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Electrochemical monitoring of metal ions removal in Fe⁰/H₂O systems: competitive effects of cations Zn²⁺, Pb²⁺, and Cd²⁺

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Abstract

Metallic iron (Fe^0) is a reactive material that is widely used for industrial water treatment. The course of the metal ion removal process using Fe⁰ (iron powder) was monitored electrochemically (differential pulse polarography). As probe species, Zn^{2+} , Pb^{2+} , and Cd²⁺ were selected for their different (1) adsorptive affinity to iron corrosion products (FeCPs), (2) redox properties, (3) precipitation ability at various pH. Batch experiments were carried out with binary $(Zn^{2+}/Pb^{2+}$ and Zn^{2+}/Cd^{2+}) and ternary $(Zn^{2+}/Cd^{2+}/Pb^{2+})$ systems to reveal the mutual interference of these cations. Detailed time monitoring of iron aging for up to 14 days as well as concentration decay of individual removed cations represent important data for mechanistic discussions. The aqueous concentration of Fe^{2+} was also monitored. FeCPs were characterized using X-ray photoelectron spectroscopy (XPS) and scanning electron microscopy (SEM). Results showed that the presence of Pb^{2+} delays the Zn^{2+} removal whereas the presence of Cd^{2+} in solution accelerates its removal. The removal of Pb²⁺ by FeCPs was not affected by the presence of Zn^{2+} and Cd^{2+} , moreover, the Pb²⁺ inhibited the effect of Cd^{2+} on the removal of Zn^{2+} . XPS has proven existence of $Fe₂O₃$ and hydrated Fe oxidic phase, whilst the SEM showed that the original Fe grains were partly dissolved into bufered ambient under formation of fne particles of FeCPs. Results confrm that reductive transformation of any contaminant in a $Fe^{0}/H_{2}O$ system is the consequence and not the cause of iron corrosion.

Graphic abstract

Keywords Heavy metals · Multiple cations · Electrochemistry · Water treatment · Aged zero-valent iron

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Introduction

The presence of heavy metals in wastewater generated from industrial activities such as mining and smelting and battery manufacturing [[1\]](#page-11-0) is one of the most serious environmental problems worldwide. Heavy metals persist in the environment and pose a high risk to ecosystems and human health [\[2\]](#page-11-1). There is a crucial need for low-cost, effective approached to remove heavy metals from wastewater. Metallic iron materials— $Fe⁰$ (or zero-valent iron—ZVI) has been

Table 1 Diversity of experimental conditions (appeared in literature) for batch experiments using metallic iron and various types of FeCPs for Zn^{2+} , Cd²⁺, and Pb²⁺ removal

Type	Quantity/g	pH	$[Zn^{2+}]/$ mmol/dm ³	$\lceil Cd^{2+} \rceil$ / mmol/dm ³	$[Pb^{2+}]$ mmol/ Duration/h Temp/°C dm^3			Volume/ cm^3	Mixing	References
ZVI	$40 - 1000$	$3 - 13$	50 ^b			24	n.s	1000	Shaker	$[14]$
Hematite	$5 - 8$	$2.40-$ 7.10	$\overline{}$	$(100-1000)^a$	$(100-1000)^a$	$0.25 - 2$	RT	100	Shaker	$\left[31\right]$
nZVI	2	4.0 ± 0.2	$0 - 0.5$	$0 - 0.412$	$0 - 0.29$	48	21 ± 2	100	Rot. shaker	[40]
nZVI	0.03	$4 - 10$	1			$0 - 72$	RT	60	Agitation	[39]
Goethite	$(0.1 \text{ and } 1)^b$	$4 - 8$		4.45×10^{-3}	4.69×10^{-3}	2 and 4	n.s	n.s	Bath shaker	$\left[32\right]$
Ferrihydrite	$(10^{-3})^c$	$3 - 10$	5×10^{-3} and 1×10^{-2}	10^{-2}	10^{-2}	$1 - 3$	n.s	$10 - 40$	Rotation	[47]
$Fe2O3·H2O$	$(10^{-3})^c$	$4.5 - 8$	5×10^{-2}	5×10^{-4} to 5×10^{-2}	5×10^{-2}	4	20 and 25	n.s	n.s	[48]
Fe gel	$(0.093)^c$	$4 - 10$	0.125	0.125	0.125	3	n.s	25	n.s	$[49]$
goethite	0.02	$4.7 - 8$	2.62	2.62	2.62	25	20	40	n.s	$[33]$
Hydrous iron oxides	$(6.25 \times 10^{-3}$ and 5×10^{-2} °	$4 - 8$	$\mathbf{1}$		$0.5 - 4$	0.166	RT	100	n.s	$[34]$

n.s. not specifed, *RT* room temperature, *nZVI* nano zero-valent iron

a Concentration expressed in ppm

^bQuantity expressed in g/dm³

^cQuantity expressed in mmol/dm³

used for this purpose for quite a long time $[3-5]$ $[3-5]$ $[3-5]$ however, on a pure pragmatic approach [\[6](#page-12-0)].

Metallic iron materials (Fe \rm^0) have been broadly utilized in the water remediation industry for the past three decades [[5,](#page-11-3) [7–](#page-12-1)[14\]](#page-12-2). The interactions of Fe^0 with water ($\text{Fe}^0/\text{H}_2\text{O}$ systems) involves the in-situ generation of solid iron corrosion products (FeCPs), which in turn act as contaminant scavengers [\[6](#page-12-0), $15-20$]. The efficiency of freshly generated in-situ FeCPs for the removal of dyes $[18, 21]$ $[18, 21]$ $[18, 21]$ $[18, 21]$, fluoride ion $[20, 22]$ $[20, 22]$ $[20, 22]$, and Zn^{2+} [[19](#page-12-8)] has been investigated in batch systems. In addition, Touomo-Wouafo et al. [\[19](#page-12-8)] monitored the time-dependent changes in a Fe^0/Zn^2 ⁺/H₂O system to better characterize the remediation process. The main outcome of these studies is that $Fe⁰$ is not the agent reducing directly the cations of contaminants under environmental conditions.

This conclusion is present in the literature since 2007 [\[23,](#page-12-9) [24\]](#page-12-10) but has been largely ignored by active researchers $[6, 25, 26]$ $[6, 25, 26]$ $[6, 25, 26]$ $[6, 25, 26]$ $[6, 25, 26]$. A recent overview article by Hu et al. $[27]$ $[27]$ $[27]$, summarizes the complexity of the $Fe^{0}/H_{2}O$ system and recalls that contaminant removal is an inherent property of aqueous iron corrosion. This implies that upon proper design each polluted water can be treated using $Fe⁰$. For this reason, to gain more information about the efficiency of each system, either several Fe^0 materials are used for a single-contaminant or multi-contaminant systems are used for the same material, The approach used herein is the latter. Really polluted

wastewaters contain more than one heavy metal. Therefore investigation of the efectiveness of FeCPs for the removal of multiple competing cations is very important [\[28](#page-12-14)[–30](#page-12-15)].

In scientific literature considering $Fe⁰$ as a stand-alone reducing agent, the diversity of used experimental conditions renders the comparison of achieved results almost impossi-ble (Table [1\)](#page-1-0). It is evident from the Table [1](#page-1-0) that the majority of selected studies deals with defned oxides like hematite $[31]$ $[31]$, goethite $[32, 33]$ $[32, 33]$ $[32, 33]$ $[32, 33]$ $[32, 33]$, or hydrous iron oxides $[34]$ $[34]$. Those systems are limited by the fact that there is not a continuous production of in-situ FeCPs, the time development is not followed and, therefore, the interpretation of metals removal is limited to adsorption at equilibrium. On the other hand, using $Fe⁰$, the removal of contaminants is governed by a synergy of freshly and continuously in situ-generated FeCPs leading to adsorption and precipitation/co-precipitation. In this case, however, detailed time dependence is necessary to understand more deeply the remediation mechanisms.

Recently, Vollprecht et al. [[14](#page-12-2)] investigated the removal of multiple metal cations from wastewater using Fe⁰. In their batch experiments, substantial diferences in reactivity towards FeCPs were observed. These diferences infuencing efectivity of metals removal are caused among others by diferent conditions (e.g. pH) and also by the presence of both anions and cations in the tested water. However, in their paper, there is not specified the $Fe⁰$

material (size, surface), its aging is not considered and some important metal cations are missing.

For the present work, fresh iron powder -200 mesh (74 μ m) with defined size and surface [[19\]](#page-12-8) was used as the remediation agent and Zn^{2+} , Cd^{2+} and Pb^{2+} ions have been chosen as contaminants because they are commonly present in wastewater and because they have diferent (1) adsorptive affinity to FeCPs, (2) redox properties, (3) precipitation ability at various pH. The study is performed with binary (Zn^{2+}/Pb^{2+}) and Zn^{2+}/Cd^{2+}) and ternary (Zn^{2+}/Pb^{2+}) Cd^{2+}/Pb^{2+}) mixtures of various proportions of ions, in batch systems at pH 5.5 which is the optimum pH for the removal of Zn^{2+} obtained from our previous study [[19\]](#page-12-8). The concentration changes of aqueous Fe^{2+} , Zn^{2+} , Cd^{2+} , and Pb^{2+} are monitored within the time span from minutes to 14 days, using diferential pulse polarography (DPP). The DPP technique was chosen because it was possible to follow simultaneously the current (concentration) of several metal ions in aqueous solution. The X-ray photoelectron spectroscopy (XPS) and scanning electron microscopy (SEM) are used for the characterization of FeCPS after the remediation process with the aim to intercept and describe the form of removed metals.

The purpose of the present study is to investigate (1) the efficiency of differently aged FeCPs for the removal of multiple competing heavy metals; (2) the time development of all processes; (3) the iron powder after the process with adsorbed/precipitated/reduced products; (4) the mutual infuence of the present metal cations being simultaneously in the mixture because their interference is very probable due to their different adsorptive affinity to FeCPs, and diferent redox properties. All experiments should contribute to the explanation of all observed efects (for example the reason and relevance of the "induction period" at the beginning of the ZVI aging) and thus to detailed understanding of the mechanism of removal of selected heavy metals.

Results and discussion

Monitoring of Fe0 pre‑corrosion

When 0.8 g of Fe^0 was added in 0.1 mol/dm³ acetate buffer solution pH 5.5, in the presence of air oxygen (in the absence of Zn^{2+} , Cd^{2+} , and Pb^{2+}), typically only Fe^{2+} was identifed at −1.4 V vs. SCE and its concentration–time profle is depicted in Fig. [1.](#page-2-0)

It can be observed at the Fig. [1a](#page-2-0) that the concentration of $Fe²⁺$ gradually increases then reaches a maximum after approx. 3 h, then remains unchanged during few hours (where a plateau is formed). Thereafter, Fe^{2+} starts to decreases progressively with time. An increase of pH up to 6.7 was noticed during the frst 3 h (although the experiment is performed in buffered solution, initial pH 5.5), afterwards the pH diminishes progressively and returns back to its initial value. Similar observation has been reported by Touomo-Wouafo et al. [\[19](#page-12-8)]. The authors explained this efect by the corrosion of iron by water with dissolved oxygen leading to the release of Fe^{2+} and OH⁻ in solution which will progressively transformed to FeCPs [\[19\]](#page-12-8).

The detailed view of this experiment reveals an "induction period" of the corrosion which occurs during the frst 30 min of experiment (Fig. [1](#page-2-0)b) which could be attributed to the activated time of iron. In that period $Fe²⁺$ is not released and its concentration in solution is zero. The same kind of "induction period" was reported in our previous study [\[19](#page-12-8)]. In that study, only 0.1 g of Fe^0 was used, the "induction period" lasts the frst 1–2 h, the pH increased up to 6.0 and then returned back to 5.5. The present investigation points out that, the "induction period" depends on the amount of $Fe⁰$ used: higher amount of $Fe⁰$ employed in the experiment of the same volume causes shorter "induction period" and higher pH during the maximal concentration of Fe^{2+} . Most probably, these effects are connected with the reaction of $Fe⁰$ with dissolved oxygen in the frst part of the corrosion process. The detailed interpretation of these induction periods

is the subject of our further studies. In the past, analogous kind of induction period but under diferent conditions was observed (without explanation) by Lavine et al. [[35\]](#page-12-25), who "pre-treated" Fe^0 by washing it with a variety of aqueous solutions, including HCl.

The preliminary experiments reveal that 0.8 g of $Fe⁰$ aged 3 h was suitable, therefore, for all investigations in this study, 0.8 g of Fe^0 aged 3 h (time corresponding to maximum of Fe^{2+} in solution) in 0.1 mol/dm³ acetate buffer solution pH 5.5 was used.

Efect of competitive cations on the removal of Zn2+

Binary systems

For this study, each solution contained only two target metallic cations (besides in-situ Fe²⁺). The concentration of Zn^{2+} is set to 0.3 mmol/dm^3 whilst the concentration of the competitive cation corresponds to 0.15 mmol/dm^3 , 0.3 mmol/d dm³, and 0.6 mmol/dm³ respectively for the ratio $\text{Zn}^{2+}: \text{M}^{2+}$ (M represents Pb or Cd), 1:0.5, 1:1, and 1:2.

*Efect of Pb2***⁺** *on the removal of Zn²***⁺**

The time-dependence of Zn^{2+} decay after addition of 1 cm³ of binary metal mixed stock solutions (Zn^{2+}/Pb^{2+}) of various ratio) in 199 cm³ of acetate buffer containing 0.8 g of Fe^0 prior aged 3 h is presented in Fig. [2.](#page-3-0)

From Fig. [2a](#page-3-0), it is evident that in the absence of Pb^{2+} (ratio Zn^{2+} :Pb²⁺, 1:0), the majority of Zn^{2+} ion is removed within the frst hours and completely after 3 days, whereas in the increasing presence of Pb^{2+} the remediation occurs slower and slower and, finally, 97% of Zn^{2+} is removed after 14 days. When the experiment is evaluated at short reac-tion time (Fig. [2](#page-3-0)b), it is obvious that the efficiency of Zn^{2+} removal using aged Fe⁰ decreases by increasing concentration of Pb^{2+} ion in solution. Accordingly, only 88.6, 83, and 68.6% of Zn^{2+} removal is obtained respectively with 0.15, 0.3, and 0.6 mmol/dm³ of Pb^{2+} concentration in solution after 3 days. Based on these results, it can be concluded that, the Pb²⁺ ion delays substantially removal of Zn^{2+} from the solution and the final percentage of remaining Zn^{2+} is higher.

Besides the above results, monitoring of the Pb^{2+} concentration shows that Pb^{2+} ions completely disappear shortly after their addition to the solution. Hence, interaction of Pb^{2+} with the aged iron (or with the present solution) is fast regardless to the ratio Zn^{2+} : Pb²⁺. The same result was obtained in the absence of Zn^{2+} in solution. Thus, Zn^{2+} ion does not influence the removal of Pb^{2+} using ZVI aged 3 h. Similar fnding has been reported by Gadde and Laitinen [[34](#page-12-19)], in the binary system Pb^{2+}/Zn^{2+} using hydrous iron and manganese oxides. The authors mentioned that lead is adsorbed more strongly than any other metal ion studied. However, the role of pH should be also taken into account in the evaluation and interpretation of the data from the Fig. [2](#page-3-0)a, b. Since the pH of the solution reaches 6.7 after 3 h of aging of iron in the absence of heavy metals, the precipitation of their hydroxides could likewise contribute to the observed rapid removal of Pb^{2+} . This result is consistent with those of Khorshidi and Azadmehr [\[31\]](#page-12-16). Using hematite as adsorbent, the authors underlined that at pH more than 6, lead is entirely precipitated into $Pb(OH)$ ₂. However, those authors did not prove the presence of $Pb(OH)_{2}$.

All these observations highlight the ion-selective nature of FeCPs including the present solution) towards the present target heavy metals. As a result, after several hours the aged FeCPs mixture reacts preferentially with Pb^{2+} (or with its precipitate) than with Zn^{2+} . It may cause blocking of the reactive sites at the surface of the aged iron powder and the removal of the remaining Zn^{2+} occurs substantially slower. This outcome is consistent with Pauling electronegativity values of each investigated cation which are 2.33 and 1.65, respectively, for Pb^{2+} and Zn^{2+} [[36](#page-12-26)], hence higher electronegativity causes stronger interaction with FeCPs. The obtained result also matches with the hardness index of target cations, 0.131 and 0.115 for Pb^{2+} and Zn^{2+} , respectively, and the values of logarithm of the frst hydrolysis constant

of cations which are -7.6 and -9 , respectively, for Pb²⁺ and Zn^{2+} [\[36\]](#page-12-26).

In addition of these results, it was also observed a progressive vanishing of Fe^{2+} concentration in solution with time. This decrease underlines a continuous production of FeCPs and the formation of an oxide layer on $Fe⁰$ ("passivation") [\[37](#page-12-27), [38\]](#page-12-28). This outcome was expected since the consumption of Fe²⁺ by dissolved oxygen in water or OH[−] leads to Fe³⁺ and Fe(OH)₂. Fe³⁺ thereafter reacts with OH⁻ in solution to form Fe(OH)₃. Both Fe(OH)₂ and Fe(OH)₃ are later transformed to FeOOH, $Fe₂O₃$ and $Fe₃O₄$ [[19\]](#page-12-8).

*Efect of Cd²***⁺** *on the removal of Zn²***⁺**

In contrast to the results of above section, the presence of Cd^{2+} promotes the removal of Zn^{2+} in solution. As a result, in the binary $\text{Zn}^{2+}/\text{Cd}^{2+}$ system the remediation of Zn^{2+} by aged $Fe⁰$ is almost completed after 0.2 days which corresponds to approx. 4 h while in the absence of Cd^{2+} such result is achieved after 3 days (Fig. [3](#page-4-0)c). The facilitation of Zn^{2+} removal by Cd^{2+} requires detailed studies and will be the subject of our further study.

The time-dependence of the decrease of the Cd^{2+} ion concentration (in the absence or in the presence of Zn^{2+}) depicted in Fig. [3b](#page-4-0) displays a slight decrease of Cd^{2+} ion concentration during the first day then reaches

Fig. 3 Time-dependence of the decrease of the \bf{a} Zn²⁺, \bf{b} Cd²⁺ ions during remediation using ZVI at various Zn^{2+} :Cd²⁺ ratio. $(0.8 \text{ g of } \text{Fe}^0 \text{ prior aged } 3 \text{ h in})$ 199 cm³ of 0.1 mol/dm³ acetate bufer pH 5.5, in the presence of air oxygen). **c** Comparison of the time-dependence of the concentration decay of Zn^{2+} and Cd^{2+} , both 0.3 mmol/dm³ at the same conditions

a pseudo-equilibrium in solution. After 6 days, a new decrease of Cd^{2+} ion concentration is observed. This behavior might be due to the fact that, the FeCPs formed at the equilibrium (after 3 h of aging) are not suitable for the removal of Cd^{2+} but appropriate for Zn^{2+} removal (Fig. [3c](#page-4-0)). On the other hand, after 6 days, the FeCPs are convenient for the trapping of Cd^{2+} .

It is also evident from the Fig. [3c](#page-4-0) that the order of efectiveness of metal ions removal by aged $Fe⁰$ is as follows: $\text{Zn}^{2+} > \text{Cd}^{2+}$. Like in the previous case, this is consistent with the hardness index of cations, 0.115 and 0.081 for Zn^{2+} and Cd²⁺, respectively, and the values of logarithm of the frst hydrolysis constant of cations which are -9 and -10.1, respectively, for Zn^{2+} and Cd^{2+} [\[36\]](#page-12-26).

When considering the inverse case (how Zn^{2+} ions affect the removal of Cd^{2+}), the percentage of removal of Cd^{2+} obtained after 14 days of reaction is moderately dependent on the Zn^{2+} :Cd²⁺ ratio in a remarkable manner: Subsequently, 65, 67, 63, and 75% of Cd^{2+} are removed respectively in the ratio Zn^{2+} : Cd^{2+} , 0:1, 1:0.5, 1:1, 1:2. It is noticed that the Zn^{2+} slightly diminishes the percentage of the Cd^{2+} removal. Analogous result has been reported by Boparai et al. [[39](#page-12-21)]. In their work, the authors attributed this effect to the chemical similarities between Cd^{2+} and Zn^{2+} , consequently they may strongly compete for the

same adsorption sites. However, in their study, they have not considered the effect of Cd^{2+} on the removal of Zn^{2+} .

Ternary systems

In the present study, various ratios $\text{Zn}^{2+}:\text{Cd}^{2+}:\text{Pb}^{2+}$ were investigated namely: 1:0.5:0.5, 1:0.5:1, 1:1:0.5, 1:1:1, 1:1:2, 1:2:1, 1:2:2, where the concentration of Zn^{2+} was constant and set to 0.3 mmol/dm^3 whilst the concentration of competitive cations varied from 0.15 to 0.6 mmol/dm³.

The Fig. [4](#page-5-0) shows the concentration evolution of Zn^{2+} with time during its remediation using $Fe⁰$ (aged 3 h in 199 cm^3 of 0.1 mol/dm³ acetate buffer pH 5.5) at various ratio $\text{Zn}^{2+}:\text{Cd}^{2+}:\text{Pb}^{2+}$ (for clarity all eight dependences were divided into two graphs). Although the systems were analyzed in detail for 14 days, the presented dependences are described for the contact time 3.5 days when the data are the most informative.

Generally, it appeared that the percentage of removal of Zn^{2+} after 14 days is more than 98% from all data of Fig. [4,](#page-5-0) except in the ratio 1:0:0, where Zn^{2+} is completely removed after 3 days, hence it is evident that the presence of both competitive cations delays the removal of Zn^{2+} in solution. This is mainly owing to the already mentioned slowing effect of Pb^{2+} upon the removal of Zn^{2+} , which inhibited the slightly accelerating effect of Cd^{2+} .

It was also observed a rapid disappearing of Pb^{2+} at the initial stage of reaction as it was the case in the binary system $\text{Zn}^{2+}/\text{Pb}^{2+}$. Accordingly, the presence of Cd^{2+} does not have any influence on the removal of Pb^{2+} . Moreover, pseudo-equilibrium in the removal of Cd^{2+} appeared likewise in the ternary system with a short duration in comparison of binary system.

The percentage of removal of Zn^{2+} ions after approx. 3 days reaction time (taken from the data of Fig. [4](#page-5-0)) and those of Cd^{2+} ions at 14 days reaction time are presented in the Table [2.](#page-5-1) It follows from the data of Table [2](#page-5-1) that after 3 days more than 90% removal of Zn^{2+} is obtained when concentration of $Cd^{2+} \ge Pb^{2+}$. These results confirmed our

Table 2 Percentage of Zn^{2+} (after 3 days) and Cd^{2+} (14 days) removal from the ternary mixtures using $Fe⁰$ aged for 3 h

Zn^{2+} :Cd ²⁺ :Pb ²⁺ ratio	Removal of $\text{Zn}^{2+}/\text{\%}$	Removal of $Cd^{2+}/\%$
1:0.5:0.5	91	55
1:0.5:1	87	52
1:1:0.5	96	59
1:1:1	96	58
1:1:2	84	58
1:2:1	99	65
1:2:2	91	64

earlier observation obtained in the binary systems where it was highlighted that the Cd^{2+} accelerates whilst the Pb^{2+} reduces the Zn^{2+} removal percentage (cf. Fig. [2b](#page-3-0)). It is also evident that for the equal concentration of Cd^{2+} and Pb^{2+} , a "neutralization" of rather opposing effects of Cd^{2+} and Pb^{2+} on the Zn^{2+} removal occurs.

A close comparison of percentages of removal of Cd^{2+} obtained in Zn^{2+}/Cd^{2+} system with those presented in Table [2](#page-5-1) reveals that any addition of Pb^{2+} in solution decreases the percentage of removal of Cd^{2+} which is in agreement with the early observation of Gadde and Laitinen [[34\]](#page-12-19).

According to the above-mentioned results, the following order of decreasing efficiency of metal cations removal by aged Fe⁰ can be deduced: $Pb^{2+} > Zn^{2+} > Cd^{2+}$. This is analogous to the decrease order of selectivity of FeCPs towards the investigated metallic cations reported by several authors [\[32](#page-12-17)[–34](#page-12-19), [40\]](#page-12-20), using goethite, iron nanoparticles, hydrous iron, and manganese oxides.

Though no explanation of such order was given by some of those authors, the obtained order correlates well with the hardness index of investigated cations which are respectively for Pb^{2+} , Zn^{2+} , and Cd^{2+} 0.131, 0.115, and 0.081 as reported Kinraide and Yermiyahu [\[36](#page-12-26)] and also with the values of logarithm of frst hydrolysis constant of each cations, −7.6, -9 , and -10.1 , respectively, for Pb²⁺, Zn²⁺, and Cd²⁺ [\[36](#page-12-26)]. In any case, one has to keep in mind that it is hardly possible

Fig. 4 Time-dependence of the decrease of the Zn^{2+} ion concentration during remediation using Fe^0 (0.8 g of Fe^0 prior aged 3 h in 199 cm^3 of 0.1 mol/ $dm³$ acetate buffer pH 5.5, in the presence of air oxygen) of various ratio Zn^{2+} :Cd²⁺:Pb²⁺ from 0 to 3.5 days (for clarity the set of eight dependences was divided into two graphs)

to fnd one single well-ftting correlation because the remediation mechanism of these three cations is based on diferent processes: acidobasic at higher pH, (co-)precipitation, adsorption on FeCPs and/or redox. The elucidation of more detailed mechanism distinguishing role of various conditions is in our next plans.

Characterization of the solids by SEM and XPS mechanistic considerations

The surface of the iron powder exposed to bufered water ambient before and after addition of Zn^{2+} , Cd^{2+} , and Pb^{2+} ions was characterized by X-ray photoelectron spectroscopy (XPS) and its morphology by scanning electron microscopy (SEM).

The aging of Fe^0 powder in the buffer is naturally accompanied by extensive corrosion of Fe⁰ powder which changes substantially the surface morphology. As follows from SEM results (Fig. [5](#page-6-0)) the originally smooth grains of the sample **1** (bare Fe powder taken directly from the original fask) after 10 days in the bufer (sample **3**), they are partly dissolved and simultaneously/consequently covered by a thick layer of FeCPs fne crystals with high specifc surface. Aging is, therefore, a multistep process which manifests itself by the observed "induction period" (cf. Fig. [1](#page-2-0)b) and by unusual shape of the Fe^{2+} time dependence (cf. Fig. [1a](#page-2-0)), and causes curious beginning of all ions removal (cf. Figs. [2,](#page-3-0) [3\)](#page-4-0).

The survey photoelectron spectra of the samples **4** (top) and **7** (bottom) sputtered by Ar^+ ions ($t=5$ min) measured at low resolution are depicted in Fig. [6](#page-6-1). The spectra are normalized relative to the unit height of O 1 s line for comparison. The low energy regions of spectra $(<520$ eV, in red) are expanded to make more visible low intensive photoelectron lines. The survey spectra of the samples **1**, **2**, **3**, and **6** are qualitatively the same as the spectrum of the sample **4**, spectrum of the sample **5** qualitatively corresponds to that of the sample **7**. The same results were obtained from the spectra of the non-sputtered samples.

The assigned photoelectron and Auger lines detected in investigated samples and presented in the Table [3](#page-7-0) show that

Fig. 6 Photoelectron survey spectra of the samples **4** (top) and **7** (bottom) sputtered by Ar^+ ions ($t=5$ min) measured at low resolution

all samples are composed from Fe, C, and O. Presence of Pb was detected in the samples **5** and **7**. On the other hand, the presence of Si in the sample **1**, Cd in the sample **6**, and Zn in the samples **4** and **7** was not observed on this survey spectrum because their concentration was close to the detection limit. Confrmation of these elements was done using measurements at high resolution (Fig. [7](#page-7-1)) (Si found in the sample **1** can be due to the presence of trace of Si in the original container of Fe⁰ powder). Results of quantitative XPS analysis of the samples **1**–**7** are summarized in Table [4.](#page-7-2) Concentrations of Fe, C, O, Cd, Pb, and Zn are expressed in atomic %, calculated using Eq. ([1\)](#page-10-0). Intensities of photoelectron spectra were calibrated using Wagner sensitivity factors [\[41](#page-12-29)].

To discuss the effect of exposition of the sample to buffered water ambient the photoelectron Fe $2p_{3/2}$, C 1s, and O 1s spectra of the samples **1** and **3** measured in high

Line #	E_h /eV	assignment
I	23	O _{2s}
П	56	Fe 3p _{3/2,1/2}
Ш	93	Fe 3s
IV	137, 146	Pb $4f_{7/2,5/2}$
V	285	C _{1s}
VI	414, 446	Pb $4d_{5/2,3/2}$
VII	531	O _{1s}
VIII	713, 727	Fe 2p _{3/2, 1/2}
IX	783	Fe K $L_{2,3}L_{2,3}^{\ \ a}$
X	847	Fe K $L_1L_{2,3}^a$
XI	900	Fe K $L_1L_1^a$
XII	976	O K $L_{2,3}L_{2,3}^{\ \ a}$

Table 3 Assignment of the photoelectron and Auger spectra measured at low resolution

a Auger spectra

resolution before (blue color) and after $Ar⁺$ sputtering for **7** min (red color) are compared in Fig. [8.](#page-8-0)

The Fe $2p_{3/2}$ spectra (line I) at binding energy $E_b \sim 711.4$ eV measured before sputtering correspond to the oxide layer (Fe₂O₃) on the surfaces of samples 1 and 3, which can be in the case of the sample **1** almost completely eliminated by sputtering by Ar^+ ions for 7 min. Asymetric line (II) at $E_b = 707.3$ eV observed in the sputtered sample 1

belongs to metallic Fe, its asymmetry is afected by presence of very small amounts of residual Fe oxide (cf. intensity of O 1 s line after sputtering).

Much weaker line II is present in the Fe $3p_{3/2}$ spectrum of sputtered sample **3** (cf. low energy shoulder in the spectrum) and line I is shifted to lower E_b . These effects reflect much thicker oxide layer of the sample **3** due to long aging of the sample 3 in the buffer. While the oxide layer can be almost quantitatively eliminated from the sample **1**, rather thick oxidic layer remained on the sample **3** even after 7 min of sputtering. Obtained fndings are in line with observed intensity changes of O 1 s photoelectron spectra (Fig. [8](#page-8-0)a) and results of quantitative analysis (cf. Table [4\)](#page-7-2). Sputtering further reduced surface hydrocarbon contamination of the samples.

Summary of the photoelectron Fe $2p_{3/2,1/2}$, O 1 s, and C 1 s spectra of the samples **3**—**7** measured at high resolution is depicted in Fig. [8](#page-8-0)b. To minimize erosion of the samples the sputtering time was reduced to 5 min.

Non‑sputtered samples

The samples **4**–**6** contain various amounts of products of surface corrosion (Fe oxide phase) and contamination (cf. Table [4](#page-7-2) above, Fig. [8](#page-8-0)b, blue lines). The surface Fe oxidic phase is hydroxylated (cf. broadening of O 1 s spectra in the region of high E_b , which is typical for the presence of $-OH$

Table 4 Surface concentrations of Fe, C, O, Cd, Pb, and Zn in the samples **1**–**7** expressed as at.%

^aNumbers in brackets belong to the XPS measurements after Ar⁺ ion sputtering

Fe $2p_{3/2}$ O_{1s} C_{1s} Intensity / arb. unit Intensity / arb. unit x0.5 295 290 285 720 710 540 535 530 E_b / eV E_b / eV E_b / eV

Fig. 8 a Comparison of the Fe $2p_{3/2}$ O 1 s and C 1 s spectra of the samples 1 and 3 . Blue color: before $Ar⁺$ sputtering, red color: after Ar⁺ sputtering. **b** The Fe 2 $p_{3/2}$, O 1 s and C 1 s photoelectron spectra

before (blue) and after (red) Ar^+ sputtering for 7 min (sample 3) and 5 min (samples **4**–**7**). Intensities of the photoelectron spectra are normalized relative to the intensity of Fe 3p spectrum

groups). This Fe oxide phase could be ascribed to FeOOH resulting from surface hydroxylation and subsequent dehydration of the exposed iron in aqueous solution as reported Xi et al. [[42\]](#page-12-30).

The line shapes of the photoelectron spectra of the sample **5** are deformed by diferential charging. This sample is covered by the phase which is in poor electrical contact with its surface, which induces diferential charging, which disables discussion of the line shapes of photoelectron spectra in this case. On non-sputtered samples, Zn (sample **4**), Pb (sample **5**), and Cd (sample **6**) have been observed (Fig. [9](#page-9-0)a). Hydrocarbon contamination present on the surfaces is composed mostly from aliphatic hydrocabons (C 1 s line at \sim 285 eV, Fig. [8](#page-8-0)b).

Sputtered samples

Rather similar effect of sputtering is observed for the samples **4**–**7**. Much thicker oxide layer remained on the sample surfaces after their short (5 min) time sputtering (cf. absence of low energy shoulder in the Fe $2p_{3/2}$ spectrum of the samples **4**–**7** (Fig. [8](#page-8-0)b). However, the high energy asymmetry of the O 1 s spectra is reduced, i.e. only small concentration of hydroxylated Fe oxide phase remained after sputtering (Fig. [8](#page-8-0)b). Hydrocarbon contamination is also reduced (C 1 s spectra in Fig. [8](#page-8-0)b). No diferential charging is observed in the sputtered sample **5**.

In agreement with the Table [4](#page-7-2), where data for all elements (except Fe) are mostly lower after sputtering, we can conclude that a substantial part of the precipitated phase on the surfaces (together with the adsorbates) of the samples **4**–**7** was eliminated by sputtering. Thus, Pb is adsorbed on the samples **5**, **7**, Cd is adsorbed on the sample **6**, and Zn on the sample **7** (pertinent spectra cf. Fig. [9](#page-9-0)a). However, the extent of erosion of the oxidic coating of Fe grains by sputtering is not clear.

The Pb $4f_{7/2,5/2}$ photoelectron spectra observed in the samples **5** and **7** are depicted in Fig. [9](#page-9-0)b. The spectrum was simulated by two doublets (sample **5**) and three doublets (sample **7**). The doublet I is assigned to Pb^0 , doublet II to PbO. This result is consistent with those of Xi et al. [\[42](#page-12-30)], where their XPS analysis has confrmed that immobilized Pb was present in its zero and bivalent forms. Moreover, the authors proposed that using nano-zero-valent iron, partial reduction of Pb^{2+} takes place following by its precipitation as PbO.

The XPS study points to the contribution of adsorption in the mechanism of removal of heavy metals using aged $Fe⁰$. Furthermore, since it was found lead in the oxidation number 0 (Pb⁰) we can conclude that partial reduction of Pb^{2+} by remaining Fe^0 contributes in the removal of Pb^{2+} . This mechanism is in straight line with the mechanism reported by Li and Zhang [\[43](#page-12-31)], Xi et al. [\[42](#page-12-30)]. Moreover, precipitation of lead as $Pb(OH)$ ₂ (or PbO after drying) also takes place as earlier reported [\[42](#page-12-30)].

In the case of Zn^{2+} and Cd^{2+} , based on the results of characterization, we can suggest that the removal of both cations depends on the affinity of the respective cation towards FeCPs (adsorption onto FeCPs) which could be according to the present study $Fe₂O₃$ and FeOOH. Nevertheless, co-precipitation should be the other important reaction pathway, as

Fig. 9 a Photoelectron spectra of non-sputtered sample 4 (Zn $2p_{3/2}$), **5** (Pb $4f_{7/2,5/2}$), and **6** (Cd $3d_{5/2,3/2}$). (red doublet in Pb 4f spectrum: lines shifted by differential charging); **b** measured and simulated Pb $4f_{7/2,5/2}$ spectra of the sample 5 before Ar^+ sputtering (top), and samples 5 ,

earlier mentioned Statham et al. [\[13](#page-12-32)], Noubactep [\[23](#page-12-9), [44\]](#page-12-33). It is crucial to point out that the whole discussion has ignored reductive processes but has most rationally discussed the process of Cd²⁺, Pb²⁺ and Zn²⁺ removal in Fe⁰/H₂O systems. Thus, reductive transformation, when they occur are mediated by iron corrosion products, mainly Fe^{2+} and H_2 species [\[6](#page-12-0), [27,](#page-12-13) [30\]](#page-12-15).

Conclusions

This study assessed the efficiency of aged $Fe⁰$ powder for the removal of Zn^{2+} , Cd^{2+} , and Pb^{2+} in binary and ternary systems by monitoring their removal from aqueous solution under various experimental conditions. Results demonstrated the existence of an "induction period" after immersion of Fe⁰ powder in buffered solutions. The duration of this lag time depends on the used $Fe⁰$ amount. The lag time corresponds to the time necessary for generation of sufficient amount of solid iron corrosion products (FeCPs) for cations removal by adsorption and co-precipitation. SEM results confrmed the formation of high specifc surface FeCPs.

The attention was aimed to the mutual interference of multiple cations simultaneously present in the sample during their remediation. Rapid removal of Pb^{2+} was observed every time at the initial stage of reaction. In the binary system Pb^{2+}/Zn^{2+} the Pb^{2+} ion delays substantially removal of

7 after Ar^+ ion sputtering. Blue doublet I, I^* : Pb⁰, black doublet II, II^{*}: PbO, red doublet III, III^{*}: spectrum of PbO affected by differential charging

 Zn^{2+} whereas Zn^{2+} ion does not influence the removal of Pb^{2+} . In the system Cd^{2+}/Zn^{2+} the presence of Cd^{2+} promotes the removal of Zn^{2+} in solution while the Zn^{2+} ions slightly diminish the percentage of the Cd^{2+} removal. In case of Cd^{2+}/Pb^{2+} mixture, any addition of Pb^{2+} in solution decreases the percentage of removal of Cd^{2+} but the presence of Cd^{2+} does not have any influence on the removal of Pb^{2+} . In the ternary system the accelerating effect of Cd^{2+} upon the removal of Zn^{2+} is competitively inhibited by the presence of Pb^{2+} .

The following order of decreasing efficiency of removal of metal cations by aged Fe⁰ was found: $Pb^{2+} > Zn^{2+} > Cd^{2+}$. This order positively correlates with the hardness index of investigated cations which are respectively for Pb^{2+} , Zn^{2+} , and Cd^{2+} 0.131, 0.115, and 0.081 and also with the values of logarithm of their frst hydrolysis constants, −7.6, −9, and −10.1, respectively.

XPS analysis has proven the existence of $Fe₂O₃$ and FeOOH phases as iron corrosion products. Furthermore, XPS analysis of sputtered and non-sputtered samples reveals that the investigated heavy metals were adsorbed onto FeCPs. In the case of multiple cations present simultaneously in the tested solution, they may strongly compete for the same adsorption sites. Their mutual interference, however, refects not only diferent adsorptivity, but also different reaction mechanisms of remediation of Pb^{2+} , Zn^{2+} , and Cd^{2+} which involves (co)precipitation depending on pH and redox processes where also the dissolved oxygen plays a role.

Experimental

Chemicals

The used chemicals: cadmium acetate dihydrate $(Cd(CH_3COO)_2 \cdot 2H_2O)$ and lead acetate trihydrate $(Pb(CH_3COO)_2$ •3H₂O) were supplied by Aldrich, whilst zinc acetate dihydrate (Zn(CH₃COO)₂•2H₂O), acetic acid sodium salt trihydrate (CH₃COONa•3H₂O), and glacial acetic acid ($CH₃COOH$) were of analytical grade. Concentration of acetate buffer pH 5.5 was 0.1 mol/dm^3 . Ethanol and acetone of analytical grade were furnished by Lachner Company. Various stock solutions of heavy metals in single $(Zn^{2+}, Cd^{2+}, Pb^{2+})$, binary (Zn^{2+}/Pb^{2+}) and Zn^{2+}/Cd^{2+}), and ternary $(Zn^{2+}/Cd^{2+}/Pb^{2+})$ systems were prepared by dissolving the appropriate amount of weighed individual metallic salts in 0.1 mol/dm³ acetate buffer pH 5.5. In the single system, the concentration of stock solution was 0.06 mol/dm³ whereas in the stock solutions of binary as well as in ternary systems the concentration of Zn^{2+} remains unchanged (0.06 mol/dm^3) only the concentrations of Cd²⁺ and Pb²⁺ vary from 0.03 to 0.12 mol/ $dm³$. The working solution of Zn^{2+} ion was 0.3 mmol/dm³ whereas the concentration of Cd^{2+} and Pb²⁺ were varying from 0.15 to 0.6 mmol/dm³ depending on the investigated ratios.

Materials

The Fe⁰ powder utilized in the present study (99.8% Fe⁰, −200 mesh, 74 µm, Alfa Aesar) with a specifc surface area equal to 13.4 $m^2 g^{-1}$, was identical to that used in our previous study and was employed without any further pretreatment [[19](#page-12-8)]. Standard flter papers of 55 mm supplied by Fisher scientifc and a vacuum pump of 7. 0 mbar were used to dry selected samples for XPS and SEM analysis.

Experimental procedure

All experiments regarding the pre-corrosion and corrosion of iron powder as well as heavy metals ions removal were carried out in duplicates at room temperature in open fasks of 500 cm^3 in presence of air oxygen (oxic conditions).

Pre‑corrosion

The procedure of pre-corrosion of Fe^0 powder as well as that of concentration determination of the $Fe²⁺$ ion during the pre-corrosion time was similar to that realized in our previous study $[19]$ $[19]$ $[19]$. Indeed, 0.8 g of Fe^0 powder was

pre-equilibrated in 199 cm³ of 0.1 mol/dm³ acetate buffer at pH 5.5 for 0–3 days to generate in-situ FeCPs. Throughout the pre-equilibrated period, the fasks with solution containing Fe⁰ were gently shaken using a bath shaker with periodic linear motion by 10 cm (speed 10 cm s⁻¹). For concentration determination of Fe^{2+} , amount of 20 cm³ was regularly taken away from the fask at various time intervals and directly subjected to DPP where the concentration of $Fe²⁺$ was determined from the cathodic peak at -1.4 V versus saturated calomel electrode (SCE). After this procedure, the analyzed samples (after separation from mercury by decantation) were always put back to the original fask to keep on the aging.

Efect of competitive cations on the removal of Zn2+

Here, the impacts of Cd^{2+} and Pb^{2+} ions on the removal of Zn^{2+} were investigated in binary and ternary systems. Two binary systems were tested (Zn^{2+}/Pb^{2+}) and Zn^{2+}/Cd^{2+}), where the influence of Pb^{2+} and Cd^{2+} , respectively, on the Zn^{2+} removal was studied. In the ternary system, $Zn^{2+}/Cd^{2+}/$ Pb^{2+} , the cumulative effect of Cd^{2+} and Pb^{2+} on the removal of Zn^{2+} was investigated. The time dependences of all effects were followed and evaluated.

The batch experiments for the removal of heavy metal ions were carried out by adding of 1 cm^3 of stock solutions of heavy metal ions of various concentration (from 0.03 to 0.12 mol/dm^3) to the flasks with 199 cm³ of buffer containing 0.8 g of Fe^0 (aged for 3 h). All experiments were then monitored during 14 days. Regularly, at various time intervals, 20 cm^3 of the mixture (Fe⁰-heavy metals ions) was carefully withdrawn and rapidly subjected to DPP analysis without any dilution. The Zn^{2+} , Cd^{2+} , and Pb^{2+} ions were always identified by DPP at -1.04 , -0.6 , and -0.43 V vs. SCE, respectively. After analysis the solution was put back to the original fask to keep on the aging.

The percentage of metallic cation removal was calculated by means of equation below where $C_0(M^{2+})$ and $C_1(M^{2+})$ are the initial concentration of metallic cation (M^{2+}) and that at time *t*, respectively:

% of removal of
$$
M^{2+}
$$
 = $\left[\frac{C_0(M^{2+}) - C_t(M^{2+})}{C_0(M^{2+})} \right] \times 100.$ (1)

Drying of samples for characterization

Seven samples of the iron powder were selected for characterization: six of them, after 14 days reaction time in the presence of air oxygen with differently aged $Fe⁰$ were dried before analysis. As a standard (the seventh sample) fresh Fe⁰ powder was taken directly from the flask without any treatment. Those samples were denoted and described as follows: (1) Fe^0 powder; (2) 0.8 g of Fe^0 aged 3 h in 199 cm³

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of 0.1 mol/dm³ acetate buffer pH 5.5; (3) 0.8 g of $Fe⁰$ aged 10 days in 199 cm³ of 0.1 mol/dm³ acetate buffer pH 5.5; (4) 0.8 g of Fe⁰ aged 3 h in 199 cm³ of 0.1 mol/dm³ acetate

the samples was evaluated in the atomic percents calculated from corrected integral intensities *I* of the Fe 3p, C 1s, O 1s, Pb 4f, Zn 2p, and Cd 4d spectra:

$$
A(x)\left[\frac{I(x)^{\text{corr}}}{I(\text{Fe 3p})^{\text{corr}} + I(\text{C 1s})^{\text{corr}} + I(\text{O 1s})^{\text{corr}} + I(\text{Pb 4f})^{\text{corr}} + I(\text{Cd 4d})^{\text{corr}} + I(\text{Zn 2p})^{\text{corr}}}\right] \times 100. \tag{2}
$$

buffer pH 5.5 plus 1 cm³ of stock solution of Zn^{2+} (0.06 mol/ dm³), final concentration of Zn^{2+} 0.3 mmol/dm³; (5) 0.8 g of Fe⁰ aged 3 h in 199 cm³ of 0.1 mol/dm³ acetate buffer pH 5.5 plus 1 cm³ of stock solution of Pb^{2+} (0.06 mol/dm³), final concentration of Pb^{2+} 0.3 mmol/dm³; (6) 0.8 g of Fe^{0} aged 3 h in 199 cm³ of 0.1 mol/dm³ acetate buffer pH 5.5 plus 1 cm³ of stock solution of Cd^{2+} (0.06 mol/dm³), final concentration of Cd^{2+} 0.3 mmol/dm³; (7) 0.8 g of Fe⁰ aged 3 h in 199 cm³ of 0.1 mol/dm³ acetate buffer pH 5.5 plus 1 cm³ of stock solution of $\text{Zn}^{2+}:\text{Cd}^{2+}:\text{Pb}^{2+}$ (0.06 mol/dm³), ratio 1:1:1, fnal concentration of each heavy metal equals to 0.3 mmol/dm^3 .

Those six samples were fltered under vacuum with standard flter paper size 55 mm, and then washed respectively with ethanol and acetone. The obtained dried powders were carefully withdrawn from the paper and kept in a clear container, ready for XPS and SEM analysis.

Analytical methods

The HI 3220 pH/ORP meter was used for pH determination of the solution.

Diferential Pulse Polarography (DPP) was employed for concentration determination of Fe^{2+} and Zn^{2+} , Cd^{2+} , and Pb^{2+} ions in solution. Differential pulse polarographic curves were recorded with the 663 VA Stand series 05 connected to a digital computer controlled potentiostat PGSTAT 30 (Autolab-Metrohm). Three electrode system was used with mercury drop working electrode, SCE as reference and Pt wire as auxiliary electrode. DPP parameters: scan rate 10 mV/s, modulation peak amplitude 25 mV, modulation time 50 ms, and drop time 1 s [\[19](#page-12-8)].

An Omicron Nanotechnology ESCAProbe P spectrometer (Omicron Nanotechnology GmbH, Taunusstein, DE) was used to measure the photoelectron spectra. XPS analysis was performed at a pressure of $\sim 10^{-8}$ Pa. The X-ray source was monochromatic at 1486.6 eV. The photoelectron spectra were measured at low resolution (survey spectra in the energy region of 0–1200 eV with a step size of 0.6 eV) and at high resolution in 30 eV scans with a step size of 0.1 eV). The samples were measured before and after sputtering by argon ions (Ar^+) . The abundance $A(x)$ of the elements in

It can be assumed the presence of the precipitated phase created by dissolution of the powder on the grains surface. To test this possibility the photoelectron spectra were measured as received samples and after their soft argon ion Ar⁺ sputtering $(E=5 \text{ keV}, i \sim 5 \text{ mA}, t=5 \text{ min}, 7 \text{ min}).$ Possible surface precipitated phase might be reduced by this treatment. Sputtering can erode the samples surface, however. Damped nonlinear least-squares ftting procedure was used to distinguish partially resolved lines in the Pb 4f photoelectron spectra measured in high resolution [[45](#page-12-34)]. Minimal number was used in simulation of the spectra. Assignment of the photoelectron lines was done by comparison of estimated binding energies B.E. (eV) with standard ones [[46\]](#page-12-35). The samples were dried before XPS experiment. The efect of aging of Fe powder in bufered water ambient is investigated frst. Then the samples exposed to buffered water ambient which contained Zn^{2+} , Cd^{2+} , and Pb²⁺ ions are characterized. Metal ions can be present on the Fe powder during aging period (i.e. due to adsorption from water ambient) or during drying of the samples (i.e. as a contamination). We tried to resolve the both of this mechanism by XPS analysis of the samples as received and after cleaning by argon (Ar^+) ion sputtering.

For SEM analysis, the S 4800-I scanning electron microscope (Hitachi, Tokyo, Japan) was utilized and acceleration voltage of 5 kV was applied.

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References

- 1. Gosar M (2004) Geoenviron 51:2097
- 2. Xiao R, Wang S, Li R, Wang JJ, Zhang Z (2017) Ecotox Environ Safe 141:17
- 3. Oldright GL, Keyes HE, Miller V, Sloan WA (1928) Precipitation of lead and copper from solution on sponge iron. Bulletin 281, Bureau of Mines, p 131
- 4. Bojic AL, Bojic D, Andjelkovic T (2009) J Hazard Mater 168:813
- 5. Vollprecht D, Plessl K, Neuhold S, Kittinger F, Öfner W, Müller P, Mischitz R, Sedlazeck KP (2020) Processes 8:279
- 6. Xiao M, Hu R, Cui X, Gwenzi W, Noubactep C (2020) Processes 8:409
- 7. O'Hannesin SF, Gillham RW (1998) Ground Water 36:164
- 8. Henderson AD, Demond AH (2011) Environ Eng 137:689
- 9. Kishimoto N, Iwano S, Narazaki Y (2011) Water Air Soil Pollut 221:183
- 10. Guan X, Sun Y, Qin H, Li J, Lo IMC, He D, Dong H (2015) Water Res 75:224
- 11. Noubactep C (2015) Water Res 85:114
- 12. Suponik T, Winiarski A, Szade J (2015) Water Air Soil Pollut 226:360
- 13. Statham TM, Mumford KA, Stark SC, Gore DB, Stevens GW (2015) Sep Sci Technol 50:2427
- 14. Vollprecht D, Krois LM, Sedlazeck KP, Müller P, Mischitz R, Olbrich T, Pomberger R (2018) J Clean Prod 208:1409
- 15. Devonshire E (1890) J Frankl Inst 129:449
- 16. Lauderdale RA, Emmons AH (1951) J Am Water Works Ass 43:327
- 17. Gatcha-Bandjun N, Noubactep C, Loura Mbenguela B (2014) Fresenius Environ Bull 23:2663
- 18. Gatcha-Bandjun N, Noubactep C, Loura Mbenguela B (2017) Environ Technol Innov 8:71
- 19. Touomo-Wouafo M, Donkeng-Dazie J, Btatkeu-K BD, Tchatchueng JB, Noubactep C, Ludvík J (2018) Chemosphere 209:617
- 20. Nde-Tchoupé AI, Nanseu-Njiki CP, Hu R, Nassi A, Noubactep C, Licha T (2019) Chemosphere 219:855
- 21. Phukan M, Noubactep C, Licha T (2015) Chem Eng J 259:481
- 22. Hildebrant B, Ndé-Tchoupé AI, Lufngo M, Licha T, Noubactep C (2020) Processes 8:265
- 23. Noubactep C (2007) Open Environ Sci 1:9
- 24. Noubactep C (2008) Environ Technol 29:909
- 25. Ghauch A (2015) Freiberg Online Geosci 32:1
- 26. Gheju M (2018) Water 10:651
- 27. Hu R, Yang H, Tao R, Cui X, Xiao M, Konadu-Amoah B, Cao V, Lufngo M, Soppa-Sangue NP, Ndé-Tchoupé AI, Gatcha-Bandjun N, Sipowo-Tala VR, Gwenzi W, Noubactep C (2020) Water 12:641
- 28. Cantrell KJ, Kaplan DI, Wietsma TW (1995) J Hazard Mater 42:201
- 29. Qiu SR, Lai HF, Roberson MJ, Hunt ML, Amrhein C, Giancarlo LC, Flynn GW, Yarmoff JA (2000) Langmuir 16:2230
- 30. Scott TB, Popescu IC, Crane RA, Noubactep C (2011) J Hazard Mater 186:280
- 31. Khorshidi N, Azadmehr AR (2017) Desalin Water Treat 58:106
- 32. Christophi CA, Axe L (2000) J Environ Eng 126:66
- 33. Forbes EA, Posner AM, Quirk JP (1976) J Soil Sci 27:154
- 34. Gadde RR, Laitmen HA (1974) Anal Chem 46:2022
- 35. Lavine BK, Auslander G, Ritter J (2001) Microchem J 70:69
- 36. Kinraide TB, Yermiyahu U (2007) J Inorg Biochem 101:1201
- 37. Nesic S (2007) Corros Sci 49:4308
- 38. Lazzari L (2008) General aspects of corrosion. Encyclopedia of hydrocarbons, chapter 9.1, vol V. Istituto Enciclopedia Italiana, Rome
- 39. Boparai HK, Joseph M, O'Carroll DM (2013) Environ Sci Pollut Res 20:6210
- 40. Pawluk K, Fronczyk J (2015) Pol J Chem Technol 15:7
- 41. Wagner CD, Davis LE, Zeller MV, Taylor JA, Raymond RH, Gale LH (1981) Surf Interface Anal 3:211
- 42. Xi Y, Mallavarapu M, Naidu R (2010) Mater Res Bull 45:1361
- 43. Li XQ, Zhang WX (2007) J Phys Chem C 111:6939
- 44. Noubactep C, Btatkeu-K BD, Tchatchueng JB (2011) Chem Eng J 178:78
- 45. Kwok RWM (1999) XPSPeak, Version 4.1. Hong Kong, Available online: [https://www.phy.cuhk.edu.hk/surface/XPSPeak](http://www.phy.cuhk.edu.hk/surface/XPSPeak). Accessed on 21 Sept 2019
- 46. Briggs D, Seah MP (1996) Practical surface analysis by Auger and X-ray photoelectron spectroscopy. Wiley, New York
- 47. Schultz MF, Benjamin MM, Ferguson JF (1987) Environ Sci Technol 121:863
- 48. Benjamin MM (1981) J Coll Inter Sci 79:209
- 49. Kinniburgh DG, Jackson ML, Syer JK (1976) Soil Sci Soc Am J 40:796

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