REVIEW



Production of hydrogel microparticles in microfluidic devices: a review

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Abstract

Hydrogels are biocompatible materials commonly used in biological applications, such as cell encapsulation, tissue engineering and drug delivery systems. The use of hydrogels in the form of microparticles brings, for several purposes, many advantages, since the particles have a high surface-to-volume ratio and they can be delivered inside microscale structures such as blood microvessels and tissues. Microfluidic devices are a promising approach to produce hydrogel microparticles because they enable a high precision control of the flow streams during the microfabrication process, leading to microparticles with precise size, shape, mechanical properties and cross-linking density. In this review, the focus is put on the most important features to be considered when producing hydrogel microparticles through microfluidic devices. First, the design strategies of microfluidic devices, the selection of the operating conditions and the importance of surfactants are analyzed. Then, the most important gelation mechanisms are reviewed. Afterwards, the most commonly used hydrogel materials are introduced, and their properties are referred. Finally, the different methods to control the size, shape and particle microstructure are discussed and the main challenges for the future are addressed.

 $\label{eq:constraint} \begin{array}{l} \mbox{Keywords} \ \mbox{Hydrogels} \cdot \mbox{Droplet microfluidics} \cdot \mbox{Surfactants} \cdot \mbox{Thermal gelation} \cdot \mbox{Ionic gelation} \cdot \mbox{Photopolymerization} \cdot \mbox{Photopilymerization} \cdot \mbox{Photopilymerization} \cdot \mbox{Surfactants} \cdot \mbox{Thermal gelation} \cdot \mbox{Ionic gelation} \cdot \mbox{Photopolymerization} \cdot \mbox{Photopilymerization} \cdot \mbox{Surfactants} \cdot \mb$

Abbreviations PEG	Poly(ethylene glycol)	PVA HA	Poly(vinyl alcohol) Hyaluronic acid
PEGDA ELPs PEO-PPO-PEO PNIPAAM PEGMEA	Poly(ethylene glycol) diacrylate Elastin-like peptides Poly(ethylene oxide)–poly(propylene oxide)–poly(ethylene oxide) Poly(N-isopropyl acrylamide) Poly(ethylene glycol) methyl ether	List of symbols Ca _i μ _i ν _i σ	Capillary number of the phase <i>i</i> Viscosity of the phase <i>i</i> Velocity of the phase <i>i</i> Surface tension between the two phases
CFL PDMS SFL SFIL SLMs DEP EWOD CMC EDS	acrylateCFLContinuous flow lithographyPDMSPoly(dimethyl siloxane)SFLStop flow lithographySFILStop flow interference lithographySLMsSpatial light modulatorsDEPDielectrophoresisEWODElectrowetting on dielectricCMCCritical micelle concentrationEDSEquilibrium droplet size	Re_{i} ρ_{i} ν_{i} D φ Q_{d} Qc λ μ_{c} μ_{c} We_{i} Ca_{c}	Reynolds number of the phase <i>i</i> Density of the phase <i>i</i> Velocity of the phase <i>i</i> Diameter of the microchannel Flow rate ratio Flow rate of the dispersed phase Flow rate of the continuous phase Viscosity ratio Viscosity of the dispersed phase Viscosity of the continuous phase Weber number of the phase <i>i</i> Capillary number of the continuous

Ca_d

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¹ CEFT, Transport Phenomena Research Center, Chemical Engineering Department, Faculty of Engineering, University of Porto, 4200-465 Porto, Portugal Capillary number of the dispersed

phase

1 Introduction

Microparticles are used for cell encapsulation, medical imaging, drug delivery, biomolecule synthesis and diagnosis (Teh et al. 2008; Mazutis et al. 2015; Anna and Mayer 2006; Cubaud and Mason 2008), among other biomedical applications. To perform these roles, microparticles must be biocompatible, easy to produce and able to incorporate drugs or microorganisms (Tumarkin and Kumacheva 2009). These requirements can be easily met by hydrogels, due to the versatility of this family of materials (Tumarkin and Kumacheva (2009); Khademhosseini and Langer 2007; Zhang et al. 2016). Morphologically, hydrogels are cross-linked polymer networks that can contract or expand by releasing or absorbing water (Tumarkin and Kumacheva 2009). They change size in response to pH, temperature and ionic strength variations and their properties can be modified by introducing copolymers or other molecules in their network (Tumarkin and Kumacheva 2009). Hydrogels can be obtained through natural or synthetic resources, presenting in each case different characteristics (Tumarkin and Kumacheva 2009; Gao et al. 2012a).

Hydrogel microparticles can be produced by several methods, of which the most widespread are emulsification (Zamora-Mora et al. 2014a; Chuah et al. 2009), direct agitation and grinding of the polymer (Oliveira and Mano 2011), spray drying (Ré 2006) and microfluidics (Teh et al. 2008). Compared with the alternative methods, microfluidics has several unique advantages, as the size and shape of the microparticles can be accurately controlled enabling the manufacturing of monodispersed populations (Leng et al. 2010) with a large variety of shapes and compositions. Microfluidic devices are also suitable to control reaction, heat and mass transport rates, reducing waste and enabling the control of the characteristics of the microparticles. Furthermore, composite particles can be manufactured with precision and reproducibility combining different streams and using double-emulsion techniques or photolithography. The particle fabrication can be integrated with other components such as sensors, heaters, coolers, visualization windows and elements to conduct biological experiments. Finally, scaling up is possible through parallelization, which facilitates large-scale production.

The most straightforward method to produce hydrogel microparticles in microfluidic devices is droplet microfluidics. Microdroplets are produced using multiphase systems comprising a continuous phase (usually an oil), a dispersed phase (in this specific case, a hydrogel precursor) and a surfactant. To generate the droplets, the driving forces are the shear stress and the interfacial tension between phases. The surfactant is used to lower the interfacial tension between the phases and to prevent coalescence of the droplets (Baret 2012; Baroud and Willaime 2004; Baret et al. 2009; Sharma et al. 2013; Xu et al. 2012). After formation, the microdroplets are solidified into hydrogel microparticles (gelation), inside or outside the channel, and through many different mechanisms depending on the hydrogel. The final size and shape of the microparticles depend on multiple parameters including the flow rates of the fluids, geometry, material composition and size of the channels and the fluid properties (Teh et al. 2008; Leng et al. 2010; Lee et al. 2009).

This review summarizes the different aspects of hydrogel microparticles production in microfluidic devices aiming to provide guidelines to select the operating conditions, the microfluidic device design and the selection of precursor fluids and carrier phases. Among the wide set of hydrogels available, the most commonly produced in microfluidic devices are agarose, alginate and poly(ethylene glycol)-PEG. These hydrogels will be analyzed in more detail. The design of microfluidic devices is analyzed in Sect. 2 and the role of surfactants in hydrogel particle formation is described in Sect. 3. Hydrogels have different gelation mechanisms, which have implications on the design of the microfluidic devices to produce microparticles. The gelation mechanisms are discussed in Sect. 4: thermal gelation (Tumarkin and Kumacheva 2009; Jagur-Grodzinski 2009), ionic gelation (Patil et al. 2010, 2012; Patel et al. 2017; Sacco et al. 2016) and photopolymerization (Nguyen and West 2002). The properties of some hydrogel precursors and hydrogel particles are summarized in Sect. 5. The size, accuracy and shape restrictions of each fabrication method are discussed in Sect. 6. The challenges for the future are addressed in Sect. 7, with emphasis on the development of high-throughput particle production.

2 Microfluidic systems

Microfluidic technologies offer efficient methods to produce highly monodispersed microparticles of new materials, which are applicable in different fields such as biology, medicine and chemistry (Teh et al. 2008; Mazutis et al. 2015; Anna and Mayer 2006; Christopher and Anna 2007). There are many options to produce and manipulate droplets, namely through: dielectrophoresis (DEP) -driven droplet generation (Yang et al. 2010), electrowetting on dielectric (EWOD) -driven droplet generation (Yang et al. 2010), electrohydrodynamic manipulation (Yang et al. 2010), thermocapillary manipulation (Yang et al. 2010; Baroud et al. 2007; Darhuber et al. 2003; Chen et al. 2010; Gao et al. 2012b), magnetic actuation (Yang et al. 2010; Yizhong et al. 2007; Todd and Jon 2013; Tsuchiya et al. 2008; Say-Hwa et al. 2010; Zhang and Nguyen 2017), acoustic actuation (Yang et al. 2010; Wixforth et al. 2004; Oberti et al. 2009; Destgeer and Sung 2015) and hydrodynamic manipulation (Teh et al. 2008; Yang et al. 2010; Yizhong et al. 2007; Pethig 2010; Jones et al. 2001; Wehking et al. 2013; Nelson and Kim 2012; Sung Kwon et al. 2003; Gong and Kim 2008). Although all these techniques are very important in the production and manipulation of droplets, hydrodynamic methods are the most commonly used, so they get more attention in the following sections.

2.1 Droplet production

Hydrodynamic droplet production techniques take advantage of shear and interfacial forces to generate droplets (Leng et al. 2010). The production rate, size and shape of the droplets are mostly dependent on the flow rates, physical properties of the phases and geometry/design/material of the channels (Teh et al. 2008; Leng et al. 2010; Lee et al. 2009).

The channels used in hydrodynamic manipulation are usually made in PDMS—poly(dimethylsiloxane)—due to the low-cost fabrication process and easy control of the surface chemistry (Duffy et al. 1998; McDonald and Whitesides 2002). Although with these advantages over other materials, PDMS swells or degrades when exposed to some solvents (Lee et al. 2003). Other materials that can be used to replace PDMS are glass, silicon and thiolene (Teh et al. 2008; Christopher and Anna 2007; Lee et al. 2003). Methods to fabricate PDMS microfluidic devices have been described in detail by Duffy et al. (1998), McDonald and Whitesides (2002), Mata et al. (2005) and McDonald et al. (2000), while detailed information on solvent selection is available in Lee et al. (2003) work. The most common microfabrication technique for the production of PDMS channels is based on planar photolithography, for the production of SU-8 molds (Campo and Greiner 2007; Lorenz et al. 1997; Natarajan et al. 2008), and soft lithography for the production of the channels from the molds (Friend and Yeo 2010). Using these techniques, the characteristic size of the channels can be smaller than 2 μ m (Campo and Greiner 2007). Alternatively, the community working on droplet microfluidics also uses capillary tubing devices (Jeong and Kim 2011; Utada et al. 2005; Martinez et al. 2012).

To produce microdroplets by hydrodynamic manipulation, the most common designs are T-junction, co-flow and flow-focusing geometries (Christopher and Anna 2007). In a T-junction configuration (Fig. 1a), the continuous phase, which flows in the main channel, is intersected by the dispersed phase, which flows in a secondary channel. In a flowfocusing configuration (Fig. 1b), the flow of the dispersed phase in the main channel is squeezed by the flow of the continuous phase entering by two lateral channels (Samanipour et al. 2016; Xu et al. 2009). A configuration similar to the flow-focusing configuration is the co-flow configuration (Fig. 1c), in which the dispersed and continuous phases flow in the same direction in parallel microchannels (Christopher and Anna 2007; Yang et al. 2010); in the inner flows the dispersed phase and in the outer the continuous phase.



Fig. 1 Designs commonly used in droplet microfluidics: a T-junction scheme; b flow-focusing scheme; c Co-flow scheme; d droplet formation using capillaries

As aforementioned, microcapillary tubing is another approach to fabricate microchannels for droplet microfluidics (Jeong and Kim 2011; Utada et al. 2005; Martinez et al. 2012). A typical configuration is shown in Fig. 1d. Two tapered capillaries are inserted, pointing each other, inside a squared capillary. One of the tapered capillaries is the inlet of the dispersed phase and the other is the outlet that collects the droplets. The continuous phase flows in the space between the inlet microcapillary and the squared capillary.

The size of the droplets formed depends on the fluids viscosity and density, surface tension, flow rates and surface properties and geometry of the device (Teh et al. 2008; Choi et al. 2007). Dimensional analysis leads to a correlation between the non-dimensional size of the droplets and Capillary (Ca_i) and Reynolds (Re_i) numbers of each phase, viscosity ratio (λ) and contact angle. Alternatively, one of the Capillary numbers can be replaced by the flow rate ratio (φ). Typical flows in microfluidic systems are characterized by very low Reynolds numbers; viscous forces are dominant and no significant flow variations are observed when the Reynolds number changes (Teh et al. 2008; Lee et al. 2009; Yang et al. 2010). Only in high-speed flows, the inertial forces become significative and the Reynolds number effects should then be taken into account (Baroud et al. 2010).

In droplet formation, the flow patterns are influenced by the aforementioned dimensionless numbers. To visualize this dependence, the data from experiments are usually represented in regime maps. A typical regime map displays the regimes in two-dimensional diagrams like the one represented in Fig. 2. In this diagram, the coordinates are the



Fig. 2 Scheme of a flow map regimes for a flow-focusing device based on Cubaud and Mason (2008). Each flow map regime is valid for a viscosity ratio

Capillary numbers. The regime map is valid for a given viscosity ratio.

In a flow-focusing device, the most commonly observed flow patterns are: jetting, dripping, threading, tubing and viscous displacement (Cubaud and Mason 2008; Carneiro et al. 2016). In the jetting regime, Fig. 3a, the thread of the dispersed phase breaks far from the focusing section. In the dripping regime, Fig. 3b, the thread of the dispersed phase breaks and retracts, leading to the formation of a droplet near the focusing section. When the thread is stable and does not break, a threading pattern is observed—Fig. 3c. Tubing (Fig. 3d) is similar to threading, but, in this case, the dispersed phase fills almost all the cross-section of the main channel. When the flow rates ratio is too high, the dispersed phase starts to invade the inlet channels of the continuous phase, leading to viscous displacement regime-Fig. 3e. Two additional flow patterns have been referred in the literature for $Ca_d < 10^{-3}$ and $Ca_c > 0.3$: tip streaming (Anna and Mayer 2006; Jeong et al. 2012) and tip-multi-breaking (Zhu et al. 2015).

To produce hydrogel particles with specified characteristics, some tools are required to predict the flow regime, the polydispersity and particle size. Microdroplets are generated only in the dripping and jetting regimes and the regime map shows the ranges of Capillary numbers where those regimes lie (Carneiro et al. 2016). Polydispersity is directly related to the flow regime. Carneiro et al. (2016) characterized PDMS droplet formation in a microfluidic flow-focusing device and concluded that the best flow conditions to obtain monodispersed microdroplets are the dripping regime. The particle size trends can be analyzed through the equations of Cubaud and Mason (2008). These authors developed and tested predictive equations for the size of the droplets in the dripping and jetting regimes for systems without surfactants.

The analysis of particle size trends is not a simple matter, since size trends are geometry dependent and interplay with regime changes, as shown by the results of several papers in the literature. For example, Dang et al. (2012) produced monodisperse PEG microparticles in a flow-focusing device and observed a decrease in the size of the droplets with the increase of the continuous phase flow rate, behavior consistent with the trend predicted by Cubaud and Mason (2008). Dang et al. (2012) also observed that high concentrations of PEG induce large microdroplets. Since multiple factors are involved, the explanation of this effect is not straightforward. Concentrated PEG solutions have high viscosity and high surface tension, being the viscosity increase dominant. For this reason, high concentrations lead to high Capillary numbers of the dispersed phase. Carneiro et al. (2016) PDMS data show that the effect of the Capillary number of the dispersed phase on the droplet size is non-monotonic and depends on the flow regime. As Dang et al. (2012) did not characterize the flow regime, their findings cannot be





checked in more detail. Furthermore, they used non-standard geometry and geometrical effects alone may explain the observed increase of the particle size with concentration. This emphasizes the importance of the regime map for the specific experimental conditions used.

Hydrodynamic droplet formation is a passive method that relies on the use of syringe pumps to control the flow rates and on geometrical constrictions of the microdevice. It is not always possible to produce droplets of the desired size because the ranges of flows and control precision required are not achievable using syringe pumps. Active methods based on acoustic actuation (Brenker et al. 2016; Schmid and Franke 2014) have been used to circumvent some of the limitations of the hydrodynamic methods, such as size and size distribution limitations. Acoustic actuation based on surface acoustic waves has smaller capacitive effects, and thus are suitable to precisely control droplet formation and to obtain very small droplets.

2.2 Droplet manipulation

Microfluidic techniques enable the production of highly monodispersed droplets and each one of these droplets can serve as a base for chemical reactions or cell encapsulation (Teh et al. 2008). Procedures such as droplet fission, droplet fusion and droplet sorting may be required during the fabrication and encapsulation processes. Sequential droplet fission can help to scale-up droplet formation (Teh et al. 2008) and can be attained by passive or active methods. The passive methods consist of using the shear forces that are created by specific designs of the microchannels to split the droplets, such as T-junctions, channels with branches or with obstructions (Teh et al. 2008; Sharma et al. 2013; Yang et al. 2010; Cerdeira et al. 2020). Active methods use external power or electrical forces to split the droplets (e.g., EWOD) (Teh et al. 2008). Through droplet fusion (Teh et al. 2008; Sharma et al. 2013), it is also possible to merge the droplets, creating droplets with larger diameters. This procedure is useful in particle production to enable reaction control. The passive methods consist on the use of a specific microchannel design to control the fusion in a certain location, such as a channel junction, an obstruction or an expanded region in the microchannel (Teh et al. 2008; Yang et al. 2010). Drop fusion can also be promoted by active methods, like EWOD or other techniques that require electrical forces (Teh et al. 2008; Sharma et al. 2013).

Sorting of droplets can also be interesting for the study of isolated droplets, purification of droplets and control of polydispersed droplet mixtures (Teh et al. 2008). The sorting of the droplets can be promoted using a channel geometry based on the size of the droplets or using the gravitational force (Teh et al. 2008; Yang et al. 2010). Electrical forces can also be employed to sort the droplets. EWOD and DEP are two of the techniques used to sort the droplets (Teh et al. 2008; Sharma et al. 2013).

3 Surfactants

Despite the several advantages of the microfluidic systems to produce hydrogel microparticles, droplet coalescence can arise before gelation, becoming a problem for particle production. To stabilize the droplet emulsion, prevent coalescence and stabilize the droplet interface, surfactants must be added to one of the phases. Surfactants are amphiphilic molecules that modify the properties of interfaces. Amphiphilic molecules have two different functional groups, usually hydrophilic and oleophilic groups (Baret 2012; Baroud and Willaime 2004). For this reason, the surfactant is driven to the interface, reducing the interfacial tension (Baret 2012; Xu et al. 2012; Mazutis and Griffiths 2012). The interfacial tension reaches its lowest value at the critical micelle concentration (CMC) (Tostado et al. 2011), which is a characteristic of the surfactant. Above the critical concentration, the additional surfactant molecules form micelles (Farn 2008) and the interfacial tension is constant (Tostado et al. 2011; Myers 2005). The surfactant can also modify the rheology of the interface (Fischer and Erni 2007) (its viscosity and elasticity), which has an impact on the particle size. This effect is usually difficult to analyze since data are scarce and interface rheology requires specialized equipment unavailable in most laboratories.

Furthermore, the distribution of surfactant in the flow is significantly influenced by mass transport limitations, which hinder droplet formation and stability. Coalescence can persist if the adsorption time of the surfactant into the interface is longer than the formation time of a new droplet (Baret 2012; Baret et al. 2009; Xu et al. 2012). However, mass

transport limitations can also contribute to droplet stability. When the distribution of the surfactant at the surface of the droplet is not uniform and a concentration gradient is created, a stress opposed to the flow direction can be generated rigidifying the interface; this is called the Marangoni effect—Fig. 4. Marangoni forces can impact the flow around the interface of the droplet (Baret 2012; Xu et al. 2012) and hinder coalescence. The Marangoni effect can also influence droplet size, as shown in the work of Xu et al. (2012).

Another effect that can be observed in microfluidic droplet generation is the Ostwald ripening effect, which is characterized by the growth of large droplets (McClements et al. 2012; Wooster et al. 2008), due to the coalescence of small ones (McClements et al. 2012; Wooster et al. 2008). This effect is induced by the higher Laplace pressure in the smaller droplets leading to their dissolution in the bigger ones, (Baret 2012). The Ostwald ripening effect can be avoided by adding hydrophobic molecules to the continuous phase (McClements et al. 2012).

Figure 5, based on information from Baret (2012), shows combinations of hydrocarbon oils/surfactants that can be used for several applications. In the formation of hydrogel droplets in microfluidics, the most used surfactant is Span 80. Span 80 is a non-ionic surfactant that can be used together with different hydrocarbon oils, such as hexadecane, mineral oil, rapeseed oil and kerosene (Baret 2012). It is largely used in the pharmaceutical industry due to its properties and effects in emulsions at low concentrations (Pensado et al. 2014). Span 80 is used in microfluidics with two purposes: decrease the interfacial tension between phases and to form a protective coat around the droplets to avoid coalescence (Benmekhbi et al. 2014). Park et al. (2016) used Span 80 to prevent the coalescence of gelatin droplets (Fig. 6a) and Zamora-Mora et al. (2014a) used Span 80 to obtain the same effect in cooperative hydrogels of chitosan/ agarose—Fig. 6b and c.

A few experimental reports have analyzed the effect of the surfactant on droplet formation. (Choi et al. 2007)

Fig. 4 Marangoni effect: **a** in the presence of surfactant, the flow induces a concentration distribution of surfactant around the droplet causing a stress opposed to the flow direction (Marangoni stress—red arrows); **b** Marangoni stresses act against the film avoiding coalescence







Fig. 5 Guide for the selection of the continuous phase and surfactants for different applications [based on information from Baret (2012)]. Please take note that some substances can affect the PDMS performance (Lee et al. 2003)

produced monodispersed droplets of alginate using Span 80 as a surfactant—Fig. 7a. They concluded that the size of the droplets decreases with increasing concentration of Span 80. Choi et al. (2009) produced monodispersed microspheres of PEGDA using a flow-focusing device—Fig. 8 a and b. They found that the surfactant concentration must be above 3%, otherwise the interfacial tension is too high and the microdroplets formed have an irregular shape. They also concluded that when the concentration of the surfactant increases, the size of the droplets decreases. These results are consistent with the observation by Cubaud and Mason (2008) that the droplet size decreases with the increase of the Capillary number of the continuous phase. They are also consistent with the results obtained by Xu et al. (2012).

Capillary numbers are inversely proportional to the interfacial tension between phases and so, according to Fig. 2, the surfactant plays an important role in droplet formation. When the surfactant concentration increases, the interfacial tension decreases leading to higher Capillary numbers. The increase of the Capillary number of the continuous phase leads to smaller droplets, while the effect of increasing the Capillary number of the dispersed phase is dependent on the flow regime. If the regime changes from dripping to jetting, sub-channel size particles can be obtained. The surfactant can also change the Capillary number through an alteration of the viscosity.

4 Gelation mechanisms

The most common gelation methods are thermal gelation, ionic gelation and photopolymerization. Each of these methods has specific requirements with implications on the design and operation of the devices. The gelation mechanism usually requires heating or cooling systems, channels



Fig. 6 Microparticles and microdroplets obtained by thermal gelation: a optical microscopy of gelatine hydrogel microspheres suspended in water-Adapted by permission from Springer Nature, Macromolecular Research, Synthesis and characterization of thermosensitive gelatin hydrogel microspheres in a microfluidic system, (Park et al. 2016). Copyright 2020. Scale $bar = 100 \mu m$. b Optical microscopy image of chitosan/agarose in PBS buffer at 25 °C; and c optical microscopy images of the chitosan/agarose droplets. Scale bar = 70 µm. Reprinted from Carbohydrate Polymers, Vol 111, (Zamora-Mora et al. 2014b), chitosan/agarose hydrogels: cooperative properties and microfluidic preparation, Copyright 2020, with permission from Elsevier. doi.org/10.1016/j.carbpol.2014.04.087. d Warm droplets of agarose and e lyophilized microparticles of agarose-Reprinted from Acta Biomaterialia, Vol 12, Agarose particletemplated porous bacterial cellulose and its application in cartilage growth in vitro, (Yin et al. 2015). Copyt 2020, with permission from Elsevier. doi.org/10.1016/j.actbio.2014.10.019

to deliver specific reactants, waveguides or optical windows for UV light sources.

4.1 Thermal gelation

Thermal gelation is a physical cross-linking method (Tumarkin and Kumacheva 2009; Jagur-Grodzinski 2009; Pochan et al. 2003; Cellesi et al. 2004; Hoare and Kohane 2008) induced by hydrophobic interactions, hydrogen bonding or ionic interactions caused by temperature changes in the polymeric solution (Tumarkin and Kumacheva 2009; Jagur-Grodzinski 2009). The gelation temperature depends on the concentration and chemical structure of the polymer (Hoare and Kohane 2008; Huang et al. 2013). Since gelation is reverted when the temperature is set back (Jagur-Grodzinski 2009; Jo et al. 2006), hydrogels that undergo thermal gelation (Huang et al. 2013) are usually called thermoreversible hydrogels. Examples of microparticles produced by thermal gelation can be found in Fig. 6.

Thermal gelation can be triggered upon cooling (Pochan et al. 2003; Joo et al. 2007; Klouda and Mikos 2008; Park et al. 2011) or heating (Pochan et al. 2003; Joo et al. 2007; Klouda and Mikos 2008; Park et al. 2011) of the hydrogel precursor. Materials that change from liquid to gel form upon cooling include agarose, kappa-carrageenan, poly(vinyl alcohol)—PVA and gelatin (Jo et al. 2006; Klouda and Mikos 2008; Nishinari and Watase 1987; Petka et al. 1998; Liu et al. 2010). Materials that undergo gelation by heating include elastin-like peptides (ELPs), Pluronics, block and star copolymers of PEG and poly(N-isopropyl acrylamide) and cellulose derivatives (Gao et al. 2012a; Hoare and Kohane 2008; Klouda and Mikos 2008; Petka



Fig. 7 Alginate microparticles. **a** Encapsulation of GFP-yeast cell into alginate microbeads—Adapted by permission from Springer Nature, Biomedical microdevices, Generation of monodisperse alginate microbeads and in situ encapsulation of cell in microfluidic device (Choi et al. 2007). Copy 2020. Scale bar=50 μ m. **b** Algi-

nate microparticles with biconcave shape produced in a microfluidic chip—Reprinted from John Wiley and Sons, Macromolecular Bioscience, Microfluidic Production of Alginate Hydrogel Particles for Antibody Encapsulation and Release (Mazutis et al. 2015), © 2015 WILEY–VCH Verlag GmbH & Co. KGaA, Weinheim



Fig. 8 Microparticles obtained by photopolymerization. **a** Optical microscopy image of the monodispersed PEG microspheres suspended in hexadecane; and **b** SEM image of PEG microspheres. Scale bar=100 μ m. Adapted by permission from Springer Nature, Macromolecular Research, In situ microfluidic synthesis of monodisperse PEG microspheres, (Choi et al. 2009). Copyt 2020. **c** Microparticles of PEGDA containing fluorescently labeled TMV nanotemplates—Adapted with permission from (Lewis et al. 2010). Copyright 2020 American Chemical Society. Scale bar=100 μ m. **d** Optical

et al. 1998; Lin and Cheng 2001; Weng et al. 2004; Ahmadi and Bruijn 2008).

Thermoreversible hydrogels do not require chemical reactions, cross-linkers or UV irradiation. Thus, thermoreversible hydrogels are usually biocompatible, biodegradable and have low toxicity (Tumarkin and Kumacheva 2009; Jagur-Grodzinski 2009). Due to these characteristics, thermal gelation can be used to produce biocompatible microparticles for biomedical purposes. For example, Yin et al. (2015) incorporated monodispersed agarose microparticles,

image of encapsulated *E. coli* in PEG microbeads—Adapted by permission from Springer Nature, Macromolecular Research, Synthesis and utilization of *E. coli*-encapsulated PEG-based microdroplet using a microfluidic chip for biological application, (Lee et al. 2010a. Copyt 2020. Scale bar=100 μ m. e Fluorescence micrographs of PEGDA Janus microparticles with one side of the particles containing fluorescently labeled TMV—Adapted with permission from (Lewis et al. 2010). Copyt 2020 American Chemical Society. Scale bar=100 μ m

thermally treated, in the fabrication of porous bacterial cellulose (pBCs) scaffolds for in vitro cell culture—Fig. 6d and e. They used a microfluidic device to control the dimensions and the monodispersity of the microparticles.

To produce microparticles by thermal gelation in microfluidic devices by droplet microfluidics (Table 1), the experimental setups require temperature control systems at different steps of the process (Tumarkin and Kumacheva 2009). This problem has been solved by operating the device in a temperature-controlled room or chamber, moving the

Hydrogel	Continuous phase	Surfactant	Size	Channel width	References
Agarose	Mineral oil and glycerol	Span 80 (3% wt)	110 µm	20 µm	(Kumachev et al. 2011)
Agarose	Oil	_	$180 \pm 7 \ \mu m$	360 µm	(Leng et al. 2010)
Chitosan/agarose	Mineral oil	Span 80 (3% w/v)	$18.4 \pm 2.3 \ \mu m$	70 µm	(Zamora-Mora et al. 2014a)
Agarose	Mineral oil	-	300–500 µm	889 µm	(Yin et al. 2015)
Gelatine	Soybean oil	-	45–120 μm	100 µm	(Yeh et al. 2013)
Gelatine	Mineral oil	Span 80 (20% w/w)	66 µm	54 µm	(Park et al. 2016)
Gelatine	Rapeseed oil	-	115–160 µm	20 µm	(Wassén et al. 2012)
Gelatine	Liquid parafin	-	200 µm	300 µm	(Sakai et al. 2011)
K-carrageenan	Palm oil	-	0.76 mm	0.55 mm	(Leong et al. 2011)
K-carrageenan	Palm oil	-	1.3–1.8 mm	0.8 mm	(Jegannathan et al. 2009)

Table 1 Production of thermoreversible microparticles in microfluidic devices

droplets between controlled environments at different temperatures (Aubry et al. 2015) or, the ideal choice, by adding heating elements to the microdevice (Yeh et al. 2013). An example of a microfluidic device with an integrated heating element was developed by Yeh et al. (2013). The heating element consists of an indium thin oxide (ITO) electrode controlled by an imposed voltage. The temperature was monitored near the droplet formation and kept at 95 °C.

4.2 Ionic gelation

Ionic gelation is the cross-linking of polyelectrolyte polymer solutions by counter ions induced by a specific condition, such as pH (Patil et al. 2010, 2012; Patel et al. 2017; Sacco et al. 2016). Several hydrogels can form a gel in the presence of ions. The most commonly used in microfluidics are sodium alginate (Table 2), chitosan and gellan gum. Sodium alginate is soluble in water, however, in contact with divalent or polycations forms an insoluble solid structure (Patil et al. 2010, 2012; Patel et al. 2017; Leong et al. 2016). The most used ions to cross-link sodium alginate are calcium and zinc (Patil et al. 2010, 2012; Sacco et al. 2016; Leong et al. 2016). Chitosan is cross-linked with poly-anions, such as alginates (Patil et al. 2010, 2012; Perez Bravo and Francois 2016). Gellan gum can be cross-linked with mono- or divalent cations and carboxymethyl cellulose derivatives are usually cross-linked with metal ions (Patil et al. 2010, 2012).

Ionic gelation can arise through several different mechanisms: external gelation, internal gelation, inverse gelation, interfacial gelation and multi-step interrupted gelation

 Table 2
 Production of alginate microparticles in microfluidic devices

	• ·					
Cross-linker	Cont. phase	Surfactant	Method	Size	Channel width	Ref
Calcium chloride	N-Hexadecane	Span 80 (1 wt%)	On-chip coalescence of droplets	60–95 μm	90 µm	(Choi et al. 2007)
	Food oil	-	On-chip coalescence of droplets	104–167 µm	50 µm	(Shintaku et al. 2006)
	FC 40 carrier oil	Fluorinated sur- factant (3% w/w)	On-chip coalescence of droplets	10 µm	10 µm	(Mazutis et al. 2015)
	Mineral oil	Span 80 (0.5% w/w)	On-chip coalescence of droplets	107 µm	50 µm	(Um et al. 2008)
	Mineral oil	Span 80 (0.4% w/w)	On-chip coalescence of droplets	60–230 µm	40 µm	(Martinez et al. 2012)
	Mineral oil	-	On-chip coalescence of droplets	41.2 μm	50 µm	(Liu et al. 2012)
	Octyl alcohol oil	-	On-chip internal gelation	50–300 µm	130 µm	(Xu et al. 2008)
	Soybean oil	-	On-chip coalescence of droplets	41.3 µm	50 µm	(Liu et al. 2006)
CaCO ₃ nanoparticles	Corn oil + acetic acid	Tween 20 (0.1% w/w)	On-chip internal gelation	94–112 μm	50 µm	(Tan and Takeuchi 2007)
	Fluorocarbon oil	Fluorinated sur- factant (1% w/w)	On-chip internal gelation	26 µm	20 µm	(Akbari and Pir- bodaghi 2013)

(Leong et al. 2016). The most commonly used mechanisms in microfluidics are internal gelation and external gelation, therefore they will be described in more detail.

In external gelation, the droplets of the pre-polymer solution are surrounded by ions introduced in the continuous phase of the microfluidic device. Afterwards, the ions start to cross-link and the interface of the droplet turns into solid (Tumarkin and Kumacheva 2009; Leong et al. 2016); a solid shell and a liquid core are then formed. In the literature, the simplest procedure to carry out external gelation is to promote the contact between the formed droplets and the ions off-chip, in a bath containing ions (Tumarkin and Kumacheva 2009; Leong et al. 2016). External gelation can also be conducted on-chip, but care must be taken to assure that gelation does not start before droplet formation. This requirement led to the development of several new chip designs (Fig. 9b-d) and mixing strategies, including the mixing of the pre-polymer and the cross-linker in the region of droplet formation (Choi et al. 2007), the fusion of droplets containing the cross-linker with droplets containing the prepolymer (Liu et al. 2006, 2012; Shintaku et al. 2006) and the use of a third fluid layer to delay the diffusion of the crosslinker to the region containing the pre-polymer (Mazutis et al. 2015; Xu et al. 2008).

In internal gelation, gelation is induced by a trigger external to the droplet (Leong et al. 2016). The cross-linker is initially in an inactive state within the droplet and is activated by an external factor, releasing ions (Leong et al. 2016), which start to cross-link the droplet. Internal gelation of alginate can be induced on-chip or off-chip. In both cases, droplets containing CaCO₃ nanoparticles and alginate are formed and afterwards get in contact with a low pH phase that induces the release of Ca²⁺ from the nanoparticles leading to gelation (Fig. 9a).

4.3 Photopolymerization

Photopolymerization is induced by UV radiation in the presence of a photoinitiator. The UV light interacts with the photoinitiator originating free radicals which polymerize forming a cross-linked hydrogel (Nguyen and West 2002). Photopolymerization facilitates the temporal and spatial control of the polymerization, induces fast curing rates and can be conducted at room or physiological temperature (Nguyen and West 2002). Hydrogels that undergo photopolymerization include PEG derivatives, PVA derivatives and hyaluronic acid derivatives.

The simplest approach to produce microparticles by photopolymerization is by combining droplet microfluidics with UV radiation to solidify the droplets (Table 3). For example, Dang et al. (2012) produced monodispersed microparticles of PEGDA and poly(ethylene glycol) methyl ether acrylate



Fig.9 Schemes used for alginate microparticle production: **a** use of acidic oil to induce pH gelation(Tan and Takeuchi 2007); **b** slow fusion of alginate and $CaCl_2$ droplets using a water layer to separate the two monomers (Mazutis et al. 2015); **c** fusion of alginate droplets

with $CaCl_2$ droplets, with an expansion zone to obtain disk-shaped microparticles (Liu et al. 2006); **d** fusion of alginate and $CaCl_2$ droplets (Shintaku et al. 2007)

Hydrogel	Continuous phase	Particle shape	Photoinitiator	Surfactant	Size (µm)	Channel width (µm)	References
PEGDA	Mineral oil	Spheres, plugs and disks	2-Hydroxy-2-meth- ylpropiophenone, 2-hydroxy-4'-(2- hydroxyethoxy)-2- methylpropiophenone	Abil EM 90 (3% v/v)	10.8	40	(Hwang et al. 2008a)
PEGDA/PEG- MEA	Mineral oil	Spheres	2-Hydroxy-2-methyl- propiophenone	Octylphen oxypolyeth- oxyethanol (1 wt%)	40–200	100	(Dang et al. 2012)
PEGDA	Mineral oil	Spheres	2-Hydroxy-2-methyl- propiophenone	ABIL EM 90 (3% v/v)	50	50	(Lewis et al. 2010)
PEGDA	Hexadecane	Spheres	2-Hydroxy-2-methyl- 1-phenyl-propan- 1-one	Span 80 (> 3 wt%)	45–95	200	(Choi et al. 2009)
PEGDA	Silicon oil	Spheres	2-Hydroxy-2-methyl- propiophenone	_	75–375	75	(Yu et al. 2013)

Table 3 PEG microparticles production by photopolymerization in microfluidic devices

(PEGMEA) using a microfluidic device and photopolymerization by UV irradiation. They studied the influence of the channel geometry, flow rates and hydrogel concentration. Lee et al. (2010b) produced PEGDA microgels for *E. coli* encapsulation by polymerization using a microfluidic device—Fig. 8d. Lewis et al. (2010) used a flow-focusing device to produce microparticles of viral nanotemplates in PEGDA—Fig. 8c and e. The viral nanotemplates were uniformly distributed through the PEGDA, while the droplets were polymerized by UV irradiation. Hwang et al. (2008a) produced spherical and non-spherical magnetic microgel particles using a microfluidic device and a UV light reflector. They used PEGDA and obtained monodispersed microparticles. The use of a UV light reflector contributed to improving the photopolymerization of the hydrogel.

The combination of droplet microfluidics with UV radiation has inherent limitations, as the range of geometries that can be produced is restricted to spheres, plugs or disks (Dendukuri et al. 2007). The alternative is to use photolithography, a method that enables the design on demand of the particle shape. The shape of the particle is defined by an optical mask that partially blocks the incident UV light (Dendukuri et al. 2007).

Photolithography requires that only a defined region of fluid is exposed to UV light for a short time. Since the target material is flowing in the microchannel, the high-throughput production of microparticles is an important challenge for photolithography. This problem is the motivation for the development of techniques to operate the microparticle production continuously:

1. Continuous flow lithography (CFL) (Dendukuri and Doyle 2009) takes advantage of the inhibition reaction

caused by the oxygen from the air diffusing through the polymer. This inhibition creates a barrier against the photopolymerization of the hydrogel near the wall, enabling the transport of microparticles through the microchannel. CFL must operate at a low flow rate otherwise the particles obtained will be smeared and will have a poor resolution.

- Stop flow lithography (SFL) (Dendukuri et al. 2007; Dendukuri and Doyle 2009) can overcome the limitations of the CFL process. The flowing stream of the photopolymerizable hydrogel is stopped, and only then the UV light is turned on, improving the resolution of the microparticles.
- 3. Stop flow interference lithography (SFIL) (Dendukuri and Doyle 2009; Jang et al. 2007) enables the formation of microparticles with 3D characteristics. A phase mask that induces peaks into the light intensity and in the direction of propagation is used, enabling the control of the geometrical parameters and of the volume fraction of the microstructure formed.

Photolithography has led to the production of a large variety of particle shapes and functionalities. Hwang et al. (2008a) obtained disk, plug and sphere shape microparticles through photomasks—Fig. 10a–c. They noticed that the deformation of the microparticles can occur due to non-uniform UV light exposure and to large gradients of UV light. This problem was solved through the use of a UV light reflector made of aluminum foil. Zhan et al. (2002) produced PEG hydrogel parallelepipedic microparticles (135 μ m × 200 μ m × 15 μ m) using photomasks in microchannels. The size of the microchannel and the size and shape of the photomask defined the size and shape of the microparticles.



Fig. 10 Microparticles of PEG with different shapes obtained by photolithography: **a** disks; **b** plugs; **c** spheres; **d** hexagon; **e** butterfly; **f** butterfly and ring. Scale bars for **a**–**c** are of 20 μ m and for **d**–**f** are of 100 μ m. Images **a**–**c** Republished with permission of Royal Society of Chemistry (Great Britain) from Microfluidic-based synthesis of non-

It is also possible to use maskless lithography techniques. These techniques use spatial light modulators (SLMs) controlled by a computer (Chung et al. 2007). Chung et al. (2007) used an optofluidic maskless lithography process to obtain PEGDA microstructures. They were able to produce a butterfly and a ring microstructure (with approximately 150 μ m length and 130 μ m height)—Fig. 10d and e. This type of photolithographic method reduces the time and cost spent to generate the masks.

5 Hydrogel properties

Hydrogels can be produced from natural sources (natural hydrogels) or by chemical synthesis in laboratories (synthetic hydrogels) (Tumarkin and Kumacheva 2009; Gao et al. 2012a)—Table 4. Natural hydrogels present poor mechanical properties, but, due to their biocompatibility, have a high potential to interact directly with cells. Synthetic hydrogels present poor interaction with cells, but they have better mechanical properties and can be easily produced in large quantities. The selection of a hydrogel depends on the intended application. Due to their biocompatibility, agarose, alginate and poly(ethylene glycol), Pluronic F-127 and carrageenan are the most used hydrogels and their characteristics will be discussed in some detail.

To design a microfluidic setup for particle production, the fluids used need to be fully characterized. As shown in Sect. 2, in droplet microfluidics, the flow regime and the droplet size depend on the Capillary numbers of both phases and on the viscosity ratio. Droplet size is also influenced spherical magnetic hydrogel microparticles, (Hwang et al. 2008b), 2020; permission conveyed through Copyt Clearance Center, Inc. While d-f Reprinted from (Chung et al. 2007), with the permission of AIP Publishing

Table 4 Natural and synthetic hydrogels

Hydrogels		
Natural hydrogels		Synthetic hydrogels
Proteins	Polysaccharides	
Collagen	Agarose	PEG—poly(ethylene glycol)
Gelatin	Alginate	PAC—poly(acrylic acid)
Fibrin	Chitosan	PVA-poly(vinyl alcohol)
Elastin-like polypeptides (ELPs)	Hyaluronic acid	Poloxamers
	Cellulose derivatives	pNiPAAm—poly(N-isopro- pyl acrylamide)
	Dextran	
	Xyloglucan	
	Carrageenan	

by the surfactant concentration and interfacial tension. Depending on the gelation method, additional properties are required such as the gelation temperature and reactant concentration.

5.1 Properties of thermoreversible hydrogels

In microfluidics, the most commonly used thermoreversible hydrogels are agarose, Pluronic F-127, carrageenan and gelatine. Their gelation properties (Table 5) are critical to the design of the device and the setting of the operational conditions of the experimental setup. These properties include the melting temperature, the gelling temperature and the

	Agarose	Pluronic F-127	Gelatin	K-Carrageenan
Gelling temperature (°C)	15–30 (Tumarkin and Kumacheva 2009; Leng et al. 2010)	20–40* (Matthew et al. 2002)	<25 (Yeh et al. 2013)	< 30 (Grenha et al. 2010)
Melting temperature (°C)	56 (Leng et al. 2010)	60 (Matthew et al. 2002)	>25 (Yeh et al. 2013)	> 30 (Grenha et al. 2010)
Viscosity (Pa.s)	$0.5 \times 10^{-2} (0.5\% \text{ wt})$ (Kumachev et al. 2011) $2.4 \times 10^{-1} (3.0\% \text{ wt})$ (Kumachev et al. 2011)	≈ 0.1 Pa.s (15% wt, 25°C) (Stoeber et al. 2005)	1.35×10^{-3} (1% wt) (Park et al. 2016) 3.07×10^{-2} (30% wt) (Park et al. 2016)	1.31×10 ⁻¹ (15 g/L, 40°C) (Leong et al. 2011)
Interfacial tension (mN/m)	2.2 (Kumachev et al. 2011; Oh et al. 2008)	36±0.29 (at 1% wt and 25°C) (Shah et al. 2015)	4 (Aubry et al. 2015)	7.08 (Leong et al. 2011)
Critical concentration	$0.065 \pm 0.005 \times 10^{-4} \text{ (mol/L)}$ (high viscosity) $0.106 \pm 0.005 \times 10^{-4} \text{ (mol/L)}$ (low viscosity)	17–18% wt in water (Matthew et al. 2002)	-	-

Table 5 Physical properties of agarose, Pluronic F-127, getaun and k-carrage
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*Depending on the concentration

monomer critical concentration (minimum concentration of the hydrogel monomer required for gelation). The hydrogel needs to be in the liquid state when it is injected into the microchannel. After, the microdroplets need to be solidified by decreasing or increasing the temperature, depending on the hydrogel used. After gelation, the microparticles remain solid below its melting temperature, which, usually, does not coincide with its solidification temperature.

Agarose is a neutral polysaccharide extracted from seaweeds (Zamora-Mora et al. 2014a; Ellis and Jacquier 2009a) extensively used in biomedical research (Leng et al. 2010; Kumachev et al. 2011) and in the food industry (Ellis and Jacquier 2009a). The gelling temperature of agarose is in the range 15-30 °C (Tumarkin and Kumacheva 2009; Leng et al. 2010) and above this temperature, agarose is in the liquid state (Leng et al. 2010). Agarose gels will only change again to the liquid state when the temperature rises to its melting temperature (56 °C) (Leng et al. 2010). The correct design of the microfabrication procedure also needs to take into account the variability of agarose properties with concentration. According to Normand et al. (2000), the gelation temperature increases when agarose concentration increases. The authors also referred that agarose has a critical concentration bellow which gelation does not occur; this limit is 6.5×10^{-6} mol/L for high viscosity agarose and 1.06×10^{-5} mol/L for low viscosity agarose.

Pluronic F-127 is a copolymer (Yeh et al. 1996; Matthew et al. 2002; Geroski and Edelhauser 2000; Gilbert et al. 1987) with many applications since its gelation temperature (20–40 °C) is close to the human body temperature. Besides, Pluronic F-127 is non-toxic and so it can be easily employed in drug delivery systems (Giovagnoli et al. 2010; Nie et al. 2011). At low temperatures, Pluronic F-127 is a micellar liquid and when the temperature starts to increase, the micelles start to aggregate and pack forming a gel (Dumortier et al. 2006). The gelling temperature depends on the concentration, decreasing when the concentration increases (Matthew et al. 2002; Dumortier et al. 2006). A solution with a concentration between 20 and 30% (wt) can form a gel between 30 and 35 °C (Matthew et al. 2002). According to Matthew et al. (2002), the minimum concentration to form a gel is about 17–18% (wt) in water. Gilbert et al. (1987) studied the thermal gelation of Pluronic F-127. They concluded that at higher concentrations (24–34% wt), the gelling temperature is very low. Stoeber et al. (2005) studied Pluronic F-127 solutions (10–30% wt) and concluded that above 26 °C, the viscosity strongly increases. Stoeber et al. (2006) observed that Pluronic F-127 presents a shear-thinning behavior near the gelling point, however, at lower temperatures, it exhibits a Newtonian behavior.

The properties of Pluronic F-127 were explored by Aubry et al. (2015) to immobilize early larval *Caenorhabditis elegans* for visualization. The larvae were first isolated inside droplets of 25% (w/v) Pluronic F-127 solution formed at 12 °C in a microfluidic device. The droplets were then heated, by moving the device to a room at 22 °C, to entrap the larvae in solid Pluronic F-127. The authors selected 12 °C as the temperature of droplet formation, using a controlled chamber to avoid unstable flow conditions at temperatures near the gelling temperature.

Carrageenan (Leong et al. 2011; Grenha et al. 2010) is, like agarose, extracted from seaweeds and, depending on the method of extraction, different types of Carrageenan are obtained (Grenha et al. 2010). From all the carrageenan types, only κ -carrageenan and τ -carrageenan can form gels, being κ -carrageenan gels more rigid (Grenha et al. 2010). κ -Carrageenan gels form at low temperatures and turn into the liquid state when heated (Leong et al. 2011; Grenha et al. 2010; Ellis and Jacquier 2009b; Li et al. 2014). It can also form a gel in the presence of mono- and divalent cations such as KCl, NaCl and MgCl₂ (Leong et al. 2011; Li et al. 2014).

Gelatine, another natural hydrogel, is suitable for medical and pharmaceutical applications due to its biocompatibility, biodegradability, non-toxicity and easy removal in physiological environment (Park et al. 2016; Yeh et al. 2013). Gelatine is thermoreversible and becomes a gel when the temperature decreases bellow 25 °C (for a solution of 1% (w/v)) (Yeh et al. 2013).

The properties of the microparticles are also very important, since for each application they should have specific characteristics. One of the most important is their integrity, i.e., the particles need to have good mechanical characteristics, otherwise can fragment. The mechanical properties are also important for the design of biomimetic fluids (e.g., blood analogue fluids). In the area of drug delivery, the cross-linking density and the diffusion coefficient are also very relevant, to control the drug release rate. A low crosslinking density will result in a rapid drug release.

Significant research has been dedicated to optimizing the conditions required to improve the mechanical properties of hydrogel particles, by testing different temperatures and composition and by experimenting hybrid materials. Kumachev et al. (2011) produced agarose microbeads by droplet microfluidic with different mechanical properties by modifying the agarose concentration and temperature. When they increased the concentration, the gel became stronger, since the elastic shear modulus increased: at 4 °C, agarose hydrogels with a concentration of 0.75% (wt) had an elastic shear modulus of 26 Pa while agarose hydrogels with a concentration of 3.0% (wt) had an elastic shear modulus of 4420 Pa. When they increased the temperature, the gel became weaker; when the temperature was increased to 37 °C, the elastic shear modulus for 0.75% (wt) and 3.0% (wt) decreased to 1 Pa and 700 Pa, respectively. They also concluded that a longer gelation time increases the rigidity of agarose microbeads. Zamora-Mora et al. (2014a) produced chitosan/agarose microparticles with controlled size using microfluidic emulsification. They concluded that chitosan offers a reinforcement of the gel structure, improving the mechanical properties of agarose. In addition, Park et al. (2016) concluded that, for gelatine microparticles, the increase in gelatine concentration led to the formation of strong networks and, by consequence, gel microparticles with better mechanical properties. Increasing the temperature, the microparticles stiffness decreases mostly due to the degradation of the polymer network.

5.2 Properties of ionic hydrogels

One of the most used hydrogels that undergo ionic gelation is alginate. Alginate is a linear copolymer also extracted from seaweeds composed of two acid monomers: β -D-mannuronic

acid and α -L-guluronic acid (Gao et al. 2012a; Choi et al. 2007; Xu et al. 2008; Tan and Takeuchi 2007). When alginate chains get into contact with multivalent cations such as Ca²⁺, Ba²⁺ or Fe³⁺, an alginate hydrogel is easily obtained (Gao et al. 2012a; Choi et al. 2007; Shintaku et al. 2006; Xu et al. 2008).

Alginate hydrogels can be formed by fast and easy methods (Mazutis et al. 2015; Choi et al. 2007; Xu et al. 2008) and also present a slow degradation rate (Mazutis et al. 2015). Alginate viscosity depends on the concentration of the solution while the interfacial tension depends on the specific surfactant and continuous phases used (Table 6). Viscoelastic and shear-thinning behaviors (Martinez et al. 2012) have been observed and viscosity is sensible to pH variations (Lee and Mooney 2012). Alginate concentration and the critical concentration of the cross-linker (minimum concentration of the reactive species to occur gelation) need to be specified and controlled during microparticle formation. Mazutis et al. (2015) produced biconcave alginate microparticles with a size similar to mammalian cells in a microfluidic device—Fig. 7. They concluded that above 2% (w/w) of alginate, the process is unfeasible due to the high viscosity of the solution. They also concluded that a concentration of CaCl2 between 2 and 5% (w/w) leads to gelation before droplet formation, while a concentration of 0.1%(w/w) does not promote gelation. The most viable concentration range of CaCl₂ to produce droplets of alginate hydrogel is between 0.5 and 1.0% (w/w), for which gelation occurs after the droplet formation. Microbeads can be obtained by adding a surfactant to decrease the interfacial tension of the continuous phase.

For alginate hydrogels, the mechanical properties are determined by the sodium and alginate solution concentrations, cross-linking density and gelation rate of the hydrogel (LeRoux et al. 1999). An increase in the sodium and alginate solution concentrations leads to an increase in the viscosity and surface tension (Ye et al. 2017). The higher is the

Table 6 Properties of alginate

Property	Value
Viscosity (0.5% wt) (Pa.s) (Choi et al. 2007)	4.0×10^{-2}
Viscosity (1.0% wt) (Pa.s) (Choi et al. 2007)	8.0×10^{-2}
Viscosity (2.0% wt) (Pa.s) (Choi et al. 2007)	2.4×10^{-1}
Surface tension (mN/m) (Shintaku et al. 2006) Sodium alginate solution 1.5% (w/w)at 20 °C	72
Interfacial tension (mN/m) (Shintaku et al. 2006) Sodium alginate solution 1.5% (w/w) and food oil at 25 °C	34
Density (g/cm ³) (Lee et al. 2000) Sodium alginate solution 2% (w/w) at 25 °C	0.8755
Minimum concentration of CaCl ₂ to form hydrogel (w/w) (Mazutis et al. 2015)	0.5%

concentration of alginate the higher are compressive and shear moduli, while the concentration of Na²⁺ has the opposite effect (LeRoux et al. 1999). The mechanical strength of alginate hydrogel decreases when it is exposed to physiological environments (Lee et al. 2000; LeRoux et al. 1999). (Benavides et al. 2012) studied the effect of CaCO₃ concentration on the mechanical properties of alginate hydrogels. They concluded that, in the presence of CaCO₃, the mechanical strength of the hydrogels improved due to the development of a rigid network, originated by the interactions between the alginate and calcium ions. The gelation rate of alginate hydrogels also influences the final mechanical properties. Kuo and Ma (2001) concluded that a slow gelation rate results in better mechanical properties. The mechanical properties of alginate hydrogels are summarized in Table 7.

5.3 Properties of photopolymerizable hydrogels

The most used synthetic photopolymerizable hydrogels are poly(ethylene glycol) derivatives such as PEG acrylate and PEG methacrylate derivatives (Nguyen and West 2002). PEG hydrogels are bio-inert (Gao et al. 2012a; An et al. 2009), can easily incorporate bioactive and biodegradable species (Gao et al. 2012a), are non-toxic (Lee et al. 2010b; An et al. 2009), hydrophilic (An et al. 2009; Rossow et al. 2012) and can resist to cell and protein adhesion and absorption (An et al. 2009), the reason why they are immune and resist to inflammatory processes (Gao et al. 2012a; An et al. 2009). PEG was approved by the Food and Drug Administration (FDA) for oral and dermal applications (Xue et al. 2014; Evans et al. 2014).

The production of microparticles by photopolymerization has additional constraints and new additional parameters

 Table 7
 Mechanical properties of alginate hydrogels

Property	Value
Maximum shear modulus (kPa) (Lee et al. 2000) (gel formed with an alginate solution of 2% (w/w))	24.4 ± 0.6
Tensile strength (MPa) (Benavides et al. 2012) (film of hydrogel formed with an alginate solution of 1.5% (w/v), addition of glycerol as plasticizer)	$\begin{array}{c} 39.7 \pm 5.3 \\ (0 \text{ g} \\ CaCO_3/\text{g} \\ alginate) \\ 52.6 \pm 6.1 \\ (0.01 \text{ g} \\ CaCO_3/\text{g} \\ alginate) \\ 51.9 \pm 5.8 \\ (0.02 \text{ g} \\ CaCO_3/\text{g} \\ alginate) \\ 52.9 \pm 5.5 \\ (0.03 \text{ g} \end{array}$
Percent of elongation (%) (Benavides et al. 2012) (film of hydrogel formed with an alginate solution of 1.5% (w/v), addition of glycerol as a plasticizer)	CaCO ₃ /g alginate) 4.4 ± 0.5 (0 g CaCO ₃ /g alginate) 4.5 ± 0.8 (0.01 g CaCO ₃ /g alginate) 2.3 ± 1.2 (0.02 g CaCO ₃ /g alginate) 2.3 ± 0.9 (0.03 g CaCO ₃ /g alginate)
Dynamic shear modulus (kPa) (LeRoux and M., F. Guilak, and L. Setton, 1999) (get formed with an alginate solution of 2% (w/w))	23.57 ± 5.91
Young Modulus (kPa) (Chan et al. 2011) (gel formed with an alginate solution of 15 g/L and $CaCl_2=0.5 M$)	339

need to be known, namely: the photoinitiator concentration, hydrogel monomer concentration, UV light intensity, wavelength and exposure time. When PEG acrylate and PEG methacrylate derivatives are exposed to UV light in the presence of a photoinitiator, the photoinitiator dissociates and creates radicals that attack the carbon-carbon double bond of the acrylate, triggering a free radical polymerization (An et al. 2009). Filatov et al. (2017) performed a study to obtain the gelation time and the mechanical properties of PEGDA microparticles. They concluded that the gelation time is strongly dependent on the photoinitiator concentration and that SPAN 80 influences the solidification of the particles (comparison with the absence of surfactant and with the use of Abil EM 180). They obtained an optimal value for the photoinitiator concentration around 1% (w/w). Table 8 summarizes the key physical properties of the poly(ethylene glycol) diacrylate.

The monomer concentration influences the cross-linking density, which determines the microparticle mechanical properties. Allazetta et al. (2013) produced PEG hydrogels with different cross-linking densities by varying PEG concentration. Duprat et al. (2015) developed a method to measure the elastic modulus of PEGDA microparticles produced in a microfluidic device and showed that the elastic modulus increases with the increase of PEG concentration and exposure time. The diffusion of solutes in hydrogels can be estimated by optical and elution methods. Evans et al. (2014) used a microfluidic device, optical and elution methods and effluent analysis to estimate the solute diffusion in PEG hydrogels. They concluded that with high polymer concentrations, the hydrogel becomes more cross-linked and the diffusion coefficients are smaller.

Merkel et al. (2011) used 2-hydroxyethylacrylate combined with PEGDA to reproduce red blood cells. The objective was to obtain particles with properties (size, shape and deformability) similar to those of red blood cells. They concluded that the cross-linking density strongly influences the mechanical properties of the microparticles. With a crosslinking density of 10%, they obtained an elastic modulus of 63.9 kPa, while for a cross-linking density of 1% the modulus was 7.8 kPa. The elastic modulus of the red blood cells (RBCs) is 26 ± 7 kPa (Tomaiuolo 2014), indicating that PEGDA can be used to mimic the RBCs by tuning the concentration.

Poly(vinyl alcohol) (PVA) derivatives and hyaluronic acid (HA) derivatives are also photopolymerizable (Nguyen and West 2002). Poly(vinyl alcohol) has good mechanical properties and demonstrates good optical and elastic properties (Kityk et al. 1997; Schmedlen et al. 2002). PVA is biocompatible and resists to protein adsorption and cell adhesion and has properties suitable for drug delivery (Schmedlen et al. 2002). Schmedlen et al. (2002) concluded that the elastic modulus and ultimate tensile strength of PVA hydrogels increase with an increase of the PVA concentration. Hyaluronic acid is a natural hydrogel found in the human body (Burdick et al. 2005; Burdick and Prestwich 2011). Hyaluronic acid solutions have high viscosity and shear-thinning behavior (Schanté et al. 2011). Due to its biocompatibility, hyaluronic acid has many applications and can be used in drug delivery systems and eye surgeries (Burdick and Prestwich 2011; Schanté et al. 2011).

6 Control of size, shape and microstructure

Particles produced by droplet microfluidics are spherical by default, but other shapes can be obtained by modifying the technique. Cylindrical particles can be obtained if the gelation is carried out when the particles are confined along axisymmetric microchannels (Cai et al. 2019). Double-emulsion techniques are used to obtain core and shell (Yu et al. 2019) and Janus particles (Geng et al. 2018) comprising different materials. Spherical microparticles can be combined in clusters of different arrangements to produce colloidal molecules (Shen et al. 2016). However, more complex shapes require photolithography. By selecting the appropriate mask shape, it is possible to produce planar particles of any shape and even composite particles of different materials (Dendukuri and Doyle 2009; Dendukuri et al. 2007).

In droplet microfluidics, the size of the particle produced depends on the size of the microchannel and on the operational conditions that determine the flow regime. In the dripping regime, the particle is usually larger than the channel width, while in the jetting regime the particle can be much smaller than the channel width (see works listed in Tables 1, 2, 3). Depending on the flow rate ratio (Cubaud and Mason 2008), the size of the particles can be 25% of the channel width (Cubaud and Mason 2008; Carneiro et al. 2019).

Table 8 Physical propertiesof the poly(ethylene glycol)diacrylate

Property	Value
Viscosity (10% wt)	2.2×10^{-2} (Pa.s) (Ziemecka et al. 2011)
Surface tension (10% wt)	0.1(mN/m) (Ziemecka et al. 2011)
Critical surfactant concentration-wt%	> 3 (PEGDA 95% wt) (Choi et al. 2009)
Critical surfactant concentrarion-wt%	1 (PEGDA 50% wt) (Yousefi et al. 1997)

Practical limits restrict the size, and size distribution, of the particles that can be produced by droplet microfluidics. To operate in the dripping regime, the Capillary number of the dispersed phase must be smaller than the critical value, 0.1, which implies that μv must be smaller than 0.1 σ . Therefore, to operate in the dripping regime, the flow rate has an upper threshold, which is lower when the viscosity of the dispersed phase is higher. In addition, viscous fluids lead to high pressures in the device, restricting the size of the channel that can be used for the same throughput.

Photolithography is an alternative to droplet microfluidics for two main reasons: the fabrication accuracy is higher and the range of shapes that can be produced is wider. Photolithography can produce structures of 400 nm on a stationary polymer precursor (Nakagawa et al. 1990). In the case of two-photon laser writing, the particles can have 200 nm and the accuracy of the technique can reach 20 nm. However, to achieve high throughput, the production needs to operate in a continuous flow, which reduces the accuracy of the method. Furthermore, if the liquid precursor flows too fast, the particles can be distorted by the velocity gradients in the flow. Stop and flow techniques (Dendukuri et al. 2007; Dendukuri and Doyle 2009) have been developed to address this problem, but the stop/flow process is difficult to control and some smear of the particles can still be observed at high flow velocities. Full 3D particles, with detailed features and high throughput, can be obtained by moving the light source to offset the flow distortion (Shaw et al. 2018).

7 Challenges and future developments

The production of hydrogel microparticles through microfluidic systems presents several advantages, such as control over the size and shape of the droplets, control over the consumption of reactants, control over the timing of the reactions and the ability to conduct reactions with high efficiency under safe conditions. Although all these advantages, some issues need to be studied and developed further.

Cell encapsulation and drug delivery systems can be used for several therapies, such as diabetes, bone and cartilage injuries, heart diseases and cancer. Hydrogel microparticles in these therapies require the removal of the continuous phase from the particles. If the continuous phase is not completely removed, contamination of the microparticles may trigger an immune response of the human body (Gao et al. 2012a). In addition, it is still not possible to encapsulate precisely only one cell per droplet, which has been and will be a challenge (Tumarkin and Kumacheva 2009).

In chemical reactors, hydrogel microparticles promote higher reaction rates due to their higher surface-to-volume ratio (Teh et al. 2008). However, there is a chance that the molecular adsorption at the microparticles interferes with the reaction when the reaction rate is too high. Extreme reaction conditions can damage the hydrogel microparticles and this can also be a challenge for several applications (Teh et al. 2008).

Photolithographic techniques have had significant progress in recent years. It is now possible to produce 3D particles with 3D features and submicrometric accuracy. The field is now ready to address new challenges. The most prominent is the scale-up of the microparticles production and the development of new applications for which microparticles with 3D features are relevant. The most promising approach to scale-up is parallelization, which, in the case of photolithography, requires the parallelization of the optical equipment. The integration of the optical equipment in the microdevice, using optofluidic (Fan and White 2011; Schmidt and Hawkins 2008) miniaturization fabrication method is a route that needs to be explored. New applications need to be developed for microparticles with 3D features. Among the most promising are the use of particles as components of more complex structures and machines (Chung et al. 2008; Sacanna et al. 2010; Wang et al. 2014). Particles could also be used as lock and key devices for selective interactions with biological species.

Hydrogels are responsive to temperature and pH variations and so they are suitable for actuator functions (Ionov 2014; Ma et al. 2018). The responsiveness of hydrogels can also be explored to develop swimmers suitable to operate as microbots (Magdanz et al. 2014; Jeon and Hayward 2017). Anisotropic particles are also suitable for the development of microbots (Palacci et al. 2015) and fluids with anisotropic viscosity. Microfabrication techniques able to produce particles of any shape and of different materials can be combined with the manipulation of the particle environment to obtain microbots able to perform medical roles, like complex drug delivery operations in specific spots of the human body.

The particle output of a microfluidic device is in the range of microliters per minute, which limits significantly the amount of particles that can be produced using a single microfluidic device. The flow rate of the dispersed phase is limited by the high-pressure drop and the maximum pressure the device can support. Furthermore, to obtain monodispersed particles, the system must operate in the dripping regime, and so this limit is even lower. The amount of particles that can be produced is also constrained by the viscosity of the dispersed phase. Therefore, high-throughput microfluidic systems are only feasible by scale-up through parallelization (Tumarkin and Kumacheva 2009). But parallelization itself has also its issues. Parallel devices are based on hierarchical networks prone to feedback effects and chaotic flow patterns, which lead to the formation of polydispersed microparticles. Two types of networks are usually used, tree configurations and ladder configurations. Ladder configurations generate more stable flows, while in tree configurations

the flow is sensitive to small microfabrication defects (Tetradis-Meris et al. 2009).

To be effective, parallelization needs to have a 3D arrangement, leading to new design and fabrication challenges. Recently, femtosecond laser micromachining has been used to produce 3D microstructures (Maia et al. 2017; Liao et al. 2012) and the technique is suitable for the fabrication of 3D networks with integrated waveguides (Maia et al. 2017), facilitating the integration of optical components for high-throughput photolithography.

Control of the mechanical properties of the hydrogels to extend their range of applicability is also a topic that requires further developments. The mechanical properties of the hydrogel microparticles can be improved by the introduction of new materials in their cross-linked structure. Carbon nanotubes are one of the promising materials to improve hydrogel mechanical properties (Kawaguchi et al. 2006). More complex structures, such as micro-vascularized networks, can be obtained with the use of 3D microfluidic platforms (Chung et al. 2012).

One significant challenge is the use of hydrogel microparticles as oxygen carriers (Kimelman-Bleich et al. 2009; Wijekoon et al. 2013). Hydrogels need to be combined with perfluorocarbons or hemoglobin to produce particles that can carry high quantities of oxygen. Production and rheology of the particles and blood analogues need to be optimized. This approach may contribute to the development of blood substitutes for disease treatments and tissue engineering without the ethical limitations of actual blood.

8 Conclusions

This review describes the most important aspects of the production of hydrogel microparticles through microfluidic devices. These devices enable the control of the size, shape and mechanical properties of the hydrogel microparticles. Several routes are available for particle fabrication in microfluidic devices. The properties of the precursor fluids and the definition of the operating conditions are crucial for the design of the microfluidic device, mainly because they determine the flow regimes and the droplet sizes. Surfactants should be carefully chosen to assure that the droplets do not coalesce before the solidification step. The surfactants distribution can have complex interactions with the flow patterns influencing the particle size.

Complex particle shapes can be produced by photolithography. However, to increase the throughput, the device needs to operate in continuous flow. Methods to achieve this, by synchronizing the UV radiation emission with the flow, and compensating distortions due to the fluid flow, were reviewed. Presently, the available technologies can produce, in principle, any particle shape with submicrometric accuracy.

The hydrogel microparticles have a great potential in several biomedical applications, and the use of microfluidics enables precise control over the formation of the particles and is useful to overcome most of the specific needs of these applications. Significant challenges remain yet to use microfluidics for large-scale particle production.

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