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Properties of lightweight fibrous structures made by a novel foam forming technique

S. R. Burke · M. E. Möbius · T. Hjelt · S. Hutzler

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Abstract We describe a novel method for the production of lightweight fibrous structures of densities as low as 8.8 kg m⁻³. The method is based on the use of liquid foam as a carrier medium for dispersed Kraft fibres. Different to the process of foam forming, where the quick removal of the foam results in the formation of thin fibrous sheets, our samples are allowed to slowly drain and dry until all foam has disappeared. This procedure results in bulk samples whose height (up to 25 mm) and density are controlled

by initial fibre concentration and liquid fraction of the foam. Above a minimum density, the compression modulus of elasticity of the samples increases linearly with density. Furthermore, we show compressive strength of the structures being controlled via the initial liquid fraction of the foam, making this an important process parameter for the fabrication of such structures.

S. R. Burke (⊠) · M. E. Möbius · S. Hutzler School of Physics, Trinity College Dublin, The University of Dublin, Dublin, Ireland e-mail: Burkes24@tcd.ie

T. Hjelt VTT Technical Research Centre of Finland Ltd., Espoo, Finland

Graphical abstract



Introduction

Non-woven fibrous structures made from natural materials find many applications, including thermal insulation (Poehler et al. 2017), acoustic dampening, and visually pleasing wall panels (Härkäsalmi et al. 2017). Here we describe a novel technique for producing bulk materials from northern bleached softwood Kraft fibres. The technique involves the initial dispersion of the fibres in a liquid foam which is then slowly dried. Height, density and compressive strength of the samples can be tuned via the fibre concentration and the initial liquid fraction ϕ_i of the foam, defined as the fraction of liquid contained in the foam to the total volume of the foam. Figure 1 shows an example of the low density fibrous structure, together with the pulp sheet of Kraft fibres from which



Fig. 1 Low density fibrous structure (right) obtained using the foam-forming technique described in the text. The sample was produced from a thin sheet of compressed Kraft fibres, as shown on the left



it was made. The density of the sheet is 450 kg m⁻³, while that of the structure on the right is 25 kg m⁻³. Both the sheet and the foam-formed structure in the figure contain the same mass of fibres.

The use of foam for the formation of pulp sheets dates back to the early 1960s (Radvan 1964). Surfactant is added to an aqueous solution of fibres, which is then agitated to produce a foam dispersion containing fibres. The bubbles in the foam act as spacer particles between fibres, preventing their flocculation. If the foam is quickly removed via suction, this results in sheets of fibres with a greater uniformity than may be achieved in water-based papermaking, in particular when long fibres are used (Al-Qararah et al. 2012; Lehmonen et al. 2013). If the foam is allowed to drain freely it is possible to create three dimensional fibrous materials (Alimadadi and Uesaka 2016).

An advantage to the foam-forming method is that it allows for a control of porosity via the control of the average bubble size. For sheets it was shown that their density is decreased by using longer fibres which allow for more and/or larger bubbles to aggregate between them, while fibre-fibre contacts are still maintained (Madani et al. 2014). As the foam is removed this results in larger voids, and thus decreased sample density. The initial liquid fraction of the foam, ϕ_i , is a further control parameter for varying sheet density (Madani et al. 2014). Also fibreorientation may be controlled by the use of foam. Compared to water-formed structures, where there is a tendency for the fibres to orientate in the horizontal plane, fibres dispersed in foam were found to orientate through a broad range of angles in a 12 mm thick sample produced by Alimadadi and Uesaka 2016.

In the following we describe a novel, foam based process for the production of lightweight fibrous structures. Allowing the foam to drain freely results in sample heights exceeding that of previously published work, where immediately after the foam has been poured into the drainage vessel a vacuum is applied from below (Alimadadi and Uesaka 2016). The description of our method is followed by demonstrations of how density and compressive strength can be tailored via the choice of fibre concentration and initial liquid fraction of the foam.

Adding foam to the production process of fibrous materials thus allows for a much greater control of their properties.

Sample preparation

The samples described in the following were made from bleached and dried softwood Kraft fibres with average length 2.0 ± 0.1 mm and diameter of 35 µm, and thus an aspect ratio of approximately 60 (Al-Qararah et al. 2013). As a surfactant we used commercial SDS from Sigma-Aldrich with a purity of 98.5%.

Sample preparation is illustrated in Fig. 2. Disintegration of dry pulp fibre sheets was achieved by soaking them in a specified amount of water for 24 h (Al-Qararah et al. 2013). The samples described below were produced with weight to weight ratios (referred to as fibre concentration) ranging from 1 to 6.25%. Following this, the aqueous fibre suspension is placed into a vessel and sheared with a mixing disk at a constant speed (5000 RPM) for 3 min. The diameter of the mixing disk was 50 mm, with two opposing 25° bends. The design of the disk allows air to be drawn into the suspension during shearing. SDS is then added at a weight per weight (w/w) concentration of 0.66%, in practice 1 g of SDS per 150 ml of water and thus above the critical micelle concentration of 2.3 g/L. The aqueous dispersion is foamed up by shearing once again for 3 min. The use of such a high surfactant concentration is necessary to create foams which are stable for a longer time period than the few seconds that is required for the foam forming of paper sheets (Lee et al. 2014).

The initial volume of the aqueous fibre suspensions ranged from 300 to 600 ml; this resulted in a final volume of fibre containing foam of 1200 ml, corresponding to initial average liquid fractions ϕ_i of 0.25, 0.33, 0.42 and 0.50 for the samples described below.

The fibre-containing foam was then poured into a container (width 125 mm, length 200 mm, depth 50 mm) with a wire mesh (50 μ m hole size) as a base (Fig. 2b) to allow the liquid to drain from the foam.

A rigid plastic sheet was placed on top of the container during this drying process. The plastic sheet did not touch the fibre-foam, nor did it make an airtight seal. However, we found through initial experiments that the sheet plays a crucial role, particularly for samples with lower fibre concentrations, which would collapse completely without its presence. The sheet reduces the evaporation of the liquid and creates a pressure gradient that slows down the drainage; the resulting extension of the drying time may contribute to a better bonding of the fibres, enabling us to reduce

Fig. 2 Sketch of the experimental set-up used to create foam-formed fibrous structures. a Steps taken to create a foamed fibre dispersion. After shearing, the dispersion is poured into a container with a wire gauze base. b A non-airtight plastic cover is placed on top. The foam is then left to drain under gravity. As the sample dries out eventually all the bubbles disappear, leaving a three dimensional fibre network



the minimum fibre concentrations required for mechanically stable structures.

After approximately 12 h of drying we uncover the plastic sheet and remove the sample, together with the mesh that supports it, from the container. Doing so speeds up the drying time by exposing more of the surface area to air. At this point it is observed that all the foam has decayed from the structure, however there is still a significant volume of liquid contained within. When the samples are dry to the touch we monitor their weight at regular intervals until the drying has effectively ceased (see "Drying process" section).

The dried samples are then carefully removed from the mesh and cut into equal sized pieces using a surgical scalpel (see Fig. 3). The dimensions of each piece are 33 mm by 33 mm, with a height that is dependent on fibre concentration, as discussed in "Variation of sample height with fibre concentration" section.

Figure 1 shows a foam-formed three dimensional fibre structure alongside a fibre sheet. Both samples contain the same type and mass of fibres. However, there is a large difference between the densities of both, the sheet on the left has a density of 450 kg m⁻³, while the density of the foam-formed structure is 25 kg m^{-3} .

Drying process

The rate at which the samples dry varies with time; it is also dependent on the concentration of fibres used. Figure 4 shows the ratio of the total sample mass m_d to

Fig. 3 Top view of a foam-formed fibrous structure that has dried but has not yet been cut into samples for further testing. The average height of the structure shown is 25 mm

the total fibre mass m_0 for one sample from the initial pouring of the fibre laden foam until the sample has fully dried. The data was obtained by placing the fibrefoam dispersion onto a mass balance, the liquid was able to drain from the sample, which was supported by the wire gauze.

Immediately after the fibre-foam dispersion has been poured into the container, the ratio m_d/m_0 decreases very rapidly, as gravitationally induced drainage removes most of the liquid from the foam within the first few minutes (Haffner et al. 2017). This regime can be described by a numerical solution of the foam drainage equation (Verbist et al. 1996) (see inset of Fig. 4).

As drainage slows down and eventually stops, further drying is mainly due to evaporation. This is initially accompanied by the rupturing of foam films, but then also due to the evaporation of liquid attached to fibre surfaces and at fibre-fibre contacts. A higher concentration of fibres will allow more water to attach to fibres and is therefore responsible for the slow-down in drying that we observe in this case.

We can define a "drying time" T_d as the time it takes for the sample to reduce its weight to 0.95 times the weight of the initial fibres, to within \pm 5% of the mass of fibres, allowing for any fibre loss that may have occurred during the pouring stage. The typical drying times of about $T_d \simeq 40$ h found for our experiments are impractical for any large-scale production of fibrous samples. Several techniques are available for the reduction of T_d , such as placing samples into an oven, impingement-infrared drying, as well as other methods, such as impingement drying under vacuum (Timofeev et al. 2016). Impingement drying is well suited to the fibrous samples due to the porosity of both the structure and the gauze it is formed on. The technique consists of blowing hot air through the sample, which is then recirculated back to a air drier where the moisture is extracted. The benefit of this technique is that it can evenly and rapidly dry the samples, unlike oven drying, which usually dries the outermost part of the samples first (Timofeev et al. 2016). We will address the possible shortening in drying times of our samples in future work.





Fig. 4 Drying curve for a fibre-foam dispersion containing 3% fibre concentration showing the ratio of the mass of the dispersion to the mass of the fibres (m_d/m_o) as a function of time. The accelerated mass loss in the initial 20 min (inset), is due to gravitationally induced foam drainage and can be

Sample characterisation

We analysed our samples in terms of homogeneity (local density), sample height as a function of fibre concentration, and compression modulus. Here, fibre concentration is defined by the weight of fibres added to the weight of liquid (before foaming). Each quantity was determined by averaging the measurements from four samples produced under the same conditions. In our experiments fibre concentrations ranged from 1 to 6.3%.

Sample uniformity

Most practical applications of fibrous structures require a uniform sample density. Our structures dry under gravity which may lead to a vertical density variation. We have probed for this by measuring optical absorption in 1 mm thick slices of our samples. To achieve such thin slices we placed the sample in a holder, with a 1 mm protruding edge which is then cut using a thin surgical scalpel.

An LED backlight was placed behind each slice and images were taken using a digital camera (Canon EOS 50D). The images were then converted to greyscale and ImageJ (Schneider et al. 2012) was used to

modelled using the foam drainage equation. Further mass loss is mainly due to evaporation of liquid. After 21 h the sample was removed from the container, doing so increases the rate of evaporation by exposing a larger surface area, as is evident by the sharp decrease in m_d/m_0

compute an average grey value through the horizontal plane of each sample. The resulting grey value was then plotted as a function of sample height. In order to smooth the profiles we averaged the results over four slices to reduce the contribution any single large void would have on the overall distribution.

The light transmitted through the sample is represented by the greyscale value, i.e. a reduction in transmittance indicates a higher fibre content. The transmission data thus provides a (qualitative) measure of sample uniformity.

Figure 5 shows photographs of the thin slices, as well as the averaged profiles for fibre concentrations of 2.4%, 3.3% and 6.3%, respectively. In all cases both top and bottom of the profiles feature a peak which represents sample edges. The steep curves, rather than an abrupt drop at the top and bottom is due to the edges of the sample being orientated slightly off plane to the plane of the pixels.

The data indicates that an increase in fibre concentration leads to a decrease of the gradient in the sample profiles. The fibre concentration of 6.3% results in a nearly uniform profile away from top and bottom of the sample. The increased density of the samples made from higher fibre concentrations also leads to reduced



Fig. 5 The graphs on the left show measurements of optical transmittance for samples obtained with different fibre concentrations (c). (x-axis: sample height in pixels). The straight line fit to the data (dashed line) shows that sample uniformity away

sample transmittance, i.e. lower greyscale values, as seen in Fig. 5.

Our samples differ greatly from the ones made by (Haffner et al. 2017), also produced via foam forming, but in narrow vertical cylinders of 150 mm in length. In this case drainage of the liquid resulted in a sharp downward gradient of fibre concentration, presumably due to the large volume of liquid drained per cross-sectional area of foam. Also, unlike the experiments carried out here, there was no mesh to act as a stable platform to support the drying fibre structure after the foam had drained.

Variation of sample height with fibre concentration

For all our experiments we kept the initial volume (hence height) of the fibre-foam dispersions constant

Deringer

from top and bottom increases with fibre concentration. The photographs on the right shows the height variation of the samples with an increase in fibre concentration, see also Fig. 6

at 1200 ml. After pouring the fibre-foam into the vessel, the height of the dispersions decreased as drainage and drying took place, asymptoting to a constant value, provided a minimum fibre concentration is exceeded, see section "Stress–strain behaviour under uni-axial compression". This height is reached long before the sample has reached the drying time T_d , defined in section "Drying process". An increase of fibre concentration leads to an increase of up to 20% in the final height (defined as height at time T_d), as shown in Fig. 6. This is presumably due to the increased number of fibre-fibre-contacts being formed during the initial decay of the foam.

Fig. 6 The final height of the fibrous structures increases with fibre concentration. Each data point is an average over four samples, the dashed line indicates a linear trend. The data shown is for the samples made from fibrefoam dispersions with an initial liquid fraction of $\phi_i = 0.42$, a similar trend was also observed for other values of ϕ_i



The final sample density ρ is controlled by the fibre concentration *c* used in its preparation, as shown in Fig. 7a. The increase is linear in *c* but a minimum concentration $c_{crit} \sim 0.6\%$ is required for sample stability, see section "Stress–strain behaviour under uni-axial compression". The rate of increase scales roughly linearly with the initial liquid fraction ϕ_i of the foam, see Fig. 7b, highlighting its role as a control parameter in sample production.

Stress-strain behaviour under uni-axial compression

We tested the mechanical strength of the dried samples by subjecting them to uni-axial compression. The samples were placed in a rheometer (Anton Paar Physica MCR301) with a plate-plate configuration (Plate diameter 50 mm). All our samples had a contact area of 33 mm by 33 mm. Stress–strain curves were obtained by applying an increasing load to the sample and measuring the resulting deformation up to a maximum strain of 0.6. For each sample density the tests were carried out on four samples and the results were then averaged.

Figure 8 shows the stress–strain curves for samples produced with fibre-foam dispersions of $\phi_i = 0.25$. Similar curves were obtained for initial liquid fractions of 0.33, 0.42 and 50. The compression modulus

of elasticity E_c (BS EN826 1996) is given by the slope of the initial linear increase of the stress-strain data, see inset of Fig. 8. Figure 9 shows the compression modulus computed from fits over a strain of 0.15 as a function of sample density for samples produced with four different values of ϕ_i . In all cases E_c increases linearly with sample density. Linear extrapolation of the data leads to a minimum sample density ρ_c , dependent on ϕ_i , which is required for mechanical stability, i.e. $E_c > 0$. Above ρ_c the data is described by

$$E_c = s(\phi_i)(\rho - \rho_c(\phi_i)) \tag{1}$$

Figure 10a shows that the minimum sample density ρ_c varies roughly linear with ϕ_i . These values are in line with $\rho_c = 5 \text{ kg m}^{-3}$, as reported by Alimadadi and Uesaka (2016). Also the slope $s(\phi_i)$ (Fig. 10b), varies linearly with the initial liquid fraction for $\phi_i \ge 0.22$. The minimum fibre concentrations c_{crit} corresponding to the minimum sample densities $\rho_c(\phi_i)$, were obtained by inserting the values of $\rho_c(\phi_i)$ into the fits to the data in Fig. 7a. This results in values of c_{crit} around 0.6%.

Figures 7 and 9 demonstrate that both the sample density and compressive strength can be controlled by varying the initial liquid fraction of the fibre-foam dispersions. In particular, Fig. 9 shows that samples of a similar density can have a range of compressive strengths which are determined by the initial liquid fraction. Two of our samples highlight this point. The first was produced from a fibre-foam dispersion with



Fig. 7 a Variation of sample density ρ as a function of fibre concentration c for samples produced with Kraft fibres. For all values of initial liquid fraction we find $\rho \propto c$, however, there is a minimum fibre concentration c_{crit} below which no stable structures can be formed (see section "Stress-strain behaviour under uni-axial compression"). Each data point is an average over four samples. b The constant of proportionality, ρ/c , scales linearly with the initial liquid fraction of the foam



an initial liquid fraction of 0.25 and contained a 5% fibre concentration. The second sample was made from a fibre-foam dispersion of an initial liquid fraction of $\phi_i = 0.42$ and a 3% fibre concentration. The structures have similar densities (26 kg m⁻³ and 25 kg m⁻³ respectively), since the mass of fibres in each dispersion was almost the same. However, the compression modulus of the samples produced with the higher initial liquid fraction is almost seven times that of the samples produced with a lower initial liquid fraction.

Fibre network and percolation theory

The experimental finding that a finite sample density is required for sample stability, i.e. compression modulus $E_c > 0$ (Fig. 9), allows us to make a connection to percolation theory (Gu et al. 2016). Equation (1) can be re-expressed in terms of a volume fraction of fibres in the sample, $\phi_v = \rho/\rho_f$ where ρ_f is the fibre density ($\rho_f = 1500$ kg m⁻³) and ρ is the sample density (Al-Qararah et al. 2016). This results in

$$E_{c} = E_{c,0}(\phi_{i})(\phi_{v} - \phi_{v,c}(\phi_{i})), \qquad (2)$$

10

Fig. 8 Stress-strain curves for three dimensional fibrous structures for four different sample densities, produced from foams with $\phi_i = 0.25$. Each data point is averaged over four experimental runs carried out with four individual samples. The inset shows the initially linear part of these data sets, where the stress is proportional to strain



0.6

Fig. 9 Variation of compressive modulus E_c with sample density. Linear extrapolation of the data suggests that there is a lower limit to the density of the structures. The corresponding

where, as before, ϕ_i is the initial liquid fraction of the foam used in producing the sample. The value of the constant $E_{c,0} = s(\phi_i)/\rho_f$ is determined by the material properties of the fibres (length, cross-section, density, elastic modulus) as well as by the structure of the network. From Fig. 10a we then obtain that the value

critical densities for the range of initial liquid fractions ($\phi_i = 0.25, 0.33, 0.42$ and 0.50) were found to be 3.2 kg m⁻³, 4.4 kg m⁻³, 6 kg m⁻³ and 7.2 kg m⁻³ respectively

of the critical volume fraction $\phi_{v,c}(\phi_i) = \rho_c(\phi_i)/\rho_f$ varies linearly between 0.002 and 0.005.

Gu et al. (2016) performed computer simulations of fibre networks. For a fibre aspect ratio of approximately 60, as for the fibres in our experiments they report a critical volume fraction $\phi_{\nu,c}$ of about 0.005, consistent with our data.

Fig. 10 a The minimum sample density $\rho_c(\phi_i)$, from the fits to the data in Fig. 9 and equation 1, scales linearly with initial liquid fraction. b The rate at which the compressive strength of the structures scales with density is also dependent on the initial liquid fraction



Note however that these authors studied networks formed from randomly distributed fibres. A preliminary analysis of our samples suggest that there is some fibre alignment. We will carry out X-ray scans of our samples to determine how this alignment correlates with the initial liquid fraction of the foam. This should elucidate the origin of the dependence of both $E_{c,0}$ and $\phi_{v,c}$ on the initial liquid fraction ϕ_i .

Conclusions and Outlook

We have described how a foam forming process can be used to produce lightweight three dimensional fibrous structures, using Kraft fibres. Their height and densities can be controlled by the fibre concentration and the initial liquid fraction of the fibre-foam dispersion. The densities of our fibrous structures ranged from 8.8 to 46 kg m⁻³. Sample density varies linearly with fibre concentration. From uni-axial compression tests we found a linear increase also of the compression modulus with sample density. There is a lower density limit below which samples are no longer mechanically stable corresponding to the percolation threshold of fibre networks. The initial liquid fraction of the foam is an important control parameter over both sample density and compressive strength. X-ray imaging will be required to relate these sample properties to the structure of the fibre network (isotropy, alignment). The obvious shortcoming in the current production of these fibrous samples is the long time required for their drying. Several methods exists for shortening this (detailed in section "Drying process") and we will address this in future work, together with an analysis of the shape of the drying curves.

The foam forming technique introduced here can be applied to produce a variety of structures from a range of fibre types; we have successfully produced similar structures using fibres from peat and spent grain. This will broaden the range of applications for such nonwoven fibrous materials (Härkäsalmi et al. 2017). The compressive strength of the structures can be greatly increased with the addition of a bonding agent (PVA) to the process as found in our preliminary work.

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