of pseudo-first-order and pseudo-two-order equations for sodium alginate hydrogel beads at 308 K

Materials	q _e (exptl.) (mg/g)	Pseudo-first-order kinetic model			Pseudo-second-order kinetic model		
		$q_{\rm e}({\rm mg/g})$	k ₁ (1/h)	\mathbb{R}^2	$q_{\rm e}({\rm mg/g})$	k ₂ [g/(mg/h)]	R ²
SA	59.25 ± 1.56	55.54	0.4372	0.9857	74.07	0.00648	0.9844
SAC	61.56 ± 1.75	24.79	0.3972	0.7536	94.88	0.01063	0.9894
SAB	61.64 ± 2.01	34.35	0.5858	0.9423	65.53	0.02357	0.9989

exptl. experimental

85.1%, 87.0%, and 89.2%, respectively (Fig. 8), while the adsorption efficiency of other coexisting ions on SA, SAC, and SAB hydrogel beads were only from 7.3%–26.9%,

4.8–28.9%, and 1.5–26.1%, respectively (data not shown in Fig. 8). The selectivity of adsorption was identified by the separation factor β [45]. The separation factors of Cu²⁺ to



Fig. 7 Adsorption isotherm curve of SA (a), SAC (b), and SAB (c) hydrogel beads

Table 3 Simulation parameters of Langmuir equation and Freundlich equation for adsorption isotherm curve of SA, SAC, and SAB hydrogel beads at 308 K

Materials	q _e (exptl.) (mg/g)	Langmuir adsorption isotherm model			Freundlich adsorption isotherm model		
		$q_{\rm m}$ (mg/g)	K _L	R ₁ ²	K _F	m	R ₂ ²
SA	527.5 ± 5.7	- 1365.65	-7.3519×10^{-3}	0.6856	8.7216	0.5134	0.8453
SAC	817.3 ± 6.4	625.00	8.9888×10^{-2}	0.5743	10.4431	0.4629	0.8642
SAB	822.6 ± 6.3	384.62	0.1566	0.7510	10.4792	0.4265	0.9210



Fig.8 The adsorptive selectivity of Cu^{2+} on SA, SAC, and SAB hydrogel beads



Fig.9 The recycling times of SA, SAC, and SAB hydrogel beads adsorption/desorption to Cu^{2+}

other ions β (Cu²⁺/other ions) was 3.2–11.7 for SA beads, β (Cu²⁺/other ions) was 3.0–18.1 for SAC, and β (Cu²⁺/other ions) was 3.4–59.5 for SAB, which reflected the adsorption separation abilities of SA, SAC, and SAB hydrogel beads between Cu²⁺ and other coexisting ions. Thus, the SA, SAC, and SAB hydrogel beads prepared with Cu²⁺ as template, especially SAB beads, show better selectivity for Cu²⁺ than other coexisting ions.

Cycling and Regeneration

Figure 9 showed the effect of HCl solution on the desorption and regeneration of Cu^{2+} adsorbed sodium alginate hydrogel beads. Although the adsorbent maintained its original morphology with the increase of elution time, the desorption-adsorption process caused some damage inside the adsorbent, resulting in a gradual decrease in the adsorption efficiency of Cu^{2+} on the hydrogel beads, the adsorption efficiency of Cu^{2+} on the SAC and SAB hydrogel beads remained above 88% after recycling desorption-adsorption process for six times, while the adsorption efficiency of SA hydrogel beads decreased to below 80%. All above-mentioned results proved that the hydrogel beads synthesized by our proposed method possessed high specific adsorption, selectivity, and reusability.

Conclusions

In this study, to realize the specific adsorption and removal of Cu^{2+} from wastewater, three kinds of environmentally friendly Cu^{2+} ion-imprinted hydrogel beads with high adsorption capacity and high selectivity for Cu^{2+} were successfully prepared using natural raw materials such as sodium alginate. In the process of preparing ion-imprinted sodium alginate hydrogel beads, blending with carboxymethyl cellulose or β -cyclodextrin could improve the saturated adsorption capacity of Cu^{2+} . Thus, ion-imprinted sodium alginate hydrogel beads, especially enhanced with carboxymethyl cellulose or β -cyclodextrin can be developed and utilized as a new type of adsorption material for heavy metal. Once the adsorption achieves saturation, the copper could be recycled by electrochemical treatment or burning treatment of the absorbed beads, which should be investigated further.

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Declarations

Conflict of interest The authors declared that they have no conflicts of interest to this work.

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