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Highly efficient conversion of 1-cyanocycloalkaneacetonitrile using a "super nitrilase mutant"

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Received: 14 August 2018 / Accepted: 21 November 2018 / Published online: 28 November 2018 © Springer-Verlag GmbH Germany, part of Springer Nature 2018

Abstract

Nitrilase is the member of carbon–nitrogen hydrogen hydrolase superfamily, which has been widely used for the hydrolysis of nitriles into corresponding carboxylic acids. But most nitrilases are plagued by product inhibition in the industrial application. In this study, a "super nitrilase mutant" of nitrilase with high activity, thermostability and improved product tolerance from *Acidovorax facilis* ZJB09122 was characterized. Then, an efficient process was developed by employing the whole cell of recombinant *E. coli* for the conversion of high concentration of 1-cyanocyclohexylacetonitrile-to-1-cyanocyclohexaneacetic acid, an important intermediate of gabapentin. Under the optimized conditions, the higher substrate concentrations such as 1.3 M, 1.5 M and 1.8 M could be hydrolyzed by 13.58 g DCW/L with outstanding productivity (> 740 g/L/day). This study developed a highly efficient bioprocess for the preparation of 1-cyanocyclohexaneacetic acid which has the great potential for industrial application.

Keywords Nitrilase · Product tolerance · Biocatalysis · 1-Cyanocyclohexaneacetic acid · Gabapentin

Introduction

Cyano carboxylic acids, as important building blocks, are widely used in the preparation of various pharmaceuticals and agrochemicals [1-5]. The selective hydrolysis of dinitrile is one of the important approaches for the preparation of cyano carboxy acids. However, the chemical method affords product in low yield and produce large amounts of unwanted byproducts and inorganic wastes. Nitrilase is a kind of important hydrolase [6-13]. Due to the high regioselectivity, nitrilase becomes attractive biocatalyst for the preparation of cyano carboxylic acids by selective hydrolysis of dinitriles in one single step.

Within the past few years, selective hydrolysis of dinitriles to cyano carboxylic acid by nitrilase has been explored

Ya-Ping Xue xyp@zjut.edu.cn and become highly appealing. The nitrilase from *Acidovorax facilis* 72W was utilized in the synthesis of 4-cyanopentanoic acid [14], an important precursor of 1,5-dimethyl-2-piperidone, and 1-cyanocyclohexaneacetic acid (1-CA), an intermediate of gabapentin [15]. The nitrilase bll6402 from *Bradyrhizobium japonicum* USDA 110 was reported to hydrolyze α,ω -dinitriles to ω -cyanocarboxylic acids [16, 17]. Plant nitrilases from *Arabidopsis thaliana* [18], *Brassica rapa* [19], *Arabis alpina* [20] were described to hydrolyze racemic isobutylsuccinonitrile to (3S)-3-cyano-5-methyl hexanoic acid which is the key intermediate for the preparation of Pregabalin. In addition, several nitrilases with satisfactory regioselectivity were found in natural isolates such as *Rhodococcus rhodochrous* and *R. sphaeroides* or by genome mining [5, 21–25].

In recent research, our group cloned a regioselective nitrilase from *A. facilis* ZJB09122 [4, 26]. After mutation on F168 and process optimization, the activity of the nitrilase mutant AcN (F168V) was improved greatly [26–29]. Nevertheless, similar to other nitrilases, the nitrilase AcN shared some common limitation, such as poor thermostability and product tolerance. Very recently, protein engineering was employed to modify the nitrilase AcN, and a "super nitrilase mutant" AcN-M (AcN-T201F/Q339K/Q343K) with dramatically improved thermostability was obtained [30].

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Here, we selected AcN-M as the catalyst for the hydrolysis of 1-cyanocyclohexylacetonitrile (1-CN) and its kinetic parameters were determined. After overexpressing the nitrilase in *Escherichia coli* (*E. coli*) BL21 (DE3), the recombinant *E. coli* was applied to the hydrolysis of 1-CN to 1-CA with high substrate loading (Scheme 1). Under optimized conditions, the conversion rate of 1-CN reached \geq 99% with a productivity of 740.4 g/L/day, which represents the highest level so far. This work provides an advantage over all the existing biocatalysis process toward 1-CN.

Materials and methods

Chemicals

1-CN, 1-CA and 1-carboxycyclohexaneacetic acid were obtained from Zhejiang Chiral Medicine Chemicals Co., Ltd. (Hangzhou, China). Other chemicals were of analytical grade and purchased from local suppliers.

Strains, culture conditions and protein purification

The AcN and AcN-M were cloned, mutated previously and overexpressed in host *E. coli* BL21 (DE3) [4, 30]. These recombinant *E. coli* strains were grown at 37 °C in Luria–Bertani (LB) medium (10 g/L tryptone, 5 g/L yeast extract, 10 g/L NaCl) with the addition of 50 µg/mL kanamycin. The induction of the nitrilase was achieved by adding 0.1 mM of isopropyl β -D-thiogalactoside (IPTG) to the medium when OD₆₀₀ was 0.6–0.8, and the strain was cultured for another 10–12 h at 28 °C and 150 rpm. The cells were harvested by centrifugation at 10,000×g for 10 min and washed by 0.9% (w/v) NaCl twice.

The resulted cells were resuspended in a 0.2 M sodium phosphate buffer (pH 7.0) and the cell extract was prepared by the ultrasonic cell-break method. The nitrilase AcN and AcN-M were purified by standard Ni–NTA affinity chromatography as previously described [30]. The concentration of purified nitrilase was determined by Bradford protein assay [31].



Scheme 1 Regioselective hydrolysis of 1-CN for the production of 1-CA with whole cell of recombinant *E. coli*-harboring nitrilase

Kinetic measurement

About 0.25 µg purified nitrilases were assayed in 10 mL sodium phosphate buffer (0.1 M, pH 7.0) containing 0-200 mM 1-CN at 45 °C. The reaction was stopped by adding 100 µL 6.0 M HCl and the concentration of 1-CA was detected using high-performance liquid chromatography (HPLC). The inhibition constant (K_i) was determined using the sodium phosphate buffer (0.1 M, pH 7.0) containing 2–100 mM 1-CA and a series of concentrations of 1-CN (0–200 mM).

Nitrilase assay

The standard reaction was performed at 45 °C by mixing 67.9 mg DCW resting cells with 0.2 M 1-CN in 10 mL sodium phosphate buffer (0.2 M, pH 7.0). The reaction mixture was incubated in an orbital shaker at 200 rpm at 45 °C for 10 min. The aliquot (500 μ L) was withdrawn and the reaction was stopped by 5 μ L 6.0 M HCl and centrifuged at 12,000×*g* for 3 min. The concentration of 1-CA in the supernatant was determined by HPLC. One unit of the nitrilase activity (*U*) was defined as the amounts of resting cells that produced 1 μ mol of product per min under the standard assay conditions.

Product tolerance

Assay to measure the product tolerance of recombinant *E. coli* and cell extract was performed in an orbital shaker at 200 rpm at 45 °C. 10 mL reaction mixture contained 67.9 mg DCW cells or cell extract, 0.2 M substrate, and different concentration of 1-CA. The pH was adjusted to 7.0 with 1.0 M NaOH solution. Aliquots (500 μ L) were taken after 10 min and the product concentration was determined by HPLC.

Effect of temperature and pH

The influence of temperature on the nitrilase activity of recombinant *E. coli* was measured in the range of 25–60 °C. To determine the thermal stability of recombinant *E. coli*, the resting cells were incubated in sodium phosphate buffer (0.2 M, pH 7.0) at 25–50 °C with regular time intervals, and the initial and residual activities were measured under the standard assay conditions.

The pH dependence of recombinant *E. coli* was studied under the standard assay condition using following buffers at 0.2 M concentration: citric acid–sodium citrate buffer, pH 4.0–5.0; sodium phosphate buffer, pH 6.0–8.0; Gly–NaOH buffer, pH 9.0–10.0. The stabilities of the recombinant *E*. *coli* under different pH values were studied by incubating them at pH 7.0 or pH 7.5 in an ice bath. The residual activities were measured under the standard assay conditions.

Effect of 1-CA concentration on cell integrity and cell-specific activity

The effect of 1-CA concentration on resting cells were monitored by incubating 13.58 g DCW/L *E. coli* BL21 (DE3)/pET-28b(+)-AcN-M cells in sodium phosphate buffer (0.2 M, pH 7.0) with 0.50 M or 0.75 M 1-CA at different temperature (25–45 °C). At regular time intervals, an aliquot (5 mL) was taken and centrifuged at 15,000×*g* for 1 min. The protein in the supernatant was analyzed by sodium dodecyl sulfate–polyacrylamide gel electrophoresis (SDS–PAGE) (with 12% polyacrylamide) [32] and Bradford method. The initial and residual nitrilase activity (A_i and A_r) of cells was determined under the standard assay conditions. Half-lives were measured from plots of the natural logs of A_r/A_i versus the incubating time.

Hydrolysis of 1-CN by recombinant E. coli

Recombinant *E. coli* BL21 (DE3)/pET-28b(+)-AcN-M (1.358 g DCW) was added into a 250 mL flask containing 100 mL sodium phosphate buffer (0.2 M, pH 7.5) and different concentration of 1-CN (1.0–2.0 M). The reaction was carried out at different temperatures (25–45 °C) and 200 rpm. During the hydrolysis reaction, the samples were withdrawn at the required time and analyzed by HPLC for profiling the product formation. The same samples (500 μ L) were extracted by 500 μ L ethyl acetate and the organic phase was analyzed by gas chromatography (GC) for determining 1-CN residue.

Scaling-up the biotransformation of 1-CN

(1) In a 1-L stirred reactor, 500 mL of distilled water containing 6.79 g DCW of *E. coli* BL21 (DE3)/pET-28b(+)-AcN-M cells and 111 g of 1-CN were added. The mixture was incubated at 35 °C, 200 rpm for 6 h. (2) In a 1-L stirred reactor 500 mL of distilled water containing 6.79 g DCW of *E. coli* BL21 (DE3)/pET-28b(+)-AcN-M cells and 133 g of 1-CN were added. The mixture was incubated at 25 °C, 200 rpm for 8 h. Samples (1 mL) were withdrawn at intervals to analyze the concentrations of 1-CA and 1-CN.

Recovery of 1-CA

After the hydrolysis reaction, the cells were removed by centrifugation $(12,000 \times g, 10 \text{ min})$. The supernatant was mixed with 1% (*w*/*v*) polyaluminum chloride and agitated at 400 rpm for 4 h. 1% (*w*/*v*) diatomite (median size: 19.6 µm)

was added and the mixture was agitated at 400 rpm for additional 2 h. After filtration, the filtrate was acidified to a pH of 1.5–2.0 with 6.0 M HCl and mixed with an equal volume of dichloromethane under stirring. The extraction operation was repeated for 2–3 times. The organic layer was combined and distilled under vacuum. The solid obtained was dried at 52 °C.

Analytical methods

1-CA and 1-carboxycyclohexaneacetic acid were separated by HPLC (Shimadzu LC-16 with a UV detector) with a XBridge BEH C_{18} Column (130 Å, 5 µm, 4.6 mm×250 mm, 1/pkg, column temperature 40 °C), 76% acetonitrile, 24% 0.58 g/L NH₄H₂PO₄ and 1.83 g/L NaClO₄ in water (pH 1.8) as solvent. The UV detector was set at a wavelength of 215 nm.

1-CN was analyzed by GC (Agilent 7890A system with a FID Detector) with Agilent J&W HP-5 Column ($30 \text{ m} \times 0.32 \text{ mm}$, 0.25 µm film thickness). The inlet temperature was 320 °C, and the column temperature was 160 °C. The carrier gas was nitrogen and the detector temperature was 340 °C.

Results and discussion

Kinetic constants of mutant nitrilase

In previous work, E. coli BL21 (DE3)/pET-28b(+)-AcN was constructed and shown as a robust catalyst to hydrolyze 1-CN. But, the thermostability is relatively poor. Recently, a nitrilase mutants AcN-M (AcN-T201F/Q339K/Q343K) from AcN was isolated with improvement in thermostability and specific activity toward 1-CN [30]. To analyze the mutational effect, the kinetic parameters of nitrilase AcN and AcN-M were determined (Fig. 1). To our surprise, the mutant AcN-M has similar $K_{\rm m}$ with parent nitrilase AcN, and 1-CA was bound with an affinity ($K_i = 8.15 \text{ mM}$) that was less than that exhibited for AcN ($K_i = 1.97 \text{ mM}$) by ca. fourfold, which indicated that AcN-M facilitated the product release without perturbing the binding of substrate. Alteration of the quaternary structure impact by the mutations on site 201 which was located on "A" surface (responsible for the dimerization and positioning of active sites) and the top of substrate-binding pocket might be the explanation for the reduction of product inhibition [33, 34].

In addition, when comparing parent and mutant nitrilases in *E. coli* BL21 (DE3), the recombinant *E. coli* BL21 (DE3)/pET-28b(+)-AcN-M showed higher specific activity (Table 1). No 1-carboxycyclohexaneacetic acid was detected in the reactions, which indicated there were no changes in their regioselectivity.



Fig.1 Comparison of the kinetic constants obtained for the AcN and AcN-M $% \mathcal{A}$

Effect of temperature and pH on the cell-specific activity

The activity of whole cells of *E. coli* BL21 (DE3)/pET-28b(+)-AcN-M was monitored at different temperature (25–60 °C) (Fig. 2a). The result indicated that the resting cells showed maximum activity at 55 °C and the activity declined when the temperature was above 60 °C. To analyze the thermostability, the resting cells were incubated at 25 °C, 35 °C, 45 °C and 50 °C before measuring the residual activity under the standard assay conditions. As shown in Fig. 2b, the mutant displayed high thermostability below 45 °C with a half-life time of about 198.3 h. At 50 °C, the resting cells lost activity more rapidly and only retained 20% of the initial activity after incubating for 45 h.

The recombinant *E. coli* maintained higher activities in the pH range from 7.0 to 9.0 (Fig. 2c) and Fig. 2d confirmed the excellent stability at pH 7.0 and pH 7.5. In the following experiments, pH 7.5 was selected as the optimal condition for the reactions.

Product tolerance

Generally, low product tolerance is particularly limiting factor in the enzymatic conversion of nitriles to acids under the high substrate loadings and represents a barrier to achieving the high product concentration necessary for an efficient process [35–39]. For example, *Nocardia rhodochrous* LL100-21 was inhibited by the product nicotinic acid and 0.3 M nicotinic acid caused 44% inhibition of 3-cyanopyridinase activity [40]. Nicotinic acid at concentrations greater than 0.2 M inhibited the 3-cyanopyridinase activity of nitrilase from the thermophilic bacterium *Bacillus pallidus* Dac521 [41].

In the nitrilase-mediated hydrolysis of 1-CN, the product tolerance to 1-CA was estimated by comparing the activities of parent and mutant nitrilases in *E. coli* BL21 (DE3) under inhibiting conditions to that without adding inhibitors. As shown in Fig. 3, the mutant exhibited a higher level of 1-CA resistance than the wild type. Under 0.7 M product, AcN lost ca. 82% of initial activity while AcN-M only lost ca. 45% of initial activity. Even when the concentration of 1-CA raised to 1.3 M and 1.5 M, AcN-M retained 26% and 23% of initial activity, respectively, while AcN was strongly inhibited and almost lost all of the catalytic activity, which proved the product tolerance of this mutation was improved.

Dependence of product accumulation on temperature

As described above, the mutant *E. coli* BL21 (DE3)/pET-28b(+)-AcN-M exhibited higher activity and great thermostability at 45 °C compared to *E. coli* BL21 (DE3)/pET-28b(+)-AcN (Table 1). At 45 °C, AcN-M (13.58 g DCW/L) exhibited high hydrolysis activity toward 1.0 M 1-CN and the conversion reached more than 99% within 2 h, with productivity 1886 g/L/day. But, when the concentration of 1-CN was higher than 1.3 M, substrates were not hydrolyzed completely at 45 °C. After comparing the hydrolysis reactions at different temperature (25 °C, 35 °C and 45 °C) under high substrate loading (Table 2), it showed that: (1) high temperature resulted in shorter reaction time and higher productivity

Table 1Improvement of cell-specific activity, thermostabilityfor 1-CN hydrolysis by wholecells of mutant nitrilasecatalysts compared to parentnitrilase catalyst

Whole cells of recombinant <i>E. coli</i>	Cell-specific activity (U/g DCW) ^a	Half-life (h) ^b	Regiose- lectivity (%) ^c
<i>E. coli</i> BL21 (DE3)/pET-28b(+)-AcN	2478.8 ± 129	24.0 ± 2.3	≥ 99
<i>E. coli</i> BL21 (DE3)/pET-28b(+)-AcN-M	2790.1 ± 102	198.3 ± 5.1	≥ 99

^aCell-specific activity (U/g DCW) was determined at 45 $^{\circ}$ C using 6.79 g DCW/L resting cells in 0.2 M sodium phosphate buffer (pH 7.0) containing 0.2 M 1-CN

^bHalf-life was measured by incubating the resting cells at 45 °C in 0.2 M sodium phosphate buffer (pH 7.0) and assaying residual activity under standard assay condition

^cRegioselectivity was defined as molar ratio of the 1-CA to the total amount of carboxylic acid products formed





Fig. 2 a Effect of temperature on the cell-specific activity of E. coli BL21 (DE3)/pET-28b(+)-AcN-M (6.79 g DCW/L biocatalyst, 0.2 M 1-CN in pH 7.0 sodium phosphate buffer (0.2 M)). b Thermostability of E. coli BL21 (DE3)/pET-28b(+)-AcN-M at different temperature.



Fig. 3 Effect of product 1-CA to the activity of on the whole cells of recombinant E. coli. The ability of AcN and AcN-M to hydrolyze 1-CN was determined in the presence of 0-1.5 M 1-CA, and the reactions were carried out by standard assay. The relative activity is shown relative to the activity without adding 1-CA

c Dependence of nitrilase activity of E. coli BL21(DE3)/pET-28b(+)-AcN-M (6.79 g DCW/L biocatalyst, 0.2 M 1-CN) on pH at 45 °C. d Stability of E. coli BL21 (DE3)/pET-28b(+)-AcN-M at different pH values

under low substrate loading due to the higher cell-specific activity. At 45 °C, 13.58 g DCW/L of resting cells demonstrated faster reaction rate and higher productivity than that at low temperature (Entry 1-3). Similarly, at 35 °C, using the same amount of resting cells, almost no substrate was detected after 4 h of conversion with 1.3 M 1-CN in which the productivity reached up to 1187 g/L/day (Entry 5), when the substrate concentration increased to 1.5 M, 0.139 mol 1-CA along with the catalyst yield $(g_{product}/g_{catalyst})$ of 16.4 and productivity of 974 g/L/day could be obtained (Fig. 6) (Entry 8), which was also faster than that at 25 °C (Entry 4, Entry 7). (2) The low temperature was of benefit to the accumulation of product under high substrate loading. As mentioned above, a high concentration of 1-CN (\geq 1.3 M) could not be completely converted to 1-CA at 45 °C (Entry 6, Entry 9, Entry 12). Although 1.3 M and 1.5 M substrate could be completely consumed at 35 °C, when increasing initial concentration of 1-CN to 1.8 M the conversion decreased to 89.9% (Entry 11). When the reaction run at 25 °C, a reaction time of 8 h resulted in > 99% total conversion of 1.8 M 1-CN, affording a catalyst yield of 18.9 and productivity of 767 g/L/day (Entry 10). In addition, because

 Table 2
 Effect of temperature on hydrolysis reaction toward high substrate loading

Entry	Substrate loading (M)	Tempera- ture (°C)	Reaction time (h)	Conversion (%) ^a
1	1.0	25	3	> 99
2		35	2.5	> 99
3		45	2	> 99
4	1.3	25	5	> 99
5		35	4	> 99
6		45	8	91.3
7	1.5	25	6	> 99
8		35	5.5	> 99
9		45	8	77.9
10	1.8	25	8	> 99
11		35	8	89.9
12		45	8	69.4
13	2.0	25	12	95.1
14		35	12	77.5
15		45	12	61.4

Reaction condition: 100 mL pH 7.0 sodium phosphate buffer (0.2 M), 13.58 g DCW/L resting cells, 1.0–2.0 M 1-CN at 25–45 °C.

 $^{\rm a} {\rm Conversion}$ (%) is defined as total mass of 1-CN consumed divided by the total mass of 1-CN fed

of high product accumulation and strong product inhibition, 2.0 M 1-CN could not be completely consumed within 12 h (Entry 13–15).

During the reaction, the product 1-CA not only acted as competition inhibitor to nitrilases, but also was hypertoxic to cells which led to cell lysis [28]. High temperature can also lead to the increased permeability of cell. To investigate the synergistic effect of 1-CA and temperature on resting cells, suspension of the resting cells in pH 7.0 sodium phosphate buffer with 0.50 M and 0.75 M 1-CA were incubated at different temperature (25 °C, 35 °C, 45 °C). As shown in Fig. 4a, the cell lysis showed a positive correlation with temperature under 0.50 M 1-CA. Under the combined effect of product and high temperature, the rate of protein accumulation in cell suspension at 45 °C and 0.50 M 1-CA was far faster than that at 35 °C and 25 °C. Similar result was obtained in the SDS-PAGE analysis of the protein in the supernatant which showed more nitrilase leaked at elevated temperature (identified based on the molecular weight) (Fig. 4b). The leakage of protein led to the inactivation of resting cells. In Fig. 5, the calculated inactivation curves and half-life $t_{1/2}$ were shown. It could be seen that the inactivation of the resting cell exhibited first-order inactivation kinetics, which showed that low temperature led to a significant increase in stability of resting cells under high concentration of 1-CA. On the other hand, the activity of the leaked protein was investigated in presence of 1-CA. The product tolerance of cell extract which was equivalent of 6.79 g DCW/L fresh cells was inferior to that of whole cells, and the concentration of leaked protein which was up to 1200 parts per million (ppm) was far less than that of cell extract (ca. 4000 ppm). After diluting the cell extract of E. coli BL21 (DE3)/pET-28b(+)-AcN-M to ca. 1400 ppm, the loss of activity under 0.4 M product increased to 65%, and almost lost all of activity under 0.70 M 1-CA (data not shown), which suggested that the leak protein could not hydrolyze the substrate under a high concentration of product.

Therefore, cell integrity was an important factor for hydrolysis reaction under high substrate loading and temperature was an essential means of regulation to balance the cell integrity and reaction rate. A temperature of 45 °C resulted in super high reaction rate and productivity which could be employed in the hydrolysis reaction with low substrate loading (≤ 1.0 M) and short reaction time (≤ 3 h). A temperature of 35 °C was optimal when the concentration of 1-CN was 1.0–1.5 M for a faster reaction rate. Meanwhile, when the hydrolysis reaction runs at higher substrate concentrations (≥ 1.5 M) or need more than 6 h to complete, a reaction temperature of 25 °C was more suitable (Fig. 6).

Fig. 4 a Effect of product 1-CA and temperature on cell lysis of E. coli BL21 (DE3)/ pET-28b(+)-AcN-M. 13.58 g DCW/L resting cells of E. coli BL21 (DE3)/pET-28b(+)-AcN-M were incubated under different temperature and different concentration of 1-CA. The protein concentration was determined by Bradford protein assay. b SDS-PAGE analysis of the protein leaked from free cells incubated under 0.5 M 1-CA at different temperature for 3 h. Lane 1: 25 °C; lane 2: 35 °C; lane 3: 45°C





Fig. 5 Influence of 1-CA and temperature on inactivation of *E. coli* BL21 (DE3)/pET-28b(+)-AcN-M and lines calculated for first-order inactivation

Scaling-up the hydrolysis of 1-CN

To explore the potential synthetic value of the AcN-M mutant in industry, the whole-cell biocatalyst was used to produce 1-CA in a 1-L stirred bioreactor. To avoid the presence of too many salts that would have to be removed during the purification steps [26], purely aqueous solution at pH 7.0 was used as a good alternative to buffers in the experiments for the preparation of 1-CA. Hydrolysis of 1.5 M and 1.8 M 1-CN by 13.58 g DCW/L whole cells was carried out in purely aqueous solution (initial pH 7.0), respectively. As shown in Fig. 7, the mutant could completely hydrolyze 1.5 M 1-CN in 6 h at 35 °C, providing a productivity of 882.9 g/L/day. The aqueous reaction mixture was extracted with dichloromethane and analyzed by HPLC to reveal an 88% yield of 1-CA. 1.8 M 1-CN could also completely convert to 1-CA at 25 °C with a productivity of 740.4 g/L/ day and catalyst yield of 18.9. The yield of 1-CA separated



Fig. 6 Time courses of 1-CA synthesis under high substrate loading and protein accumulation in the 100 mL reaction system are shown. Reactions were performed at 13.58 g DCW/L resting cells, 1.0-1.8 M 1-CN, 25-45 °C, pH 7.0

from the reaction mixture was 86%. *E. coli* BL21 (DE3)/pET-28b(+)-AcN-M was demonstrated to potential in the industrial production of 1-CA.

Conclusion

In summary, we demonstrated that product 1-CA and temperature were crucial to sustain cell integrity and optimal biocatalyst performance. After optimization of reaction condition, the mutant *E. coli* BL21 (DE3)/pET-28b(+)-AcN-M was proved to be an exceedingly robust catalyst with high cell-specific activity and improved tolerance to the product. Productivity and catalyst yield have been significantly improved compared to the previous reports. This was an efficient, practical and economical enzymatic process featuring high substrate loading, outstanding catalyst yield and high productivity which has potential in industrial application.



Fig.7 Scaling-up the regioselective hydrolysis of 1-CN for synthesizing 1-CA in a 1-L reactor containing 0.5 L reaction mixture. The experiments were performed at 35 $^{\circ}$ C/25 $^{\circ}$ C and 200 rpm with

Acknowledgements This work was funded by the National Natural Science Foundation of China (nos. 21476210 and 21706235).

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aqueous solution. ^aThe productivity was defined as the 1-CA synthesized per volume; per day

1.5 M/1.8 M substrate and 13.58 g DCW/L biocatalyst in purely

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