

# **Enhancement of potable water production from an inclined photovoltaic panel absorber solar still by integrating with fat‑plate collector**

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# **Abstract**

This manuscript brings out with an enhancement of the freshwater productivity from the active inclined solar panel basin solar still (AISPBSS). The research was conducted on the AISPBSS by the diversified mass flow rate of water  $(m_f)$ . The maximum freshwater yield obtained at  $m_f$  at 1.8, 3.2 and 4.7 kg/h is 7.5, 6.5 and 5.4 kg, respectively. The daily average thermal and exergy efficiency of the AISPBSS at  $m_f$  at 1.8, 3.2 and 4.7 kg/h is 43.71, 38.27 and 29.62% and 8.39, 6.94 and 5.08%, respectively. The daily average PV panel power production of  $47.71$ ,  $49.84$  and  $53.83$  watts, electrical efficiency of  $7.2$ ,  $7.6$  and  $8.1\%$ , thermal efficiency of 17.3, 18.3 and 19.7%, exergy efficiency of 18.32, 20.23 and 22.39%, the overall thermal efficiency of  $61.39$ ,  $57.44$  and  $51.37\%$  and the overall exergy efficiency of 26.52, 27.14 and 27.40% are obtained from the system under  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. When  $m_f$  increases, there are decreases in the AISPBSS distillate yield, thermal, exergy and the overall thermal efficiency and increases in the PV panel power production and electrical, thermal, exergy and the overall exergy efficiency. Further, energy return term and carbon credit attained for the AISPBSS have been calculated. It was found that payback period of 20, 18.7 and 17.5 years and carbon credit earned of 21, 25 and 30 \$ are obtained at  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively.

**Keywords** Photovoltaic panel-integrated solar still  $\cdot$  Mass flow rates  $\cdot$  Panel efficiency  $\cdot$  PV thermal and exergy analysis · Energy payback period · Carbon credit earned

### **Abbreviations**



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## **Subscript**



# **1 Introduction**

Over the earlier time, shortage of potable water has turned out to be progressively risky due to the regularly expanding populace of the world, the fast improvement in an industry and the increasing contamination of water assets. Close to 2025, there will be the signifcant issue confronting half of the total populace, to be specifc the absence of the freshwater (Kabeel et al. [2018\)](#page-20-0). Elective methods for producing the potable water must be found. A lot of studies have been done to augment the freshwater from the solar still. Among the several design modifcations (single-basin, double-basin, single-slope and double-slope solar still, pyramid, tubular and hybrid solar still), inclined solar still (ISS) performance is better than the conventional solar still (CSS). The main advantage of an ISS over the CSS is, it can maintain minimum water depth of the basin. A slim layer of water in the absorber plate results in quick evaporation and higher yield than the CSS (Kabeel et al. [2017\)](#page-20-1). El-Agouz et al. ([2015\)](#page-20-2) theoretically examined the ISS performance by reusing the hot water to the still basin using the water pump. Aybar et al. [\(2016](#page-20-3)) carried out the comparative investigation of single-basin ISS and double-basin ISS. Ravishankar et al. theoretically (Sathyamurthy et al. [2016\)](#page-21-0) and experimentally (Nagarajan et al. [2017\)](#page-21-1) calculated the production rate of the ISS with and without baffle plates by varying  $m_f$ . The freshwater production from the ISS with and without baffles was 5.4 and 3.4  $\text{kg/m}^2$ , respectively. El-Agouz [\(2014](#page-20-4)) used a storage tank for continuous water circulation in a stepped solar still (SSS) to augment the production time. He found that SSS with saltwater as inlet formed the daily productivity of 6.3 L/m<sup>2</sup> and seawater formed the productivity of 6.1 L/m<sup>2</sup>. Comparative study of the CSS and the SSS with refectors attached to the perpendicular sides of the steps was done by Omara et al. [\(2013](#page-21-2)). The SSS with and without an internal refector improves the daily yield of about 75 and 57%, respectively, than the CSS. Omara et al. ([2014\)](#page-21-3) also researched the SSS with internal mirrors and outside mirrors (top and bottom). This system produced the maximum yield of about  $8100 \text{ ml/m}^2$  which was  $125\%$  higher than the CSS. Velmurugan et al. [\(2009](#page-22-0)) researched the SSS for sewage desalination. It was found that the productivity of the SSS with fns, with fns and pebbles, with fns and sponge and with fns, pebbles and sponge was 1.27, 1.37, 1.4 and 1.65  $L/m<sup>2</sup>$ , respectively. The freshwater production rate was increased about 53, 68, 65 and 98% when fns, fns and pebbles, fns and sponge and fns, pebbles and sponge, respectively. Abujazar et al. ([2017a](#page-20-5), [b\)](#page-19-0) researched the SSS performance by replacing an absorber plate made of galvanized iron tray with copper tray. The absorber plate was made of copper to increase the thermal conductivity of the absorber plate. This SSS enhances the evaporation area of about 55.6% more than the CSS. It was found that copper inclined SSS produced the daily maximum freshwater production of about 4383 ML/m<sup>2</sup> and maximum hourly efficiency of 58% at 5 p.m. Tanaka and Nakatake [\(2007](#page-22-1)) introduced the novel vertical fat-plate refector (VFPR) attached inclined wick solar still (IWSS) and numerically derived its performance. In this system, wick-type absorber plate received the direct, difuse and refected solar intensity. It was found that an IWSS with and without VFPR produces the daily maximum yield of about 6.5 and 5.7 kg/ m<sup>2</sup>, respectively. Tanaka ([2011,](#page-22-2) [2013\)](#page-22-3) also numerically studied the performance of the bottom fat-plate refector attached with an IWSS. It was found that an IWSS with and without bottom flat-plate reflector produces the daily maximum yield of about 7.5 and 6.01 kg/m<sup>2</sup>, respectively. Sathyamurthy et al. ([2015\)](#page-21-4) introduced a novel semicircular trough basin solar still coupled with baffles. Experiments were conducted by  $m_f$  at 8 kg/h and 10 number of baffles arranged in an absorber plate and results were compared with the CSS. It was concluded that the novel system with baffles and the CSS provide the maximal yield of 3.2 and 2.6 kg/m<sup>2</sup> and maximum efficiency of 38.48 and 32.4%, respectively. Experimental study of pyramid solar still (PSS) integrated with an ISS with baffles has been done by Kumar et al. [\(2017](#page-20-6)). In this research, three solar stills (PSS, ISS and PSS integrated with ISS) were tested. Experiments were conducted by the ISS at  $m_f$  at 8.33 kg/h and the PSS at water height of 0.02, 0.04 and 0.06 m, respectively. The daily productivity from the PSS, ISS and PSS integrated with the ISS is 4.2, 5.04 and 7.52 kg/m<sup>2</sup>, respectively. Economic and exergy analysis of the PSS and the PSS integrated with an ISS with baffles has been done by Panchal et al.  $(2017)$  $(2017)$ . From the exergy analysis, it was reported that exergy efficiency during

the evening time was higher for the 0.05-m water depth. The maximum exergy efficiency of 14 and 35% was obtained for the PSS and still integration at the higher water depth.

Diferent experimental works were conducted on the PV panel integrated with an FPC in the active type solar distillation, and it was submitted that this system produced the water productivity of  $6-10 \text{ kg/m}^2$ /day. By integrating the solar panel in the still, the productivity was increased about 60% than the CSS (Kumar and Tiwari [2009,](#page-20-7) [2010](#page-20-8); Dev and Tiwari [2010;](#page-20-9) Gaur and Tiwari [2010](#page-20-10); Kumar [2013](#page-20-11); Eltawil and Omara [2014;](#page-20-12) Saeedi et al. [2015;](#page-21-6) Tiwari et al. [2015](#page-22-4); Singh et al. [2016](#page-22-5)). Kabeel et al. ([2012](#page-20-13)) researched the CSS by incorporating with the rotary fan which was operated by a vertical shaft powered by the PV panel. It was submitted that this system produced the daily productivity of  $4.75 \text{ L/m}^2$  and it was  $25\%$  higher than the CSS. The solar still incorporated with the vacuum tube coupled with a PV panel has been experimentally investigated by Abdallah et al. [\(2009\)](#page-19-1). Yari et al. [\(2016](#page-22-6)) researched the active type solar still by attaching the solar cells at the glass surface, and it was reported that this system produced 32% higher productivity than the CSS. Hidouria et al. [\(2017\)](#page-20-14) and Al-Nimr et al. ([2016](#page-20-15)) developed a hybrid desalination system. The CSS integrated with an AC heater and a solar panel was experimentally studied by Riahi et al. [\(2015](#page-21-7)) and Praveen Kumar et al. [\(2017\)](#page-21-8).

Abdullah ([2013\)](#page-19-2) has done the design modifcations of SSS such as the use of aluminum flling in the absorber plate as thermal storage medium, integrating solar air heater (active mode) and glass cover cooling technology. Kabeel et al. [\(2012](#page-20-16)) researched the SSS performance by varying the width of trays, depth of water, attaching a wick cloth on the perpendicular side of the trays and an integrating the vacuum tube solar collector (active mode).

Al-Nimr and Qananba ([2018](#page-20-17)) researched a novel CSS incorporated with a fnned condensing unit, solar cells and thermoelectric generator. Experiments were conducted on hybrid system with and without condensing unit. From the experimentation, it was reported that distilled water production rate increased up to 27% when ambient temperature increased from 10 to 35 °C and solar intensity was 1000  $W/m<sup>2</sup>$  and production rate decreased up to 37% when the wind velocity was 10 m/s. Similarly, fnned condensing unit increased the distilled water production rate up to 14% as compared to the CSS. This hybrid system negatively afects the solar cells performance for the reasons of higher heat gain in the PV cells. Fathy et al. ([2018\)](#page-20-18) fabricated parabolic trough collector (PTC) integrated with a doubleslope solar still (DSSS). In this work, oil pipes are connected with a solar still basin to transmit heat from the PTC to the DSSS. Experiments were conducted on CSS, CSS integrated with fixed PTC and CSS integrated with tracked PTC at the water depth of 20 and 30 mm, respectively. It was submitted that the maximum daily yield of 4.51, 8.53 and 10.93 kg/m<sup>2</sup> and daily efficiency of 36.87, 23.26 and 29.81% were obtained for the CSS, CSS integrated with fxed PTC and CSS integrated with tracked PTC, respectively, at 20 mm water depth on summer month. The CSS integrated with tracked PTC produced 142.3% higher freshwater production than the CSS. Malaeb et al. ([2016\)](#page-21-9) numerically derived the performance of the modifed solar still with and without rotating drum in the basin of the still. It was reported that still with rotating drum produced about 3 L of water whereas still without rotating drum produced about 1 L of water. Singh et al. ([2016\)](#page-22-7) researched the CSS and DSSS performance by using energy matrices based on exergy for the atmospheric conditions of India. It was reported that based on the exergy analysis CSS performance is better than the DSSS. Singh and Tiwari [\(2017a](#page-21-10)) theoretically augmented the DSSS energy matrices by integrating with N identical PVT collector. It was reported that hybrid PVT integrating with the FPC coupled with DSSS produced higher annual yield than the hybrid PVT integrating with the CPC coupled with DSSS and conventional DSSS. Singh and Tiwari ([2017b](#page-21-11)) also numerically derived the performance of the CSS and DSSS by integrating with PVT-CPC. It was reported that DSSS performance was higher than the CSS.

Al-Nimr et al. ([2018\)](#page-20-19) researched a distiller with photovoltaic/thermoelectric cooler (PV/ TEC). The TEC is used to augment the condensation rate and avoid excessive heating in this model. Al-Nimr and Al-Ammari [\(2016](#page-20-20)) also researched a new model of PV/T distillation unit with the CSS in which the solar cells were attached in the basin which produced yield of 6.8 L/m<sup>2</sup>/day. Al-Nimr [\(2015](#page-20-21)) next designed a novel PV/T system, which was fitted with an evaporator and a condenser to improve its performance. Manokar et al. ([2018d](#page-21-12)) introduced a PV/T-integrated ISS. In this research work, the PV panel is integrated with an ISS to produce an electrical power and freshwater. It consists of the PV panel as an absorber plate, glass collector cover and water storage tank. Water is uniformly distributed through the PVC pipe which is attached at the top of the experimental setup. Constantly water is fowing over the PV panel, which absorbs the heat energy from the panel and produces simultaneously hot water and freshwater. Increasing  $m_f$  positively affects the panel performance and negatively afects the still performance. It was submitted that increases in the basin temperature result in higher distillate yield and lower power production. The maximum productivity of 7.3 kg and efficiency of  $71.2\%$  are obtained when the system is fully insulated condition. From the above studies, it is found that only few researchers carried out an inclined solar still integrated with preheating methodologies (active mode) (Kumar et al. [2017](#page-20-6); Abdullah [2013;](#page-19-2) Kabeel et al. [2012](#page-20-16)).

## **2 Identifcation of knowledge gap**

Various comprehensive review articles have been studied (Kumar et al. [2015;](#page-20-22) Manokar et al. [2014](#page-21-13), [2018a](#page-21-14), [b](#page-21-15), [c](#page-21-16), [2019;](#page-21-17) Nayi and Modi [2018;](#page-21-18) Murugavel et al. [2013;](#page-21-19) Kaviti et al. [2016;](#page-20-23) Kabeel et al. [2019\)](#page-20-24). From the review articles of Kali et al. (Murugavel et al. [2013\)](#page-21-19), Kaviti et al. ([2016\)](#page-20-23) and Kabeel et al. ([2019\)](#page-20-24), it was found that only few experimental works have been published on active ISS. In the previous study, Manokar et al. [\(2018d](#page-21-12), [e](#page-21-20)) reported that bottom insulation reduces the PV panel performance because of higher panel temperature whereas without insulation reduces the freshwater yield. Hence, the main novelty of this research work is integrating the ISPB still without any insulation with an FPC to enhance the electrical performance of the solar panel and also freshwater yield.

#### **3 Design and construction of the AISPBSS**

The schematic representation and photographic view of an AISPBSS are shown in Figs. [1](#page-5-0) and [2](#page-5-1), respectively. The saltwater from the cylindrical water storage tank is fed into the FPC at a constant  $m_f$ . The water flowing inside the absorber tube of the FPC gets heated, and heated water is again fed into the AISPBSS. In the absorber of the AISPBSS, wick material (cotton thread) is fxed in-between the space between the solar cells to augment the evaporation rate. Due to inclined position of PV panel, water is fowing through it and hot water is collected at the bottom of the experimental setup. Every hour the collected hot water is manually flled in the storage tank. The collector cover of the experimental setup is made of 4-mm-thick normal glass. In the collector cover surface, a glass strip is attached to collect the freshwater and it is collected at the bottom of the experimental setup.  $m_f$  is adjusted by using the control valves. Thermocouples were attached at the diferent places of the experimental setup to measure the temperatures. The dimensions of the FPC water heater and an AISPBSS are given in Table [1](#page-5-2). The AISPBSS was placed at south direction with a decline equal to 13°N. During the



<span id="page-5-0"></span>**Fig. 1** Schematic diagram of an AISPBSS

<span id="page-5-1"></span>**Fig. 2** Photographic view of an **AISPBSS** 





<span id="page-5-2"></span>

operation of an AISPBSS, we are facing the problem of salt deposition on the solar panel and it requires maintenance. The periodic maintenance of the solar panel by Windex crystal rain glass cleaner is required because of salt deposition (Manokar et al. [2018e\)](#page-21-20).

$S$ . no.	Instruments	Measuring parameter	Accuracy	Range
$\mathbf{1}$	Thermocouple	Temperature	$+1$ °C	$0-100$ °C
2	Solar power meter	Solar intensity	$\pm 1$ W/m <sup>2</sup>	0–2500 $W/m^2$
3	Anemometer	Wind velocity	$+0.1$ m/s	$0 - 15$ m/s
$\overline{4}$	Measuring jar	Water mass	$\pm 10$ m L	$0 - 1000$ m L
5	Multimeter	Voltage and current	$+1V$	$0 - 1000$ V
			$\pm 0.1$ A	$0-10A$

<span id="page-6-0"></span>**Table 2** Accuracy, range and error limits for diferent measuring instruments

<span id="page-6-1"></span>**Table 3** Cost analysis for an AISPBSS

S. no.	Materials	Unit cost $(\$)$	Total cost $(\$)$
1	Solar PV panel (150 watts)	\$1.48/watts	\$222.68
$\overline{2}$	Glass material (walls and collector)	\$23.75	\$23.75
3	Distillate collector	\$1.48	\$1.48
	ISPB still	(A)	\$247.91
$\overline{4}$	Copper material	\$10.39	\$10.39
5	FPC collector cover	\$4.45	\$4.45
6	Wooden box	\$8.91	\$8.91
	FPC water heater	(B)	\$23.75
7	Storage tank and stand	\$7.42	\$7.42
8	Control valve	\$2.23/2 pieces	\$4.45
9	Windex crystal rain glass cleaner	\$19.30	\$19.30
10	Labor cost	\$3.71/h	\$14.85
	Accessories and labor cost	(C)	\$46.02
	Total cost	$(A+B+C)$	\$317.68

 $1\text{ s} = \text{Rs } 67.39$ 

The range and accuracy in the present investigations are given in Table [2.](#page-6-0) The detailed error analysis of the instrument (uncertainty) is provided in ["Appendix](#page-19-3)." Cost breakdown for the AISPBSS is given in Table [3.](#page-6-1)

Experiments were performed on July 2017 in three different  $m_f$  conditions: (i) 1.8, (ii) 3.2 and (iii) 4.7 kg/h. During the testing period, the average solar intensity was calculated and three similar atmospheric conditions days July 21, 2017 (average  $I(t)$  718 W/m<sup>2</sup>), July 23, 2017 (average  $I(t)$  709 W/m<sup>2</sup>), and July 24, 2017 (average  $I(t)$  716 W/m<sup>2</sup>), were selected for the comparative studies.

# **4 Results and discussion**

## **4.1 Variations of solar irradiance, wind speed, atmospheric temperature and glass temperature**

Fluctuations of the solar irradiance and atmosphere temperature for the duration of the study of an AISPBSS are shown in Fig. [3](#page-7-0)a, b. During the testing periods, the solar intensity



<span id="page-7-0"></span>**Fig. 3** Diurnal variation of **a** solar intensity and **b** atmospheric temperature

and atmosphere temperature increase at the morning session and attained its highest value at 1 p.m. At the evening session, it is decreasing. The maximum solar intensity of 890, 940 and 910 W/m<sup>2</sup> and the daily average solar intensity of 718, 709 and 716 W/m<sup>2</sup> are noted on July 21, 2017, July 23, 2017, and July 24, 2017, respectively. The maximum atmosphere temperature of 34, 33 and 35  $^{\circ}$ C is noted on July 21, 2017, July 23, 2017, and July 24, 2017, respectively. During the experimental day, the daily average atmospheric temperature is between 30 and 32 °C.

Variations of wind speed and the collector cover temperature during the study of an AISPBSS are plotted in Fig. [4](#page-8-0)a, b. During the investigational day, the average wind speed is noted as 1.5, 1.8 and 2 m/s on July 21, 2017, July 23, 2017, and July 24, 2017, respectively. The maximum collector cover temperature of the AISPBSS is 51, 48 and 47  $^{\circ}$ C on July 21, 2017, July 23, 2017, and July 24, 2017, respectively. The daily average collector cover temperature of 45, 43 and 41.22 °C is measured for the daily average wind speed of 1.5, 1.8 and 2 m/s, respectively. From the above data, it is clear that when the wind speed is higher, collector cover surface enhances the convective heat transfer from the collector cover to the atmosphere, which resulted in lower collector cover temperature.

# **4.2 Efect of** *m***<sup>f</sup> on basin and water temperature**

Variations of the basin temperature for an AISPBSS under different  $m_f$  are plotted in Fig. [5a](#page-8-1). Basin temperature increases with increasing solar intensity and reached its peak value at 2 p.m., and from there on it gets reduced. The maximum basin temperature of 71, 67 and 65 °C is obtained for  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. The daily average basin temperature of an AISPBSS at  $m_f$  at 1.8, 3.2 and 4.7 kg/h is 60.78, 57.34 and 54.56 °C, respectively. When  $m_f$  increases from 1.8 to 3.2 kg/h and from 1.8 to 4.7 kg/h, there is a decrease in the daily average basin temperature of about 5.66 and 10.24%, respectively. An increase in  $m_f$  results in higher volume of flowing saline water in the AISPBSS basin, which resulted in the lower basin temperature.

Variations of the water temperature for an AISPBSS under different  $m_f$  are plotted in Fig. [5b](#page-8-1). Water temperature is directly equivalent to the basin temperature and it reached the



<span id="page-8-0"></span>**Fig. 4** Diurnal variations of **a** wind speed and **b** glass temperature



<span id="page-8-1"></span>**Fig. 5** Hourly variations of **a** basin temperature and **b** water temperature for an AISPBSS

peak value at 2 p.m., and from there on it gets reduced. The maximum water temperature of an AISPBSS at  $m_f$  at 1.8, 3.2 and 4.7 kg/h is 74, 71 and 68 °C, respectively. The daily average water temperature of 63.78, 61 and 58.23 °C is obtained for  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. Water temperature is reduced up to  $4.36$  and  $8.71\%$  when  $m_f$  increases from 1.8 to 3.2 kg/h and from 1.8 to 4.7 kg/h, respectively. The minimum  $m_f$  of an AISPBSS increases the contact time between the saline water and the absorber plate, which resulted in higher water temperature and hence higher yield.  $m_f$  is inversely proportional to the basin and water temperature. When  $m_f$  increases, the volume of flowing water in the absorber plate increases, which reduces the contact time between the saline water and an absorber plate and hence produces lower productivity.



<span id="page-9-0"></span>**Fig. 6** Hourly variations of **a** EHTC and **b** accumulated yield for an AISPBSS

## 4.3 Effect of  $m_{\rm f}$  on Evaporative Heat Transfer Coefficient (EHTC), accumulated yield, **thermal and exergy efficiency**

Variations of the EHTC for an AISPBSS at different  $m_f$  are shown in Fig. [6a](#page-9-0). The maximum EHTC of 86.7, 76.7 and 67.6 W/m<sup>2</sup>k is obtained for an AISPBSS under  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. The daily average EHTC for an AISPBSS under  $m_f$  at 1.8, 3.2 and 4.7 kg/h is 59.2, 52.5 and 45.86 W/m<sup>2</sup>k, respectively. There are 11.31 and 22.53% decreases in daily average EHTC when  $m_f$  is increased from 1.8 to 3.2 kg/h and from 1.8 to 4.7 kg/h, respectively. An increase in  $m_f$  decreased the saline water temperature and EHTC, hence resulted in lower freshwater production.

The EHTC from the feed water to glass is calculated by (Manokar et al. [2018d\)](#page-21-12),

$$
h_{\rm e,w-g} = 16.273 \times 10^{-3} x h_{\rm c,w-g} \left[ \frac{P_{\rm w} - P_{\rm gi}}{T_{\rm w} - T_{\rm gi}} \right] \tag{1}
$$

The convective heat transfer coefficient from the feed water to glass is calculated by (Manokar et al. [2018d](#page-21-12)),

$$
h_{\rm c,w-g} = 0.884 \left[ \left( T_{\rm w} - T_{\rm gi} \right) + \frac{\left( P_{\rm w} - P_{\rm gi} \right) \left( T_{\rm w} + 273 \right)}{\left( 268.9 \times 10^{-3} - P_{\rm w} \right)} \right]
$$
(2)

Partial vapor pressure at the feed water temperature and inner glass is calculated by (Manokar et al. [2018d](#page-21-12)),

$$
P_{\rm w} = \exp\left(25.317 - \left(\frac{5144}{273 + T_{\rm w}}\right)\right)
$$
 (3)

$$
P_{gi} = \exp\left(25.317 - \left(\frac{5144}{273 + T_{gi}}\right)\right)
$$
(4)



<span id="page-10-0"></span>Fig. 7 Hourly variations of a thermal efficiency and **b** exergy efficiency for an AISPBSS

Variations of cumulative yield for an AISPBSS at different  $m_f$  are shown in Fig. [6](#page-9-0)b. The daily productivity from an AISPBSS is maximum at minimum  $m_f$ . The daily productivity from an AISPBSS at  $m_f$  at 1.8, 3.2 and 4.7 kg/h is 7.5, 6.5 and 5.4 kg, respectively. The amount of distilled yield production from the AISPBSS mainly depends on the water temperature. It can be seen that at the minimum  $m_f$ , the basin water temperature is higher. It is found that the daily yield decreases up to  $14$  and  $28.14\%$  when  $m_f$  increases from 1.8 to 3.2 kg/h and from 1.8 to 4.7 kg/h, respectively.

Variations of thermal efficiency for an AISPBSS at different  $m_f$  are plotted in Fig. [7](#page-10-0)a. The highest thermal efficiency for an AISPBSS at  $m_f$  at 1.8, 3.2 and 4.7 kg/h is 62.24, 56.11 and 47.5%, respectively. It is found 43.71, 38.27 and 29.62% of daily average thermal efficiency for an AISPBSS at  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. The thermal efficiency of an AISPBSS is decreased when  $m_f$  is increased. There are 12.45 and 32.24% decreases in the daily average thermal efficiency of an AISPBSS when  $m_f$  is increased from 1.8 to 3.2 kg/h and from 1.8 to 4.7 kg/h, respectively.

Thermal effectiveness of the AISPBSS is given by (Manokar et al. [2018e\)](#page-21-20),

$$
\eta_{A,th} = \frac{m_{\rm ew} h_{\rm fg}}{[A_{\rm c} \times I_{\rm c}(t) + A_{\rm s} \times I_{\rm s}(t)] \times 3600} \times 100
$$
 (5)

Variations of the exergy efficiency for an AISPBSS under different  $m_f$  are shown in Fig.  $7b$  $7b$ . The maximum hourly exergy efficiency of an AISPBSS is 13.2, 10.6 and 8.7% at  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. The daily average exergy efficiency of 8.39, 6.94 and 5.07% is obtained for  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. An increase in  $m_f$ resulted in decreasing exergy efficiency of the AISPBSS. When  $m_f$  is increased from 1.8 to 3.2 kg/h and from 1.8 to 4.7 kg/h, the exergy efficiency of an AISPBSS decreased up to 17.3 and 39.4%, respectively. Table [4](#page-11-0) summarizes the positive outputs of productivity, energy efficiency and exergy efficiency by decreasing  $m_f$  in an AISPBSS.

The exergy efficiency of the AISPBSS is given by (Manokar et al. [2018e\)](#page-21-20),

$$
\eta_{\text{a.e}} = \frac{e_{\text{a,out}}}{e_{\text{p.in}} + e_{\text{fpc.in}}}
$$
(6)

2 Springer

S. no	Mass flow		Yield $(kg)$		Energy efficiency $(\%)$		Exergy efficiency $(\%)$	
	rate $(kg/h)$	Actual	$%$ Increase	Actual	% Increase	Actual	% Increase	
	4.7	5.4	Reference	29.62	Reference	5.07	Reference	
2	3.2	6.5	17	38.27	22.6	6.94	27	
3	1.8	7.5	28	43.71	32.2	8.39	39.6	

<span id="page-11-0"></span>**Table 4** Improvements in yield and the energy and exergy efficiency of the AISPBSS for different  $m_f$ 

The exergy output of the AISPBSS is given by (Manokar et al. [2018e](#page-21-20)),

$$
e_{\text{a.out}} = (m_{\text{d}} x h_{\text{fg}}) \left( 1 - \left[ \frac{T_{\text{a}} + 273}{T_{\text{w}} + 273} \right] \right) \tag{7}
$$

The exergy input of the AISPBSS is given by (Manokar et al. [2018e](#page-21-20)),

$$
e_{\rm a.in} = e_{\rm p.in} + e_{\rm fpc.in} \tag{8}
$$

The exergy input to the solar water heater is given by (Manokar et al. [2018e\)](#page-21-20),

$$
e_{\text{fpc.in}} = Q_{\text{u}} \left[ 1 - \frac{T_{\text{a}} + 273}{T_{\text{w}} + 273} \right] \tag{9}
$$

The heat attained by the solar water heater is given by (Manokar et al. [2018e\)](#page-21-20),

$$
Q_{\rm u} = \left(IxA_{\rm p}\right) - q\tag{10}
$$

The heat lost from the solar water heater is given by (Manokar et al. [2018e](#page-21-20)),

$$
q = UA(T_b - T_a) \tag{11}
$$

## **4.4 Efect of** *m***<sup>f</sup> on the solar panel power production, solar panel electrical, energy**  and exergy efficiency of the AISPBSS

Figure [8a](#page-12-0)-d shows the deviation of the solar panel temperature and solar panel efficiencies for an AISPBSS at different  $m_f$ . From Fig. [8a](#page-12-0)–d, it is noted that the panel temperature decreases with an increase in  $m_f$ . The PV panel temperature reached the maximum value of 63, 59 and 54 °C for  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. The daily average panel temperature at  $m_f$  at 1.8, 3.2 and 4.7 kg/h is 51.34, 49 and 44.56 °C, respectively. An increase in  $m_f$  resulted in decreases in panel temperature. The daily average panel temperature decreases up to 4.55 and 13.2% when  $m_f$  increases from 1.8 to 3.2 kg/h and from 1.8 to 4.7 kg/h, respectively.

It is noted that the maximum hourly PV panel power generation and efficiency from an AISPBSS at  $m_f$  at 1.8, 3.2 and 4.7 kg/h are 70.2, 74.1 and 80 watts and 8.6, 8.9 and 9.6%, respectively. Similarly, the daily average power generation and efficiency are 46, 50.88 and 55.16 watts and 7.13, 7.62 and 8.14% for  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. The power generation from an AISPBSS is increased with increasing  $m_f$ . It is found that there are 4.2 and 5.2% increases in the PV panel power production and the efficiency when the daily average PV panel temperature reduces up to 4.55%. Similarly, there are 11.4 and 12% increases in the PV panel power production and the efficiency when the daily average PV panel temperature reduces up to 13.2%.



<span id="page-12-0"></span>Fig. 8 Hourly variations of a solar panel temperature, **b** PV electrical efficiency, **c** PV thermal effectiveness and **d** PV exergy effectiveness for the different flow rates  $(m_f)$ 

The electrical efficiency of the PV panel is calculated by (Manokar et al. [2018e\)](#page-21-20),

$$
\eta_{\text{pv electrical}} = \frac{FF \times V \times I}{I_s(t) \times A_s} \times 100\%
$$
\n(12)

The thermal efficiency of the PV panel has the same trend as the solar panel electrical efficiency and it reached its maximal value of 20.76, 20.74 and  $23.13\%$  at  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. The daily average thermal efficiency of the solar panel is  $17.34$ , 18.30 and 19.69% at  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively.

The thermal efficiency of the solar panel is obtained by (Singh et al.  $2016$ ),

$$
\eta_{\text{pv thermal}} = \frac{FF \times V_{\text{oc}} \times I_{\text{sc}}}{0.38I_{\text{s}}(t) \times A_{\text{s}}} \times 100\%
$$
\n(13)

Figure [8a](#page-12-0)–c shows that the exergy efficiency of the PV panel is maximum at the minimum panel temperature. The daily average solar panel exergy efficiency is 18.32, 20.23 and 22.39% at  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. When  $m_f$  is increased from 1.8 to 3.2 kg/h and from 1.8 to 4.7 kg/h, the exergy efficiency of a PV panel increases up to  $9.5$ and 18.2%, respectively.

The exergy efficiency of the solar panel is calculated by (Singh et al. [2016](#page-22-8)),

<span id="page-13-0"></span>

$$
\eta_{\text{pv exergy}} = \frac{FF \times V_{\text{oc}} \times I_{\text{sc}} - VI}{0.933 I_{\text{s}}(t) \times A_{\text{s}}} \times 100\%
$$
\n(14)

2 3.2 50.88 9.6 7.62 6.4 3 4.7 55.16 16.6 8.14 12.4

Table [5](#page-13-0) shows the improvements made in the PV panel power production and efficiency by increasing  $m_f$  in an AISPBSS.

#### **4.5 Monthly power generation from the system at diferent** *m***<sup>f</sup>**

The monthly solar radiation data for the experimental place are obtained from the Atmos-pheric Science Data Center, NASA Surface Meteorology and Solar Energy—location<sup>[1](#page-13-1)</sup>

Monthly power generated from the solar panel is theoretically calculated by the following formula, $\frac{2}{3}$  $\frac{2}{3}$  $\frac{2}{3}$ 

$$
E = A \times r \times H \times PR \tag{15}
$$

Table [6](#page-14-0) shows the monthly power generation from the PV panel at different flow rates. From the table, it is identifed that the electrical power production from the solar panel is maximum on March month and minimum on November month for the average monthly solar intensity of 205.84 and 121.5 kWh, respectively. The annual electrical energy generation from the PV panel at  $m_f$  at 1.8, 3.2 and 4.7 kg/h is 101.96, 108.96 and 116.4 kWh, respectively. The annual energy generation from the panel at  $m_f$  at 3.2 and 4.7 kg/h is 6.43 and 12.41% higher than the minimum  $m_f$ .

#### **4.6 Environmental analysis**

### **4.6.1 Embodied energy**  $(E_{in})$

Total embodied energy is the total energy necessary to manufacture the AISPBSS (Eltawil et al. [2018;](#page-20-25) Saini et al. [2017](#page-21-21)). The embodied energy of the diferent components which are used in the present study is given in Table [7](#page-14-1).

#### **4.6.2 Energy payback period (EPBP)**

EPBP is the entire period essential to recover the total  $E<sub>in</sub>$  involved in manufacturing the system. It is defned as the ratio between the *E*in and *E*out (Eltawil et al. [2018;](#page-20-25) Saini et al. [2017](#page-21-21)) (Table [8](#page-14-2)).

<span id="page-13-1"></span><sup>1</sup> [https://eosweb.larc.nasa.gov/cgi-bin/sse/grid.cgi.](https://eosweb.larc.nasa.gov/cgi-bin/sse/grid.cgi)

<span id="page-13-2"></span><sup>2</sup> <http://photovoltaic-software.com/>.

S. no.	Month	Solar intensity $(kWh/$ /month)	Energy (kWh) $m_f = 1.8 \text{ kg/h}$	Energy (kWh) $m_f = 3.2 \text{ kg/h}$	Energy (kWh) $m_f = 4.7 \text{ kg/h}$
			$\eta_{\rm pv} = 7.13\%$	$\eta_{\rm pv} = 7.62\%$	$\eta_{\rm pv} = 8.14\%$
1	January	152.83	8.17	8.73	9.32
$\overline{2}$	February	164.92	8.81	9.42	10.06
3	March	205.84	11.00	11.76	12.56
$\overline{4}$	April	201.6	10.77	11.51	12.30
5	May	189.72	10.14	10.84	11.58
6	June	157.2	8.40	8.98	9.59
7	July	146.63	7.84	8.37	8.95
8	August	148.8	7.95	8.50	9.08
9	September	150.3	8.03	8.58	9.17
10	October	137.02	7.32	7.83	8.36
11	November	121.5	6.49	6.94	7.41
12	December	131.44	7.02	7.51	8.02
	Annual energy output $(E_{\text{out}})$		101.96	108.96	116.40

<span id="page-14-0"></span>**Table 6** Monthly power generation from the AISPBSS at different  $m_f$ 

<span id="page-14-1"></span>**Table 7** Embodied energy calculation data for the proposed AISPBSS

S. no.	Materials	Embodied energy (kWh/kg)	Weight (kg)	Embodied energy (kWh)
1	PV panel	1130.56 (kWh/m <sup>2</sup> )	$1.6 \text{ (m}^2)$	1808.896
2	Aluminum angle	43.1	0.5	21.55
3	glass	4.2	5	21
$\overline{4}$	Copper material	11.67	2	23.34
5	Wooden box	4.2	4	16.8
6	Steel stand	7	10	70
7	Storage tank	21.44	0.2	4.288
8	PVC pipe	25	3	75
Total embodied energy (kWh)				2040.874

<span id="page-14-2"></span>

$$
EPBP = \frac{E_{\text{in}}}{E_{\text{out}}} \tag{16}
$$

#### **4.6.3 Carbon dioxide (CO<sub>2</sub>) emission**

The average  $CO<sub>2</sub>$  emission for the coal-based thermal power plant is approximately 0.98 kg/kW (Singh et al. [2016](#page-22-8); Eltawil et al. [2018;](#page-20-25) Saini et al. [2017](#page-21-21)).

$$
Co_2 \text{emission per year} = \frac{E_{\text{in}}}{L} \times 2.042 \text{ kg}
$$
 (17)

#### **4.6.4 Net CO<sub>2</sub> mitigation**

The net  $CO<sub>2</sub>$  mitigation for the system is given by the difference between the total  $CO<sub>2</sub>$ mitigation and total CO<sub>2</sub> (Eltawil et al. [2018;](#page-20-25) Saini et al. [2017](#page-21-21)).

$$
\text{Net CO}_2 \text{ mitigation} = (E_{\text{out}} \times L - E_{\text{in}}) \times 2.04 \text{ kg} \tag{18}
$$

#### **4.6.5 Carbon credit**

If  $CO<sub>2</sub>$  discharge is being traded at 10 US\$/t of  $CO<sub>2</sub>$  mitigation, then the carbon credit earned by the system is given by (Eltawil et al. [2018](#page-20-25); Saini et al. [2017\)](#page-21-21).

The carbon credit earned = Net CO<sub>2</sub> mitigation (in t) 
$$
\times
$$
 10 US $\frac{\$}{t}$  (19)

#### **4.7 Variations of the overall thermal and exergy efficiency of the AISPBSS**

Variations of the overall thermal efficiency of the AISPBSS (thermal efficiencies of an AISPBSS and a PV panel) at different  $m_f$  are shown in Fig. [9](#page-16-0)a. The overall thermal efficiency of the AISPBSS is maximum at minimum  $m_f$ . When  $m_f$  increases, the thermal efficiency of the AISPBSS is decreased, whereas the thermal efficiency of the PV panel is increased. The maximum hourly overall thermal efficiency of the system is 83, 72.86 and 70.64% at  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. The daily average overall thermal efficiency of the system is 61.39, 57.44 and 51.37% at  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. It is concluded that there are  $6.43$  and  $16.33\%$  decreases in the daily overall thermal efficiency of the system when  $m_f$  is increased from 1.8 to 3.2 kg/h and from 1.8 to 4.7 kg/h, respectively.

The overall thermal efficiency of the AISPBSS is given by (Al-Nimr [2015](#page-20-21); Manokar et al. [2018e\)](#page-21-20),

$$
\eta_{\text{overallA.thermal}} = \frac{m_{\text{ew}} h_{\text{fg}}}{\left[A_{\text{c}} \times I_{\text{c}}(t) + A_{\text{s}} \times I_{\text{s}}(t)\right] \times 3600} \times 100 + \frac{FF \times V_{\text{oc}} \times I_{\text{sc}} - VI}{0.933 I_{\text{s}}(t) \times A_{\text{s}}} \times 100\%
$$
\n(20)

Figure [9b](#page-16-0) shows the overall exergy efficiencies of an AISPBSS at different  $m_f$ . The daily average exergy efficiency of the AISPBSS is about 8.39, 6.94 and 5.08%, daily average PV panel exergy efficiency is about  $18.32$ ,  $20.23$  and  $22.39\%$  and the overall average exergy efficiency of the AISPBSS is about 26.52, 27.14 and 27.40% at  $m_f$  at 1.8, 3.2 and 4.7 kg/h, respectively. The daily average exergy efficiency of the AISPBSS decreases with an increase in  $m_f$ , whereas the daily average exergy efficiency of the solar panel is increased.



<span id="page-16-0"></span>**Fig. 9** Hourly variations of **a** the overall thermal and **b** the overall exergy efficiency of the AISPBSS

The reduction in exergy efficiency of the AISPBSS and increases in panel exergy efficiency resulted in nearly equal overall exergy efficiency for all  $m_{\rm f}$ .

The overall exergy efficiency of the AISPBSS is given by (Al-Nimr [2015;](#page-20-21) Manokar et al. [2018e\)](#page-21-20),

$$
\eta_{\text{overallAexergy}} = \frac{\left(m_{\text{d}} \times h_{\text{fg}}\right)\left(1 - \left[\frac{T_{\text{a}} + 273}{T_{\text{w}} + 273}\right]\right)}{\left(A_{\text{s}} \times I_{\text{t}}\right)\left[1 + \left(\frac{1}{3}\left[\frac{T_{\text{a}} + 273}{6000}\right]^4 - \frac{4}{3}\left[\frac{T_{\text{a}} + 273}{6000}\right]\right)\right] + Q_{\text{u}}\left[1 - \frac{T_{\text{a}} + 273}{T_{\text{w}} + 273}\right]} \tag{21}
$$

$$
+ \frac{FF \times V_{\text{oc}} \times I_{\text{sc}} - VI}{0.933I_{\text{s}}(t) \times A_{\text{s}}} \times 100\%
$$

#### **4.8 Comparison of yield of various types of ISS**

The comparison of productivity of various types of the ISS is given in Table [9](#page-17-0). The productivity was maximum in the case of the solar still incorporated with the electrical heater (yield—12  $L/m^2$ ) (Abdallah et al. [2009\)](#page-19-1). The PV panel-integrated ISS without any insulation created the productivity of 4.4 kg (Manokar et al. [2018d](#page-21-12)). In the present study, AISPBSS produced the daily productivity of 7.5 kg. An active mode enhances the productivity up to 41.33% than the passive mode.

# **5 Conclusions**

In drinking water and electricity scarcity region, solar still desalination is popular. Especially in desert region, government is struggling to meet the demand of drinking water and electricity. The PV panel-integrated ISS is a good option which fulflls the need of both electricity and drinking water. The results inferred that solar panel power generation mainly depends on the both panel temperature and solar intensity. In this study, the solar panel performance was improved by increasing  $m_f$ . But increasing  $m_f$  reduces the performance of an AISPBSS. When  $m_f$  is varied from 1.8 to 3.2 kg/h, the daily productivity and

<span id="page-17-0"></span>



thermal, exergy and overall thermal efficiency of the system are decreased about 14, 12.45, 17.3 and 6.43%, respectively, and the solar panel power production and electrical, exergy and overall exergy efficiency are enhanced up to  $4.3$ ,  $5.2$ ,  $9.5$  and  $2.29\%$ , respectively. Further  $m_f$  is varied to 4.7 kg/h, the daily productivity and thermal, exergy and overall thermal efficiency of the system are decreased about  $28.14$ ,  $32.24$ ,  $39.4$  and  $16.33\%$ , respectively, and solar panel power production and electrical, exergy and overall exergy efficiency are enhanced up to 11.4, 12, 18.2 and 3.23%, respectively.

# <span id="page-19-3"></span>**Appendix**



The uncertainty of instruments is calculated based on the internal uncertainty of instrument  $(U)$  and average values of experimental results  $(X)$ . The value of  $U$  is mathematically expressed as,

$$
U = \frac{\sqrt{\sigma_1^2 + \sigma_2^2 + \sigma_3^2 + \sigma_4^2 + \sigma_5^2 + \sigma_6^2 + \dots + \sigma_n^2}}{N}
$$

Similarly, the value of  $\sigma$  (standard deviation) is expressed as,

$$
\sigma = \frac{\sqrt{\sum (X - \bar{X})}}{N}
$$

The uncertainty (%) is calculated as,

Uncertainty percentage = 
$$
\frac{U}{x} \times 100\%
$$

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