

Accessibility of hydroxyl groups in birch kraft pulps quantified by deuterium exchange in D₂O vapor

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Abstract Deuterium exchange in a deuterium oxide (D₂O) atmosphere (95 % relative humidity), quantified by a dynamic vapor sorption (DVS) apparatus, was applied for assessing the accessibility of hydroxyl groups in birch kraft pulps. Achieving the maximum deuteration level exhibited slower kinetics than was earlier reported for experiments with ground wood and bacterial cellulose. The deuterium exchange process followed two parallel phenomena. Applying multiple drying and rewetting cycles gave kinetic information also on the hornification phenomenon occurring during these cycles. Dry birch pulps treated with sodium hydroxide solution of varying alkalinities at elevated temperatures were assessed for their accessible hydroxyl groups by DVS with deuterium exchange. This method was evaluated against deuteration combined with Fourier transform infra-red

spectroscopy and water retention value (WRV). DVS measurements were in correlation with WRV and both the methods indicated that an alkaline treatment of dry birch pulp improves cellulose accessibility. The level of irreversible deuteration also decreased as the alkalinity was increased. DVS was shown to provide quantitative information on the accessibility but to be a time-consuming method for the pulp samples. A potential means to decrease the duration of the measurement is increased D₂O exposure by excluding the drying phases.

Keywords Accessibility · Birch · Deuteration · Dynamic vapor sorption · Infrared spectroscopy · Water retention value

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Introduction

Cellulose accessibility, a term for the accessibility of the hydroxyl groups in cellulose, has been of increasing interest lately. Manufacture of novel cellulosic products, such as biofuels, nanocrystals and nanofibrils, require chemical modification of cellulose or even its dissolution in some cases. Cellulose accessibility can be considered a decisive factor during these heterogeneous chemical or biochemical treatments. In the past, cellulose accessibility was of interest mainly because of the importance of water retention properties of pulps in papermaking. Development of the

reactivity of pulps during their processing has been studied widely (Pönni et al. 2012), e.g., during drying (Minor 1994; Nazhad and Paszner 1994; Weise 1998; Fernandes Diniz et al. 2004), chemical pulping (Hult et al. 2001; Fahlén and Salmén 2003, 2005; Pönni et al. 2014), and paper recycling (Howard 1990; Nazhad and Paszner 1994). The factors affecting the accessibility include pulp properties, such as hemicellulose (Oksanen et al. 1997) and acidic group content (Lindström and Carlsson 1982; Lindström 1992), and process parameters, such as temperature and pH (Maloney and Paulapuro 2000; Fahlén and Salmén 2003). Despite the vast research in the past, the question still remains: how to improve cellulose accessibility?

Alkaline treatments are known to improve cellulose accessibility (Klungness 1974; Lindström and Carlsson 1982; Lindström 1992; Weise et al. 1998). Especially strongly alkaline pretreatments for cellulosic raw materials have been studied since the mercerization process was developed (Mercer 1851) to improve the strength and appearance of cotton fibers. In mercerization (>8–9 % NaOH) the most severe changes occur in the crystallinity of cellulose (McKenzie and Higgins 1958; Philipp et al. 1959; Dinand et al. 2002; Kljun et al. 2011). The strong alkaline treatment swells the native cellulose I which after washing forms another allomorph, cellulose II (Klemm et al. 1998). In cellulose I the polymer chains are parallel, whereas cellulose II is considered to be formed of antiparallel chains (Nishiyama et al. 2000; Dinand et al. 2002).

Swelling of cellulose, in general, refers to the loosening of the intermolecular interactions relative to the competing interactions with the swelling agent, commonly water. Alkali improves the swelling of the aqueous cellulose suspensions due to ionization of the hydroxyl groups and cleavage of inter- and intramolecular hydrogen bonds (Klemm et al. 1998). The maximum in swelling is obtained at approximately 10 % NaOH concentration, slightly depending on the cellulosic raw material (Saito 1939). In addition, the alkaline treatments are known to dissolve hemicelluloses (Sjöström and Enström 1967).

To date, there has not been a single method that could directly quantify the amount of accessible hydroxyl groups in cellulosic materials, i.e. cellulose accessibility. Jayme (1944) introduced the first widely accepted analytical method to approximate the accessibility of cellulose, namely the water retention value

(WRV), lately standardized as the ISO 23714:2007 method. WRV describes the amount of water retained on pulp under standard centrifugal forces. Commonly, WRV is approximated to present the amount of water inside the cell wall (Jayme 1944, 1958). Fiber saturation point (FSP), measured as a volume that high molecular weight dextran cannot occupy, is another widely accepted method to quantify the cell wall bound water (Stone and Scallan 1967; Maloney et al. 1999). In addition, cellulose accessibility has been related with pore size distribution of fiber wall measured by a number of techniques including solute exclusion (Stone and Scallan 1967, 1968), thermoporosimetry conducted with differential scanning calorimetry (DSC) by the isothermal melting technique (Maloney et al. 1998; Wang et al. 2003), DSC combined with thermogravimetric analysis (TGA) (Park et al. 2006), nuclear magnetic resonance (NMR) cryoporosimetry (Gane et al. 2004; Östlund et al. 2010), and inverse size-exclusion chromatography (ISEC) (Berthold and Salmén 1997). In addition, many techniques that can visualize changes in the size and aggregation of microfibrils have been used to show reduction in cellulose accessibility. These methods include transmission electron microscopy (TEM) (Billosta et al. 2006), NMR spectroscopy, and atomic force microscopy (AFM) (Hult et al. 2001; Fahlén and Salmén 2003, 2005; Lee et al. 2007).

A more direct method to analyze the changes in cellulose accessibility is deuteration combined with Fourier transform infra-red (FT-IR) spectroscopy, a technique that has been widely applied for native cellulose, cellulose derivatives, pulp, and wood (Jeffries 1963; Tsuchikawa and Siesler 2003a, b; Hofstetter et al. 2006). Lately, this method was successfully implemented to evaluate changes in cellulose accessibility during various treatments of wood and pulps including their drying and wet thermal treatments (Suchy et al. 2010a, b; Pönni et al. 2013, 2014). The method is based on deuteration of the accessible hydroxyl groups prior to the treatment to be studied (Frilette et al. 1948; Mann and Marrinan 1956). After the treatment in deuterium oxide (D_2O) and subsequent washing with water, the extent of the irreversible deuteration can be considered as a measure of decrease in the accessibility of hydroxyl groups in the sample. However, this method has so far not been standardized to give a precise number for the change in the accessible hydroxyl groups.

Recently, dynamic vapor sorption (DVS) with deuterium exchange was applied for bacterial cellulose and wood to determine the amount of their accessible hydroxyl groups (Lee et al. 2011; Rautkari et al. 2013). When protons in the accessible hydroxyl groups are exchanged for deuterons, the mass of the sample increases and this increase can be quantified with a highly sensitive ultrabalance in the DVS apparatus. On contrast to other methods, DVS with deuterium exchange provides the actual number of accessible hydroxyl groups in the sample. The principle of the method was proposed already in the 1960s (Morrison 1960; Sepall and Mason 1961). Previously, DVS has been applied commonly to assess the water vapor sorption behavior of various materials including wood (Sharratt et al. 2011; Hill et al. 2012), natural fibers (Kohler et al. 2003; Xie et al. 2011; Hill et al. 2009; Okubayashi et al. 2004, 2005) and microcrystalline cellulose (Kachrimanis et al. 2006).

In this paper deuterium exchange in DVS was applied for quantifying accessible hydroxyl groups in birch kraft pulp. WRV and deuteration combined with FT-IR spectroscopy were used as reference methods. The potential of deuterium exchange coupled with DVS for studying drying induced changes in cellulosic materials is discussed. The advantages and disadvantages of the method are critically reviewed.

Experimental

Materials

Industrially dried fully bleached birch pulp (kappa number 0.7, viscosity 674 ml g⁻¹) was obtained from a Finnish pulp mill. The dry pulp was soaked overnight in an excess of water and manually disintegrated. To set the alkalinity during alkaline pretreatments of the pulp, 8 M aqueous NaOH was prepared from solid NaOH pellets (VWR, Leuven, Belgium). For converting the pulp to the Na⁺-form for WRV analysis an aqueous solution of NaHCO₃ was prepared from solid 99.5 % NaHCO₃ (Merck, Darmstadt, Germany). In addition to NaHCO₃, 0.1 M NaOH and HCl were applied (Merck, Darmstadt, Germany). Water was purified in a Milli-Q system (Millipore Corporation, resistivity 18.2 MΩ cm). D₂O (99.9 atom% D, Sigma Aldrich, St. Louis, USA) was used for deuteration.

DVS with deuterium exchange

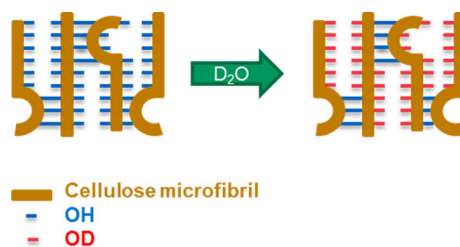
The amount of accessible hydroxyl groups in the pulp was quantified by measuring its mass increase during deuterium exchange in a DVS elevated temperature (ET) apparatus (Surface Measurement Systems, UK) with a measuring accuracy of 0.1 μg and chamber volume of 100 cm³. Approximately 10–30 mg of pulp was placed in the sample pan and preconditioned at 0 % relative humidity (RH) with dry nitrogen gas flow (200 cm³ min⁻¹) at 25 °C until the change in the mass of the sample was <0.002 % min⁻¹ over a 30 min period. Multiple (15–30) adsorption–desorption cycles with alternating RH between 0 and 95 % (dry N₂ and D₂O vapor) were then conducted. During the cycles, the DVS apparatus maintained a constant RH until the change in the sample mass was <0.002 % min⁻¹ over a 10 min period to ensure a constant equilibrium condition after each RH step. The amount of accessible hydroxyl groups in the sample was calculated according the Eq. 1 with the approximation that atomic mass difference between deuterium (²H) and protium (¹H) is 1 g mol⁻¹:

$$A = (m_f - m_i)/m_i \times 1000 \text{ (mol/kg)} \quad (1)$$

where A is the amount of accessible hydroxyl groups per dry mass of the sample, m_i is the dry weight of the sample prior to exposure to D₂O vapor, and m_f is the dry weight of the sample after the multiple DVS cycles. Scheme 1 illustrates the conversion of the accessible OH groups into OD groups as the RH of the mixture of dry N₂ and D₂O vapor is increased from 0 to 95 % in the DVS chamber.

Alkali treatment of pulp in D₂O and water

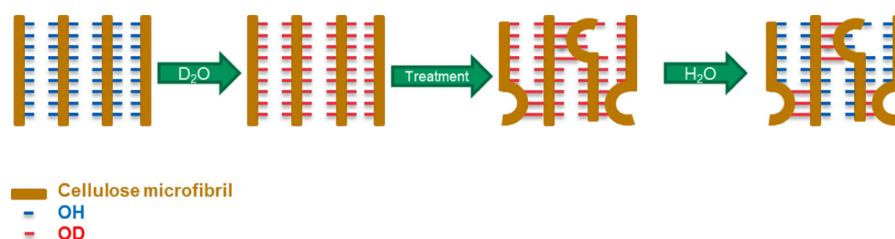
The disintegrated pulp was treated in plastic bags for a period of 2 × 20 min with an excess of D₂O, namely



Scheme 1 Principle of the deuteration of accessible hydroxyl groups during exposure to D₂O vapor at 95 % RH in DVS chamber

20 ml of D₂O per 1 g of dry pulp to convert all the accessible hydroxyl groups to OD groups. The sufficiency of time for the reversible deuteration and reprotonation was discussed in an earlier paper (Suchy et al. 2010b). The slurry was mixed twice during the 20 min by kneading. Between the deuteration treatments, D₂O was squeezed out of the bag before fresh D₂O was added. After the deuteration, the pulp was immediately subjected to an alkaline treatment.

The deuterium exchanged pulp was treated at 5 % consistency in D₂O and varying alkalinity (0.25–2 M) in plastic bags in a temperature controlled oven at 90 °C for 4 h. The influence of the applied aqueous NaOH solution on the level of deuteration was taken into account when processing the data. After the treatment, the pulps treated were washed twice with 100 ml of water per 1 g of dry pulp, allowing the suspension to stand for 20 min at room temperature before filtration. The alkali treatments for WRV and DVS analysis were carried out similarly but using water instead of D₂O. Scheme 2 illustrates the principle of deuteration of cellulose microfibrils, their aggregation in a subsequent treatment in the presence of D₂O, and the final washing with H₂O to remove deuterium in the non-aggregated areas (Suchy et al. 2010b; Pönni et al. 2013). The difference between the methods illustrated in Schemes 1 and 2 is the measured value, which in Scheme 1 is the amount of accessible hydroxyl groups in the sample, whereas Scheme 2 gives the amount of inaccessible OD formed during the studied treatment. Thus, FT-IR spectroscopy combined with deuteration has the limitation to detect only the changes within a certain treatment. In addition, the deuterium exchange is much slower in the vapor state compared to the liquid state (Mann and Marrinan 1956).



Scheme 2 Deuteration of cellulose microfibrils, and their aggregation in a subsequent treatment in the presence of D₂O followed by exchange of the accessible deuterium by water

FT-IR PAS spectroscopy

Prior to the FT-IR spectroscopy, the samples were dried at 40 °C in an oven. The spectra were collected using a Bio-Rad FTS 6000 spectrometer (Cambridge, MA, USA) with a Gasera PA301 photoacoustic cell (Turku, Finland) at a constant mirror velocity of 5 kHz, 1.2 kHz filter, and 8 cm⁻¹ resolution. In the beginning of each set of measurements, a background spectrum was collected using a standard carbon black. The photoacoustic cell was purged with helium gas for 30 s prior to each measurement. 200 scans per spectrum were collected using the Win-IR Pro 3.4 software (Digilab, Holliston, MA, USA). Every sample was measured in duplicate and the averaged spectra were baseline corrected and normalized for cellulose band height at 1,200 cm⁻¹ (Hofstetter et al. 2006), using Grams/AI 9.00 software (Thermo Fischer Scientific Inc., Waltham, MA, USA).

The area of the OD stretch band at around 2,500 cm⁻¹ in the FT-IR spectrum was integrated using Grams/AI 9.00 software (Thermo Fischer Scientific Inc., Waltham, MA, USA). This band does not overlap with any other band in the FT-IR spectrum and, thus the normalized area of the OD stretch band measures the extent of irreversible deuteration (Suchy et al. 2010b).

WRV analysis

Prior to the analysis, the pulp samples were converted to their Na⁺-form. All of the subsequent treatments were done at 1 % consistency and each exchange of solution was done after filtration on a Büchner funnel. First, the samples were converted to their protonated form by a treatment in 0.01 M HCl for 1 h. Then, the

samples were washed twice with water. Conversion to the Na^+ -form was done in 0.001 M NaHCO_3 for 2 h with the pH adjusted to 9.5–10 with 0.1 M NaOH . Then, the samples were washed with water until the conductivity of the slurry was lower than $5 \mu\text{S cm}^{-1}$. The WRV analysis was done according to the standard SCAN-C 102 XE with a Jouan GR 4.22 centrifuge. The standard deviation was determined from four parallel measurements.

Results and discussion

Deuterium exchange

Deuterium exchange with multiple drying and rewetting cycles has been applied earlier for studying wood samples (Lee et al. 2011; Rautkari et al. 2013). It has also been shown that critical RH above which no further deuteration occurs is 60 % (Taniguchi et al. 1978). Figure 1 illustrates changes in the mass of birch pulp during the first and last three cycles of a 30 cycle DVS measurement. In order to quantify the amount of accessible hydroxyl groups, the increase in the dry mass of the sample after each cycle was recorded. Figure 2 illustrates this increase after the exposure to D_2O vapor during these cycles. The increase in dry mass appeared to follow a multicomponent exponential function (parallel exponential kinetics). Thus, the following equation (Eq. 2) was fitted to the results:

$$\Delta m = \Delta m_0 + \Delta m_1(1 - \exp(-x/x_1)) + \Delta m_2(1 - \exp(-x/x_2)), \quad (2)$$

where, Δm is the increase in mass at infinite time (x) of exposure to a constant RH, Δm_0 is the increase in mass during the first cycle, Δm_1 and Δm_2 are the increases in mass at infinite time associated with fast and slow phenomena respectively, and $1/x_1$ and $1/x_2$ are the rate constants for these phenomena.

The deuterium exchange was earlier suggested to consist of two parallel phenomena; a fast reaction corresponding to the exchange of protons in the amorphous regions and a slow reaction corresponding to the exchange on the surface of the crystalline regions (Mann and Marrinan 1956; Jeffries 1963). Hofstetter et al. (2006) proposed the two phenomena to be due to the exchange at the surfaces (fast) and at the interiors (slow) of the cellulose microfibrils. The deuteration of the less-ordered regions of cellulose, i.e.

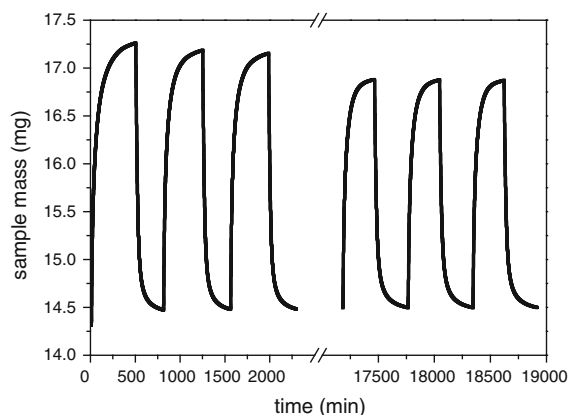


Fig. 1 The first and last three cycles of a 30 cycle DVS experiment with birch kraft pulp. The lower and upper values express the sample mass in dry (RH 0 %) and humid (RH 95 %) conditions

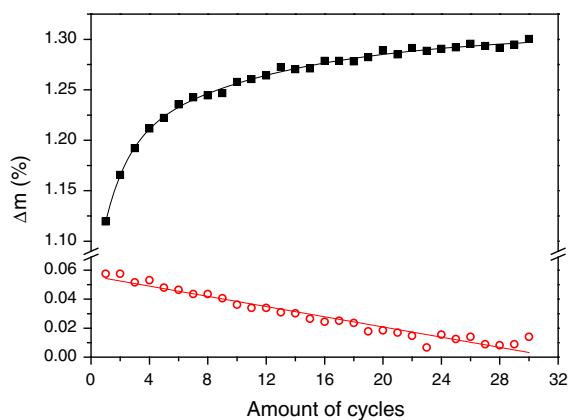


Fig. 2 Percentual increase in the dry mass (Δm) of birch kraft pulp as a function of the number of drying (N_2 , RH 0 %) and rewetting [D_2O (square) and H_2O (circle) vapor in N_2 , RH 95 %] cycles in DVS

fast process, was considered to be complete and to occur within some minutes to 1 day depending on the conditions, e.g., temperature (Jeffries 1963). Jeffries (1963) suggested the main reason for the slow exchange in the crystalline regions to be the low concentration of D_2O within these regions. Even exchange in the liquid state proceeds through fast and slow kinetics (Frilette et al. 1948). In this case, the fast exchange is considered to be diffusion controlled and to occur within a few minutes (Frilette et al. 1948; Tsuchikawa and Siesler 2003a, b). The slow exchange was shown to proceed even after 1 week of exposure to liquid D_2O (Frilette et al. 1948). The slow reaction

was not reported in previous studies on deuterium exchange in bacterial cellulose and wood powder (Lee et al. 2011; Rautkari et al. 2013). Thus, the more pronounced slow exchange in the birch kraft pulp is suggested to be due to the chemical processing and drying that the pulp has undergone.

In order to verify the deuterium exchange as the cause for the mass increase, a 30 cycle DVS trial for the birch pulp was conducted with water vapor. Prior to the experiment, the sample was dried over a period of time significantly longer to that applied between the cycles. Thus, the observed initial small mass increase could only indicate that the sample was not completely dried between the cycles (Fig. 2). As the water vapor cycles were continued, the dry mass of the sample slowly decreased. This might be due to hornification, which reduces the number of accessible hydroxyl groups and changes the fiber structure e.g., by pore closure (Higgins and McKenzie 1963; Scallan 1974). In any case, the mass increase during the first cycle with water vapor was only approximately 5 % of the mass increase obtained with D₂O vapor (Fig. 2). Thus, the mass increase in D₂O vapor must be mainly due to the deuterium exchange.

The necessity of the multiple drying and rewetting cycles was evaluated by applying a series of only two extended cycles having the overall exposure time with D₂O comparable to that of the experiments with the shorter cycles. The amount of accessible hydroxyl groups determined after these extended cycles was within the standard deviation of the experiment conducted with 30 cycles but with similar overall exposure time for D₂O (Table 1). Thus, the measurement is not dependent on the drying and rewetting, but on the extended exposure to D₂O to allow also the slow exchange to occur. This was also found earlier by Jeffries (1963). More recently, the deuterium exchange of fully amorphous cellulosic films with D₂O vapor was reported to occur within 10 h (Hishikawa et al. 1999).

Even though the extended cycles gave similar results, we chose to proceed with 15 cycles experiments, in order to have the measurement resemble the earlier work conducted on DVS with deuterium exchange (Lee et al. 2011; Rautkari et al. 2013). The duration for recording the 15 cycles was approximately 6 days. Three parallel measurements were completed for each sample. Thus, the overall duration for one sample was around 18 days. Moreover, the

Table 1 Number of accessible hydroxyl groups measured by 2 and 30 DVS cycles but similar total exposure time for D₂O vapor

Exposure to D ₂ O time (min)	Two extended cycles accessible OH groups (mol kg ⁻¹)	30 short cycles accessible OH groups (mol kg ⁻¹)
5,000	12.2 ± 0.5	12.7 ± 0.5
10,000	12.6 ± 0.5	13.0 ± 0.5

measurement was very sensitive to any unexpected disturbance and occasionally the measured value was out of range of the parallel measurements. These values were excluded from the data.

Hornification

In addition to the increase in dry mass due to the exchange of protons with deuterons, the DVS data showed a decrease in the wet mass of the pulp, i.e. its equilibrium moisture content (EMC), with time during the repeated humidity cycles as well as a decrease in the duration to reach the EMC at the high humidity. The decrease in the wet mass is most likely due to the drying induced hornification. Even though the raw material was industrially dried birch kraft pulp, the cellulose microfibril aggregation, i.e. hornification, proceeds as the drying cycles are continued. Previously, hornification was reported to be most severe during the first cycle but to proceed to a smaller extent with multiple drying and rewetting cycles (Laiwins and Scallan 1993; Wistara and Young 1999). Changes in WRV of regenerated cellulosic fibers were reported to be most pronounced during the first five drying and rewetting cycles and to stabilize after around 15 cycles (Siroká et al. 2012). The decrease in the obtained moisture content at 95 % RH appears to follow an exponential function (Fig. 3). Thus, a corresponding equation (Eq. 3) was fitted with the results:

$$\text{EMC} = \text{EMC}_0 + \text{EMC}_1(\exp(-x/x_1)), \quad (3)$$

where EMC is the moisture content at infinite time of exposure to a constant RH, EMC₀ is the initial moisture content, EMC₁ is the moisture contents at infinite time associated with hornification, and 1/x₁ is the rate constant related to the rate of the hornification. As expected, the parameters were hardly affected by the sorbate (water or D₂O) and the exponential

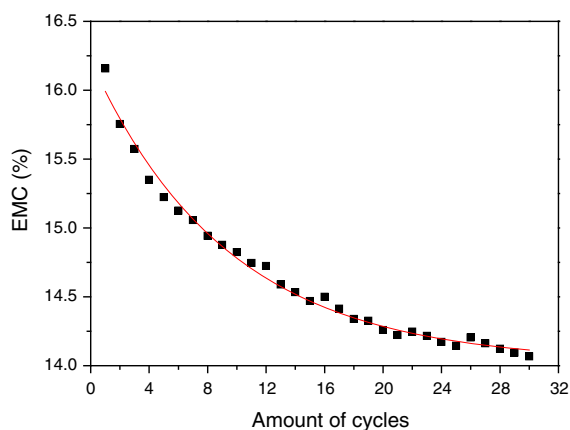


Fig. 3 Reduction in EMC of birch kraft pulp at 95 % RH after repeated DVS cycles in D_2O vapor

function (Eq. 3) approached $EMC = 14\%$ in both cases.

The DVS cycles have earlier been modeled with parallel exponential kinetics (Kohler et al. 2003; Kachrimanis et al. 2006; Hill et al. 2010; Xie et al. 2011). The hornification phenomenon can thus be observed by applying the model (Eq. 4) for individual DVS cycles:

$$EMC = EMC_0 + EMC_1(1 - \exp(-x/t_1)) + EMC_2(1 - \exp(-x/t_2)), \quad (4)$$

where EMC is the moisture content at infinite time of exposure to a constant RH, EMC_0 is the initial moisture content, EMC_1 and EMC_2 are the moisture

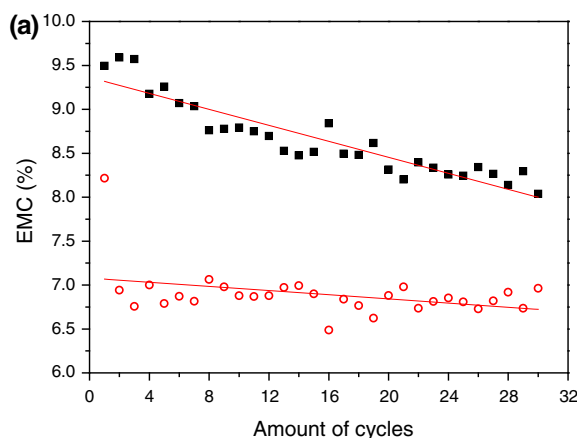
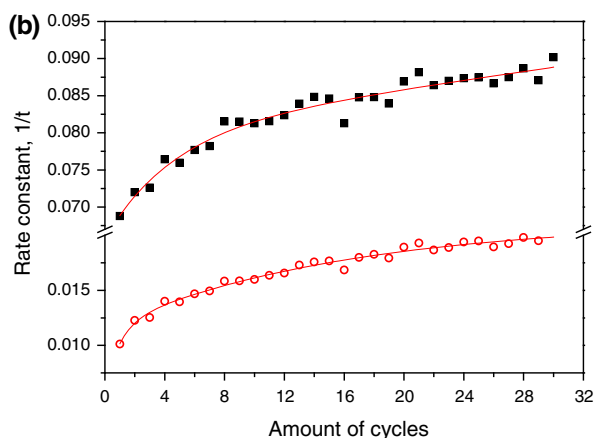


Fig. 4 Effect of repeated DVS cycles on dynamics of hydration and EMC of birch kraft pulp. The constants of the PEK model; the infinite moisture contents **a** for the fast reaction (EMC_1) (square) and for the slow reaction (EMC_2) (circle) and the

contents at infinite time associated with the fast and slow phenomena respectively, and $1/t_1$ and $1/t_2$ are rate constants for the fast and the slow phenomena, respectively. Information on the dynamics of hornification can be obtained by observing changes in parameters EMC_1 , EMC_2 , $1/t_1$ and $1/t_2$ as the function of repeated DVS cycles (Fig. 4). Both rates increase with repeated DVS cycles. Interestingly, the extent of the slower phenomenon (EMC_2) is unaffected by the continuing repetitions on contrary to the faster hydration the extent of which (EMC_1) decreases linearly with time. Thus, the slow phenomenon, unlike the faster one, appears not to be related with hornification.

Comparison between pulps

The idea in developing the DVS analysis coupled with deuterium exchange was to have a method to assess the reactivity of different pulps. An alkaline treatment series was performed for the dry bleached birch pulp because such treatments are often used to activate pulps for increased reactivity. The series had varying alkalinities between 0.25 and 2 M NaOH concentrations. The temperature during the treatments was 90 °C, duration 4 h, and consistency 5 % in all of the experiments. Figure 5 illustrates the extent of irreversible deuteration (alkali treatments in D_2O) as observed by the integrated area of the FT-IR band at $2,500\text{ cm}^{-1}$ and WRV (alkali treatments in water) for the treated pulps. The effect of the aqueous NaOH solution applied in the D_2O experiments was taken



reaction rates **b** for the fast reaction ($1/t_1$) (square) and for the slow reaction ($1/t_2$) (circle); applied to 30 DVS cycles for a dry birch pulp sample

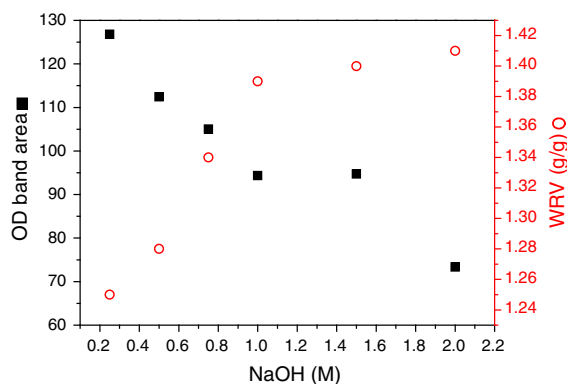


Fig. 5 The level of deuteration observed as the OD band area at $2,500\text{ cm}^{-1}$ (square) and WRV (circle) for dry birch pulps treated at various NaOH concentrations for 4 h at $90\text{ }^{\circ}\text{C}$

into account according to the applied molar ratios. WRV increased as a function of alkalinity while the level of irreversible deuteration was decreased. From previous research, it is known that WRV increases during an alkali treatment of dry pulps, through increased swelling (Weise et al. 1998). Irreversible deuteration, measured after washing the alkali treated pulp with water, was previously shown to be mostly reversed in a second alkali treatment in water (Pönni et al. 2012). Thus, the alkali treatment was suggested to induce an equilibrium state between the microfibrils and microfibril aggregates. It was also shown, that during kraft pulping, where cellulose microfibrils aggregate due to the removal of lignin and hemicelluloses, the extent of irreversible deuteration decreases as the alkali concentration approaches the mercerization level (Pönni et al. 2014). Thus, the irreversible deuteration under the conditions applied in this study should present an equilibrium state between the microfibrils and microfibril aggregates. Obviously, the equilibrium is shifted towards decreased aggregation as the alkalinity is increased.

The number of accessible hydroxyl groups was determined for the dry birch pulp and the pulps treated with 0.25 and 2 M NaOH and correlated with WRV (Fig. 6). Only these few samples were tested due to the long time needed for the determination of the accessible hydroxyl groups by DVS. Regardless, the correlation provides supporting evidence for WRV as an approximate measure of cellulose accessibility for dry and alkaline treated birch pulps. In addition, Fig. 6 suggests an increase in the amount of accessible

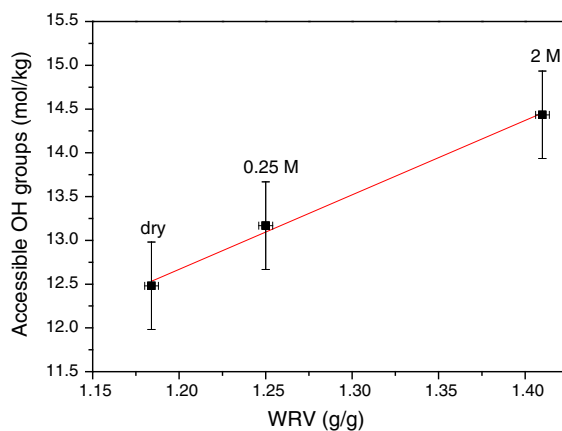


Fig. 6 The amount of accessible hydroxyl groups as a function of WRV for dry birch kraft pulp and the same pulp treated with 0.25 and 2 M NaOH at $90\text{ }^{\circ}\text{C}$ for 4 h

hydroxyl groups during the alkaline treatment. This increase is visible even though strong alkali treatments are known to remove the highly accessible hemicelluloses (Sjöström and Enström 1967).

Conclusions

The use of a DVS apparatus with deuterium exchange is a powerful analytical tool to quantify the accessible hydroxyl groups in chemical pulps. The weakness of the measurement, at the moment, is its long duration. The measurement does not depend on the number of drying and rewetting cycles, but on the overall time of exposure to D_2O vapor. The deuteration follows parallel exponential kinetics, which is in agreement with the earlier finding on fast and slow exchange of protons in the amorphous regions and crystallite surfaces, respectively. In addition to the number of accessible hydroxyl groups, DVS gives also information on the dynamics and extent of hornification during repeated humidity ramps. The number of accessible hydroxyl groups in dry pulp correlates with the traditional measure of cell wall bound water, the WRV. In future, DVS in D_2O vapor could be used to calibrate OD group measurement by FT-IR spectroscopy. This would enable a quantitative assessment of deuterium intake in liquid D_2O , too.

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