ORIGINAL PAPER

Activated Carbon From Palm Fibres Used as an Adsorbent for Methylene Blue Removal

Lana S. Maia¹ · Andressa I. C. da Silva¹ · Emanuel S. Carneiro¹ · Francisco Maciel Monticelli² · Fernanda R. Pinhati¹ · **Daniella R. Mulinari[3](http://orcid.org/0000-0003-4464-5620)**

Accepted: 24 October 2020 / Published online: 2 November 2020 © Springer Science+Business Media, LLC, part of Springer Nature 2020

Abstract

In this paper, activated carbon was synthesized by chemical activation using sodium hydroxide as an activating agent from residues of the stem and sheath palm fibres, and their efficacies in the removal of methylene blue were evaluated. The materials were characterized by techniques like thermogravimetric analysis (TGA), Fourier transform infrared spectroscopy (FTIR), X-ray difraction (XRD), scanning electron microscopy (SEM), and surface area (BET). The infuence of two experimental factors, such as contact time (10 to 70 min) and initial dye concentration (25, 50, 100, 250, and 500 mg.L⁻¹) was investigated. The adsorption process was followed by the Langmuir isotherm model with a maximum adsorption capacity of 110.79 and 162.54 mg.g−1 for stem and sheath palm. Results demonstrated that activated carbon from palm fbres have characteristics necessary for the removal of methylene blue. The equilibrium data were well adjusted in the Langmuir isotherm model, which confirms that the adsorption was heterogeneous and occurred through physicochemical interactions.

Graphic Abstract

Keywords Palm fbres residue · Activated carbon · Methylene blue · Adsorption

 \boxtimes Daniella R. Mulinari

dmulinari@hotmail.com; daniella.mulinari@fat.uerj.br

Extended author information available on the last page of the article

Introduction

The concern with wastewater generated by industries has stimulated the development of new technologies [[1\]](#page-11-0). In this context, attention has been given to industrial effluents containing organic dyes, heavy metals, and contaminants, afecting water quality [[2\]](#page-11-1).

In Brazil, the National Environment Council (CON-AMA) of the Environment Ministry establishes the disposal of liquid effluents. The CONAMA Resolution 430 regulates the conditions, parameters, standards, and directives to manage effluent releases into receptor water bodies, partially changing and complementing Resolution 357 [\[3,](#page-11-2) [4\]](#page-11-3). Effluents from any polluting source may be directly released into receptor bodies after their duly treatment and demands established in this Resolution and by other applicable standards.

One of the industrial pollutants of wastewater is the dye, extensively used in multiple industries such as textile, printing, cosmetics, ink, and plastics.

Among the various dyes, methylene blue (MB) is a cationic dye in the phenothiazine class and has various applications in chemistry, biology, and medicine [[5,](#page-11-4) [6](#page-11-5)]. Exposure to MB can cause harmful health efects, such as high blood pressure, gastrointestinal pain, and nausea. Several methods are used to eliminate pollutants from aquatic environments, including coagulation-focculation, precipitation, and oxidation [\[7](#page-11-6), [8](#page-11-7)]. However, these methods are expensive and produce dangerous by-products [[9](#page-11-8)].

Thus, adsorption has been the most used treatment process. Several studies focused on the adsorption of MB using activated carbon from vegetable fbres [\[6,](#page-11-5) [8,](#page-11-7) [10–](#page-11-9)[12](#page-11-10)].

Activated carbon is the most widely used adsorbent due to its excellent color removal efficiency. However, the coal has an electrically positive surface, making the adsorption of cationic dyes difficult $[12]$ $[12]$ $[12]$. The use of agro-industrial waste is an alternative to developing low-cost adsorbents, contributing to reducing waste disposal costs. Among the various materials used to develop carbon, natural fbres originating from agro-industrial wastes are highlighted because they are renewable sources available at a low cost [[13\]](#page-11-11). Consequently, activated carbon prepared from a large number of agro-industrial wastes such as cofee [\[14\]](#page-11-12), pineapple plant leaves [[15](#page-11-13)], pine cone [[16](#page-11-14)], date palm leafets [[17](#page-11-15)] rice husk [\[18](#page-12-0)], apple peels [\[19\]](#page-12-1), among others [\[20–](#page-12-2)[24\]](#page-12-3). These wastes are found to be the most appropriate precursors due to their higher percentage of carbon and a lower amount of ash content [\[21\]](#page-12-4).

Among the various natural fibres, palm fiber is a very abundant agro-industrial residue in Brazil and may have many more applications $[25-27]$ $[25-27]$ $[25-27]$ $[25-27]$. The heart of palm, also known as palmetto, can be extracted from various

species of palms. *Archontophoenix alexandrae* produces the heart of palm of the noble type, with higher quality and superior favor than other species of palm. For each palm, approximately 400 g of commercial palm heart is harvested. The residue constitutes 80 to 90% of the total palm weight, with some variation depending on the species [[26](#page-12-7)]. According to the Brazilian Institute of Geography and Statistics (IBGE), the production of palm in Brazil was approximately 107.9 thousand tons, representing about 86.3 thousand tons of waste generated in 2018 [[28](#page-12-8)].

The residues from king palm are mainly the leaves and leaf sheaths. Some quantity of this highly cellulosic material is currently used as boiler fuel to prepare fertilizers or as mulching material, but the majority is left on the mill premises [[27\]](#page-12-6). However, the accumulation of this waste can generate environmental problems. Several studies seek to add value to this raw material produced from the extraction of palm heart by using it in other ways [[26\]](#page-12-7).

In this work, activated carbons prepared by chemical activation with NaOH from residues of the stem and sheath palm fibres for methylene blue removal. The materials were characterized by techniques like thermogravimetric analysis (TGA), Fourier transform infrared spectroscopy (FTIR), X-ray difraction (XRD), scanning electron microscopy (SEM), and surface area (BET). The two experimental factors were investigated, such as contact time (10 to 70 min) and initial dye concentration (25, 50, 100, 250, and 500 mg.L-1).

Materials and Methods

Materials

Palm fbres (stem and sheath) were kindly provided by Biosolvit S/A, Rio de Janeiro/ Brazil. Royal palm, also known as *Archontophoenix alexandrae*, is a species originated from Australia, Oceania. In Brazil, its production stands out in the South and Southeast regions. Firstly, fbres were dried at 80 °C for 24 h for moisture removal. The fbres were ground in a mill and sieved to obtain samples that passed through 35 mesh screens.

Preparation of Activated Carbon

In this work, a method for the development of activated carbon from palm fbres using physical-chemical activation was performed, with chemical treatment and pyrolysis. Firstly, the fbres were dried in an oven at 80 °C for 24 h. Then, the palm fibres were impregnated with NaOH (80 g. L^{-1}) as an active agent (weight ratio 1/1) and dried at 100 °C for 24 h. Subsequently, the material was pyrolyzed in a muffle furnace under the inert atmosphere, fowing with 100 mL.

 min^{-1} of argon, where the material was exposed to 400 °C for 3 h. After activation, the activated carbon was washed with distilled water, neutral pH, to remove the active agent and clear the formed pores (Fig. [1\)](#page-2-0). Alkaline activation was used due to the synergistic effects between chemical activation and pyrolysis to fully expose the active adsorption sites and increase functional groups through the reaction between the carbon-oxygen and alkaline bond, increasing the adsorption capacity of the product [[29–](#page-12-9)[31\]](#page-12-10). In activated carbon preparation, the yield was defned as the fnal weight of activated carbon produced after activation, washing, and drying, divided by the initial weight of raw palm fbres.

Characterization of Activated Carbon

The proximate analysis of the raw palm fbres (stem and sheath) was carried out to determine the mass of moisture and ash of the *in natura* palm fbres (stem and sheath). The ultimate analysis to determine the mass of carbon, hydrogen, nitrogen, sulfur, and oxygen (C, H, N, S, and O) of the raw palm fbres (stem and sheath) and activated carbon was performed using the CHNS-O analyzer Flash 2000.

The morphology of the raw palm fbres (stem and sheath) and activated carbon were analyzed by Scanning electron microscopy (SEM), using a microscope HITACHI with tungsten flament operating at 5 kV, employing a low-vacuum technique and a secondary electron detector. Samples were dispersed on brass support and fxed with a double face 3M tape.

Diameter size distribution and surface area were determined using mercury porosimetry equipment from Quantachrome Instruments®. Hg porosimetry was used with were 241 kPa of pressure, 20 s of dwell time, and a vacuum of 25 kPa. Parameters were used to ensure no compressibility in the material during analysis.

The chemical structures of the raw palm fbres (stem and sheath) and activated carbon were analyzed by attenuated total refectance Fourier transform infrared (ATR-FTIR) spectroscopy. The analysis was performed in a transmittance mode, in a range of $4500 - 400$ cm⁻¹, at the resolution of 4 cm^{-1} .

The physical structures of the raw palm fibres (stem and sheath) and activated carbon were evaluated by X-ray difraction using a Shimadzu difractometer, model XDR-6100. The measuring conditions were: CuKa radiation with graphite monochromator, 30 kV voltage, and 40 mA electric current. The patterns were obtained in 10–50° angular intervals with 0.05 steps and 1 s of counting time.

The fbres' thermal behavior and activated carbon were examined by performing the thermogravimetric analysis (TGA). This test method computes the weight loss incurred in the materials with temperature in a controlled atmosphere. Measurements were made by subjecting the material to a temperature range of 25–600 °C. TGA was conducted using SII Nanotechnology INC, model Exstar 6000 at a heating rate of 10 \degree C/min in a nitrogen atmosphere, and specimen weight of 10 mg.

Fig. 1 Specimens from fbres stem and sheath from palm: **a** Fibres of the sheath *in natura*; **b** Sieved fbres of the sheath; **c** Activated fbres of the sheath; **d** Activated carbon of the sheath; **e** Fibres of the stem

in natura; **e** Sieved fbres of the stem; **f** Activated fbres of the stem; **g** Activated carbon of the stem

Removal Methylene Blue

The method used for the measurement of methylene blue (MB) sorption capacity of the sorbent was based on the research developed by Pathania et al. [\[12\]](#page-11-10). The methylene blue sorption capacity from activated carbon was studied under a dynamic system. The sorbent (30 mg) was immersed in 100 mL of the aqueous methylene blue solution in the concentration range of 25, 50, 100, 250, and 500 mg. L^{-1} . The adsorption process was followed for 1 h under mechanical agitation in a shaker (40 rpm). To determine the pH value at the point of zero charge (pH_{zpc}), 0.1 g of activated carbon was added into 50 mL of 0.1 mol.L⁻¹ NaCl solution. The pH was then adjusted to 2.0–10.0 by 0.1 mol.L⁻¹ HCl or NaOH solution. After 24 h, the fnal pH values of the solution were measured. The pH_{zpc} was the point at which $pH_{initial}$ equaled pH_{final} . The dye concentration in the solution was observed using a UV–visible spectrophotometer referring to the standard curve of methylene blue at the maximum wavelength of 665 nm. The quantity of dye adsorbed onto adsorbent (q_e, mg, g^{-1}) and removal (%) of MB were calculated using Eqs. (1) (1) and (2) (2) , respectively:

$$
q_e = (C_0 - C_e) \frac{V}{M}
$$
 (1)

$$
\%Removal = \frac{C_i - C_e}{C_i} \cdot 100\tag{2}
$$

where: q_e quantity of dye in mg per gram of adsorbent; C_i and C_e are respectively initial concentration and equilibrium time of MB (mg. L^{-1}); V volume of the solution; M mass of adsorbent.

Also, the effect of contact time in the removal efficiency of methylene blue sorbent was evaluated. The sorbent (30 mg) was immersed in 100 mL of the aqueous solution of methylene blue in the concentration 50 mg. L^{-1} under mechanical agitation in a shaker (40 rpm) in diferent times (10, 20, 30, 40, 50, 60 and 70 min).

Adsorption Isotherm

Adsorption isotherms can demonstrate the interaction between adsorbates and adsorbents, where the equilibrium distribution of adsorbate molecules occurs between the liquid and solid phases at a typical temperature [[32](#page-12-11)]. The adsorption data were ftted to Langmuir isotherm model. Langmuir sorption isotherm is employed for equilibrium sorption, assigning monolayer sorption on a surface with a fnite number of identical sites [\[12\]](#page-11-10). Experimental data were treated using a Wolfram Mathematica version 11.0, a software with extensive internal functionality for graphics,

linear algebra, and direct implementation. Besides, this software offers an intuitive environment and visualization functions. Therefore, it is an ideal package for educational or research purposes [[33,](#page-12-12) [34](#page-12-13)]. The Langmuir equation can be written by Eq. [3:](#page-3-2)

$$
\frac{1}{q_e} = \frac{1}{q_m} + \frac{1}{K_l q_m C_e} \tag{3}
$$

Thus, the shape of this isotherm can also be expressed in terms of separation factor (RL), which can be given by Eq. [4](#page-3-3):

$$
RL = \frac{1}{1 + K_L C_e} \tag{4}
$$

where: K_L is Langmuir constant $(L.mg^{-1})$ related to the affinity of binding sites and the free energy of sorption; q_e is dye concentration at equilibrium onto biosorbent $(mg.g^{-1});$ C_e is dye concentration at equilibrium in solution (mg. L^{-1}); q_m is dye concentration when monolayer forms on biosorbent (mg.g⁻¹); RL is a separation factor.

In several adsorption situations, adsorbate (favors) solid to liquid phase and adsorption is said to be favorable, $0 < R L < 1$. When $R L > 1$, there is an indication that the solute (favors) liquid to the solid phase. $RL = 1$ corresponds to a linear isotherm [[35](#page-12-14)].

Results

Characterization of Activated Carbon

The chemical compositions of the *in natura* palm fbres (stem and sheath) used in activated carbons preparation evidence contained about 47.8% of cellulose, 23.7% of hemicellulose, 25.9% of lignin, and 1.8% ash [[36\]](#page-12-15). Thus, low ash and high lignin contents were observed, which are essential characteristics in producing activated carbon with optimal properties [[37\]](#page-12-16). High lignin contents provided high yields, thereby contributing to the fxed carbon content at the end of the carbonization and activation processes [\[37](#page-12-16)]. Then, when analyzing the ultimate analysis results, it was observed that the carbon content from activated carbons had been risen from 50.86% to 75.81 wt%, as can be seen in Table [1](#page-4-0). In activated carbon, hydrogen, nitrogen, sulfur, and oxygen contents decreased due to the decomposition during the pyrolysis and activation process. There were no signifcant diferences between the palm fbres (stem and sheath) in carbon, hydrogen, and oxygen content. From the analyses, it was exhibited that the low ash content of the precursor makes it a good starting material for the preparation of activated carbon. The activated carbon yield ranged from

Table 1 Composition and properties of the materials

*FIS (in natura fbre from sheath); FAS (activated fbre from sheath); ACS (activated carbon from sheath); FIST (in natura fbre from stem); FAST(activated fbre from stem); ACST (activated carbon from stem)

68.30 to 64.50% for ACS (activated carbon from sheath) and ACST (activated carbon from stem), respectively.

Figure [2](#page-5-0) shows the surface morphological of fbres (*in natura* and activated) and activated carbon in different magnifcations. It was observed a diference in the surface morphology of the *in natura* fibres (stem and sheath) compared to activated fbres, due to the NaOH activation that resulted in a well developed and uniform surface, producing an orderly pore structure. However, after the pyrolysis, the surface morphological of activated carbon presented an expanded state of pore structure due to the evaporation of the NaOH during carbonization, leaving the space previously occupied by the activation agent available for the adsorption of MB. All samples showed irregular and porous surfaces at depths that possibly allow the transport, entry, and adsorption of MB. Heidarnejad et al. [[10\]](#page-11-9) obtained similar behavior with activated carbons from the date the press cake by lowfrequency ultrasound.

Diferent pores were observed in the activated carbon samples. Due to activation and carbonization, volatiles was removed, producing a fxed carbon mass with the widening of pore networks present in activated carbon samples [\[38](#page-12-17)]. Thus, the activated carbon presents an adequate morphology for MB adsorption. In general, carbon surfaces have irregular pores and well-developed pores on the surface of the activated carbon.

Porosity was measured via Hg porosimetry, as shown in Table [1](#page-4-0). Each material density tends to be lower for *in natura* fbres (sheath and stem), presents the same tendency to increase for fiber activation (i.e. $\approx 10\%$ of increases). Activated carbon exhibited a higher density increase, 51% for the sheath, and 71% for the stem palm, compared to *in natura* fbres. This behavior is a result of densifcation, confrming SEM images results.

The determination of surface area is an essential characteristic because it will result in higher sorption capacity [\[39](#page-12-18)]. Thus, both activated carbons (sheath and stem) presented a signifcant increase in surface area compared to *in natura* fbres, an improvement of 38% and 71% for sheath (ACS) and stem (ACST) was observed, respectively. Consequently, the expected result of MB sorption capacity should be better for ACST showed higher superficial area than ACS and, respectively, higher superficial contact with MB.

Porosity characteristics directly influence the superficial area. For a better understanding of porosity analysis, Fig. [3](#page-6-0) shows the histogram of pore size distribution. Thus, the average pore diameter revealed the macroporous structure of prepared activated carbon according to the IUPAC classifcation, indicating that the materials have a relatively large surface area, which is one of the prerequisites as excellent adsorption material, as can be seen in Fig. [2](#page-5-0)b.

A higher diference between *in natura* fbres and activated carbon showed that the stem palm (Fig. [3b](#page-6-0)) presented a higher frequency of larger porosity (>40 µm) for *in natura* fbres. After activation of the fbres processes, larger porosities are broken into smaller voids. Activation of the carbon process densities the material and creates a homogeneity distribution of pore size, between small and larger porosity.

The same behavior was found for sheath palm fbres and activated carbon, which *in natura* fbres presented higher frequency for larger porosity (i.e. $> 40 \mu m$), with less frequency when compared to *in natura* fbres from stem. The frst treatment (activated fbre) broke larger porosity into small one (i.e. $<$ 15 μ m), and then, the activated carbon densities the material (as shown in SEM images – Fig. [2](#page-5-0)), and created more homogeny distribution of pore size. The larger pore diameter is essential for initial oil sorption; although, it exhibits low retention capacity [[40\]](#page-12-19). On the other hand, the smaller pore diameter is also relevant concerning capillary effects that create a sorption force, facilitating retention [[40–](#page-12-19)[42\]](#page-12-20). Considering previous porosity distribution for all materials, the activation of carbon results in pore size with homogeneity in a frequency distribution, presenting appropriated sorption characteristics.

FTIR analysis was used to identify some characteristic functional groups of activated carbon and fbres (*in natura* and activated) [[12\]](#page-11-10). The analyzed spectra demonstrated the activating agent's ability to alter the chemical surface of **Fig. 2 a** SEM of the palm fbres (superior view): (a) FIS (*in natura* fibre from sheath); (b) FIST (*in natura* fibre from stem); (c) FAS (activated fbre from sheath); (d) FAST(activated fbre from stem); (e) ACS (activated carbon from sheath); (f) ACST (activated carbon from stem); **b** graphical representation of diferent sizes of pores (macropores, mesopores, and micropores) in a lateral view

activated carbon, which could be detected from functional groups present in the sample (Fig. [4\)](#page-6-1).

In *natura* fibres (stem and sheath), the FTIR spectra showed broadband situated about in the range $3500 - 3200$ cm⁻¹ ascribed to O–H stretching vibration. The bands near 2920 and 1620 cm^{-1} corresponded to the stretching vibration of aliphatic C–H and aromatic C=C. Two bands at approximately 1160 and 1020 cm−1 related to stretching vibration of C–O bond in organic compounds (such as alcohols, phenols, acids, ethers or esters) [[26](#page-12-7)]. Some bands associated with organic groups such as C–H and C–O bonds expressed the higher intensities for the spectrum

of activated fbres from stem. However, for the spectrum of activated fbres from sheath, these organic groups expressed the lower intensities.

After carbonization, all samples of activated carbon substantially decreased of band intensities such as in the range $3500 - 3200$ cm⁻¹ vibration related to the O-H stretch bonded, alcohol, phenol functional group; 2920 and 1620 cm−1 related to stretching vibration of aliphatic C–H and aromatic C=C; and 1160 and 1020 cm^{-1} related to stretching vibration of C–O bond in organic compounds.

This behavior can be observed in several carbons obtained from natural fbres, which provides activated carbon with

Fig. 3 Pore size distribution: **a** sheath and **b** stem

Fig. 4 FTIR of the palm fbres: **a** stem and **b** sheath

NaOH more signifcant natural substances, such as natural or synthetic pigments [\[38](#page-12-17), [43](#page-12-21)]. This data corroborates the results obtained in the adsorption capacity of coal in methylene blue.

Similar vibration was observed in other works with activated carbon developed from green coconut shell, *fcus carica bast*, and date press cake by low-frequency ultrasound $[10, 12, 38]$ $[10, 12, 38]$ $[10, 12, 38]$ $[10, 12, 38]$ $[10, 12, 38]$ $[10, 12, 38]$ $[10, 12, 38]$. El-Shafey et al. $[44]$ $[44]$ $[44]$ also observed a reduction of the band related to the -OH stretching vibration and, therefore, favored the methylene blue adsorption.

These changes in absorption bands suggest the interactions of stained cells with biosorbent functional groups [\[45](#page-12-23)].

Figure [5](#page-7-0) evidences the TGA and DTG curves for the materials. The *in natura* and activated fibres presented two important weight loss steps. Between 30 and 120 °C, which is characteristic of the evaporation of water molecules adsorbed on the surface [\[1\]](#page-11-0). Mulinari et al. [[46](#page-12-24)] obtained similar behavior with the sugarcane bagasse fibres. Another stage of weight loss was the thermal decomposition of the

cellulose structure, which was occurred at 260–350 °C. Somseta et al. [[1\]](#page-11-0) evidenced similar behavior when studying activated carbon/cellulose biocomposite flms to remove MB.

Only a single weight loss step was observed in the activated carbon, which occurred near 100 °C.

Analyzing both curves showed that the activated carbon loses less weight loss than *in natura* and activated fbres in the same range temperature (Fig. [5\)](#page-7-0). Thus, the activated carbon can be exposed to 600 °C without much signifcant weight loss adsorbent. However, it was noted that fbres from the sheath presented a minimal diference in thermal stability compared to fbres from the stem, which can be evidenced in Table [2.](#page-7-1)

Thus, it can be observed that, when comparing these results to the green coconut shell carbon, a greater thermal resistance was obtained because the weight loss of the sheath and stem was 17.69% and 20.96%, respectively, in the range 27 to 600 $^{\circ}$ C [\[38](#page-12-17)].

Fig. 5 TGA and DTG of the palm fbres: (**a** and **b**) sheath and (**c** and **d**) stem

Degradation temperature peak $({}^{\circ}C)$	Weight loss $(\%)$							
	600 °C	500 °C	400 °C	300 $\mathrm{^{\circ}C}$	200 °C	100 °C		
	307	51.64	49.16	44.61	27.33	12.51	10.46	FIS
	251	47.57	45.91	41.69	36.70	25.22	21.16	FAS
	$---$	17.96	14.7	11.99	10.40	9.42	7.83	ACS
	312	55.11	52.21	47.04	25.51	8.83	6.46	FIST
	268	33.21	30.98	25.47	18.77	6.92	1.82	FAST
	$---$	20.96	16.70	12.49	9.67	7.88	4.89	ACST

FIS in natura fbre from sheath, *FAS* activated fbre from sheath, *ACS* activated carbon from sheath, *FIST* in natura fbre from stem, *FAST* activated fbre from stem, *ACST* activated carbon from stem

El-Shafey et al. [[39\]](#page-12-18) obtained a constant weight loss of about 22.1% between 120 and 785 °C, with maximum weight loss at 280 °C. Somsesta et al. [\[1](#page-11-0)] obtained thermal decomposition in the cellulose structure between 276 and 350 °C, showing that the activated carbon of the sheath and stem have greater resistance to high temperatures.

From difractograms (Fig. [6\)](#page-8-0) two peaks at angle 22° and 43° relayed to (002) and (100/101) lattice planes were noted for *in natura* and activated fbres (sheath and stem),

respectively. The broad peak at 22° is characteristic of disordered aromatic carbon structure, and the peak at 43.4° is characteristic of graphitic or organized carbon. The signal intensities of both materials' graphitic carbon are similar, indicating that their structures are also similar [\[15](#page-11-13)].

After the pyrolysis process, the disappearance of peaks was observed in both materials indicating the amorphous nature of the adsorbent, contributing to methylene blue removal [[46\]](#page-12-24). Sahu et al. [\[22\]](#page-12-25) evidenced similar results

Fig. 6 XRD of the palm fbres: **a** sheath and **b** stem

Table 3 Removal of MB of the activated carbon from sheath and stem

Concentration	$ACS (\%)$	$ACST(\%)$	
25	89.9	95.0	
50	82.6	89.7	
100	73.8	80.8	
250	54.7	44.0	
500	54.2	43.2	

ACS activated carbon from sheath, *ACST* activated carbon from stem

when synthesizing activated carbon from kendu fruit peel by the carbonization and chemical activation with ammonium carbonate.

Effect of Concentration in the Removal Efficiency of Methylene Blue

The effect of concentration in removing MB (25 to 500 mg. L^{-1}) on activated carbon (stem and sheath) with a contact time of 1 h was varied. Table [3](#page-8-1) shows that MB removal decreased with a higher concentration of adsorbent due to the increase in the driving force for mass transfer [\[12](#page-11-10)]. At low concentrations, there will be unoccupied active sites on the adsorbent surface. On the other hand, above optimal MB concentration, the active sites required for the dye's adsorption will lack, which can retard the MB adsorption by activated carbon. Pathania et al. [[12\]](#page-11-10) also observed similar behavior to study activated carbon developed from *Ficus carica bast* (FCBA).

The highest efficiency in the sorption carried out with the stem and sheath's activated carbon is 95% and 89.88% at 25 mg.L⁻¹. Ibupoto et al. [\[48](#page-12-26)] studied the reusable carbon nanofibres for MB removal for the removal efficiency

at 25 mg. L^{-1} and observed that in 15 min a removal of 85% occurred; and in 1 h a complete removal occurred, considering the equilibrium time to optimize parameters. Thus, compared to the activated carbon proposed in this work, it was demonstrated that the activated carbon from the stem and sheath obtained better adsorption performance than carbon nanofbres.

The adsorption capacity was evaluated using the Langmuir isotherm model. It has been observed that the sorption capacity (q_m) was found to be 110.79 and 162.54 mg.g⁻¹ for stem and sheath palm, respectively (Table [4](#page-9-0)). However, to compare the separation factors *RL*, obtained from the isotherms, it was noticed that the MB sorption was more favorable for the activated carbon of the palm stem at lower concentrations (Fig. [7](#page-9-1)). This can be identifed through the range of *RL* values, which were slightly lower than the carbon from the sheath, indicating a greater affinity between adsorbent and adsorbate (Table [4\)](#page-9-0). When comparing the *RL* values with Doke et al. [[49](#page-12-27)], both favor the adsorption process.

Table [5](#page-9-2) shows the maximum adsorption capacity of MB on adsorbent obtained by Langmuir isotherm. It is possible to deduce that activated carbon from palm residue is a good precursor for producing efficient organic adsorbents with adequate adsorption capacity for MB dyes.

The pH value is one of the factors that infuence the adsorption performance [\[1](#page-11-0)]. To understand the adsorption process was necessary to determine the pH_{ZPC} (the pH at which the net surface charge of the adsorbent is zero) of the adsorbent material [[50](#page-12-28)]. Cationic dyes such as methylene blue and methyl violet are usually adsorbed minimally at low pH and exhibit increased adsorption with increasing pH [[51](#page-13-0)]. This behavior is due to the electrostatic interaction between cationic dye molecules and anionic functional groups on the adsorbent's surface. Thus, the pH_{ZPC} of activated carbon

Fig. 7 Adsorption isotherms: **a** activated carbon from stem and **b** activated carbon from sheath

Table 4 Langmuir Isotherm coefficients

 10

 \boldsymbol{s}

 $\overline{2}$

 $\overline{2}$

pH_{final}

 (a)

 q_m (dye concentration when monolayer forms on biosorbent); K_L (Langmuir constant); RL (separation factor)

Table 5 Adsorption capacity of MB in mg per gram of the activated carbon from sheath and stem

Concentration	$ACS (mg.g^{-1})$	$ACST$ (mg.g ⁻¹)	
25	22.47	23.75	
50	41.32	44.85	
100	86.89	80.84	
250	136.65	110.08	
500	271.01	216.15	

ACS activated carbon from sheath, *ACST* activated carbon from stem

pH_{zpc}

s

 ϵ

pH_{initia}

(sheath and stem) was approximately 6, which means that the surface of the carbon is positively charged when the pH of the solution is lower than 6 and is negatively charged at pH values higher than 6, as can be seen in Fig. [8.](#page-9-3)

Therefore, as MB is a cationic dye, its adsorption will be favored by the more highly negatively charged activated carbon under alkaline conditions. When the pH of the dye solution increases, the positive charge at the interface of that solution decreases, and the negative charge appears on the adsorbent surface resulting in an increase in MB adsorption due to the more signifcant electrostatic attraction between the positively charged adsorbate and the negatively charged adsorbent [[52](#page-13-1)]. The adsorption capacity increases in basic media due to the adsorption mechanism, which involves the interactions between cationic dye and negatively charged adsorbent surface. Oppositely, in acidic medium, the positively charged surface of sorbent tends to oppose the adsorption of the cationic adsorbate [[12](#page-11-10), [53–](#page-13-2)[55](#page-13-3)]. The literature shows the performance in MB removal with $pH \sim 7.0$ and basic. In this work, the pH of the solution was adjusted to 6.

Fig. 8 μ H_{zpc} of the activated carbon: **a** sheath and **b** stem

Then, if the pH of the MB solution in this study is changed, it will be possible to increase the proposed adsorbent's removal efficiency.

Similar results have been reported in the literature by researchers with pH value \sim 6 or superior to 6 for MB removal [[1,](#page-11-0) [12\]](#page-11-10). Li et al. [\[56](#page-13-4)] proposed methylene blue and aniline's adsorption onto activated carbon from waste edible fungus residue. These authors presented an adsorption capacity of MB superior to 95% with pH 6–10 at 100 mg. L−1 and an adsorbent dose of 40 mg. Saheed et al. [\[57](#page-13-5)] realized the sorption study of methylene blue on activated carbon prepared from jatropha curcas (JAC) and terminalia catappa seed coats (TAC). They observed that TAC presented a dye removal capacity of 25 mg.g⁻¹ with pH 6 at 40 mg.L⁻¹ and an adsorbent dose of 20 mg.

Effect of Contact Time in the Removal Efficiency of Methylene Blue

The effect of contact time in the removal of MB can be seen in Fig. [9.](#page-10-0) Analyzing the efficiency of activated carbon from the stem, the highest percentage rate of MB removal was 53.21% in 40 min (Fig. $9a$). On the other hand, the efficiency of activated carbon from sheath was 65.26% in 10 min for removing MB (Fig. [9b](#page-10-0)). It can also be seen that the dye adsorption capacity of the activated carbon of the stem is 26.61 mg.g⁻¹ (Fig. [9](#page-10-0)c) and that of the activated carbon of the sheath is $32.63 \text{ mg} \cdot \text{g}^{-1}$ (Fig. [9d](#page-10-0)).

The adsorption rate change is because, initially, all the adsorbent sites are empty, and the solute concentration gradient is very high. Subsequently, the lower adsorption rate is due to a decrease in the number of vacant sites of adsorbent and dye concentrations. The decrease in adsorption particularly indicates a possible monolayer of MB in the adsorbent surface [\[45](#page-12-23), [55\]](#page-13-3). This can be attributed to the lack of available active sites necessary for greater uptake after reaching equilibrium [\[45](#page-12-23)].

Figure [9](#page-10-0) shows that in shorter contact times, MB's removal by the activated carbons is faster.

Somsesta et al. [\[1\]](#page-11-0) analyzed MB's removal efficiency at 40 mg.L^{-1} and obtained a removal rate of 70%, considering pH 6.9, at 35 °C, and in 360 min.. Compared to the activated carbon proposed in this work, the sheath's activated carbon shows the removal of 65.26%, at 50 mg.L⁻¹, considering pH 6.0, at 25 °C in 10 min. In this way, the activated carbon of the sheath palm presents better adsorption results.

Fig. 9 Efect of contact time in the removal efciency of methylene blue: **a** activated carbon from stem and **b** activated carbon from sheath; Efect of contact time on adsorption capacity: **c** activated carbon from stem and **d** activated carbon from sheath

Meili et al. [\[24](#page-12-3)] observed that the activated carbons from sugarcane bagasse and soursop could remove MB about 75% and 50% in 50 mg. L^{-1} solution for 60 min. Compared to the activated carbon proposed in this work, the stem and sheath obtained, respectively, 89.7% and 82.63% in 50 mg. L−1 solution. Then, the activated carbon of the stem and sheath palm present better adsorption results.

The adsorbent materials, once saturated, are directly discarded. However, several studies have shown the possibility of reusing these sorbents to minimize operating costs and product waste [\[12](#page-11-10), [13\]](#page-11-11). Typically, regeneration techniques are selected according to the contaminant's nature, the operating cost, and the conditions of the processes [[58\]](#page-13-6). All the studies exposed demonstrate favorable results for the process of regeneration and reuse of the adsorbent materials. It is possible to observe that, after a few adsorption-desorption cycles, the adsorption capacity of the activated carbon is reduced due to the occurrence of strong interactions between the dye molecules and the adsorbent [\[59](#page-13-7)].

Conclusion

Palm fbres from stem and sheath based activated carbon were successfully prepared by the chemical activation method with NaOH. The operating parameters for the maximum sorption were dye solution concentration (25 mg.L^{-1}) , sorbent dosage (30 mg), contact time (60 min), and temperature (303 K) . Both achieved removal efficiency greater than 85% at 25 mg. L^{-1} . The adsorption isotherm was well defned by the Langmuir model with a maximum adsorption capacity of 110.79 and 162.54 mg.g⁻¹ for stem and sheath palm. The equilibrium data were well adjusted in the Langmuir isotherm model, which confrms that the adsorption is heterogeneous and occurred through physicochemical interactions. Of this form, the activated carbon from the sheath and stem of the palm has the characteristics necessary to use adsorbents to remove blue methylene.

Acknowledgements Authors are grateful for the research support by FAPERJ (process E-26 /010.001800 / 2015 and E-26 / 010.101232 / 2018).

Compliance with Ethical Standards

Conflict of interest The authors declare that they have no confict of interest.

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Lana S. Maia¹ · Andressa I. C. da Silva¹ · Emanuel S. Carneiro¹ · Francisco Maciel Monticelli² · Fernanda R. Pinhati¹ · **Daniella R. Mulinari[3](http://orcid.org/0000-0003-4464-5620)**

- ¹ Departament of Chemistry and Environmental, Universidade do Estado do Rio de Janeiro, Resende, Brazil
- ² Department of Materials and Technology, Guaratinguetá School of Engineering, São Paulo State University (Unesp), Guaratinguetá, Brazil
- Department of Mechanicaland Energy, Universidade do Estado do Rio de Janeiro, Rodovia Presidente Dutra km 298, Polo Industrial, CEP 27537-000 Resende, Brazil