

# Life cycle assessment of the Spanish cement industry: implementation of environmental-friendly solutions

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**Abstract** This study tries to find out the hotspots of the Spanish cement sector in 2010 by the life cycle assessment (LCA) and evaluates some improvement scenarios where best available technologies and substitution measures are taken into consideration. The document presents an environmental LCA of the cement production using the 2011 International Reference Life Cycle Data System method recommended by the European Commission. Attending to the clinker production by stage, fossil fuel combustion is the most important source in terms of impacts. Besides, limestone's calcination is crucial attending to the climate change. Electricity consumption is also relevant both in human toxicity with cancer effects and freshwater eutrophication (FE). Accordingly, solutions deployed lead to reductions in different impact categories. Fossil fuel substitution scenario achieves to reduce 33 and 37 % photochemical ozone formation and acidification (A), while material substitution scenario leads to reduce 10–13 % each impact category. On the other hand, fossil fuel substitution scenario entails an increase of 10 % in FE. Considering the ideal case of applying all these improvements together, reductions go from 15 % in FE to 49 % in A, respectively. To face the problems derived from fossil fuel combustion, a fuel shift is needed to reach less contaminant options such as biomass and bio-waste. Material substitution is another good solution for the industry, but it requires

a change in the demand and further research to ensure the properties of cement. Authors recommend taking into consideration the collateral increase of the FE due to the phosphates increase coming from the alternative fuels combustion.

**Keywords** LCA · Cement · BAT · Fossil fuel substitution · Material substitution · ILCD method

## Introduction

Relevant life cycle assessment (LCA) studies are only available for a specific cement plant located in Spain (Cardim de Carvalho 2001; Josa et al. 2007; Masanet et al. 2012; Valderrama et al. 2012, 2013) but not for the Spanish cement industry as a whole. Besides, there is an increasing interest on both the environmental profile and the sustainability of the cement production. Several authors have been working on to reduce the emissions coming from cement production from a technological approach (Benhelal et al. 2013; Brown et al. 2014), while other authors have been discussing the environmental consequences of applying different solutions (Huntzinger and Eatmon 2009; Fiksel et al. 2011; Volkart et al. 2013) from a LCA approach.

This study gives a LCA using the Spanish cement industry as the assessment object. The work is also remarkable due to the fact that the Spanish industry is obliged to reduce greenhouse gases (GHG) and industrial emissions in order to abide by the European Directives 2001/81/EC, 2009/29/EC and 2010/75/EC.

The objective of the document is to carry out a LCA of the Spanish cement sector by identifying its hotspots and analysing the implementation of best available technologies

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**Table 1** Spanish grey cement production by type and cement types composition, in 2010

Cement type	Production (%)	Clinker (%)	BFS (%)	Pozzolana (%)	FA (%)	Limestone (%)
CEM I—Portland	25.4	97.5				
CEM II/A-M—Portland composite	10.8	84.0		0.3	5.4	9.2
CEM II/B-M—Portland composite	6.6	72.0		1.9	3.6	22.0
CEM II/A-L—Portland calcareous	13.4	87.0				13.0
CEM II/B-L—Portland calcareous	6.8	72.0				28.0
CEM II/A-V—Portland with fly ash	14.8	87.0			13.0	
CEM II/B-V—Portland with fly ash	3.0	72.0			28.0	
CEM II/A-S—Portland with BFS	4.4	91.0	9.0			
CEM II/A-P—Portland with pozzolana	5.2	87.0		13.0		
CEM II/B-P—Portland with pozzolana	1.1	72.0		28.0		
CEM III/A—Blastfurnace cement	3.3	64.0	36.0			
CEM III/B—Blastfurnace cement	0.5	34.0	66.0			
CEM IV/A—Pozzolanic cement	0.9	85.0		3.8	11.3	
CEM IV/B—Pozzolanic cement	2.4	66.0		8.5	25.5	
CEM V/A—Composite cement	0.9	52.0	27.8	10.0	10.0	
OTHER CEM (ESP VI, CAC, G)	0.4	40.0	20.0	20.0	20.0	

BFS = Blast Furnace Slag. FA = Fly Ashes. Pozzolana is a silica sand

(BAT) as well as some improvement scenarios where substitution measures are taken into consideration.

### Cement production

Cement is generally produced as a mixture of limestone, clay and sand, which provides the four key ingredients required: lime, silica, alumina and iron. By mixing these ingredients and exposing them to intense heat, the resulting chemical reactions convert the partially molten raw materials into pellets called clinker. After adding gypsum and other minerals, the mixture is ground to form cement, a fine grey powder (IEA 2009a).

The process of producing cement consists of three main stages: raw material preparation, clinker burning (pyro-processing) and cement preparation (IEA GHG 2008; EI-PPCB 2013).

Depending on the moisture content of the material, cement production routes may be classified into four types: dry, semi-dry, semi-wet and wet. Nowadays, BATs in cement production are based on dry processes. The dry process route requires less energy than the wet route so it is generally preferred (IEA GHG 2008).

### Spanish cement industry

In 2010, the production of cement was 3,310 Mt worldwide and 191 Mt in the European Union (EU-27) (CEMBUREAU 2011), from which 23.5 Mt was produced in Spain (OFICEMEN 2010a). Most of the cement was produced using dry production techniques. In 2010, there were 58

clinker kilns operating in Spain, from which 55 had dry-route kilns (OFICEMEN 2010a).

According to the European standard EN 197-1:2000, there are 27 types of cement classified into 5 groups (CEN/TC-51 2000). The most common is the Portland cement' (type-I), with a composition of 95–100 % clinker and up to 5 % gypsum. Portland cements entailed 91.5 % of the total grey cement production in Spain in 2010 (OFICEMEN 2010a). Cement produced in Spain in 2010 can be grouped in 16 types according to the standard. Several cement types, such as II/B-S, II/A-D, II/A-Q, II/B-Q, II/A-W, II/B-W, II/A-T, II/B-T, III/C and V/B, were not produced in Spain in 2010.

In line with the cement(s) disaggregation in Table 1, grey cement production meant 97.3 % of the total production in 2010, the rest being white cement (not analysed). Gypsum addition was 4.5 % each. Grey clinker and grey cement productions were 21.2 and 22.8 Mt in 2010, respectively (OFICEMEN 2010a).

Regarding atmospheric emissions, operative cement facilities reported 7 % of the total CO<sub>2</sub> Spanish emissions in 2010 (PRTR-ES 2010; MAGRAMA 2012). From that CO<sub>2</sub>, 63.06 % came from process (calcination) and 36.94 % from fuel combustion (OFICEMEN 2010a).

National inventory distinguishes between CO<sub>2</sub> coming from combustion (CO<sub>2c</sub>) and from process (CO<sub>2p</sub>). Besides, amounts of Table 2 are higher than those from Spanish Pollutant Release and Transfer Registry (PRTR-ES), since this inventory only gives account for emissions above certain limit, i.e. the CO<sub>2</sub> threshold is 100 kt/year per releasing point. In other words, the PRTR-ES registry only shows the largest emission sources. With respect to

**Table 2** Main atmospheric pollutants emitted by the Spanish cement industry in 2010 (MAGRAMA 2012)

CO <sub>2p</sub> (Mt)	CO <sub>2c</sub> (Mt)	CO (kt)	NO <sub>x</sub> (kt)	SO <sub>2</sub> (kt)	NMVOC (kt)	PM <sub>2.5</sub> (t)	PM <sub>10</sub> (t)
11.21	7.01	44.16	36.94	8.09	1.05	475	1068

CO<sub>2p</sub> refers to CO<sub>2</sub> from process (limestone’s calcination). CO<sub>2c</sub> refers to CO<sub>2</sub> from combustion. CO = carbon monoxide. NO<sub>x</sub> = nitrogen oxides. SO<sub>2</sub> = sulphur dioxide. NMVOC = non-methane organic volatile compounds. PM<sub>2.5</sub> = particulate matter <2.5 μm. PM<sub>10</sub> = particulate matter <10 μm

the Spanish total, CO<sub>2</sub> from cement industry means 6.4 % in 2010 (MAGRAMA 2012). Other pollutants also have significant contributions: NO<sub>x</sub>, 3.8 %; SO<sub>2</sub>, 1.7 %; CO, 2.5 % and VOC, 0.15 %.

**Methodology**

Life cycle assessment is a technique for addressing the environmental aspects and potential environmental impacts throughout a product’s life cycle from raw material acquisition through production, use, end-of-life treatment, recycling and final disposal. There are four phases in an LCA study (ISO 2006):

The *goal and scope*. The scope, including the system boundary and level of detail, of an LCA depends on the subject and the intended use of the study.

The *life cycle inventory* (LCI). It is a list of input/output data with regard to the system being studied.

The *life cycle impact assessment* (LCIA). The purpose of LCIA is to provide additional information to help assess a product system’s LCI results so as better understand their environmental significance.

The *life cycle interpretation*. The results of an LCI or an LCIA, or both, are summarized and discussed as a basis for conclusions and recommendations.

Life cycle assessment

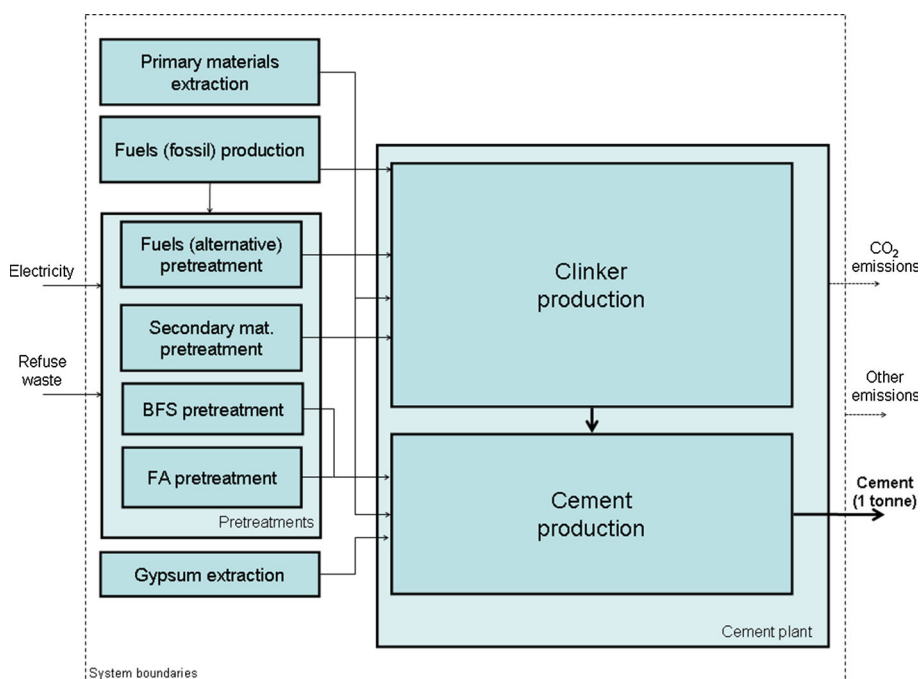
*Goal and scope*

The goal of this LCA is to analyse the Spanish cement production in 2010 in terms of environmental impacts and to examine the effect on the environment and human health of applying BAT according to EIPPCB (2013) and Moya et al. (2010).

This LCA is a cradle-to-gate analysis of the Spanish cement sector in 2010. It goes from the extractive processes to the cement production as shown in Fig. 1. The work is divided into two analyses:

- First, a technical approach by production phase using 1 t of clinker as functional unit. This assessment excludes cement production phase to avoid confusions in the second analysis. As clinker is the same for each cement type although there is not one cement type that represents

**Fig. 1** Scheme of the main processes in cement production for this LCA study. Notes (1) Electricity mix is excluded from the scheme. (2) BFS blast furnace slag, FA fly ashes



the entire production, it seemed reasonable to exclude the cement phase (mainly cement milling) from the first analysis. Besides, cement milling only enters an extra amount of electricity (around 1/3 of the electricity consumption in a cement plant) to the system.

- Second, an assessment of the Spanish cements industry as a whole using 1 t of cement as functional unit. This analysis is done in absolute midpoint units.

Both analyses are focused on several impact categories compiled by the recommendations for life cycle impact assessment from the International Reference Life Cycle Data System (ILCD) handbook (EC-JRC 2011). The emissions and resources derived from LCI are assigned to each of these impact categories. They are then converted into indicators by factors calculated by impact assessment models. These factors reflect pressures per unit emission or resource consumed in the context of each impact category. Emissions and resources consumed, as well as different product options, can then be cross-compared in terms of the indicators (EC-JRC 2011). Using the ILCD 2011 midpoint method, the following impact categories have been analysed: climate change (CC), human toxicity with cancer effects (HTce), photochemical ozone formation (POF), acidification (A) and freshwater eutrophication (FE) (EC-JRC 2012).

Spanish electricity mix in 2010 (Table 3) has been built in order to describe the burdens of the electricity grouping data from Red Eléctrica de España (the Spanish electricity system operator) (REE 2011) and using existing electricity processes from Ecoinvent database (ECOINVENT 2010).

The LCA software SimaPro 7.3 (PRé Consultants 2012) has been used to build all inventories and scenarios. Most of the processes have been taken from the Ecoinvent database (ECOINVENT 2010).

### Life cycle inventory

Figure 1 shows the main processes in cement production for this LCA study. System boundaries include waste from refuse as secondary materials and as alternative fuels. Only the pre-treatment and transport burdens of the waste are considered before using them as secondary materials (Haber 2013) or alternative fuels (Boesch and Meister 2011).

The inventory is split into two linked unit processes: clinker and cement production, each of them with different functional units, 1 t of clinker and 1 t of grey cement. The clinker unit process includes the primary raw materials and the fuels required as well as the transport of the materials and the infrastructures (see Table 4). The cement unit process introduces the clinker and the extra constituents according to each cement subtype production in 2010 (see Table 1). Mean values of the constituents' ranges,

**Table 3** List of input/output data of the Spanish electricity production mix in 2010

Technology	kWh (input)
Hard coal	0.0810
Lignite	0.0040
Natural gas, NGCC	0.2308
Natural gas, GT	0.0065
Hydropower, large	0.1381
Hydropower, run-of-river	0.0244
Nuclear	0.2215
Solar, PV	0.0219
Solar, CSP	0.0025
Wind	0.1544
Biomass	0.0088
Biogas cogeneration	0.0025
Natural gas cogeneration	0.0892
Gas oil, fuel, propane cogeneration	0.0092
MSW at incineration plant	0.0052
<hr/>	
Electricity from the mix	kWh (output)
Electricity	1

NGCC natural gas combined cycle plant, GT gas turbine, PV photovoltaic, CSP concentrated solar power, MSW municipal solid waste

established in the EN 197-1:2000 standard (CEN/TC-51 2000), have been assumed.

In 2010, Spanish cement factories produced 21.2 Mt of grey clinker and 22.8 Mt of grey cement (OFICEMEN 2010a). In terms of energy, the average Spanish thermal consumption of the kiln was 3,536 MJ/t of clinker, and the electricity consumption was 92 kWh/t of clinker. Cardim de Carvalho (2001) indicates that clinker unit process consumes 65.5 % of the total electricity, mainly due to the raw material mills and the clinker kiln processes, whereas the cement unit process (cement milling) consumes 30.8 % of the electricity.

Thermal contribution of the alternative fuels was 15.8 % of the total energy in 2010. Those alternative fuels are divided into 14 types (see 'Appendix 1') which have been categorised into three: biomass, partial-biomass and alternative-fossil (OFICEMEN 2010a). These valorised wastes are described in EC (2008), Law 16/2002, Law 22/2011 and Royal Decree 653/2003 and specifically in CEMA (2009, 2010).

In addition to the LCI of the alternative fuels ('Appendix 1'), a LCI of fossil fuels is described in 'Appendix 2'. Petroleum coke is the most relevant, with a contribution of 82 % of the total energy consumption (OFICEMEN 2010a).

CO<sub>2</sub> from process (limestone calcination) is introduced in Table 4. Emissions coming from combustion, both for

**Table 4** List of input/output data of the Spanish clinker production in 2010

	Amount
<b>Input</b>	
<b>Primary materials</b>	
Limestone (t)	1.12E+00
Calcareous marl (t)	2.77E-01
Clay (t)	7.97E-02
Sand (t)	2.73E-02
Iron ore, 46 % Fe (t)	8.33E-03
Kaolin (t)	5.28E-03
Silica sand (t)	3.66E-03
Bauxite (t)	2.61E-03
Feldspar (t)	2.86E-04
Ammonia (t)	2.02E-04
Aluminium oxide (t)	1.27E-04
<b>Secondary materials</b>	
Aluminium oxide, waste (t)	3.98E-04
Blast furnace slag (t)	3.16E-03
Carbonized sludges (t)	3.12E-03
Ceramic materials (t)	7.19E-04
Clay (recycling) (t)	7.01E-04
Sugar beet limes (t)	9.54E-05
Fly ashes (t)	2.98E-03
Foundry sand (t)	2.74E-04
Iron ore, waste (t)	4.76E-03
Iron recycled (t)	6.59E-04
Mining wastes (t)	1.61E-03
Other secondary materials (t)	1.80E-03
Other slag from meal (t)	4.45E-04
Pyrite ashes (t)	2.92E-03
Industrial solids (t)	1.00E-03
Water (m <sup>3</sup> )	1.62E-03
<b>Infrastructure</b>	
Industrial machine, heavy (t)	3.76E-05
Cement plant (p)	6.27E-12
<b>Transport</b>	
Conveyor belt (km)	2.00E + 00
Lorry 20–28 t (tkm)	3.19E+00
Lorry >28 t (tkm)	1.89E+01
<b>Fossil fuels</b>	
Petroleum coke (GJ)	2.89E+00
Heavy fuel oil (GJ)	3.41E-02
Natural gas (GJ)	4.36E-03
Diesel (GJ)	5.72E-04
Hard coal (GJ)	4.37E-02
<b>Alternative fuels</b>	
Other liquid fuels biomass (GJ)	3.23E-05
Used tyres (GJ)	1.72E-01
Meat bone and meal (GJ)	4.96E-02

**Table 4** continued

	Amount
Municipal sewage sludge (GJ)	3.01E-02
Refuse-derived fuel MSW (GJ)	9.73E-02
Wood waste (GJ)	5.76E-02
Impregnated sawdust (GJ)	4.17E-02
Varnishes and solvents (GJ)	4.54E-02
Used oils (GJ)	6.57E-03
Plastics (GJ)	2.53E-02
Pulp, paper, paperboard (GJ)	5.80E-04
Textile waste (GJ)	3.14E-04
Others no biomass (GJ)	3.13E-02
Hydrocarbon residues (GJ)	3.03E-03
<b>Electricity</b>	
Electricity (MWh)	9.20E-02
<b>Output</b>	
<b>Emissions</b>	
Carbon dioxide (process) (t)	5.28E-01
Particulates (PM <sub>10</sub> ) (t)	1.04E-05
<b>Products</b>	
Clinker (t)	1.00E+00

*Notes* Output section only includes the product (clinker) and the emissions coming from process (CO<sub>2p</sub> and PM<sub>10</sub>). The rest of the emissions, linked to the combustion of fuels, are included in ‘Appendices 1, 2’. It must be noted that all the values are referred to 1 tonne of clinker as functional unit

CO<sub>2</sub> and other pollutants, are imputed to the fuel entered in the LCI of the clinker. Consequently, a detailed characterisation of the fuels has been done in ‘Appendix 1’ (alternative fuels) and ‘Appendix 2’ (fossil fuels).

Regarding PM<sub>10</sub> emissions, results from Cardim de Carvalho (2001) have been assumed due to the lack of disaggregated data available concerning particulate matter <10 μm (PM<sub>10</sub>) emission factors from clinker and cement. It has been assumed that 64.87 % of the PM<sub>10</sub> emissions come from the clinker unit process and 30.62 % from the cement unit process. The rest of PM<sub>10</sub> until 100 % is lost in quarrying, transportation and fuel preparation.

#### Scenarios description

Human and environmental impacts of Spanish cement have been estimated using the 2010 cement production by type (Table 1), the LCI of Spanish clinker in 2010 (Table 4) and the average values of the European standard of cements EN 197-1 (CEN/TC-51 2000) (see Table 1). BASE scenario is then depicted for the Spanish cement production in 2010.

Once cements subtypes are specified, the LCI of the cement production is simplified grouping the production

**Table 5** List of input/output data of the production of 1 t of Spanish cement (generic)

	Amount
Input	
Materials	
Production breakdown by cement subtype (Table 1)	–
Electricity	
Electricity (MWh)	3.91E–02
Output	
Emissions	
PM <sub>10</sub> (t)	4.57E–06
BASE scenario	

shares and adding both the electricity consumed and PM<sub>10</sub> emissions released by cement mills in the latter phase of the production (see Table 5).

Besides the BASE scenario, the document introduces five scenarios (E1–E5), adding improvements to reduce the environmental impacts of cement production. BAT and some technology perspectives have been taken into account in the description of new scenarios.

#### *Thermal efficiency scenario (E1)*

This scenario considers a reduction in the use of thermal energy in the clinker kiln. World Business Council for Sustainable Development (WBCSD) gives some values depending on the kiln technology: the lowest figure (from 2006) is for dry kilns with preheater and precalciner (3,382 MJ/t clinker) (WBCSD 2009). European Integrated Pollution Prevention and Control Bureau (EIPPCB) points out that consumption varies depending on the type and size of the kiln system (EIPPCB 2013). Plants using dry process, with multistage cyclone preheaters and precalcining kilns (the majority in Spain), start at about 3,000 and can reach more than 3,800 MJ/t of clinker. Spanish statistics from OFICEMEN (2010a) give an average thermal consumption of 3,536 MJ/t clinker in 2010. Moya et al. (2010) show that thermal consumption in clinker production is expected to be 3,300 MJ/t of clinker in 2030. E1 scenario includes this reduction. Some BAT options for meeting that target are based on varying the modes of operation. Specific measures could be to install modern clinker coolers; to optimise the length of the kiln, as well as its design thinking about the fuels selection; to optimise the process controls; to reduce the air-in leakage; to extent the precalcination to the raw material; to increase the number of cyclone stages; to reduce the moisture content of the raw material; etc. (MMA 2004; EIPPCB 2013).

#### *Electrical efficiency scenario (E2)*

According to EIPPCB (2013), the electricity demand for a cement plant in Europe ranges from 90 to 150 kWh/t of cement. Although electricity consumption reported in Moya et al. (2010) in the EU27 is around 110 kWh/t cement, Spanish statistics (OFICEMEN 2010a) show a value of 130 kWh/t of cement.

In the Spanish case, system boundaries include not only the electricity consumption regarding raw material grinding, fuel preparation and cement milling, but also the consumption of the associated quarry. In spite of that electricity consumption at quarry is very low (Cardim de Carvalho (2001) reports 1 %) so the value is accepted.

Projections of the electricity consumption get to 106 kWh/t cement in 2030 (Moya et al. 2010). Subsequently, this scenario entails a reduction of 19 % in the total electricity consumption compared to 2010 statistics. EIPPCB (2013) remarks one single BAT option in order to reduce consumption: exchanging old raw material mills for new alternatives.

#### *Material substitution scenario (E3)*

E3 scenario analyses the reduction of the clinker-to-cement ratio, from 0.8 in 2010 to 0.7 in 2030 (Moya et al. 2010). In order to build E3, European Standard EN197-1 (CEN/TC-51 2000) for cement compositions has been adjusted keeping the 2010 cement production breakout (see Table 1).

Achieving this target requires to substitute part of the clinker with other mineral compounds (see ‘Appendix 3’). Attending to OFICEMEN (2010a), alternative materials used to produce cement in Spain in 2010 were ashes and slag from the recycling of cement and steel production, waste from iron ore, and recycled gypsum. This is in line with the assumption of blast furnace slag, fly ashes, pozzolana and limestone, as the main extra constituents of Spanish cement. Subsequently, BASE scenario entails a clinker-to-cement ratio by 0.8 and E3 scenario, by means of ‘Appendix 3’, introduces a clinker-to-cement ratio of 0.7.

If one tries to keep the cement production breakout constant, it is necessary to modify the percentages of the cement constituents. It is quite difficult to keep the ranges for the classification of cements according to EN 197-1 standard while keeping the same production breakout. Consequently, a conservative rupture beyond the limits only for the Portland cements (types I and II, in bold) has been assumed.

Furthermore, secondary material pre-treatment has been considered (Habert 2013). Limestone has been approached by an Ecoinvent existing process, and pozzolana has been understood as silica sand in Ecoinvent.

Alternative raw materials can be used to replace traditional raw materials extracted from quarries, such as clay, shale and limestone, which are inserted in the kiln, not only for cement production. The chemical suitability of alternative raw materials is important to ensure that they provide the necessary constituents in the formation of clinker (CEMBUREAU 2009). Boesch and Hellweg (2010) describe a case with 4 % weight of material substitution (+1 % each: slag, fly ash, waste limestone and contaminated soil). In Spain, the material substitution before kiln entailed 1.3 % (in mass) in 2010 (OFICEMEN 2010a). Material substitution before kiln is not considered in this work.

#### *Fossil fuel substitution scenario (E4)*

E4 scenario considers the fossil fuel substitution by alternative fuels. The use of this type of fuels in the cement industry offers the opportunity to reduce production costs, dispose of waste and reduce CO<sub>2</sub> emissions. Cement kilns are well suited for waste combustion due to their high process temperature and because clinker product and limestone feedstock act as gas-cleaning agents (IEA 2007). OFICEMEN (2010a) reported that 15.8 % of the thermal energy came from alternative fuels in 2010. EC made several projections for the fossil fuel substitution assuming 50–50 % between fossil and alternative fuels in 2030 in EU27 (Moya et al. 2010). In order to meet this target, both fossil and alternative fuels have been carefully described in ‘Appendices 1, 2’. For the implementation of this framework, incoming of fuels listed in Table 4 has been modified to accomplish with the 50–50 %, but keeping the 2010 fuel shares.

#### *Ideal scenario (E5)*

Finally, E5 scenario gathers all the measures described in the aforementioned scenarios (see Table 6). It is akin to an ideal scenario where all the possible expected improvements take place. It describes the optimum expected situation in the Spanish cement industry.

## Results and discussion

### Clinker production assessment (by process stage)

Table 7 shows the absolute values (per tonne of clinker) for each impact category using the ILCD 2011 midpoint method. As this analysis is referred to the generic Spanish cement (which encompasses the 16 subtypes produced in

**Table 6** Description of the Spanish cement production scenarios

Scenario	Description	Detail
BASE	Base case	2010 Spanish statistics
E1	Thermal efficiency	From 3,536 MJ/t clinker to 3,300 MJ/t clinker
E2	Electrical efficiency	From 130 kWh/t cement to 106 kWh/t cement
E3	Material substitution	Clinker-to-cement ratio: from 0.8 to 0.7
E4	Fossil fuel substitution	Alternative fuels share: from 15.8 to 50 % (in energy)
E5	Ideal	All improvements together

**Table 7** LCIA results of the Spanish clinker and cement production in 2010

Impact category	Clinker (per 1 tonne of clinker)	Cement (per 1 tonne of cement)
Climate Change (kg CO <sub>2</sub> eq)	9.29E+02	7.99E+02
Human toxicity with cancer effects (CTUh)	1.20E−06	1.25E−06
Photochemical Ozone Formation (kg NMVOC eq)	1.24E+00	1.09E+00
Acidification (molc H <sup>+</sup> eq)	3.93E+00	3.40E+00
Freshwater Eutrophication (kg P eq)	1.21E−02	1.23E−02

#### BASE scenario

The units of the impact categories are those used and recommended by the European Commission in the ILCD handbook (EC-JRC 2011)

Spain in 2010), values from Table 7 cannot be disaggregated by production stages.

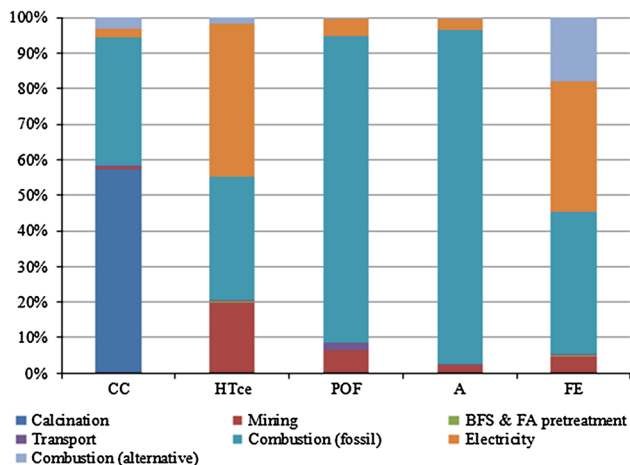
Paying attention to the results (see ‘Appendix 4’), it is observed that each cement subtype contribution is at the same level than productions. Portland cement type-I contributes with up to 30 % to each impact. Portland cement types II/A-V (fly-ashed), II/A-L (calcareous) and II/A-M (composite) also have remarkable contributions accounting for 10–15 % each. Apart from this analysis by cement type, it is interesting to consider the impact of the different process stages in the clinker production, the most energy intensive part in cement manufacture, since it includes kiln.

Impacts derived from clinker respect to the ones from cement are high enough for considering reasonable to focus only on the clinker production (Table 8). This avoids confusion with the selection of Spanish cement which it is considered generic (as in Table 7) and it makes possible to carry out a technical approach by production stage.

Figure 2 shows the LCIA results in the production of 1 t of clinker in 2010 in Spain. The most relevant point is the large contribution of fossil fuel combustion in all impacts,

**Table 8** Relative contribution (LCIA) of clinker respect to the cement production for a clinker-cement ratio of 0.8

CC (%)	HTce (%)	POF (%)	A (%)	FE (%)
93.5	77.4	91.7	92.9	78.9

**Fig. 2** LCIA results (relative units) of the production of 1 t of clinker in 2010 by production stage

especially in POF and A. The contribution of transport is up to 2 % in POF but, in the same way as the material pretreatment, it is almost negligible when compared to the rest of the categories.

Contribution of calcite's calcination entails 58 % of the CC, whereas 36 % comes from combustion processes: this is connected to the origin of the CO<sub>2</sub>. OFICEMEN (2010b) reports that 63 % of CO<sub>2</sub> came from process and 27 % from combustion. Petcoke combustion entails 98 % of the process contribution title 'fossil fuel combustion', being 99 % CO<sub>2</sub> and almost 1 % methane. A slight 3.5 % contribution of alternative fuel combustion is linked to the non-bio part, mostly used tyres (52 %).

Human toxicity with cancer effects is divided into main three contributions: 20 % mining, 35 % fossil fuel combustion and 43 % electricity coming from the network. This impact derives from the introduction of aluminium oxides linked to mining processes. Material input introduces a chromium VI burden into the water, imputing up to 86 % of the mining process contribution to the human toxicity. Fossil fuel combustion contribution is linked to the petroleum coke combustion mainly (98 % of 29 %), and electricity consumed drags the chromium VI burden from the grid. While contribution of the chromium VI (compared with the rest of HTce-substances) entails 85 % weight in the case of electricity, this value falls to 51 %

when looking at petcoke combustion where others substances (such as mercury and nickel) also have significant contributions.

In the category of POF, combustion of fossil fuels means 86 % of the total. Within this contribution, 68 % comes from nitrogen oxides, 19 % from sulphur dioxides and 11 % from non-methane volatile organic compounds (NMVOC).

Something similar occurs in A: fossil fuel combustion contributes, through petcoke combustion, up to 94 % of the total, from which 86 % is originated by sulphur dioxides and resting 14 % comes from the nitrogen oxides released.

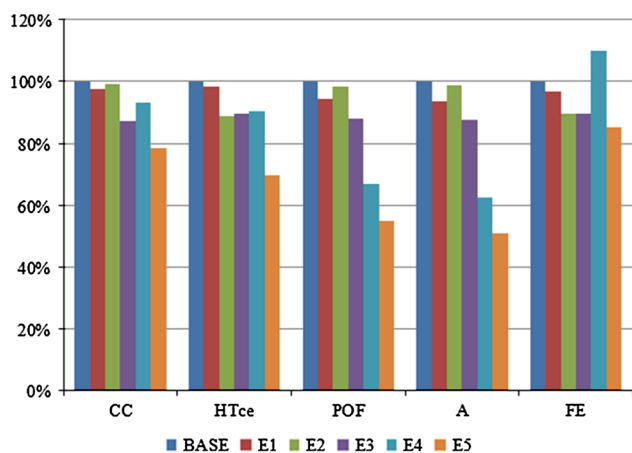
Finally, fossil fuel combustion and electricity consumed entail 40 and 37 % in the FE category, respectively. Mining processes entail 5 %, and alternative fuels combustion emerges, with contributions up to an 18 %. This category impact is characterised in ILCD 2011 method by a unique substance: phosphates. Attending to the fossil fuel combustion, petcoke is the cause of the 86 % of the sub-contribution. Phosphates from electricity are due to the coal existing in the electricity mix. In addition, the majority of the phosphates in the alternative fuel contribution live in the combustion of refuse-derived fuel, municipal solid waste (MSW), used oils, and varnishes and solvents.

Comparing other impact categories with Cardim de Carvalho (2001), whose study thoroughly depicts the Spanish production, a major contribution of the eutrophication in our work is observed, mainly due to the introduction of alternative fuels in the 2010 energy mix (in 2001, cement plants did only burn fossil).

Aside from the national statistics (see Table 1), OFICEMEN (2010b) reported a value of 837 kg of CO<sub>2</sub>/t of clinker in 2010. For the total cement production, Portland Cement Association gives an approximate value of 900 kg CO<sub>2</sub>/t of clinker for a dry kiln with preheater and precalciner (Masanet et al. 2012), while other authors (Van Oss and Padovani, 2003) report 940 kg CO<sub>2</sub>/t of clinker, of which 54.2 % comes from calcination and 45.8 % from combustion. This share is very dependent on the fuel mix and the energy required. In this work, absolute CO<sub>2</sub> emission in the production of clinker is 919 kg CO<sub>2</sub> (929 kg CO<sub>2</sub>-eq), being CO<sub>2</sub> from process 57.9 % and CO<sub>2</sub> from combustion 42.1 %. A ratio of 60/40 of CO<sub>2</sub> coming from process (limestone calcination) and from combustion, respectively, is accepted.

From the LCIA results obtained for the clinker production (see Fig. 2), several hotspots are found. Due to the contribution of the fossil fuel combustion to each impact, it is crucial to focus on that point. The main solution for the 'combustion problem' is to apply energy consumption improvements (BAT measures). This idea encompasses scenarios E1 and E2. Additionally, the scenarios E3 and E4 are focused on reducing the energy consumption, and the





**Fig. 3** LCIA results (relative units) of the production of 1 t of cement in 2010 considering the implemented scenarios

CO<sub>2</sub> emissions by applying structural changes in the way the fuels and the materials are consumed.

#### Cement production assessment (sectorial analysis)

Once the technical approach has been done and hotspots have been found, second part of the study is focused on the Spanish cement sector in 2010. Thanks to EN 197-1:2000 (CEN/TC-51 2000) and introducing the modifications included in ‘Scenarios description’ section, LCIA results for the cement produced in Spain are obtained.

Absolute values for each impact category are shown in Fig. 3. CC goes from 799 kg CO<sub>2</sub>-eq in the BASE scenario to 628 kg CO<sub>2</sub>-eq in the ideal scenario, E5. In addition, both A and POF decrease almost to a half. In contrast, HTce and FE reduce their amounts by around 30 and 15 % in E5, the most advantageous scenario. Besides, it is observed that FE grows significantly (+10 %) in E4, the fossil fuel substitution scenario.

Scenario E1 achieves 6 % reductions both in A and POF and 2–3 % in the rest of the categories. The scenario E2 reaches to reduce FE up to 11 % and HTce 8 %, being the rest negligible. Scenario E3, the material substitution scenario, achieves 10–13 % reductions in each category impact. Finally, scenario E4 reaches great reductions in A and POF, 37 and 33 % respectively. Furthermore, a 7 %-decrease takes place in CC and 5 % in HTce. Furthermore, by applying alternative fuels in the kiln, it is observed that FE does not experience any reduction. This is due to the effect of the burdens derived from the combustion of alternative fuels, mainly sewage sludges, refuse-derived fuel, MSW, used oils and varnishes, as shown in ‘Clinker production assessment (by process stage)’ section.

The ideal scenario, E5, proposed as an exploration for 2030 using the projections of the EC (Moya et al. 2010), entails very different reductions: 21 % in CC, 49 % in A, 45 % in POF, 30 % in HTce and 15 % in FE. These achievements are only attained as a result of all improvements described.

Focusing on achieving reductions in the CC impact category, the best way is to reduce the clinker-to-cement ratio followed by substituting fossil fuels with alternative ones. In terms of reducing the impacts in all environmental categories, fossil fuel substitution would be the first solution to be taken into consideration.

Material substitution scenario, E3, looks like the second preferred way to achieve reductions. This scenario is linked to the decarbonisation of the cement production process, i.e. reducing CO<sub>2</sub> emissions coming from limestone’s calcination, and it could contribute positively in diminishing the CC. Nevertheless, its implementation is difficult: keeping the European standard ranges for cements while keeping production breakdown is quite complex. In this work, a rupture of the European standard has been assumed in order to reduce the clinker-to-cement ratio from 0.8 to 0.7. In order to achieve that target, the need of a change in both cement’s demand, going from the current majority of Portland cements (type-II, 66.1 % and type-I, 25.4 %) to a major participation of non-Portland cements (types-III–IV–V), i.e. more declinkered cements; and more research on mechanical and chemical properties of cements (IEA 2009b), is quite obvious. To do so, an improvement in the process control systems (testing in detail the strength, durability, setting time, etc.) is required to ensure that mineral composition of the product is kept (Shi et al. 2011; Ioannou et al. 2014). Currently, some material substitution projects are taking place in many countries, but they are still at an early stage (CEMBUREAU 2012).

Valderrama et al. (2013) show results of a Spanish cement plant with a pair of scenarios: a material one and a fossil fuel substitution scenario. Material substitution scenario enters to the kiln 1.35 % (in mass) of dried sludge, the rest being limestone. As E3 scenario introduces secondary materials after the kiln, comparison is unsuitable. Moreover, its fossil fuel substitution scenario entails a unique entrance of dried sludge matter by 5.8 % (in mass). Reductions achieved are 1 % in CC, 5.2 % in A, 4.6 % in POF and 3 % in FE. In comparison, our BASE scenario (depicting a sectorial framework) enters 15.8 % (in energy, what is slightly different) through 14 alternative fuels and E4 scenario extends the contribution up to 50 %, reason for which our reductions are higher.

From the point of view of industry, a preferred way is observed: fossil fuel substitution. In 2002, substitution rate was 2 %, growing up to 15.8 % in 2010 and being 22 % in 2011 (OFICEMEN 2010a, 2011). Spanish cement producers are trying to make people aware of the benefits of fuel substitution, not only because it is the most cost-effective option (according to EIPPCB (2013), energy-related costs mean 40 % of the total production costs), but also because the use of alternative fuels is carbon neutral and avoids burning waste at incineration plants.

Nowadays, the Spanish cement producers association, OFICEMEN, and the CEMA foundation (CEMA 2009, 2010, 2011) are developing the current framework to apply all these measures in the Spanish cement industry: substitution scenarios and use of waste, mainly. The European Cement Research Association, ECRA, is developing an ambitious plan to build a satisfactory cement industry roadmap where BAT, substitution scenarios and even CO<sub>2</sub> capture have been studied.

To sum up, results have shown that a swap to alternative fuels usage is the best option to achieve the highest reductions in most of the impact categories considered, followed by the use of alternative materials in the composition of cement. On the contrary, these solutions are not ideal, since burning waste also releases large amounts of pollutants. Emissions derived from alternative fuels or materials also have an impact in human health and the environment, so these effects should be considered and evaluated in detail. Despite the cement industry is very interested in reducing its emissions, mainly CO<sub>2</sub>, NO<sub>x</sub>, SO<sub>2</sub> and particulates, all options must be very carefully taken into account.

## Conclusions

This work has addressed both human and environmental improvements applied on the Spanish cement making industry, implementing BAT on efficiency measures and considering other prospective solutions suggested by EC.

The first part of the study is focused on a technical analysis of the clinker production by process stage. Several hotspots have been found, depending on the impact category analysed: fossil fuel combustion, use of electricity and mining (quarry). Besides, CC presents an extra contribution coming from the CO<sub>2</sub> from limestone's calcination, the so-called CO<sub>2</sub> from process. It is also remarkable that alternative fuels combustion is still low, and material pre-treatments and transportation are negligible.

Going beyond the hotspots' recognition, this document has explored the Spanish cement sector in 2010, but looking at future. Consequently, a variety of scenarios have been developed in order to implement BAT and other technical solutions which would allow reduce emissions, waste and energy consumption.

Most significant improvements are referred to the energy requirements, both at the clinker kiln and power consumption. To face these challenges, it is needed to improve (or re-design) the kiln or change the mills for new ones. Notwithstanding, reductions in the considered impact categories are low (as much as 11 % in FE in E2). On the other hand, both material and fossil fuel substitution scenarios are the best options to achieve impact reductions.

Thus, changing the primary materials (entered in the cement mill with clinker) by secondary materials, previously considered waste (fly ashes, blast furnace slag, silica sands and non-calcined limestone), leads to 10–13 % reductions in each impact category. Furthermore, using alternative fuels instead of fossil has shown its advantages, decreasing 37 and 33 % A and POF, but increasing 10 % FE. Finally, in an ideal scenario where all technological options are implemented, reductions would reach from 21 % in CC to 49 % in A.

On this sectorial approach to the Spanish cement industry, it is possible to conclude that, in order to face the problems derived from fossil fuel combustion, a fuel shift is needed to reach less contaminant options. Material substitution is another good solution for the industry in terms of impact, but it requires a change in the demand and further research. Consequently, it will be necessary to ensure the properties of the cements (considering their uses) to the extent of the non-Portland cements demand grows. Beyond that, statistics are showing that the most cost-benefit option for cement producers in Spain is fossil fuel substitution, since alternative fuels shares are continuously growing (15.8 % in 2010, 22.4 % in 2011). Authors recommend taking into consideration the indirect increase of the FE due to the phosphates increase coming from the alternative fuels combustion.

As further developments of this work, the consideration of introducing carbon capture solutions to reduce CO<sub>2</sub> emissions and its environmental impacts has been carried out (García-Gusano et al. 2013).

## Appendix 1

See Table 9.

**Table 9** LCI of the pre-treatment, transport and combustion of 1 kg of each alternative fuel used in the Spanish cement production in 2010

Input	01	02	03	04	05	06	07	08	09	10	11	12	13	14
LHV(1)	kg	1	1	1	1	1	1	1	1	1	1	1	1	1
Materials/fuels	MJ/kg	18.88	13.29	20.14	12.4	15.17	12.94	17.13	12.48	31.34	27.04	14.81	29.84	24.67
Transport, lorry >28t (2)	tkm	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.05
Electricity/heat	kWh	0.008	0.251	0.003	0.008	0.033	0.033	0.092	0.003	0.045	0.003	0.033	0.066	0.003
Electricity, medium voltage (2)	MJ		6.265				0.23							
Heat from incineration plant (2)														
Output														
Emissions to air														
Carbon monoxide, biogenic	kg	1.35E-04	4.00E-05		2.23E-04	2.23E-04	2.23E-04	1.35E-04	2.23E-04					
Carbon monoxide, fossil	kg	8.82E-05					8.82E-05		2.23E-04		1.21E-05	2.23E-04	1.21E-05	1.21E-05
Carbon dioxide, biogenic	kg	7.23E-01	7.26E-02		1.46E+00	1.46E+00	7.23E-01	7.23E-01	1.25E+00					
Carbon dioxide, fossil	kg	4.74E-01					4.74E-01		3.09E+00	1.10E+00	1.73E+00	2.30E+00	1.80E+00	1.10E+00
Methane, biogenic	kg	3.86E-06	1.14E-06		6.38E-06	6.38E-06	3.86E-06	6.38E-06						
Methane, fossil	kg	2.53E-06					2.53E-06		6.38E-06			6.38E-06		
Sulphur dioxide	kg	4.46E-06	3.97E-06		5.99E-06	5.35E-07	8.44E-07	4.46E-06	6.19E-05	1.58E-05	7.70E-06	7.70E-06	5.99E-06	7.70E-06
Nitrogen oxides	kg	9.94E-05	6.75E-05		1.20E-04	3.14E-05	3.14E-05	9.94E-05	2.25E-03	2.66E-04	2.66E-04	2.66E-04	1.94E-04	2.66E-04
Ammonia	kg	2.48E-06	1.68E-06		2.98E-06	7.82E-07	7.81E-07	2.48E-06	5.61E-05	1.02E-05	1.02E-05	1.02E-05	4.84E-06	1.02E-05
Dinitrogen monoxide	kg	1.32E-05	9.79E-06		1.59E-05	4.17E-06	4.16E-06	1.32E-05	2.99E-04	3.69E-05	3.69E-05	3.69E-05	2.58E-05	3.69E-05
Cyanide	kg	2.81E-06	1.91E-06		3.38E-06	8.88E-07	8.87E-07	2.81E-06	6.38E-05	9.22E-06	9.22E-06	9.22E-06	5.50E-06	9.22E-06
Phosphorus	kg	8.94E-07	1.01E-06		1.13E-07	1.09E-07	1.09E-07	8.94E-07	3.75E-08	7.00E-07	7.00E-07	7.00E-07	5.25E-07	7.00E-07
Boron	kg	8.63E-07			2.06E-06	2.53E-07	3.28E-06	8.63E-07						
Hydrogen chloride	kg	6.64E-08			2.04E-08	3.67E-09	3.67E-09	6.64E-08	1.99E-08	2.22E-07	7.54E-06	7.54E-06	2.01E-07	7.54E-06
Bromine	kg	4.07E-08					4.07E-08							
Hydrogen fluoride	kg	2.97E-08			1.02E-08	1.11E-08	2.97E-08	2.97E-08						
Iodine	kg	1.31E-13					1.31E-13							
Silver	kg	9.28E-12			6.20E-13		9.28E-12							

Table 9 continued

	01	02	03	04	05	06	07	08	09	10	11	12	13	14
Arsenic	kg	6.38E-15	9.33E-16	2.09E-14	4.31E-15	2.75E-15	6.38E-15	6.12E-16				1.81E-14	1.22E-14	
Barium	kg	3.60E-08		1.14E-07			3.60E-08					1.74E-07		
Cadmium	kg	6.37E-10	3.58E-12	9.16E-11	1.10E-11	7.49E-11	6.37E-10	2.20E-12	4.41E-10			4.17E-09	4.41E-11	
Cobalt	kg	4.27E-14	1.19E-14	2.34E-14	2.76E-15	2.59E-09	4.27E-14			2.87E-09	2.00E-09	9.36E-13		2.87E-09
Chromium	kg	4.10E-12	2.09E-13	1.07E-12	4.86E-14		4.10E-12	4.14E-14				2.82E-12	8.28E-13	
Copper	kg	4.88E-09	9.62E-11	4.50E-10	3.06E-11		4.88E-09	3.30E-10		3.60E-09	3.00E-09	2.19E-09	7.00E-08	3.60E-09
Mercury	kg	4.07E-14	2.24E-15	4.80E-15	1.10E-14	1.10E-14	4.07E-14	2.07E-18	3.45E-17			2.74E-14	4.14E-17	
Manganese	kg	1.41E-12	6.68E-14	2.19E-13	2.89E-13	2.89E-13	1.41E-12					4.06E-13		
Molybdenum	kg	3.91E-09	4.43E-10	8.60E-09	1.66E-09	1.66E-09	3.91E-09							
Nickel	kg	2.35E-12	5.26E-14	4.08E-13	2.40E-14	2.39E-14	2.35E-12	6.91E-15		2.98E-09	2.00E-09	8.30E-13	2.24E-09	2.98E-09
Lead	kg	1.13E-08	1.34E-10	2.98E-09	1.03E-09	1.03E-09	1.13E-08	9.50E-10	2.60E-09			1.62E-08	6.83E-09	
Antimony	kg	5.48E-14		2.76E-15			5.48E-14					1.56E-13		
Selenium	kg	1.16E-15		1.30E-14			1.16E-15					9.85E-15		
Tin	kg	7.46E-08	1.23E-09				7.46E-08					3.24E-08		
Vanadium	kg	9.21E-10					9.21E-10					2.69E-08		
Zinc	kg	1.61E-08	5.80E-10	2.04E-09	2.91E-10	2.90E-10	1.61E-08	1.72E-09	2.61E-07	2.93E-08	2.90E-08	8.52E-09	4.76E-07	2.93E-08
Silicon	kg	3.63E-05	3.22E-06	4.95E-05			3.63E-05			7.29E-05	7.29E-05			7.29E-05
Iron	kg	2.80E-07	2.08E-07	3.97E-08	5.17E-10	5.16E-10	2.80E-07			5.93E-08	5.90E-08	1.16E-07		5.93E-08
Calcium	kg	1.47E-05	3.91E-06	5.73E-06	2.18E-07	2.18E-07	1.47E-05							
Aluminium	kg	1.19E-05	1.08E-06	1.94E-05	9.89E-09	9.88E-09	1.19E-05							
Potassium	kg	6.19E-06		4.00E-06	1.97E-07	1.97E-07	6.19E-06							
Magnesium	kg	3.44E-06	3.62E-07	5.92E-06	2.72E-07	2.72E-07	3.44E-06							
Sodium	kg	8.92E-06		8.65E-06	1.32E-07	1.47E-06	8.92E-06							
Emissions to water														
COD (r)	kg	4.02E-05	2.34E-04	2.70E-05	2.68E-05	2.68E-05	4.02E-05	2.31E-05	5.70E-05	2.40E-05	2.40E-05	4.23E-05	3.91E-05	2.40E-05
Nitrate (r)	kg	4.00E-05	1.28E-03	4.81E-05	1.26E-05	1.26E-05	4.00E-05	9.06E-04		1.33E-04	1.33E-04	7.82E-05		1.33E-04
Phosphate (r)	kg	1.75E-07	1.44E-05	2.21E-08	2.13E-08	2.13E-08	1.75E-07	7.33E-09		4.80E-05	4.80E-05		3.60E-05	4.80E-05
COD (g)	kg	1.82E-02	4.92E-04	9.97E-03	9.91E-03	9.89E-03	1.82E-02	8.52E-03	2.11E-02	7.75E-03	7.75E-03	1.56E-02	1.26E-02	7.75E-03
Nitrate (g)	kg	1.12E-04	7.62E-05	1.35E-04	3.55E-05	3.54E-05	1.12E-04	2.55E-03		3.72E-04	3.72E-04	2.20E-04		3.72E-04
Phosphate (g)	kg	1.05E-04	1.18E-04	1.32E-05	1.28E-05	1.27E-05	1.05E-04	4.39E-06		6.74E-04	6.74E-04		5.06E-04	6.74E-04
Ammonium, ion	kg		2.76E-04											
Nitrogen	kg		1.89E-05											

01 Meat and bone meals, 02 Municipal sewage sludge, 03 Other liquid fuels (bio), 04 Pulp, paper and paperboard, 05 Wood, 06 Impregnated sawdust, 07 Refuse-derived fuel MSW, 08 Textile waste, 09 Used tyres, 10 Hydrocarbon residues, 11 Others no biomass, 12 Plastics, 13 Used oils, 14 Varnishes and solvents

COD chemical organic demand, r river, g groundwater

Notes (1) Energy output (usable) refers to the low heating value (LHV) of each fuel according to CEMA (2010). (2) Both transport, electricity and heat required drag burdens from transportation and material pre-treatment. These values were obtained from Boesch and Meister (2011). (3) Emissions to air and water come from Ecoinvent (2010). In some vague cases, LHV was used for approaching factual fuel to an existing one in Ecoinvent database

## Appendix 2

See Table 10.

**Table 10** LCI of the fossil fuels combustion introduced in the 2010 Spanish cement production (CORINAIR 2006)

		Petcoke	Hard coal	Heavy fuel oil
Input	kg	1	1	1
LHV	MJ/kg	32.21	26.26	40.19
Output				
Emissions to air				
Carbon dioxide, fossil	kg	3.19E+00	2.26E+00	3.09E+00
Carbon monoxide, fossil	kg	3.12E−03	–	4.90E−03
NM VOC	kg	4.83E−05	–	1.21E−03
Nitrogen oxides	kg	6.44E−03	1.49E−02	7.78E−03
Sulphur dioxide	kg	2.19E−02	4.18E−03	3.07E−02
Benzene	kg	6.50E−07	6.50E−07	2.67E−08

NM VOC refers to non-methane organic volatile compound

## Appendix 3

See Table 11.

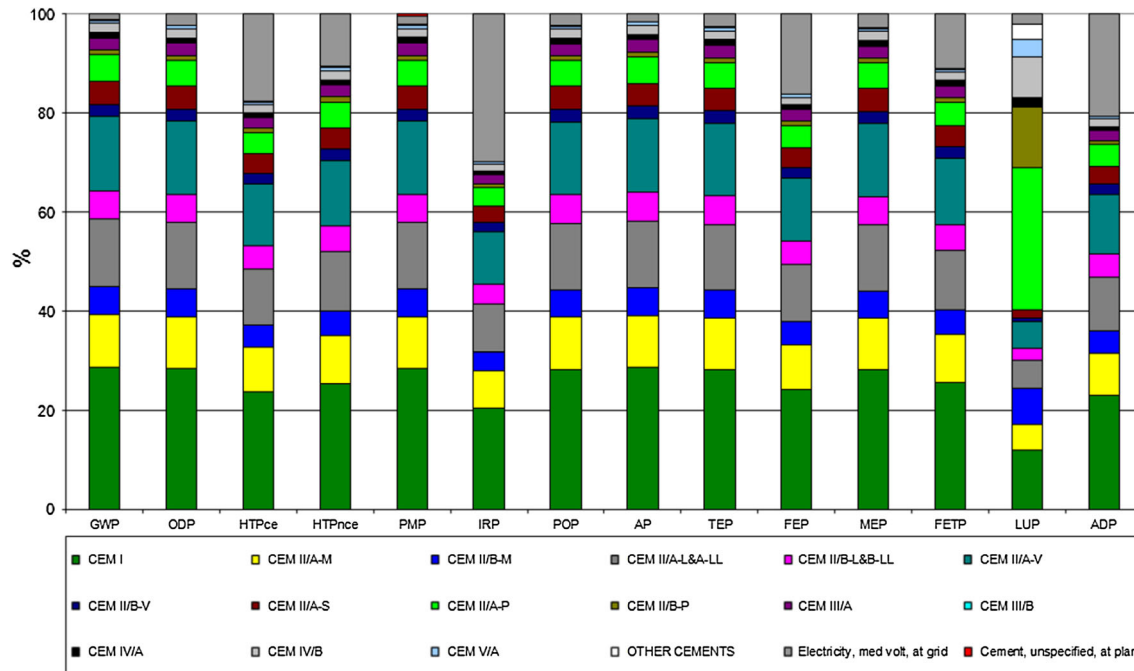
**Table 11** Spanish grey cements by type, E3 scenario adjustment (bold)

Cement type	Clinker (%)	BFS (%)	Pozzolan (%)	FA (%)	Limestone (%)
CEM I—Portland	<b>94.9</b>				
CEM II/A-M—Portland composite	<b>73.1</b>		0.4	8.2	14.1
CEM II/B-M—Portland composite	<b>59.8</b>		2.8	5.3	32.2
CEM II/A-L—Portland calcareous	<b>75.8</b>				19.9
CEM II/B-L—Portland calcareous	<b>59.4</b>				40.6
CEM II/A-V—Portland with fly ash	<b>75.7</b>			19.9	
CEM II/B-V—Portland with fly ash	<b>59.4</b>			40.6	
CEM II/A-S—Portland with BFS	<b>79.2</b>	13.8			
CEM II/A-P—Portland with pozzolan	<b>75.7</b>		19.9		
CEM II/B-P—Portland with pozzolan	<b>59.4</b>		40.6		
CEM III/A—Blastfurnace cement	50.3	49.7			
CEM III/B—Blastfurnace cement	22.7	77.3			
CEM IV/A—Pozzolan cement	74.0		5.7	17.2	
CEM IV/B—Pozzolan cement	52.5		11.9	35.6	
CEM V/A—Composite cement	38.2	36.0	12.9	12.9	
OTHER CEM (ESP VI, CAC, G)	27.5	24.2	24.2	24.2	

BFS blast furnace slag, FA fly ashes

## Appendix 4

See Fig. 4.



**Fig. 4** LCIA results (relative units) of the production of 1 t of cement (generic) in Spain in 2010. *Note* SimaPro output

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