

# **Integrated system for bioremediation of Nile tilapia rearing efuent and astaxanthin production by** *Haematococcus pluvialis*

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### **Abstract**

*Haematococcus pluvialis* is a microalga that can reduce the levels of inorganic and organic components in effluents, in addition to production of the high-value carotenoid astaxanthin. The present study proposed an integrated system for the simultaneous treatment of efuent from a Nile tilapia recirculation system and astaxanthin production using the microalga *H. pluvialis*. Cultures were developed in 2 L bottles, with freshwater previously treated and enriched with a modifed Bold's Basal Medium (BBM). The experiment was carried out on a laboratory scale using a completely randomized experimental design with fve treatments: control (100% BBM), E25 (25% Nile tilapia effluent +75% BBM), E50 (50% Nile tilapia effluent + 50% BBM), E75 (75% Nile tilapia effluent + 25% BBM), E100 (100% Nile tilapia effluent), with three replicates for each condition. *H. pluvialis* could grow in all proportions of effluent from Nile tilapia cultivation. The use of effluent as culture medium (E100), despite having lower cell density and biomass, resulted in biomass with high astaxanthin content (10 mg  $g^{-1}$ ) and antioxidant activity (89% inhibition of DPPH radicals). Meanwhile, this integrated system significantly contributed to the effluent remediation (98% N and 91% P removal). *H. pluvialis* can be used for cost-efective treatment of aquaculture effluent with simultaneous production of astaxanthin, with potential application as aquafeed, in a holistic bioeconomy approach.

**Keywords** Microalgae · High-value biomass · Antioxidant activity · Wastewater · RASbased system

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### **Introduction**

As a result of global population increase, several environmental problems such as contamination of soil and water bodies caused by improper disposal of efuents have intensifed, afecting the ecosystem functioning of aquatic and terrestrial environments (Chai et al. [2021\)](#page-11-0). In view of the pollution increase and scarcity of freshwater resources, the treatment and reuse of wastewater result in social, environmental, and economic benefts (Tortajada [2020\)](#page-12-0). Among the generated effluents, industrial and domestic effluents stand out, in addition to those from aquaculture, which when released into rivers and lakes lead to eutrophication (Nogueira et al. [2022\)](#page-12-1).

Fish rearing is a growing activity worldwide due to its economic, social, and nutritional impact, contributing signifcantly to achieve a few sustainable development goals of the 2030 Agenda (Ashour et al. [2021](#page-11-1); Wang et al. [2021](#page-12-2); Oliveira et al. [2022a\)](#page-12-3). The increase in this activity resulted, almost in the same proportion, in the increase in the production of efuents, which can cause environmental impacts due to the release of inorganic compounds, mainly nitrogen and phosphorus, from leftover feed and fsh excreta (Kurniawan et al. [2021](#page-11-2)). The recirculation aquaculture system (RAS) is a way to reduce the disposal of efuents containing high levels of inorganic compounds; however, due to the intensive mode of production, it is essential to treat waste both within the recirculation circuit and in the effluents of these systems (Rijn  $2013$ ). Nevertheless, the use of conventional chemical products can cause imbalance in the system's microbiota; thus, the use of algae and plants has proven to be an efficient way to solve this problem.

Algae require macronutrients and micronutrients and can absorb these compounds from effluents (Mohsenpour et al. [2021\)](#page-11-3). In recent years, studies have been carried out aimed at the use of microalgae for the bioremediation of diferent types of efuents (Daneshvar et al. [2019;](#page-11-4) Oliveira et al. [2020](#page-12-5); Chai et al. [2021](#page-11-0); Moraes et al. [2021](#page-12-6)). When cultivated in media rich in nitrogen, phosphorus, and organic carbon, microalgae can growth quickly, using heterotrophic or mixotrophic pathways—depending on the availability of light energy (Lv et al. [2018](#page-11-5); Perez-Garcia et al. [2011](#page-12-7)). Furthermore, algae can be inserted in several industrial segments, including agriculture, human and animal nutrition, and energy plants (Yap et al. [2021](#page-13-0); Oliveira et al. [2021](#page-12-8)). *Haematococcus pluvialis* is especially known for its high content of carotenoids, mainly astaxanthin (reaching a concentration of up to 5% of the cellular content) (Mota et al. [2022](#page-12-9)). Astaxanthin is a carotenoid with high antioxidant capacity, which acts to protect cells against free radical damage, combating oxidative stress and reducing the risk of diseases in humans and animals (Mota et al. [2022\)](#page-12-9). In recent years, astaxanthin has gained attention as a dietary supplement for animals, particularly in aquaculture (Lim et al. [2018\)](#page-11-6).

Studies have shown that astaxanthin feed supplementation in aquaculture can improve immune function, reduce infammation, increase resistance to environmental stressors, and improve reproductive performance, growth, and coloration (Lim et al. [2018;](#page-11-6) Ashour et al. [2021\)](#page-11-1). The use of *H. pluvialis* as a source of astaxanthin in animal feed ofers several advantages: it is a natural and sustainable source, with greater antioxidant power than the synthetic form (Mota et al. [2022\)](#page-12-9); it can be cultivated using wastewater as an environmentally friendly and low-cost culture medium (Pan et al. [2021\)](#page-12-10); the inclusion of *H. pluvialis* in animal feed can lead to an improvement in product quality (Su et al. [2020\)](#page-12-11).

Although several microalgae have been studied in terms of growth kinetics and nutrient uptake to treat aquaculture effluents, few studies have focused on evaluating the high-value commercial metabolites produced during the bioremediation process. In view of this, this

study proposed an integrated system for the bioremediation of effluents from a tilapia recirculation system and astaxanthin production by *H. pluvialis*, with potential application as aquafeed.

### **Material and methods**

#### **Strain and culture conditions**

*H. pluvialis* was obtained from the Live Food Production Laboratory, at the Fisheries and Aquaculture Department of the Federal Rural University of Pernambuco. Cultures were developed in 2 L bottles, with freshwater previously treated with chlorine (3 ppm), filtered (22  $\mu$ m) and autoclaved (120 °C), and then enriched with a modified version of Bold's Basal Medium (BBM) proposed by Moraes et al. [\(2023](#page-12-12)) that contains (in mg  $L^{-1}$ ) 118 NH<sub>4</sub>NO<sub>3</sub>; 25 CaCl<sub>2</sub>·2H<sub>2</sub>O; 25 NaCl; 31 KOH; 50 EDTA Na·2H<sub>2</sub>O; 75 K<sub>2</sub>HPO<sub>4</sub>; 175  $KH_2PO_4$ ; 4.98 FeSO<sub>4</sub>·7H<sub>2</sub>O; 75 MgSO<sub>4</sub>·7H<sub>2</sub>O; 11.42 H<sub>3</sub>BO<sub>3</sub>; 1.412 ZnSO<sub>4</sub>·7H<sub>2</sub>O; 0.232  $MnCl<sub>2</sub>·4H<sub>2</sub>O$ ; 0.252 CuSO<sub>4</sub>·5H<sub>2</sub>O; 0.192 Na<sub>2</sub>MoO<sub>4</sub>·2H<sub>2</sub>O; 0.08 Co(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O.

#### **Experimental design**

The experiment was carried out on a laboratory scale using a completely randomized experimental design with fve treatments: control (100% BBM), E25 (25% Nile tilapia effluent +75% BBM), E50 (50% Nile tilapia effluent +50% BBM), E75 (75% Nile tilapia effluent  $+25\%$  BBM), and E100 (100% Nile tilapia effluent), with three replicates each.

*H. pluvialis* was inoculated in 2 L bottles with an initial concentration of 20,000 cells mL−1, using 60 mL of inoculum, at a temperature of 22 °C, photoperiod of 12 h, and 40 µmol photons  $m^{-2}$  s<sup>-1</sup> irradiance, under continuous aeration. In the stationary phase, to stimulate the carotenogenesis (cystic phase), there was an increase in light intensity (40 to 100 µmol photons  $m^{-2} s^{-1}$ ), in addition to the natural nitrogen deprivation (Moraes et al. [2023](#page-12-12)).

#### **Efuent from Nile tilapia in Oasis® recirculation system**

The effluent from a culture tank of Nile tilapia (*Oreochromis niloticus*) in Oasis<sup>®</sup> production system was used for *H. pluvialis* cultivation. The Oasis® is a RAS-based system that aims at high productivity, low water renewal, and full use of the waste generated. In this system, Nile tilapias of about  $10.88 \pm 0.77$  cm and  $31.47 \pm 2.71$  g were cultivated for 45 days using a feed of 45% of crude protein ofered three times a day (ad libitum) and presenting a feed conversion factor of 0.98. The effluent was subjected to filtration  $(40 \,\mu m)$ , chlorination with sodium hypochlorite at 3 ppm for 24 h (with aeration), and autoclaving at 120  $\degree$ C for 15 min (Moraes et al. [2021](#page-12-6)). After these procedures, the effluent was character-ized regarding the concentrations of nitrogenous compounds and phosphate (APHA [2012](#page-11-7)). This effluent contained  $0.275 \pm 0.04$  mg L<sup>-1</sup> of NH<sub>3</sub>-N,  $0.846 \pm 0.01$  mg L<sup>-1</sup> of NO<sub>2</sub>-N,  $40.184 \pm 0.06$  mg L<sup>-1</sup> of NO<sub>3</sub>-N, and  $13.224 \pm 0.03$  mg L<sup>-1</sup> of PO<sub>4</sub>-P.

#### **Growth analysis and biomass harvesting**

To evaluate growth, samples were taken daily and fxed in formaldehyde (2%) for quantifcation using a hemocytometer (Neubauer chamber). The growth curves with the average daily cell density were ftted by approximating the logistic curve (Sproufske and Wagner [2016](#page-12-13)). The logistic equation describes the population size  $N_t$  at time *t* Eq. [\(1\)](#page-3-0):

<span id="page-3-0"></span>
$$
N_{t} = \frac{K}{1 + \left(\frac{K - N_{0}}{N_{0}}\right)e^{-rt}}
$$
(1)

where  $N_0$  is the population size at the beginning of the growth curve,  $K$  is the maximum possible population size in a particular environment, and *r* is the specifc growth rate. With this ft, the following parameters were calculated: specifc growth rate (*r*, day−1) and doubling time (DT, division day<sup>-1</sup>). The maximum specific growth rate ( $\mu_{\text{max}}$ ) was calculated according to the equations below.

The following asymmetric logistic Eq.  $(2)$  was used to fit the cell concentration  $(N(t))$  versus time (*t*) data in order to accurately determine the specifc growth rate:

<span id="page-3-1"></span>
$$
N(t) = y_0 + \frac{a}{\left[1 + e^{\frac{-(t-t_0)}{b}}\right]}
$$
 (2)

where *a*, *b*,  $t_0$ , and  $y_0$  are constants. The cell-specific growth rate ( $\mu$ , day<sup>-1</sup>) was calculated using the best fit curve of Eq.  $(2)$  $(2)$ ; thus:

<span id="page-3-2"></span>
$$
\mu(t) = \frac{1}{N(t)} \left( \frac{dN(t)}{dt} \right) \tag{3}
$$

where  $\mu_{\text{max}}$  (day<sup>-1</sup>) is the maximum specific growth rate in the exponential phase according to Eq.  $(3)$  $(3)$ .

For maximum cell density ( $C_{\text{max}}$ , cells mL<sup>-1</sup>), it was considered the day of culture in which the population reached the maximum cell density.

The dry biomass (g  $L^{-1}$ ) and biomass productivity (g  $L^{-1}$  day<sup>-1</sup>) were determined by filtering 10 mL aliquots of suspended cells through a Whatman GF/C glass microfber flter  $(1.2 \,\mu\text{m})$  and drying at 75 °C for 24 h (Choi et al. [2018\)](#page-11-8).

#### **Water quality and nitrogen removal**

The parameters of water quality, pH, temperature, ammonia-N  $(NH<sub>3</sub>-N)$ , nitrite-N  $(NO<sub>2</sub>-N)$ , nitrate–N ( $NO_3-N$ ), and phosphate-P ( $PO_4-P$ ) were analyzed in the culture medium on days 0 (frst day), 12 (exponential phase), and 20 (last day). Samples of 10 mL were fltered through a Whatman GF/C glass microfiber filter  $(1.2 \mu m)$ , and then, the filtered volume was collected for analysis of the nitrogen compounds and phosphate (APHA [2012\)](#page-11-7). The pH and temperature were measured using a digital pHmeter (Kmoon pH/EC-983).

The determination of the percentages of nutrient removal from the culture media was carried out at the end of the experiment using Eq. [4:](#page-3-3)

<span id="page-3-3"></span>
$$
Removal(\%) = 100 - \left(\frac{\text{final nutrient concentration}}{\text{initial nutrient concentration}}\right) \times 100\tag{4}
$$

### **Quantifcation of total carotenoids and astaxanthin**

The concentrations of total carotenoids and astaxanthin were determined at the end of cultivation. Carotenoid and astaxanthin analyses were performed from a 10 mL and 1 mL aliquot of the algae suspension, respectively, and analyzed in a spectrophotometer, according to Moraes et al.  $(2023)$  $(2023)$ .

The concentration of total carotenoids was calculated by  $[4 \times OD_{480}]$ , and astaxanthin concentration and content were calculated from the expressions  $[4.5 \times OD_{490} \times (Va)$ / Vb)] and [*P* / *W*], respectively, where Va (mL) was the volume of DMSO, Vb (mL) was the volume of microalgae samples,  $P$  (mg  $L^{-1}$ ) was the concentration of astaxanthin, and *W* (g  $L^{-1}$ ) denoted the dry biomass of microalgae per unit volume of medium (Cheng et al. [2016](#page-11-9)).

#### **Antioxidant activity**

Extracts of *H. pluvialis* biomass were obtained using 0.1 g of dried biomass resuspended and homogenized in 2 mL of 99.9% dimethyl sulfoxide. Afterwards, the mixture was centrifugated at 1000 rpm for 2 min. The supernatant was collected subjected to serial dilution  $(50, 25, 12.5, 6.25, \text{ and } 3.12 \text{ mg } \text{mL}^{-1})$  for posterior antioxidant assays as proposed by Oliveira et al.  $(2022b)$  $(2022b)$ . The antioxidant activity (inhibition %) of the extracts were evaluated by 2,2'-azino-bis (3-ethylbenzothiazoline-6-sulfonic acid) (ABTS<sup>+</sup>\*) (Guedes et al. [2013\)](#page-11-10) and 2,2-diphenyl-1-picrylhydrazyl (DPPH• ) (Dantas et al. [2019](#page-11-11)) methods. Trolox® was used as standards for calibration curve as well as positive control.

#### **Statistical analysis**

The response variables were submitted to the Shapiro–Wilk normality test and to the Bartlett's test of homogeneity of variances. All data were submitted to ANOVA followed by Tukey's test when a signifcant diference was observed. *p* values<0.05 were considered statistically signifcant for all tests. Statistical analysis was performed using the R Core Team software (R Core Team [2023\)](#page-12-15).

# **Results and discussion**

#### **Cell growth and biomass production of** *H. pluvialis*

*H. pluvialis* could grow in all proportions of the Oasis® effluent from Nile tilapia rearing. The variables growth rate (*r*), doubling time (DT), and maximum specifc growth rate  $(\mu_{\text{max}})$  were higher for treatments E0 (control) and E75 followed by E100, while the lowest values were presented by E50 and E25. On the other hand, the maximum cell density  $(C_{\text{max}})$  was higher at E0 and E25; these treatments were significantly different from E50, E75, and E100 (Table [1\)](#page-5-0).

Regarding the biomass, E0 and E25 obtained the highest values, with an average yield of 0.75 g L<sup>-1</sup> and average productivity of 0.047 g L<sup>-1</sup> day<sup>-1</sup>. While E50 and E75 showed



**Table 1** Growth variables of *Haematococcus pluvialis* cultivated with diferent proportions of BBM culture medium and efuent from the Nile tilapia farming in Oasis® sys-

Table 1 Growth variables of Haematococcus pluvialis cultivated with different proportions of BBM culture medium and effluent from the Nile tilapia farming in Oasis® sys-

<span id="page-5-0"></span>

an average yield and productivity of 0.61 g L<sup>-1</sup> and 0.038 g L<sup>-1</sup> day<sup>-1</sup>. E100 was significantly diferent for all treatments, except E75, and showed average yield and productivity of 0.53 g L<sup>-1</sup> and 0.033 g L<sup>-1</sup> day<sup>-1</sup> (Table [1\)](#page-5-0).

The growth curves of *H. pluvialis* which show the daily cell densities of each treatment are presented in Fig. [1](#page-6-0). The control treatment (E0) presented a longer exponential phase than the others. This may have occurred due to the availability of mixed sources of nitrogen in the effluent. Once the higher affinity nitrogen source, ammonia, is depleted, there is a metabolic readjustment to absorb the following sources, nitrate and nitrite (Su [2021](#page-12-16)). This condition justifes the "pseudo-stationary phases" along the efuent treatment curves, which may infuence the lower growth. Possibly, vegetative cells multiplied later compared to the control and treatment with lower percentage of effluent addition (i.e., E25), resulting in a lower cell density in treatments E75 and E100.

Besides the presence of nutrients, like nitrogen, other physicochemical aspects play a crucial role in cellular metabolism, such as temperature and pH. Maintaining minimal pH fuctuations ensures a more consistent chemical environment and, as a result, improved conditions for the division of *H. pluvialis* cells (Dos Santos and Lombardi [2017\)](#page-11-12). In this study, the initial pH had no significant difference between treatments  $(p > 0.05)$ , with an average of  $7.2 \pm 0.2$ ; generally, at an initial pH of 7, greater growth of *H. pluvialis* is observed (Sarada et al. [2002\)](#page-12-17). The pH variation until the end of cultivation was higher in treatments E50, E75, and E100  $(8.4 \pm 0.03, 8.26 \pm 0.01, 8.37 \pm 0.05,$  respectively), differing



<span id="page-6-0"></span>Fig. 1 Logistic growth curve of *H. pluvialis* cultivated under different proportions of BBM and effluent from the Nile tilapia Oasis® system

significantly of treatments E0 and E25 (7.8 $\pm$ 0.01, 7.9 $\pm$ 0.02). This may also have influenced the lower  $C_{\text{max}}$ , biomass, and biomass productivity in treatments with a higher proportion of effluent (i.e., E50, E75, and E100). The temperature had no significant difference between treatments or over time, remaining at  $22.2 \pm 0.4$  °C.

#### **Removal of nitrogen and phosphate compounds by** *H. pluvialis*

Regarding nitrogen sources, ammonia is the nitrogen compound most easily incorporated by microalgae (Su [2021\)](#page-12-16). Thus, for microalgae in general, the order of preference for nitrogen utilization is  $NH_4^+ - > NO_3 - > NO_2$ , due to no redox reaction requirement and less energy cost to assimilate ammonia (Ramanna et al. [2014\)](#page-12-18). Ammonia was more abundant (25 mg  $L^{-1}$ ) in the treatments with higher amounts of BBM, i.e., E0 and E25 (Fig. [2a](#page-7-0)), which showed higher  $C_{\text{max}}$ , biomass, and biomass productivity (Table [1](#page-5-0)). Despite that, the total nitrogen concentration was similar for the treatments, with an average of 40 mg  $L^{-1}$ . Hence, nitrogen in the form of ammonium contributed to greater biomass, like previous studies also conducted with *H. pluvialis* using different effluents (Mourya et al. [2023](#page-12-19); Yap et al. [2022](#page-13-1)). For example, Pan et al. ([2021\)](#page-12-10) demonstrated a removal of  $83.4\%$  of NH<sub>4</sub>-N from potato juice wastewater after methanation and acidifcation of the efuent. Integrating



<span id="page-7-0"></span>**Fig. 2** Concentrations of  $NH_3-N$  (**a**),  $NO_2-N$  (**b**),  $NO_3-N$  (**c**), and  $PO_4-P$  (**d**) over 20 days and uptake of nitrogen and phosphate compounds (e) by *H. pluvialis* under different proportions of BBM and effluent from the Nile tilapia Oasis.® system. Different letters indicate a significant difference among treatments by the Tukey's post hoc test  $(p < 0.05)$ 

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processes with other microorganisms can optimize growth conditions, making other compounds bioavailable to algae, and increasing the uptake rates.

*H. pluvialis* only uses other sources of nitrogen, such as nitrate and nitrite, when ammonia is no longer available in the environment (Markou and Georgakakis [2011\)](#page-11-13). The average initial concentration of NO<sub>2</sub>-N in treatments E75 and E100 was 0.8 mg L<sup>-1</sup>, while for treat-ments E0 and E[2](#page-7-0)5, it was  $0.04$  and  $0.2$  mg L<sup>-1</sup>, respectively (Fig. 2b). Meanwhile, higher concentrations of NO<sub>3</sub>-N (27–40 mg L<sup>-1</sup>) were found in treatments with a high proportion of efuent (E100 and E75) (Fig. [2c](#page-7-0)). The nitrogen uptake by *H. pluvialis* in the efuent was more than 95% for NH<sub>3</sub>-N (except in E100 that reached 52%), 94% for NO<sub>3</sub>-N, and  $100\%$  for NO<sub>2</sub>-N (Fig. [2e](#page-7-0)). Regarding the total nitrogen concentration, there was an average absorption of 97.7% for all treatments, being the highest absorption in E75 (99.5%), whose growth velocity data  $r$  and  $\mu_{\text{max}}$  were higher.

In addition to nitrogen, phosphorus is an essential element as it assists in metabolic processes, photosynthesis, and energy conversion (Marinho et al. [2021\)](#page-11-14). The initial concentra-tion of PO<sub>4</sub>-P varied between 13 (E100) and [2](#page-7-0)4 mg L<sup>-1</sup> (E0) (Fig. 2d), being consumed by the microalgae throughout the cultivation, with a final removal efficiency of 84 to  $98\%$ (Fig. [2](#page-7-0)e). The highest phosphate absorption occurred in E75 and E100, which had a lower initial concentration of  $PO<sub>4</sub>$ -P.

In summary, the results of the study indicate that *H. pluvialis* has a signifcant ability to capture nutrients from effluent, improving, therefore, the levels of these compounds in the water, and this is in agreement with previous studies (Wu et al. [2013](#page-12-20); Mourya et al. [2023;](#page-12-19) Pan et al. [2021](#page-12-10); Yap et al. [2022](#page-13-1)).

#### **Production of high‑value metabolites from** *H. pluvialis*

In addition to *H. pluvialis* acting in the bioremediation of efuent, it can produce highvalue metabolites such as carotenoids, especially astaxanthin (80–99% of total carotenoids). As for the total carotenoids obtained in the cystic phase, higher concentrations (5.32–6.06 mg L<sup>-1</sup>) and content (7.6–10.1 mg g<sup>-1</sup>) were observed in the treatments E0, E25, and E100 (Fig. [3](#page-9-0)a, b). Following the same trend, higher concentrations (5.34–5.50 mg  $L^{-1}$ ) and content (7.26–10.25 mg g<sup>-1</sup>) of astaxanthin were obtained in treatments E0, E25, and E100 (Fig. [3c](#page-9-0), d).

Astaxanthin synthesis occurs under nutrient starvation (i.e., nitrogen and phosphate), which triggers the upregulation of genes associated with astaxanthin biosynthesis to act in defense metabolism to this stress condition (Liyanaarachchi et al. [2020\)](#page-11-15). On day 20, total nitrogen depletion was observed in all treatments, accompanied by a predominance of cystic cells, with accumulation of astaxanthin. Furthermore, under nitrogen deprivation, the carbon fux is directed towards the synthesis of astaxanthin (Lu et al. [2019;](#page-11-16) Moraes et al.  $2023$ ). The use of effluent from the Nile tilapia recirculation system (E100) contributed to the high content of astaxanthin (10 mg  $g^{-1}$ ), similar to E0 and E25, although E100 had a low biomass compared to these treatments. The use of effluent replacing the culture medium was a stress factor for microalgae, primarily attributed to the signifcantly reduced initial concentration of  $PQ_4$ -P (1.8 times lower than E0), leading to low growth and greater astaxanthin production.

Astaxanthin is a carotenoid widely used in the pharmaceutical, nutraceutical, cosmetic, and food industries, in addition to aquaculture, both for pigmentation and to improve the immune response and zootechnical performance of aquatic organisms (Lim et al. [2018](#page-11-6); Su et al. [2020](#page-12-11)). This carotenoid has anti-infammatory, antitumor, antidiabetic,



<span id="page-9-0"></span>**Fig. 3** Concentrations (mg L−1) and contents (mg g.−1) of total carotenoids (**a**, **b**) and astaxanthin (**c**, **d**) produced by *Haematococcus pluvialis* cultivated in different proportions of BBM and effluent from the Nile tilapia Oasis® system (diferent letters indicate a signifcant diference by the Tukey's post hoc test  $(p < 0.05)$ 

immunomodulatory, and antioxidant properties, highlighting its antioxidant activity, which is 10 times greater than that of β-carotene (Mota et al.  $2022$ ). The antioxidant activity of microalgal biomass extract cultured in effluent from Oasis® system was investigated using ABTS and DPPH assays (Table [2\)](#page-9-1). As noted, all treatments exhibited antioxidant efects, even at varying degrees (47.4–88.7% inhibition). The highest percentages of inhibition of ABTS and DPPH radicals were presented by treatments E50 (73.9 $\pm$ 7.9%) and E100  $(88.7 \pm 1.5\%)$ , respectively. The percentage of inhibition observed in the present study was

<span id="page-9-1"></span>

Diferent letters on the same column indicate a signifcant diference by the Tukey's post hoc test  $(p < 0.05)$ 

like that reported by Al-Tarif et al. ([2020\)](#page-11-17), using the same solvent (DMSO) for astaxanthin powder, approximately 85% inhibition of DPPH radical. Therefore, the biomass produced in effluent showed greater antioxidant activity.

The findings indicate that the biomass of *H. pluvialis*, cultivated in effluent from Nile tilapia rearing—which is rich in astaxanthin and possesses high antioxidant properties holds potential for utilization in aquaculture feed. This aquafeed could be used in the production of tilapia in the Oasis® system, as well as the treated water could be returned to replenish the cultivation system, in a circular economy approach. Furthermore, the astaxanthin from *H. pluvialis* biomass has promise as a bioactive compound in nutraceutical and pharmaceutical products for human applications. Thus, the use of effluent as a culture medium contributes to the sustainable production of *H. pluvialis* biomass and astaxanthin, considering the replacement of high-cost culture media, the valorization of effluents in high-value metabolites, and the treatment of effluents (potential source of contamination for the environment).

# **Conclusions**

*H. pluvialis* was able to grow in all proportions of RAS efuent from the Nile tilapia rearing. The use of efuent as culture medium, despite having lower cell density and biomass, had a higher astaxanthin content. Therefore, the present study proposes an ecofriendly and low-cost medium formed only by effluent from the Nile tilapia recirculation system for astaxanthin production. Meanwhile, the integrated system contributed to the effluent remediation. *H. pluvialis* can be used for cost-effective treatment of aquaculture effluent with simultaneous production of astaxanthin with great potential for a holistic bioeconomy.

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**Author contribution** LM: writing—original draft, conceptualization, investigation, methodology, formal analysis, and data curation. GM and BS: investigation, methodology, and formal analysis. CO: formal analysis, data curation, and writing—review and editing. JS: resources and data curation. AG: resources, supervision, and writing—review and editing. RB: study conception and design, resources, and project administration.

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**Data availability** The authors certify that all data support the published claims and comply with feld standards.

**Code availability** Not applicable.

# **Declarations**

**Competing interests** The authors declare no competing interests.

**Ethics approval** This article does not contain any studies with animals performed by any of the authors.

**Confict of interest** The authors declare no competing interests.

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