# Chemical routes to materials



# Facile preparation of magnetic sodium alginate/carboxymethyl cellulose composite hydrogel for removal of heavy metal ions from aqueous solution

Sisi Wu<sup>1</sup>, Juan Guo<sup>1</sup>, Ying Wang<sup>1</sup>, Chao Huang<sup>1,\*</sup>, and Yong Hu<sup>1,\*</sup>

<sup>1</sup> School of Food Science, Guangdong Pharmaceutical University, Zhongshan 528458, China

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#### ABSTRACT

A novel magnetic polysaccharide composite hydrogel was successfully constructed by using sodium alginate (SA) and carboxymethyl cellulose (CMC) as the backbone and filled with in situ  $Fe<sub>3</sub>O<sub>4</sub>$  nanoparticles, which was then employed for removal of heavy metal ion from aqueous solution. The obtained magnetic SA/CMC composite hydrogel was characterized by Fourier transform infrared spectroscopy, fluorescence microscope, thermogravimetric and vibrating sample magnetometer. Effect of contact time, pH and adsorbent dosage on the adsorption of heavy metal ions by the magnetic SA/CMC hydrogel have also been studied. The results show that the prepared magnetic SA/CMC hydrogel can be effectively utilized in the removal of heavy metal ions from aqueous solution. The maximal adsorption capacity of Mn(II), Pb(II), and Cu(II) as calculated from the Langmuir model were 71.83, 89.49, and 105.93 mg/g, respectively. The adsorption process of the magnetic SA/CMC hydrogel on the heavy metal ions can be attributed to ion exchange and chemical adsorption. What's more, the magnetic hydrogel exhibited high efficiency after four cycles, which indicating it offers great potential for practical application in the removal of heavy metal ions from aqueous solution.

# Introduction

Pollution of aquatic ecosystems by heavy metals is one of the most important issues that has received special attention in recent years due to the rapid development of industry, agriculture, traffic, and

residential activities  $[1-3]$ . The discharge of heavy metal-containing wastewater into the environment can damage ecosystems and even threaten the health of humans through the food chain [[4,](#page-9-0) [5](#page-9-0)]. Therefore, how to efficiently remove heavy metal ions has been a significant interest in research. It is particularly worth noting that heavy metals such as Mn(II), Pb(II),

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Address correspondence to E-mail: huangc@gdpu.edu.cn; lidhyong@126.com

and Cu(II) can be accumulated in the human body through inhalation, ingestion, drinking polluted water, and dermal contact, which may lead to potential damage to bone, brain, kidney, and liver [\[6–8](#page-9-0)]. In general, the methods for the removal of heavy metal ions from wastewater include electrolysis, reduction-precipitation, photocatalysis, membrane separation, ion exchange, and adsorption, etc. [\[9](#page-9-0), [10\]](#page-9-0). Among these technologies, adsorption is regarded as one of the most promising ways for the removal of heavy metal ions due to inexpensive, superior efficiency, and nontoxic to the environment [\[11–14](#page-9-0)].

With the requirements for the recovery and reuse of specific heavy metals and the environmental demand, degradable adsorption materials such as sodium alginate (SA) and carboxymethyl cellulose (CMC) are increasingly used in the removal of heavy metal ion from wastewater due to the presence of various functional groups within them [\[15](#page-9-0), [16\]](#page-9-0). SA is a natural polysaccharide extracted from brown algae. Due to the presence of free carboxyl groups and can be easily cross-linked by divalent and trivalent cations such as  $Ca^{2+}$ ,  $Ba^{2+}$ , and  $Fe^{3+}$  to produce a stable gel, SA has been widely used in water treatment applications [\[17](#page-10-0), [18\]](#page-10-0). In addition to SA, as an anionic polymeric obtained from the natural cellulose, CMC can also produce hydrogel by coordinating with multivalent cations such as  $Fe^{3+}$  and  $Al^{3+}$ , which make it possible for binding metal ions due to the presence of hydroxyl and carboxyl groups on the structure [[19,](#page-10-0) [20](#page-10-0)].

Recently, it has been reported that nanomaterials such as magnetic nanoparticles, carbon nanotubes, graphene were used to compound with polysaccharide hydrogels to improve its adsorption and mechanical properties [\[21–23](#page-10-0)]. Among them, due to the simple preparation process, high specific surface area, and the ability to treat a large amount of wastewater in a short time without producing contaminants, the polysaccharide hydrogels incorporated with  $Fe<sub>3</sub>O<sub>4</sub>$  magnetic nanoparticles have become the focus of adsorption research [[24,](#page-10-0) [25\]](#page-10-0). However, although SA/CMC hydrogel has been investigated in some articles for the removal of heavy metal ions from aqueous solution, there is rare research on the preparation of magnetic SA/CMC composite hydrogel filled with in-situ formation of  $Fe<sub>3</sub>O<sub>4</sub>$  nanoparticle by a green and facile method without additional chemical cross-linking agents and organic solvents [[26,](#page-10-0) [27\]](#page-10-0).

In this work, the magnetic SA/CMC composite hydrogel filled with  $Fe<sub>3</sub>O<sub>4</sub>$  nanoparticles was successfully constructed by co-precipitation and subsequent freezing–thawing method. A series of experiments were carried out to investigate the structural characteristics and adsorption performance of the magnetic SA/CMC composite hydrogel. The results demonstrate the magnetic composite hydrogel has good adsorption and solid–liquid separation performance, which can be used to remove heavy metal ions from contaminated aqueous solution.

#### Materials and methods

#### Materials

Sodium alginate (SA, viscosity,  $\geq 200$  mPa·s, average MW, 270 kDa) was purchased from Aladdin Chemistry Co., Ltd. Carboxymethyl cellulose (CMC, sodium salt, substitution degree  $\geq 60\%$ , average MW, 250 kDa) were purchased from Sinopharm Chemical Reagent Co., Ltd. Other reagents such as sodium hydroxide, ethanol, manganese nitrate, lead nitrate, copper sulfate,  $FeCl<sub>2</sub>·4H<sub>2</sub>O$ , and  $FeCl<sub>3</sub>·6H<sub>2</sub>O$ were purchased from China National Pharmaceutical Corporation Limited. The chemical reagents were of analytical grade and employed directly without further purification. All solutions were prepared with distilled water.

# Preparation of magnetic composite hydrogels

First, 2.50 g SA and 2.50 g CMC were weighed and dissolved in 100 ml deionized water under magnetic stirring at 600 rpm for 2 h to generate a homogeneous  $CMC/SA$  solution. Secondly, 6.41 g FeCl<sub>3-</sub>  $6H_2O$  and  $3.19g$  FeCl<sub>2</sub>.4H<sub>2</sub>O were weighed and dissolved in 50 ml deionized water to form a uniform solution, and then was placed in CMC/SA solution followed by magnetic stirring for 1 h at room temperature. Finally, the dark brown color suspension solution after ultrasonic for 1 h was reduced by 0.1 mol/L ammonia until pH 9 and kept overnight at room temperature. The obtained gel was thoroughly rinsed with deionized water three times to remove unreacted reagents, and then frozen and thawed three times to make the gel more uniformly crosslinked. Scheme 1 represents the formation of magnetic SA/CMC composite hydrogel. First, the compound solution of CMC and SA was cross-linked with  $Fe^{3+}$  and  $Fe^{2+}$  to form an inclusion complex, and then an appropriate amount of ammonia was added into the mixed iron-polysaccharide solution to form a magnetic composite hydrogel. Finally, the obtained magnetic composite hydrogel was subjected to freezing–thawing for further cross-linking.

#### Characterizations

The surface morphologies of the SA/CMC magnetic hydrogel were observed by fluorescence microscope (BX-50 Olympus, Japan). The functional groups of these samples were detected using Fourier transform infrared spectrophotometer (Nicolet 5700, American) by KBr pellet method in the range between 4000 and  $500 \text{ cm}^{-1}$  with a spectral resolution of 4 cm<sup>-1</sup> and 20 scans. Thermogravimetric analysis (TGA) was measured under a nitrogen atmosphere with NetzschTG-209 from 40 to 600 °C with a heating rate of 10 °C/ min. Magnetization measurements were performed by Lakeshore 7400-S vibrating sample magnetometer (VSM).

#### Sorption experiments

In order to study the metal adsorption capacities of SA/CMC magnetic hydrogel, three types of heavy metal ions [Cu(II), Pb(II), and Mn(II)] were selected. The 0.01 g dry hydrogel was mixed in metal ion solutions, and then placed in a constant temperature vibrating shaker until the adsorption reaches equilibrium. At different intervals, the metal ion concentrations were determined by resonance light scattering (RLS) spectra, which were achieved by means of a fluorescence spectrophotometer (RF5301- PC, Shimadzu, Japan) with  $\Delta \lambda = 0$  nm. The pH values of the solution were adjusted by 0.1 M HCl or NaOH solutions. The adsorption rate (E), adsorption capacity  $(q_e)$ , and distribution coefficient  $(K_d)$  were calculated according to the following equation:

$$
E = \frac{C_0 - C_e}{C_0} \times 100\% \tag{1}
$$

$$
q_{\rm e} = \frac{(C_0 - C_{\rm e})V}{m} \tag{2}
$$

$$
K_{\rm d} = \frac{V(C_0 - C_{\rm e})C_{\rm e}}{C_{\rm e} \times m} \tag{3}
$$

Here,  $C_0$  (mg/L) and  $C_e$  (mg/L) are the initial concentrations of metal ions and the remaining metal ions concentration in the solution after adsorption equilibrium, respectively;  $V(L)$  represents the volume of the metal ions solution;  $m$  (g) indicates the weight of magnetic hydrogels.

#### Kinetics of adsorption

Crushed 0.01 g dry SA/CMC magnetic hydrogel sample was added to the 20 mL metal ion storage solution with an initial concentration of 100 mg $\cdot L^{-1}$ , and then was placed in a constant temperature vibrating shaker until the adsorption reaches equilibrium. The remaining metal ions concentration is analyzed to calculate the adsorption capacity. The kinetic rate of different metal ions adsorption on the magnetic hydrogels was investigated by using the pseudo-first-order, pseudo-second-order, and intraparticle diffusion models. The expressions are as follows:

$$
lg(q_e - q_t) = lg q_e - k_1 t \tag{4}
$$

$$
\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \tag{5}
$$



Scheme 1 The scheme for constructing magnetic SA/CMC composite hydrogel.

$$
q_t = k_{\rm id} t^{1/2} + C \tag{6}
$$

where  $q_e$  (mg·g<sup>-1</sup>) is the equilibrium adsorption capacity,  $q_t$  (mg·g<sup>-1</sup>) is the adsorption capacity in t time,  $k_1$  (min<sup>-1</sup>),  $k_2$  (g·mg<sup>-1</sup> min<sup>-1</sup>), and  $k_{id}$  $(mg·g<sup>-1</sup> min<sup>-0.5</sup>)$  are the rate constants of the pseudofirst-order, pseudo-second-order, and kinetic models, respectively. C is the boundary layer thickness.

#### Adsorption isotherm

The 0.01 g dry SA/CMC magnetic hydrogel was placed in a solution of 20 mL metal ions with initial concentrations of 10, 20, 40, 60, 100, 150, 200 mg $\cdot L^{-1}$ , and then was shaken in a water bath oscillator for 24 h at room temperature. The remaining metal ions concentration was analyzed to calculate the adsorption capacity of the adsorbent. The adsorption isotherm was fitted by the Langmuir and Freundlich model equations. The expressions are as follows:

$$
\frac{C_e}{q_e} = \frac{1}{k_L q_m} + \frac{C_e}{q_m} \tag{7}
$$

$$
\ln q_e = \ln K_F + \frac{1}{n} \ln C_e \tag{8}
$$

In the formula,  $K_{\text{L}}$  and  $K_{\text{F}}$  are the constants related to adsorption in the Langmuir and Freundlich models, respectively;  $n$  is the Freundlich adsorption index, which is related to the properties of the adsorbent.

#### Competitive adsorption

Crushed 0.01 g dry SA/CMC magnetic hydrogel sample was added into a flask with 20 mL of a mixed solution containing three metal ions [Cu(II), Pb(II), and Mn(II)], and then was shaken in a thermostatic oscillator for 24 h at room temperature.

#### Desorption and regeneration

After the adsorption experiment is completed, the used magnetic hydrogel is eluted with 1 M HCl solution and regenerated with 0.1 M NaOH solution, and then washed with deionized water until it is neutral. According to the above method, the regeneration performance was tested four times through the adsorption/desorption cycle, and each experiment used the same heavy metal ion solution.

#### Results and discussion

## Characterization of SA/CMC magnetic hydrogel

The appearance and FM images of the SA/CMC magnetic hydrogel are displayed in Fig. 1. It can be observed from the surface of the magnetic hydrogel (Fig. 1a) that the hydrogel appeared to be rough and uneven. As seen from the FM image of freeze-dried magnetic hydrogel (Fig. 1b), the obtained magnetic hydrogel has a honeycomb porous network structure and can be considered suitable for the adsorption of metal ions.

The FTIR spectra of SA, CMC, and SA/CMC magnetic hydrogel were used to confirm the existence of the expected functional groups. As shown in Fig. [2](#page-4-0)b, c, both SA and CMC exhibit a common characteristic absorption peaks at about 3453  $cm^{-1}$ , which can be attributed the stretching vibration of O– H. However, the stretching vibration peak of O–H in CMC/SA magnetic hydrogel is narrowed and moved to a low wavelength that is locked at  $3418 \text{ cm}^{-1}$ , indicating hydrogen bonds may occur between CMC and SA macromolecules [\[28](#page-10-0)]. The characteristic absorption peaks at 1622  $\text{cm}^{-1}$  and 1413  $\text{cm}^{-1}$  relating to the asymmetric and symmetric vibration of COO<sup>-</sup> are occurred at 1618 cm<sup>-1</sup> and 1396 cm<sup>-1</sup> in a magnetic hydrogel, respectively, which indicating  $COO<sup>-</sup>$  may participate in the cross-linking reaction. In addition, the characteristic peak belongs to the stretching vibration peak of C–O in pure SA and pure CMC is observed at  $1028 \text{ cm}^{-1}$  and  $1030 \text{ cm}^{-1}$ ,



Figure 1 Appearance (a) and FM photographs (b) of magnetic SA/CMC hydrogel.



<span id="page-4-0"></span>

Figure 2 FTIR spectra of magnetic hydrogel (a), CMC (b) and SA (c).

respectively, while in CMC/SA magnetic hydrogel occurs at  $1023$   $cm^{-1}$ . Other important consideration that the characteristic peak due to the stretching vibration of Fe-O is observed at  $568 \text{ cm}^{-1}$ , which demonstrates the presence of ion oxide in the hydrogel networks [[29\]](#page-10-0). From the above analysis, it can be seen that the SA/CMC magnetic hydrogel has been generated successfully.

Thermogravimetric (TG) was carried out to examine the thermal stability of the SA/CMC magnetic hydrogel. As shown in Fig. 3a, the weight losses of SA are presented in two stages. The first stage appeared between 30 and 150  $^{\circ}$ C due to the evaporation of moisture. The second stage appeared

between 250 and 300  $^{\circ}$ C can be attributed to the breaking and losing of O–H groups on the alginate structure [\[30\]](#page-10-0). However, the TGA curve of SA/CMC magnetic hydrogel can be divided roughly into three stages. The first slight weight loss of 1.6% at 80–150  $\degree$ C due to the loss of adsorbed water in the sample. The other two weight loss step seen in the range of 250–350 °C and 420–480 °C can be ascribed to the network structural degradation of the magnetic hydrogel and the decomposition of molecular structure [[31\]](#page-10-0). The different thermal degradation rates of the SA and CMC/SA magnetic hydrogel demonstrate the cross-linking reaction between chains, which leads to the formation of the composite adsorbent. The magnetization curve of SA/CMC magnetic hydrogel is shown in Fig. 3b. Obviously, the mild magnetic saturation value (3.2 emu  $g^{-1}$ ) is attributed to the presence of  $Fe<sub>3</sub>O<sub>4</sub>$  nanoparticles. The inset image further proves that the prepared hydrogel has good magnetic properties and can be used for the adsorption and separation of heavy metal ions.

#### Adsorption experiments

Resonance light scattering (RLS) is analytical technology that depends upon the measurements of light scattering of particles [\[32](#page-10-0)]. Particularly, when analytical conditions such as wavelength and pH are fixed, the RLS intensity is proportional only to the concentration of scattering particles [[33\]](#page-10-0). It is shown in Fig. [4](#page-5-0)a, the RLS intensity of Cu(II) solution is very



Figure 3 TGA of SA/CMC magnetic hydrogel (a1), SA(a2), and DTG of SA/CMC magnetic hydrogel (a3); Magnetization of SA/CMC magnetic hydrogel (b).

<span id="page-5-0"></span>obvious. However, the RLS intensity of Cu(II) solution occurs remarkable decrease after the addition of CMC/SA magnetic hydrogel, which demonstrates that the absorption capacity of the magnetic hydrogel can be calculated by lowering the RLS intensity in solution. Figure 4b shows FTIR spectra of CMC/SA magnetic hydrogel before and after the adsorption of Cu(II) ions. After adsorbing Cu(II) ions, the asymmetric and symmetric vibration peak of COO<sup>-</sup> at 1622 cm<sup>-1</sup> and 1413 cm<sup>-1</sup> are shifted to 1635 cm<sup>-1</sup> and  $1399 \text{ cm}^{-1}$ , respectively, and the stretching vibration peak of C–O at 1023  $\text{cm}^{-1}$  is almost disappeared. In view of the existence of electrostatic attraction and ion exchange reaction between –COO– and heavy metal ions in solution, it can be inferred that the COO- group in magnetic hydrogel may play an important role in adsorption.

Since the prepared magnetic SA/CMC composite hydrogel can effectively adsorb copper ions, it is also considered to be able to adsorb other heavy metal ions such as lead and manganese ions. Figure [5a](#page-6-0) shows the effect of contact time on the adsorption of Cu(II), Mn(II), and Pb(II) by magnetic SA/CMC composite hydrogel. The observed order of absorption capacity of these metal ions to reach equilibrium is  $Cu(II) > Pb(II) > Mn(II)$ , which mainly related to the electronegativity and ionic radius of different heavy ions (the electronegativities for the Pb(II), Cu(II) and Mn(II) are 2.33,1.90 and 1.55, respectively; the ionic radius for the Pb(II), Cu(II) and Mn(II) are 1.33  $\AA$ , 0.72  $\AA$  and 0.67  $\AA$ , respectively). In addition, it can be seen that about 70% of total Mn(II), Cu(II),

and Pb(II) were absorbed by the magnetic hydrogel occurs within the first 50 min. The fast adsorption may be due to the three-dimensional loose and porous structure of the magnetic hydrogel, providing heavy metal ions with easier access to the adsorption sites. It also should be noted that there exist a slightly difference in contact time for each metal ion to reach the adsorption equilibrium, reflecting the differentiation of adsorption rate between different heavy metal ions and the magnetic SA/CMC hydrogel.

As is known to us, the initial pH of solution is another important parameter in the adsorption process of heavy metal ions [\[34](#page-10-0)]. Figure [5b](#page-6-0) shows the effect of solution pH on the adsorption of Pb(II), Cu(II), and Mn(II) by SA/CMC magnetic hydrogel. In the lower pH values (2.0–3.0), the adsorption capacity of the three heavy metal ions on the magnetic hydrogel starts to increase slowly may be due to part of the COO<sup>-</sup> in the magnetic hydrogel combined with the  $H^+$  in solution. As the pH value of the solution increases, the adsorption capacity for Pb(II) increases gradually in the pH range of 4–5, while for  $Cu(II)$  and  $Mn(II)$  in the range of 4–6. The reason is that the  $COO<sup>-</sup>$  ions can fully combine with metal ions due to the decreasing amount of  $H^+$  in solution, which leads to a remarkable increase in adsorption. However, further increasing the pH value of the solution shows different effects on the adsorption process. When the pH increases from 5.0 to 7.0, the adsorption amount of Pb(II) dropped rapidly, which can be due to and the precipitation in the form of Pb(OH)<sub>2</sub> [\[35](#page-10-0)]. For Cu(II), the adsorption capacity



Figure 4 RLS (a) and FTIR (b) spectra of  $Cu^{2+}$  before and after treating with SA/CMC magnetic composite hydrogel.



<span id="page-6-0"></span>

Figure 5 The effect of contact time (a) and pH (b) on adsorption capacity of SA/CMC magnetic hydrogel at room temperature.

begins to decrease when the pH is greater than 6. This can be attributed to OH  $^-$  ions react with metal ions at the active sites on the absorbent surface [\[36](#page-10-0)]. For Mn(II), the adsorption capacity continues to increase when the pH is greater than 6. This is because manganese usually precipitates at higher pH values than 8.0 [\[37](#page-10-0)].

#### Adsorption kinetics

The adsorption kinetics of three metal ions were investigated by using the pseudo-first-order, pseudosecond-order, and intraparticle diffusion models, and the results were depicted in Fig. [6](#page-7-0). The calculated result of corresponding adsorption parameter values and correlation coefficients were presented in Table [1](#page-7-0). It is found that the correlation coefficients of modeled pseudo-second-order by experiment data shown in Fig. 5a are larger than that of the pseudofirst-order and intraparticle diffusion model. Meanwhile, the equilibrium adsorption capacity calculated by the pseudo-second-order model is also closer to the experimental data. Therefore, the adsorption of metal ions by SA/CMC magnetic hydrogel can be better described by the pseudo-second-order kinetic model, which means the chemisorption dominates the adsorption of heavy metal ions [\[38](#page-10-0)]. In particular, an obvious inflection point can be found from the fitting results of the intra-particle diffusion model, which indicates that the adsorption of metal ions by the magnetic hydrogel may be divided into two stages  $[39]$  $[39]$ . The first linear stage (t < 120 min) is the

diffusion process of metal ions on the gel surface, and the second stage  $(t > 120$  min) can be attributed to internal diffusion. Besides, although the fitting between  $q_t$  and  $t^{1/2}$  exhibits a substantially linear relationship, the straight line does not pass through the origin, which demonstrates that the absorption of metal ions by the magnetic hydrogel is jointly controlled by multiple steps [[40\]](#page-10-0).

#### Adsorption isotherms

Isotherm is one of the important factors to understand the adsorption efficiency and explore the adsorption mechanism. Figure [7](#page-8-0) shows the adsorption isotherms of Pb(II), Cu(II), and Mn(II) on SA/ CMC magnetic hydrogel fitted by the Langmuir and Freundlich models, respectively. The corresponding parameters and correlation coefficients  $(R^2)$  are listed in Table [2.](#page-8-0) It can be seen from the fitting results in Table [2](#page-8-0) that the adsorption process can be better explained by the Langmuir model, which suggests the adsorption process was carried out on the monolayer surface. Additionally, according to the value of  $n$  estimated by the Freundlich model, it can be inferred that there is a certain degree of heterogeneous adsorption between metal ions and magnetic hydrogel [[41\]](#page-11-0). Therefore, the adsorption mechanism of metal ions by the SA/CMC magnetic hydrogel can be due to chemical adsorption accompanied ion exchange.

<span id="page-7-0"></span>

Figure 6 Pseudo-first-order (a), pseudo-second-order (b) and intraparticle diffusion (c) kinetic model on Cu (II), Pb (II) and Mn (II) ions adsorption.



#### Competitive selective adsorption

The results of competitive selective adsorption of Cu(II), Pb(II), and Mn(II) are shown in Fig. [8](#page-8-0). During the adsorption process, it can be seen that the amount of adsorption of Cu(II) by SA/CMC magnetic hydrogel is the largest, followed by Pb(II) and Mn(II). Additionally, the distribution coefficient of Cu(II) is the highest with the value of  $64.03 \text{ L/g}$ , while only 15.08  $L/g$  for Mn(II), which further demonstrates the competitive adsorption relationship between different metal ions and hydrogel. The main reason is that each metal ion has a different electronegativity and coordination ability with the SA/CMC magnetic hydrogel. Obviously, when the number of adsorption active sites of the adsorbing material is limited, the three metal ions will compete to adsorb the active sites in the material network.

<span id="page-8-0"></span>

Figure 7 Langmuir (a) and Freundlich (b) isotherm model on Cu (II), Pb (II), Mn (II) ions adsorption.





Figure 8 Selective adsorption of the SA/CMC magnetic hydrogel.

#### Adsorbent recycling

The results of recovery efficiency of metal ions by SA/CMC magnetic hydrogel are shown in Fig. 9. As it indicated, the adsorption efficiency of the three metal ions is gradually decreased after adsorption/ stripping cycles. In the first cycle, the removal efficiency is 92.1%, 90.1%, and 79.9% for Cu(II), Pb(II), and Mn(II), respectively. At the end of the fourth cycle, the adsorption efficiency of Cu(II), Pb(II), and Mn(II) can reach 65.3%, 61.7%, and 58.6%,





Figure 9 Removal efficiency after adsorption–desorption cycles.

respectively. The results show that, although part of the functional groups was destroyed after acid treatment, the magnetic hydrogel still retains a better desorption cycle utilization rate.

# **Conclusion**

In this study, the magnetic SA/CMC hydrogel was prepared with a simple and green preparation approach, and its adsorption of Cu(II), Pb(II), and Mn(II) was studied experimentally. Results showed

<span id="page-9-0"></span>that the adsorption equilibrium was substantially reached in about 240 min and the adsorption capacity for Cu(II), Pb(II), and Mn(II) were 105.93, 89.49, and 71.83 mg/g, respectively. Additionally, the adsorption kinetics could be better described by pseudosecond-order and the adsorption isotherms were fitted better with the Langmuir model. It was also examined that the magnetic SA/CMC hydrogel had

good removal efficiency after four circulations. It is expected that the magnetic composite hydrogel will potentially be used to remove heavy metal contaminants from aquatic systems.

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# Author contributions

Hu Yong: Conceptualization, Methodology, Writingoriginal draft, Funding acquisition. Wu Sisi: Experiment investigation, Data curation. Guo Juan: Instrumental analysis, Funding acquisition. Wang Ying: Instrumental analysis. Huang Chao: Writing- review.

## Declarations

Conflict of interest The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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