



Quaternary phosphonium cationic ionic liquid/porous metal–organic framework as an efficient catalytic system for cycloaddition of carbon dioxide into cyclic carbonates

Yu Lin Hu¹ · Rui Li Zhang¹ · Dong Fang²

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Abstract

Global warming and climate change concerns are triggering worldwide interest for sustainable transformation of CO₂ into useful chemicals. Here, a new and efficient multifunctional catalytic system for the cycloaddition of carbon dioxide with epoxides to synthesize cyclic carbonates under mild and solvent-free reaction conditions has been developed. The catalytic tests revealed that [P_{12,4,4,4}]Br/MIL-53(Cr) (MIL: Materials of Institut Lavoisier) was the best and powerful catalytic system in the cycloaddition with excellent yields (96–99%) under solvent-free condition and 100 °C, 1.0 MPa for 2–3 h. The synergistic effect of anion and cation of ionic liquid [P_{12,4,4,4}]Br as well as the chromium site of cocatalyst MIL-53(Cr) contributed to the excellent catalytic activity. The present catalytic system has several unique features such as simple operation, good to excellent yields, high catalytic activity, environmentally benign and safe. This study provides a sustainable and efficient synergistic strategy for chemical carbon dioxide fixation via the combination of ionic liquids and metal–organic frameworks.

Keywords Ionic liquid · Metal–organic framework · Cycloaddition · Epoxides · Carbon dioxide · Cooperative catalysis

Introduction

Carbon dioxide (CO₂) is the main greenhouse gas which caused the global warming and climate change. The keeping increase of CO₂ emission aggravates global warming, and controlling its emission is the only way to stop the climatic deterioration. Hence, a number of strategies have been proposed to reduce the CO₂ emission such as CO₂ capture, storage and chemical utilization (Carena and Vione 2016; Chatterjee and Krupadam 2018; Kumar et al. 2018; Lais et al. 2018; Liu et al. 2018; Nandigama et al. 2018;

Zhang et al. 2016). Among them, CO₂ chemical utilization is regarded as the most attractive one because CO₂ has been sorted as a cheap, nontoxic and abundant C1 building block for the preparation of a wide range of valuable chemicals (Sołtys-Brzostek et al. 2017). Currently, numerous strategies have been developed for CO₂ chemical utilization, and the cycloaddition of CO₂ and epoxides is one of the most attractive and sustainable crafts due to a wide range of applications of the target products cyclic carbonates in fine chemistry (Arshadi et al. 2017). However, the activation of CO₂ is difficult due to its inert nature resulting from its high thermodynamic and kinetic stability. The development of efficient catalytic systems for conversion of CO₂ into the desired cyclic carbonates is a crucial role for CO₂ utilization. In general, the cycloaddition of CO₂ to epoxides can proceed under alkali metal or quaternary ammonium salts catalysts (Ju et al. 2008; Zhou et al. 2010; Martín et al. 2015). However, these traditional catalysts are not entirely satisfactory owing to the limitations of corrosive wastes, tedious work-up and harsh reaction conditions. To overcome these restrictions, some representative catalytic systems used for the cycloaddition have been developed, including zinc(II) complexes of arylhydrazones of β-diketones/tetrabutylammonium bromide (Montoya et al. 2016), KI-tetraethylene

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✉ Yu Lin Hu
huyulin1982@163.com

¹ College of Materials and Chemical Engineering, Key Laboratory of Inorganic Nonmetallic Crystalline and Energy Conversion Materials, China Three Gorges University, Yichang 443002, People's Republic of China

² College of Chemistry and Environmental Engineering, Yancheng Teachers University, Yancheng 224002, People's Republic of China

glycol (Kaneko and Shirakawa 2017), organocatalysts (Alves et al. 2017; Sopeña et al. 2017; Fiorani et al. 2015; Whiteoak et al. 2012; Gennen et al. 2015; Wang and Zhang 2016), organometallic complexes (Tian et al. 2012; Chen et al. 2017), ascorbic acid/tetrabutylammonium iodide (Arayachukiat et al. 2017), poly(4-vinylimidazolium)s/diazabicyclo[5.4.0]undec-7-ene/ZnBr₂ (Seo and Chung 2014) and others (Kelly et al. 2017; Khatun et al. 2017; Lan et al. 2014, 2015, 2016a, b). Most of these catalytic methodologies, however, still suffer from several shortcomings such as the use of expensive reagents, high reaction temperature and pressure, unsatisfactory activity without co-catalysts, difficulties in work-up and environmental hazards. Consequently, there is an enormous demand for the development of efficient and eco-friendly catalytic systems for conversion of CO₂ to cyclic carbonates.

Ionic liquids, completely composed of ions, could be designed to possess a definite set of properties, and thus have wide applications as reaction medium or catalyst in chemical reactions. Further, due to their low vapor pressure and nonflammable, ionic liquids were assigned as a class of environmental materials (Sharifi et al. 2014; Tomé and Marrucho 2016; Costa et al. 2017). Nowadays, examples of their applications as catalysts in cycloaddition of CO₂ to epoxides were reported and demonstrated good catalytic activities (Qiu et al. 2017; Rojas et al. 2014; Lan et al. 2018). However, because of the difficulties associated with unsatisfactory catalytic performance and harsh reaction conditions, the development of novel and efficient ionic liquid-based catalytic systems is still in great demand. Phosphonium cation-based ionic liquids as a family of ionic liquids that in catalytic cycloaddition of CO₂ applications offer superior properties of thermal stability, solubility and high efficiency compared to the corresponding ammonium cation-based ionic liquids. Therefore, phosphonium ionic liquids have been utilized as nontoxic, environmentally benign and recyclable catalysts and widely adopted in foregoing researches (Bellina et al. 2012; Dai et al. 2016). Metal–organic frameworks (MOFs) are a class of fascinating materials that consist of coordination bonds between transition-metal cations and multidentate organic linkers, and they have been received considerable attentions as nontoxic and environmentally friendly heterogeneous catalysts in cycloaddition of CO₂ due to their attractive physical structure properties (Rubio-Martinez et al. 2017; Kaneti et al. 2017; He et al. 2016; Zhu et al. 2018). However, their weak activity and hydrothermal stability limited their catalytic applications. It is obvious that ionic liquids and metal–organic frameworks based dual catalytic system would exhibit more outstanding catalytic performances by combining the advantages of two materials, based on a synergistic effect of transition-metal center of metal–organic framework and the basic

sites (anion and cation) of ionic liquid (Ding et al. 2017). In light of the above-mentioned advantages of phosphonium ionic liquids and metal–organic frameworks, it is envisaged that phosphonium ionic liquid/metal–organic framework dual catalytic systems would have excellent synergistic effect and exhibit more highly efficient catalytic activity toward the cycloaddition of CO₂ to epoxides.

On the basis of the aforementioned considerations, herein, we report a simple, novel and efficient dual catalytic system containing porous metal–organic framework for the cycloaddition of CO₂ to epoxides in the presence of phosphonium ionic liquid tributyldecylphosphonium bromide ([P_{12,4,4,4}]Br). To our pleasure, the newly developed multifunctional synergistic system was endowed with excellent catalytic activity and reusability in good yields and selectivity for the cycloaddition under mild conditions.

Experimental

Materials and methods

The reagents were of analytical grade, and the ionic liquids were purchased from Aladdin and Lanzhou Greenchem ionic liquids, Chinese Academy Science. The chemical structures of catalysts were characterized by Fourier transform infrared spectroscopy (FT-IR) spectra using a Nicolet Nexus 470 spectrometer. The powder X-ray diffraction (XRD) analysis was carried out on a Rigaku Ultima IV diffractometer. N₂ adsorption–desorption measurements were measured on a Micromeritics-2010 apparatus. Thermal gravimetric (TG) analysis was performed using a Netzsch Thermoanalyzer STA 449 analyzer under nitrogen atmosphere. The element analysis of catalysts was determined by an Arcos EOP ICP-OES (Kleve, Germany). Scanning electron microscopy (SEM) was recorded on a JSM-7500F instrument. Gas chromatography (GC) analysis was carried out on a Agilent GC-7890A instrument. ¹H NMR (nuclear magnetic resonance) spectra were recorded on a Bruker 400 MHz spectrometer. Elemental analysis was performed on a Vario Micro cube elemental analyzer.

Preparation of metal–organic frameworks

Metal–organic frameworks were prepared following the procedures (Rubio-Martinez et al. 2017; Kaneti et al. 2017), and their characterization results (Fig. 1a, Fig. S1–S5, ESI) match well with those in the studies.

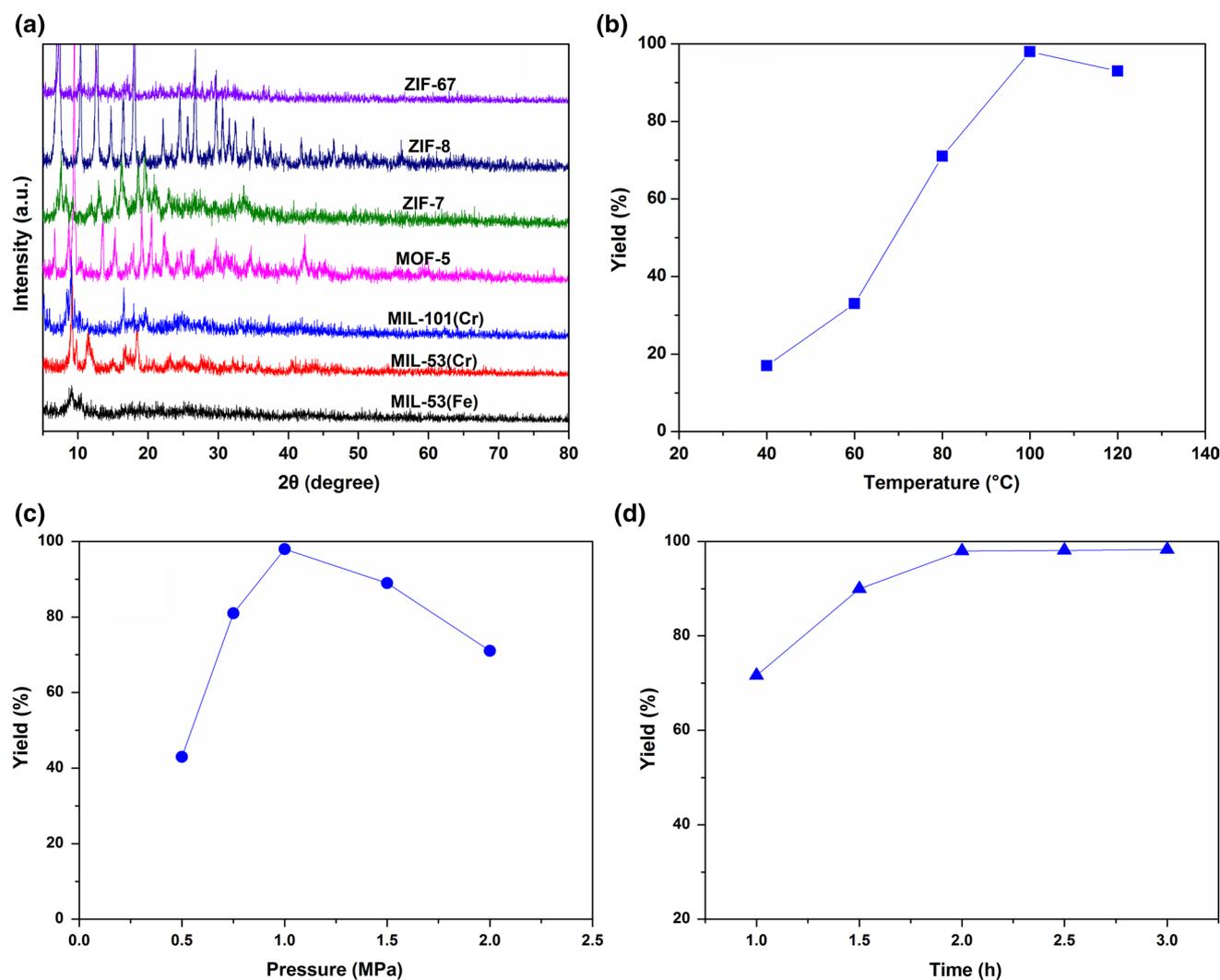


Fig. 1 XRD patterns of metal–organic frameworks (a) and influences of reaction conditions on the cycloaddition of CO₂ to propylene oxide over [P_{12,4,4,4}]Br/MIL-53(Cr) (b, c, d)

General procedure for catalytic cycloaddition of CO₂ to epoxides

In a typical process, epoxide (20 mmol) and ionic liquid (1.2 mmol), metal–organic framework cocatalyst (15 mg) were introduced into a stainless steel high pressure reactor. The reactor was sealed and flushed three times with CO₂ at room temperature. The pressure was then adjusted to 1.0 MPa, and the reaction mixture was stirred at 100 °C for the desired time. After the completion of the reaction, monitored by GC, the pressure of reactor falls down to a presetting value; then, the excess of CO₂ was vented. The catalytic system was collected by centrifugation and the products were analyzed by GC. For the recycling experiments, collection of the catalytic system was separated by centrifugation, and then fresh substrates were then recharged to the recovered catalytic system and then recycled under

identical reaction conditions. The products were identified by comparing their physical and GC spectra with those of commercial materials.

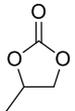
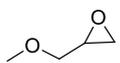
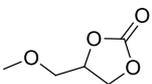
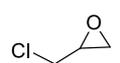
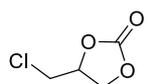
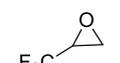
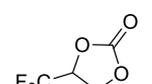
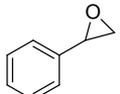
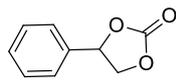
Spectral data

4-Methyl-1,3-dioxolan-2-one (Table 1, entry 1): ¹H NMR: δ = 1.41 (dd, *J* = 7.2 Hz, CH₃, 3H), 3.97 (t, *J* = 5.2 Hz, CH, 1H), 4.56 (t, *J* = 5.0 Hz, CH, 1H), 4.93 (t, *J* = 7.0 Hz, CH, 1H). Anal. Calcd. for C₄H₆O₃: C, 47.02; H, 5.89; O, 46.97. Found: C, 47.06; H, 5.92; O, 47.02.

1,3-Dioxolan-2-one (Table 1, entry 2): ¹H NMR: δ = 4.54 (s, CH₂CH₂, 4H). Anal. Calcd. for C₃H₄O₃: C, 40.89; H, 4.55; O, 54.48. Found: C, 40.92; H, 4.58; O, 54.50.

4-(Methoxymethyl)-1,3-dioxolan-2-one (Table 1, entry 3): ¹H NMR: δ = 3.33 (s, OCH₃, 3H), 3.72 (dd, *J* = 7.0 Hz, OCH₂, 2H), 4.08 (dd, *J* = 7.0 Hz, CH₂, 2H), 4.96 (m, CH,

Table 1 Catalytic cycloaddition of various epoxides with CO₂

Entry ^a	Epoxide	Product	Time (h)	Conversion (%) ^b	Yield (%) ^c
1			2	99	98
2			2	99	99
3			2	100	99
4			3	98	97
5			3	97	96
6			3	98	96

^aReaction conditions: epoxide (20 mmol), [P_{12,4,4,4}]Br (1.2 mmol), MIL-53(Cr) (15 mg), CO₂ (1.0 MPa), were stirred at 100 °C

^bIsolated conversion

^cIsolated yield

1H). Anal. Calcd. for C₅H₈O₄: C, 45.42; H, 6.05; O, 48.42. Found: C, 45.46; H, 6.10; O, 48.44.

4-(Chloromethyl)-1,3-dioxolan-2-one (Table 1, entry 4): ¹H NMR: δ = 3.76 (dd, *J* = 6.8 Hz, CH₂, 2H), 4.35 (dd, *J* = 7.0 Hz, CH₂, 1H), 4.63 (dd, *J* = 7.0 Hz, CH₂, 1H), 4.91 (m, CH₂, 1H). Anal. Calcd. for C₄H₅ClO₃: C, 35.15; H, 3.63; Cl, 25.95; O, 35.13. Found: C, 35.19; H, 3.69; Cl, 25.97; O, 35.15.

4-(Trifluoromethyl)-1,3-dioxolan-2-one (Table 1, entry 5): ¹H NMR: δ = 4.06–4.15 (dd, *J* = 7.4 Hz, CH₂, 2H), 5.09 (t, *J* = 6.9 Hz, CH, 1H). Anal. Calcd. for C₄H₃F₃O₃: C, 30.76; H, 1.90; F, 36.48; O, 30.74. Found: C, 30.78; H, 1.94; F, 36.52; O, 30.76.

4-Phenyl-1,3-dioxolan-2-one (Table 1, entry 6): ¹H NMR: δ = 4.36 (t, *J* = 8.2 Hz, CH₂, 1H), 4.75 (t, *J* = 8.2 Hz, CH₂, 1H), 5.66 (t, *J* = 8.0 Hz, CH₂, 1H), 7.29–7.46 (m, Ar–H, 5H). Anal. Calcd. for C₉H₈O₃: C, 65.82; H, 4.89; O, 29.21. Found: C, 65.85; H, 4.91; O, 29.24.

Results and discussion

Initial experiments were using the cycloaddition of CO₂ and propylene oxide to screen of catalysts. The catalytic activities of different ionic liquids, such as

tetrabutylphosphonium bromide ([P_{4,4,4,4}]Br), tetrabutylphosphonium bis(trifluoromethyl)sulfonylimide ([P_{4,4,4,4}]NTf₂), tetrabutylphosphonium tetrafluoroborate ([P_{4,4,4,4}]BF₄), tetrabutylphosphonium hexafluorophosphate ([P_{4,4,4,4}]PF₆), tetrabutylphosphonium chloride ([P_{4,4,4,4}]Cl), tributyldecylphosphonium bromide ([P_{8,4,4,4}]Br), tributyldecylphosphonium bromide ([P_{12,4,4,4}]Br), tetrabutylammonium bromide ([*n*-Bu₄N]Br), 1-butyl-1-methylpyrrolidinium bromide ([P_{1,4}]Br), were tested with MIL-53(Cr) as cocatalyst in the reaction (Table 2, entries 1–9). The results demonstrated that the types of ionic liquids had great effects on the catalytic activity. Results showed that [P_{12,4,4,4}]Br exhibited the highest reactivity (Table 2, entry 7). Besides MIL-53(Cr), the effects of other metal–organic frameworks cocatalysts including MIL-53(Fe), MIL-101(Cr), ZIF-67 (ZIF: zeolitic imidazolate framework), ZIF-7, ZIF-8 and MOF-5 were studied (Table 2, entries 15–20). The results showed MIL-53(Cr) and MIL-101(Cr) present more catalytic activity than MIL-53(Fe), ZIF-67, ZIF-7, ZIF-8 and MOF-5, and the activity of MIL-53(Cr) is slightly higher than that of MIL-101(Cr). The results indicated that the highly active chromium sites of metal–organic frameworks are crucial for the reaction, possibly facilitating the activation of epoxide and CO₂. For more investigation, a decrease in the catalytic activity was observed when common MIL-53(Cr) or

Table 2 Catalyst effect in the cycloaddition of CO₂ to propylene oxide

Entry ^a	Ionic liquid	Cocatalyst	Time (h)	Conversion (%) ^b	Yield (%) ^c
1	[P _{4,4,4,4}]Br	MIL-53(Cr)	3	91	89
2	[P _{4,4,4,4}]NTf ₂	MIL-53(Cr)	6	75	69
3	[P _{4,4,4,4}]BF ₄	MIL-53(Cr)	6	62	57
4	[P _{4,4,4,4}]PF ₆	MIL-53(Cr)	6	67	63
5	[P _{4,4,4,4}]Cl	MIL-53(Cr)	4	80	75
6	[P _{8,4,4,4}]Br	MIL-53(Cr)	2	95	93
7	[P _{12,4,4,4}]Br	MIL-53(Cr)	2	99	98
8	[<i>n</i> -Bu ₄ N]Br	MIL-53(Cr)	3	85	80
9	[P _{1,4}]Br	MIL-53(Cr)	3	82	77
10	–	MIL-53(Cr)	6	55	51
11	[P _{12,4,4,4}]Br	–	6	83	82
12	[P _{12,4,4,4}]Br	MIL-53(Cr)	2	98	97 ^d
13	[P _{12,4,4,4}]Br	MIL-53(Cr)	2	98	97 ^e
14	[P _{12,4,4,4}]Br	MIL-53(Cr)	2	96	95 ^f
15	[P _{12,4,4,4}]Br	MIL-53(Fe)	2	90	87
16	[P _{12,4,4,4}]Br	MIL-101(Cr)	2	94	92
17	[P _{12,4,4,4}]Br	ZIF-67	3	89	86
18	[P _{12,4,4,4}]Br	ZIF-7	3	85	83
19	[P _{12,4,4,4}]Br	ZIF-8	3	88	85
20	[P _{12,4,4,4}]Br	MOF-5	3	87	86

^aThe reactions were carried out with propylene oxide (20 mmol), ionic liquid (1.2 mmol), cocatalyst (15 mg) and CO₂ (1.0 MPa) at 100 °C

^bIsolated conversion

^cIsolated yield

^dThe first run

^eThe second run

^fThe third run

[P_{12,4,4,4}]Br as the catalyst was used (Table 2, entries 10 and 11). The results mean that ionic liquid or metal–organic framework alone does not work effectively in the reaction, and [P_{12,4,4,4}]Br/MIL-53(Cr) was the most suitable catalytic system for the cycloaddition. The active sites of this catalytic system were sufficient for the reaction, which may be attributed to the synergistic effects of MIL-53(Cr) active site and the basic sites of ionic liquid. Furthermore, the catalytic system [P_{12,4,4,4}]Br/MIL-53(Cr) could be typically recovered and reused with no obvious decrease in catalytic activity (Table 2, entries 12–14). The TGA spectra confirmed the good thermal stability up to 500 °C of MIL-53(Cr) (Fig. S5, ESI) and 200 °C of [P_{12,4,4,4}]Br (Fig. S8, ESI), providing beneficial information for the reusability of the catalytic system. The morphology of cocatalyst displayed obviously unchangeable after recycling has been confirmed by SEM image (Fig. S3 h, ESI). FT-IR and XRD analysis of the reused cocatalyst after three runs was very similar to that of

the fresh catalyst, indicating that no obvious change in the characteristic structure of the catalyst happened exhibits during the reaction (Fig. S6 and S7, ESI). Moreover, elemental analysis of the reused catalytic system illustrated that the content of active species in [P_{12,4,4,4}]Br and MIL-53(Cr) did not change obviously (Tables S1 and S2, ESI). On the basis of these results, we concluded that [P_{12,4,4,4}]Br/MIL-53(Cr) shows excellent stability and reusability during the reaction.

The reaction parameters such as reaction temperature, CO₂ pressure and reaction time have significant effects on the cycloaddition (Fig. 1). It can be seen that an increase in reaction temperature up to 100 °C led to a remarkable increase of the propylene oxide conversion (~99%) and yield of 4-methyl-1,3-dioxolan-2-one (~98%). However, when the reaction temperature is further increased to 120 °C, the product yield will decline to 93% (Fig. 1b). During the catalytic process at overly high temperatures, a small amount of by-products of acetone and propylene glycol were formed, which were detected by GC analysis, mostly due to the side reactions including the propylene oxide isomerization and hydrolysis of propylene oxide. Effect of CO₂ pressure on the cycloaddition was studied, and the results are shown in Fig. 1c. It was found that propylene oxide conversion and product yield could be enhanced when the CO₂ pressure increases from 0.5 to 1.0 MPa, with 57% increase in conversion and 55% increase in yield being probed. The increased pressure can enhance the concentration of CO₂ and the interaction between propylene oxide and CO₂, which favors the cyclic carbonate formation (Alves et al. 2015). However, the yield and conversion were obviously decreased with further increasing CO₂ pressure beyond 1.0 MPa. Increasing the pressure to 2.0 MPa exhibited a severely negative effect on the cycloaddition, and only 71% yield and 74% conversion were obtained. A possible explanation was that the exceedingly high CO₂ pressure may block the interaction between propylene epoxide and the catalyst, and would reduce the concentration of propylene epoxide in the bottom catalyst phase. More propylene epoxide was extracted into CO₂ phase leading to the decreased conversion and yield. The effect of the reaction time (Fig. 1d) on the cycloaddition was also investigated; the propylene oxide conversion and product yield increased when the reaction duration was extended from 1.0 to 2.0 h, with 27% increase in conversion and 26% increase in yield being probed. Further increases in reaction time did not significantly improve the conversion and yield.

To survey the efficiency and generality of the catalytic system [P_{12,4,4,4}]Br/MIL-53(Cr), the cycloaddition of CO₂ to different terminal epoxides was examined, and the results are presented in Table 1. All terminal epoxides including electron-deficient and electron-rich groups were smoothly and successfully converted and gave their corresponding cyclic carbonates with excellent yields and selectivities (Table 1, entries 1–6). It is worth noting that this novel catalytic

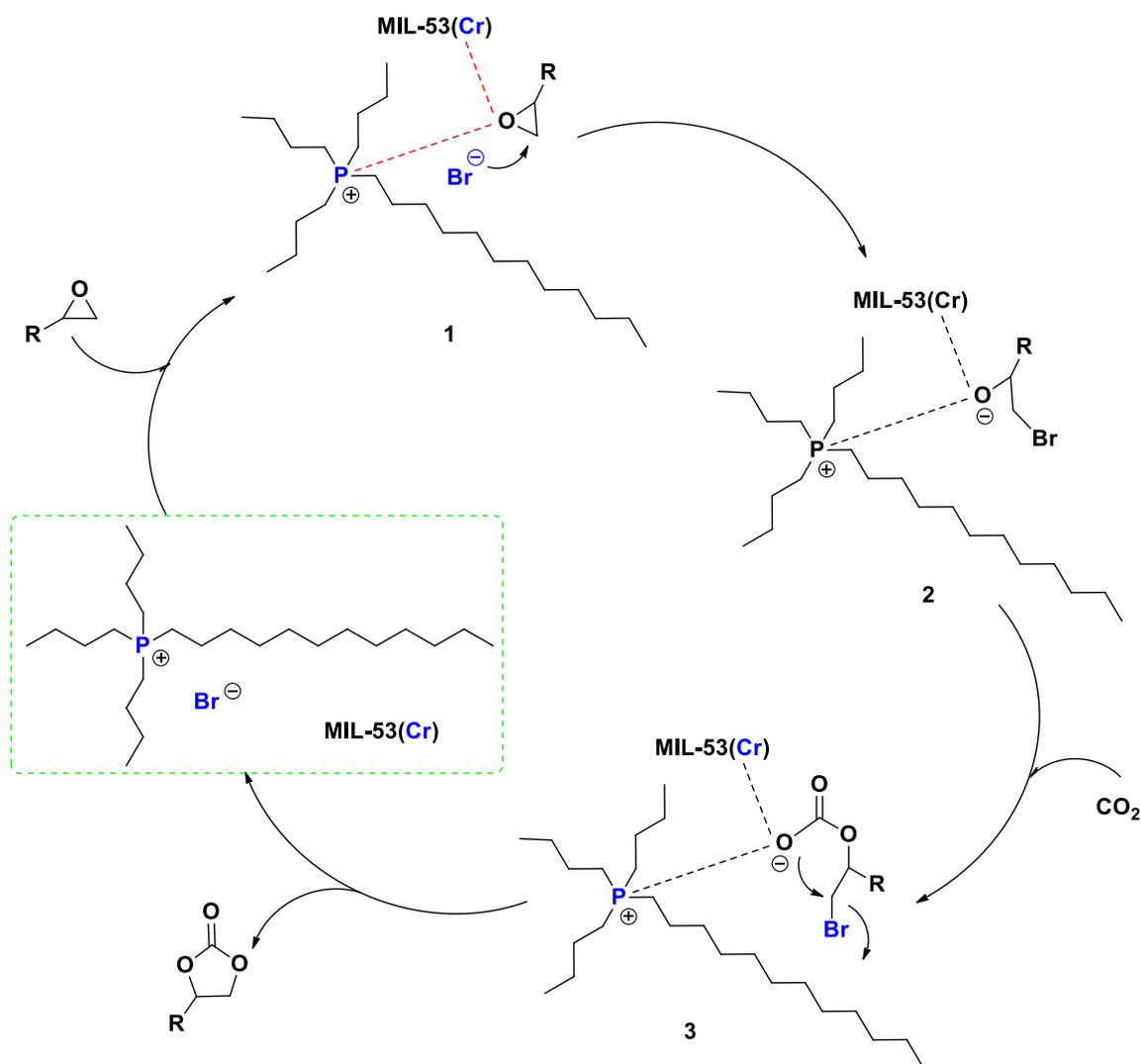


Fig. 2 Possible mechanism for cycloaddition of CO₂ to epoxides

system could tolerate a broad range of groups. However, epoxides with electron-withdrawing groups decreased the reaction rate, and slightly longer reaction times were needed to obtain excellent yields (Table 1, entries 4–6).

On the basis of the above results and previously reported works (Montoya et al. 2016; Arayachukiat et al. 2017; Seo and Chung 2014), a possible mechanism for the cycloaddition is proposed in Fig. 2. Epoxide is firstly activated by the cooperative catalytic system [P_{12,4,4,4}]Br/MIL-53(Cr) to form intermediate 1 through the coordination of MIL-53(Cr) and the cationic site of ionic liquid (P) with O atom, followed by nucleophilic attack of the anionic site of ionic liquid (Br) on the less sterically hindered carbon atom of epoxide to form intermediate 2. Then, the interaction occurred between the intermediate 2 and CO₂ to afford intermediate 3 undergoes the nucleophilic attack and coordination. Finally, the cyclic carbonate was generated through an intramolecular

substitution cyclic step, together with liberation of the [P_{12,4,4,4}]Br/MIL-53(Cr) cooperative catalytic system.

Conclusion

In summary, we have developed a new and highly efficient multifunctional catalytic system with applications to the cycloaddition CO₂ to different epoxides under mild and solvent-free reaction conditions. The catalytic tests revealed that the dual catalytic system of [P_{12,4,4,4}]Br coupled with MIL-53(Cr) displayed the best catalytic property due to the synergetic effects involving basic sites phosphonium cation and bromide anion of ionic liquid as well as the active site chromium of MIL-53(Cr). Compared with the previous catalytic systems, the present catalytic system has several attractive features such as simple operation, good to

excellent yields, high catalytic activity, low loading of catalyst, environmentally benign and safe. This study provides a new insight into design of sustainable and efficient catalytic systems via the combination of metal–organic frameworks and ionic liquids for chemical carbon dioxide fixation.

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