## Numerical simulation of effect of convection-diffusion on oxygen transport in microcirculation<sup>\*</sup>

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Abstract The entire process of oxygen transport in microcirculation by developing a 3D porous media model is calculated numerically with coupled solid deformation-fluid seepage-convection and diffusion . The principal novelty of the model is that it takes into account volumetric deformation of both capillary and tissues resulting from capillary fluctuation. How solid deformation, fluid seepage, and convection-diffusion combine to affect oxygen transport is examined quantitatively: (1) Solid deformation is more significant in the middle of capillary, where the maximum value of volumetric deformation reaches about 0.5%. (2) Solid deformation has positive influence on the tissue fluid so that it flows more uniformly and causes oxygen to be transported more uniformly, and eventually impacts oxygen concentration by 0.1%–0.5%. (3) Convection-diffusion coupled deformation and seepage has a maximum (16%) and average (3%) increase in oxygen concentration, compared with pure molecular diffusion. Its more significant role is to allow oxygen to be transported more evenly.

**Key words** porous medium, microcirculation, oxygen transport, convection-diffusion, solid deformation, fluid seepage

Chinese Library Classification 0241 2010 Mathematics Subject Classification 92C10

#### 1 Introduction

Oxygen is primarily carried in the form of oxyhemoglobin, that is, bound to the hemoglobin (Hb) molecules inside red blood cells (RBCs). The process that oxygen is released from RBCs to plasma and is transported to cells is accomplished in the microcirculation<sup>[1]</sup>. The microcirculation, which comprises arterioles, venules, and capillaries, is very different from that in large arteries and it is appropriate to consider the flow properties within them separately. Understanding the oxygen transport properties at micro level is a difficult and fundamental topic and it is helpful for gaining insight into a number of diseases that involve the microcirculation<sup>[2–4]</sup>. Capillaries are where fluid, gasses, nutrients, and wastes are exchanged between the blood and body tissue by diffusion. Capillary walls contain small pores that allow certain substances to pass into and out of the blood vessel. Water and small solutes are allowed to pass through

<sup>\*</sup> Received May 24, 2014 / Revised Aug. 23, 2014

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its pores but proteins are not allowed. As blood enters the capillary bed on the arteriole end, fluid moves from the vessel to the body tissue. At the middle of the capillary bed, fluid passes equally between the capillary vessel and the body tissue. Oxygen is also exchanged at this point. On the venule end of the capillary bed, fluid, carbon dioxide and wastes are drawn from the body tissue into the capillary vessel<sup>[5–6]</sup>.

Various theoretical, experimental, and numerical studies have been performed. The first attempt to mathematically describe the phenomenon of oxygen supply to living tissues through the microcirculation of blood was the classical Krogh's model<sup>[7]</sup>. This model dealt with an idealized geometric arrangement, consisting of one capillary of circular cross-section concentric with a circular cross-section of muscle tissue. This pioneering theoretical model was built on a number of idealized assumptions, including constant oxygen consumption rate, uniform oxygen diffusivity, and homogeneous capillary distribution<sup>[8]</sup>. The derivation of this model in tissue sub-domain was found, in terms of the diffusion equation<sup>[9]</sup>. Since then, much attention has been focused on the role of oxygen transport to tissues, leading to more advanced mathematical models for the movement of oxygen, incorporating variable oxygen consumption rate, intravascular oxygen transport resistance, myoglobin (Mb) facilitated diffusion, axial oxygen diffusion in the tissue, time dependent oxygen transport, pre- and post-capillary transport and flow redistribution<sup>[10-12]</sup>. In early studies, tissue oxygen consumption was often assumed to be uniform, then oxygen dependent consumption was proposed to simulate the oxygen delivery under hypertension<sup>[13]</sup> and under the condition of high oxygen demand<sup>[14]</sup>. A global existence of a unique smooth solution of the nonlinear diffusion of oxygen in tissue, in presence of consumption due to metabolism, was discussed<sup>[15]</sup>. Yulianti and Gunawan proposed a critical ratio between supply and consumption of oxygen in tissue region in order to fulfill cell's oxygen  $requirements^{[16]}$ .

In addition, axial oxygen diffusion in the tissue has been found important for the transport of solute in microcirculation, but axial diffusion inside following capillaries is less important due to the relatively greater effect of axial convection<sup>[17]</sup>. An asymptotic solution for a diffusion problem in 2D to describe oxygen transport from multi-capillaries to skeletal muscle tissue was studied<sup>[18]</sup> and a system of ordinary differential equations for oxygen transport in 2D array of capillaries were coupled with a system of algebraic equations for the fluxes<sup>[19]</sup>. Several studies used time-dependent Krogh-type models since the convective oxygen supply to individual capillaries could vary considerably over time and there were many problems of interest in which time dependent oxygen transport is relevant<sup>[20]</sup>. Arterioles and venules were also involved in blood-tissue diffusive oxygen transport, and it was important to understand how they carry oxygen and release oxygen to tissue<sup>[21–22]</sup>.

Lots of theoretical models for solute transport based on porous medium mechanics were established<sup>[23-26]</sup>. Schuff presented a comprehensive model that included transport in the vessel lumen, the vessel wall, and the interstitial space and considered the effect of the solute concentration on fluid flow<sup>[27-28]</sup>. This was used to examine fluid and solute transport for simplified case of an axisymmetric geometry but no solid deformation.

Though the knowledge of oxygen transport has revealed that oxygen has the ability to transport from any capillary to another location under the conditions in which there exists a large enough oxygen tension gradient and that the seepage for oxygen along the intervening pathway is sufficient<sup>[29–30]</sup>, the effect of convection-diffusion and deformation of tissue scaffold had not been paid sufficient attention. It was generally viewed that convection of oxygen within tissue could be neglected because many studies considered that tissue fluid flowed very slowly within tissues. However, the deficiency remains existing in studying for seepage of tissue fluid: seepage might be significantly affected by the deformation of microcirculatory structure which could be caused by capillary fluctuation. The deformations at micro level are very difficult to be measured by the experiments biologically. Thus, the deformation was considered and studied in some relevant mathematical models<sup>[31–32]</sup>. Therefore, we take account of oxygen transport in

deformable porous media, where the volumetric deformation is modelled based on the pressure variations of capillary fluctuation from experiments<sup>[33]</sup>.

In the present study, we develop a mathematical model based on a porous medium mechanics, coupling solid deformation of tissue scaffold, fluid seepage, convection-diffusion and molecular diffusion, and study the convection-diffusion of oxygen on oxygen transport at micro level, especially within tissue. Based on this more comprehensive model, the effects of seepage, deformation, and convection-diffusion on oxygen transport are discussed and the numerical results of the distributions of pore pressure, seepage velocity, and oxygen concentration are presented as below.

### 2 General coupled mathematical model with solid deformation, fluid seepage, and convection-diffusion and molecular diffusion

A general system of the coupled mathematical model for solute transport in microcirculation with solid deformation, fluid seepage, and convection-diffusion and molecular diffusion of solute is presented below.

#### 2.1 Basic assumptions

Based on physiological regulations of oxygen transport in the microcirculation, the assumptions are proposed as follows:

(i) The computational domain is modelled as a porous medium, which is assumed to be isotropic and uniform.

(ii) Solid scaffold in the porous medium is modelled as continuously elastic, of which deformation complies with Hooke's law.

(iii) The microcirculatory system is assumed to be a saturated porous medium due to the fact that the interstitial space is normally filled with tissue fluid.

(iv) The volume deformation of the saturated porous medium includes two parts: the deformation of solid framework and pore<sup>[34]</sup>. Since the volume deformation of framework is substantially smaller than that of pore, we assume the volume deformation of the porous medium to be equal to pore deformation.

(v) The pore pressure in the tissue complies with Biot's effective stress law.

(vi) The fluid seepage complies with Darcy's law.

(vii) Mass transport by convection-diffusion and molecular diffusion follows Fick's law.

(viii) The microcirculatory system is considered as a thermodynamic equilibrium system.

#### 2.2 Governing equations of solid deformation

Capillary network and cells are modelled as solids, while all other phases are fluids. From the assumption (ii), solid deformation can be expressed by General Hooke's equation

$$\sigma_{ij}' = \lambda e \delta_{ij} + 2\mu \varepsilon_{ij},\tag{1}$$

$$\Theta' = \sigma'_x + \sigma'_y + \sigma'_z = Ke,\tag{2}$$

where  $\sigma'_{ij}$  is the effective stress tensor,  $\varepsilon_{ij}$  is the strain tensor,  $\lambda$  and  $\mu$  are the Lamé constants, e is the volumetric deformation,  $\delta_{ij}$  is the Kronecker tensor, K is the volume modulus,  $\Theta'$  is the effective volume stress, and  $\sigma'_x, \sigma'_y$ , and  $\sigma'_z$  represent the effective stresses in the x-, y-, and z-directions, respectively. According to the assumption (v), the total stress can be expressed as

$$\sigma_{ij} = \sigma'_{ij} + \alpha p \delta_{ij}. \tag{3}$$

The stress equilibrium can be written as

$$\sigma_{ij,j} + F_i = 0. \tag{4}$$

Substituting (3) into (4), we get

$$\sigma'_{ij,j} + F_i + (\alpha p)_{,i} = 0. \tag{5}$$

Substituting (1) into (5), we get the solid deformation equation taking into account the pore pressure expressed by the displacement which is the Lamé-Navier equation, i.e.,

$$(\lambda + \mu) u_{i,ji} + \mu u_{i,jj} + F_i + (\alpha p)_{,i} = 0.$$
(6)

Assume that the compression strain is positive and the tensile strain is negative.  $\lambda$  and  $\mu$  are the Lamé coefficients,  $F_i$  is the external force,  $\alpha = 1$  is the effective stress coefficient, p is the pore pressure, and  $u_{i,j}$  is the displacement tensor. In addition,  $\lambda$ ,  $\mu$ , and K all can be expressed as the function of the Young modulus E and the Poisson ratio v of material, i.e.,  $\lambda = \frac{Ev}{(1+v)(1-2v)}$ ,  $\mu = \frac{E}{2(1+v)}$ , and  $K = \frac{E}{3(1-2v)}$ . 2.3 Governing equations of fluid seepage

The mass equilibrium equation for per unit volume of fluid is given by

$$\operatorname{div}(\rho q) = \frac{\partial (n\rho)}{\partial t} - W = \rho \frac{\partial n}{\partial t} + n \frac{\partial \rho}{\partial t} - W, \tag{7}$$

where  $\rho$  is the density of fluid, t is time, n is porosity, q is the seepage velocity of fluid with the unit "volume/time/area", i.e.,  $cm^3 \cdot s^{-1} \cdot cm^{-2} = cm/s$ , and W is the source or sink of fluid. According to the assumption (vi), we have  $q_i = k_{ij}p_{,j}$ , where p is the pore pressure in (3), and  $k_{ij}$  is the permeability coefficient. From assumptions (iii) and (iv),  $\frac{\partial e}{\partial t} = -\frac{\partial n}{\partial t}$ . Because of the micro compressibility of fluid,  $\frac{\partial \rho}{\partial t} = -\beta \rho \frac{\partial p}{\partial t}$ , in which  $\beta$  is the compressibility coefficient of water. Substituting them into (7), we get div  $(\rho q) = -\rho \frac{\partial e}{\partial t} - \beta \rho n \frac{\partial p}{\partial t} - W$  finally. The fluid seepage equation taking account of solid deformation is

$$\left(k\left(\Theta,p\right)p_{,j}\right)_{,j} = \beta n \frac{\partial p}{\partial t} + \frac{\partial e}{\partial t} + W,\tag{8}$$

where  $\beta n$  indicates the compressibility coefficient of the tissue fluid, and  $k(\Theta, p)$  is given to be constant for assumption (i) in Table 1. Comparing with the oxygen transport model that only considers molecular diffusion, some modifications in this coupled mathematical model are shown as follows:

(I) Considering the interaction with fluid seepage and solid deformation of cells and capillary wall, the term  $\frac{\partial e}{\partial t}$  is added into the seepage (8).

(II) The term  $(\alpha p)_{,i}$  is added into the solid deformation (6).

#### 2.4 Governing equations of convection-diffusion and molecular diffusion

From the assumption (vii), the diffusion flux can be expressed by Fick's tensor equation, i.e.,

$$J_i = -D_{ij} \frac{\partial C}{\partial x_i},\tag{9}$$

where  $J_i$  is the diffusion flux tensor, C is the concentration of solutions and the function of time and position, and  $D_{ij}$  is the diffusion coefficient. The mass conservation for oxygen in the microcirculation is given as

$$\frac{\partial C_{\mathrm{O}_2}}{\partial t} = \frac{\partial}{\partial x_i} \left( D_{ij} \frac{\partial C_{\mathrm{O}_2}}{\partial x_i} \right) - \frac{\partial}{\partial x_i} (C_{\mathrm{O}_2} V_i) + I, \tag{10}$$

where the seepage velocity of fluid is q in (7).  $V_i$  in (10) also indicates seepage velocity of fluid because  $V_i$  is commonly used in the convection-diffusion and molecular diffusion equation. I is a source and sink term of oxygen related to oxygen solubility in fluid and oxygen consumption. The first term on the right side indicates oxygen transport by molecular diffusion, and the second term indicates oxygen transport by convection-diffusion.

#### 2.5 Coupled model

The coupled model for oxygen transport consists of (6), (8), and (10) as follows:

$$\begin{cases} (kp_{,j})_{,j} = \beta n \frac{\partial p}{\partial t} + \frac{\partial e}{\partial t} + W, \\ (\lambda + \mu) u_{i,ji} + \mu u_{i,jj} + F_i + (\alpha p)_{,i} = 0, \\ \frac{\partial C_{O_2}}{\partial t} = (D_{ij}C_{O_2,i})_{,i} - (C_{O_2}V_i)_{,i} + I. \end{cases}$$
(11)

All the equations expressed as tensor are solved by the finite element method (FEM).

#### 3 Application of coupled model for oxygen transport

Based on the above coupled model for solute transport, this section focuses on the oxygen distribution in microcirculation.  $C_{O_2}$  is necessary for solving (10) and is calculated by using the oxygen partial pressure in plasma  $P_{O_2}$ .

#### 3.1 Hemoglobin saturation

Oxygen is carried dissolved in the plasma, but to a much lesser degree. Hemoglobin is the primary vehicle for transporting oxygen in the blood. The relationship between the fractional saturation of hemoglobin with oxygen of  $S_{O_2}$  and blood oxygen partial pressure of  $P_{O_2}$  is proposed by the most common equation of two-parameter Hill's equation as follows:

$$S_{O_2} = \frac{\left(P_{O_2}/P_{50}\right)^m}{1 + \left(P_{O_2}/P_{50}\right)^m},\tag{12}$$

where  $P_{50}=3.626.4$  Pa is the oxygen tension at 50% saturation, and the dimensionless exponent is m = 2.6. When the arterial blood reaches the capillary bed, its  $P_{O_2}$ , oxygen partial pressure in plasma, is about 12665.6 Pa on arteriole end, while  $P_{O_2}$  in the interstitial tissue averages only 5332.9 Pa and entering the systemic veins is also about 5332.9 Pa<sup>[35]</sup>. Therefore, we take  $P_{O_2}=12665.6$  Pa in arteriole end and  $P_{O_2}=5332.9$  Pa in venule end. The total oxygen volume concentration within capillary vessel can be expressed as

$$C_{\rm O_2} = 1.39 S_{\rm O_2} \varphi \delta + K_{\rm O_2} (1 - \varphi) P_{\rm O_2}.$$
 (13)

The first term on the right side indicates the concentration of oxygen bound to Hb where  $\varphi = 0.45$  is the volume concentration of RBCs in blood,  $\delta = 0.25$  is the volume concentration of Hb in RBC, and  $S_{O_2}$  is obtained from (12). The second term indicates that concentration of oxygen dissolved in plasma follows Henry's Law, where  $K_{O_2}$  is solubility of oxygen in plasma in the human body.

#### 3.2 Oxygen exchange between RBC and plasma

Because oxygen bound to Hb has to dissociate from Hb and pass through RBC membrane into plasma, oxygen molecules can pass through the capillary wall into the tissues. Here, the following assumptions about the source for oxygen are proposed:

(i) Reduced oxygen in suspension in RBC to diffuse into the plasma can be supplied instantaneously from oxygen dissociated from Hb.

(ii) Oxygen can be transported instantaneously through the RBC membrane.

(iii) Hb concentration is considered as a constant in the process of oxygen bound to Hb and dissociated from Hb.

(iv) The molecular of Hb is much larger than that of oxygen, so whether oxygen absorbed in Hb or released from Hb, the diffusion coefficient of Hb remains a constant.

 $t_0$  is the initial time. Assume that  $C_{O_2}$  in plasma decreases  $\Delta C(x, t_0)$  from  $t_0$  to  $t_1$ . Then,  $C_{O_2}$  at  $t_1$  can be expressed as

$$C_{O_2}(x, t_1) = C_{O_2}(x, t_0) - \Delta C(x, t_0).$$
(14)

Since capillary  $C_{O_2}$  decreases,  $P_{O_2}$  also decreases to  $P_{O_2}(x, t_1)$ . From the assumptions,  $C_{O_2}$  also can be expressed by (13) as follows:

$$C_{O_2}(x, t_1) = 1.39 S_{O_2} \varphi \delta + K_{O_2}(1 - \varphi) P_{O_2}(x, t_1), \tag{15}$$

where  $S_{O_2}$  is the function of  $P_{O_2}$  and can be computed from (12) as follows:

$$S_{O_2} = S_{O_2} \left( P_{O_2}(x, t_0) \right). \tag{16}$$

Combining (14) and (15) and substituting (16) into (15) to get the results of  $P_{O_2}(x, t_1)$ , which is O<sub>2</sub> partial tension at  $t_1$  with decrease of oxygen concentration. From assumption (ii) in this section, oxygen partial pressure is changed instantaneously to  $P'_{O_2}(x, t_1)$  which can be obtained by (15) as follows:

$$\begin{cases} C'_{O_2}(\mathbf{x}, t_1) = 1.39 S_{O_2} \varphi \delta + K_{O_2} (1 - \varphi) P'_{O_2}(\mathbf{x}, t_1), \\ S'_{O_2} = S_{O_2} \left( P'_{O_2}(x, t_1) \right), \end{cases}$$
(17)

where  $P'_{O_2}(x, t_1)$  also can be used as the value of  $P_{O_2}(x, t_2)$  at  $t_2$ . The optimization method is used for solving  $C_{O_2}$  from (17), owing to the calculation error of the least squares solution is very small, only  $0.4345 \times 10^{-4}$ .

#### 3.3 Source and sink of oxygen

Two essential parameters of the density of cells and oxygen consumption rate for body cells are necessary to solve oxygen transport problem. Here, cells consume oxygen is known at a rate of  $6.25 \times 10^{-17} \,\mathrm{M} \cdot \mathrm{cells}^{-1} \cdot \mathrm{s}^{-1[36]}$ . Assume the tumor cells density in tissues as  $6.7 \times 10^7 \,\mathrm{cells} \cdot \mathrm{mL}^{-1[37]}$ , and since we know that 1 M of oxygen occupies 22 400 mL, then we calculate  $C_{\mathrm{used} O_2} = 6.25 \times 10^{-17} \times 6.7 \times 10^7 \times 22 \,400 = 9.38 \times 10^{-5} \,\mathrm{mL} \cdot \mathrm{mL}^{-1} \cdot \mathrm{s}^{-1}$ . Because the parameters of cells density in tissue and oxygen consumption rate would alter in the different organs, even normal cells and tumor cells, here we assume oxygen consumption rate for normal body cells, i.e.,  $C_{\mathrm{used} O_2} = 5.38 \times 10^{-5} \,\mathrm{mL} \cdot \mathrm{mL}^{-1} \cdot \mathrm{s}^{-1}$ . This mathematical model is solved by the FEM, where each element represents as a volume unit, not a single cell.

#### 3.4 Capillary fluctuation

Capillary fluctuation acts as the source power for solid deformation. There are several time scales of pressure variation within a given capillary. First, there are cardiac oscillations, which could be observed throughout the length of the capillary. Their normal amplitude is about 0.01– $0.02 \times 10^4 \,\mathrm{N \cdot m^{-2}}$  (Type I). The propagation of these oscillations through the microcirculation is discussed below. The second form of these fluctuations is one lasting for 15–20s and is associated with pressure variation in the region of  $0.04-0.07 \times 10^4 \,\mathrm{N \cdot m^{-2}}$ ; the pattern of such changes is random (Type II). The third type of pressure variation is more substantial and lasts longer. It is in the region of  $0.13 \times 10^4 \,\mathrm{N \cdot m^{-2}}$  and occurs over a period of 5–8 min, followed by a return to the steady state condition in about 2–3 min (Type III)<sup>[33,38]</sup>.

# 4 Numerical simulation on oxygen transport by convection-diffusion and molecular diffusion

#### 4.1 Geometry and boundary conditions of model

Parallel capillary-tissue cylinder arrangement was proposed by Ref. [7] and is widely applied to study many problems on microcirculation. The oversimplification of real situation introduces the concept of repetitive unit structure. Such a unit structure implies that each section of capillary is responsible for the supply of a corresponding cylindrical section of the surrounding tissue. In order to model more realistic phenomenon of oxygen supply, arteriole end and venule end are incorporated. Since the main aim of this paper is to examine the effect of convectiondiffusion on oxygen distribution, a single parallel capillary tissue as computational model is employed, but complex capillary network is not incorporated. Geometry and boundary conditions of the physical model are shown in Fig. 1. The radius of capillary is  $3\,\mu$ m, the thickness of capillary wall is  $0.3\,\mu$ m, the distance between two parallel capillaries is  $36\,\mu$ m, and the length of capillaries is  $630\,\mu$ m. For the solid deformation model, normal displacement on all six surfaces is zero; for seepage model, the permeability flux is assumed to be zero on all six surfaces of our model, i.e., the directional derivative of pore pressure  $p, \frac{\partial p}{\partial n} = 0$ ; for the convection-diffusion and molecular diffusion model, the directional derivative of oxygen concentration  $\frac{\partial C_{O_2}}{\partial n} = 0$  on all of six surfaces. On arteriole end of the capillary,  $P_{t_0} = 0.26 \,\text{N/cm}^2$  respectively at the x-, y-, and z-directions of all the nodes and  $C_{O_2}(t_0) = 0.001\,664\,\text{cm}^3/\text{cm}^3$  (calculated from (13)).



Fig. 1 Geometry and physical conditions of (a) solid deformation model, (b) seepage model, and (c) convection-diffusion and molecular diffusion model

#### 4.2 FEM

The program flowchart for FEM method is shown in Fig. 2. Solid deformation and fluid seepage model are solved by iterative method, then the seepage velocity is substituted into (10) to obtain the oxygen concentration of convection-diffusion. The computational time step  $\Delta t=0.0625$  s is used for making the results of oxygen distribution to present the regulation of oxygen transport more clearly and more definitely. Parameters used for this coupled mathematical model are shown in Table 1.

#### 5 Results

#### 5.1 Numerical results for solid deformation

5.1.1 Volumetric deformation under capillary fluctuation

In the present model, we combine solid deformation into seepage and obtain the results of the seepage velocity from the coupled deformation and seepage model, then use the seepage velocity as the velocity for convection-diffusion to calculate the oxygen concentration.



Fig. 2 Flowchart of FEM program for time-dependent oxygen transport model where  $\Delta t=0.0625$  s and  $t_0=0$  s

Parameter	Description	Value	Unit
$k_1^{[25,39]}$	Permeability coefficient in tissue	$8 \times 10^{-6} - 8 \times 10^{-8}$	${ m cm\cdot s^{-1}}$
$k_2^{[25,39]}$	Permeability coefficient at capillary wall	$2 \times 10^{-6} - 2 \times 10^{-8}$	$ m cm\cdot s^{-1}$
$k_3^{[25,39]}$	Permeability coefficient in capillary	0.005	$ m cm\cdot s^{-1}$
$p_{\text{inletI}}^{[33]}$	Pore pressure under fluctuation (Type I)	0.026	$ m N\cdot cm^{-2}$
$p_{\rm inlet II}^{[33]}$	Pore pressure under fluctuation (Type II)	0.065	$ m N\cdot cm^{-2}$
$p_{\mathrm{inletIII}}^{[33]}$	Pore pressure under fluctuation (Type III)	0.13	$ m N\cdot cm^{-2}$
$p_{t_0}^{[33]}$	Initial pore pressure	0.26	$N \cdot cm^{-2}$
$D_1^{0}[37]$	Diffusion coefficient in tissue	$2 \times 10^{-5} - 2 \times 10^{-7}$	$\mathrm{cm}^2\cdot\mathrm{s}^{-1}$
$D_2^{[37]}$	Diffusion coefficient at capillary wall	$10^{-5} - 10^{-7}$	$\mathrm{cm}^2\cdot\mathrm{s}^{-1}$
$D_{3}^{[37]}$	Diffusion coefficient in capillary	0.0003	$\mathrm{cm}^2\cdot\mathrm{s}^{-1}$
$n_0^{[34]}$	Initial porosity	0.35	Dimensionless
$K_{O_2}$	Oxygen solubility of blood at 37 °C, 1 atm	0.023	$\mathrm{mL} \cdot \mathrm{mL}^{-1} \cdot (\mathrm{atm})^{-1}$
$c_{\text{used O}_2}^{[37]}$	Oxygen consumption rate in tissues	$5.38 \times 10^{-5}$	$\mathrm{mL} \cdot \mathrm{mL}^{-1} \cdot \mathrm{s}^{-1}$
$P_{O_2}(t_0)^{[35]}$	Initial oxygen partial pressure	13332.2	$\mathbf{Pa}$
$E_1^{[34]}$	Young modulus in tissue	10.0	$N \cdot cm^{-2}$
$E_2^{[34]}$	Young modulus at capillary wall	20.0	$N \cdot cm^{-2}$
$E_{3}^{[34]}$	Young modulus in capillary	0.05	$ m N\cdot cm^{-2}$
$v^{[34]}$	Poisson ratio	0.45	Dimensionless
$\Delta t$	Time step	0.0625	s
$\beta^{[34]}$	Compressibility coefficient of tissue fluid	$10^{-7}$	Dimensionless
$\alpha^{[34]}$	Effective stress coefficient	1	Dimensionless

 Table 1
 Parameters used in mathematical model

As described in Sections 3 and 4, the present model considers capillary fluctuations as a power source, so the wave pattern of fluctuations must be represented accurately and completely. Some numerical tests are carried out to determine an appropriate time step. The results indicate that the wave pattern of capillary fluctuations can be simulated well at 1/16 s, but there is only a small difference (relative error of 0.5%) when using 1/32 s. Thus, we select a time step of 1/16 s for the entire computational process, and the pressure at the inlet end of capillary over time which can represent the wave pattern of capillary fluctuation is shown in Figs. 3(a) and

3(b), where two sets of time are marked, i.e.,  $t_1$ ,  $t_2$  and  $t_3$ ,  $t_4$  represent the pressure under the impact of capillary fluctuation from trough to peak. Correspondingly, the relative volumetric deformation distributions from  $t_1$  to  $t_2$  and  $t_3$  to  $t_4$  are presented by percentage in Figs. 3(c) and 3(d). This clearly indicates that capillary fluctuation has a greater effect on volumetric deformation in the middle of capillary region than around the inlet end and around the outlet end, and the largest value of relative volumetric deformation from trough to peak reaches about 0.7% when  $k_1 = 8 \times 10^{-6} \text{ cm} \cdot \text{s}^{-1}$ , and reaches about 0.8% when  $k_1 = 8 \times 10^{-7} \text{ cm} \cdot \text{s}^{-1}$ . The greatest deformation appears in the tissue where surrounds the middle of capillary and is furthest from capillary.



Fig. 3 Effect of capillary fluctuation on volumetric deformation: pressure in inlet end of capillary over time, when (a)  $k_1 = 8 \times 10^{-6}$ , (b)  $k_1 = 8 \times 10^{-7}$ ; percentage of volumetric deformation under impact of capillary fluctuation in some xy-slices, (c) at  $z=225 \,\mu\text{m}$  (left),  $z=325 \,\mu\text{m}$  (middle),  $z=425 \,\mu\text{m}$  (right) from  $t_1$  to  $t_2$  shown in (a) when  $k_1 = 8 \times 10^{-6}$ , (d) at  $z=225 \,\mu\text{m}$  (left),  $z=325 \,\mu\text{m}$  (left),  $z=325 \,\mu\text{m}$  (middle),  $z=425 \,\mu\text{m}$  (right) from  $t_3$  to  $t_4$  shown in (b) when  $k_1 = 8 \times 10^{-7}$  (unit of  $k_1$  is cm  $\cdot \text{s}^{-1}$ )

#### 5.2 Numerical results for seepage

#### 5.2.1 Pore pressure under capillary fluctuation

The seepage could be affected by solid deformation which is caused by capillary fluctuation, and the distributions of pore pressure under the impact of volumetric deformation of microcirculatory structure are shown in Fig. 4, which exemplifies the change of pore pressure from trough to peak in half a second corresponding to the volumetric deformation presented in Figs. 3(a) and 3(c). These results indicate that with the increasing pressure of capillary resulting from



capillary fluctuation, capillary and tissues would be deformed and as a result the pore pressure is increased.

Fig. 4 Example of distribution of pore pressure from trough to peak in half second at  $z=350 \,\mu\text{m}$ when  $k_1 = 8 \times 10^{-6} \,\text{cm} \cdot \text{s}^{-1}$ : (a)–(i) time points corresponding to period from  $t_1$  to  $t_2$  in Fig. 3(a) with time step of 1/16 s; (j) curve of pore pressure within capillary and average pore pressure at  $z=350 \,\mu\text{m}$  between  $t_1$  and  $t_2$ 

5.2.2 Pressure distribution corresponding to three extreme values of capillary fluctuation

According to the experimental data on three forms of the capillary fluctuation within a given capillary (details in Sections 3 and 4), they correspond to three extreme values for the pressure variations in the arteriole end, i.e.,  $p_{inlet}=0.39 \text{ N/cm}^2$  basically,  $p_{inlet}=0.546 \text{ N/cm}^2$  with the fluctuations of Types I and II,  $p_{inlet}=0.611 \text{ N/cm}^2$  with the fluctuation of Types I, II, and III. When the values of  $p_{inlet}$  are the three extreme values, Fig. 5 shows their pore pressure

distributions in xy-slices along the direction of blood flow. Comparing these results, the same pore pressure behavior can be observed.



(e) *z*=550 μm



Fig. 5 Comparison of distribution of pore pressure in xy-slices corresponding to three extreme values of capillary fluctuation, i.e., values of pore pressure in inlet end are respectively 0.39 (left column), 0.546 (middle column), 0.611 (right column) with unit of N/cm<sup>2</sup>. These xy-slices locate at (a)  $z=0\,\mu$ m, (b)  $z=50\,\mu$ m, (c)  $z=250\,\mu$ m, (d)  $z=500\,\mu$ m, (e)  $z=550\,\mu$ m, (f)  $z=630\,\mu$ m, and (g) average pore pressure along z-direction with  $k_1 = 8 \times 10^{-6} \text{cm} \cdot \text{s}^{-1}$ 

(i) The pressure gradient decreases along the direction of blood flow.

(ii) Within the tissue surrounding the middle capillary, the pore pressure decreases in the direction from the capillary to the tissue.

(iii) The pressure varies slightly in the region surrounding the middle capillary.

5.2.3 Seepage velocity distribution

The seepage velocity distribution at t=133.0625 s,  $p_{inlet} = 0.39 \text{ N/cm}^2$  is shown in Figs. 6 and 7. Figure 6 shows the seepage velocity distribution in each xy-slice, which also indicates that counter-current flow occurs near the arteriole end and venule end of capillary. It is in agreement with the findings from the pore pressure distribution. The seepage velocity distribution in each yz-slice is shown in Fig. 7. The velocity of tissue fluid in the middle of capillary, changes little in the direction of blood flow. Within the tissues which are further away from the capillary, the lower velocity is.

5.2.4 Counter-current flow phenomenon

The results of pore pressure show the flow of blood and fluid in tissue and indicate that fluid seepage from the capillary vessel into the peripheral tissues on the arteriole end (see Fig. 5(a)), and thus soon partly return into the capillary vessel from the tissue near the arteriole end (see Figs. 5(b) and 6(b)). In the middle of the capillary, fluid seepage from the capillary vessel to the body tissue (see Figs. 5(c) and 5(d)), and thus near the venule end of the capillary, small amount of fluid partly return into the capillary vessel (see Figs. 5(e) and 6(e)). On the venule end of capillary, finally fluid is drawn from the tissue into the capillary vessel (see Fig. 5(f)). Namely, the counter-current flow (from tissue to capillary) located occurs near the arteriole end and venule end of capillary.



Fig. 6 Seepage velocity distribution of fluid with unit of  $\text{cm} \cdot \text{s}^{-1}$  at t = 133.0625 s,  $p_{\text{inlet}} = 0.39 \text{ N/cm}^2$ , and  $k_1 = 8 \times 10^{-6} \text{ cm} \cdot \text{s}^{-1}$ . Sub-figures are all located in *xy*-slice and respectively at (a)  $z=25 \,\mu\text{m}$ , (b)  $z=75 \,\mu\text{m}$ , (c)  $z=225 \,\mu\text{m}$ , (d)  $z=425 \,\mu\text{m}$ , (e)  $z=525 \,\mu\text{m}$ , and (f)  $z=615 \,\mu\text{m}$ . Color scale shows magnitude of  $V_i$  on *xy*-plane, and arrows indicate seepage direction

This particular phenomenon reflects an unique feature of the fluid field in the microcirculation, because this counter-current flow allows oxygen to be transported to each cell uniformly. That is, when the arterial blood reaches single capillaries, the oxygen concentration in the blood is much higher than that in the peripheral tissues. This causes a tremendous concentration difference between the capillaries and the tissue. As a result, oxygen diffuses rapidly from the capillary blood into its surrounding tissue, where excess oxygen would partly be stocked. Thus, to supply adequate oxygen to cells that are further away from the arteriole end, the oxygen near the arteriole end must partly return to the capillary vessel from the tissue to be carried to other regions through the blood. This is a more efficient method of supplementing and consuming oxygen for all body cells. The sudden change in pore pressure gradient allows the oxygen to partly return into the capillary by convection-diffusion. Similarly, because the oxygen in the blood continues to be carried to the tissues, oxygen within the capillary becomes depleted near the venule end, meaning that the oxygen concentration within the tissue near the venule end becomes relatively higher. To reach cells that are farther from the arteriole end, the oxygen has to partly return to the capillary near the venule end. A certain percentage of oxygen in the blood must be carried into the venule  $(P_{O_2}=5332.9 \text{ Pa} \text{ at the venule end})$ . At the venule end of the capillary, deoxygenated blood is carried from the tissues back to the heart. If some non-homogenous materials could be produced surrounding the arteriole end physiologically that leads the permeability in arteriole end to be less, the counter-current flow might not appear. But if only basing on the heterogeneity of capillaries and tissue, this counter-current flow would appear. The results also may provide some explanations for why more fluid is often found in the tumor tissue. For example, high permeability coefficient together with a high tissue boundary pressure may lead to the counter-current flow, which in turn causes more fluid to be stocked within the tissue, and thus oxygen transport is affected.

The effect of different permeability coefficients on the counter-current flow is examined in Fig. 8. This indicates that counter-current flow becomes more obvious with the increasing permeability coefficient, which agrees with the study<sup>[39]</sup>. He and Himeno<sup>[39]</sup> showed that the



Fig. 7 Distribution of seepage velocity along direction of blood flow with unit of  $cm \cdot s^{-1}$  at t=133.0625 s,  $p_{\text{inlet}} = 0.39 \text{ N/cm}^2$ , and  $k_1 = 8 \times 10^{-6} \text{ cm} \cdot \text{s}^{-1}$ . Sub-figures are all located in yz-slice and respectively at (a)  $x=0.75\,\mu\text{m}$ , within capillary, (b)  $x=3.15\,\mu\text{m}$ , at capillary wall, (c)–(g) within tissue: (c)  $x=5.25 \,\mu\text{m}$ , (d)  $x=7.50 \,\mu\text{m}$ , (e)  $x=10.50 \,\mu\text{m}$ , (f)  $x=13.50 \,\mu\text{m}$ , and (g)  $x=16.50\,\mu\text{m}$ . Color scale shows magnitude of  $V_i$  on yz-plane and arrows only show velocity direction

interstitial fluid will be reabsorbed into the capillary and that counter-current flow occurs near the outlet end if the seepage is sufficiently strong.

#### Numerical results for oxygen concentration 5.3

5.3.1Oxygen concentration given by coupled convection and diffusion model

Oxygen concentration given by the present coupled model are shown by the distribution of concentration in some xy-slices in the left column of Fig. 9, which can clearly indicate how the oxygen concentration varies from capillary to surrounding tissues, and also shown by the distribution of concentration in some yz-slices in the left column of Fig. 10, which can clearly indicate how the oxygen concentration varies in the direction of blood flow. It can be observed that oxygen concentration gradient in tissues changes little, especially in the middle of capillary vessel, also be found that oxygen concentration reduces rapidly in the front of capillary vessel, but reduces very slowly from around  $z=200\,\mu\text{m}$ . This also agrees with the physiology that when arterial blood reaches capillary bed, oxygen in plasma is immediately transported to tissues, then is evenly supplied to all the individual cells, which accomplished in the middle of capillary vessel.





Fig. 8 Effect of permeability coefficient on counter-current flow: comparisons of distribution of pore pressure in xy-slices between  $k_1=8\times10^{-6}$  cm·s<sup>-1</sup> (left column) and  $k_1=8\times10^{-8}$  cm·s<sup>-1</sup> (right column) (unit of pore pressure is N/cm<sup>2</sup>)



Fig. 9 Comparison of oxygen concentration distribution in xy-slices given by coupled solid deformation, fluid seepage, convection-diffusion, and molecular diffusion model, i.e., this present model (left column), by coupled fluid seepage, convection-diffusion, and molecular diffusion model with no coupling solid deformation (middle column), and by pure molecular diffusion model with no coupling convection (right column). Three models use same parameters: diffusion coefficient  $D_1=2\times10^{-6}$  cm<sup>2</sup>·s<sup>-1</sup> and permeability coefficient  $k_1=8\times10^{-6}$  cm·s<sup>-1</sup> used in coupled model, and xy-slices are located at (a)  $z=0\,\mu$ m, (b)  $z=100\,\mu$ m, (c)  $z=300\,\mu$ m, and (d)  $z=500\,\mu$ m (unit of oxygen concentration is mL·mL<sup>-1</sup>)

#### 6 Discussion

#### 6.1 Effect of convection-diffusion on oxygen transport

To study how convection-diffusion impacts on oxygen transport, comparing with the oxygen concentration given by the coupled convection-diffusion and molecular diffusion model, the third

column of Fig. 9 and the second column of Fig. 10 give the distribution of oxygen concentration given by the pure molecular diffusion model in xy-slices and in yz-slices, respectively. The same parameters are used for their comparison in Figs. 9 and 10. For further discussing the effect of convection-diffusion on oxygen transport, we denote the oxygen concentration obtained from the coupled model of convection-diffusion and molecular diffusion as  $C_{\text{coupled}}$  and that obtained from the pure molecular diffusion model as  $C_{\text{diff}}$ . The relative difference in oxygen concentration



Fig. 10 Comparison of oxygen concentration distribution along direction of blood flow given by coupled solid deformation, fluid seepage, convection-diffusion, and molecular diffusion model, i.e., this present model (left column), by the coupled fluid seepage, convection-diffusion, and molecular diffusion model, i.e., no coupling solid deformation (middle column), and by pure molecular diffusion model, i.e., no coupling convection (right column). Three models use same parameters: diffusion coefficient  $D_1 = 2 \times 10^{-6} \text{ cm}^2 \cdot \text{s}^{-1}$  and permeability coefficient  $k_1 = 8 \times 10^{-6} \text{ cm} \cdot \text{s}^{-1}$  used in coupled model, and yz-slices are located at (a)  $x=0\,\mu\text{m}$ , (b)  $x=4.5\,\mu\text{m}$ , (c)  $x=12\,\mu\text{m}$ , and (d)  $x=18\,\mu\text{m}$  (unit of oxygen concentration is mL·mL<sup>-1</sup>)

between the two models can be calculated by (18). This gives the relative effect of convectiondiffusion to molecular diffusion.

$$r = \frac{(C_{\text{coupled}} - C_{\text{diff}})}{C_{\text{diff}}}.$$
(18)

The curves of this relative difference along the direction of capillary in Figs. 11(a), 11(b), and 11(c), where the average of r for fixed values of x and z, i.e., the average of r over y, is measured on the vertical axis, and the horizontal axis ranges from 1 to 14, corresponding to the xy-slice number. They show that convection-diffusion has an impact in the capillary vessel and also in the tissue, and has a greater effect in the middle of the capillary than near the inlet end and the outlet end of capillary. This is good in agreement with the findings from Yao and Gu<sup>[31]</sup>. From Figs. 10 and 11, we can see that the further the tissue is away from the capillary, the more obvious the effect becomes. It can be concluded that both molecular diffusion and convection-diffusion are needed to ensure oxygen to be transported to all the cells more equally and more



(c) ( $C_{\rm coupled}{-}C_{\rm diff}){/}C_{\rm diff}$  with  $D_1{=}2\times10^{-7}$ 

Fig. 11 Comparison of relative effect of convection-diffusion for different values of permeability coefficient and diffusion coefficient. Vertical axis shows relative difference of oxygen concentration of each line at y-direction in xy-slices, calculated by (18), which corresponds to slice number i along horizontal axis. There are 10 points between each value of i and i+1 corresponding to 10 lines in ith xy-slice located at x=0, 1.5, 3, 3.3, 4.5, 6, 9, 12, 15, and 18 µm. Slices 1 to 14 correspond to z=0, 50, 100, 150, 200, 250, 300, 350, 400, 450, 500, 550, 600, and 630 µm. Relative difference of convection-diffusion to molecular diffusion on oxygen transport is in cases of (a)  $D_1 = 2 \times 10^{-5}$ , (b)  $D_1 = 2 \times 10^{-6}$ , and (c)  $D_1 = 2 \times 10^{-7}$  with unit of cm<sup>2</sup> · s<sup>-1</sup>. Pink (-+-) denotes  $k_1 = 8 \times 10^{-8}$  and blue (- $\times$ -) denotes  $k_1 = 8 \times 10^{-6}$  with unit of cm · s<sup>-1</sup>

efficiently, because convection-diffusion through the tissue allows more oxygen to be transported quickly to the cells away from oxygen source. In addition, how the effect of convection-diffusion on oxygen transport is affected by the different permeability coefficient and diffusion coefficient is also studied, and is found that larger values of the permeability coefficient produce a more obvious convection-diffusion effect, as do smaller values of the diffusion coefficient. Many previous models for oxygen transport neglected the convection-diffusion of oxygen: some of them completely neglected the convection-diffusion of oxygen within capillary and within tissue<sup>[39–43]</sup>, or only incorporated the convection-diffusion of oxygen within capillary, and assumed the velocity of tissue fluid to be zero in tissue<sup>[28]</sup>, this assumption was commonly used. However, as presented in Fig. 11, included in this present model, in addition to the standard axial convection-diffusion inside the capillary vessel and molecular diffusion in the tissue, convections are across the capillary wall and in the surrounding tissue. The numerical results conclude that at this level there is maximum of 16% and average of 3% increases in capillary-tissue oxygen transport due to convective transport across capillary wall and in the surrounding tissue.

### 6.2 Effect of solid deformation on oxygen transport

Though a few theoretical models considered the deformable porous media in the numerical simulation for microcirculation<sup>[31-32]</sup>, they failed to model the deformation of circulatory structure according to the physiological power source of the capillary fluctuation. For example, in Ref. [31], the solute flux and convective flux in a porous medium were investigated using a mechano-electrochemical mixture theory and the dynamic unconfined compression test configuration for solute desorption experiments was carried out to simulate the solid deformation in a porous medium. Thus, basing on the experimental data of the pressure variations for capillary fluctuation, we couple the solid deformation with the fluid seepage which has not been found in other models. How solid deformation affect oxygen transport can be examined by comparing the oxygen concentration given by the coupled fluid solid seepage and deformation model  $(C_{\text{coupled}})$ and by the pure seepage model (denoted as  $C_{nodefor}$ ).  $C_{nodefor}$  in xy-slices shown in the second column of Fig. 9 indicate that solid deformation has an impact on oxygen transport but not too much, and the effect is greater in the front of capillary than that in the latter of capillary. Moreover, the relative difference between the both models, i.e.,  $(C_{\text{coupled}} - C_{\text{nodefor}})/C_{\text{nodefor}}$ , in the direction of blood flow is shown in Fig. 12. From this, we can see that the relative effect of solid deformation to oxygen concentration in the direction of capillary is about 0.5% maximum



Fig. 12 Comparison of relative difference in oxygen distribution given by this present coupled model and by model with no solid deformation, when  $k_1=8\times10^{-6}$  cm·s<sup>-1</sup> and  $D_1=2\times10^{-6}$  cm<sup>2</sup>·s<sup>-1</sup>. Vertical axis shows relative difference of oxygen concentration of each line at y-direction in xy-slices, calculated by  $(C_{\text{coupled}} - C_{\text{nodefor}})/C_{\text{nodefor}}$ , which corresponds to slice number *i* along horizontal axis. There are 10 points between each value of *i* and *i*+1 corresponding to 10 lines in *i*th xy-slice located at x=0, 1.5, 3, 3.3, 4.5, 6, 9, 12, 15, and 18 µm. Slices 1 to 14 correspond to z=0, 50, 100, 150, 200, 250, 300, 350, 400, 450, 500, 550, 600, and 630 µm

and 0.3% average. From comparing the first column and the second column in Fig. 10, it can be observed the significant impact of solid deformation in oxygen transport is that the solid deformation can help the fluid to seepage more uniformly, further can help the oxygen to be transported more uniformly.

#### 7 Conclusions

The present study numerically simulates an entire process of oxygen transport at the level of microcirculation by developing a 3D coupled solid deformation-fluid seepage-convection and diffusion porous media model, which newly takes account of volumetric deformation of both capillary and tissue resulting from capillary fluctuation, and couples the deformations into seepage, then, the seepage coupled the deformation affects on convection-diffusion of oxygen. We quantitatively examine how solid deformation, fluid seepage and convection-diffusion affect the transport of oxygen, and have some important findings as follows:

(i) Solid deformation is more significant in the middle of a capillary, where the maximum value of volumetric deformation reaches about 0.5%.

(ii) Though solid deformation has a small impact on seepage, it can exert a positive influence on the tissue fluid so that it flows more uniformly, and it can also cause the oxygen to be transported more uniformly, which eventually impacts on the distribution oxygen concentration by 0.1%-0.5%.

(iii) The change in pore pressure distribution within the tissue near the arteriole end and near the venule end of a capillary is several times larger than that within the tissue surrounding the middle of the capillary.

(iv) Convection-diffusion given by coupled deformation and seepage has a maximum (16%) and average (3%) increase in oxygen concentration, compared to pure diffusion. Its more significant role is to allow oxygen to be transported more evenly, especially away from the capillary.

(v) Convection-diffusion has a greater effect in the middle of a capillary than that near the ends of a capillary. Also, larger values of the permeability coefficient, or smaller values of the diffusion coefficient, produce a more obvious effect on oxygen transport.

Thus, this numerical results from this more comprehensive theoretical model indicate that the convection-diffusion of oxygen transport should be necessary to be considered in the relevant studies, its important role of allowing oxygen to be transported more uniformly should be paid more attention and studied further.

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