

Heterologous expression and biochemical characterization of glucose isomerase from *Thermobifida fusca*

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Abstract Glucose isomerase (GIase) catalyzes the isomerization of D-glucose to D-fructose. The GIase from *Thermobifida fusca* WSH03-11 was expressed in *Escherichia coli* BL21(DE3), and the purified enzyme took the form of a tetramer in solution and displayed a pI value of 5.05. The temperature optimum of GIase was 80 °C and its half life was about 2 h at 80 °C or 15 h at 70 °C. The pH optimum of GIase was 10 and the enzyme retained 95 % activity over the pH range of 5–10 after incubating at 4 °C for 24 h. Kinetic studies showed that the K_m and K_{cat} values of the enzyme are 197 mM and $1,688 \text{ min}^{-1}$, respectively. The maximum conversion yield of glucose (45 %, w/v) to fructose of the enzyme was 53 % at pH 7.5 and 70 °C. The present study provides the basis for the industrial application of recombinant *T. fusca* GIase in the production of high fructose syrup.

Keywords Characterization · Expression · Glucose isomerase · *Thermobifida fusca* · *Escherichia coli*

Introduction

D-Xylose isomerase (EC 5.3.1.5) is an intracellular enzyme whose physiological function is to isomerize D-xylose to

D-xylulose. In addition, this enzyme also catalyzes the isomerization of D-glucose to D-fructose. Hence, it is often referred to as glucose isomerase (GIase). GIase is one of the key enzymes in the industrial production of high fructose syrup (HFS), which is a mixture of glucose and fructose. As it is very sweet and has a low caloric content, HFS is widely used in soft drinks and other food products as a sucrose succedaneum [1]. Usually, HFS is produced from corn starch by three consecutive enzymatic steps: liquefaction, saccharification and isomerization [2]. In the first two steps, corn starch is converted into dextrin and glucose. In the last step, glucose is converted into fructose by GIase [3, 4].

GIses have been found to exist in both prokaryotes and eukaryotes [5]. Based on primary amino acid sequence homology, GIses are classified as classes I or II. The class II enzymes contain an additional insert of about 50 amino acid residues at N-terminus, which is not present in the class I enzymes [6]. Although the homology of the primary sequences of the two classes is low (25–30 %), their three-dimensional structures are similar [7]. Most forms of GIase are homo-tetramers composed of two tightly bound dimers, which are associated with non-covalent bonds [5]. Each subunit contains two domains: a N-terminal major domain folded as an eight-stranded α/β catalytic pocket and a C-terminal minor domain folded as a large loop that embraces the adjacent subunit [8].

Currently, most GIses used in HFS production are from microorganisms, such as *Streptomyces* sp. [9, 10], *Streptomyces olivaceoviridis* [11], *Streptomyces olivochromogenes* [12–14], *Arthrobacter* sp. [15] and *Actinoplanes missouriensis* [16–18]. All of these strains belong to *Actinomycetales* and the GIses produced by them belong to class I. These GIses perform well under the production conditions of the HFS industry, in which the temperature is usually 55–65 °C and the pH is 7.0–8.5.

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In the present study, a GIase from a thermophilic actinomycete, *Thermobifida fusca*, was cloned and expressed in *Escherichia coli*. The recombinant protein was purified and its biochemical properties were investigated in detail.

Materials and methods

Strains and reagents

The *T. fusca* WSH03-11 strain [19] was isolated from soil samples and stored in our laboratory. *E. coli* BL21(DE3) and the plasmid pET24a (+) were purchased from Novagen (Madison, WI, USA). The EZ-10 Spin Column Plasmid Mini-Preps kit and agarose gel DNA purification kit were purchased from Tiangen Biotech Co. Ltd. (Beijing, China). Prime STAR[®]HS DNA polymerase, restriction enzymes, CIAP, and T4 DNA ligase were obtained from TakaRa (Dalian, China). DNA primer syntheses and DNA sequencing were performed by Shanghai Sangon Biological Engineering Technology & Services Co. Ltd. (Shanghai, China). Tryptone and yeast extract were purchased from Oxoid (Hampshire, UK). Isopropyl β -D-1-thiogalactopyranoside (IPTG) was purchased from Sigma-Aldrich (Milwaukee, WI, USA). Middle molecular weight markers for SDS-PAGE were purchased from Genaray (Shanghai, China). Molecular weight markers for gel filtration were purchased from Sigma. *pI* markers and broad *pI* kit 3–10 were purchased from GE Healthcare. Other chemicals were obtained from Sinopharm Chemical Reagent Co. Ltd. (Shanghai, China).

Gene cloning

The gene encoding GIase was amplified by standard polymerase chain reaction methods using the *T. fusca* WSH03-11 genomic DNA as template. The cloning primer sequences were designed according to gene *Tfu-1603* (GeneID: CP000088.1) as follows: CATATGAGCAACTACCAGCCCACACCCGAG (forward primer) and AAGCTTTTAGCGCACGCCAGGAGGTAGT (reverse primer). The *NdeI* and *HindIII* restriction sites (underlined) were designed into the primers. The amplification was carried out under the following conditions: the first step was at 95 °C for 4 min; followed by 30 cycles of 98 °C for 10 s, 55 °C for 5 s, and 72 °C for 2 min; and the final extension was carried out at 72 °C for 8 min. The PCR product was gel purified and then ligated into pMD18-T. The recombinant plasmid pMD18-T/*xyIA* was transformed into *E. coli* JM109 and was identified by restriction analysis and sequencing. pMD18-T/*xyIA* was digested with *NdeI* and *HindIII*. The target gene was gel purified and then ligated into plasmid pET24a (+), which was subjected to a similar

treatment. The recombinant plasmid pET24a (+)/*xyIA* was transformed into *E. coli* JM109 and was identified by restriction analysis. The resulting expression vector was transformed into *E. coli* BL21(DE3) for expression.

Expression of recombinant GIase

To express the recombinant enzymes, recombinant *E. coli* BL21(DE3) was inoculated into 100 mL of Luria–Bertani (LB) medium containing 30 μ g/mL kanamycin (Kana) and grown overnight at 37 °C in an orbital shaker at 200 rpm. The overnight culture was inoculated into fresh TB medium and shaken (200 rpm) at 37 °C until the OD₆₀₀ reached 1.5. The recombinant enzyme was induced by the addition of IPTG to a final concentration of 0.05 mM. Incubation was continued for another 25 h at 25 °C, and the cells were harvested by centrifugation at 8,000 rpm for 10 min at 4 °C.

Purification of recombinant GIase

Cells were separated from the fermentation medium by centrifugation at 10,000 rpm for 5 min and suspended in the same volume of 50 mM Na₂HPO₄–KH₂PO₄ buffer (pH 7.5). The suspension was sonicated on ice for 10 min at 38 % output power and centrifuged (13,000 rpm, 30 min, 4 °C) to remove insoluble denatured proteins. The supernatant was used as the crude enzyme preparation. The activity of the crude enzyme preparation was determined as the yield of GIase in the fermentation broth.

The crude enzyme preparation was heated for 10 min at 70 °C, and the soluble fractions were recovered after centrifugation at 13,000 rpm at 4 °C for 30 min. The enzyme preparation was then filtered (0.22 μ m membrane) and loaded on to a DEAE-Sepharose Fast Flow column that had been pre-equilibrated with 30 mM Na₂HPO₄–KH₂PO₄ buffer (pH 7.5). The column was eluted using a linear gradient of 0–1 M NaCl in the same buffer using an ÄKTA[™] protein purification system. The active-peak fractions were pooled and loaded onto a Superose G-75 gel filtration column and eluted with Na₂HPO₄–KH₂PO₄ buffer, and the active-peak fractions were pooled, concentrated, and stored at –80 °C.

Enzyme activity assay

The activity of GIase was measured according to the amount of D-fructose isomerized from D-glucose. The reaction mixture (1 mL) contained 50 mM Na₂HPO₄–KH₂PO₄ buffer (pH 7.5), 800 mM D-glucose, 5 mM MgSO₄, and 0.1 mL of enzyme solution diluted appropriately. It was then incubated at 70 °C for 10 min and terminated by adding 1 mL of 0.5 M HClO₄. The mixture was

further diluted with double-distilled water. D-fructose formed in the reaction mixture was measured by the cysteine–carbazole–sulfuric acid method using a spectrophotometer [20, 21]. One unit (U) of enzyme activity was defined as the amount that produced 1 μM D-fructose per min under the above conditions.

Biomass determination

After incubation, the cell mass was obtained by centrifuging the culture broth at 12,000 rpm for 20 min and washing twice with distilled water in centrifuge tube of predetermined weights. The tube was dried in a hot air oven at 100 °C to a constant weight. The dry cell weight (DCW) of culture broth was then calculated.

Molecular weight determination

The molecular weight (M_r) of the subunit of GIase was determined by SDS-PAGE. The M_r of GIase in its native state was determined by gel filtration utilizing a Superdex 200 10/300GL gel filtration column, and β -amylase (200,000), alcohol dehydrogenase (M_r 150,000), albumin bovine serum (M_r 66,000), carbonic anhydrase (M_r 29,000), and cytochrome *C* (M_r 12,400) were used as M_r standards. The elution volume was determined in triplicate for all samples and standards.

Isoelectric point determination

The isoelectric point of GIase was determined by 7.5 % polyacrylamide gel isoelectric focusing. Standard proteins and samples were mixed with gel, cathode solution (1 M NaOH), and anode solution (1 M H_3PO_4). Standard proteins were amyloglucosidase (pI 3.50), trypsin inhibitor (pI 4.55), b-lactoglobulin A (pI 5.20), carbonic anhydrase B (bovine) (pI 5.85), myoglobin acidic band (pI 6.85). The relative distance was determined in triplicate for all samples and standards.

Temperature optimum and thermostability

The optimal temperature of the GIase was measured in the temperatures range of 40–95 °C. The thermostability was determined by incubating the enzyme in 30 mM Na_2HPO_4 – KH_2PO_4 buffer (pH 7.5) containing 5 mM MgSO_4 at 70 and 80 °C. At different intervals, samples were taken and assayed at 70 °C for residual isomerizing activity. The measurements were carried out in three independent experiments.

pH optimum and stability

The pH optimum of the GIase was measured over a pH range of 4.0–11.0 using 30 mM NaAc–HAc buffer (pH

4.0–5.0), 30 mM Na_2HPO_4 – KH_2PO_4 buffer (pH 5.0–9.0), and 30 mM Gly–NaOH buffer (pH 9.0–11.0). To determine the pH stability, the enzyme was preincubated in the various buffers described above at 4 °C for 48 h, and then assayed for residual isomerizing activity at pH 7.5. The measurements were carried out in three independent experiments.

Determination of kinetic parameters

The catalytic properties of the enzyme were determined in Na_2HPO_4 – KH_2PO_4 buffer (pH 7.5) at 70 °C using glucose as the substrate. Substrate concentrations were in the range of 30–900 mM. The Michaelis–Menten parameters, V_{max} , K_m , and K_{cat} , were calculated from double reciprocal plots of the reaction curve [22]. The measurements were carried out in three independent experiments.

Isomerization of glucose to fructose

Fructose was produced by incubation of 45 % (w/v) glucose in 30 mM Na_2HPO_4 – KH_2PO_4 buffer (pH 7.5) containing 5 mM MgSO_4 and GIase (at a final activity of 20 U/g glucose) at 70 °C. Samples were withdrawn and analyzed by HPLC.

HPLC analysis

At different intervals, 100 μL of reaction mixture was taken and incubated at 100 °C for 10 min to inactivate the enzyme. The mixture was diluted to 1/100, centrifuged at 12,000 rpm for 10 min, and filtered (0.22 μm). Treated samples of 5 μL were loaded on to an Aminex HPX-87H ion Exclusion Column (7.8 mm \times 300 mm) pre-equilibrated with the buffer (0.001 M H_2SO_4 solution). The column was eluted with the same buffer using an Agilent separation module (model 1200), the temperature of the column was set at 50 °C, and a refractive index detector (model 1200) was used. The measurements were carried out in three independent experiments.

Fed-batch fermentation

The recombinant *E. coli* BL21(DE3) was cultured in LB medium (containing 30 $\mu\text{g}/\text{mL}$ Kana). A 10 % (v/v) inoculum concentration was inoculated into the fermentation medium for fed-batch cultivation in a 3-L fermentor (BioFlo 110, New Brunswick Scientific Co, Edison, NJ, USA). Fed-batch cultivation consisted of three phases: the first phase was batch cultivation with an initial glycerol concentration of 8 g/L at 37 °C. After inoculation, the pH and glycerol content decreased gradually. The end of glycerol consumption was detected by a sudden increase in

both dissolved oxygen (DO) and pH value, and then the second phase (the pre-induction phase of fed cultivation) started. When a DCW of 25 g/L was reached, the inducer was fed at 0.2 g/L/h and the temperature was lowered to 30 °C for GIase production, and then the third phase (the induction phase of fed cultivation) began. In the present study, a two-stage feeding strategy was applied. During the pre-induction phase, the glycerol feeding rate was increased exponentially according to the exponential feeding method [23], and cell growth was controlled at a specific growth rate of 0.22. When the induction phase began, the feeding rate was shifted to a gradient-decreasing method. During the entire process, the pH was maintained at 7.2 by the addition of 100 % (v/v) ammonia solution. The DO level was kept at 30 % of air saturation by adjusting the cascading impeller speed and supplementing with oxygen. The DO concentration, pH, temperature, and impeller speed were recorded using advanced fermentation software (AFS) from New Brunswick Scientific Co. Inc.

Results and discussion

Selection of the encoding gene of GIase

T. fusca is a moderately thermophilic soil actinomycete that grows in an environment with a temperature range of 40–70 °C and pH range of 4–10 [24]. A search for the *T. fusca* YX genome in the NCBI database yielded two possible GIases: one is Tfu_1603, which is 385 amino acids long; the other is Tfu_2709, which is 305 amino acids long. The structure modeling showed that Tfu_1603 exhibits a typical GIase structure with an N-terminal major domain and a C-terminal minor domain (Fig. 1a), whereas Tfu_2709 only contains the N-terminal domain of a GIase and lacks the C-terminal domain (Fig. 1b).

Cloning, expression, and purification of GIase

The GIase gene was amplified from the genomic DNA of *T. fusca* WSH03-11 using primers designed according to the *Tfu_1603* gene. For expression, the gene was ligated into the expression vector of pET24a(+), and the resulting plasmid was transformed into *E. coli* BL21(DE3). After 25 h of induction, the activity of GIase reached 21 U/mL. The recombinant GIase was isolated and purified from the cultured cells by sonication, thermo-denaturation, ion exchange chromatography, and gel filtration. The final specific activity of the purified GIase was 33.8 U/mg.

Physical properties of the recombinant GIase

The M_r of GIase was found to be 165 kDa, as determined by Superdex 200 gel filtration chromatography, whereas the M_r of the subunit of GIase, as determined by SDS-PAGE, was found to be 42 kDa. Thus, it seemed that GIase was composed of homo-tetrameric subunits, which is consistent with a previous study that reported GIase is usually a tetramer or dimer [5]. The pI value of *T. fusca* GIase is 5.05, as determined by polyacrylamide gel iso-electric focusing.

Effect of metal ions on recombinant GIase

It was reported that GIase is usually activated by Co^{2+} , Mg^{2+} , or Mn^{2+} ions and inhibited by Ca^{2+} ions [5]. To determine the effect of various metal ions on recombinant *T. fusca* GIase, the purified GIase was incubated with 1 mM EDTA at 4 °C for 30 min and the remaining activity was measured. The results showed that the residual enzyme activity was 6 %. When various metal ions (2 mM) were added to the treated sample, different activation effects on the GIase were found, in which $\text{Co}^{2+} > \text{Mg}^{2+} > \text{Mn}^{2+}$ (Table 1). The role of these metal ions is to form a bridge between the enzyme and the

Fig. 1 Structure models of a hypothetical GIase from *T. fusca*. **a** TFU_1603, **b** TFU_2709. The structure models of TFU_1603 and TFU_2709 were simulated by Swiss model server according to the crystal structure of 1 MUW and 3 AAL, respectively

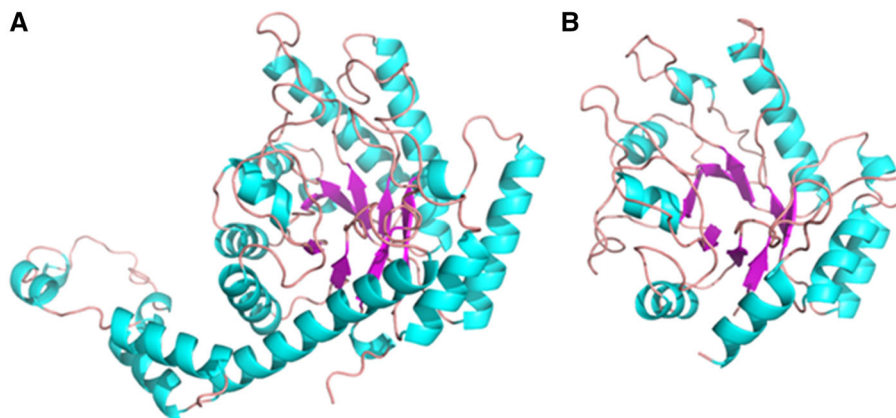


Table 1 Effect of EDTA and various metal ions on the activity of Glase

	Control	EDTA (1 mM)	CaCl ₂ (2 mM)	MnCl ₂ (2 mM)	MgCl ₂ (2 mM)	CoCl ₂ (2 mM)
Relative activity (%)	100 ± 1.7	6 ± 1.1	6 ± 1.3	44 ± 1.6	268 ± 2.1	456 ± 2.8

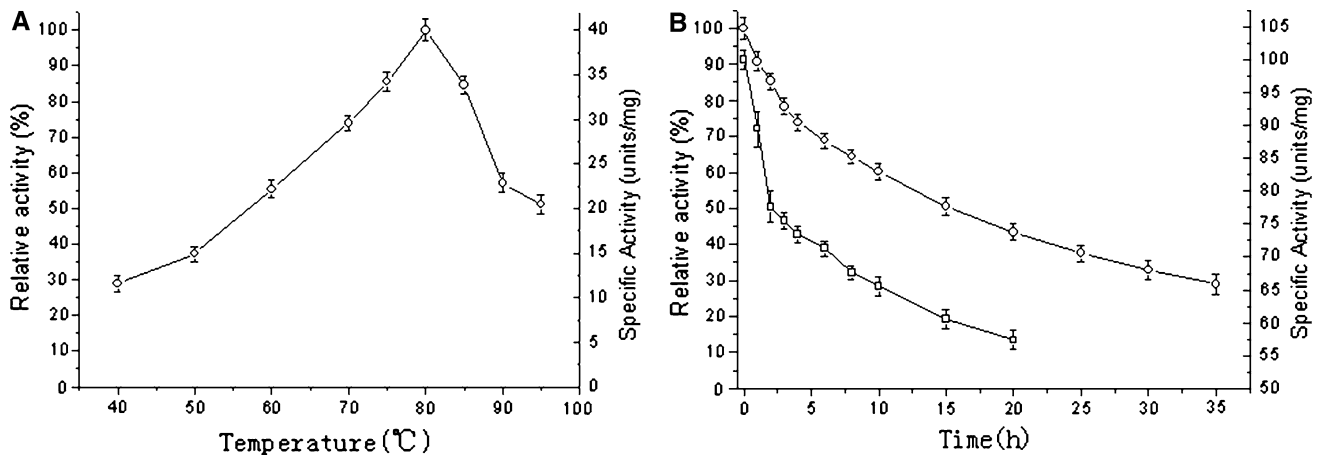


Fig. 2 Temperature optimum and thermostability of recombinant Glase. **a** Temperature optimum. The activity of Glase at 80 °C was defined as 100 %. **b** Thermostability at 70 °C (unfilled circle) and

80 °C (unfilled square). The activity of the Glase without heat treatment was defined as 100 %

sugar in the enzyme-substrate complex. From the various 3D structures of the enzyme that were determined in the presence of metal ions and substrate, product, or their analogs, it has been concluded that there are two metal-ion-binding sites. Metal site 1 is four-coordinated and tetrahedral in the absence of substrate and is six-coordinated and octahedral in its presence. Metal site 2 is octahedral in all cases and is involved in the binding of oxygen atoms O1 and O2 of the substrate [8]. It has been reported that metal cations that have ionic radii ≤ 0.8 Å, such as Mg²⁺, Mn²⁺, Co²⁺, and Fe²⁺, can activate Glase, while larger alkali earth metal cations Ca²⁺, Ba²⁺, Sr²⁺, and transition metal cations Hg²⁺, Pb²⁺, Ni²⁺, Cu²⁺, Cd²⁺ inhibit Glase [25, 26]. The current experimental results verified these theories, the Mg²⁺ or Co²⁺ enhance the catalytic activity of Glases, while Ca²⁺ inhibits the activity of Glases.

Optimal temperature and thermostability of recombinant Glase

The influence of temperature on the enzyme activity was investigated in the range 40–95 °C in 30 mM Na₂HPO₄–KH₂PO₄ buffer (pH 7.5) containing 5 mM MgSO₄. The results showed that the optimal temperature of the purified Glase is 80 °C, and the activity decreased rapidly with further increases in temperature, at 70 °C, was found to be about 75 % of its maximal activity (Fig. 2a). The thermostability experiments showed that the enzyme retains 50 % of its activity after 2.0 h at 80 °C or 15 h at 70 °C (Fig. 2b).

Optimal pH and stability of recombinant Glase

The pH optimum and stability of Glase were measured over a pH range of 4.0–11.0. The optimum pH of the Glase was 10.0, and the activity of the enzyme at pH 7.5 was 78 % of its maximal activity (Fig. 3a). The Glase retained more than 95 % of its initial activity after incubation in the pH range 5.0–10.0 at 4 °C for 24 h, but the residual activity decreased rapidly at pH values lower than 5 or higher than 10 (Fig. 3b).

Kinetic analysis of recombinant Glase

The kinetic properties of the purified Glase were analyzed using glucose as the substrate through the double reciprocal curve of the initial conversion rate and substrate concentration. At pH 7.5 and 70 °C, the K_m , K_{cat} , and K_{cat}/K_m values of the Glase were 197 mM, 1,680 min⁻¹, and 8.56 min⁻¹ mM⁻¹, respectively (Table 2). To our knowledge, this is the highest catalytic efficiency reported for class I Glases.

To explain why *T. fusca* Glase is more stable and have a high catalytic efficiency, the crystal simulation structure models of *T. fusca* Glase and other Glases were studied. These Glases come from the strains: *Streptomyces olivaceoviridis* [10], *Streptomyces olivochromogenes* [9, 12–14, 27], *Streptomyces rubiginosus* [28–30], *Arthrobacter* sp. [15], and *Actinoplanes missouriensis* [12, 15, 16, 31–36], which all have good performance under application

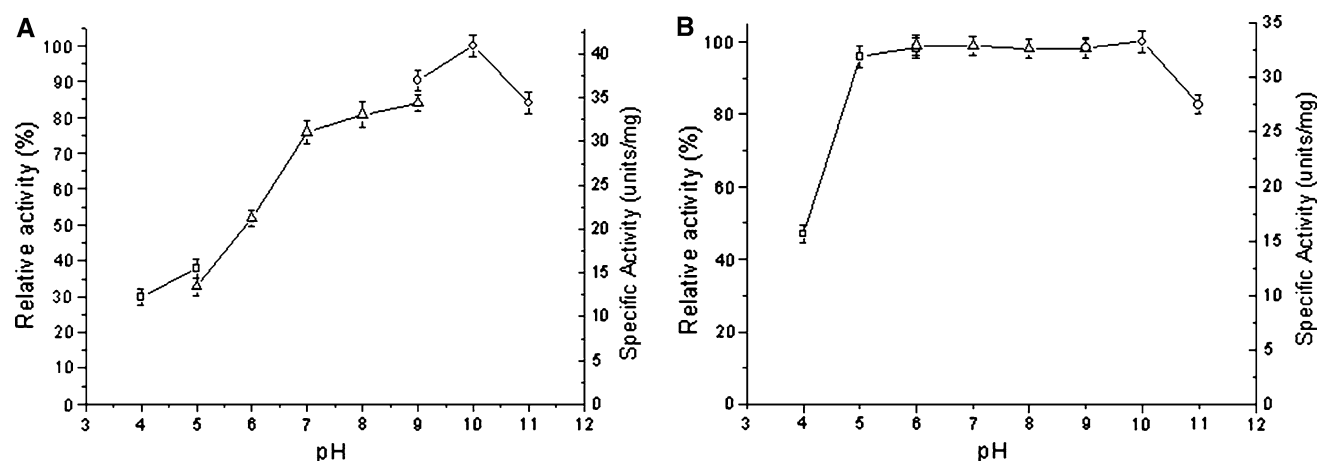


Fig. 3 Effects of pH on the activity and stability of Glase. **a** pH optimum. The activity of the Glase at pH 10.0 was defined as 100 %. **b** pH stability. The activity of the Glase without treatment was

defined as 100 %. NaAc-HAc buffer (unfilled square), Na₂HPO₄-KH₂PO₄ buffer (unfilled triangle) and Gly-NaOH buffer (unfilled circle)

Table 2 Comparison of the kinetic parameters of Glases from different sources

Organism	Temp (°C)	K_{cat} (min ⁻¹)	K_m (mM)	K_{cat}/K_m (min ⁻¹ mM ⁻¹)	References
Class I					
<i>Thermobifida fusca</i>	70	1,688	197	8.6	This work
<i>Arthrobacter</i> sp.	60	1,190	210	5.7	[29]
<i>Actinoplanes missouriensis</i>	60	1,494	290	5.2	[39]
<i>Streptomyces olivochromogenes</i>	60	760	220	3.4	[12]
<i>Streptomyces griseoflavus</i>	60	230	250	0.9	[29]
<i>Thermus aquaticus</i>	70	294	93	3.2	[40]
Class II					
<i>Bacillus stearothermophilus</i>	60	330	220	1.5	[29]
<i>Thermoanaerobacter saccharolyticum</i>	65	315	120	2.6	[42]
<i>Thermoanaerobacter thermosulfurigenes</i>	65	265	142	1.9	[41]
<i>Thermoanaerobacter maritima</i>	90	810	118	6.9	[43]
<i>Thermoanaerobacter neapolitana</i>	90	1,139	88.5	12.9	[44]

conditions of HFCS industrial production. *T. fusca* Glase structures model (Fig. 4) was simulated by Swiss Modle according to the known GIs crystal structures. It was found that nine amino acid residues (88P, 89M, 134T, 180A, 214G, 243F, 244H, 284P, 286H) intensively located at or near to the bottom of “active center pocket” in *T. fusca* were conservative in corresponding sites of above Glases, but the nine conserved amino acids were not all exist in the Glases with poor performance under application conditions. It was interesting that some amino acid residues containing annular structure were introduced to *T. fusca* Glase sites 88P, 243F, 244H, 284P, 286H, which might increases steric constraints for substrate glucose. However, these amino acid might used their ring structures to make glucose molecule form a more favorable posture while enter active center, hereby to speed up catalytic action. In addition, these rings may increase the stability of substrate

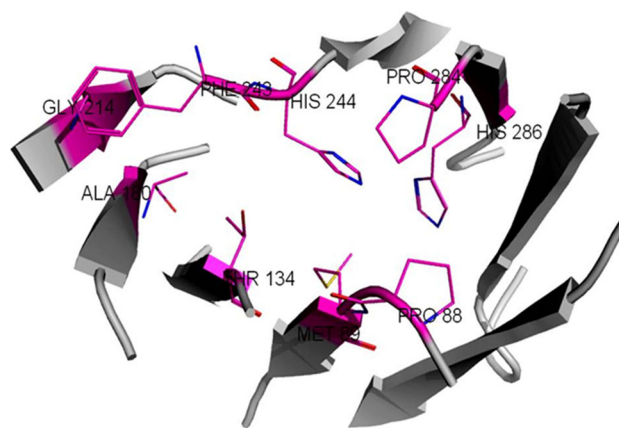


Fig. 4 The bottom of active center pocket of *T. fusca* Glase structures model. *T. fusca* Glase model, based on template [1 MUW _A] (0.86 Å), Sequence Identity 69.95 %, Evaluate: 3.79e-159, QMEAN Z score: -0.98

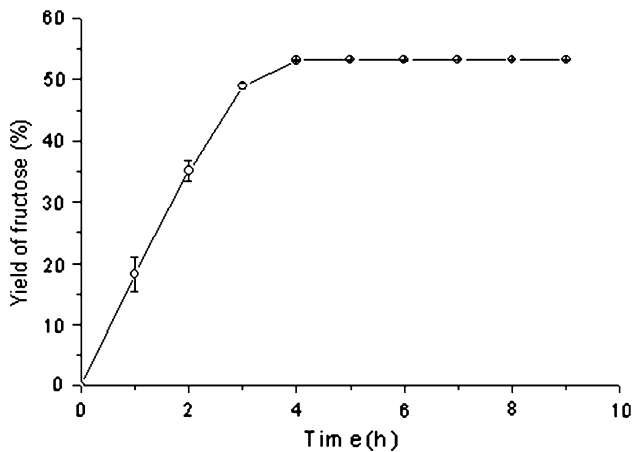


Fig. 5 Isomerization process of glucose to fructose. 45 % (w/v) glucose in 30 mM Na₂HPO₄–KH₂PO₄ buffer (pH 7.5) containing 5 mM MgSO₄ was incubated at 70 °C with GIase (20 U/g glucose)

domain. What the other structural features of *T. fusca* GIase make it more stable and more high catalytic efficient, here need more experiments to test.

Isomerization of glucose to fructose by recombinant GIase

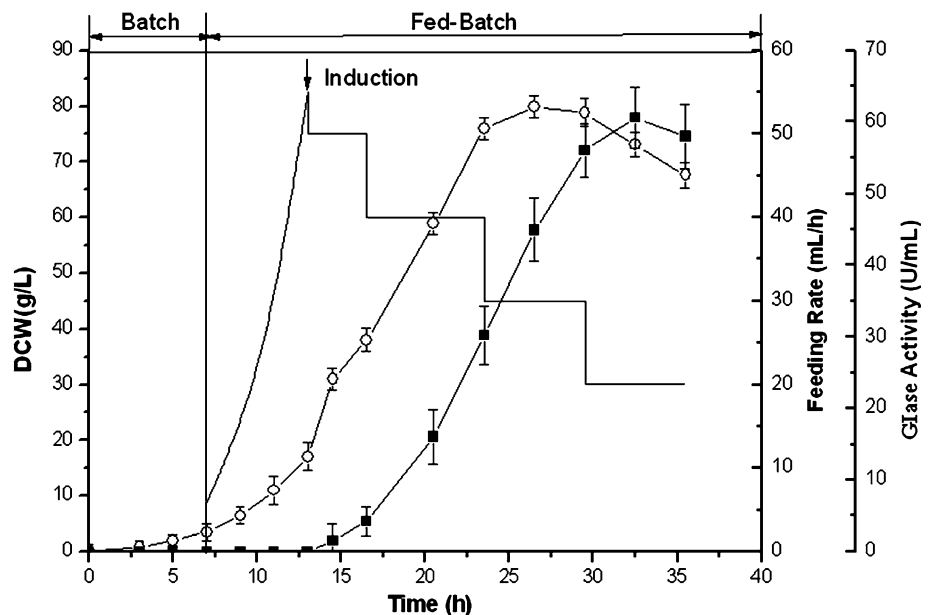
The proportion of D-glucose isomerized to D-fructose by GIase is critical to its industrial application to HFS production. To investigate the conversion ability of the *T. fusca* GIase, the recombinant GIase was utilized to isomerize glucose to fructose at pH 7.5 and 70 °C, with 45 % (w/v) glucose as substrate. The results showed that the concentration of fructose in the reaction mixture increased rapidly during the initial reaction phase and the isomerization

reached equilibrium within 4 h. The yield of fructose reached 53 % (Fig. 5), which was comparable to the yields reported in the literature at similar reaction temperatures. Previously, although the yields of fructose using some thermostable GIases from hyperthermophiles were reported to reach 55 % [37–41], the reaction temperature used by these authors was not less than 90 °C. Such high temperatures would increase the by-products and energy consumption. Moreover, the activity of these thermostable GIases declined sharply as the reaction temperature increased.

High cell-density fermentation

An excessive production of enzyme via a high-density fermentation strategy is an effective way to reduce production costs. High-density fermentation of engineered *E. coli* was performed in a 3-L fermentor. The fed-batch cultivation consisted of three phases: a batch cultivation phase, a pre-induction phase of fed cultivation, and the induction phase of fed cultivation. The culture temperature during the batch phase was 37 °C. When the carbon source of the medium was consumed, the pre-induction phase of fed cultivation started, in which the glycerol feeding rate was increased exponentially. When a DCW of 25 g/L was reached, the induction phase of fed cultivation was initiated. The feeding rate was shifted to a gradient-decreasing method, and the temperature was decreased to 30 °C for GIase production. After cultivation for 33 h, the yield of GIase reached 60.6 U/mL (Fig. 6). To our knowledge, the production of GIase in the present study is the highest level.

Fig. 6 Fermentation process of recombinant GIase. Bacteria concentration (unfilled circle), enzyme activity (filled square), glycerol feeding rate (solid line). The arrow indicates the induction starting point



Conclusions

In summary, the Glase of *T. fusca* was cloned, expressed, and its biochemical properties were investigated in detail. The Glase displayed a high catalytic rate ($8.56 \text{ min}^{-1} \text{ mM}^{-1}$) and good thermal stability at pH 7.5 and 70 °C. The glucose conversion rate by the recombinant Glase reached 53 % (w/w) with 45 % glucose as substrate. In addition, the activity of the Glase reached 60.6 U/mL in a 3-L fermentor, which represents the highest yield reported so far. All of these properties of the *T. fusca* Glase indicate that it may be utilized in HFS production.

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