

Deletion of genes involved in glutamate metabolism to improve poly- γ -glutamic acid production in *B. amyloliquefaciens* LL3

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Abstract Here, we attempted to elevate poly- γ -glutamic acid (γ -PGA) production by modifying genes involved in glutamate metabolism in *Bacillus amyloliquefaciens* LL3. Products of *rocR*, *rocG* and *gudB* facilitate the conversion from glutamate to 2-oxoglutarate in *Bacillus subtilis*. The gene *odhA* is responsible for the synthesis of a component of the 2-oxoglutarate dehydrogenase complex that catalyzes the oxidative decarboxylation of 2-oxoglutarate to succinyl coenzyme A. In-frame deletions of these four genes were performed. In shake flask experiments the *gudB/rocG* double mutant presented enhanced production of γ -PGA, a 38 % increase compared with wild type. When fermented in a 5-L fermenter with pH control, the γ -PGA yield of the *rocR* mutant was increased to 5.83 g/L from 4.55 g/L for shake flask experiments. The *gudB/rocG* double mutant produced 5.68 g/L γ -PGA compared with that of 4.03 g/L for the wild type, a 40 % increase. Those results indicated the possibility of improving γ -PGA production

by modifying glutamate metabolism, and identified potential genetic targets to improve γ -PGA production.

Keywords Gamma-PGA · Glutamate metabolism · *B. amyloliquefaciens* · Markerless gene replacement

Introduction

Poly- γ -glutamic acid (γ -PGA) is a naturally occurring polymer that has attracted extensive investigations due to its outstanding qualities, such as water solubility, biocompatibility and degradability [19]. Composed of L- and D-glutamic acids linked by γ -amide linkages, γ -PGA has a wide range of applications ranging from hydrogels, flocculants, drug delivery, cosmetics to feed additives [2–4, 17, 22]. Regardless of its valuable characteristics, the practical use of γ -PGA is hindered mostly by its high cost compared with conventional materials in current use. Improving microbial γ -PGA production, especially using molecular biology techniques, is thus an important goal in both scientific and industrial fields. However, only very limited information is available regarding the genetic elements that can be targeted to improve existing γ -PGA producers. To the best of our knowledge, those elements include a gene responsible for the synthesis of exopolysaccharides, genes encoding γ -PGA degradation enzymes and the *vgb* gene coding for hemoglobin [12, 15, 18, 21].

We previously reported that the deletion of *RocR*, a transcriptional regulator in glutamate metabolism, may have contributed to the increase of γ -PGA production in *Bacillus amyloliquefaciens* LL3 [24]. Wu et al. [23] also reported that by directing more carbon flux distribution toward glutamate synthesis by the presence of additives, γ -PGA production was increased. Those results suggested that elevating intracellular glutamate concentration may be an approach to improve

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γ -PGA production. Moreover, *B. amyloliquefaciens* LL3 is a glutamic acid-independent γ -PGA-producing strain, which suggests that intracellular glutamate is the only substrate for γ -PGA synthesis in this bacterium [5]. Therefore, it is tempting to speculate that elevated intracellular glutamate concentration facilitates γ -PGA production of LL3 more effectively than in glutamic acid-dependent γ -PGA-producing strains.

Besides *rocR*, there are several other genes known to participate in glutamate metabolism in *Bacillus*, which are summarized in Fig. 1 and Table 1. The gene *rocG* encodes the glutamate dehydrogenase (GDH) in *B. subtilis*, which is devoted to glutamate degradation rather than its synthesis [7]. The expression of *rocG* is controlled by the transcriptional activator RocR. RocG has another role as a regulator that inhibits GltC, which activates the *gltAB* operon encoding the glutamate synthase [10]. In *B. subtilis*, *gudB* is a second, cryptic glutamate dehydrogenase gene harboring an insertion of three amino acids with respect to the common ancestral GDH sequence [14]. In *B. amyloliquefaciens* LL3, however, the insertion does not exist (data not shown), suggesting its potential role in glutamate degradation together with RocG. The genes *odhA*, *odhB* and *pdhD* encode the 2-oxoglutarate dehydrogenase complex (ODHC) catalyzing the oxidative decarboxylation of 2-oxoglutarate to succinyl

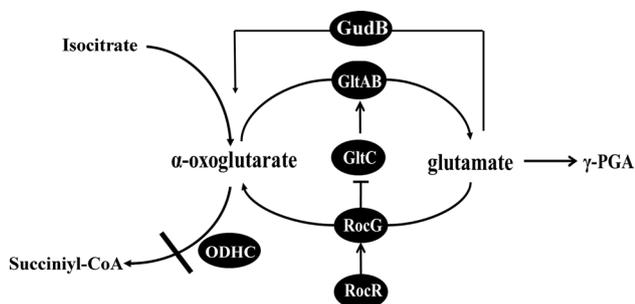


Fig. 1 Postulated glutamate metabolism in *B. amyloliquefaciens* LL3 based on reports in *B. subtilis* 168. GudB and RocG are glutamate dehydrogenases. *rocG* is positively regulated by RocR. Alpha-oxoglutarate dehydrogenase complex (ODHC) mediates the conversion from 2-oxoglutarate to succinyl coenzyme A

coenzyme A (succinyl-CoA) in *B. subtilis* [6]. By reducing the flux from 2-oxoglutarate to succinyl-CoA, the flux from 2-oxoglutarate to glutamate may be enhanced.

The functions of the four genes (*rocR*, *rocG*, *gudB* and *odhA*) and their interactions led us to hypothesize that their deletions may elevate intracellular glutamate concentration, which facilitates γ -PGA production. With these expectations, we performed in-frame deletions of these four genes in *B. amyloliquefaciens* LL3 and examined the effects of their deletions on cell growth and γ -PGA production. By doing this we hope to identify more genetic targets for improvement of γ -PGA production.

Materials and methods

Strains and growth conditions

Strains used in this study are listed in Table 2. *E. coli* DH5 α was used for plasmid construction and *E. coli* GM2163 was used to prepare the unmethylated plasmids. *E. coli* strains were grown in LB medium at 37 °C with aeration. The *B. amyloliquefaciens* LL3 strain is deposited in the China center for type culture collection (CCTCC) with accession number CCTCC M 208109 [9]. *B. amyloliquefaciens* strains were grown at 37 °C (except during gene deletion procedure) in LB or fermentation medium, which contains sucrose 50 g/L, (NH₄)₂SO₄ 2 g/L, MgSO₄ 0.6 g/L, KH₂PO₄ 6 g/L, K₂HPO₄ 14 g/L, and 2 mL mineral elements including 1 mM FeSO₄·4H₂O, CaCl₂·2H₂O, MnSO₄·4H₂O and ZnCl₂ (pH 7.2). When required, media were supplemented with ampicillin (Ap 100 μ g/mL) and chloramphenicol (Cm 5 μ g/mL). Stock solutions (75 mg/mL) of 5-fluorouracil (5-FU) were prepared in DMSO and added into the media at a final concentration of 1.3 mM.

Plasmid construction

Primers used in this study are listed in Table 3. Homology arms for gene deletion were obtained using overlapping

Table 1 Genes selected for this study

Gene	Products	Amino acid identity ^a (%)	aa ^b retained after deletion
<i>rocR</i>	Transcriptional regulator (NtrC/NifA family)	85	N ^c :23, C ^d :7
<i>rocG</i>	NAD-specific glutamate dehydrogenase	92	N:14, C:21
<i>gudB</i>	Cryptic glutamate dehydrogenase	94	N:9, C:8
<i>odhA</i>	2-Oxoglutarate dehydrogenase E1	93	N:27, C:180

^a Comparison with its orthologous protein from *B. subtilis* 168

^b Amino acid residues

^c Amino acid residues retained at the N terminus of the protein in the mutant strain

^d Amino acid residues retained at the C terminus of the protein

Table 2 Strains used in this study

Strains	Description	Source
<i>B. amyloliquefaciens</i>		
LL3	Glutamic acid-independent poly- γ -glutamic acid (γ -PGA) producing strain	[9]
LL3 Δ U	LL3 carrying an in-frame deletion in the <i>upp</i> gene	[24]
LL3 Δ UR	LL3 Δ U carrying an in-frame deletion in the <i>rocR</i> gene	[24]
LL3 Δ UR-C	LL3 Δ UR complemented with the <i>rocR</i> gene inserted in the genome	This study
LL3 Δ UG	LL3 Δ U carrying an in-frame deletion in the <i>rocG</i> gene	This study
LL3 Δ UB	LL3 Δ U carrying an in-frame deletion in the <i>gudB</i> gene	This study
LL3 Δ UB-C	LL3 Δ UB complemented with the <i>gudB</i> gene inserted in the genome	This study
LL3 Δ UA	LL3 Δ U carrying an in-frame deletion in the <i>odhA</i> gene	This study
LL3 Δ UA-C	LL3 Δ UA complemented with the <i>odhA</i> gene inserted in the genome	This study
LL3 Δ UBG	LL3 Δ UB carrying an in-frame deletion in the <i>rocG</i> gene	This study
LL3 Δ UGB	LL3 Δ UG carrying an in-frame deletion in the <i>gudB</i> gene	This study
<i>E. coli</i> strains		
DH5a	<i>supE44 lacU169</i> (Δ 80 <i>lacZ</i> Δ M15) <i>recA1 endA1 hsdR17</i> (r_{m}^+) <i>thi-1 gyrA relA1 F-Δ(lacZYA-argF)</i>	TransGen
GM2163	F- <i>dam-13::Tn9</i> (Cam ^r) <i>dcm-6 hsdR2</i> (r_{m}^+) <i>leuB6 hisG4 thi-1 araC14 lacY1 galK2 galT22 xylA5 mtl-1 rpsL136</i> (Str ^r) <i>fhuA31 tsx-78 glnV44 mcrA mcrB1</i>	Fermentas

PCR and are 500–800 bp in length. A mutant allele of our target gene was obtained by overlapping PCR and then ligated to pKSV7-based counterselection plasmid pKSU. Using *odhA* deletion as an example, primers OdhAUP-F/OdhAUP-R and OdhADN-F/OdhADN-R were used to amplify the up- and down-stream homology arms. The two fragments were spliced in a subsequent PCR using primer pair OdhAUP-F/OdhADN-R. The resulting homology arms carried an in-frame deletion of the *odhA* gene and were ligated to pKSU. DNA polymerases, digestion enzymes and T4 DNA ligase were purchased from Takara (Dalian, China). PCR, enzymatic digestion and ligation reactions were performed as recommended by the enzymes suppliers. DNA fragments were analyzed on 0.8 % agarose gels and purified using an Axygen gel DNA recovery kit (Axygen, CA, USA).

Bacterial transformation

Competent *E. coli* cells were purchased from TransGen Biotech (TransGen, Beijing, China) and were transformed according to the manufacturer's instructions. *B. amyloliquefaciens* LL3 and its derivatives were transformed using the high-osmolarity electroporation method as described previously [24].

Construction of recombinant strains

A *upp*-based markerless gene replacement method was used to perform in-frame deletion of the target genes [24].

LL3 Δ U carrying an in-frame deletion of the gene coding for the uracil phosphoribosyltransferase was used as the starting strain. Using *odhA* deletion as an example, deletion plasmid pKSU- Δ OdhA was transformed in LL3 Δ U through electroporation. After plasmid integration/excision, double-crossover recombinants were selected with the aid of 1.3 mM 5-fluorouracil (5-FU) using the primer pair OdhAOUT-F/OdhAOUT-R. Primer nomenclatures for other gene deletions are similar. Mutant strains were verified using PCR and DNA sequencing. One correct colony carrying an in-frame deletion of *odhA* was designated LL3 Δ UA. Similarly, mutants carrying deletions for *rocR*, *rocG* and *gudB* were designated LL3 Δ UR, LL3 Δ UG and LL3 Δ UB, respectively. The amino acid residues retained in the mutants are shown in Table 1.

Fermentation in shake flasks and 5-L fermenters

For shake flask experiments, *B. amyloliquefaciens* LL3 Δ U and its derivatives were first grown overnight in test tubes containing LB liquid medium, and then inoculated into 100 mL fresh fermentation medium in 500-mL shake flasks at an optical density at 600 nm (OD₆₀₀) of approximately 0.05–0.1. The shake flasks were then grown at 37 °C for 48 h with an agitation speed of 200 rpm. Experiments were independently repeated at least three times and means and standard deviations were calculated. For fermentation in a 5-L jar fermenter (Bailun, Shanghai, China), cultures from the shake flasks grown overnight were used as seed cultures and diluted 10-fold into 3 L fresh fermentation medium.

Table 3 Plasmids and primers used in this study

Plasmids	Description	Source
pKSV7	<i>E. coli</i> - <i>Bacillus</i> shuttle vector, colE1, pE194ts, Ap ^r , Cm ^r	[20]
pKSU	pKSV7 derivative, carrying an ectopic copy of <i>upp</i> gene from <i>B. subtilis</i> 168	[24]
pKSU-ΔRocG	pKSU derivative, carrying homology arms for the deletion of the <i>rocG</i> gene	This study
pKSU-ΔGudB	pKSU derivative, used for the deletion of the <i>gudB</i> gene	This study
pKSU-ΔOdhA	pKSU carrying a mutant copy of the <i>odhA</i> gene	This study
pKSU-rocR	Complementing plasmid for the <i>rocR</i> mutant	This study
pKSU-gudB	Complementing plasmid for the <i>gudB</i> mutant	This study
pKSU-odhA	Complementing plasmid for the <i>odhA</i> mutant	This study
Primer names	Sequence (5'–3') ^a	
RocGUP-F	ATCTGGATCCGACGATTCCCACACCAAG	
RocGUP-R	GAGGTGATAAAACGTGTTATCCGCAAAGGAATTTTG	
RocGDN-F	TTTGGGATAACACGTTTTATCACCTCATCGT	
RocGDN-R	GCGAGTGCCTGGGTAAGGTGGTAGATTATTC	
RocGOUT-F	TTTTCTTCATCTTTCTGATTGC	
RocGOUT-R	GATTTTCAGCTGATGTGAACC	
GudBUP-F	GTAGGATCCAAGCTCTTCACCCGGTATG	
GudBUP-R	ATCGATTCACCGGTGCTTCGCGCTTCAGAGGC	
GudBDN-F	TGAAGCGGAAGCACCGGTGAATCGATCGGCT	
GudBDN-R	ACAGTGCACGCAGAAGACGACGAATATGAC	
GudBOUT-F	TTCCCGCCGATTACGGCAAC	
GudBOUT-R	TTTGAAGCGAATGGTCCGATC	
OdhAUP-F	ACTTGGATCCTTAGTTTTTGGCGAGTCAAGC	
OdhAUP-R	AAGATTTTACGGAAGAAGACAAGCGAAAATGCTG	
OdhADN-F	TTCGCTTGCTTCTTCCGTAAAAATGTTCCCAATTC	
OdhADN-R	TCGAGTGCACGACGGATATGCCATCAGAC	
OdhAOUT-F	GATTGATTCTGCTAATTCAGTACC	
OdhAOUT-R	TACCGTGATCCGTTTGAAGAG	

^a Restriction sites for plasmid construction are indicated in bold

Fermentation was continued at 37 °C for 48 h with an agitation speed of 400 rpm. The pH was kept at 7.0 via automatic addition of 1 M NaOH. After 24 h, 50 mL fermentation broth was withdrawn every 6 h and centrifuged at 8,000g (4 °C) for 20 min. The cell pellet was washed three times with dH₂O then dried and weighed to determine dry cell weight (DCW). Fourfold volume of cold anhydrous ethanol was added to the supernatant followed by incubation at 4 °C overnight. The precipitate was centrifuged at 4,000×g (4 °C) and then dialyzed against distilled water and lyophilized to obtain γ-PGA. [24].

Quantitative RT-PCR analysis

Bacillus amyloliquefaciens strains were grown to mid-log phase (approximately 20 h) in fermentation medium in shake flasks as described above. Cells were collected at 4 °C and the RNA was isolated using TransZol™ Up (TransGen, Beijing, China) according to the manufacturer's instructions. cDNA was reverse transcribed using a GoS-cript™ reverse transcription system (Promega, Wisconsin,

USA). Real-time PCR analysis for the target genes was performed using the SYBR Premix Ex Taq™ II (Takara, Dalian, China). Transcription levels of the target gene were normalized against the levels of *rspU* [8].

Preparation of cell-free *B. amyloliquefaciens* extracts and measurement of GDH and OGDH activity

Cultures (100 mL) grown under γ-PGA production conditions in shake flasks for 36 h were collected and washed four times with potassium phosphate buffer (50 mM, pH 7.5), and resuspended in 5 ml of the same buffer and disrupted by sonication for 15 min (500 W) on ice. The cell debris was removed by centrifugation at 4 °C for 10 min at 8,000g. Measurement of GDH and OGDH activities was performed as described by Krog et al. [11] with slight modifications. Briefly, the GDH assay mixture generally contained 100 mM glycine-KOH (pH 7.5), 200 mM L-glutamate, 10 mM MgSO₄, and 0.2 mM NAD⁺; the OGDH assay mixture generally contained 50 mM Tris-HCl (pH 7.5), 0.25 mM NAD⁺, 50 mM 2-oxoglutarate,

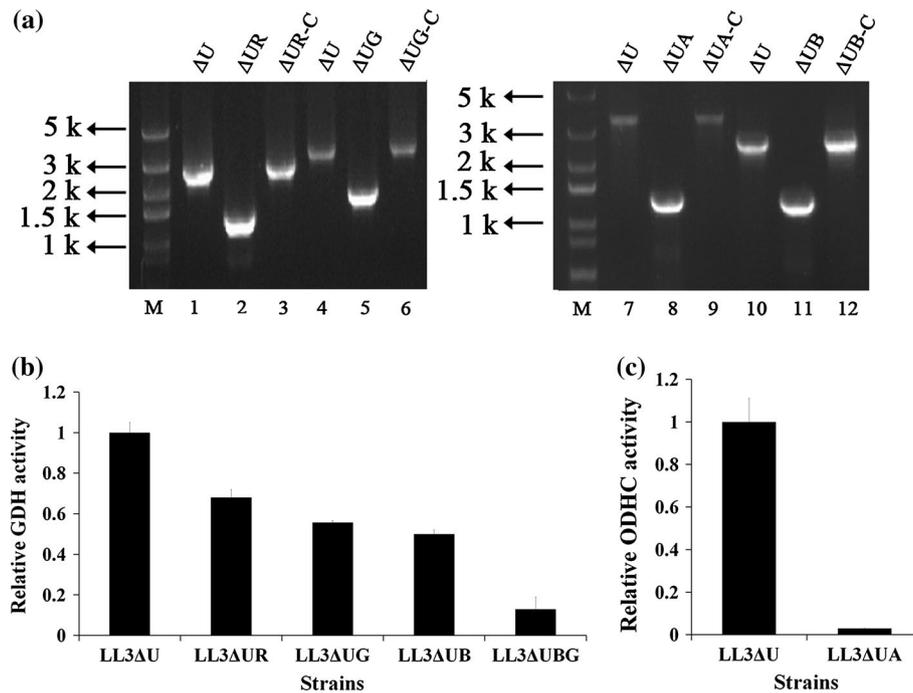


Fig. 2 Confirmation of the deletion-carrying mutants by PCR and phenotypes. **a** Chromosome structures of deletion-carrying strains were analyzed by agarose gel electrophoresis of PCR products generated with primers RocROUT-F/RocROUT-R (lanes 1–3); with primers RocGOUT-F/RocGOUT-R (lanes 4–6); with primers OdhAOUT-F/OdhAOUT-R (7–9); with primers GudBOUT-F/GudBOUT-R (lanes 10–12). M DNA marker, and the size of each band is reported on the left. Primer nomenclature is as in Table 2. The genotypes of strains are indicated on the top of each lane. Mutant strains carry-

ing correct deletions would yield PCR products shorter than that of the wild type. Complementation strains would yield PCR products identical to that of the wild type. **b** Relative glutamate dehydrogenase (GDH) activities of the mutant strains. GDH activities of the *rocR* (LL ΔUR), *rocG* (LL ΔUG) and *gudB* (LL ΔUB) mutants were determined and normalized against that of the wild type (LL ΔU), which was set as 1. Values are an average from technical triplicates. **c** Relative 2-oxoglutarate dehydrogenase (ODGH) activity of the *odhA* (LL ΔUA) mutant. Values are an average from technical triplicates

1 mM coenzymeA (CoA), 1 mM thiamine pyrophosphate, 3 mM L-cysteine-HCl, and 1 mM MgCl₂. The mixtures were prewarmed to 37 °C in quartz cuvettes. After the addition of 0.1 ml cell extract, yielding a total volume of 1 ml, the production of NADH was monitored at 340 nm for 4 min. One unit of enzyme activity was defined as the amount of enzyme needed to produce 1 μmol NADH per minute under the conditions described above. The background activity from the cell extract was measured by adding all components but glutamate or 2-oxoglutarate, and the background activity was subtracted from the total activity. The total protein concentration was determined with the Bio-Rad protein assay (Bio-Rad).

Results

Construction of recombinant strains carrying deletions for *rocR*, *rocG*, *gudB* or *odhA*

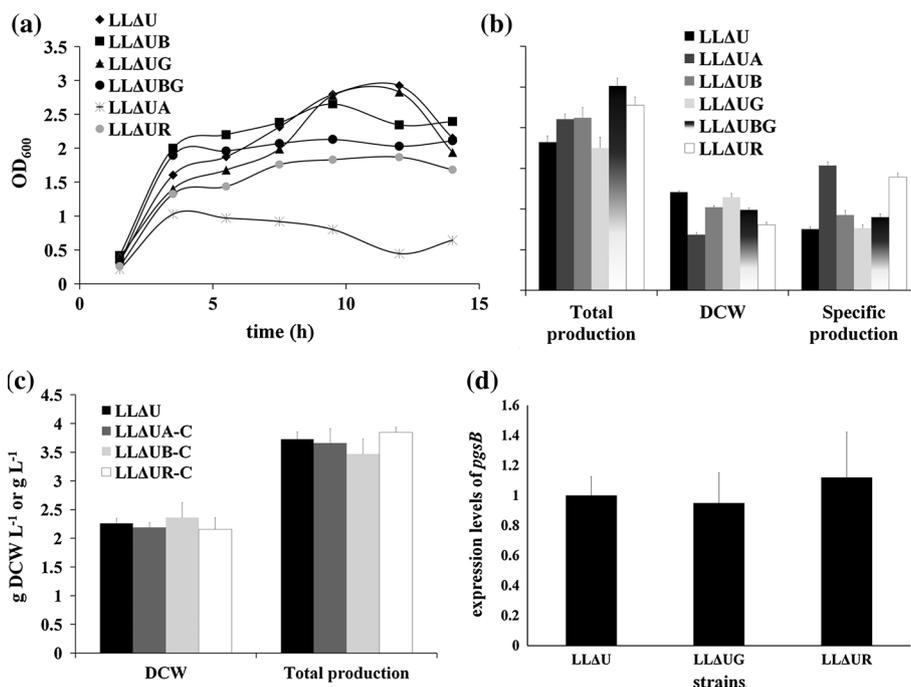
The *rocR* mutant was previously described, and the other three mutants were constructed as described in the

materials and methods section. For *rocG* and *gudB* deletion, approximately 50 % of the colonies subjected to PCR verification were shown to carry an in-frame deletion of the target genes (data not shown). For *odhA* deletion, however, only one mutant strain was identified among the 60 colonies that were subjected to PCR verification. The *rocG* gene was deleted in LL3 ΔUB to obtain the double-deletion carrying strain LL3 ΔUBG. LL3 ΔUGB was similarly constructed by deleting the *gudB* gene from LL3 ΔUG. The obtained mutants were streaked on LB agar and verified by PCR and DNA sequencing (Fig. 2a and data not shown).

Cell growth and γ-PGA production of the mutant strains in shake flasks

Growth profiles of the *rocG*, *gudB*, *odhA* and *rocG/gudB* (LL ΔUG, LL ΔUB, LL ΔUA and LL ΔUBG, respectively) mutants and the wild-type LL3ΔU were tested in LB medium as shown in Fig. 3a. The *odhA* mutant showed a severe growth defect, while others except the *rocR* mutant presented a growth pattern similar to the wild-type strain. The final dry cell weight (DCW) of the above mutants was

Fig. 3 Characterization of the mutant strains in shake flasks. **a** Growth profiles of the *rocG*, *gudB*, *odhA* mutants and the *rocG/gudB* double mutant (LL Δ UG, LL Δ UB, LL Δ UA and LL Δ UBG, respectively) in LB medium. Values were an average from biological duplicate set and standard deviations were essentially within 10 %. **b** cell growth and γ -PGA production of the mutants in fermentation medium at 48 h. **c** Growth and γ -PGA production of complementation strains for the *rocR*, *odhA* and *gudB* mutants (LL Δ UR, LL Δ UA and LL Δ UB, respectively) at 48 h. **d** Transcriptional levels of gene *pgsB* of the mutants (at 20 h). Values were an average from a biological triplicate set



also determined in fermentation medium at 48 h (Fig. 3b). Similar to that in LB medium, the *odhA* mutant showed the lowest DCW, while others showed a slight reduction compared with wild-type strain. The highest total γ -PGA production was found in LL3 Δ UBG which carries a double deletion for *gudB* and *rocG*, yielding 5.03 g/L γ -PGA compared with 3.64 g/L from the wild type (a 38.2 % increase). LL3 Δ UGB showed similar characteristics of growth and γ -PGA production with LL3 Δ UBG (data not shown), excluding the possibility of introduction of other mutations during strain construction. LL Δ UB showed a 15 % increase (4.245 g/L) in γ -PGA production, while LL Δ UG almost remained unchanged. Regardless of its deteriorated growth, the *odhA* mutant LL Δ UA produced 4.21 g/L γ -PGA, about 15 % more than the wild type. The specific production (the relative amount of γ -PGA per dry cell weight) for γ -PGA of the *odhA* mutant was 3.07 g/g DCW, presenting a 100 % increase compared with the wild type (1.5 g/g DCW), followed by the *rocR* mutant (2.79 g/g DCW, an 86 % increase). The data for the *rocR* mutant in shake flasks were reported previously and included here for comparison (Fig. 3a, b).

Considering the noticeable changes in cell growth and γ -PGA production in the *rocR*, *odhA* and *gudB* mutants, their complementation strains were constructed. Our previous studies showed that overexpression of *rocR* in *B. amyloliquefaciens* LL3 caused severe growth defect [25]. Therefore, all the complementation experiments in this study were carried out by inserting the gene with its own promoter and terminator in its original position in the genome. Using *rocR* as an example, a fragment obtained

by PCR with primer pair RocRUP-F/RocRDN-R using genomic DNA from LL Δ U as template was ligated to pKSU. The resulting complementation plasmid pKSU-RocR was used to transform LL3 Δ UR through electroporation. The *rocR* gene in pKSU-RocR was inserted in the genome of the *rocR* mutant strain by homologous recombination. Selection procedure for recombinant strains was similar to that of gene deletion as described previously. The resulting complementation strain for *rocR* was designated LL3 Δ UR-C. Complementation strains for *rocG*, *gudB* and *odhA* were similarly constructed. As shown in Fig. 3c, the phenotypes of the complementation strains resembled the wild-type strain in cell growth and γ -PGA production.

GDH and ODHC activities of the mutants

As a demonstration of roles of the target genes in glutamate metabolism, the GDH activities of the *rocR*, *rocG* and *gudB* mutants were determined and compared with the wild type. As shown in Fig. 2b, the *rocR* mutant (LL Δ UR) showed a 32 % decrease of GDH activity, and the *rocG* (LL Δ UG) and *gudB* (LL Δ UB) mutants showed ~50 % reduction. In the *odhA* (LL Δ UA) mutant, ODHC activity was very low, confirming the removal of the *odhA* gene (Fig. 2c).

Transcriptional levels of *pgsB* in the mutant strains

RocR and RocG are reported as transcriptional regulators. Therefore, we investigated whether transcription of *pgsB* (the first gene in the *pgsBCA* operon) was affected by the deletion of the *rocR* and *rocG* genes using qRT-PCR. As

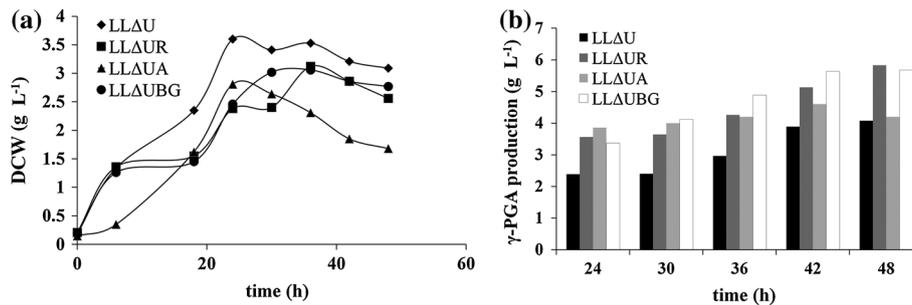


Fig. 4 Characterization of the mutant strains in fermenters. **a** DCW of the wild type, the *rocR*, *odhA* and *gudB/rocG* double mutants (LL ΔU, LL ΔUR, LL ΔUA and LL ΔUBG, respectively) at different

time points. **b** Absolute γ -PGA production of the mutants at different time points. All the values were means from a duplicate set, and standard deviations were essentially within 8 %

shown in Fig. 3d, no significant changes were observed in the mutant strains compared with the wild type at 20 h, which verified that the improved polymer production is not due to increased *pgs* operon transcription.

Further improvement of γ -PGA production using pH control strategy

Our previous report showed that the pH of the medium for the *rocR* mutant was lower than that of the wild type when fermented in shake flasks [24]; therefore, we performed fermentation of some of the mutants in fermenters with pH control. As shown in Fig. 4a, DCW of the *odhA* mutant (LL ΔUA) was obviously different from the other three mutants: it reached 2.81 g/L at 24 h, and dropped quickly thereafter, decreasing to 1.68 g/L at 48 h. The DCW of the wild-type strain showed a slight reduction after 24 h and was 3.09 g/L at 48 h. Compared with its growth in shake flasks, the *odhA* mutant showed obvious growth improvements in the fermenter, especially for the first 24 h. The final DCW at 48 h of the two culture conditions, however, showed no significant differences (1.37 g/L for shake flasks and 1.68 g/L for fermenters). Similar to results from shake flask experiments, the wild-type LL ΔU showed a slight advantage over the *rocR* (LL ΔUR) and *gudB/rocG* (LL ΔUBG) mutants in fermenters. DCW of LL ΔUR (2.56 g/L) and LL ΔUBG (2.77 g/L) in fermenters was improved compared with those in shake flask experiments (1.61 and 1.98 g/L, respectively).

The highest gamma-PGA production for *odhA* mutant (LL ΔUA) was obtained at 42 h, reaching 4.6 g/L, a slight improvement compared with that in shake flask experiments (4.21 g/L at 48 h), while the wild-type strain produced 4.08 g/L γ -PGA at 48 h in fermenters. The *gudB/rocG* (LL ΔUBG) mutant produced 5.68 g/L γ -PGA, a slight increase compared with that for shake flask experiments (5.06 g/L). The γ -PGA production of the *rocR* mutant (LL ΔUR) was increased by 28 % in the fermenter

compared with that in shake flask experiments (4.55 g/L), reaching 5.83 g/L, the highest among all the mutants tested (Fig. 4b).

Discussion

Gamma-PGA producers are usually divided into two groups according to their nutritional requirements: the glutamic acid-dependent bacteria and glutamic acid-independent bacteria. The former kind requires addition of L-glutamate in the medium to stimulate γ -PGA, and the latter does not. Wu et al. [23] reported that the addition of glycerol, Tween-80 and dimethyl sulfoxide (DMSO) increased the production of γ -PGA likely caused by depression of 2-oxoglutarate dehydrogenase and the enhancement of isocitrate dehydrogenase, which increased the flux from 2-oxoglutarate and isocitrate to glutamate, respectively. Enlightened by that, we attempted to enhance intracellular glutamate synthesis by genetically modifying related genes. Deletion of RocR (a regulator participating in glutamate degradation by activating the gene encoding glutamate dehydrogenase, *rocG*) was found to increase the flux from 2-oxoglutarate to glutamate, and then lead to increased synthesis of the other amino acids via transamination in *B. subtilis* 168 [13]. Besides *rocR*, *rocG*, *gudB* and *odhA* were also targeted in this study. We attempted to identify genes that might have a positive effect on γ -PGA production.

Unlike reports from *B. subtilis* 168 [14], the deletion of *rocG* (the gene encoding one of the glutamate dehydrogenase) in *B. amyloliquefaciens* LL3 seemed to confer no remarkable phenotype changes except the reduction of intracellular glutamate dehydrogenase (GDH) activity (Fig. 2b). In *B. subtilis*, RocG is the major glutamate dehydrogenase. The cryptic GudB (the second glutamate dehydrogenase) is only activated in the absence of RocG [10, 16]. In *B. amyloliquefaciens* LL3, however, the *gudB* gene lacks the insertion mutation found in *B. subtilis*. Therefore, GudB

may play an equally or more important role as that of RocG. The *gudB* mutant (LL Δ UB) presented a slightly higher γ -PGA production and lower DCW (Fig. 3b), although not significant. What is worth noting is that although the *rocR* mutant (LL Δ UR) showed a higher GDH activity than LL Δ UB and LL Δ UG, it produced more γ -PGA (both total and specific production) than those two mutants (Figs. 2b, 3b). Transcription of the *pgsBCA* operon was not affected by the absence of RocR, as shown by qRT-PCR analysis (Fig. 3d). There seemed to be no clear relationships between GDH activities and γ -PGA production. The *gudB/rocG* double mutant (LL Δ UBG) presented the highest γ -PGA production in shake flask experiments among all the mutant strains constructed, and showed no obvious growth defect both in LB and fermentation medium, thus qualifying as a promising producer for further investigations.

In *Corynebacterium glutamicum*, the deletion of *odhA* (encoding α -oxoglutarate dehydrogenase complex that mediates the conversion from 2-oxoglutarate to succinyl coenzyme A) greatly induced the production of L-glutamate [1]. *B. amyloliquefaciens* LL3 deleted for *odhA*, however, showed severe growth defect in LB medium. The ODH complex is part of the citric acid (TCA) cycle which provides reducing power and anabolic biomass precursors to the cell. The complex may be involved in substrate channeling through the TCA cycle. Although not essential both in LB and fermentation medium, the absence of the *odhA* gene did affect cell growth. This may partly account for the low deletion rate (1/60) during its deletion. The growth of the *odhA* mutant was partly restored in the fermentation medium and its γ -PGA production was even a little higher than the wild type (Fig. 4a, b). The latter phenomenon may be explained by the fact that ODH complex is not directly involved in the biosynthesis of intracellular glutamate, which is the direct unit for γ -PGA production.

Our previous report showed that in shake flask experiments without pH control, the pH of the medium for the *rocR* mutant was lower than that of the wild type and we suggested that the drop of pH may be more detrimental for the mutant [24]. The restoration of growth defect of LL Δ UA in fermentation medium with phosphate buffer also indicated that pH control may facilitate the growth of the mutants. Enzyme production of the *rocG* mutant of *B. subtilis* was enhanced by the NH_3 -pH auxostat approach [14]. We therefore perform fermentation of LL Δ UR, LL Δ UBG and LL Δ UA in a 5-L fermenter using NaOH to keep pH stable at 7.0–7.2, expecting to enhance their growth and further improve their γ -PGA production. Unfortunately, LL Δ UA showed no improvements in DCW or γ -PGA yield (Fig. 4a). Lower DCW and quicker cell decline may contribute to the low γ -PGA yield. The LL Δ UBG mutant showed a 1.39-fold increase in γ -PGA production compared with the wild type, almost the same from shake flask

experiments. A remarkable improvement was observed in LL Δ UR (Fig. 4b). Further optimization of fermentation parameters is needed to enhance the performance of the mutants, such as concentration of the nitrogen sources or pH maintenance using liquid ammonia.

Given the complicated nitrogen metabolism regulations in bacteria, modification of glutamate to improve cell growth and γ -PGA production needs tremendous work, and the number of genes selected for this study is in fact very limited. Enhancement of glutamate synthesis could also be achieved through introduction of certain genetic elements or replacement of regulatory elements (promoters for example) of genes responsible for glutamate synthesis, such as GltAB, and other regulators (GlnR for example) involved in nitrogen metabolism may also be targeted [7, 10], which will be our work in the future.

Conclusions

In summary, the present study attempted to uncover the effects of deletions of several genes involved in glutamate metabolism on γ -PGA production. Compared with the addition of additives in the fermentation medium, such as DMSO and glycerol, the engineered strains add no complexity or cost to fermentation process. The *rocR* mutants and the *gudB/rocG* double mutants showed great potential for industrial use. Our work identifies genes that can be targeted to improve γ -PGA production in *B. amyloliquefaciens* LL3, a strategy that may be also applicable in other γ -PGA producers to establish microbial cell factories with higher capacity.

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Conflict of interest The authors declare that they have no conflict of interest.

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