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# A continuum-scale two-parameter model for non-Darcian flow in low-permeability porous media

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### Abstract

Numerous studies have demonstrated that Darcy velocity exhibits nonlinear dependence on the pressure gradient in lowerpermeability porous media such as clays and shales when the pressure gradient is low. Non-Darcian flow has important implications to geologic disposal of high-level nuclear waste, because shale has been proposed as a disposal medium, with compacted bentonite clay as a buffer material. Consideration of the impact of temperature on non-Darcian flow in an engineered clay barrier is necessary, because the clay barrier is subjected to significant temperature changes resulting from the heat-releasing nuclear waste package. In this study, a continuum-scale, two-parameter predictive model is developed to facilitate experimental data interpretation and to provide mechanistic insights into the role of temperature on non-Darcian flow in saturated lowpermeability porous media. This model has several advantages when it is applied at the continuum scale. First, this model is consistent with the current theory about the role of temperature and provides more flexibility in fitting experimental data associated with varying temperatures. Second, the values of the two independent parameters in the model can be easily determined and the solution is unique. This leads to practical convenience when the model is used to interpret continuum-scale laboratory data. Third, although the two-parameter model is simple, its performance in fitting existing experimental data is satisfactory. This suggests that the model achieves a balance between simplicity and effectiveness.

Keywords Non-Darian flow . Groundwater flow . Conceptual model . Temperature . Threshold gradient

## Introduction

Darcy's law, characterized by a linear correlation between flow velocity and pressure gradient, is widely used to describe fluid flow in porous media (Bear [1979](#page-5-0); Chen et al. [2010](#page-5-0)) and is the basis of most reservoir simulators. However, numerous studies (Miller and Low [1963;](#page-6-0) Bear [1979](#page-5-0); Hansbo [2001](#page-5-0); Sanchez et al. [2007](#page-6-0); Cui et al. [2008](#page-5-0); Liu and Birkholzer [2012;](#page-6-0) Liu et al. [2012](#page-6-0)) have demonstrated that Darcy velocity, in both saturated and unsaturated flows, exhibits nonlinear dependence on the pressure gradient in low-permeability porous media such as clays and shales when the pressure gradient is low. Non-Darcian flow results from the strong liquid– solid interactions (Miller and Low [1963\)](#page-6-0) in a thin layer close to clay surface, which are the combined effects of various

 $\boxtimes$  Cheng Chen [chen08@vt.edu](mailto:chen08@vt.edu) interfacial forces including the van der Waals forces (Liu [2017\)](#page-5-0). In low-permeability porous media, such as the shale formations and engineered clay barriers in nuclear waste repositories, the nanoscale pore size is comparable to the interfacial layer thickness so the influence of strong liquid-solid interactions is not negligible (Wang [2014](#page-6-0); Chen [2016\)](#page-5-0). A certain hydraulic gradient (i.e., the threshold gradient) is required to overcome the binding energy between water molecules and solid surfaces to trigger water flow (Miller and Low [1963;](#page-6-0) Hansbo [2001\)](#page-5-0), which leads to a nonlinear relationship between water flux and pressure gradient (Liu et al. [2016](#page-6-0)).

Non-Darcian flow has important implications to geologic disposal of high-level nuclear waste, because shale has been proposed as a disposal medium with compacted bentonite clay as a buffer material. Non-Darcian flow can occur in both the geologic barrier (shale) and engineered barrier (bentonite clay) systems (Liu [2014](#page-6-0)). For example, non-Darcian flow can lead to extremely low water velocity in the excavation damaged zone (EDZ) of a shale host rock, much lower than the velocity predicted by a Darcian flow model, and as a result diffusion will dominate solute transport in the EDZ (Bianchi et al.

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<span id="page-1-0"></span>[2015\)](#page-5-0). In a bentonite clay buffer, the initial water content is usually low, which causes water imbibition into the buffer from the surrounding host rock (Rutqvist et al. [2011\)](#page-6-0). This process develops an unsaturated zone in the near field of the waste container. Water flow under unsaturated conditions in bentonite clay usually shows stronger non-Darcian behaviors than saturated conditions, because in unsaturated media water generally occupies smaller pores and has lower connectivity (Liu et al. [2012;](#page-6-0) Fan et al. [2018\)](#page-5-0). Advanced understanding of non-Darcian flow in a bentonite clay buffer is critical for accurate prediction of water migration and saturation evolution over the time scale of 100,000 years in the near field of a repository. Heat generated by nuclear waste will greatly affect the distribution and transfer of water in the bentonite clay buffer. Furthermore, the wetting process resulting from water imbibition causes the bentonite clay to swell, which increases in-situ stress and provides an improved sealing effect to close the open space between the waste container and host formation. Thus, advanced understanding of non-Darcian flows in engineered clay barriers is crucial to accurately simulate the coupled thermal-hydrological-mechanical (THM) processes (Rutqvist et al. [2011,](#page-6-0) [2014\)](#page-6-0) and to reduce uncertainties associated with long-term performance assessment of nuclear waste disposal. Furthermore, study of non-Darcian flow in low-permeability media has direct applications to the recovery of unconventional hydrocarbon resources such as shale oil and gas, which requires improved understanding of the flow and transport processes in low-permeability shale formations (Chen [2016](#page-5-0)).

Consideration of the impact of temperature on non-Darcian flow in an engineered clay barrier is necessary, because the clay barrier is subjected to significant temperature changes resulting from the heat-releasing nuclear waste package. For instance, a recent THM simulation (Rutqvist et al. [2011](#page-6-0)) indicated that the temperature evolution in a bentonite-backfilled engineered barrier could be from a level lower than 30 °C to around 90 °C over a time scale of 100,000 years. The temperature can be even higher depending on the configuration of waste emplacement. Although experimental data with respect to the role of temperature on non-Darcian flows are rare, at least two groups (Miller and Low [1963;](#page-6-0) Zeng et al. [2010\)](#page-6-0) reported inspiring experimental data. Miller and Low [\(1963\)](#page-6-0) defined threshold gradient as the pressure gradient below which no flow occurs. They measured threshold gradient in a clay sample under two temperatures (10.15 and 20.00 °C) and found that it decreased with increased temperature; they speculated that the increased temperature might weaken the binding energy between water molecules and clay surfaces. Zeng et al. ([2010](#page-6-0)) measured the threshold gradient for oil flow in low-permeability sandstones under two temperatures (70 and 90 °C) and found a similar conclusion as Miller and Low ([1963](#page-6-0)). Although these experimental results are remarkable, an advanced theoretical framework is needed to improve

the fundamental understanding of the temperature dependence of non-Darcian flow in low-permeability porous media.

In this study, a continuum-scale, two-parameter predictive model is developed to facilitate experimental data interpretation and to provide mechanistic insights into the role of temperature on non-Darcian flow in saturated low-permeability porous media. Specifically, the new theoretical and modeling framework, when calibrated with experimental data, has the potential to improve the fundamental understanding of the temperature dependence of the threshold gradient in saturated non-Darcian flow and thus can provide reliable model inputs for coupled THM simulations for bentonite clay buffers in nuclear waste repositories.

# **Methods**

### Threshold and critical hydraulic gradients

In this study, the threshold gradient  $(J_t)$  is defined as the gradient below which no flow occurs. The critical gradient  $(J_c)$  is the intersection between the x (gradient) axis and the extension of the linear part of the curve, as shown in Fig. 1. The definition of threshold gradient  $(J_t)$  used here is the same as those in experimental studies such as Miller and Low [\(1963\)](#page-6-0), Zeng et al. [\(2010\)](#page-6-0), and Sanchez et al. [\(2007\)](#page-6-0). This is because  $J_t$  is straightforward and convenient to capture in experiments if equipment accuracy is sufficiently high. Conversely, Liu ([2014](#page-6-0)) defined  $J_c$  in Fig. 1 as the threshold gradient. Generally, from a modeling perspective, defining  $J_c$  as the threshold gradient will bring certain convenience in establishing the nonlinear relationship between water flux and gradient. For example, Liu and Birkholzer ([2012](#page-6-0)) developed a three-parameter, generalized Darcy's law, which under certain circumstances reduces to the correlations of Bear [\(1979](#page-5-0))  $(J<sub>t</sub> = J<sub>c</sub> > 0)$ , Swartzendruber ([1961\)](#page-6-0)  $(J<sub>t</sub> = 0$  and  $J<sub>c</sub> > 0)$ , and classic Darcy's law  $(J_t = J_c = 0)$ .



Fig. 1 Threshold gradient  $(J_t)$  and critical gradient  $(J_c)$  in non-Darcian flow.  $U$  is flow velocity and  $J$  is hydraulic gradient

#### <span id="page-2-0"></span>Conceptual model

It is hypothesized that there is an "effective" immobile layer at the liquid-solid interface in nanotube flow. This effective immobile layer is an ensemble concept, which takes into account all combined effects that hinder fluid movement in lowpermeability porous media such as strong liquid-solid interactions at solid surfaces, pore size heterogeneity, and barrier energy required for the fluid to enter small hydrophobic pores. It is hypothesized that the thickness of this immobile layer  $(h)$ decreases exponentially as the velocity gradient at the tube wall increases:

$$
h = h_0 \exp\left(-a \frac{\partial u}{\partial r}\Big|_{r=R}\right) \tag{1}
$$

where r is the distance from the tube center (m),  $R$  is tube radius (m),  $h_0$  is the initial immobile layer thickness (m) when the flow velocity is zero, and  $a$  is the characteristic time (s). Both parameters  $(h_0 \text{ and } a)$  are positive, might depend on the temperature, and need to be determined by fitting experimental data, which will be discussed later. It should be noted that Eq. (1) is formulated to enhance the two-parameter model's capability in fitting the phenomenological correlation between threshold gradient and clay permeability at the laboratory scale. For incompressible Newtonian laminar flow in a circular tube (Gerhart and Gross [1990\)](#page-5-0), one has:

$$
\left. \frac{\partial u}{\partial r} \right|_{r=R} = \frac{R}{2\mu} \left| \frac{\partial p}{\partial x} \right| \tag{2}
$$

where  $\mu$  is water viscosity (Pa s), and  $\partial p/\partial x$  is pressure gradient (Pa/m). Plugging Eq.  $(2)$  into Eq.  $(1)$ , one obtains:

$$
h = h_0 \exp\left(-\frac{aR}{2\mu} \left|\frac{\partial p}{\partial x}\right|\right) \tag{3}
$$

The apparent permeability (Chen  $2016$ ) ( $k_a$ ) which is subjected to the influence of the effective immobile layer, is calculated as:

$$
k_{\rm a} = \frac{1}{8} (R - h)^2 \tag{4}
$$

Combining Eqs.  $(3)$  with  $(4)$ , one obtains:

$$
k_{\rm a} = \frac{1}{8} \left[ R - h_0 \exp\left( -\frac{aR}{2\mu} \left| \frac{\partial p}{\partial x} \right| \right) \right]^2 \tag{5}
$$

When  $h$  is sufficiently low due to the increased pressure gradient,  $R \geq h$ , which suggests that water flow starts to occur. One can calculate the threshold pressure gradient,  $J_t$  (Pa/m), which is the minimum absolute value of  $\partial p/\partial x$  needed to ensure a positive value inside the parentheses on the right-hand side of Eq.  $(5)$ :

$$
J_{t} = \begin{cases} \left(\frac{-2\mu}{aR}\right) \ln\left(\frac{R}{h_{0}}\right) & \text{if } h_{0} > R\\ 0 & \text{if } h_{0} \leq R \end{cases}
$$
(6)

# Results

### Fitting experimental data

The threshold gradient as a function of permeability based on Eq. (6) is plotted, as illustrated in Fig. [2](#page-3-0). Specifically, given the effective pore radius  $(R)$  the absolute permeability of the porous medium is calculated as  $k = R^2/8$  and plotted as the x axis. R is then used to calculate the threshold gradient based on Eq. (6) and plotted as the y axis. It is assumed that  $\mu =$ 0.001 Pa s (water viscosity at the temperature of 20 °C),  $a =$ 1 s, and  $h_0 = 1$  μm, which is larger than all R values used in Fig. [2](#page-3-0) so a non-zero threshold gradient is needed to initiate fluid flow (see Eq. 6). With the two parameters (a and  $h_0$ ) determined tentatively, this base scenario (scenario 1) shows a power-law relationship between the threshold gradient,  $J_t$ (m/m), and the permeability,  $k$  (m<sup>2</sup>):

$$
J_t = 9 \times 10^{-13} k^{-0.85}
$$
 (7)

Liu and Birkholzer [\(2012\)](#page-6-0) also found a power-law correla-tion (Fig. [3](#page-3-0)) between  $J_t$  (m/m) and  $k$  (m<sup>2</sup>) by fitting experimental data from seven groups (Lutz and Kemper [1959;](#page-6-0) Miller and Low [1963;](#page-6-0) Blecker [1970;](#page-5-0) Dubin and Moulin [1986;](#page-5-0) Zou [1996;](#page-6-0) Cui et al. [2008](#page-5-0); Wang et al. [2011](#page-6-0)):

$$
J_t = Ak^B \tag{8}
$$

where  $A = 4.0 \times 10^{-12}$  and  $B = -0.78$ . Note that in this twoparameter model  $a = 1$  s and  $h_0 = 1$  μm were chosen as the initial, tentative parameter values. The values of  $a$  and  $h_0$  will then be adjusted to match the values of A and B which result from experimental data fitting. By investigating Eq. (6), it is found that changing the value of  $h_0$  will change both A and B. Conversely, changing the value of a will only change A. In other words, when the temperature is fixed (i.e., fixed  $\mu$ ), the coefficient (A) depends on both a and  $h_0$ , whereas the powerlaw exponent  $(B)$  depends only on  $h_0$ . This suggests that, although there are two unknown parameters (*a* and  $h_0$ ) in Eq. (6), it is possible to find a unique solution to them by fitting experimental data. Specific workflow is as follows:

Step 1: Conduct laboratory experiments and then use data fitting to obtain the empirical, power-law correlation between threshold gradient and medium permeability,  $J_t = Ak^B$ .

<span id="page-3-0"></span>Fig. 2 Threshold gradient  $(J_t)$  as a function of permeability  $(k)$  based on Eq. ([6\)](#page-2-0). Temperatures in scenarios 1 and 2 are 20 °C and 55 °C, respectively. In scenario 3, temperature is still 55 °C but  $h_0$  is reduced to 0.7 μm

Step 2: Fit the experimental data using Eq. [\(6\)](#page-2-0); adjust the value of  $h_0$  to match the power-law exponent (*B*). Step 3: Adjust the value of a to match the coefficient  $(A)$ .

Using this workflow, it is found that  $h_0 = 1.4$  µm and  $a =$ 4 s, which lead to  $A = 4.0 \times 10^{-12}$  and  $B = -0.78$ , exactly the same as the coefficients found by Liu and Birkholzer [\(2012\)](#page-6-0) for Eq. [\(8\)](#page-2-0). Therefore, it is clear that the continuum-scale twoparameter model is able to fit experimental data, and unique values of the two parameters (a and  $h_0$ ) can be determined in the data fitting process based on the workflow.

### Sensitivity analysis and temperature dependence

The values of  $a$  and  $h_0$  are then adjusted for sensitivity analysis, as illustrated in Fig. 2. Scenario 1 ( $a = 1$  s and  $h_0 = 1$  µm) is referred to as the base scenario. In scenario 2, it is assumed



Fig. 3 Correlation between permeability  $(k)$  and threshold hydraulic gradient  $(J_t)$  by fitting experimental data from seven groups. Modified from Liu and Birkholzer (2012)



that temperature is raised to 55 °C so fluid viscosity accordingly drops to 0.0005 Pa s. It is observed that the curve for scenario 2 is shifted downward in a parallel manner, without any change in the power-law exponent  $(-0.85)$ . In scenario 3, the value of  $h_0$  is artificially reduced to 0.7  $\mu$ m when the temperature is 55 °C, because it is hypothesized that the increased temperature leads to a thinner effective immobile layer. The resultant curve shows that the reduction of  $h_0$  further shifts the curve downward and it has a more significant influence on higher permeabilities. As a consequence, scenario 3 shows a steeper slope in the log-log plot, leading to a higher absolute value of the power-law component  $(-1.03)$ .

Based on Eq. [\(8](#page-2-0)) and the available experimental data in the literature (Miller and Low [1963;](#page-6-0) Zeng et al. [2010\)](#page-6-0), Liu [\(2014](#page-6-0)) suggested an empirical correlation to account for the effect of temperature on the threshold gradient in saturated non-Darcian flow:

$$
J_{t} = Ak^{B}(\mu_{ref}/\mu)^{B}
$$
\n(9)

where  $\mu_{ref}$  and  $\mu$  are water viscosities at the reference temperature and current temperature, respectively. With a negative value of B, an increased temperature (i.e., reduced fluid viscosity) will result in a smaller  $J_t$ . Equation (9) suggests that temperature affects only fluid viscosity and is unable to influence the value of the power-law exponent  $(B)$ . The temperature dependence of threshold gradient based on Eq. (9) is illustrated in Fig. [4,](#page-4-0) which illustrates the same trend as that described in scenario 2 in Fig. 2 (i.e., the threshold gradientpermeability correlation shifts in a parallel manner under the influence of the varying temperature). Furthermore, the proposed two-parameter framework is able to capture more complicated trends that involve the change of the power-law exponent (i.e., scenario 3 in Fig. 2). In this study, the twoparameter predictive model provides higher flexibility because of the two independent parameters (*a* and  $h_0$ ). Adjusting  $\mu$  and  $\alpha$  changes A, while adjusting  $h_0$  changes both A and B. All of these properties of Eq.  $(6)$  $(6)$ , associated with the data-fitting workflow described in the preceding section

<span id="page-4-0"></span>

Fig. 4 Temperature dependence of threshold gradient based on Eq. (9). Modified from Liu (2014)

'[Fitting experimental data](#page-2-0)', give the new model a lot of flexibility and physical insights in fitting experimental data associated with varying temperatures.

Table 1 summarizes the values of the two parameters, a and  $h_0$ , and the value of fluid viscosity,  $\mu$ , in the continuum-scale predictive model (Eq. [6\)](#page-2-0), as well as the corresponding values of the two fitting coefficients  $(A \text{ and } B)$  in the empirical powerlaw correlation (Eq. [8](#page-2-0)). As described previously, in scenarios 1–3 illustrated in Fig. [2](#page-3-0), the values of a and  $h_0$  are assigned in Eq. [\(6](#page-2-0)) first, and then the generated data  $(J_t$  and k) are fitted using the power-law correlation to determine the values of A and B. The purpose of demonstrating scenarios  $1-3$  in Fig. [2](#page-3-0) is to investigate the influence of the values of a and  $h_0$  on the empirical power-law correlation. When fitting the experimental data shown in Fig. [3](#page-3-0), however, the procedure is reverse. The values of A and B are determined first by fitting the empirical power-law correlation to the experimental data from the seven research groups shown in Fig. [3.](#page-3-0) The values of the two parameters,  $a$  and  $h_0$ , are then adjusted to match the determined values of  $A$  and  $B$  using the data fitting workflow described in the preceding section '[Fitting experimental data](#page-2-0)', and a unique solution to  $a$  and  $h_0$  can be found.

Based on the parameter values in scenarios 1–3, Darcy's law, in which the permeability is calculated by Eq. [\(5](#page-2-0)), is used to plot apparent flow velocity  $(U)$  as a function of pressure gradient (*J*) in a clay sample having permeability of  $3.13 \times$ 10−<sup>16</sup> m2 , as demonstrated in Fig. [5.](#page-5-0) The shape of the velocitygradient curves is similar to that observed in laboratory experiments (Sanchez et al. [2007;](#page-6-0) Zeng et al. [2010](#page-6-0)), and the proposed two-parameter predictive model is able to capture both the threshold  $(J_t)$  and critical  $(J_c)$  gradients, as defined in Fig. [1](#page-1-0). Reduced fluid viscosity resulting from increased temperature (scenario 2) leads to lower  $J_t$  and  $J_c$ , as well as higher linear-part slope due to the increased fluid mobility (i.e.,  $k/\mu$ ), which is consistent with the experimental finding of Zeng et al. [\(2010](#page-6-0)). Figure [5](#page-5-0) also shows that decreased  $h_0$  (scenario 3) leads to lower  $J_t$  and  $J_c$  but does not cause significant changes in the linear-part slope. This implies that in future research it is critical to study the role of increased temperature on  $h_0$  besides studying its role on fluid viscosity.

## Discussion and conclusion

The continuum-scale, two-parameter predictive model developed in this study aims to interpret the phenomenological correlation between threshold gradient and clay permeability in saturated non-Darcian flow. This model has several advantages when it is applied at the continuum scale. First, sensitivity analyses demonstrate that this model is consistent with the current theory about the role of temperature on the threshold gradient (Eq. [9\)](#page-3-0). The current theory is a pioneering work developed by Liu ([2014](#page-6-0)) based on the analysis of available experimental data. It assumes that the temperature influences only fluid viscosity, and thus does not change the exponent value in the power law that describes the phenomenological correlation between threshold gradient and clay permeability. In the future, when more experimental data with respect to varying temperatures are available, there is a need to account for the variation in the power-law exponent due to the temperature change. Thus, the two-parameter modeling framework provides more flexibility and mechanistic insights in fitting experimental data associated with varying temperatures because of the two independent parameters in the model

**Table 1** Values of the two parameters (a and  $h_0$ ) the fluid viscosity ( $\mu$ ) and the two fitting coefficients (A and B) in scenarios 1–3 (Fig. [2\)](#page-3-0) and the process of fitting experimental data (Fig. [3](#page-3-0))

Parameter	Scenario 1	Scenario 2	Scenario 3	Fitting experimental data in Fig. 3
a(s)				4
$h_0 \,(\mu m)$			0.7	1.4
$\mu$ (Pa s)	$1 \times 10^{-3}$	$5 \times 10^{-4}$	$5 \times 10^{-4}$	$1 \times 10^{-3}$
$\boldsymbol{A}$	$9 \times 10^{-13}$	$5 \times 10^{-13}$	$1 \times 10^{-15}$	$4 \times 10^{-12}$
B	$-0.85$	$-0.85$	$-1.03$	$-0.78$

<span id="page-5-0"></span>Fig. 5 Apparent flow velocity  $(U)$  as a function of pressure gradient  $(J)$  using Eq.  $(5)$  $(5)$  for the calculation of permeability in Darcy's law



(Fig. [2](#page-3-0)). Second, although the proposed model has two independent parameters, their values can be readily determined using the data-fitting workflow described in section '[Fitting](#page-2-0) [experimental data](#page-2-0)', and the solution to the parameter values is unique. This leads to practical convenience and advantage when the two-parameter model is used to interpret continuum-scale laboratory data. Third, although the twoparameter model is simple, its performance in fitting experimental data is satisfactory. The model successfully fits existing experimental data collected by other research groups (Fig. [3](#page-3-0)). Moreover, the two-parameter model is able to accurately describe the nonlinear relationship between apparent flow velocity and hydraulic gradient (Fig. 5), which is consistent with experimental observations in the laboratory. This suggests that the two-parameter model achieves a balance between model simplicity and effectiveness.

The two-parameter modeling framework is developed at the continuum scale, and for the sake of simplicity it does not account for the pore-scale difference between interlayer space (micropores) and outerlayer space (macropores) in clays. This is because the current theory about the relationship between threshold gradient and clay permeability, which is based on an empirical, power-law correlation (Eq. [8\)](#page-2-0), uses the overall clay permeability measured at the laboratory scale, which is contributed by both the micropores and macropores. Therefore, the continuum-scale, two-parameter model does not differentiate internal pores at the two spatial scales, and as a consequence the double-structure pore geometry framework (Sanchez et al. [2005](#page-6-0)) is not used in this model. The simplification of clay pore geometry in the two-parameter model leads to certain convenience in its practical application at the continuum scale, especially in fitting laboratory hydrodynamic experimental data. The new theoretical and modeling framework, when fitted with experimental data, can improve the fundamental understanding of the temperature dependence of the threshold gradient in saturated non-Darcian flow and provide reliable model inputs for coupled THM simulations for bentonite clay buffers in nuclear waste repositories.

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