# Highly Selective Epoxidation of α-Pinene and Cinnamyl Chloride with Dry Air over Nanosized Metal Oxides

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**Abstract** Catalytic epoxidation of  $\alpha$ -H-containing olefins with air over nanosized metal oxides under mild conditions has been first reported. Nanosized Co<sub>3</sub>O<sub>4</sub> was considerably active for the epoxidation of  $\alpha$ -pinene and cinnamyl chloride with air at atmospheric pressure. A substrate  $\alpha$ -pinene conversion of 70.75 mol% with an epoxide selectivity of 87.68% was achieved at 363 K over Co<sub>3</sub>O<sub>4</sub>. Once Co<sub>3</sub>O<sub>4</sub> was further modified with metal oxides or ammonium salts through a simple procedure consisting of ultrasonic agitation, drying and calcination, thus-prepared catalysts presented lower catalytic activity and higher epoxide selectivity than cobalt oxide itself. Over Co<sub>3</sub>O<sub>4</sub> modified with surfactants, the conversion of  $\alpha$ -pinene was somewhat reduced to 48.86-63.76 mol%, but the epoxide selectivity was increased to 92.12-94.83%. However, the composite oxide  $CoO_x$ -SnO<sub>x</sub> (10:1) catalyzed 48.21 mol% of  $\alpha$ -pinene conversion with 85.82% of epoxide selectivity. For the substrate cinnamyl chloride, the best result was 40.76 mol% of conversion and 87.17% of epoxide selectivity achieved by  $CoO_x$ -ZnO (5:1). It is noteworthy that the use of TBHP in small amounts initiated the reaction efficiently, and the lack of TBHP would lead to a low conversion and selectivity.

Keywords Catalytic epoxidation  $\cdot$  Nanosized oxides  $\cdot \alpha$ -Pinene  $\cdot$  Cinnamyl chloride  $\cdot$  Butyl acrylate  $\cdot$  Co<sub>3</sub>O<sub>4</sub>  $\cdot$  CoO<sub>x</sub>-MO<sub>x</sub>  $\cdot$  Air

#### 1 Introduction

Catalytic epoxidation of olefins has attracted much attention both in industrial processes and in organic syntheses, as the epoxides are the most useful synthetic intermediates [1] or precursors in the production of fine chemicals and pharmaceuticals [2, 3]. Epoxides can find a large range of applications in pharmaceutical industry as drug intermediates, and in the preparation of epoxy resins, polymers and paints. The commercial manufacturing of epoxides involves chlorohydrins-Halcon process, which is a twostage process and produces co-products stoichiometrically. However, the chlorohydrins-Halcon process has caused seriously environmental pollution. Therefore, many alternative methodologies have been developed for the epoxidation of alkenes using single oxygen donor reagents, such as NaIO<sub>4</sub>, NaOCl, PhIO, ROOOH and H<sub>2</sub>O<sub>2</sub>.

Selective oxidation of hydrocarbons using molecular oxygen as the oxidant has been more attractive and challenging because of low cost and environmentally friendly nature [4]. Catalytic epoxidation with molecular oxygen under mild conditions is a challenging process for researchers [5, 6]. Many catalytic systems with the use of dioxygen, aliphatic aldehyde and various transition metal compounds have been reported [7-10]. Most of which describe the use of homogeneous catalysts, and only a few deal with the applications of heterogeneous catalysts [11–14]. The complexes of transition metal Co, Ti, Mn and Mo were used to catalyze the selective epoxidation of cyclic olefins such as cyclohexene and other alkenes with oxygen [15–18]. Silica-based titanium-containing materials (particularly TS-1 and TS-2) have been widely studied in the liquid-phase selective oxidation reactions using aqueous hydrogen peroxide as the oxidant [19, 20]. Wang et al. [21] employed polymer-anchored PSt-ChzAcAc-Co (II)

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with iso-butyraldehyde as co-reductant in the epoxidation of various cyclic alkenes with molecular oxygen. Raja et al. [22] developed MAIPO-36 (M=Co or Mn) catalyst for the epoxidation of cyclohexene and other alkenes in the presence of sacrificial aldehyde.  $CoO_x$ -MCM-41 prepared by the precipitation of cobalt tricarbonyl nitrosyl in declain was used in the epoxidation of alkenes by O<sub>2</sub> in the presence of iso-butyraldehyde [23]. Pruss et al. [24] reported that cobalt complexes immobilized on modified HMS could catalyze the epoxidation of alkenes with O<sub>2</sub>. Wang and co-workers described that the single site Co(II) catalysts present in faujasite zeolites or in MCM-41 were active in the aerobic epoxidation of styrene giving higher conversions and lower epoxide selectivities [25].

Nanostructured materials have attracted great interest in recent years due to their particular physical and chemical properties [26]. The properties of these materials mainly depend on their shape, size and structure, which are strongly determined by the synthetic processes. Nanostructured catalysts, such as Fe<sub>2</sub>O<sub>3</sub>, Co<sub>3</sub>O<sub>4</sub> and mixed Fe–Co oxide have been employed in the hydrocarbon oxidations [27, 28]. In the previous works, we reported the selective epoxidation of styrene with air over Co-ZSM-5 coordinated with ligands and nanosized  $Co_3O_4$  [29, 30], in which the latter showed high up to 96% of the epoxidation selectivity. The present work is first to report the epoxidation of  $\alpha$ -H-containing alkenes (like  $\alpha$ -pinene and cinnamyl chloride) by air over nanosized metal-oxides under atmospheric pressure, and further to investigate the factors influencing the conversion of substrate and the selectivity to epoxide. Under mild conditions, the best selectivity to epoxide could reach 94.83% superior to the catalysts reported in the literature, which is relatively attractive.

#### 2 Experimental

#### 2.1 Materials

 $Co(NO_3)_2 \cdot 6H_2O$  (98%),  $Zn(NO_3)_2 \cdot 6H_2O$  (99%),  $Cu(NO_3)_2 \cdot$  $3H_2O$  (99.5%), Ni(NO<sub>3</sub>)<sub>2</sub> ·  $6H_2O$  (98%), CoSO<sub>4</sub> ·  $7H_2O$  $(99.5\%), SnCl_4 \cdot 5H_2O(99\%), ZnCl_2(99\%)$  were purchased from Tianjin Bodi Chemical Co. CTAB (hexadecyl trimethyl ammonium bromide, >98%), DTAB (dodecyl trimethyl ammonium bromide, >98%), OTAB (octyl trimethyl ammonium bromide, >98%) were purchased from Tianjin Fuchen Chemical Co. The main reagents used in the epoxidations were  $\alpha$ -pinene (99.9%, Shanghai), trans-cinnamyl chloride (98%, Aldrich) and butyl acrylate (98%, Shanghai), tert-butyl hydrogen peroxide (TBHP, >65%, Shanghai) were directly used as received. The freshly distilled solvents included *N*,*N*'-dimethylformamide (DMF), N,N'-dimethyl acetamide (DMA), toluene, dioxane,

dichloroethane, dibromoethane, acetic acid, acetonitrile, cyclohexanone.

 $Co_3O_4$  nanocrystals were prepared by a precipitation route using cobalt nitrate as the precursor in the presence of surfactant. In a typical synthesis, 124.5 mmol of  $Co(NO_3)_2$  · 6H<sub>2</sub>O and 25.0 mmol of surfactant were dissolved in 750 mL of deionized water (in a 2,000-mL round bottom flask) to give a pink solution. After the pink solution was ultrasonically agitated for 40 min, 249.0 mmol of triethylamine was rapidly added to achieve a blue mixture under vigorous agitation. Then, the blue mixture was stirred at 348 K for 8 h until the color was changed into black. The precipitate was recovered by centrifugation and then dried at 353 K for 24 h, which would undergo a Soxhlet extraction by ethanol for 48 h to remove the stabilizer. The obtained solid was dried at 373 K for 8 h and then calcined at 573 K in flowing air for 2 h. The composite oxide  $CoO_x$ -MO<sub>x</sub> was prepared by the following procedure. Typically, certain molar ratio of  $Co(NO_3)_2$  and the other metal salt were mixed and ground for 30 min, which was then placed in a crucible and calcined at desired temperature in an air atmosphere for some time. After that, the black solid was ground into powder and directly used as the catalyst. The molar ratios of  $CoO_x$ -SnO<sub>x</sub> were 10:1 and 2:1, and those of  $CoO_x$ -ZnO were 10:1 and 5:1.

#### 2.2 Characterization of Catalysts

IR spectra were recorded on a Shimadzu IR Prestige-21 Fourier Transform Infrared spectrophotometer; the samples were ground with KBr and pressed into thin wafers. The scanning range was from 4,000 to 400  $\text{cm}^{-1}$ , with a resolution of 2 cm $^{-1}$ . UV-vis spectra of samples were recorded on a Shimadzu UV-2550 spectrometer. For the diffuse reflectance mode (solid), the powdered sample was loaded into a holder, and the spectra were collected in the range of 200-800 nm referenced to BaSO<sub>4</sub>. XRD (X-ray diffraction) patterns of solid samples were recorded on a Rigaku D/MAX – IIIC diffractometer with CuKa ( $\lambda = 1.54184$ Å) radiation operating at 30 kV and 25 mA. The scanning range was from  $2\theta = 5^{\circ}$  to  $65^{\circ}$  with a scanning speed of 2°/min. The particle sizes of samples were calculated based on TEM images, which were determined on a Nippon Electronics JEM-100SX transmission electron microscope.

## 2.3 Catalytic Reactions

The epoxidation of  $\alpha$ -H-containing olefins (mainly  $\alpha$ -pinene and cinnamyl chloride) with air were carried out in a batch reactor under atmospheric pressure (Scheme 1). In a typical run, 3 mmol of olefins, 10 g of solvent, 0.5 g of 3-Å molecular sieve (MS) and certain quantity of catalyst were added into a 100-mL two-necked flask equipped with





a cryogenic-liquid condenser and with an air pump. The mixture was vigorously stirred by a magnetic stirrer and heated to the desired temperature. Then dry air with a stable flow rate of 30 mL/min controlled by a flowmeter was introduced into the bottom of reactor by bubbling at atmospheric pressure. After the completion of the reaction, the mixture was cooled down to room temperature and the catalyst was filtered off. The filtrate was quantitatively analyzed by a gas chromatograph (Shimadzu GC-2010) with a DB-1 column (30 m × 0.25 mm × 0.25 µm) and an FID detector using chlorobenzene as the internal standard and hydrogen as carrier gas. The conversion of olefins (mol%) and the selectivity (%) to epoxide were calculated accordingly.

# **3** Results and Discussion

#### 3.1 Structural Characteristics of Catalyst Samples

Nanosized metal oxide Co<sub>3</sub>O<sub>4</sub> were prepared from nitrates in the presence of surfactants (inclusive of CTAB, DTAB and OTAB) and amines (including triethylamine, tributylamine, triethanolamine and di-n-propylamine). Figure 1 shows the FT-IR spectra of Co<sub>3</sub>O<sub>4</sub> (calcined at 773 K for 2 h), which underwent modification by triethylamine (traces a, b and c) before extraction of the stabilizer by ethanol. There was no peak observable at 2,915 and 2,848 cm<sup>-1</sup> of the C-H stretching modes resulting from CTAB and triethylamine, suggesting that surfactant and triethylamine had been totally removed from samples. Two bands appearing at 668 and 579  $\text{cm}^{-1}$  could be assigned to the vibrations of Co–O due to  $Co_3O_4$  nanoparticles [31], as evidenced by the color change from blue to black of the mixture after the addition of triethylamine. Distinctly, the presence of CTAB, DTAB, OTAB and triethylamine, tributylamine, triethanolamine, or di-n-propylamine stabilized nanoparticles by capping the surface of nanoparticles with organic ligands. The formation of nanoparticles was proposed through a model of inorganic-



**Fig. 1** FT-IR spectra of  $Co_3O_4$  after calcination at 773 K for 2 h. *a* Modified by OTAB; *b* modified by DTAB; *c* modified by CTAB

organic layered particles. This is that the polar surface of metal oxide particles benefited the adsorption of the organic cations generated in situ to form the organic shells on the surface of nanoparticles and to prevent nanoparticles from aggregation through enhancing steric hindrance to overcome van der Waals interactions between the nanoparticles, as proposed by the literature [32, 33]. Figure 2 compares the UV-vis spectra of Co<sub>3</sub>O<sub>4</sub> samples, which show evidently different ultraviolet absorbance characteristics. UV-vis spectra of  $Co_3O_4$  samples show absorbance bands at 392, 677 nm for trace-a (modified by OTAB), at 376, 671 nm for trace-b (modified by DTAB), and at 357, 639 nm for trace-c (modified by CTAB), similar to the absorbance bands at 384, 687 nm of trace-d (calcined directly from cobalt nitrate), totally different from those at 259, 263, 282, 305, 313 nm of the corresponding metal salt  $Co(NO_3)_2 \cdot 6H_2O$  [34].



**Fig. 2** UV–vis spectra of  $Co_3O_4$  nanocatalysts. *a* Modified by OTAB; *b* modified by DTAB; *c* modified by CTAB; *d* calcined directly from cobalt nitrate

The preparation of composite oxide catalysts  $CoO_r$ -MO<sub>x</sub> was quite straightforward, requiring only a simple calcination procedure instead of very complicated synthesis and modification. FT-IR spectra of 10:1 CoO<sub>x</sub>-SnO<sub>x</sub> and 2:1  $CoO_x$ -SnO<sub>x</sub> samples showed characteristic twin bands at 668 and 579 cm<sup>-1</sup>, assigned to the vibrations of Co–O bands. The weak band emerging at about  $600 \text{ cm}^{-1}$ in the IR spectra of traces a and b can be assigned to the vibration of Sn-O bands. The IR absorption bands near 668 and  $579 \text{ cm}^{-1}$  observed from traces c and d are also ascribable to Co-O bands. The weak band emerging at about 400  $\text{cm}^{-1}$  is assigned to the Zn–O vibration. UV–vis spectra of composite oxides  $CoO_x$ -MO<sub>x</sub> (containing SnO<sub>x</sub>) and ZnO, shown in Fig. 3) possess considerably different ultraviolet absorbance characteristics from pure Co<sub>3</sub>O<sub>4</sub>, which may indicate the interaction between cobalt oxide and other metal oxide by calcination. For example, there are recognizable four bands at 264, 269, 346, 655 nm for 10:1 CoO<sub>x</sub>-SnO<sub>x</sub>, four bands at 272, 293, 375, 675 nm for 2:1  $CoO_x$ -SnO<sub>x</sub>, three bands at 286, 363, 681 nm for 5:1  $CoO_x$ -ZnO; while four bands of  $Co_3O_4$  emerge at 263, 313, 354. 698 nm.

Figure 4 summarizes XRD patterns of the calcined catalysts  $Co_3O_4$  and  $CoO_x$ -MO<sub>x</sub> prepared by our methods. Observable eight peaks at  $2\theta = 19.16$ , 31.46, 37.08, 39.02, 45.48, 56.06, 59.74, and 65.76 for three samples can be assigned to the cubic structure of  $Co_3O_4$  phase with an *Fd3m* space group as compared to a data file of JCPDS-43-1003, which gives eight peaks at  $2\theta = 36.88$ , 65.28, 59.38,



**Fig. 3** UV–vis spectra of various composite  $Co_3O_4$ –MO<sub>x</sub> oxides. *a*—10:1 CoO<sub>x</sub>–SnO<sub>x</sub>; *b*—2:1 CoO<sub>x</sub>–SnO<sub>x</sub>; *c*—5:1 CoO<sub>x</sub>–SnO<sub>x</sub>; *d*–Co<sub>3</sub>O<sub>4</sub>, modified by DTAB



**Fig. 4** XRD patterns of the calcined catalysts  $Co_3O_4$  (*a*—modified by DTAB) and  $CoO_x$ -MO<sub>x</sub> (*b*—10:1  $CoO_x$ -SnO<sub>x</sub>; *c*—10:1  $CoO_x$ -ZnO)

31.38, 44.88, 19.08, 38.58, and 55.78. The cell constant a = 0.8082 is very near to the published data for Co<sub>3</sub>O<sub>4</sub> crystal (a = 0.8084). It can be clearly observed from Fig. 4

that  $\text{CoO}_x$ -MO<sub>x</sub> merely displays several weak X-ray diffractions, such as  $2\theta = 19.16$ , 31.46, 37.08, 39.02, 45.48, 56.06, 59.74, and 65.76, indicating that cobalt species in these composite oxides exist mostly in the form of  $\text{Co}_3\text{O}_4$ .

The particle sizes of  $Co_3O_4$  (a—) and  $CoO_x$ -MO<sub>x</sub> (b— 10:1  $CoO_x$ -SnO<sub>x</sub> and c-10:1  $CoO_x$ -ZnO) calculated from the (311) plane using the Sherrer equations [35] were 33, 24, and 19 nm, respectively. TEM analysis has revealed evidences that the particles exhibit platelet morphologies with minor particle agglomeration and a relatively narrow particle size distribution. One can observe one-dimensional arrays of Co<sub>3</sub>O<sub>4</sub> nanoparticles (calcined at 623 K at a heating rate of 1 °C/min) interconnected along the original directions of the nitrate nanorods. The average particle size is about 40 nm (in the range of 12.5-50 nm diameter with nanostructures of uniform morphology), consistent with the XRD result and the calculation from the Sherrer equation. Once the calcination temperature was reduced to 573 K, some nonoxide impurities were still present. TEM determinations showed nanosized particles of some samples in Fig. 5, e.g. ca. 20 nm for Co<sub>3</sub>O<sub>4</sub> (modified by DTAB and calcined at 573 K for 8 h), 15 nm for Co<sub>3</sub>O<sub>4</sub> (modified by OTAB and calcined at 573 K for 2 h), 10-150 nm for 10:1  $CoO_x$ -SnO<sub>x</sub> (calcined at 823 K for 4 h) and ca. 15 nm for 10:1 CoO<sub>x</sub>-ZnO (calcined at 573 K for 2 h), respectively.

# 3.2 Catalytic Epoxidation of α-Pinene and Cinnamyl Chloride with Air

## 3.2.1 Catalytic Activity of Nanosized Co<sub>3</sub>O<sub>4</sub> Catalysts

Table 1 compares the catalytic activities of nanosized Co<sub>3</sub>O<sub>4</sub> catalysts modified with different surfactants in the epoxidation of  $\alpha$ -pinene with air. Obviously, nanosized Co<sub>3</sub>O<sub>4</sub> modified by OTAB obtained the highest conversion of  $\alpha$ -pinene (63.76 mol%) and higher selectivity of epoxide (92.12%). However, when no TBHP was added, the conversion and the selectivity of epoxide would be reduced to 20.86 mol% and 69.17%. TBHP played a key role in enhancing the epoxidation activity and selectivity (Table 1); however, when no air was introduced into the reaction (adding 0.7 mmol TBHP), the conversion was largely reduced to 12.07 mol% with an epoxide selectivity of 90.76%. It is noteworthy that the use of TBHP in small amounts initiated the reaction efficiently, and the lack of TBHP or air would lead to a low conversion and selectivity. The catalytic activity (based on the conversion) of all the nanosized Co<sub>3</sub>O<sub>4</sub> samples gradually decreased in the following sequence of 63.76 mol% (modified by OTAB) >61.71 mol% (modified by CTAB) >48.86 mol% (modified by DTAB). Very interestingly, Co<sub>3</sub>O<sub>4</sub> modified by DTAB showed the best epoxide selectivity of 94.83%, although it converted only 48.86 mol% of  $\alpha$ -pinene under identical conditions. Based on the results in Fig. 5 and





Entry	Surfactant	α-Pinene conversion (mol%)	Selectivity (%)			
			Epoxide	Verbenol	Verbenone	
1	CTAB	61.71	83.01	6.94	10.05	
2	DTAB	48.86	94.83	2.84	2.33	
3 <sup>a</sup>	OTAB	20.86	69.17	18.53	12.30	
4 <sup>b</sup>	OTAB	12.07	90.76	3.82	5.42	
5	OTAB	63.76	92.12	3.55	4.33	

Table 1 Epoxidation of  $\alpha$ -pinene with air on  $\text{Co}_3\text{O}_4$  modified by different surfactants

Substrate: 3 mmol; solvent: 10 g; catalyst: 30 mg; TBHP: 0.1 g; 3 Å MS: 0.5 g; temperature: 363 K; time: 5 h; flow rate of air: 30 mL/min <sup>a</sup> Not any TBHP

<sup>b</sup> Not any air (only TBHP)

Table 1, it is obvious that the reactivity and epoxidation selectivity of  $\alpha$ -pinene catalyzed by the nanosized Co<sub>3</sub>O<sub>4</sub> catalysts (modified with different surfactants) could be determined by the particle size and the type of surfactants used in the preparation.

Table 2 shows the epoxidation of cinnamyl chloride with air on Co<sub>3</sub>O<sub>4</sub> (modified by DTAB), where the calcination temperature exerted an obvious impact on the catalytic performance of Co<sub>3</sub>O<sub>4</sub>. Apparently, the catalytic activity (based on the conversion) of Co<sub>3</sub>O<sub>4</sub> samples seriously depended on the calcination temperature regardless of time, which showed a reduction of 52.11 mol% (573 K, 2 h)  $\approx$ 50.92 mol% (573 K, 8 h) > 39.02 mol% (673 K, 2 h) > 38.01 mol% (823 K, 2 h). However, the epoxidation selectivity of Co<sub>3</sub>O<sub>4</sub> samples displayed a reversal sequence of 87.16% (823 K, 2 h) > 63.05% (673 K, 2 h) > 62.62% (573 K, 2 h) > 60.03% (573 K, 8 h). Lower calcination temperature was beneficial to the activity of the catalyst but not to the epoxidation selectivity.

The impact of reaction temperature on the epoxidation of  $\alpha$ -pinene and of cinnamyl chloride over Co<sub>3</sub>O<sub>4</sub> (modified by OTAB) is shown in Figs. 6 and 7. Distinctly, the conversions of  $\alpha$ -pinene and cinnamyl chloride exhibited an increase with the reaction temperature from 333 to 373 K.

Table 2 Epoxidation of cinnamyl chloride with air on  $Co_3O_4$  (modified by DTAB)

Entry	Calcination program	Cinnamyl chloride conversion (mol%)	Selectivity (%)			
			Epoxide	1-One	Acyl chloride	
1	573 K, 2 h	52.11	62.62	31.81	5.56	
2	573 K, 8 h	50.91	60.03	19.03	20.94	
3	673 K, 2 h	39.02	63.05	36.31	0.64	
4	823 K, 2 h	38.01	87.16	10.53	2.32	

Substrate: 3 mmol; solvent: 10 g; catalyst: 30 mg; TBHP: 0.1 g; 3 Å MS: 0.5 g; time: 5 h; temperature: 363 K; flow rate of air: 30 mL/min



**Fig. 6** Effect of reaction temperature on the epoxidation of  $\alpha$ -pinene with air over Co<sub>3</sub>O<sub>4</sub> (modified by OTAB and calcined at 673 K for 2 h): ( $\blacklozenge$ )  $\alpha$ -pinene conversion, ( $\blacksquare$ ) epoxide selectivity, ( $\blacklozenge$ ) Verbenol selectivity, ( $\blacklozenge$ ) Verbenone selectivity. Substrate: 3 mmol; solvent: 10 g; catalyst: 30 mg; TBHP: 0.1 g; 3-Å MS: 0.5 g; time: 5 h; flow rate of air: 30 mL/min



**Fig. 7** Effect of reaction temperature on the epoxidation of cinnamyl chloride with air over  $Co_3O_4$  (modified by OTAB and calcined at 823 K for 4 h): ( $\blacklozenge$ ) cinnamyl chloride conversion, ( $\blacksquare$ ) epoxide selectivity, ( $\blacktriangle$ ) 1-one selectivity, ( $\times$ ) acyl chloride selectivity. Substrate: 3 mmol; solvent: 10 g; catalyst: 30 mg; TBHP: 0.1 g; 3-Å MS: 0.5 g; time: 5 h; flow rate of air: 30 mL/min

When the reaction temperature was lower than 363 K, both  $\alpha$ -pinene and cinnamyl chloride achieved low conversions. The conversion of  $\alpha$ -pinene was 23.78 mol% at 343 K, rapidly rose to 63.76 mol% at 363 K, then to 77.62 mol% at 373 K, but reduced to 65.18 mol% with a continuous increase to 383 K. The epoxide selectivity of  $\alpha$ -pinene first increased from 83.57% at 343 K to the maximum of 92.12% at 363 K, and then slightly reduced to 87.53% at 373 K. The epoxidation of cinnamyl chloride displayed the similar regularity with temperature. For example, below 343 K 32.15 mol% of the cinnamyl chloride was converted with an epoxide selectivity of 71.17%. With the increase in the reaction temperature, the conversion of cinnamyl

chloride increased quickly to 54.06 mol% at 363 K and then slowly to 61.72 mol% at 373 K; however, the epoxide selectivity first increased from 31.02% at 333 K to the maximum of 71.17% at 343 K, and then decreased quickly to about 44.39% at 363 K and to 2.97% at 373 K. This shows that the high temperature did not favor the formation of epoxides under the present experimental conditions.

It is well known that the choice of suitable solvent can play a critical role on the activity and selectivity in the liquid-phase oxidations of hydrocarbons. Various solvents have been tested for the epoxidation of  $\alpha$ -pinene by air over Co<sub>3</sub>O<sub>4</sub> at 353 K. The solvents chosen included DMF, DMA, toluene, dioxane, dichloroethane, dibromoethane, acetic acid, acetonitrile and cyclohexanone, with an increase order of dielectric constants: dioxane (2.21) < toluene(2.37) < acetic acid (6.15) < dibromoethane (9.72) < dichloroethane (10.4) < cyclohexanone (18.3) < acetonitrile (37.5) < DMF (37.6) < DMA (37.78).

It can be observed from Table 3 that  $Co_3O_4$  catalyst could catalyze the occurrence of  $\alpha$ -pinene oxidation with air in all solvents, regardless of the solvent polarity. Under identical conditions, nanosized  $Co_3O_4$  showed the best activity with an epoxide selectivity of 83.50% in DMF, while the use of DMA (an analogue of DMF) resulted in a higher conversion of 49.41 mol% but a lower epoxide selectivity of 69.47%. Although high conversion (*ca.* 64.63 mol%) of  $\alpha$ -pinene could be obtained over  $Co_3O_4$ when cyclohexanone was used as the solvent, the selectivity of epoxide was low only 61.19%. Interestingly, using dibromoethane and acetic acid as the solvents did not yield any epoxide but the main product verbenone with the

Table 3 The epoxidation of  $\alpha$ -pinene with air on Co<sub>3</sub>O<sub>4</sub> in different solvents

Entry	Solvent	α-Pinene conversion (mol%)	Selectivity (%)			
			Epoxide	Verbenol	Verbenone	
1	DMF	37.18	83.51	8.31	8.18	
2	DMF(363 K)	70.75	87.68	3.56	8.77	
3	DMA	49.41	69.47	8.26	22.27	
4	DMA(363 K)	55.86	74.99	7.15	17.85	
5	Toluene	15.53	48.75	17.93	33.31	
6	Dioxane	29.51	65.19	10.19	24.63	
7	Acetonitrile	22.45	39.08	13.79	47.13	
8	Cyclohexanone	64.63	61.19	9.51	29.30	
9	Dichloroethane	19.85	49.83	16.89	33.28	
10	Dibromoethane	54.25	0.00	10.56	89.44	
11	Acetic acid	51.08	0.00	13.69	86.31	

Substrate: 3 mmol; solvent: 10 g; catalyst: 30 mg; TBHP: 0.1 g; 3 Å MS: 0.5 g; temperature: 353 K (entry 2 and 4 are 363 K); time: 5 h; flow rate of air: 30 mL/min

selectivity of 89.44% and 86.31%, respectively. The investigation on this phenomenon is ongoing.

As the reaction temperature was risen from 353 to 363 K, 70.76 mol% of  $\alpha$ -pinene conversion and 87.68% of epoxide selectivity could be achieved in the DMF solution, notably higher than 55.86 mol% of conversion and 74.99% of epoxide selectivity in DMA. The excellent activity and selectivity of catalyst Co<sub>3</sub>O<sub>4</sub> could be due to the strong interaction of the DMF molecule with the active site, which further enhanced the desorption of products from the active sites, i.e. the affinity of DMF to O<sub>2</sub> and the cobalt oxide might promote the separation of  $\alpha$ -pinene epoxide from the catalytic sites to avoid the occurrence of deep oxidation, as has been revealed by previous studies [29, 36].

#### 3.3 Catalytic activity of Composite Oxides $CoO_x$ -MO<sub>x</sub>

When no TBHP was added, only 9.72 mol % of a-pinene could be convert1ed into the epoxide (77.79% of selectivity) at 363 K by 10:1  $CoO_x$ –ZnO catalyst. Once TBHP was used as the initiator, the conversion of  $\alpha$ -pinene was notably increased to 35.73 mol% with an epoxide selectivity of 85.03%. Table 4 presents the effect of different CoO<sub>x</sub>-MO<sub>x</sub> catalysts on the epoxidation of  $\alpha$ -pinene, in which the reactions were conducted at 363 K using DMF as the solvent and TBHP as the initiator. Very clearly, 10:1  $CoO_x$ -SnO<sub>x</sub> nanocatalyst displayed the best the catalytic activity for the epoxidation reaction of  $\alpha$ -pinene. Under our experimental conditions, 10:1  $CoO_x$ -SnO<sub>x</sub> catalyst achieved the conversion of  $\alpha$ -pinene (48.21 mol%) and the selectivity of epoxide (85.82%), while 10:1 CoO<sub>x</sub>-ZnO catalyst achieved 32.93 mol% of the conversion and 83.37% of the epoxide selectivity, showing the difference of catalytic activity of various composite metal-oxide catalysts. The catalytic activity of  $CoO_x$ -MO<sub>x</sub> catalysts gradually decreased in the sequence of 10:1  $CoO_x$ -SnO<sub>x</sub> > 2:1  $CoO_x$ -SnO<sub>x</sub> > 5:1  $CoO_x$ -ZnO > 10:1 CoO<sub>x</sub>-ZnO, implying that the addition of

**Table 4** Epoxidation of  $\alpha$ -pinene with air on CoO<sub>x</sub>-MO<sub>x</sub>

Entry	Catalyst	<ul><li>α-Pinene</li><li>conversion</li><li>(mol%)</li></ul>	Selectivity (%)			
			Epoxide	Verbenol	Verbenone	
1	10:1 $CoO_x$ -SnO <sub>x</sub>	48.21	85.82	5.6	8.58	
2	2:1 $CoO_x$ -SnO <sub>x</sub>	46.01	80.07	8.08	11.85	
3	10:1 CoO <sub>x</sub> –ZnO	32.93	83.37	7.92	8.72	
4	5:1 CoO <sub>x</sub> –ZnO	35.73	85.03	6.6	8.38	
5	5:1CoO <sub>x</sub> -ZnO*	9.72	77.79	16.43	5.78	

Substrate: 3 mmol; solvent: 10 g; catalyst: 30 mg (entry 1 and 2 calcined at 823 K for 4 h; entry 3 and 4 calcined at 673 K for 4 h); entry 5: not any TBHP; 3 Å MS: 0.5 g; temperature: 363 K; time: 5 h; flow rate of air: 30 mL/min

 Table 5 Epoxidation of cinnamyl chloride with air on various catalysts

Entry	Calcination	Cinnamyl chloride conversion (mol%)	Selectivity (%)			
	program		Epoxide	1-One	Acyl chloride	
1	Co <sub>3</sub> O <sub>4</sub>	50.26	60.28	20.16	13.73	
2	10:1 CoO <sub>x</sub> –ZnO	46.53	81.37	17.68	0.95	
3	5:1 CoO <sub>x</sub> –ZnO	40.76	87.17	11.45	1.37	
4	10:1 $CoO_x$ -SnO <sub>x</sub>	22.25	58.62	29.26	12.12	
5	ZnO	17.12	37.93	46.78	15.29	

Substrate: 3 mmol; solvent: 10 g; catalyst: 30 mg (metal oxides 1 and 2 calcined at 573 K for 2 h, metal oxides 3 and 4 calcined at 673 K for 4 h); TBHP: 0.1 g; 3 Å MS: 0.5 g; time: 5 h; temperature: 363 K; flow rate of air: 30 mL/min

basic ZnO was unbeneficial to the epoxidation of  $\alpha$ -pinene with air. Additionally, based on the Fig. 5, the reactivity and epoxidation selectivity of  $\alpha$ -pinene could be associated with the particle size and composition of the catalyst, which led to different catalytic performances. The size of CoO<sub>x</sub>-MO<sub>x</sub> catalysts decreased in the sequence of 10:1 CoO<sub>x</sub>-SnO<sub>x</sub> > 2:1 CoO<sub>x</sub>-SnO<sub>x</sub> > 5:1 CoO<sub>x</sub>-ZnO > 10:1 CoO<sub>x</sub>-ZnO, in good agreement with the change of their activities.

Table 5 presents the effect of different  $CoO_r-MO_r$  catalysts on the epoxidation of cinnamyl chloride with air. As the comparison, the Co<sub>3</sub>O<sub>4</sub> catalyst was prepared through a direct calcination of  $Co(NO_3)_2 \cdot 6H_2O$  at 573 K for 2 h. About 50.26 mol% conversion of cinnamyl chloride was obtained over 30 mg of  $Co_3O_4$ , but the selectivity of epoxide was only 60.28%. As shown in Table 5, the catalytic activity of  $CoO_x$ -MO<sub>x</sub> catalysts gradually decreased in the order of  $Co_3O_4$  (50.26 mol% of conversion) > 10:1  $CoO_x$ -ZnO (46.53 mol%) > 5:1  $CoO_x$ -ZnO (40.76 mol%) > 10:1  $CoO_x$ -SnO<sub>x</sub> (22.25 mol%) > ZnO (17.12 mol%). However, the selectivity of epoxide exhibited an entirely different descending order of 5:1  $CoO_x$ -ZnO (87.17%) > 10:1  $CoO_x$ -ZnO (81.37%) >  $Co_3O_4$  (60.28%) > 10:1  $CoO_x$ -SnO<sub>x</sub> (58.62%) > ZnO (37.93%). The 5:1 CoO<sub>x</sub>-ZnO and 10:1 CoO-ZnO nanocatalysts were favorable to the epoxidation of cinnamyl chloride, likely because the insertion of ZnO into the domain of Co<sub>3</sub>O<sub>4</sub> diluted and modified the catalytic active sites to reduce the possibility of the deep oxidations. Different from the case of  $\alpha$ -pinene, the reactivity and epoxidation selectivity of cinnamyl chloride could not be correlated with the variation of nanoparticle sizes. The deep investigations are ongoing.

Note that for the epoxidation of butyl acrylate the result was totally different from above those. Whatever the catalyst was, the conversion of butyl acrylate was always not more than 10 mol% in the range of the reaction temperature from 343 to 383 K, but only an epoxide (butyl acrylate oxide with 100% of selectivity) was yielded.

#### 4 Conclusions

The present work has first described a novel finding in the epoxidation of  $\alpha$ -H containing olefins with air catalyzed by nanosized metal oxides under mild conditions. Several transition metal-containing nanosized samples, such as  $Co_3O_4$ ,  $CoO_x$ -SnO<sub>x</sub> and  $CoO_x$ -ZnO, were prepared by different routes, followed by drying and calcination. Structural characterizations by IR, UV, XRD and TEM have revealed the successful preparation of nanosized  $Co_3O_4$  and composite  $CoO_r$ -MO<sub>r</sub> oxides. Cobalt oxide (Co<sub>3</sub>O<sub>4</sub>) prepared from cobalt nitrate was considerably active for the epoxidation of  $\alpha$ -pinene and cinnamyl chloride with air, in which 70.75 mol% of  $\alpha$ -pinene conversion with an epoxide selectivity of 87.68% was achieved at 363 K over 30 mg of Co<sub>3</sub>O<sub>4</sub>, superior to the catalysts reported in the literature. Over the catalyst Co<sub>3</sub>O<sub>4</sub> modified with OTAB, a high epoxide selectivity up to 92.12% was achieved with a conversion of 63.76 mol%  $\alpha$ -pinene at 363 K within 5 h. The catalytic activity of  $CoO_x$ -MO<sub>x</sub> catalysts on the epoxidation of  $\alpha$ -pinene with air gradually decreased in the sequence of 10:1  $CoO_x$ -SnO<sub>x</sub> > 2:1  $CoO_x$ -SnO<sub>x</sub> > 5:1  $CoO_x$ -ZnO > 10:1  $CoO_x$ -ZnO. However, for the epoxidation of cinnamyl chloride with air the catalytic activity of  $CoO_x$ -MO<sub>x</sub> exhibited a descending order of  $Co_3O_4$  (50.26 mol% of conversion) > 10:1  $CoO_x$ -ZnO (46.53 mol%) > 5:1 CoO<sub>x</sub>-ZnO (40.76 mol%) > 10:1  $CoO_r$ -SnO<sub>r</sub> (22.25 mol%) > ZnO (17.12 mol%), entirely different from the change of epoxide selectivity of 5:1  $CoO_x$ -ZnO (87.17%) > 10:1  $CoO_x$ -ZnO (81.37%) >  $Co_3O_4$  (60.28%) > 10:1  $CoO_x$ -SnO<sub>x</sub> (58.62%) > ZnO (37.93%).

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