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Efficient biotransformation of ginsenoside $Rb₁$ to Rd by isolated Aspergillus versicolor, excreting β -glucosidase in the spore production phase of solid culture

Fujian Lin . Xiaoyan Guo . Wenyu Lu

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Abstract Ginsenosides are the major pharmacological components in ginseng. Microorganisms from a ginseng field were isolated to identify transformation of ginsenosides. Based on HPLC and LC–MS analysis, strain LFJ1403 showed strong activities to transform ginsenoside Rb_1 to Rd as the sole product. Phylogenetic analysis of 18S rDNA indicated that LFJ1403 belonged to Aspergillus versicolor. Through comparing four systems of transforming Rb_1 to Rd, strain LFJ1403 was found to secrete ginsenosideconverting enzymes in the spore production phase of plate culture. This result suggested that the enzyme could be directly obtained from the plate. The spore suspension, which contained the exocrine enzyme, was easy to prepare and efficient for biotransformation

F. Lin \cdot X. Guo \cdot W. Lu (\boxtimes) Department of Biological Engineering, School of Chemical Engineering and Technology, Tianjin University, Tianjin 300072, People's Republic of China e-mail: wenyulu@tju.edu.cn

F. Lin e-mail: linfujian1999@sina.com

W. Lu

Key Laboratory of System Bioengineering (Tianjin University), Ministry of Education, Tianjin 300072, People's Republic of China

W. Lu

SynBio Research Platform, Collaborative Innovation Center of Chemical Science and Engineering (Tianjin), Tianjin 300072, People's Republic of China

of ginsenoside Rb_1 to Rd. Further study showed that the maximum bioconversion rate was 96 $\%$ (w/w) in shake flasks when a spore suspension system was used with optimized biotransformation conditions. Scaleup of this system to 2L resulted in an 85 % conversion rate. The ginsenoside Rb_1 converting enzyme was separated by gradient HPLC with Q-Sepharose column, and its β -glucosidase activity and Rb₁converting ability was assayed by the 4-Nitrophenylb-D-glucopyranoside (PNPG) method and HPLC with C18 column, respectively. We obtained 130 U ml⁻¹ enzymatic activity with the purified β -glucosidase. This is the first report on efficiently converting ginsenoside using extracellular enzyme directly from the fungus spore production phase of solid culture.

Keywords Strain screening - Biotransformation - Extracellular enzyme \cdot Ginsenoside Rb₁ \cdot Ginsenoside Rd - Aspergillus versicolor

Introduction

Ginsenoside is the major pharmaceutical component in ginseng (Kim et al. 2007), and accounts for 4 % in ginseng dry root (Oh et al. [2014\)](#page-10-0). According to different glucoside skeletons, ginsenosides are mainly divided into the dammarane type and oleanane type (Quan et al. [2012](#page-10-0)). The dammarane type can be further classified into protopanoxadiol (PPD) and protopanaxatriol (PPT) by their aglycones (Li et al. [2015\)](#page-10-0). Among these PPD-

type ginsenosides, ginsenoside Rd especially exerts many pharmacological activities, such as a promotive effect on proliferation of neural stem cells (Lin et al. [2012](#page-10-0)), protecting kidney from chemical drugs (Yokozawa and Dong [2001\)](#page-10-0), neutral system protective effects (Li et al. [2011\)](#page-10-0) and preventing contraction of blood vessels (Zeng et al. [2003\)](#page-10-0). However, it is difficult to separate Rd from ginseng because of its low concentration and complex ginseng components (Shi et al. [2007](#page-10-0)). The amount of the major ginsenoside Rb_1 is up to 23.8 % in ginsenosides (Wu et al. [2012a](#page-10-0)), and it has the same aglycon as ginsenoside Rd; the point of difference is that Rb_1 has one more sugar residue at the C-20 position, so ginsenoside Rd can be obtained by removing this residue of ginsenoside Rb_1 (Fig. 1).

There are two ways to produce ginsenoside Rd including chemical and biological hydrolysis (Gao et al. [2014;](#page-9-0) Wu et al. [2012b](#page-10-0)). Microbial and enzymatic methods are more environmentally compatible and specific than chemical hydrolysis (Hegazy et al. [2015\)](#page-9-0). In the microbial method of fungus biotransformation, ginsenoside Rd has been converted from Rb_1 by Acremonium stritum (Chen et al. [2008\)](#page-9-0), and Cladosporium fulvumand (Zhao et al. [2009b](#page-10-0)) with a conversion rate of 72 % and 86 % respectively. Rd also has been extracted from the ginseng extraction residue by lingzhi (Ganoderma lucidum) (Hsu et al. 2013), in which eight kinds of ginsenosides were detected and the fermentation time was as long as 30 days. Although the microbial approach is feasible, there exist the drawbacks of long conversion time and low biotransformation rate. In the enzymatic manner, ginsenoside Rd has been converted by β -glucosidase from *Thermus caldophillus* GK24 (Son et al. [2008](#page-10-0)), Cladosporium fulvum (Zhao et al. [2009a\)](#page-10-0), Penicillium oxalicum sp. 68 (Gao et al. [2012](#page-9-0)) and Dictyglomus turgidum (Lee et al. [2012\)](#page-10-0). In these reports, the transformation time is much shorter than that of the microbial approaches; however, ginsenoside Rd is sometimes intermediate, and this leads to a relatively low conversion rate. What's more, the separation and purification processes of β -glucosidase are complicated.

In this study, ginsenoside Rb_1 -converting fungus was isolated and identified from the soil of a ginseng field, and we investigated the biotransformation of ginsenoside Rb_1 to Rd using extracellular enzyme directly from the fungus spore production phase of plate culture. High-performance liquid chromatography (HPLC) analysis showed that Rd was the sole product of this transformation process. The conversion rate increased as high as 96 % at 48 h in shake flasks. Scale-up in a 2L reaction system resulted in an 85 % conversion rate, which indicated that this spore suspension biotransformation system has the potential to be used for Rd production at an industrial scale.

Materials and methods

Materials

Reagent-grade ginsenoside $Rb₁$ and Rd were purchased from Solarbio Co. Ltd (Beijing, China). Total ginsenosides (80 % ginsenoside Rb₁, other 20 % compounds are Rb₂, Rc, Re, Rf and polysaccharose) were purchased from Hongjiu Biotech Co. Ltd (Jilin, China). 4-Nitrophenyl-b-D-glucopyranoside (PNPG) and 4-nitrophenol (PNP) were purchased from Dingguo Biotech Co. Ltd (Tianjin, China). Super filter tube was purchased from Millipore Co. Ltd (Massachusetts, USA). All chemicals and solvents were of analytical or HPLC grade.

Ginsenoside Rb

Ginsenoside Rd

Fig. 1 The conversion pathway of ginsenoside Rb_1 to ginsenoside Rd

Microorganisms screening and product Rd identification

LFJ1403 was isolated from a ginseng field by a standard dilution plating onto 0.1 g 1^{-1} chloramphenicol PDA plate. Single colonies were purified by transferring onto new plates, and the isolated colony was washed down by 20 mM acetate buffer (PH 5.0) to a sterile shake flask with shaking at 130 rpm and 30 °C for 2 h. After incubation, the spores were filtered with three layers of gauze and were diluted to 5×10^6 spores ml⁻¹. The above spore buffer and 0.5 mg ml^{-1} total ginsenosides (dissolved in acetate buffer and sterilized through $0.22 \mu m$ filter) were reacted with shaking at 130 rpm and 30 °C. The ginsenoside Rb_1 conversion ability of isolated strains was tested by HPLC.

The spore buffer of isolate LFJ1403 was mixed with 0.5 mM reagent-grade Rb_1 (dissolved in acetate buffer and sterilized through $0.22 \mu m$ filter) and cultivated with shaking at 200 rpm and 30 $^{\circ}$ C. HPLC and LC–MS methods were used to identify the substrate Rb_1 and its metabolite.

Strain identification

Isolated strain LFJ1403 was cultured on PDA medium at 30 \degree C to observe its phenotypic characteristic with a modified Frias-De Leon's method (Frias-De Leon et al. [2011\)](#page-9-0), and the micromorphological characteristics were analyzed using the microculture method of Ridell (Frias-De Leon et al. [2011\)](#page-9-0). The 18S rDNA gene (1650 bp) was amplified by PCR using genomic DNA isolated from LFJ1403 as a template. Both primers (FR1: 5'-ANC CAT TCA ATC GGT ANT-3' and NS1: 5'-GTA GTC ATA TGC TTG TCT C-3') were selected from the fungus universal primers database. Identification and homology search were performed with the BLAST program at the National Center for Biotechnology Information (NCBI) website [\(http://blast.ncbi.nlm.nih.gov\)](http://blast.ncbi.nlm.nih.gov). The phylogenetic tree was constructed using the neighbor-joining method through the MEGA 5.10 program.

Determination of biotransformation system

For obtaining the optimal biotransformation system, spores of Aspergillus sp. LFJ1403 cultured on PDA plate for 2 days were scraped down with 0.1 % Tween80 acetate buffer (pH 5.0) and made into spore buffer

(diluted to 5 \times 10⁶ spores ml⁻¹). Subsequently, the four biotransformation systems were made as follows: above spore buffer was used as the spore suspension system; the supernatant after spore buffer centrifugation at $25,000 \times g$ for 30 min at 4 °C was used as the supernatant system; the bottom spores after spore buffer centrifugation were again suspended with acetate buffer and used as the centrifugal spore system; the bottom spores were suspended by potato dextrose broth (PDB) and cultured for several days up to spore germination, and the mycelium suspension was used as the mycelium suspension system. Then 0.25 mM $(0.277 \text{ mg ml}^{-1})$ reagent-grade ginsenoside Rb_1 was added into these four biotransformation systems and reacted with shaking at 200 rpm and 37 \degree C for 96 h. The conversion abilities of the four systems were detected by comparing the Rb_1 conversion rate and enzyme activity.

After the optimal biotransformation system was obtained, to determine the best time of collecting extracellular enzyme, spores on PDA plates were scraped down at 2, 3, 4, 5 and 6 day with 0.1 $%$ Tween80 acetate buffer (pH 5.0) and made into spore suspension systems. These spore suspensions were mixed with 0.277 mg ml⁻¹ reagent-grade ginsenoside Rb_1 and cultivated with shaking at 200 rpm and 37 °C for 96 h. The optimum time to form a spore suspension system was identified by HPLC analysis.

Scale-up reaction system

In order to gain the maximum spore yield of plate culture, the spores were transferred from slants and dissolved in sterile water to prepare spore concentration gradients of 10^4 , 10^5 , 10^6 , 10^7 , and 10^8 ml⁻¹, and $200 \mu l$ of each was inoculated to the PDA plate (D90 mm). After 3 days of incubation at 30 \degree C, spores were scraped down with 10 ml 0.1 % Tween80 acetate buffer (pH 5.0). We diluted the solution to an appropriate concentration so that we could count the spore number through a microscope to determine the spore yield.

The optimal spore concentration resulting from the above procedure was prepared. We inoculated this spore suspension onto larger PDA plates (D150 mm), and put them at 30 \degree C for 3-day cultivation. The next manipulations were the same as previously described, but the amount of 0.1 % Tween80 acetate buffer was increased proportionally. Then 1L of spore suspension $(5 \times 10^6$ spores ml⁻¹) was mixed with the same

Fig. 2 The HPLC/mass spectrum profiles of ginsenosides in reaction mixtures and the microphotograph of Aspergillus sp. LFJ1403 mycelium growing on the cover slip. a The HPLC profiles of ginsenoside Rb_1 and its metabolite Rd. **b** The mass spectrograms of ginsenoside Rb_1 and its metabolite Rd. c The

volume of 1.25 mg l^{-1} reagent-grade ginsenoside Rb1 and this biotransformation system was put in a 5L fermenter (BIOTECH-5JG, Baoxing biological equipment engineering Co. Ltd, Shanghai, China), to proceed under the conditions of 37° C and 200 rpm.

Analytical methods

The reaction mixture was extracted twice by watersaturated n-butanol and then the n-butanol fraction

microphotograph of LFJ1403 aerial mycelium. The microculture was performed at 30 \degree C until the fungus was observed to grow. Subsequently, the cover slip was separated from the agar to be observed under the microscope. The magnification was $\times100$

was evaporated to dryness and methanol was added (Huang et al. [2006](#page-10-0)). Ginsenosides were assayed by HPLC at 203 nm with a C18 column. The column was eluted at room temperature with acetonitrile (A)/water $(B) = 40$: 60 (v/v) at 1.0 ml min⁻¹.

Quantification analysis of ginsenosides was performed by LC–MS system micrOTOF-QII10204. Positive ion mode in electrospray ionization (ESI) was used to analyze ginsenoside $Rb₁$ and its metabolite. The following parameters of positive ion mode

Fig. 3 Phylogenetic tree based on the 18S rDNA gene sequence showing the relationships between the Aspergillus sp. LFJ1403 strain and related species

were used: scan begin/scan end 200/1500 m/z, set capillary 4500 V, set end plate offset -500 V, set collision cell RF 150 Vpp, set nebulizer 0.8 bar, set dry heater 180 °C, set dry gas 6.0 1 min^{-1} .

The β -glucosidase activity was measured by a colorimetric method using PNPG as the substrate. The reaction mixtures were centrifuged at $10,625 \times g$ for 5 min at 4° C, a crude enzyme was precipitated by adding 60 % saturated $(NH_4)_2SO_4$ into the supernatant and placed at 4° C overnight, and the crude enzyme was centrifuged and dialyzed sufficiently in 20 mM acetate buffer (Chang et al. [2014\)](#page-9-0). The hydrolytic reactions containing 400 μ 1 nM PNPG and 100 μ 1 enzyme solution, which were reacted in 20 mM acetate buffer (pH = 5.0), were incubated at 37 $^{\circ}$ C for 30 min, and the reaction was terminated by the addition of 0.5 ml distilled water and 2.5 ml 0.5 M NaOH (Zhao et al. [2009a\)](#page-10-0). The absorption of released PNP was measured at 405 nm. One unit $(U \text{ ml}^{-1})$ of enzyme activity was defined as the amount of enzyme required to release 1 μmol PNP per h under standard conditions (Zhang et al. [2001\)](#page-10-0).

Ginsenoside Rb_1 -converting enzyme was separated by HPLC at 280 nm with a Q-Sepharose column. The volume of column was 2 ml with 1 ml loading sample.

The column was gradient eluted at room temperature with 25 mmol 1^{-1} pH 8.2 Tris–HCL (A)/25 mmol 1^{-1} pH 8.2 Tris–HCl with $0.5 \text{ mol } l^{-1}$ NaCl (B) at 1.0 ml min-¹ . The volume of B eluent was controlled in the range of 0 and 80 %. The different enzyme fractions were collected to measure the β -glucosidase activities and ginsenoside Rb_1 -converting abilities by the PNPG method and HPLC with C18 column, respectively. The molecular weight of ginsenoside Rb_1 -converting enzyme was determined by SDS-PAGE.

Results and discussion

Isolation and identification of Rd-producing fungus

Through repeated transfer to the PDA plate, strain LFJ1403 was purified from the ginseng soil, and the product of its biotransformation activity was identified as the single metabolite ginsenoside Rd by HPLC and LC–MS (Fig. $2a$ $2a$, b).

The front colour of the colonies was greyish-green and the back was yellow; the texture of the colonies was

Fig. 4 Effects of different biotransformation systems and extracellular enzyme-collecting time on the production of Rd. a Effects of different biotransformation systems. Circle spore suspension, *regular triangle* supernatant, *square* centrifugal spore, *inverted triangle* mycelium suspension. **b** Effects of different enzyme-collecting times. Data represent the means of three experiments, and error bars represent the standard deviation

villiform and dense after 4 days culture. The mycelium shape growing on the cover slip was radial, dense close to the plate bottom and sparse close to the top (Fig. [2](#page-3-0)c). The phylogenetic tree based on its 18S rDNA sequence (GenBank Accession No. KM925044) was constructed to identify the fungus to the species level (Fig. [3\)](#page-4-0). The phylogenetic tree demonstrated that strain LFJ1403 should be affiliated with the genus Aspergillus. The closest recognized relatives of strain LFJ1403 were identified as Aspergillus versicolor. Strain LFJ1403 had less than 1 % difference in 18S rDNA gene sequence from the corresponding type strain. Morphologic observation and phylogenetic tree analysis both indicated that strain LFJ1403 belonged to A. versicolor.

This fungus was stored in the China General Microbiological Culture Collection Center (CGMCC 11038).

Selection of high-efficiency biotransformation system

The four biotransformation systems were mixed with 0.25 mM $(0.277 \text{ mg ml}^{-1})$ reagent-grade ginsenoside Rb_1 , and the conversion rates (w/w) of spore suspension and supernatant were 90 % at 12 h, then remained stable at 94 % at terminal 96 h. In contrast, the conversion rates (w/w) of centrifugal spore and mycelium suspension were 27 and 18 % at 12 h, and then increased slowly to 94 and 62.72 %, respectively (Fig. 4a); this result indicated that LFJ1403 could excrete abundant ginsenoside Rb_1 -converting enzymes, which were attached to the surface of spores. During the PDA plate culture stage, these enzymes were dissolved into spore buffer and formed a crude enzyme solution. The spore suspension and supernatant systems both contained these enzymes, but the other two systems didn't. Although the conversion rate was similar, the preparation method of the spore suspension was easier than that of the supernatant, so spore suspension was selected as the final biotransformation system. The conversion rate (w/w) of ginsenoside Rb_1 to Rd collecting enzymes at 2 and 3 days was higher than that at 4, 5 and 6 days (Fig. 4b); this result indicated that the activity of extracellular enzyme attached to spores was high in the early spore production stage and slowly decreased with time extension, so spores cultured during 2 and 3 days were washed down to form spore buffer and further made into a spore suspension system.

Optimization of biotransformation conditions

Starting with total ginsenosides, ginsenoside Rd yield was higher than that using equal quality of reagentgrade ginsenoside Rb_1 (data not shown). This result is from conversion of other PPD-type ginsenosides besides Rb_1 in total ginsenosides to Rd, but ginsenoside Rd was mainly from the conversion of ginsenoside Rb_1 , as confirmed by HPLC (data not shown). In this study, total ginsenosides (80 % ginsenoside Rb_1) were used. Up to 1.25 mg ml^{-1} total ginsenosides, the conversion rate of total ginsenosides to Rd was increased. However, above 1.25 mg ml^{-1} , the conversion rate decreased, but Rd production increased slowly with

Fig. 5 Effects of biotransformation conditions on the production of Rd. a Effects of different total ginsenosides concentrations. Ginsenoside Rd production (filled square) and conversion rate (open square). Total ginsenosides (concentration was 0.6, 1.25, 1.85, 2.5 and 3.75 mg ml^{-1} respectively) were mixed with equal volume of spore suspension (1.0 \times 10⁶ spores ml⁻¹). The mixtures were incubated with shaking at 200 rpm and 37 $^{\circ}$ C for 96 h. b Effects of different cultivate temperatures. 20 mM acetate buffer containing 1.25 mg ml^{-1} total ginsenosides was mixed with equal volume of spore suspension (1.0 \times 10⁶ spores ml^{-1}). The mixtures were incubated with shaking at 200 rpm for

increasing the concentration of total ginsenosides (Fig. 5a). To achieve a suitable conversion rate and production concentration, 1.25 mg ml^{-1} total ginsenosides (80 % ginsenoside Rb_1) was selected as the substrate concentration. The temperature affected both the reaction rate and the product yield (Eklund et al. [1990](#page-9-0)), ginsenoside Rb_1 can be converted into Rd in various degrees at different temperatures, and the Rd yield was the highest at 37 $\rm{^{\circ}C}$ (Fig. 5b). The effect of pH on the biotransformation of $Rb₁$ was also significant. The pH value had no obvious change over time; there was no fungal growth or spore germination in the

96 h at 25, 30, 37 and 40 °C, respectively. c Effects of different pH. 20 mM acetate buffer containing 1.25 mg ml^{-1} total ginsenosides was mixed with an equal volume of spore suspension $(1.0 \times 10^6 \text{ spores } \text{ml}^{-1})$. The mixtures were incubated at different pHs with shaking at 200 rpm and 37 °C for 96 h. d Effects of different cultivation times. 20 mM acetate buffer containing 1.25 mg ml^{-1} total ginsenosides was mixed with equal volume of spore suspension (1.0 \times 10⁶ spores ml⁻¹). The mixtures were incubated at pH 5.0 with shaking at 200 rpm and 37 °C for 96 h . Data represent the means of three experiments, and error bars represent the standard deviation

acetate buffer, so the initial pH value was measured as the pH value of reaction system. The Rd yield was low when the pH was over 7.0 or below 3.0, and was the highest at pH 5.0 (Fig. 5c). Under these optimum conditions, the ginsenoside Rd concentration reached up to 1.2 mg ml^{-1} with a conversion rate of 96 % (w/ w) at 48 h (Fig. 5d).

Scale-up biotransformation

The PDA plate (D150 mm) with grown spores is shown in Fig. [6a](#page-7-0). As for the optimal spore

b

 2.0 Spore yield (10'spores ml'1) 1.6 1.2 0.8 0.4 0.0 10^4 10^5 10^6 10^7 10^{48} Inoculation concentration (ml⁻¹) d_{100} 75 Conversion rate(%) 50 25 0 60 $\mathsf 0$ 12 24 36 48 72 84 96 108 $Time(h)$

Fig. 6 Scale-up of Rb1 to Rd biotransformation. a PDA plate (D150 mm) with grown spores. b Effect of different spore concentrations on the spore yield in plate culture. c Picture of the 5L fermenter with a working volume of 2L. d Effect of reaction

concentration for inoculation to the plate, the $10⁴$ spores ml^{-1} showed the maximum spore yield (Fig. 6b), so we chose this concentration for plate culture. It was also obvious that high inoculation concentration didn't lead to high spore yield. This may be caused by too many spores competing for growing space and nutrients, which in turn prevented the production of spores.

time on the conversion rate in Scale-up of Rb_1 to Rd transformation system. Data represent the means of three experiments, and error bars represent the standard deviation

We expanded the spore suspension biotransformation system in a 5L fermenter with a working volume of 2L (Fig. 6c) under the optimal biotransformation conditions and kept the reaction for 3 days. The HPLC analysis results indicated that the conversion rate reached 80 % (w/w) after 24 h' transformation, and it trended to be stable during the next 72 h, with an 85 % (w/w) conversion rate (Fig. 6d). This result showed us

Fig. 7 Assay of enzyme activities in different biotransformation systems within 96 h. Circle spore suspension, inverted triangle supernatant, square centrifugal spore, regular triangle mycelium suspension

the potential possibility of applying the spore suspension biotransformation system to industrial transformation of Rb_1 to Rd. The process of amplifying the plate culture gradually to get enough spore suspension for use is crucial and this aspect will be studied further.

Enzyme characterization

The specific activity of ginsenoside Rb_1 -converting enzyme in different biotransformation systems within 96 h were measured by a colorimetric method using PNPG as the substrate. Enzyme activities of spore suspension and supernatant were higher in the range of 80–120 U m $^{-1}$ than centrifugal spore and mycelium suspension, which were about 40 and 50 U ml^{-1} (Fig. 7). This result further demonstrated that β glucosidase was secreted in the spore production

Fig. 8 Assay of enzyme characterization. a The HPLC profiles of single enzymes separated from crude enzymes with Q-Sepharose column. **b** Assay of β -glucosidase activity from different collected tubes by PNPG method. c Assay of

ginsenoside Rb_1 -converting ability from different collected tubes by HPLC analysis. d SDS-PAGE analysis of β -glucosidase fraction in the fourth tube. SDS-PAGE was performed on an 8.0 % gel and stained with Coomassie brilliant blue

phase of plate culture, and these crude enzymes were collected to form an enzyme solution by washing spores. The enzyme activity of centrifugal spores was low because only spores were reserved by removing the enzyme supernatant, and the activity of mycelium suspension was also low because mycelium produced less β -glucosidase in the growth stage than in the spore production stage. The phenomenon that enzyme activities of supernatant and spore suspension, which both contain the secreted enzyme in the spore production phase of plate culture, were higher than mycelium was caused by different extracellular glucosidase secreting phases. A. versicolor LFJ 1403 secreted more extracellular glucosidase in spore production phase of solid culture than that in mycelium growth phase of liquid culture.

The crude enzyme solution was concentrated through the process of centrifugation, ammonium sulfate precipitation and ultrafiltration. The individual enzymes in crude enzyme solution were separated by HPLC with a Q-Sepharose column (Fig. [8a](#page-8-0)), and were collected to analyze β -glucosidase activity and ginsenoside Rb_1 -converting ability used PNPG method and HPLC detection, respectively. β -glucosidase activities assay indicated that the fourth tube had strong β -glucosidase activity, but others didn't (Fig. [8](#page-8-0)b). The enzymatic activity of this purified glucosidase is 130 U ml^{-1}, which is higher than some other glucosidases from fungi, such as 114 U ml^{-1} by thermophilic fungal strain Melanocarpus sp. MTCC 3922, 52.2 U ml^{-1} by thermotolerant fungal strain Aspergillus terreus MTCC 6335 (Sonia et al. [2008](#page-10-0)), and 102.6 U ml⁻¹ by strain *Penicillium pulvillorum* TUB F-2220, 87 U ml⁻¹ by strain *Penicillium cf*. simplicissimum TUB F-2378 (Marjamaa et al. [2013](#page-10-0)), respectively (all the cited data were converted to a unified unit for comparative purposes). HPLC analysis also indicated that the fourth tube had the ability of converting ginsenoside Rb_1 to Rd (Fig. [8](#page-8-0)c). These enzyme activity tests showed that Rb_1 -converting ability was consistent with the β -glucosidase activity. SDS-PAGE showed that the molecular weight of ginsenoside Rb_1 -converting enzyme was 97 kDa (Fig. [8](#page-8-0)d).

In summary, a fungus, A. versicolor was isolated and found to be able to convert ginsenoside $Rb₁$ to Rd without further hydrolysis. Through comparing different Rb_1 biotransformation systems, A. versicolor in the spore production phase of plate culture was found to excrete ginsenoside Rb_1 -converting enzyme. The spore suspension system, which containing these exocrine enzyme, was easy to prepare and efficient. The conversion conditions were further optimized and the maximum biotransformation rate (w/w) was up to 96 %. Scale-up in a 2L reaction system resulted in an 85 % conversion rate. Afterwards, the Rb_1 -converting enzyme was separated by gradient HPLC with Q-Sepharose column, and then the β -glucosidase activity and Rb_1 -converting ability were assayed, respectively. Consequently, A. versicolor, and its characteristic of excreting highly active enzyme on the solid culture plate, may be suitable for production of ginsenoside Rd.

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