

Solid-state potentiometric gas sensors—current status and future trends

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Abstract The development of potentiometric sensors for monitoring environmental gases has become a well-established direction in sensor technology. Various types of potentiometric sensors employing solid electrolytes for in situ measurements of such gases as oxygen, hydrogen, carbon dioxide, sulfur oxides, carbon monoxide, nitrogen oxides, and hydrocarbons are reviewed. Particular concern was given to the CO₂ potentiometric sensor which is an example of successful commercial application. The construction details, working mechanism, and performance of different types of potentiometric gas sensors are given. Special emphasis is given for the mixed-potential electrodes, which seems to be the principal direction for the future research and development of the sensor science and technology. Additionally, the future use of potentiometric sensors for the detection of other environmental gases is discussed.

Keywords Potentiometric gas sensors · Solid electrolytes

Introduction

There is significant activity in the development of new sensor technology for monitoring of environmental gases. Several concepts for gas sensors are now under consideration. Chemical gas sensors may be classified into three main categories. The first group is composed of sensors generally based on the generation of voltage and currents in potentiometric cells using liquid or solid electrolytes. The second category includes sensors based on materials which

change their physical properties, such as surface electrical conductivity, gate effects in the characteristics of field-effect transistors and metal–oxide–silicon (MOS) structures, Curie points for piezoelectric and Hall-effect devices, and adsorption bands for optical devices [1, 2]. The third type of sensors includes catalytic combustion gas sensors operating as submicro-calorimeters.

The need for reliable, sensitive, and stable sensors is caused by a growing trend to lower the levels of concentration at which potential pollutants have to be monitored and controlled, according to what is required in many industrial applications. With the increase in environmental deterioration caused by acid precipitation, on-site measurement of acid-forming gases is desirable. Large coal-fired and oil-fired facilities are under heavy pressure to reduce the emissions of sulfur oxides (SO_x), nitrogen oxides (NO_x) and carbon oxides (CO_x) [3, 4].

Sulfur is one of the main organic impurities in fossil fuels [5]. Nitrogen oxides (NO and NO₂) are products of direct synthesis occurring at high temperatures. They are mainly emitted from automobiles, stationary combustion facilities, and homes. The interest in sulfur recovery and in the monitoring of SO_x and NO_x emissions continues to remain high because ‘it is market-driven in stringent government regulations, especially the enactment of the Clean Air Act Amendments (CAAA) of 1990 with additional US State regulations for reducing SO_x and NO_x in coal-fired boiler emissions by 90% and above’ [6, 7]. Many years of financial and intellectual effort have gone into identifying possible practical solutions. The 1990s revolution relating to the development of the in situ SO_x and NO_x combustion gas analyzers continues unabated as new analyzers are combined with microprocessor technology to produce more powerful capabilities.

Carbon dioxide concentration in air has risen from a pre-industrial level of about 265 ppm [8] to a value above

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355 ppm (1995), and recent reports [9, 10] suggest that by 2050, this value will have increased to 710 ppm. This steady CO₂ increase contributes to global warming. The most effective way of suppressing CO₂ exhaustion into the atmosphere is to control the emission amount of CO₂ at every exhaust site. For this purpose, simple inexpensive and portable sensors need to be developed.

Since the incomplete combustion of fuel sometimes causes serious carbon monoxide (CO) and hydrocarbon (CH_x) poisoning, the sensing of toxic, odorless CO has recently become increasingly important with regard to the safety of gas appliances. As a consequence of this, compact solid-state CO and CH_x sensors are needed in order to detect the incomplete combustion of gas appliances. For the above uses, the sensors should have high CO sensitivity combined with high CO selectivity against coexistent CO₂, NO_x, H₂, H₂O, and hydrocarbon gases. The development of CH_x and CO sensors is particularly important in the prevention of unexpected explosions and fires in mines [11].

Although a variety of sensor development efforts may be found in the literature now, it is important to note that most of these developments are based on empirical methods, mainly trial and error [11]. Unfortunately, most of the investigated prototype sensors are not always directly applicable for making reliable measurements in the harsh industrial environments found in the steel, heat treating, metal casting, glass, ceramic, pulp and paper, automotive, utility, and power industries, agriculture, and coal mines. Moreover, a fundamental understanding of the sensing mechanism is missing, and this makes the optimization of the sensor's design a very important task.

The objective of this paper is to review the developing field of potentiometric sensors for the detection and measurement of important environmental gases such as hydrogen, oxygen, carbon dioxide, sulfur and nitrogen oxides, and other gases.

Until now, a number of papers describing electrochemical devices as sensors for various gases have been published. Depending on the type of measured signal, electrochemical sensors may be divided into three general groups: potentiometric, amperometric, and coulometric. Additionally, taking into account the structure details of the gas sensors, the other classification has been proposed by Weppner [2, 12] and then further developed by Yamazoe and Miura [13].

Conventional solid-state ionic sensors (type I)

In the case of conventional potentiometric gas sensors, the gas to be detected is converted to the mobile component in a solid electrolyte (Fig. 1). The solid electrolyte separates a reference compartment and a test compartment. A potential difference

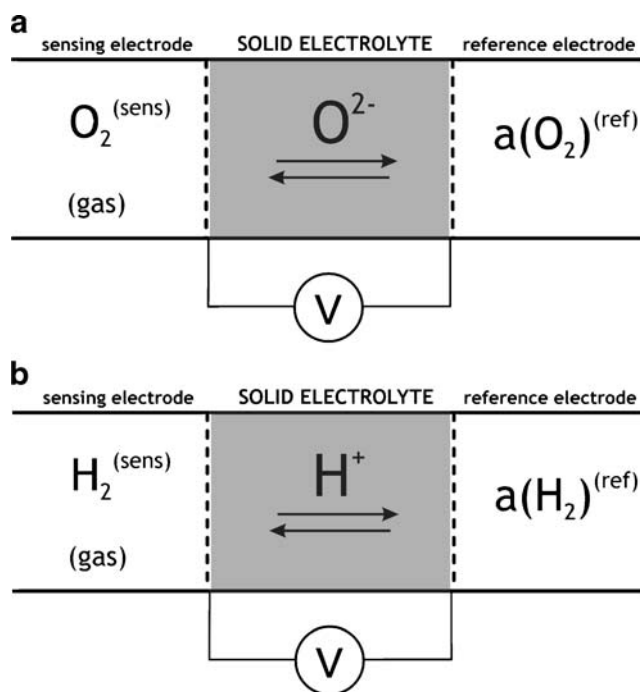


Fig. 1 Schematic illustration of type I potentiometric gas sensor with oxygen conductor (a) and protonic conductor (b) used as solid electrolytes

is established between the two sides of the solid electrolyte and is dependent on the difference in activity across the solid electrolyte of the species that will equilibrate with the conduction ions in the solid electrolyte. A spectacular example of such sensors is an oxygen sensor with an oxygen-ion conductor, such as cubic zirconia stabilized with yttria [14]. Figure 1a schematically illustrates the sensor structure. The electrodes comprise a porous layer of metal, usually platinum. The electrode reaction, taking place at the three-phase contact points (metal/electrolyte/gas), may be described in the following way:



The cell electromotive force (EMF), E , is determined from the Nernst equation:

$$E = \frac{RT}{4F} \ln \frac{p}{p_o} \quad (2)$$

where p and p_o denote oxygen partial pressures at the measuring and reference compartments, respectively. The partial pressure of oxygen at the reference electrode (more precisely oxygen activity), p_o , should maintain constant value. It may be achieved either by passing a gas containing a constant concentration of oxygen (usually air) over the reference electrode compartment or using a so-called 'oxygen buffer.'

The oxygen buffer is a heterogeneous mixture of either a metal, M , and its oxide, MO , (e.g., Pd–PdO, In–In₂O₃, Ni–NiO, etc.) or the mixture of two metal oxides containing

metals of two different valences (e.g., Cu₂O–CuO, CoO–Co₃O₄, etc.).

Taking the Ni–NiO mixture into consideration, as an example, the following chemical equilibrium is established at elevated temperatures (above ca. 1,000 K):



From the mass action law for equilibrium (3), we have:

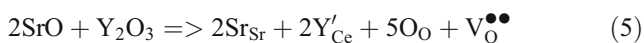
$$p_o = p(\text{O}_2) = K_T^2 = \exp\left(-\frac{2\Delta G^\circ}{RT}\right) = \text{const}|_{T=\text{const}} \quad (4)$$

where K_T and ΔG° are the equilibrium constant and the standard free enthalpy of the reaction 3, respectively.

The potentiometric hydrogen sensor with a protonic solid electrolyte is another example, important from the viewpoint of practical importance. Figure 1b shows the structure and working mechanism of such sensor.

Most potentiometric hydrogen sensors are based on a new generation of high-temperature proton-conducting materials. The KTaO₃-based material was the first one in a series of attempts [15, 16]. Then came acceptor-doped strontium or barium cerates, with the formulas SrCe_{1-x}M_xO_{3-δ} or BaCe_{1-x}M_xO_{3-δ}, respectively, where M usually denotes a rare earth element, and x is lower than the solubility limit of M³⁺ ions in the crystal lattice (usually less than 0.2). These materials exhibit p-type electronic conductivity under oxidizing atmospheres free from hydrogen-containing gases. In either wet or hydrogen atmospheres, electronic conductivity decreases and the ionic component assumes high values. The studies of potentiometric hydrogen transport revealed that ionic transport is realized by protons. Ionic conductivity is of the order of 10⁻³ to 10⁻² Ω⁻¹cm⁻¹, within 873–1,273 K. Apart from cerates, protonic conductivity was also reported in zirconate perovskites, although their conductivity is about ten times lower than that of the cerates [17, 18]. High mechanical and chemical stability of zirconates such as CaZr_{0.9}In_{0.1}O_{3-δ} (with respect to carbonate or hydroxide formation [19]) are the necessary prerequisites for their use in the construction of hydrogen sensors applied in metallurgy [20].

According to the dopant incorporation reaction (Kröger–Vink notation was used), given by Eq. 5:



Trivalent ions Y³⁺ substitute tetravalent Ce⁴⁺ ions, and an appropriate amount of oxygen vacancies is formed to maintain the electroneutrality condition:

$$x = [\text{Y}'_{\text{Ce}}] = 2[\text{V}_\text{O}^{\bullet\bullet}] \quad (6)$$

In the presence of either water vapor or hydrogen, protonic defects are formed. Taking into account the small size of protons, we can assume that they do not occupy

lattice positions but rather attach to oxide ions, forming OH groups [21]:

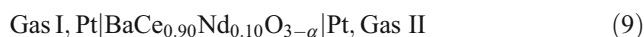


The formation of OH⁻ groups has been confirmed by means of infrared method [22, 23].

Protonic defects formed in reactions (7) or (8) (OH[•]) are free to move in the perovskite structure. Barium cerates exhibit the highest total conductivity, but the ionic conductivity component is mixed—both protonic and oxide-ion. On the other hand, strontium cerates show almost purely protonic conductivity [24, 25]. However, both Ba and Sr cerates suffer from instability in CO₂-containing gas atmospheres. In this respect, Ca or Sr acceptor-doped zirconates are much more stable [26, 27].

Acceptor-doped strontium or barium cerates were originally used as a solid electrolyte in humidity sensors [28–32]. They then received interest with regard to hydrogen sensors [32–39].

Iwahara et al. [32, 34] studied the potentiometric cell:



The cell (Eq. 9) worked in a stable manner within the 473–1,173 K range. The sensing signal (EMF) acted according to the Nernst equation. The response time, $t_{0.90}$, corresponding to 90% of the total change of the measured signal, was about 20 s. Despite these satisfactory results, instability in CO₂-containing atmospheres has remained a problem as far as Ba and Sr cerates are concerned. Stability may be improved using a small deficit of barium in respect to stoichiometric composition [36].

Indium-doped CaZrO₃ is another example of a potentiometric sensor used to determine hydrogen activity in molten metals [33, 35]. This solution has been used with great success.

A more sophisticated hydrogen sensor composed of a hydrogen pump and a solid cell with SrCe_{0.95}Yb_{0.05}O_{3-α} as the solid electrolyte was proposed by Katahira et al. [37, 38]. The constant hydrogen activity at the reference electrode is maintained here by potentiometric pumping of hydrogen from the measured gas to the reference electrode compartment. The excess of hydrogen is allowed to escape through the calibrated opening.

Figure 2 shows one of the typical sample holders used for the purpose of sensors' measurements. The construction of holder allows separating easily gases at the sensing and reference electrode compartments. Figure 3 shows the example results of the sensor response to the changes of hydrogen partial pressure. The inset in Fig. 3 shows the

Fig. 2 Sample holder together with the tubular type prototype hydrogen sensor based on protonic conductor, used for the measurements of sensor characteristics

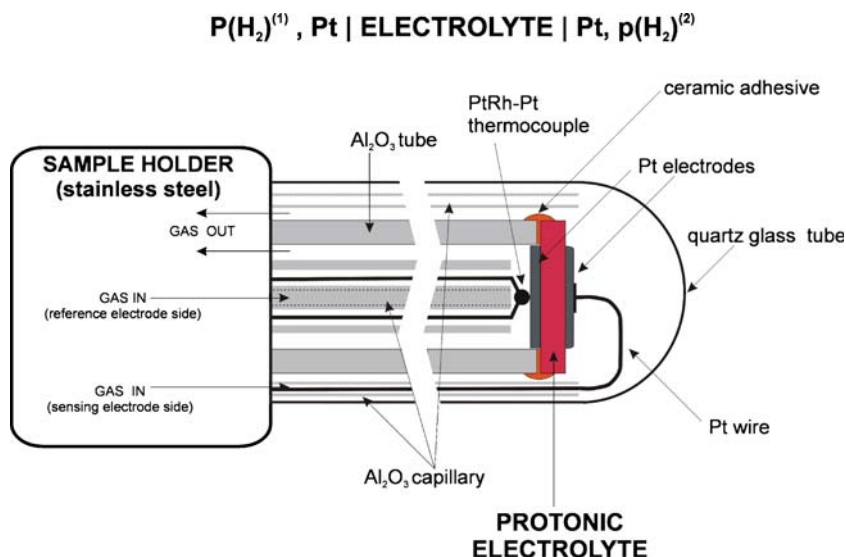


illustration of response time determination. As can be seen, the reversible changes of measured EMF can be observed. The response and recovery times are reasonably short (less than 1 min). Similar results were obtained for sensors based on yttrium-doped strontium cerate and published elsewhere [39].

The other examples of type I potentiometric sensors described in literature are listed in Table 1 [14, 32–44]. As can be seen, the list of type I potentiometric sensors is very short, due to lack of suitable solid electrolytes. There are no solid electrolytes with mobile ions originating from such gases

as NO_x, SO_x, or CO₂. The potentiometric sensor of CO₂ with mobile CO₃²⁻ described by Matsumoto et al. [45] could be treated as ‘type I’, but the electrolyte used was not solid state.

Sensors based on equilibration with the mobile component of solid electrolyte (type II)

In this type of sensors, the gas equilibrates with the component that is different from the predominantly

Fig. 3 Dynamic response at 1,023 K of hydrogen potentiometric sensor based on SrCeO₃ solid electrolyte. The inset shows the example of response time determination of the cell

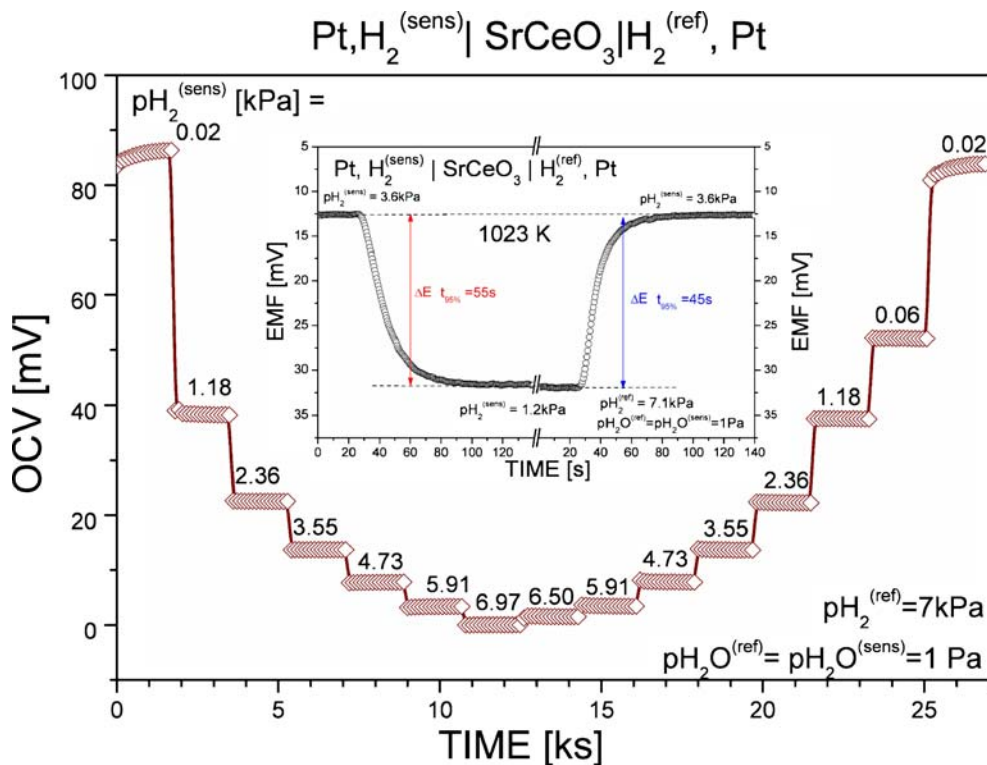
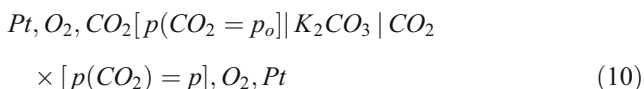


Table 1 Gas sensors of the type I

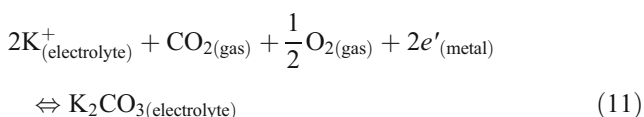
Gas	Solid electrolyte	Mobile ion	Reference	Year
O ₂	Stabilized zirconia (YSZ)	O ²⁻	[14]	1991
H ₂	HUO ₂ PO ₄ ·4H ₂ O (HUP)	H ⁺	[40]	1982
	SrCe _{1-x} M _x O _{3-δ} , BaCe _{1-x} M _x O _{3-δ} ; M=Nd, Y, Yb, etc.		[32–39]	1991–2008
F ₂	LaF ₃	F ⁻	[41]	1991
Cl ₂	SrCl ₂ -KCl	Cl ⁻	[42]	1999
	BaCl ₂ -KCl		[43]	1997
	PbCl ₂ -KCl		[42, 44]	1999, 1998

mobile species, as shown schematically in Fig. 4. One example is the CO₂ sensor with the K₂CO₃ solid electrolyte, proposed by Gauthier and Chamberland [46].

Let us consider the following solid cell:



In this cell, K⁺ ions, the only mobile ions of the solid electrolyte K₂CO₃, interact with gaseous molecules of CO₂, according to the reaction:



If oxygen activity is the same at both electrodes, then cell EMF, *E*, may be expressed as:

$$E = \frac{RT}{2F} \ln \frac{p}{p_o} \tag{12}$$

By replacing the above reference electrode by [46]:



we receive a solid cell, in which EMF:

$$E = \text{const.} + \frac{RT}{2F} \ln p \tag{14}$$

where const. includes the *E*^o of pure silver sulfate and silver-ion activity in K₂CO₃.

Several examples of type II sensors and their basic parameters are collected in Table 2 [46–54].

Furthermore, NO_x [55] and SO_x [56–59], the type II sensors, are reported.

Surface-modified solid-state ionic sensors (type III)

The application of solid potentiometric cells as gas sensors of type I or II may be successful only in certain cases, i.e., when for the given gas *A* there exists a suitable solid

electrolyte AB with ionic transference numbers—*t_A* (type I) or *t_B* (type II)—close to 1. Taking into account other important properties of solid electrolytes, such as the operating temperature range and equilibrium gas pressure, chemical reactivity with metal electrodes and surrounding construction materials, gas-tightness, etc., the list of satisfactory couples (*A*, AB) is very short, especially for type II.

The application of an additional auxiliary phase, AP, gives a much wider opportunity of applying solid cells as gas sensors [2, 60, 61].

Yamazoe and Miura [13] proposed a further modification of the proposed classification. They divided type III sensors

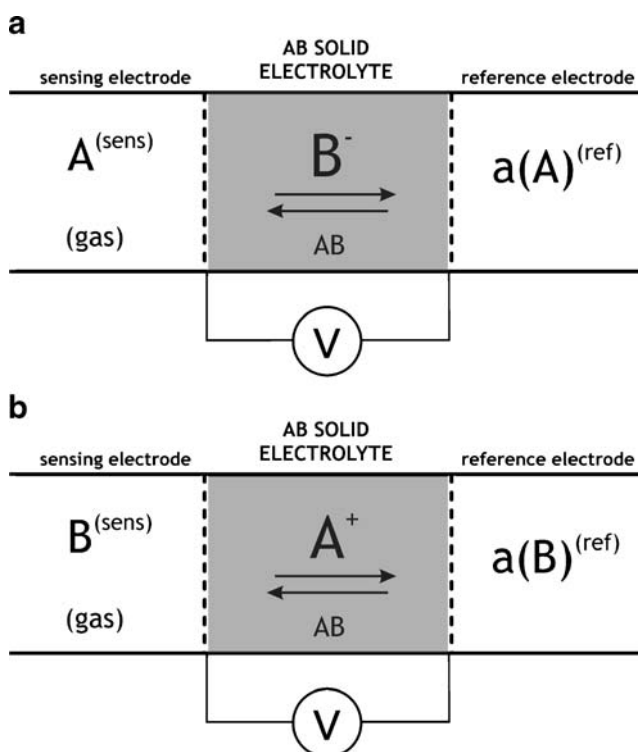


Fig. 4 The illustration of type II potentiometric gas sensor with anion conductor (a) and cation conductor (b)

Table 2 Performance of electrochemical sensors type II for CO₂

Cell structure <i>Me</i> , Ref SE Sens CO ₂ , O ₂ (air) <i>Me'</i> ^a	Operating temperature (°C)	Measured concentration (ppm)	Response time (s)	Reference	Year
Ag Ag ₂ SO ₄ (1 mol% in K ₂ CO ₃) K ₂ CO ₃ CO ₂ , O ₂ , Au	725	50–1,000	Few seconds to few minutes	[46]	1977
	300–750	9–12,000		[47]	1984
Au, CO ₂ (<i>p</i> _o), O ₂ K ₂ CO ₃ CO ₂ (<i>p</i>), O ₂ , Au	725	1–1,000		[48]	1983
<i>M</i> , CO ₂ , O ₂ Na ₂ CO ₃ –K ₂ CO ₃ –Y ₂ O ₃ CO ₂ (<i>p</i>), O ₂ , <i>M</i> ; <i>M</i> =Au, Pd, Pt	300–600	1–1,000	1–100	[49]	1997
<i>M</i> , CO ₂ , O ₂ Na ₂ CO ₃ –BaCO ₃ CO ₂ (<i>p</i>), O ₂ , <i>M</i> ; <i>M</i> =Au, Pd, Pt, Ag	580–680	300–10 ⁵	0.0045–1,000	[50]	1995
Au, O ₂ Ca–ZrO ₂ K ₂ CO ₃ CO ₂ , O ₂ , Au	750	200–2,000	15	[48]	1983
Au, O ₂ , CO ₂ Li ₂ CO ₃ +5 mol% Li ₃ PO ₄ +25 wt% Al ₂ O ₃ CO ₂ , O ₂ , Au	300–600	10–1,000	10–30 min	[51]	1995
Pt LiCoO ₂ –Co ₃ O ₄ Li ₂ CO ₃ –Li ₃ PO ₄ –LiAlO ₂ (89:5:6) CO ₂ , O ₂ , Au	350–400	40–1,000	60	[52]	1997
Au LiMn ₂ O ₄ Li ₂ CO ₃ +20 wt% MgO CO ₂ , O ₂ , Au	300–405	6×10 ³ –4×10 ⁴	60–120	[53]	1999
Au, Na ₂ ZrO ₃ + ZrO ₂ Na ₂ CO ₃ +30 mol% LiNbO ₃ CO ₂ , O ₂ , Au	450	250–1,000	45	[54]	1999

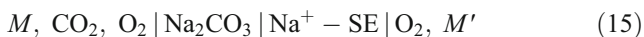
^a *Me*, *Me'* Metal; *Ref* reference electrode; *SE* solid electrolyte; *Sens* sensing electrode

into three sub-groups, depending on whether the mobile ions of solid electrolyte, SE, and AP are:

- the same—type IIIa
- different but of the same sign—type III b
- of a different sign—type IIIc

Type IIIa

Figure 5 illustrates the structure of the type IIIa sensor schematically. Let us consider the following cell as an example:



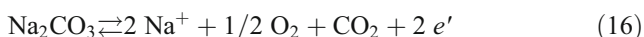
where *M*, *M'*—metal electrodes, usually Pt, Au, or Pt, Ag.

Na⁺–SE—solid electrolyte with Na⁺ as mobile ions, such as Na-β"-alumina or NASICON.

Na₂CO₃ plays the role of as the auxiliary phase, AP. The formulation of a theoretical dependence for EMF should start from the chemical reactions taking place at both electrodes.

Sensing electrode

At sensing electrodes involving sodium carbonate, the following reaction is commonly assumed:

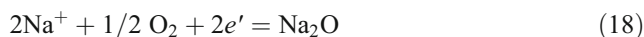


ΔG_{16} of the reaction 16 may be written in terms of the chemical potentials:

$$\begin{aligned} \Delta G_{16} = & 2\eta(\text{Na}^+) + \frac{1}{2}\mu^o(\text{O}_2) + \frac{RT}{2} \ln p(\text{O}_2) \\ & + \mu^o(\text{CO}_2) + RT \ln p(\text{CO}_2) + 2\eta(e') \\ & - \mu^o(\text{Na}_2\text{CO}_3) \end{aligned} \quad (17)$$

where μ^o and η denote standard chemical potential and potentiometric potential at the sensing electrode, respectively.

Reference electrode



ΔG_{18} of the reaction 18:

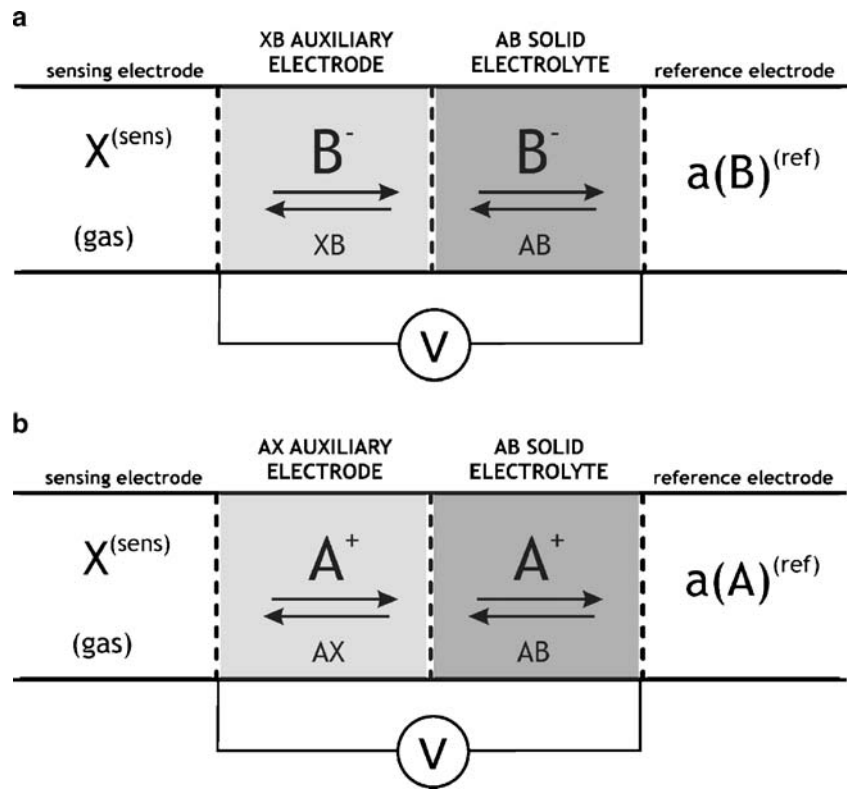
$$\begin{aligned} \Delta G_{18} = & \mu^{o'}(\text{Na}_2\text{O}) + RT \ln a'(\text{Na}_2\text{O}) - 2\eta'(\text{Na}^+) \\ & - \frac{1}{2}\mu^o(\text{O}_2) - \frac{RT}{2} \ln p'(\text{O}_2) - 2\eta'(e') \end{aligned} \quad (19)$$

The superscript ' denotes reference electrode region, *a'* (Na₂O) denotes the activity of Na₂O at the Na⁺SE/O₂, *M'* interface.

According to the definition of EMF, EMF measurements should be performed when a current flowing across the cell is near to zero, so we can assume that the local equilibria are established on both electrodes. This implies that:

$$\Delta G_{16} = \Delta G_{18} = 0 \quad (20)$$

Fig. 5 The potentiometric chain of a type IIIa gas sensor with anion conductor (a) and cation conductor (b)



Moreover, the difference of the potentiometric potentials of Na^+ ions, $\eta(Na^+)$, at both electrodes is equal to zero because of the good conductivity of Na^+ ions in the Na^+ solid electrolyte:

$$\eta(Na^+) = \eta'(Na^+) \tag{21}$$

Taking into account the general definition of EMF [62] and Eqs. 17, 19, 20, and 21, the following dependence of the electromotive force, E , can be derived:

$$E = -\frac{\eta(e') - \eta'(e')}{F} = \frac{-\Delta G^\circ(Na_2CO_3)}{2F} + \frac{RT}{2F} \ln \frac{p(CO_2)a'(Na_2O)p(O_2)^{1/2}}{p'(O_2)^{1/2}} \tag{22}$$

where $\Delta G^\circ(Na_2CO_3)$ is the standard free enthalpy of the formation of Na_2CO_3 from Na_2O and CO_2 . When oxygen partial pressure at both electrodes is the same, Eq. 22 assumes the form:

$$E = E^\circ + \frac{RT}{2F} \ln [p(CO_2)a'(Na_2O)] \tag{23}$$

where E° is the EMF of the cell in standard conditions, and may be expressed as:

$$E^\circ = -\frac{\Delta G^\circ(Na_2CO_3)}{2F} \tag{24}$$

As can be seen from Eq. 23, the linear dependence between E and $\ln p(CO_2)$ can be achieved when the activity of Na_2O at the reference electrode is constant:

$$a'(Na_2O) = f(p(CO_2)) = \text{const} \tag{25}$$

Some authors assumed a priori that condition (25) is fulfilled [63–67]; others made efforts to modify the reference electrode in order to achieve this condition.

Weppner et al. [68–70] applied the reference electrode with a constant activity of Na. According to Liu and Weppner [68, 69], the following equilibria are established at the reference electrode containing metallic Na:



and



Sodium peroxide, Na_2O_2 , is stable below 733 K. Above this temperature, it decomposes to sodium oxide, Na_2O , and oxygen. Applying the Gibbs–Duhem relation to equilibrium (26), we have:

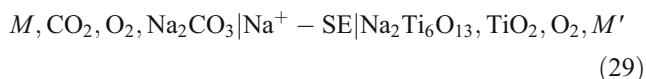
$$\ln a'(Na_2O) = \frac{\Delta G_{26}^\circ}{RT} - \ln a'(Na) - \frac{\ln p'(O_2)}{2} \tag{28}$$

where ΔG_{26}° is the standard free enthalpy of reaction (26).

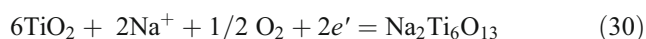
As can be seen from Eq. 28, at constant $p(O_2)$ and the constant activity of sodium, $a'(Na)$, at the reference

electrode, the activity of sodium oxide, $a'(\text{Na}_2\text{O})$, also remains constant. The constant activity of sodium can be achieved using either the Na phase [$a'(\text{Na})=1$] [56, 57] or the $\text{Na}_x\text{CoO}_{2-y}$ phase [59, 71]. The use of $\text{Na}_x\text{CoO}_{2-y}$ phase makes it possible to construct sensors showing/exhibiting Nernstian behavior.

In order to obtain the constant value of Na_2O activity, Maier et al. [72, 73] proposed the use of the other ‘ Na_2O buffer’ through the application of the heterogenous mixture $\text{Na}_2M_x\text{O}_{2x+1} - \text{MO}_2$, where $M=\text{Zr, Sn, Ti}$. Below, we present the detailed analysis of the sensing mechanism of the following cell:



It may be assumed that presented Eqs. 16, 17, and 21 are valid also for cell (Eq. 29). On the other hand, for the reference electrode, the following is true:



Then, ΔG_{30} of the reaction (30) is:

$$\begin{aligned} \Delta G_{30} = & \mu^o(\text{Na}_2\text{Ti}_6\text{O}_{13}) - 6\mu^o(\text{TiO}_2) - 2\eta(\text{Na}^+) \\ & - 2\eta'(e') - \frac{1}{2}\mu^o(\text{O}_2) - \frac{RT}{2} \ln p'(\text{O}_2) \end{aligned} \quad (31)$$

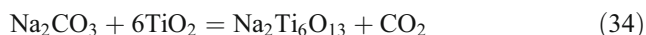
Instead of Eq. 20, we have:

$$\Delta G_{16} = \Delta G_{30} = 0 \quad (32)$$

The combination of Eqs. 17 and 21, as well as Eqs. 31 and 32, leads to the expressions for $\mu_e, \mu_{e'}$, and taking into account Eq. 22 we get the following dependence of the electromotive force, E , of the cell:

$$E = -\frac{\eta(e') - \eta'(e')}{F} = \frac{\Delta G_{34}^o}{2F} + \frac{RT}{2F} \ln \frac{p(\text{CO}_2)p(\text{O}_2)^{1/2}}{p'(\text{O}_2)^{1/2}} \quad (33)$$

where $\Delta G^o(\text{Na}_2\text{Ti}_6\text{O}_{13})$ is the standard Gibbs energy of the reaction:



When oxygen partial pressures at both electrodes are the same, Eq. 33 takes the form:

$$E = E^o + \frac{RT}{2F} \ln p(\text{CO}_2) \quad (35)$$

where E^o is the EMF of the cell in standard conditions and may be expressed as:

$$E^o = \frac{\Delta G_{34}^o}{2F} \quad (36)$$

Type IIIb

Sodium carbonate and the Na^+ -conducting solid electrolyte were first applied as the auxiliary phase and the solid electrolyte, respectively, in CO_2 sensors. However, such sensors suffer from high chemical affinity to water vapor. This leads to instability of the sensor signal and to the deterioration of the sensor structure. The use of either lithium carbonate [60, 74] or its mixture with CaCO_3 [75, 76] or BaCO_3 [77–79] considerably improves stability of the sensor in the presence of water vapor. Replacing sodium carbonate with lithium carbonate gives a new class of potentiometric sensors, classified as type IIIb.

Figure 6 illustrates the structure of type IIIb sensors schematically. A number of type IIIb sensors are known, most of which are designed specifically for the detection of CO_2 . Several examples of such sensors and their basic parameters are collected in Table 3 [63, 68, 69, 80–132].

Despite good performance of such sensors, the mechanism of charge transport through the cell is unclear. Ogata et al. [63] studied several CO_2 sensors composed from $\text{Na}\beta$ -alumina as a solid electrolyte and different auxiliary phases (carbonates of Li, Na, K, Cs and Ca). All sensors show a two-electron mechanism ($n=2$), but the standard EMF (E^o) reached different values. This suggests that the electrode reactions are similar, but other factors must be taken into account.

There are other possible explanations of the sensing mechanism of type III sensors. For example, for the auxiliary phase composed from Li_2CO_3 (either pure or in a mixture with BaCO_3), we can propose the following reactions at the sensing electrode:

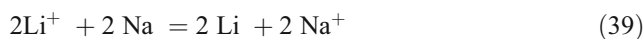
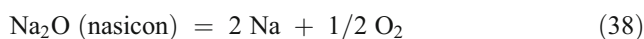
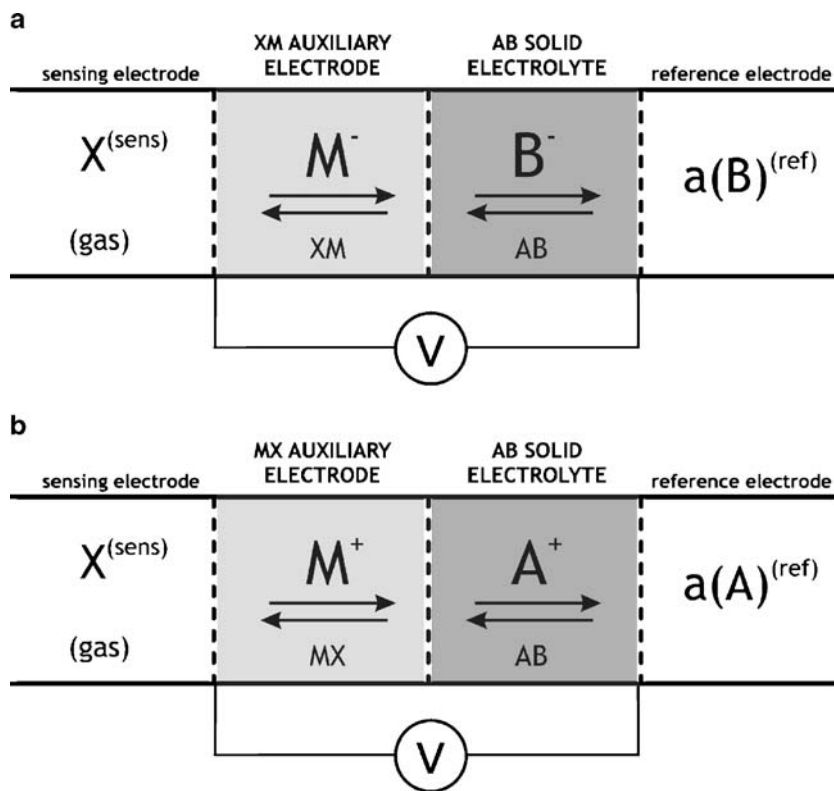


Figure 7 shows an example of CO_2 type IIIb sensor characteristics, measured at 748 K. The response time is shown in the inset. As can be seen, the changes of carbon dioxide pressure (line, right axis) are followed by the changes of measured signal, EMF (points, left axis). The determined response time is below 1 min. It is worth to mention that such structure was found to be stable only in a very limited temperature range, close to 740–750 K. At temperatures lower and higher than 740–750 K, sensors exhibit unstable behavior during the long-term exploitation. Such observation can be explained by the formation of liquid phase at the sensing electrode–solid electrolyte interface. More details can be found in [79]. The long-term stability of

Fig. 6 The potentiometric chain of a type IIIb gas sensor with anion conductor (a) and cation conductor (b)



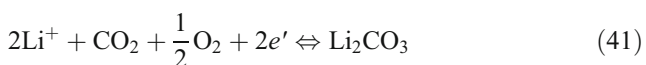
any potentiometric sensor is the important problem and wide interdisciplinary issue to be defined and solved in the future. Some selected results related to the problem of long-term stability are presented in [79, 127, 132].

Type IIIc

Figure 8 illustrates the structure of the type IIIc sensors. As an example of the type IIIc sensor, we consider the CO₂ sensor featuring stabilized zirconia as the solid electrolyte and lithium carbonate as the auxiliary phase [76]:

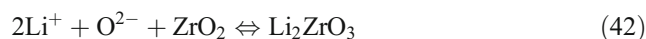


The right-hand side electrode serves solely as an oxygen-sensitive reference electrode, at which equilibrium (1) is established, and the left-hand side electrode is the sensing electrode on which the following reaction occurs:



The auxiliary phase Li₂CO₃ is a Li⁺-conducting solid electrolyte. To achieve potentiometric junction between both solid electrolytes, (O²⁻)Mg–ZrO₂ and the (Li⁺) AP, the formation of an interfacial compound Li₂ZrO₃ containing both conducting ions is postulated. This compound, playing the role of an ‘ionic bridge’ (IB) between the stabilized

zirconia and lithium carbonate, is the product of the reaction:



As follows from equilibrium (42) and Fig. 8, the ionic bridge can play the role of the source or the trap of both cations and anions, depending on cell polarization.

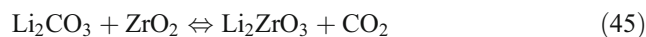
Taking into consideration electrode reactions (1) and (42) and assuming that oxygen partial pressure at both electrodes is the same, the cell EMF, *E*, may be expressed as:

$$E = E^o + \frac{RT}{2F} \ln p \quad (43)$$

where:

$$E^o = -\frac{\Delta G^o}{RT} \quad (44)$$

and Δ*G*^o is the standard free enthalpy of the following reaction:



As can be seen from the presented Eqs. 43 and 44, the measured signal *E* is independent of the parameters of the reference electrode. Moreover, this electrode does not need to be hermetically isolated from the measuring electrode.

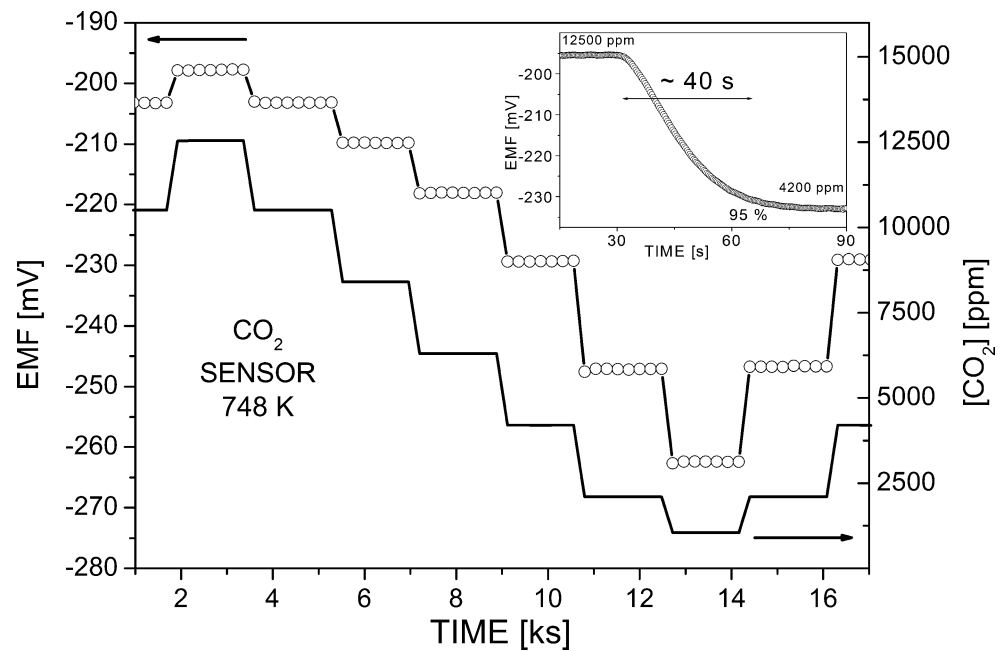
Table 3 Performance of electrochemical sensors type III for CO₂

Cell structure <i>Me</i> , Ref SE Sens CO ₂ , O ₂ (air) <i>Me'</i>	Sub-type	Operating temperature (°C)	Measured concentration (ppm)	Response time (s)	Reference	Year
Ag $-\text{Al}_2\text{O}_3 \text{Me}_x\text{CO}_3 \text{CO}_2, \text{O}_2, \text{Ag}$	IIIb	400–500	$4,000-4.5 \times 10^5$	150–280	[63]	1986
<i>Me</i> =Li	IIIa			350–2,000		
<i>Me</i> =Na	IIIb			170–1,200		
<i>Me</i> =K	IIIb			150–750		
<i>Me</i> =Cs	IIIb			170–900		
<i>Me</i> =Ca	IIIa			300	[80]	1987
Au, O ₂ NASICON or $\beta\text{-Al}_2\text{O}_3 \text{Na}_2\text{CO}_3 \text{CO}_2, \text{O}_2, \text{Au}$		320–550	$10-4.7 \times 10^4$	120	[92]	1993
Pt, O ₂ NASICON Na ₂ CO ₃ CO ₂ , O ₂ , Pt		370–520	100–10,000	60	[87]	1992
		450	2–10,000		[106]	1996
Pt, Au–Pd, O ₂ , CO ₂ NASICON Na ₂ CO ₃ CO ₂ , O ₂ , Pt	IIIa	380–450	150–10,000		[80]	1987
Au, O ₂ YSZ NASICON Na ₂ CO ₃ CO ₂ , O ₂ , Au		520–730	$200-5.5 \times 10^5$		[84]	1991
		610	100		[88]	1992
Pt, O ₂ CSZ (film) NASICON Na ₂ CO ₃ CO ₂ , O ₂ , Au	IIIa	560–650	10^4-10^5	600	[68]	1990
Na Na ⁺ – β/β'' – Al ₂ O ₃ Na ₂ CO ₃ , CO ₂ , O ₂ , Pt		150	10^4 to 6×10^5	below 60	[85]	1991
Na Na ⁺ – β/β'' – Al ₂ O ₃ Na ₂ CO ₃ , CO ₂ , O ₂ , Pt		450	$5-8 \times 10^5$	60	[69]	1992
Pt, CO ₂ , O ₂ Li ₂ CO ₃ Li _{1.3} Al _{0.3} Ti _{0.7} (PO ₄) ₃ Li ₂ CO ₃ , CO ₂ (<i>p</i>), O ₂ , Pt	IIIa	150–550	$80-10,000$	below 60	[81]	1990
Pt, O ₂ NASICON BaCO ₃ –Na ₂ CO ₃ (1.7:1 mol) CO ₂ , O ₂ , Pt	IIIa	650	4–400,000	8	[82]	1990
		550			[86]	1991
					[89]	1992
Pt, air NASICON Li ₂ CO ₃ –CaCO ₃ (1.8:1 mol) CO ₂ , air, Pt	IIIb	450–600	250–2,000	8	[90]	1992
		500	100–100,000	8	[83]	1990
			100–2,000	10–50	[108]	1997
Pt, air NASICON Li ₂ CO ₃ –BaCO ₃ CO ₂ , air, Au		350–600	20–10,000	8	[93]	1993
Pt, air NASICON Li ₂ CO ₃ –BaCO ₃ CO ₂ , air, Pt		350–450	300–5,000	10	[98]	1995
Pt, O ₂ ZrO ₂ -based SE CO ₂ , N ₂ , Pt	IIIc	725–850	5–80% in N ₂		[91]	1992
Pt, O ₂ Y–ZrO ₂ CO ₂ , N ₂ , Pt		725–850	5–80% in N ₂		[99]	1995
Au, O ₂ , CO ₂ Li ₂ CO ₃ +Li ₂ O LiTi ₂ (PO ₄) ₃ +0.2 Li ₃ PO ₄ Li ₂ CO ₃ +Li ₂ O CO ₂ (<i>p</i>), O ₂ , Au	IIIa	650	80–13,000		[94]	1993
				several min	[100]	1995
Pt, O ₂ MgZr ₁₄ (PO ₄) ₆ M ₅ CO ₃ CO ₂ , O ₂ , Pt; <i>M</i> =Na; Mg–Ca (1:1)	IIIb	400–500	$10-10^6$	few min	[96]	1994
Pt, O ₂ Mg _{1.15} Zr ₄ P _{5.7} Si _{0.3} O ₂₄ M ₅ CO ₃ CO ₂ , O ₂ , Pt; <i>M</i> =Na; K		300–500	$5,000-6 \times 10^5$	below 5 min	[101]	1995
Pt, air (+CO ₂) Mg–ZrO ₂ Li ₂ CO ₃ CO ₂ (<i>p</i>), air, Au	IIIc	400–600	100–1,000	Several tens	[97]	1994
		500–650		10	[102]	1995
Pt, air (+CO ₂) LaF ₃ Li ₂ CO ₃ CO ₂ (<i>p</i>), air, Au		400–450	40–2,000	10–20	[95]	1993
					[103]	1995
Au, O ₂ , CO ₂ Li ₂ CO ₃ +5 mol% Li ₃ PO ₄ +25wt% Al ₂ O ₃ CO ₂ , O ₂ , Au		300–600	10–1,000	10–30 min	[104]	1995
Au, O ₂ Na ₂ Ti ₆ O ₁₃ –Na ₂ Ti ₃ O ₇ (or –TiO ₂) Na – β/β'' – Al ₂ O ₃ Na ₂ CO ₃ CO ₂ , O ₂ , Au	IIIa	500–750	$740-9.5 \times 10^5$	few s	[98]	1994
					[105]	1995
					[107]	1996

Pt, air K ₂ O–Sm ₂ O ₃ –6SiO ₂ K ₂ CO ₃ CO ₂ , O ₂ , Au	IIIa	300–500	10–10,000	240	[109]	1997
Au, Na _{0.9} CoO _{2-y} NASICON Na ₂ CO ₃ CO ₂ , air, Au	IIIa	500	10 ³ –8 × 10 ⁴	1–40 min	[110]	1998
Pt, O ₂ YSZ Na ₂ O–Al ₂ O ₃ –4SiO ₂ Na ₂ CO ₃ CO ₂ , air, Pt	IIIc	470	10–10 ⁴	2 min	[111]	1998
Au Li ₃ Zr ₂ S ₂ PO ₁₂ Li ₂ CO ₃ –K ₂ CO ₃ –Na ₂ CO ₃ CO ₂	IIIb	420	10 ³ –10 ⁴	15–20 s	[127]	2005
Pt, O ₂ YSZ[(β + β′)] Al ₂ O ₃ Na ₂ CO ₃ CO ₂ , O ₂ , Au	IIIc	400–600	65–10 ⁴	ca. 30 min	[112]	2000
Pt, O ₂ YSZ Sc ₂ (WO ₄) ₃ Li ₂ CO ₃ CO ₂ , air, Pt	IIIc	550	200–5 × 10 ⁴	few min	[114]	2000
Au–Pd, O ₂ NASICON Na ₂ CO ₃ –BaCO ₃ CO ₂ , Air, Pt	IIIa	600–700	250–10 ⁴	several min	[115]	2001
Pt, air NASICON Na ₃ PO ₄ –NaHCO ₃ –Na ₂ CO ₃ CO ₂ , air, Au	IIIa	30	300–3,000	5 min	[117]	2000
Au LiCoO ₂ +5 mol% Co ₃ O ₄ Li _{2.88} PO _{3.73} N _{0.14} Li ₂ CO ₃ CO ₂ , air, Au	III a	400, 500	200–3,000	20 s	[118]	2001
Au, O ₂ LiFeO ₂ –LiFe ₅ O ₈ Li ⁺ –glass conducting Li ₂ CO ₃ –Li ₃ PO ₄ CO ₂ , air, Au	IIIa	500	350–10 ⁵	30 s	[121]	2003
Au, Na _x CoO ₂ NASICON Li ₂ CO ₃ –BaCO ₃ + In ₂ O ₃ –SnO ₂ CO ₂ , air, Pt	IIIb	30	300–3,000	below 3 min	[120]	2001
Pt, CO ₂ (p _o) BaCO ₃ –Na ₂ CO ₃ Na–β–Al ₂ O ₃ NASICON CO ₂ , air, Pt	IIIa	400–600	10 ³ –10 ⁶	50–70 s	[128]	2005
Pt, air NASICON Li ₂ CO ₃ –BaCO ₃ CO ₂ , air, Au	IIIb	400–500	100–1,000	40 s	[122]	2003
Pt Na ₂ Ti ₆ O ₁₃ –Na ₂ Ti ₃ O ₇ (TiO ₂) NASICON Li ₂ CO ₃ –BaCO ₃ CO ₂ , air, Pt	IIIb	300–500	100–12,600	35	[123]	2003
Pt Na ₂ Ti ₆ O ₁₃ –Na ₂ Ti ₃ O ₇ (TiO ₂) NASICON Na ₂ CO ₃ –BaCO ₃ CO ₂ , air, Pt	IIIa	500	10 ³ –10 ⁵	Few mn	[124]	2003
Pt, CO ₂ (p _o), air LISICON Li ₂ CO ₃ CO ₂ , air, Pt	IIIa	500	500–8,000	below 10 min	[125]	2004
Pt, O ₂ Na ₂ Ti ₆ O ₁₃ –TiO ₂ NASICON Na ₂ CO ₃ –BaCO ₃ CO ₂ , air, Pt	IIIa	500–600	370–10 ⁴	below 30 min	[126]	2005
Pt NASICON Li ₂ CO ₃ +Ln ₂ O ₃ CO ₂ , air, Au	IIIb	460			[129]	2006
Ln=La, Pr, Nd, Sm, Eu, Gd, Y					[130]	2007
Au Li ₂ TiO ₃ –TiO ₂ Li ₃ PO ₄ –SiO ₂ Li ₂ CO ₃ –BaCO ₃ CO ₂ , air, Au	IIIa	450, 500	500–5,000	20–27 s	[131]	2007
					[133]	2008
					[132]	2007

Me, Me' Metal; *Ref* reference electrode; *SE* solid electrolyte; *Sens* sensing electrode; *CSZ* Cubic Stabilized Zirconia

Fig. 7 Transient response at 773 K of type IIIa CO₂ sensor containing Na₂CO₃–BaCO₃ and NASICON as the auxiliary phase and the solid electrolyte, respectively. The response time determination of the sensor is shown in the inset



This fact gives a huge opportunity to simplify the construction of the sensor. Depending on whether the two electrodes are to be isolated or not, the planar or tubular sensors were proposed (Fig. 9a and b, respectively).

Non-Nernstian behavior of potentiometric sensors

According to the working mechanisms of the potentiometric sensors presented above, the dependence of the sensor

signal, EMF, vs partial pressure of the detecting gas, should be in agreement with the Nernst equation (see Eqs. 2, 12, 14, 35, and 43):

$$E = E^{\circ} + \frac{RT}{nF} \ln(p \times \alpha) \quad (46)$$

where: p —partial pressure of the detecting gas, α —parameter determining the activity of gas at the reference electrode (e.g., $\alpha = 1/p_0$) and the activity of other species taking part in electrode reactions (see, for example, Eq. 22).

Fig. 8 Potentiometric chain of a type IIIc gas sensor with cation conducting electrolyte (a) and anion conducting electrolyte (b)

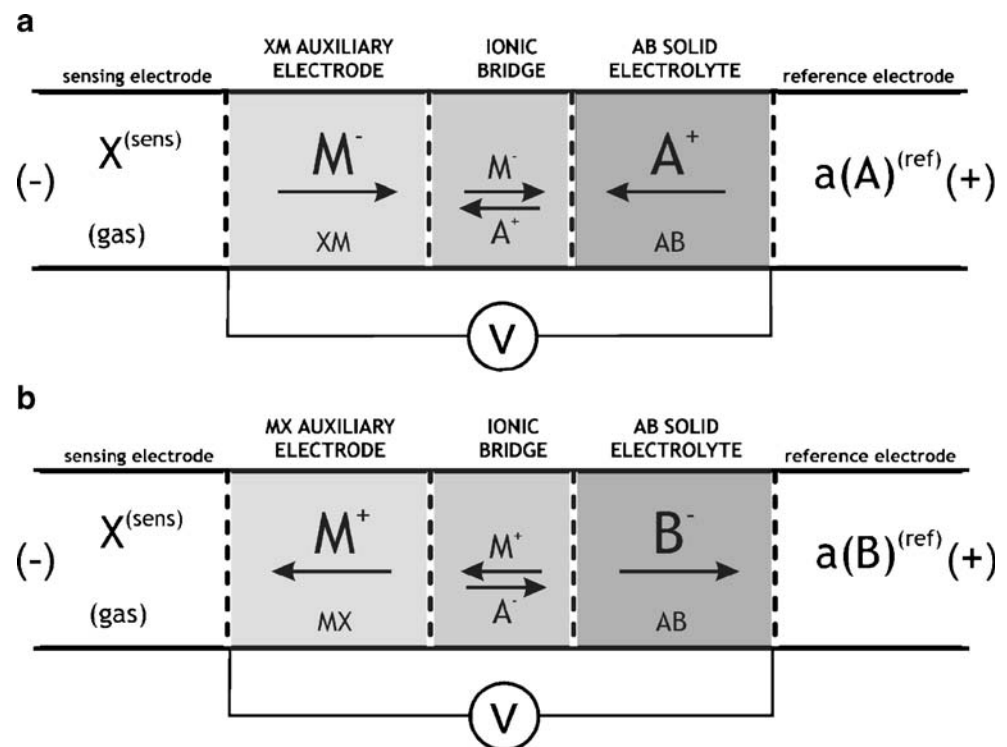
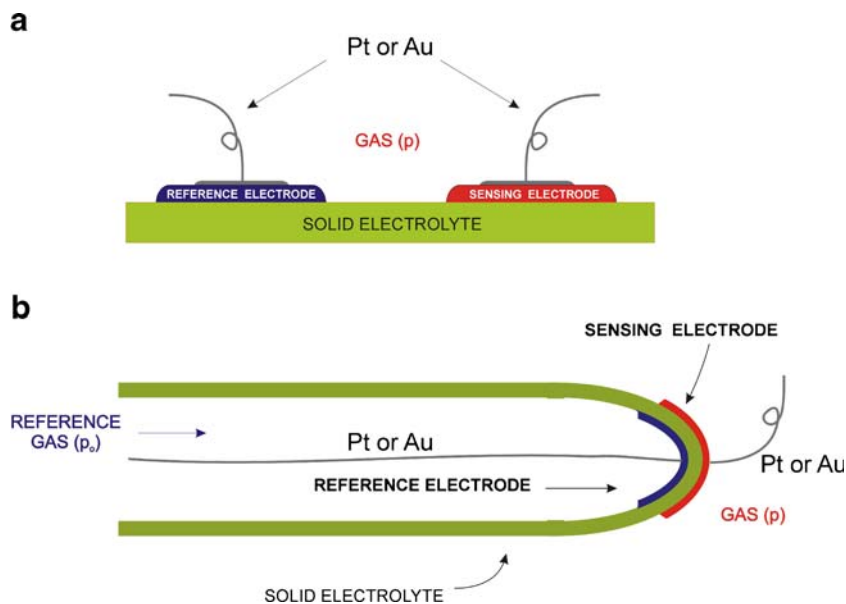


Fig. 9 Structure of planar (a) and tubular (b) potentiometric sensors



It is worth mentioning that both parameters E° and n in Eq. 46 exhibit precise physical meaning. Parameter E° involves free enthalpy of the cell reaction (see e.g., Eqs. 24 and 36), while parameter n should assume an integral value.

However, discrepancies from the theoretically predicted relationship given by Eq. 46 are observed, as illustrated in Fig. 10. The observed discrepancies in the experimental dependencies E vs p from theoretical relationship given by Eq. 46 may be explained in several ways:

- Local equilibria of the reactions which occur at the electrodes, the AP and the IB, are not established. This explanation may be particularly valid at lower operating temperatures. It is to be expected that a gradual change from non-Nernstian to Nernstian behavior with

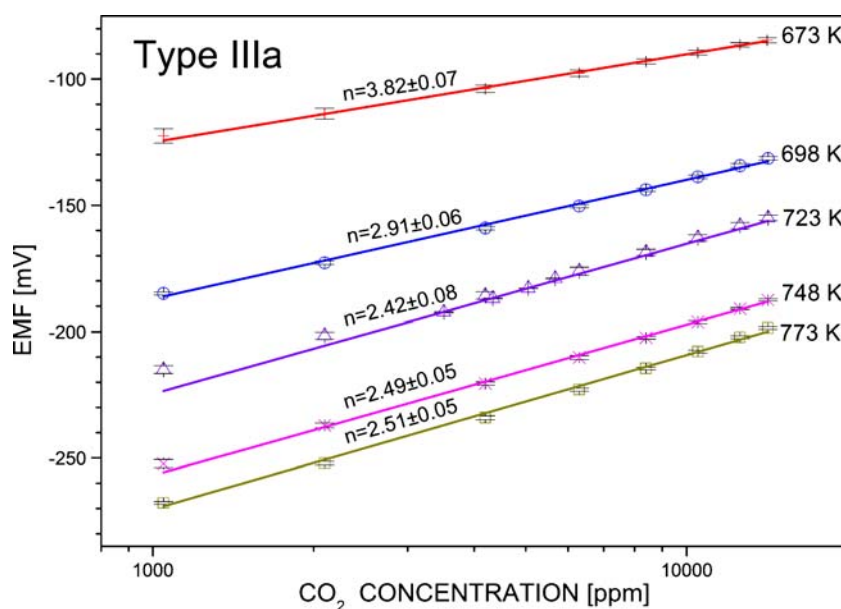
a temperature increase takes place. The observed changes of the parameter n in Fig. 10 remain in agreement with this expectation.

- Two or more competitive potentiometric reactions occur simultaneously at the sensing electrode. This phenomenon is known as ‘mixed potential.’ This issue will be discussed in greater detail in the next chapter.
- The solid electrolyte exhibits no negligible component of the electronic conductivity. Taking into consideration the following relationship [134]:

$$E_{\text{exper}} = t_{\text{ion}}E \tag{47}$$

where E_{exper} and E denote experimental and theoretical values of the EMF, respectively. According to Eqs. 46 and

Fig. 10 Experimental dependence of EMF vs $p(\text{CO}_2)$ for the CO_2 sensor containing $\text{Na}_2\text{CO}_3\text{--BaCO}_3$ and NASICON as the auxiliary phase and the solid electrolyte, respectively. The determined values of n parameters are given for every measured temperature

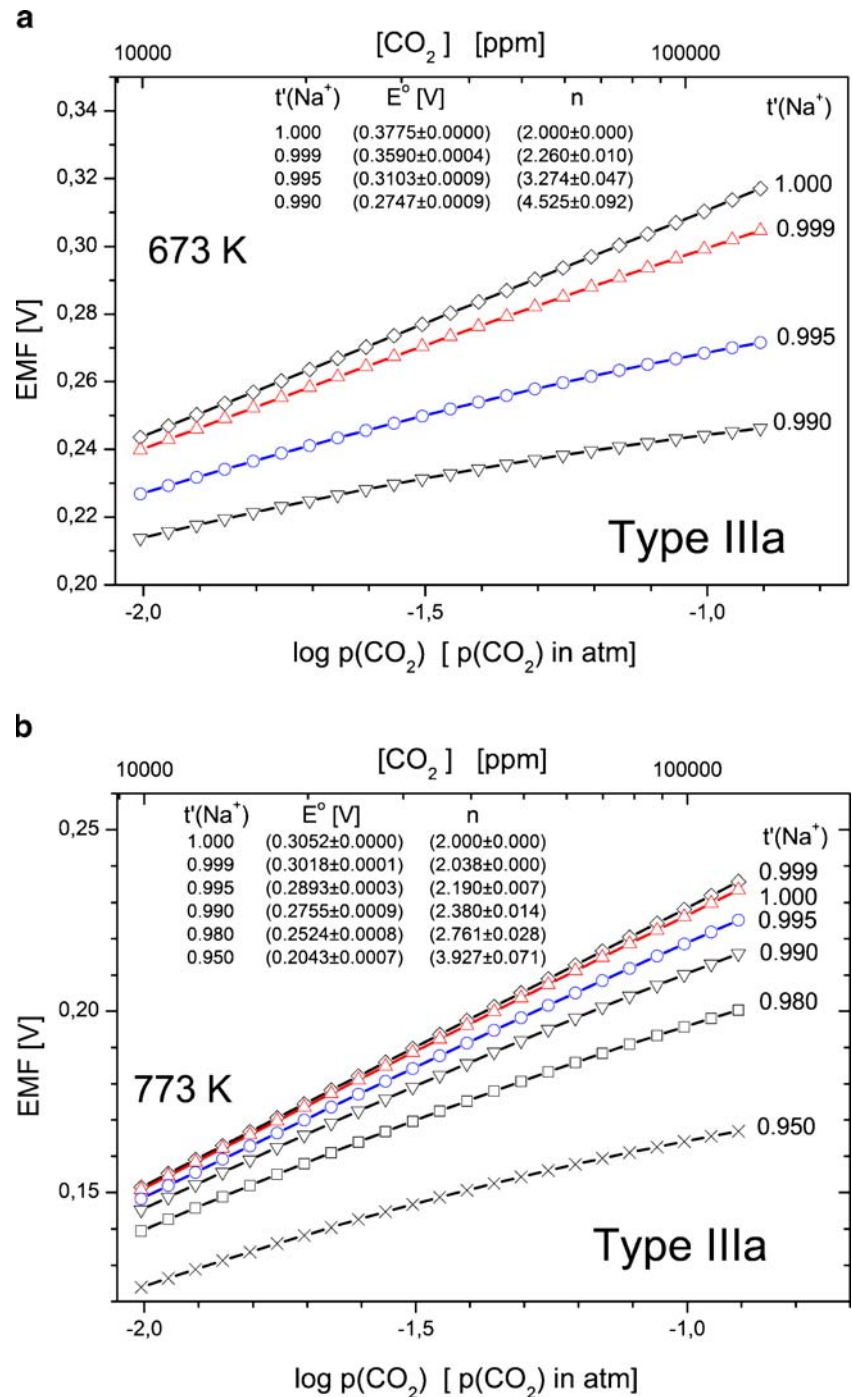


47, the experimentally determined parameter n can assume non-integral values. However, Eq. 47 may be treated as only semi-quantitative because it is assumed that the ionic transference number is constant in any place of the solid electrolyte.

A more precise explanation for the EMF behavior was first proposed by Näfe et al. [135–137] for cells with β -alumina as

the solid electrolyte. Taking into consideration Näfe's approach, the theoretical values of EMF were calculated for different arbitrarily chosen ionic transference numbers, t' (Na^+). Figure 11 shows the results of calculations for 673 K (Fig. 11a) and 773 K (Fig. 11b) for the sensor as in Fig. 10. As can be seen, even low electronic transference number (5×10^{-3}) leads to the non-Nernstian behavior (n parameter other

Fig. 11 Theoretical EMF vs p (CO_2) for arbitrarily chosen transference numbers of Na^+ ions at the auxiliary phase–solid electrolyte interface, $t'(\text{Na}^+)$, for 673 K (a) and 773 K (b). The calculated E° and n parameters for different $t'(\text{Na}^+)$ are also shown



than 2). This influence of electronic transport component is more significant at low temperatures.

- More than one type of ions is mobile in the solid electrolyte. This is expected in particular for hydrogen sensors using high-temperature proton conductors. In that case, both hydrogen and oxygen ions can participate in charge transport through the solid electrolyte [39, 138].
- Surface effects connected with contact potential difference [139].
- There are no negligible interactions between species taking part in electrode reactions. In this case, the activities of the reacting substances instead of their concentrations (expressed in partial pressures) should be placed in Eq. 46.
- The influence of high electrode polarization resistance.

Mixed potential gas sensors

A non-Nernstian behavior of zirconia-based oxygen sensors was first observed by Fleming [140].

He observed a deviation in a theoretically predicted dependence of EMF vs oxygen partial pressure (Eq. 2) in the presence of CO in a gas mixture. According to Fleming, CO may affect sensor performance in two ways. First, CO may decrease the local concentration of oxygen at the sensing electrode as a result of the reaction:



Furthermore, there is also a possibility of direct interaction between CO and the sensing electrode:



This means that apart from the potentiometric reduction given by Eq. 1, the oxidation described by Eq. 49 takes place simultaneously at the sensing electrode. The steady potential of this electrode, known as the mixed potential, is established when the rates of both mentioned reactions are equal. Taking into consideration the fact that both competing potentiometric reactions (1) and (49) take place at a three-phase boundary (named as TPB): gas phase, solid electrolyte, and metallic electrode, their rates are strongly related to chemical composition and microstructure of the electrode, as well as the solid electrolyte. Moreover, the catalytic activity of the electrode material controls the reaction rates and the resulting mixed potential. This was confirmed through experimental work by Wachsmann et al. [141, 142]. They concluded that the EMF of the mixed-potential cells is compatible with the changes in the Fermi level induced by chemisorption of the oxidizing or reducing gas in the auxiliary phase, connected to the sensing electrode. However, at present, our knowledge

about the working mechanism of this group of gas sensors is rather limited [143–146].

In order to improve the catalytic activity of the sensing electrode towards the detecting gas, several materials have been proposed as the auxiliary phase. Typical examples of the mixed potential sensors several gases are collected in Table 2 of [145]. Some examples not included in [145] are presented in Table 4 [147–168].

Potentiometric sensors for the measurement of environmental gases

Carbon dioxide sensors

Global warming (the green-house effect) has become a serious, worldwide problem that adds to environmental deterioration caused by acid precipitants and the increase of UV radiation due to depletion of stratospheric ozone. The reason for this effect is the emission of gases such as CO₂, methane, freon, and NO_x into the atmosphere. Of those gases, CO₂ has the strongest impact due to the enormous quantity of its emissions into the atmosphere. The most effective way to decrease CO₂ emission is to reduce the amounts exhausted from individual emission sites. For this purpose, the development of simple and inexpensive sensors is vital. Most proposed chemical CO₂ sensors are of the potentiometric type. Those sensors are either type II or III. There are no potentiometric CO₂ sensors of type I, since a solid electrolyte with mobile carbonate anions (CO₃²⁻) is not known. Several types of potentiometric CO₂ sensors have been reviewed above (Tables 2, 3, and 4). The commercial CO₂ potentiometric sensor is already available; namely, model TGS4160 sensor is produced by Figaro Engineering, Japan.

Nitrogen oxide potentiometric sensors

There is a growing demand for cheap, easy to operate gas sensors for in situ measurements of NO_x (NO and NO₂) in combustion exhausts with regard to the conservation of global environment. Sensors for the detection of NO_x are also useful for analytical purposes, for example in electronic noses, since biological and food processes often produce gas mixtures containing nitric oxide. Nitrogen oxides are known to cause air pollution problems, such as acid rain and photochemical smog, as well as damage to human nerves and the respiratory system. It is mainly emitted from automobiles (especially those using lean-burn and diesel engines), stationary combustion facilities and homes. The NO_x in combustion exhausts is usually present in concentrations of up to several hundred parts per million (the threshold limit values for human exposure are 3 and 25 ppm for NO₂ and NO, respectively [169]). As opposed to nitrogen dioxide, nitrogen

Table 4 Mixed potential sensors

Gas	Cell structure <i>Me</i> , Ref SE Sens CO ₂ , O ₂ (air) <i>Me'</i>	Operating temperature (°C)	Measured concentration (ppm)	Reference	Year
CO	Pt, O ₂ Ce _{0.8} Gd _{0.2} O _{1.9} CO, O ₂ , Au	550, 600	0–500	[147]	2000
	Pt, O ₂ Ce _{0.8} Gd _{0.2} O _{1.9} LaMnO ₃ CO, O ₂ , Au	600		[148]	2002
	Pt, air YSZ Y _{0.16} Tb _{0.30} Zr _{0.54} O ₂ CO, air, Au	600, 700	0–500	[149]	2002
	Pt, O ₂ Na-β Al ₂ O ₃ Au	250–600	10–200	[150]	2004
	Au, air YSZ WO ₃ , +LaFeO ₃ CO, air, Au	550–650	20–1,000	[151]	2005
	Pt(Au), CO, O ₂ YSZ Nb ₂ O ₅ CO, O ₂ , Pt (Au)	450–650	1,000	[152]	2008
CO ₂	Pt, La _{0.8} Pb _{0.2} CoO ₃ NASICON NdCoO ₃ CO ₂ , O ₂ Au	200–300	100–2,000	[153]	2000
	Pt, La _{1-x} Sr _x MnO ₃ NASICON Na ₂ CO ₃ -Ba(Sr)CO ₂ CO ₂ , O ₂ Au	150–500	1–10 ⁴	[154]	2003
NO _x	Au, air YSZ WO ₃ , +LaFeO ₃ NO ₂ , air, Au	550–650	20–1,000	[155]	2004
				[156]	2005
	Pt, O ₂ YSZ (Al _{0.2} Zr _{0.8}) _{20/19} Nb(PO ₄) ₃ (Gd _{0.9} La _{0.1}) ₂ O ₃ -LiNO ₃ NO, air, Au	250	200–2,000	[157]	2005
	Pt, O ₂ ZrO ₂ +8 mol% Sc ₂ O ₃ CuO+CuCr ₂ O ₄ NO ₂ , O ₂ , Pt	518–659	10–500	[158]	2006
	Pt, O ₂ YSZ ZnFe ₂ O ₄ NO _x , Pt	600–700	50–450	[159]	2004
	Au NASICON Pr ₆ O ₁₁ -SnO ₂ H ₂ S, air, Au	200–400	6–50	[160]	2007
CH _x	Pt, air YSZ In ₂ O ₃ +MnO ₂ CH _x , O ₂ , Au	600	0–500	[161]	2003
	Pt, air YSZ SrCe _{0.95} Yb _{0.05} O _{3-y} CH _x , O ₂ , Au	600	0–1,000	[162]	2001
	Ag Ag ₂ O α-Zr(HPO ₄) ₂ CH _x , air, Pt	200–300	0–100	[163]	2001
	Au, N ₂ Al-Na ₃ PO ₄ CH ₄ , Au	600	1×10 ⁴ to 3×10 ⁴	[164]	2002
	Pt, O ₂ YSZ La _{0.8} Sr _{0.2} CrO ₃ C ₃ H ₆ , N ₂ , Pt	500–600	0–1,250	[165]	2003
	Au, O ₂ YSZ La _{1-x} Sr _x Cr _{1-y} Ga _y O _{3-δ} CH _x , Au	600–800	0–8×10 ³	[166]	2004
	CH _x =C ₃ H ₆ , C ₃ H ₈ , C ₇ H ₈ (toluene)			[167]	2004
	Au Na ₂ CO ₃ Na-ZSM-5 (SiO ₂ /Al ₂ O ₃ =27) C ₃ H ₈ , O ₂ , Au	400	200–4,000	[168]	2006

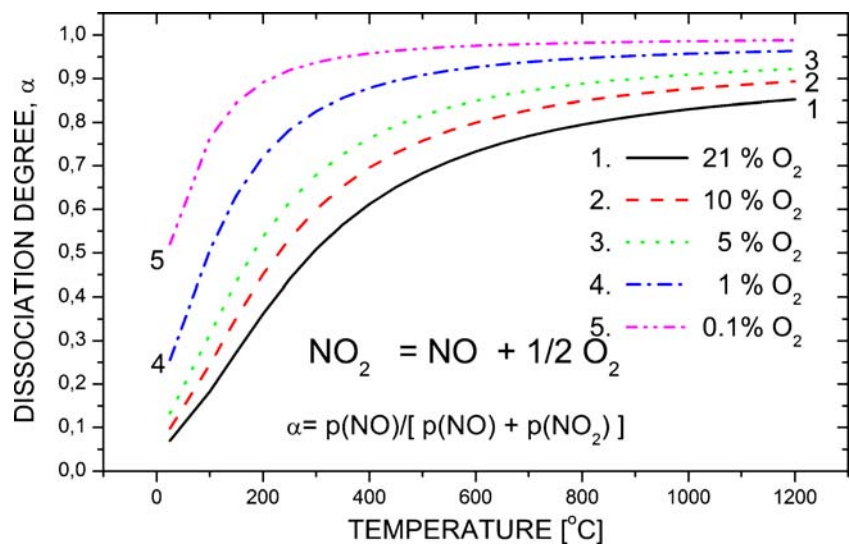
Me, *Me'* Metal; *Ref* reference electrode; *SE* solid electrolyte; *Sens* sensing electrode; Na-ZSM-5 – Na⁺ ion conducting zeolite (aluminumsilicate)

oxide is not highly toxic, but it has a strong impact on the destruction of stratospheric ozone [170]. The gas composition of NO_x is determined by temperature and *p*(O₂). Figure 12 illustrates the equilibrium composition of a NO_x gas mixture as a function of temperature at several *p*(O₂).

Measurements of NO_x concentration have so far been done by means of spectroscopic instruments based on chemical

luminescence or infrared absorption. However, such instruments cannot fit well in on-site feedback control systems because of time-consuming analytical procedures, bulky size, and high costs. It is beyond any doubt that only a gas sensor which could determine the concentration of NO_x within a range required by a particular application, with precision and negligible cross-sensitivity to other gases present in studied

Fig. 12 Equilibrium composition of NO_x gas mixture as a function of temperature at several *p*(O₂)



gas phase, may satisfy the growing demands of modern technology and environmental protection.

Since Gauthier and co-workers reported the possible use of an alkali sulfate-based gas sensor for detecting SO₂ gases in air [46], potentiometric gas sensors for other gases have been reported, with similar principles of operation. Among them, the potentiometric NO_x sensors were also reported [171–192]. The potentiometric NO_x gas sensor has the following solid-cell structure:



where Me—metallic connections, usually Pt or Au, SE—solid electrolyte, AP—the auxiliary phase.

NASICON [173, 175, 176, 181], sodium β/β"-alumina [172–174], Ag β/β"-alumina [171], and stabilized zirconia [179] were used as solid electrolytes. As the auxiliary phase, simple barium nitrate [46], sodium [174], silver [171], and sodium nitrite [174] have been proposed at the very beginning. The replacement of nitrate phase with nitrite improves NO₂ sensing characteristics and decreases the detection limit (to about 0.2 ppm) [183]. However, the low melting points of these salts (Table 5 [183]) imposes some limitations on the selection of suitable solid electrolytes and working temperatures of the sensor.

As can be seen from Table 5, the operation temperature in the case of NaNO₃ as the auxiliary phase should be lower than 307 °C. In addition, in that case, the sensor is incapable of NO detection. Higher temperature operation is achieved through the use of Ba(NO₃)₂ as the auxiliary sensing electrode [175]. Using more complex phases such as NaNO₂–Na₂CO₃ [184] or NaNO₂–Li₂CO₃ [100], the performance of the sensor, especially with diluted NO₂, may be improved.

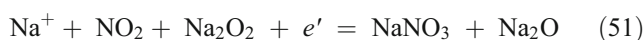
Assuming that we have a Na⁺ ionic conductor (e.g., NASICON or Na–β –alumina) as the solid electrolyte and NaNO₃ as the auxiliary phase, the electrode reactions may be expressed in a way similar to that shown for CO₂ sensors.

Table 5 Melting point of several nitrates and nitrites

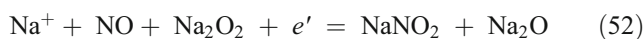
NITRATES		NITRITES	
Formula	Melting point (°C)	Formula	Melting point (°C)
LiNO ₃	264	LiNO ₂ ·H ₂ O	>100
NaNO ₃	307	NaNO ₂	271
KNO ₃	334	KNO ₂	440
Mg(NO ₃) ₂ ·2H ₂ O	129	Mg(NO ₂) ₂ ·3H ₂ O	d100
Ca(NO ₃) ₂	561	Ca(NO ₂) ₂ ·H ₂ O	d100
Ba(NO ₃) ₂	592	Ba(NO ₂) ₂	d217
AgNO ₃	d444	AgNO ₂	d140

d Decomposes

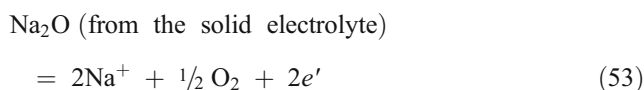
Hence, the reactions at the sensing electrode are [175]:



and:



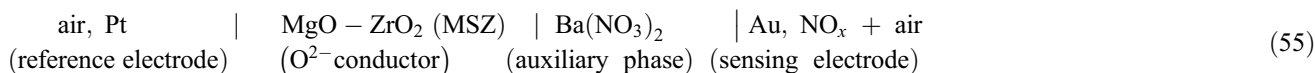
while the counter electrode reaction is:



So, under the constant *p*(O₂), we have:

$$E = E^o + \frac{RT}{F} \ln[p(\text{NO}_2) \text{ or } p(\text{NO})] \quad (54)$$

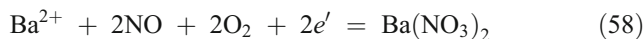
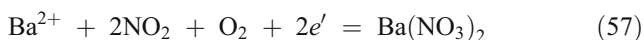
Similar processes may be proposed for other cation-conducting solid electrolytes like Ag- or Ba-β"-alumina (mobile Ag⁺ or Ba²⁺ ions, respectively) or BaZr₄P₆O₂₄ (Ba²⁺ mobile ion). Slightly different processes have been proposed for anion-conducting solid electrolytes as LaF₃ (F⁻ mobile ion) or Y–ZrO₂ (O²⁻ mobile ion). The latter case was considered by Kurosawa et al. [180]. These authors investigated the following solid cell:



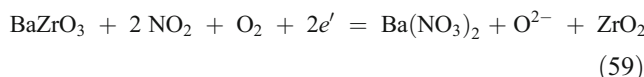
The authors postulated that a compound containing both Ba²⁺ and O²⁻ is formed at the phase interface between MSZ and Ba(NO₃)₂, according to the reaction:



At the sensing electrode, the following reactions were suggested:



By combining Eqs. 56 and 57 or 56 and 58, we have a resulting electrode reaction. For example, in the case of NO₂ gas sensing, we get:



The formed oxygen ions at the sensing electrode diffuse through the MSZ solid electrolyte to the reference electrode, where the following reaction occurs:

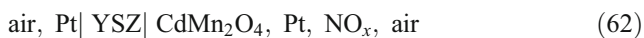


A conventional approach to the electrode equilibria (Eqs. 59 and 60) leads to the following expression for EMF:

$$E = E^o + \frac{RT}{F} \ln[p(\text{NO}_2)] + \frac{RT}{4F} \ln \frac{p(\text{O}_2)^{(s)}}{p(\text{O}_2)^{(r)}} \quad (61)$$

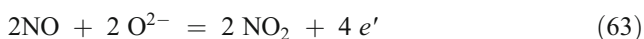
where $p(\text{O}_2)^s$ and $p(\text{O}_2)^r$ denote partial pressures of oxygen at sensing and reference electrodes, respectively.

The mechanisms of particular sensors, described above, ignore the role of chemisorption phenomena on sensor operation. Due to the chemisorption of even very diluted gases from the surrounding atmosphere, a drastic change in the EMF of zirconia oxygen gas sensor [185] takes place. Miura et al. [185, 186] reported the results concerning several materials suitable for use as auxiliary phases. Among 12 kinds of spinel-type oxides tested, CdMn_2O_4 was found to be the best material for NO_x sensing. The following sensor with CdMn_2O_4 :



showed excellent response characteristics to both NO (up to 600 ppm) and to NO_2 (up to 200 ppm), at temperatures 500 and 600 °C. The EMF of the device was an almost linear function with the logarithm of NO and NO_2 concentration, with negative and positive slopes for NO and NO_2 , respectively. The sensing mechanism involving mixed potential was derived from the polarization curves.

At the reference electrode, the equilibrium described by Eq. 60 is established, while at the sensing electrode, there is the following local equilibrium:



An interesting attempt has been made with regard to this matter in the development of a thick-film ZrO_2 -based sensor [192]. The principle of operation of this sensor is based on the removal of an amount of decomposed oxygen which is proportional to that of NO. The problem with this indirect detection is that a certain optimal oxygen partial pressure should be maintained for the decomposition to occur. This requires simultaneous monitoring of the ambient $p(\text{O}_2)$ level. In spite of the linear output characteristics of the sensor and a wide measuring range of NO concentrations (0–2,000 ppm) at temperatures up to 700 °C, this sensor suffers from a high error of measurement (ca. 8%) and still needs sufficient improvements. As mentioned above, zirconia-based sensors are versatile with regard to material selection and device construction, and by designing the auxiliary phase or sensing electrode appropriately,

they can be upgraded to show excellent sensing performance under specific conditions. With these attractive features, this group of NO_x sensors appears to be the one best suited to sensing not only NO_x but also other oxygenic gases. Unfortunately, there are still many problems related to these devices [13]. Some of them are as follows:

1. It has been proven that, in many NO_x sensing devices, the EMF is totally independent of the coexisting $p(\text{O}_2)$ and is inconsistent with the electrode reactions so far assumed. The participation of peroxides or some excess oxygen is suspected.
2. The materials for the auxiliary phase or sensing electrode, mostly composite, have so far been developed empirically. The structure and properties of these materials should be characterized carefully in order to establish guidelines for the design of auxiliary phases. Regrettably, we have no reliable criteria for finding and predicting the most useful materials for individual applications.
3. The sensitivity of sensors with mixed potential depends on the chemisorption properties of the auxiliary phase used. In order to improve the basic parameters of such sensors, knowledge about the interface properties of the applied materials is essential.

Mixed potential NO_x sensors were recently the subject of review papers [193, 194]; some examples of such sensors are also collected in Table 4.

Sulfur oxide sensors

Recently, several potentiometric SO_x sensors of type II have been proposed. They used the following metal sulfates, e.g., K_2SO_4 [195–197], Na_2SO_4 [53, 198], Li_2SO_4 [199, 200], Ag_2SO_4 [201, 202], and $\text{Li}_2\text{SO}_4\text{--Ag}_2\text{SO}_4$ [201, 203, 204] as solid electrolytes. In order to improve sensor characteristics caused by undesirable properties of the used solid electrolytes (phase transformations [205–207] and their low electrical conductivities), more complex sulfate systems and some non-sulfate additions were used, e.g., $\text{Na}_2\text{SO}_4\text{--Y}_2(\text{SO}_4)_3\text{--}(\text{Li}_2\text{SO}_4)$ SiO_2 [47, 138], $\text{Na}_2\text{SO}_4\text{--La}_2(\text{SO}_4)_3\text{--Al}_2\text{O}_3$ [208, 209], $\text{Na}_2\text{SO}_4\text{--NaVO}_3\text{--Ln}_2(\text{SO}_4)_3$ (Ln=Eu, Pr, Y) [210].

There are also some known type III SO_x sensors using $\text{Na}(\text{Ag})\text{--}\beta\text{''-alumina}$ [211–215], or NASICON [216–219] as solid electrolytes. These sensors are without any auxiliary phase added intentionally. However, the detailed studies of the phase composition of these sensors revealed that Na_2SO_4 , which plays the role of the auxiliary phase, is formed at the surface of the Na-conducting solid electrolyte through its direct reaction with gaseous SO_2 and O_2 [220]. The sensors containing both the solid electrolyte and the auxiliary phase (added intentionally) are described in [221]

(NASICON/Na₂SO₄) and [222] Lalauze and Rekas (unpublished; β-Al₂O₃/Na₂SO₄).

The principle of SO_x detection with these solid electrolytes was comprehensively described in various papers [223, 224]. These sensors repeatedly responded well to SO_x, but they appeared to suffer from sluggish responses and from the chemical instability of the solid electrolytes in atmospheres containing SO_x. Furthermore, all the sensors reported to date require an independent determination of *p* (O₂) in order to independently calculate the concentrations of both SO₂ and SO₃.

More recently it has been found that a stabilized ZrO₂ tube coated with K₂SO₄ [194] or Li₂SO₄–CaSO₄–SiO₂ [223, 225, 226] as auxiliary phases, can be utilized as an SO_x sensor with a reasonably good response and a stable output. However, both the chemical and mechanical stability of these sensors proved poor during extensive tests. Furthermore, these sensors have a working temperature range restricted to 600–800 °C and are still far from meeting the industry demands for a reliable sensor [13].

From a practical point of view, no work has been done on a solid-state sensor that would measure SO_x concentration under industrial conditions. Instead, most investigations have been focused on potentiometric sensors which measure equilibrium SO_x concentration in air, from which the SO₂ concentration is then calculated from the equilibrium constant of the reaction [227]:



The most attractive SO₃–SO₂ solid electrolyte sensor has the following properties and features [224]:

- operation temperature in the range 800–1,200°C
- in situ operation with no umbilical tubing
- no external housing or gas train
- no external reference
- no gas-handling systems
- manifold operation for process control
- no internal seal between measuring and reference electrodes
- no filters for particle-loaded gases

Not a single sensor from those described above can match all these stringent commercial requirements at the same time.

Further development of SO_x sensors has been based on the fact that the zirconia electrolyte should be combined with the composition of the metal sulfates, which plays the role of the auxiliary phase. As follows from the considerations given above (type IIIc), these SO_x sensors need an interfacial compound between the stabilized zirconia and the auxiliary phase to establish a potentiometric chain through the sensor ('ionic bridge'). Furthermore, the results

indicated that the output EMF and the sensitivity of sensor depend not only on the properties of the two gas electrodes but also on the thermodynamic properties of the interfacial compound (see Eq. 44). This suggests that the sensors which have a poor interfacial compound between the zirconia and the metal sulfate have unstable behavior and tend to show sluggish responses to SO_x. This tendency became more obvious as the concentration of SO_x increased [228].

Carbon oxide potentiometric sensors

Carbon monoxide is produced by incomplete combustion. It is commonly found in the exhaust gases from engines or as a product of incorrectly adjusted gas heaters. CO is highly toxic, rendered all the more dangerous by its colorless and odorless character. The development of solid-state CO sensors is therefore very desirable. So far, there have been many reports on CO sensors. Most of them concern semiconductor-type CO sensors, which use mainly SnO₂. However, such devices have significant disadvantages, e.g., high cross-sensitivity to other reducing gases or humidity and poor long-term electrical stability. Moreover, such sensors require laborious calibration, since their electrical conductivity is a complex function of microstructure, chemical composition, mutual relations between surface and bulk properties, and geometrical dimensions.

There is hope that these difficulties may be overcome through the development of potentiometric CO sensors. The first attempts at such sensors were amperometric and used liquid [229] or solid organic [230] electrolytes and, finally, yttria-stabilized zirconia with an attached catalyst layer for the oxidation of CO [231]. Recently, potentiometric zirconia-based sensors have also been proposed [231–238]. According to [235], the use of oxide electrodes with stabilized zirconia, based on a mixed-potential model, is an active and very selective way of detecting CO. The combination of CdO and SnO₂ as electrodes yields an excellent CO sensor. Operating at high temperatures such as 600 °C, this sensor shows very promising sensing characteristics. The times of 90% response of the sensor and the recovery to 200 ppm CO at 600 °C were as short as 8 and 10 s, respectively. The EMF value was linear with the logarithm of CO concentration in the range of 20 to 4,000 ppm. Moreover, the cross-sensitivities to other gases such as H₂, NO, NO₂, CO₂, O₂, and H₂O were small or insignificant [230]. Fortunately, it is noted that the EMF value of the sensor was almost independent of the oxygen concentration in the tested range of 2–21 vol%. The detailed sensing mechanism, long-term stability, and simplification of the sensor are now under investigation.

Another composition of a mixed electrode was proposed by Sorita and Kawano [237, 238]. Using LaMnO₃ with

yttria-stabilized zirconia oxide (YSZ), they constructed a CO sensor working at 400 °C, within 500–7,000 ppm, and a response time of less than 10 s.

Some examples of the potentiometric CO sensors are collected in Table 4. Recently, Fergus [239] has presented the review concerning potentiometric CO sensors.

Hydrocarbon potentiometric sensors

The presence of hydrocarbons in the atmosphere is a potential hazard in many industrial, commercial, and domestic environments. Since hydrocarbons, and mainly methane, are a product of decaying organic matter, they are also found in dangerous quantities in mines, sewers, and waste tips. Most proposed hydrocarbons sensors are either semiconducting (Taguchi Gas Sensors) or microcalorimetric (pellistors).

Hibino et al. [240] proposed a sensor for detecting CH₄ in exhaust gases from gasoline engines. It was constructed from two Pd (porous)|Y–ZrO₂|Au cells, which are attached to each other with their Pd electrodes on the interior side of the assembly. It was proved that CH₄ reacts with O₂ (below 200 ppm) or H₂O (above 200 ppm) on the Pd electrode and that it barely reacts at all on the Au electrode. When sample gases consisting of CH₄, O₂ and H₂O were fed to the sensor at 750 °C, EMF values were generated from one cell and then compensated by potentiometrically pumping O₂ from the other cell. The current applied to the latter cell increased linearly with methane concentration but was not influenced by changing O₂ concentration. This sensor can determine CH₄ concentrations from 50 up to 700 ppm. Recently reported mixed potential hydrocarbon sensors are collected in Table 4 and these are in review paper [239]. However, further investigations are needed to specify the sensing characteristics and long-term stability of such sensors.

Conclusions

The progress in the research and development of potentiometric sensors in the recent years has been very rapid, as research groups made great efforts to make accurate and reliable in situ measurements of various components in gas phases such as O₂, H₂, CO₂, SO_x, NO_x, CH_x, CO, etc. possible.

Generally, potentiometric gas sensors are characterized by high sensitivity and selectivity, as well as long-term stability. The sensitivity and selectivity of those sensors is affected by electrode redox reactions and by rates of simultaneous reactions occurring at electrodes (in the case of mixed potential). Usually, the sensing signal, i.e., the open cell voltage (the equivalent of the EMF), shows a logarithmic dependence on the gas concentration. This

makes it possible to analyze the gas in a wide range of concentrations. An appropriate selection of electrode materials enables the construction of a planar-type cell with sensing and reference electrodes placed in the same compartment and exposed to the same atmosphere. Finally, these sensors can be manufactured in a reproducible manner, thus eliminating the need for expensive individual calibration.

According to the original works on potentiometric sensors, they showed Nernstian behavior. Further studies revealed smaller or larger deviations from the Nernst law. This discovery led to the introduction of a new class of potentiometric sensors, known as mixed-potential sensors. The operation of mixed-potential gas sensors is based on heterogeneous catalytic phenomena. Consequently, enormous so-far knowledge of the heterogeneous catalysis in general and semiconductor chemisorptive gas sensors in particular may be used in order to further develop this class of potentiometric sensors.

However, there are still many problems which need solutions. For example, sensor parts, both solid electrolyte and electrode materials, have frequently been chosen empirically. More general rules or principles of their selection should be established to obtain better sensor parameters. In particular, we need further basic studies on the catalytic activity of both chemical and potentiometric reactions taking part in the sensor. Moreover, further studies are required to better understand the sensor mechanism.

The sensors may be used in a variety of areas, including domestic applications, agriculture, industry, medicine, automobiles, mines, control of gas emissions, leak, fire, etc. Low costs of manufacture, easy maintenance, and small dimensions of the sensors offer the possibility of installing them in many places. As a result, it will be possible to correct control gas atmosphere and to optimize various industrial processes. Other applications for potentiometric sensors still need to be explored.

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