ORIGINAL PAPER

MafiCH: a general model for H₂O–CO₂ solubility in mafic magmas

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Received: 30 June 2021 / Accepted: 24 February 2022 / Published online: 19 March 2022 © The Author(s), under exclusive licence to Springer-Verlag GmbH Germany, part of Springer Nature 2022

Abstract

The solubility of $CO₂$ in mafic magmas is strongly dependent on magma composition, which ultimately affects magma storage conditions and eruptive behavior. Recent experimental work showed that previously published volatile solubility models for mafc magmas are not well calibrated at mid-crustal pressures (400–600 MPa). Using a simple thermodynamic model, here we construct a general CO₂ solubility model for mafic magmas by establishing the compositional dependence of two key thermodynamic parameters. The model is calibrated using experimental data from 10 magma compositions that span a range of pressures as well as silica (44–53 wt.%) and total alkali (2–9 wt.%) contents. We also survey the experimental literature for relevant H_2O solubility data to determine how to model H_2O solubility for these magmas. We combine these separate CO_2 and H_2O solubility models into a single general model for mixed-fluid (H_2O – CO_2) solubility in mafic magmas called MafCH. We test the MafCH model using experiments from three compositions that fall both within and beyond the calibrated range, and find that the model accurately constrains the $CO₂$ solubility of depolymerized magmas. Sensitivity tests identify that Na, Ca, and Al have the largest effect on CO_2 solubility while Si and Mg do not play a strong role in CO_2 solubility in mafc, depolymerized melts. Overall, saturation pressures calculated using the new model presented here are typically lower than those predicted by previous models. The model provides a new framework to interpret volcanic data from mafc magma compositions for which no experimental data is available.

Keywords Volatile solubility · Basaltic volcanism · Alkali basalts · Experimental petrology · Thermodynamics

Introduction

The solubility of volatiles in magmas plays a critical role in the storage conditions and eventual eruption of magma. At magma storage depths, carbon is the primary volatile element in the exsolved phase because it has a low solubility compared to H_2O and its solubility is very strongly pressure dependent (e.g., Holloway and Blank [1994\)](#page-21-0). Mafc magmas dissolve carbon as carbonate (e.g., Fine and Stolper [1986](#page-20-0); Blank and Brooker [1994\)](#page-20-1), and experimental work has shown

Communicated by Mark S. Ghiorso.

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that mafc magmas with variable alkali contents exhibit a very wide range of CO_2 solubilities (e.g., Dixon [1997;](#page-20-2) Lesne et al. [2011b](#page-21-1); Shishkina et al. [2014;](#page-21-2) Vetere et al. [2014;](#page-21-3) Allison et al. [2019](#page-20-3)). While the compositional dependence of $CO₂$ solubility in mafic magmas is notable, $H₂O$ solubility does not vary signifcantly by composition in mafc magmas (e.g., Moore et al. [1998](#page-21-4); Lesne et al. [2011a](#page-21-5); Iacono-Marziano et al. [2012\)](#page-21-6). Of course, most natural magmas contain a mixed (H_2O-CO_2) volatile phase, so while we focus primarily on $CO₂$ solubility in this work due to its significant compositional variability, we also assess H_2O solubility in order to model behavior in natural systems.

Knowledge of volatile solubility is required to constrain characteristics of the volcanic plumbing system using preeruptive volatile contents (e.g., Lowenstern [1995\)](#page-21-7). It is not typically feasible or reasonable, however, to conduct solubility experiments on an unstudied composition solely to interpret volcanic data. Instead, well-calibrated volatile solubility models can be used to determine these properties in unstudied magma compositions. Numerous models exist (e.g., Newman and Lowenstern [2002](#page-21-8); Papale et al. [2006](#page-21-9);

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Iacono-Marziano et al. [2012](#page-21-6); Duan [2014;](#page-20-4) Shishkina et al. [2014](#page-21-2); Ghiorso and Gualda [2015\)](#page-20-5), but it is not always clear which model is most appropriate for the volcanic system of interest (e.g., Wieser et al. [2022](#page-21-10)). The choice between similar volatile solubility models may ultimately be based on familiarity and ease of use. For example, the Volatile-Calc model (Newman and Lowenstern [2002](#page-21-8)), which uses the basalt model from Dixon ([1997\)](#page-20-2), is currently commonly used to calculate fuid-saturated isobars and melt inclusion saturation pressures for basaltic compositions. In the two decades since that model was published, however, additional experiments have provided updated solubility relationships (e.g., experiments on alkali-rich mafc magmas from Botcharnikov et al. [2005,](#page-20-6) Behrens et al. [2009,](#page-20-7) Pichavant et al. [2009,](#page-21-11) Lesne et al. [2011a,](#page-21-5) [b,](#page-21-1) Iacono-Marziano et al. [2012,](#page-21-6) Iacovino et al. [2013,](#page-21-12) Pichavant et al. [2014,](#page-21-13) Shishkina et al. [2014](#page-21-2), Vetere et al. [2014](#page-21-3), Iacovino et al. [2016](#page-21-14), Allison et al. [2019](#page-20-3), and Schanofski et al. [2019](#page-21-15)).

The applicability of volatile solubility models may be limited as a result of the pressure–temperature–compositional (*P*–*T–X*) range of experiments used to calibrate the models, which may partly explain why volatile solubility models can yield drastically diferent results (e.g., saturation pressures) for a single composition (refer to Wieser et al. [2022](#page-21-10) for detailed discussion regarding volatile solubility model diferences). For instance, Allison et al. [\(2019\)](#page-20-3) presented new H_2O – CO_2 experiments in six alkali-rich mafic magmas at pressures from 400 to 600 MPa and found that previously published models did not completely describe the $CO₂$ results. Allison et al. ([2019](#page-20-3)) instead calibrated individual thermodynamic models for $CO₂$ solubility that showed strong agreement with the experimental data for each of the six compositions. In Fig. [1,](#page-1-0) we show the 400 MPa fuid-saturated isobar (at 1200 °C) calculated using two of the Allison et al. ([2019\)](#page-20-3) individual models compared with results using six earlier volatile solubility models (colored curves; models described in Table [1](#page-2-0)). In the Etna composition (Fig. [1a](#page-1-0)), for a completely anhydrous magma (at $H_2O=0$ wt%), the models predict a sizeable range of dissolved CO_2 contents from \sim 2500 to \sim 4500 ppm at 400 MPa and 1200 °C. The models show even more disagreement for the Vesuvius composition (Fig. [1](#page-1-0)b), with calculated dissolved CO_2 contents from \sim 2500 to \sim 9000 ppm at anhydrous conditions. These results illustrate that the selection of volatile solubility model can strongly impact the interpretation of a volcanic system.

In this study, we develop a method to calculate mixedfluid (H_2O-CO_2) solubility calibrated for a wide range of mafc magma compositions at pressures up to 700 MPa. The model, called MafiCH, can be thought of as a combination of models. For $CO₂$ solubility, we use a thermodynamic approach adapted from Holloway and Blank ([1994\)](#page-21-0) and incorporate the full multicomponent composition into the model to achieve robust solubility relationships. We use experiments from Allison et al. ([2019](#page-20-3)) and additional sources to calibrate the model. H_2O solubility is calculated using an empirical method adapted from Lesne et al. $(2011a)$ $(2011a)$ based on an evaluation of H₂O solubility models using experimental data from the literature. To test the accuracy and applicability of the MafCH solubility model, we

Fig. 1 Comparison of previously published solubility models for mafc magmas. 400 MPa isobars calculated using diferent models for the (**a**) Etna and (**b**) Vesuvius compositions at 1200 °C. Isobars from Allison et al. [\(2019](#page-20-3)) are calculated using the individual thermody-

namic models. For models that allow for $fO₂$ input, Fe speciation was calculated using Kilinc et al. (1983) (1983) at NNO + 1 (see supplementary material Table S2)

h *T* dependence in VolatileCalc is not calibrated from experimental data; it is a direct result of the equation of state

The Shishkina et al. (2014) equations do not include a temperature term, but the model is calibrated from experiments conducted at 1200-1250 °C iThe Shishkina et al. ([2014\)](#page-21-2) equations do not include a temperature term, but the model is calibrated from experiments conducted at 1200–1250 °C

*Calculations for these models can also be performed using VESIcal (Iacovino et al. 2021) *Calculations for these models can also be performed using VESIcal (Iacovino et al. [2021](#page-21-20))

compare model calculations with experimental data from Fanara et al. [\(2015\)](#page-20-9) and Schanofski et al. ([2019](#page-21-15)) that were not used in the model calibration. Two of the tested compositions (trachybasalt and leucitite) are largely within the calibrated range of the model, while a third more silicic magma (phonolite) was tested to explore the compositional limits of the model. We next evaluate how the choice of solubility model can impact volcanic interpretation by comparing saturation pressures calculated by diferent models. Finally, we assess what might control $CO₂$ solubility in alkali-rich mafic magmas based on insights from this new general model.

Previously published models for H₂O–CO₂ **solubility in mafc magmas**

Before building a new model, we frst examine some of the approaches that have been used to model mixed-fuid $(H₂O₋CO₂)$ solubility in mafic compositions. We focus on six solubility models that calculate changes in solubility as a result of compositional variability over a wide range of conditions. The details of the six models examined here, including how they were accessed for this study, are summarized in Table [1.](#page-2-0)

Broadly speaking, these models vary as a result of how they are constructed and calibrated. First, solubility models are calibrated using experimental data, so the *P*–*T*–*X* range for which they are valid depends on the experiments incorporated into each model. Some models are constructed as a result of new experimental data, and thus have a very specifc compositional and pressure range. Some other models are comprehensive, in that they constrain volatile solubility for all magmas, from basalt to rhyolite, across a temperature and pressure range that encompasses conditions relevant for most natural systems. The treatment of carbon in comprehensive models is variable, as some models account for the fact that mafc end members dissolve carbon solely as carbonate while felsic magmas store carbon as carbon dioxide. Second, models vary in their mathematical construction, which can range from full multi-component models based in thermodynamics to purely empirical models with singleparameter inputs. One additional manner in which models can vary is in how they are available to users. Options may include applications that are specifc to an operating system (i.e., .app for Mac or .exe for Windows), other downloadable fle formats such as spreadsheets, or web-based calculators. However, some published models may not include any sort of calculator at all, or the calculator may be missing a desired function (e.g., a method to calculate saturation pressures). Fortunately, the recent publication of open-source tool VESIcal (Iacovino et al. [2021](#page-21-20)) for Python3 has addressed many of these issues of accessibility for a number of the previously published volatile solubility models.

VolatileCalc (Newman and Lowenstern [2002\)](#page-21-8) is a very commonly used tool for determining H_2O –CO₂ solubility relationships, and it employs the oldest model that we discuss in this work. VolatileCalc is available as an excel macro spreadsheet that incorporates separate solubility models for rhyolitic and basaltic magmas. The model for basalt in VolatileCalc comes from the work of Dixon ([1997](#page-20-2)), in which a simple thermodynamic model (Fine and Stolper [1986;](#page-20-0) Stolper and Holloway [1988](#page-21-23); Dixon et al. [1995](#page-20-10)) was calibrated using previously published experiments from four mafc compositions. In this approach, major element cation fractions from these compositions were combined into a single parameter called *Π*, where cations capable of bonding with carbonate $(Ca^{+2}$, Na^{+1} , K^{+1} , Mg^{+2} , Fe^{+2}) contribute to higher Π values and polymerizing cations $(A1^{+3}$ and Si^{+4}) lower the value of *Π*. *Π* was then linearly correlated with $CO₂$ solubility at a single pressure (100 MPa) to generate a relationship between *Π* and thermodynamic equilibrium. While applying this model to natural samples, Dixon ([1997](#page-20-2)) found that Π varied linearly with SiO_2 content in glasses from an alkalic ocean island suite, and so $SiO₂$ content was used as a proxy for Π . This simplified SiO_2 -based algorithm of Dixon [\(1997](#page-20-2)) was the model incorporated into VolatileCalc (Newman and Lowenstern [2002\)](#page-21-8). While very straightforward to use, this model is restricted to calculation of solubility for magmas with $\langle 49 \text{ wt\% SiO}_2 \rangle$ and is not recommended for use at pressures>500 MPa.

A more recent model by Iacono-Marziano et al. [\(2012](#page-21-6)) provided updated solubility relationships specifc to alkalirich mafc magmas. Iacono-Marziano et al. ([2012\)](#page-21-6) presented new experimental data on a trachybasalt composition from Etna volcano, and combined the new data with experiments from the literature to calibrate a volatile solubility model. They generated a multi-parameter ft to thermodynamic expressions to produce a semi-empirical model. The Iacono-Marziano et al. ([2012\)](#page-21-6) models for H_2O and CO_2 are largely controlled by a calculated parameter, NBO/O, which had been suggested in previous studies to strongly control $CO₂$ solubility (e.g., Brooker et al. [2001](#page-20-11)). NBO refers to nonbridging oxygens, or oxygens associated with network-modifying cations (i.e., oxygens bonded with K^{+1} , Na⁺¹, Ca⁺², Mg^{+2} , and Fe⁺²) rather than polymerizing tetrahedra (i.e., oxygens bonded with Si^{+4} , Ti^{+4} , and Al^{+3}). The CO_2 model from Iacono-Marziano et al. [\(2012\)](#page-21-6) also requires inputs of $FeO + MgO$, $H₂O$, and total alkali content.

Even more recently, Shishkina et al. ([2014](#page-21-2)) conducted experiments across eight diferent mafc compositions to assess volatile solubility. Like Iacono-Marziano et al. ([2012](#page-21-6)), Shishkina et al. ([2014](#page-21-2)) combined their new experiments with literature data to calibrate a model. The Shishkina et al. (2014) study published purely empirical fits for H_2O and CO_2 solubility at 1200–1250 °C. The Shishkina et al. ([2014\)](#page-21-2) equation for $CO₂$ is an exponential relationship with an updated *Π* parameterization, termed *Π**, for its compositional factor, while the equation for H_2O is a polynomial fit that depends on the $Na + K$ cation fraction composition of the magma. The Shishkina et al. [\(2014](#page-21-2)) study did not provide a recommendation for how to combine the equations for mixed fluid compositions (i.e., how to calculate H_2O and $CO₂$ partial pressures). The details of how we perform calculations for mixed-fuids using the Shishkina et al. ([2014\)](#page-21-2) model in this study (e.g., isobars in Fig. [1](#page-1-0)) are described in a footnote to Table [1](#page-2-0).

The fnal three volatile solubility models examined here are comprehensive thermodynamic models. The Papale model (Papale [1997;](#page-21-21) Papale and Polacci [1999](#page-21-22); Papale et al. 2006) was one of the first comprehensive H₂O–CO₂ solubility models, while Duan ([2014](#page-20-4)) and MagmaSat (Ghiorso and Gualda [2015\)](#page-20-5) were developed more recently. Each of these models surveyed the experimental literature and used these data to calibrate binary interaction parameters for their thermodynamic models that describe how the volatile species interact with diferent compositional components in the melt. The main ways these three models vary from one another are the specifc experiments that are used to calibrate each model, the equations of state used for the fuids (i.e., determination of fuid fugacity), and how diferent compositional elements are used in the interaction parameters. For example, both Papale et al. [\(2006\)](#page-21-9) and MagmaSat (Ghiorso and Gualda 2015) include an influence of H_2O on CO_2 solubility, though Papale et al. (2006) (2006) shows higher CO₂ solubility at low H₂O for basalts while MagmaSat (Ghiorso and Gualda [2015\)](#page-20-5) shows the opposite efect. Both Duan ([2014\)](#page-20-4) and MagmaSat (Ghiorso and Gualda [2015\)](#page-20-5) use the same equation of state (Duan and Zhang [2006](#page-20-12)), but difer in other ways, such as the treatment of carbon speciation $(CO₃$ and $CO₂$), which is accounted for in MagmaSat (Ghiorso and Gualda [2015\)](#page-20-5) but not Duan ([2014](#page-20-4)).

There are at least three additional models that can be used to constrain volatile solubility in mafc magmas, though we do not examine them in detail for this study for the reasons discussed here. The Lesne et al. [\(2011a](#page-21-5), [b](#page-21-1)) study measured solubility in three alkali-rich compositions, but the $CO₂$ model is calibrated only at low pressures \ll 200 MPa). The Lesne et al. ([2011b\)](#page-21-1) experiments were later incorporated into the Allison et al. [\(2019\)](#page-20-3) individual thermodynamic fits for CO_2 solubility. SolEx (Witham et al. [2012\)](#page-21-24) is a program that uses the Π formulation from Dixon ([1997](#page-20-2)), as well as solubility relationships for other volatile elements (S, Cl). However, it does not include a function to calculate saturation pressure, which is a particularly meaningful way to compare models used in this work. Finally, Eguchi and Dasgupta ([2018](#page-20-13)) is a model that constrains only the solubility of $CO₂$ at relatively anhydrous compositions, and so it is not relevant for many of the mixed-fuid magmatic systems we discuss here.

The MafCH model

We construct a new general model, called MafiCH, for calculating H_2O –CO₂ solubility as a function of mafic magma composition. The strength of the new $CO₂$ model we present in MafCH comes from its thermodynamic basis, use of the full multicomponent magma composition, and calibration across a wide P-X range within the realm of mafc magmas that dissolve carbon as $CO₃$. The $CO₂$ model is calibrated with thermodynamic data from 10 compositionally variable mafc magmas for which a wide pressure range of experimental data are available, including the six compositions from Allison et al. ([2019\)](#page-20-3). The full major element composition of these magmas was used to derive a relationship describing the thermodynamic parameters. Our primary focus is on $CO₂$ solubility, but the solubility of H_2O is critical for the interpretation of natural magmas that typically contain mixed H_2O –CO₂ fluids. Thus, we also explore H_2O solubility in mafic magmas based on the experimental literature and previously published models. Note that an excel spreadsheet is provided in the supplementary material to perform solubility calculations using the model. This spreadsheet does not use macros, so it should be compatible with a range of spreadsheet programs. We also include two Python3 scripts for functions that cannot be calculated in excel without the use of macros: degassing paths and a series of saturation pressures (i.e., for a large dataset). Full details for using these scripts are included in the supplementary material. We test the new MafCH model against recent experimental data for magma compositions both within and beyond the calibrated compositional range.

CO2 solubility in mafc magmas

The thermodynamic model for CO₂ solubility in mafic **magmas**

We use the simple thermodynamic model that was described by Fine and Stolper ([1986\)](#page-20-0) and Stolper and Holloway [\(1988\)](#page-21-23) to constrain the concentration of dissolved carbon in equilibrium with a pure $CO₂$ fluid. We selected this particular model because numerous studies of $CO₂$ solubility in mafic magmas (e.g., Holloway and Blank [1994;](#page-21-0) Thibault and Holloway [1994;](#page-21-25) Dixon et al. [1995;](#page-20-10) Lesne et al. [2011b\)](#page-21-1) including Allison et al. ([2019](#page-20-3)) found that the CO_2 solubility data from experiments showed strong agreement with this thermodynamic treatment. Complete details of the model are included in Holloway and Blank ([1994](#page-21-0)) and Allison et al. [\(2019](#page-20-3)) and briefy explained here. Note that because the vast majority

of solubility experiments for a single composition are performed at a constant temperature (typically 1200 or 1250 °C for mafc magmas), we do not possess the appropriate data to explore the temperature dependence of this model and thus present the model formulation at a constant temperature.

In this model, because $CO₂$ is stored in mafic magma as $CO₃$, $CO₂$ solubility is defined by the equilibrium of the reaction:

$$
CO2(vapor) + O2-(melt) = CO32-(melt).
$$
 (1)

The equilibrium constant (*K*) of this reaction at pressure *P* and constant temperature *T* is given by:

$$
K(P, T) = K_0(P_0, T_0) \times \exp\left[-\Delta V_r^{0,m} \times (P - P_0) \times (R \times T)^{-1}\right].
$$
\n(2)

Note that because this model assumes equilibrium with a pure $CO₂$ fluid, the pressure term in Eq. [2](#page-5-0) refers to the partial pressure of $CO₂$ in the system when dealing with a mixed-fluid (H_2O-CO_2) system. In Eq. [2,](#page-5-0) $K_0(P_0, T_0)$ is the equilibrium constant at a reference pressure and temperature. $\Delta V_r^{0,m}$ is the partial molar volume change of the condensed (melt) components of the reaction in Eq. [1](#page-5-1) and is considered to be independent of pressure and temperature. Thermodynamic parameters K_0 (P_0 , T_0) and $\Delta V_r^{0,m}$ are determined empirically for diferent magma compositions.

To calculate $CO₂$ contents from the equilibrium constant *K* (*P*, *T*) determined in Eq. [2,](#page-5-0) first calculate K_f :

$$
K_f = K(P, T) \times f_{\text{CO}_2}(P, T),\tag{3}
$$

then $X^m_{\text{CO}_3}$:

$$
X_{\text{CO}_3}^m = K_f \times \left(1 - K_f\right)^{-1},\tag{4}
$$

and finally wt% $CO₂$:

wt% CO₂ =
$$
(44.01 \times X_{\text{CO}_3}^m) \times \left\{ (44.01 \times X_{\text{CO}_3}^m) + \left[(1 - X_{\text{CO}_3}^m) \times FW_{\text{one}} \right] \right\}
$$
 (5)

In Eq. [5,](#page-5-2) 44.01 is the formula weight of $CO₂$ (in g mol⁻¹) and *FW*_{one} is the formula weight of the magma on a one-oxygen basis; for alkali basalt the value of *FW*one is 36.594 g mol⁻¹ (Holloway and Blank [1994\)](#page-21-0). In this work we treat FW_{one} as a constant value since it does not vary signifcantly for mafc magmas; values of *FW*one for the 10 compositions we use to calibrate our general model are within ± 1.4 g mol⁻¹ of the alkali basalt value.

The thermodynamic parameters $\Delta V_r^{0,m}$ and K_0 (P_0 , T_0) can be determined for diferent compositions from a linear regression of experimental data (i.e., Fig. 10 in Allison et al. [2019\)](#page-20-3). On a plot with ln $\int_{f_{\text{CO}_2}}(P, T) \times \left(X_{\text{CO}_2}^m\right)$ $\Big)^{-1}$ ver-

sus $[(P - P_0) \times (R \times T)^{-1}]$, where $X_{\text{CO}_2}^m$ is the mole fraction of dissolved $CO₂$, the slope of a linear regression through experiment data yields $\Delta V_r^{0,m}$ and the *y*-intercept corresponds to $-\ln K_0$. As explained above, *P* refers to the partial pressure due to $CO₂$ for a mixed-fluid experiment. Note that the values of $\ln \left[f_{\text{CO}_2}(P, T) \times \left(X_{\text{CO}_2}^m \right) \right]$ $\Big)^{-1}$ will differ based on the units of pressure used for the fugacity term. This diference will be a constant value for every experiment data point: the natural logarithm of the conversion between pressure units (i.e., values using $MPa = ln (0.1) + values using bars$. However, the value of $[(P - P_0) \times (R \times T)^{-1}]$ does not vary by pressure units since the value of the gas constant R will also change to account for diferent units. Consequently, the *y*-intercept and therefore K_0 will change depending on what pressure units are used, but $\Delta V_r^{0,m}$ depends only on the volume unit used for *R*.

The previous studies that have used this model published $\ln K_0$ values determined from pressure in bars, so we also use units of bars for calculations to maintain legacy consistency and then convert to SI units of MPa. In this work the reference conditions are 1000 bars (i.e., 100 MPa) and 1200 °C. The presence of the gas constant R necessitates that temperature be in units of Kelvin for calculations. Thus, the value of *R* used throughout this work is 83.144621 cm³ bar K⁻¹ mol⁻¹, and the units of $\Delta V_r^{0,m}$ are cm³ mol⁻¹.

Figure [2](#page-6-0) shows the effect of the thermodynamic parameters on CO_2 solubility. More negative values of $\ln K_0$ correlate with lower CO_2 solubilities for the same value of $\Delta V_r^{0,m}$. $\Delta V_r^{0,m}$ changes the curvature of the solubility curve such that larger values of $\Delta V_r^{0,m}$ result in lower CO₂ solubilities at pressures greater than P_0 for the same value of K_0 . Changes in K_0 and $\Delta V_r^{0,m}$ have greater impact on CO₂ solubility as CO₂ fugacity increases. For the reasons described above, values of $\ln K_0$ shown in Fig. [2](#page-6-0) were calculated using pressure in bars, and the solubility curve results were then converted to MPa.

This thermodynamic model requires information about the properties of the fuid (i.e., an equation of state) to perform calculations, even for a pure $CO₂$ system. We use the modifed Redlich–Kwong equation of state (Holloway [1977,](#page-20-8) [1981](#page-21-17), [1987\)](#page-21-18) with the Saxena and Fei ([1987\)](#page-21-19) high-pressure correction as detailed in the appendix of Holloway and Blank ([1994\)](#page-21-0). Because the thermodynamic model is calibrated by correlating $CO₂$ $CO₂$ $CO₂$ solubility with $CO₂$ fugacity (see Fig. 2), any volatile solubility calculations made using the model presented in this study must use this same equation of state (modifed Redlich–Kwong with high-pressure correction). This equation of state is internally consistent with this simple thermodynamic model, and it is specifcally calibrated in the *P*–*T* region of interest for crustal magmas. One of the

*Green ticks indicate corresponding pressure for pure $CO₂$ in 100 MPa increments (100 – 700 MPa)

Fig. 2 Impact of the thermodynamic parameters on CO_2 solubility. Properties of the $CO₂$ fluid (plotted on the *x*-axis) required for calculation of the curves are determined using the modifed Redlich– Kwong equation of state (Holloway [1977,](#page-20-8) [1981,](#page-21-17) [1987](#page-21-18)) with the Saxena and Fei [\(1987](#page-21-19)) high-pressure correction as detailed in the appendix to Holloway and Blank ([1994\)](#page-21-0). **a** At constant value of $\Delta V_r^{0,m}$

decreasing $\ln K_0$ values correlate with lower CO_2 solubilities. **b** At constant value of K_0 increasing $\Delta V_r^{0,m}$ correlates with lower slope and lower CO_2 solubilities. Note that values of $\ln K_0$ shown here were calculated using pressure in bars to maintain legacy consistency, and the solubility curve results were converted to MPa for the plot

more recent equations of state for H_2O and CO_2 (Duan and Zhang [2006\)](#page-20-12) was designed to be applicable over a very wide range of crustal conditions, and it yields very similar values of pure $CO₂$ and $H₂O$ fugacity to our selected equation of state (see supplementary material Table S1). For $CO₂$, these two equations of state begin to diverge slightly only at the highest pressures considered by this study $(>600$ MPa), with Duan and Zhang (2006) predicting slightly higher $CO₂$ fugacities.

Development of a general thermodynamic model for CO₂ **solubility in mafc magmas**

To produce a general model for $CO₂$ solubility in mafic magmas, we develop a compositional fit for parameters $\Delta V_r^{0,m}$ and K_0 (P_0 , T_0) (as $\ln K_0$) in the thermodynamic model (see Eq. [2\)](#page-5-0). To ensure a wide compositional range for this model, we calibrate this general model using the six compositions from Allison et al. ([2019\)](#page-20-3), which also incorporated experimental data from Iacono-Marziano et al. [\(2012\)](#page-21-6) and Lesne et al. [\(2011b\)](#page-21-1), as well as four additional compositions from the experimental literature (see Table [2](#page-7-0) and supplementary material Table S2). We selected these 10 compositions not only for their compositional diversity, but also because the available experiments were conducted over a wide pressure range (including experiments \geq 500 MPa) and had wellconstrained fluid compositions, particularly at low $X_{\text{H}_2\text{O}}^f$.

From the literature, we incorporate experiments from a basanite (Holloway and Blank [1994](#page-21-0)), leucitite (Thibault and Holloway [1994\)](#page-21-25), basalt (N72 from Shishkina et al. [2010\)](#page-21-26), and phonotephrite (AH3 from Vetere et al. [2014](#page-21-3)). The basanite and leucitite experiments were both previously used by Dixon ([1997\)](#page-20-2) to define Π , and contain lower SiO₂ than the compositions studied by Allison et al. ([2019\)](#page-20-3). We include the basalt (N72) experiments from Shishkina et al. ([2010](#page-21-26)) to extend the compositional range of the model to lower total alkali contents. The phonotephrite composition (AH3) from Vetere et al. ([2014](#page-21-3)) contains high total alkali contents (\sim 9 wt%), with different proportions of Na₂O and $K₂O$ compared to the high-alkali compositions from Allison et al. [\(2019\)](#page-20-3), in addition to higher $SiO₂$.

The compositional variability of the 10 magmas used to calibrate the general model for $CO₂$ is shown in Fig. [3.](#page-8-0) The magmas encompass a wide range of compositions, from 44 to 53 wt% SiO₂ and 2 to 9 wt% total alkalis (Na₂O + K₂O; Fig. [3](#page-8-0)a). The compositions not only show a wide range of silica and total alkali contents, but also diferent relative proportions of each alkali component. Importantly, the compositions also vary signifcantly in the other major elements (Fig. [3](#page-8-0)b). In Fig. [3](#page-8-0)b, the relative cation fractions of each composition are plotted compared to the Etna composition. No two compositions follow the same pattern in major element composition. For example, while the Sunset Crater composition shares similar Si^{+4} , Ti^{+4} , Al^{+3} , and Fe^{+2*} contents to the Etna composition, the two magmas vary in Mg^{+2} and $Ca⁺²$. The Stromboli and SFVF compositions follow similar trends in Ti^{+4} , Al^{+3} , and Fe^{+2*} , but SFVF has higher

Composition	$\Delta V^{0,m}$	$\ln K_0^a$	$\ln K_0^{\text{b}}$	Si^{+4}	Ti^{+4}	Al^{+3}	Fe^{+2*}	Mg^{+2}	Ca^{+2}	$Na+1$	K^{+1}
Compositions from Allison et al. (2019)											
Sunset Crater	16.40	-14.67	-12.37	0.439	0.012	0.176	0.085	0.119	0.097	0.061	0.009
SFVF	15.02	-14.87	-12.57	0.490	0.008	0.189	0.061	0.081	0.091	0.061	0.018
Erebus	15.83	-14.65	-12.35	0.439	0.019	0.205	0.080	0.046	0.069	0.108	0.033
Vesuvius	24.42	-14.04	-11.74	0.452	0.007	0.167	0.063	0.092	0.115	0.035	0.069
Etna	21.59	-14.28	-11.98	0.440	0.013	0.177	0.081	0.093	0.113	0.063	0.020
Stromboli	14.93	-14.68	-12.38	0.451	0.006	0.183	0.063	0.107	0.123	0.044	0.023
Compositions from other studies											
Basanitec	21.72	-14.32	-12.02	0.423	0.022	0.165	0.092	0.124	0.081	0.077	0.016
Leucitite ^d	21.53	-13.36	-11.06	0.407	0.019	0.139	0.070	0.126	0.141	0.057	0.041
AH3 phonotephrite ^e	30.45	-13.26	-10.96	0.447	0.006	0.161	0.057	0.079	0.106	0.123	0.021
N72 Basalt ^f	19.05	-14.86	-12.56	0.466	0.006	0.200	0.073	0.097	0.113	0.042	0.003

Table 2 Thermodynamic parameters, $\Delta V_r^{0,m}$ and ln K_0 for each composition with associated cation fractions used to construct the general model for $CO₂$

Note that only the elements listed in this table are included when normalizing cation fractions (i.e., phosphorus and manganese are not included) ^aln K_0 for pressure in bars; these values were used to calibrate Eq. [7](#page-8-1)

 b ln K_0 for pressure in MPa for comparison

c Basanite composition from Holloway and Blank ([1994\)](#page-21-0)

^dLeucitite composition from Thibault and Holloway ([1994\)](#page-21-25)

^e AH3 Phonotephrite composition from Vetere et al. ([2014\)](#page-21-3)

f N72 Basalt composition from Shishkina et al. [\(2010](#page-21-26))

 $*Fe^{+2}$ calculated from total iron expressed as FeO

 $Na⁺¹$ and lower Mg⁺² and Ca⁺² content than Stromboli. This strong variability in the calibration compositions serves to generate a robust model that can predict $CO₂$ solubility in numerous mafic magmas.

The thermodynamic parameters $\Delta V_r^{0,m}$ and K_0 (P_0 , T_0) have already been determined for eight of these compositions in the original publications of those experiments. Values of $\Delta V_r^{0,m}$ and K_0 (P_0 , T_0) were calibrated in Allison et al. [\(2019](#page-20-3)) for all six compositions in that study, in Holloway and Blank ([1994\)](#page-21-0) for the basanite, and in Thibault and Holloway [\(1994\)](#page-21-25) for the leucitite. Here we calibrate values of $\Delta V_r^{0,m}$ and K_0 (P_0 , T_0) for the N72 basalt (Shishkina et al. [2010\)](#page-21-26) and AH3 phonotephrite (Vetere et al. [2014\)](#page-21-3) using the linear regression method described in the previous subsection for inclusion in this model.

We used the following criteria to select experiments from the N72 basalt (Shishkina et al. [2010\)](#page-21-26) and AH3 phonotephrite (Vetere et al. [2014\)](#page-21-3) to generate the regressions for the thermodynamic parameters $\Delta V_r^{0,m}$ and K_0 (P_0 , T_0). First, all pure $H₂O$ experiments from both compositions and four experiments in Shishkina et al. ([2010\)](#page-21-26) without successful fluid composition determinations were excluded by necessity. Second, we excluded experiments with $X_{H_2O}^f$ values below 0.1. These studies determined fuid composition by the mass loss method, and for $X_{\text{H}_2\text{O}}^f$ values below 0.1, there is only a very small mass of H_2O in the fluid

 $(generally < 0.1 \text{ mg})$, so any uncertainty in this measurement can yield large errors in fuid compositions (see supplementary material). Third, we also excluded some experiments with very low values of $[(P - P_0) \times (R \times T)^{-1}]$, because the parameter determination method does not perform well at very low partial pressures of $CO₂$ (Holloway and Blank [1994](#page-21-0)). In particular, experiments with low $[(P - P_0) \times (R \times T)^{-1}]$ values and CO₂ abundances below ~ 175 ppm were targeted for exclusion. The experiments used to calibrate the thermodynamic parameters for AH3 (Vetere et al. [2014\)](#page-21-3) and N72 (Shishkina et al. [2010\)](#page-21-26) are listed in the supplementary material (Table S3).

To produce compositional relationships for the thermodynamic parameters ($\Delta V_r^{0,m}$ and $\ln K_0$), we use a multiple linear regression of cation fractions (Table [2\)](#page-7-0) from each composition. Note that because oxygen fugacity is not always measured in experimental or natural samples, we calculate cation fractions with all iron as FeO (Fe^{+2}) . Also, because the reporting of phosphorus and manganese is inconsistent in the literature, these elements are not included in the normalization of cation fractions. A series of multiple linear regressions yielded the following best-ft compositional relationships:

$$
\Delta V_r^{0,m} = \beta + \sum (\alpha_i \times D_i)
$$
 (6)

Fig. 3 Compositions included in the general model for CO2. **a** Total alkali and silica compositions of experiments. **b** Cation fractions of each composition as referenced to the Etna composition

i	α , value	Standard error	<i>p</i> value
$Si^{+4} + Na^{+1}$	3375.552	$+322.351$	0.0090
$Ti+4$	2625.385	$+320.521$	0.0146
Al^{+3}	3105.426	$±$ 320.252	0.0105
Fe^{+2*}	3628.018	$+332.137$	0.0083
$Mg^{+2} + Ca^{+2}$	3323.320	$+318.845$	0.0091
K^{+1}	3795.115	$+317.215$	0.0069
$Na+1$ $Na^{+1} + K^{+1}$	47.004	$+6.333$	0.0177

Table 3 Coefficients for $\Delta V_r^{0,m}$ equation

Cations that are combined together in this fnal equation were selected for combination because they had similar coefficients during preliminary regression analysis. Coefficient *β*=−3350.650±320.629, *p* value=0.0090

$$
\ln K_0 = \psi + \sum (\theta_i \times D_i)
$$
 (7)

where D_i indicates the cation fraction of element *i* and α_i , β_i , θ , and ψ are coefficients determined from the multiple linear regressions. Values for the coefficients are listed in Tables $3-4$. Values of $\ln K_0$ using Eq. [7](#page-8-1) require pressure in bars for calculations; if units of MPa are desired, subtract

Table 4 Coefficients for $\ln K_0$ equation

i	θ , value	Standard error	<i>p</i> value
Si^{+4}	114.098	$+32.444$	0.0390
$Ti^{+4} + Al^{+3}$	92.263	$+32.749$	0.0669
$Fe^{+2*} + Ca^{+2} + Na^{+1}$	122.644	$+32.578$	0.0317
Mg^{+2}	111.549	$+32.651$	0.0420
K^{+1}	138.855	$+34.092$	0.0267
$Na+1$ $Na^{+1} + K^{+1}$	2.239	$+0.640$	0.0396

Cations that are combined together in this fnal equation were selected for combination because they had similar coefficients during preliminary regression analysis. Coefficient $\psi = -128.365 \pm 32.578$, *p* value=0.0291

ln (0.1) from the result of Eq. [7.](#page-8-1) The values of $\Delta V_r^{0,m}$ and ln K_0 produced by Eqs. [6](#page-7-1) and [7](#page-8-1) are within ~3% and ~0.5%, respectively, of the values determined from the experimental data for each of the 10 calibration compositions (Table [2](#page-7-0)). This analysis suggests that the general model is robust and very accurately predicts $CO₂$ solubility in these 10 compositions.

Using the general thermodynamic model for CO₂ solubility **in mafc magmas**

The general model for $CO₂$ is well-calibrated for magmas that contain 44 wt% to 53 wt% SiO₂ and 2 wt% to 9 wt% total alkalis (Na₂O + K₂O) at pressures ranging from ~50 MPa to 700 MPa. Here we summarize the general procedure for application of the model to calculate the $CO₂$ solubility for any mafc magma composition. Calculators are available in the supplementary material (an excel spreadsheet and two Python3 scripts).

We first describe how to use the $CO₂$ model for a basic system: mafic magma in equilibrium with a pure $CO₂$ fluid. To begin, calculate the cation fractions for the composition of interest and use Eqs. $6-7$ $6-7$ to compute the thermodynamic parameters $\Delta V_r^{0,m}$ and K_0 . Next, calculate $K(P, \mathbb{R})$ *T*) from Eq. [2](#page-5-0); recall that *P* must be in units of bars, unless the calculated value of K_0 is converted to alternate pressure units. P_0 is 1000 bars and T is 1200 °C (convert *T* to Kelvin for calculations since gas constant *R* is present). Finally, use Eqs. [3](#page-5-3)–[5](#page-5-2) to transform $K(P, T)$ to wt% CO_2 . Note that $f_{\text{CO}_2}(P, T)$ in Eq. [3](#page-5-3) must be in the same pressure units as *P* and calculated using the modifed Redlich–Kwong equation of state (Holloway [1977](#page-20-8), [1981,](#page-21-17) [1987](#page-21-18)) with the Saxena and Fei ([1987\)](#page-21-19) high-pressure correction as detailed in the appendix of Holloway and Blank [\(1994](#page-21-0)). Use of a diferent equation of state would require recalibration of the thermo-dynamic parameters. In Eq. [5,](#page-5-2) the value of FW_{one} should be 36.594 g mol−1, since this constant value was used to determine the thermodynamic parameters for this model.

For mixed-fluid (H_2O-CO_2) compositions, the pressure and fugacity terms in Eqs. [2](#page-5-0) and [3,](#page-5-3) respectively, must be determined based on the proportion of $CO₂$ in the fluid. To determine the fugacity of $CO₂$ in a mixed-fluid magma, calculate the pure $CO₂$ fugacity at the total pressure of the system and then multiply the pure fugacity by the fuid composition $\left(1 - X_{\text{H}_2\text{O}}^f\right)$). The partial pressure of $CO₂$ can then be determined from this value of $CO₂$ fugacity using the equation of state (modifed Redlich–Kwong with high pressure correction).

H2O solubility in mafc magmas

Previous studies have suggested that H_2O is relatively insensitive to melt composition (Moore et al. [1998;](#page-21-4) Lesne et al. [2011a;](#page-21-5) Iacono-Marziano et al. [2012\)](#page-21-6). Partly for this reason, the Allison et al. [\(2019\)](#page-20-3) experiments were not designed to assess H_2O solubility, and those experiments did not show separate trends in $H₂O$ solubility according to composition. To explore the effect of composition on H_2O solubility, we compiled experimental data for 22 mafc magma

compositions (anhydrous $SiO_2 < 56$ wt%) with a wide variety of major element compositions (Fig. [4a](#page-10-0) and supplementary material Table S4) from 14 studies (Cocheo [1994](#page-20-14); Dixon et al. [1995](#page-20-10); Moore et al. [1995](#page-21-27), [1998](#page-21-4); Ohlhorst et al. [2001](#page-21-28); Berndt et al. [2002](#page-20-15); Botcharnikov et al. [2005;](#page-20-6) Di Matteo et al. [2006](#page-20-16); Shishkina et al. [2010,](#page-21-26) [2014](#page-21-2); Lesne et al. [2011a](#page-21-5); Vetere et al. [2011](#page-21-29), [2014](#page-21-3); Iacono-Marziano et al. [2012](#page-21-6)). The experimental data from these studies is included in the supplementary material (Table S5).

We frst examine this data compilation for possible compositional controls on H_2O solubility. We compare the H_2O contents of the experiments with H_2O fugacity, calculated using the modifed Redlich–Kwong equation of state (Holloway [1977](#page-20-8), [1981](#page-21-17), [1987\)](#page-21-18) with the Saxena and Fei [\(1987](#page-21-19)) high-pressure correction as detailed in the appendix of Holloway and Blank [\(1994\)](#page-21-0). For mixed-fuid experiments, we calculate the pure H_2O fugacity at the total pressure of the experiment and then multiply it by the experiment fuid composition $(X_{H_2O}^f)$ to determine H₂O fugacity. For clarity the data are separated into two groups: roughly half of the experiments, those with compositions falling within the grey region of Fig. [4](#page-10-0)a, are shown in Fig. [4](#page-10-0)b, while the remaining experiments are shown in an identical plot in Fig. [4](#page-10-0)c. In Fig. [4b](#page-10-0), c, we also plot the power-law ft for the Etna composition from Lesne et al. [\(2011a\)](#page-21-5) for comparison:

$$
f_{\text{H}_2\text{O}}^{1200 \text{ °C}} = 104.98 \times \text{wt\% H}_2\text{O}^{1.83} \tag{8}
$$

in which fugacity is in units of bars.

Overall, the H_2O solubility data (Fig. [4b](#page-10-0), c) do not show any clear relationship to composition, and most of the exper-iments closely follow the Lesne et al. ([2011a\)](#page-21-5) power-law fit for Etna (Eq. [8\)](#page-5-1). Note that the experimental data (Fig. [4b](#page-10-0), c) is quite limited above \sim 5 wt% H₂O, which likely reflects the difficulty in quenching hydrous glasses. This data compilation lends further support to the conclusion of previous studies (e.g., Moore et al. [1998](#page-21-4); Lesne et al. [2011a](#page-21-5); Iacono-Marziano et al. 2012) that $H₂O$ solubility in mafic magmas is not strongly afected by melt composition. If there is an efect, it cannot be resolved over the broad compositional range of the current experimental literature, but it merits future careful investigation.

There exist several H_2O solubility models calibrated specifcally for alkali-rich mafc magmas (e.g., Iacono-Marziano et al. [2012](#page-21-6); Shishkina et al. [2014\)](#page-21-2), and we next evaluate how these models perform for this compilation of data. We plot the diference between the experimental data and the modelcalculated H_2O solubility in Fig. [4](#page-10-0)d, e. The average difference between measured H_2O and calculations of H_2O content using the Lesne et al. ([2011a\)](#page-21-5) power-law ft for Etna for all experiments in this compilation is 0.35 wt% (median: 0.25 wt%), with a maximum difference of 1.68 wt%. Using the Iacono-Marziano et al. [\(2012\)](#page-21-6) model, however, the average diference

Fig. 4 H_2O solubility experiments compared with models for mafic magmas. **a** Total alkali and silica compositions of experiments. **b** Experiments for compositions in the grey region of (**a**) compared with the Lesne et al. [\(2011a](#page-21-5)) power-law equation for the Etna composition. **c** Same as (**b**) except the experiments shown are for the compositions beyond the grey region of (**a**). **d**, **e** Evaluation of the

accuracy of different models for H_2O solubility, shown as differences between the experimental data and predictions from models. Results from the Lesne et al. [\(2011a](#page-21-5)) power-law equation for Etna are compared with the Iacono-Marziano et al. ([2012\)](#page-21-6) model in (**d**) and the Shishkina et al. [\(2014](#page-21-2)) model in (**e**)

is 0.70 wt% (median: 0.41 wt%), with two notable outliers at 7.43 and 7.30 wt% (Fig. [4d](#page-10-0)). We note that these two outliers are experiments published in 2014 (after the Iacono-Marziano et al. [2012](#page-21-6) model), and the maximum diference between this model and measured $H₂O$ for all other experiments in this compilation is 3.30 wt%. For the Shishkina et al. [\(2014\)](#page-21-2) model

(Fig. [4e](#page-10-0)), the average and median diferences between the experiments and this model are identical to those for the Lesne et al. [\(2011a](#page-21-5)) Etna ft, with a slightly higher maximum diference of 1.85 wt%. However, due to the polynomial formulation of the empirical Shishkina et al. ([2014\)](#page-21-2) model, it yields non-zero values for H_2O solubility at 0 MPa that depend solely on $Na + K$ cation fraction. For the compositions in Fig. [4](#page-10-0), the Shishkina et al. (2014) (2014) model calculates concentrations of $H₂O$ at 0 MPa ranging from 0.97 to 1.08 wt%. Previous experimental work suggests that H_2O solubility in mafic magmas (i.e., tholeiite) near 0 MPa is much lower than 1 wt% (-0.1 wt\% at) 1 atm; Baker and Grove [1985\)](#page-20-17).

It is apparent that models relating H_2O solubility in mafic magmas to compositional components generally show more disagreement with the experimental data than calculations using a single empirical ft (Fig. [4d](#page-10-0), e). Our data compilation shows an uneven distribution of experiments by pressure (more experiments at lower pressures) as well as diferences in the number of experiments available for each composition. For these reasons, we do not calibrate a new empirical equation from the data compilation and instead use the Lesne et al. [\(2011a](#page-21-5)) power-law fit for Etna (Eq. [8](#page-5-1)) to calculate H_2O solubility in mafic magmas. The calculators available in the supplementary material use Eq. 8 for the H₂O model (in conjunction with the thermodynamic $CO₂$ model) for all mixed-fluid determinations.

To use Eq. 8 for H₂O solubility in conjunction with the general thermodynamic model for $CO₂$ solubility to determine volatile solubilities for mixed-fluid $(H₂O-CO₂)$ magmas, we determine partial pressures of H_2O and CO_2 using the equation of state and fuid composition of the system. To determine the fugacity of H_2O in a mixed-fluid magma, we calculate the pure H₂O fugacity at the total pressure of the system and then multiply the pure fugacity by the fluid composition $\left(X_{H_2O}^f\right)$) . The partial pressure of H_2O can then be determined from this value of $H₂O$ fugacity using the equation of state (modified Redlich–Kwong with high pressure correction). For example, a magma at 500 MPa and 1200 °C with a pure fuid composition (i.e., 100% H₂O or CO₂) would have a pure H₂O fugacity of 607 MPa $\left(X_{\text{H}_2\text{O}}^f = 1\right)$ or a pure CO₂ fugacity of 1610 MPa $(X_{H_2O}^f = 0)$. At these same *P-T* conditions, a mixed-fluid experiment with fluid composition of 0.2 $X_{\text{H}_2\text{O}}^f$ will have H_2O fugacity of 121 MPa, which corresponds to a partial pressure of 122 MPa for H_2O . The CO_2 fugacity for this fluid composition is 1288 MPa, corresponding to a partial pressure of 451 MPa for $CO₂$.

Testing the MafiCH model for H₂O–CO₂ solubility **in mafc magmas**

A robust general model should be capable of predicting solubility relationships for a variety of mafc compositions for which volatile solubility has not been experimentally determined. To test the validity of the MafiCH model for unstudied compositions, we compare the model calculations with recent experimental data at 1200–1250 °C between 50 and 500 MPa from Fanara et al. ([2015\)](#page-20-9) and Schanofski et al. ([2019\)](#page-21-15). The magma compositions are a "trachybasalt" with 49 wt% SiO₂ and 4.4 wt% Na₂O + K₂O from Fanara et al. ([2015](#page-20-9)) and from Schanofski et al. ([2019](#page-21-15)), a leucitite with 44.5 wt% SiO₂ and 12 wt% Na₂O + K₂O and phonolite with 56 wt% $SiO₂$ and 15.4 wt% Na₂O + K₂O. Note that Fanara et al. ([2015\)](#page-20-9) refer to this composition as "trachybasalt" because it was synthesized to reproduce a natural trachybasalt from the Campanian Ignimbrite, but the starting glass composition is alkali basalt. The "trachybasalt" magma from Fanara et al. ([2015](#page-20-9)) is within the calibrated compositional range of the MafCH model (Fig. [5\)](#page-11-0). The leucitite magma from Schanofski et al. [\(2019\)](#page-21-15) has higher *K* content than the calibration compositions but is otherwise within the calibrated range. The phonolite composition from Schanofski et al. ([2019\)](#page-21-15) is beyond the calibrated compositional range of the CO_2 model (Fig. [5](#page-11-0)) for all elements except Ti and Na. We

Fig. 5 Compositions from Fanara et al. [\(2015](#page-20-9)) and Schanofski et al. ([2019\)](#page-21-15) compared with the compositional range of experiments used to calibrate H_2O and CO_2 models. Cation fractions are plotted relative to the Etna composition from Allison et al. [\(2019](#page-20-3))

don't specifcally intend for MafCH to be used to constrain volatile solubility in polymerized melts such as a phonolite, but we test this composition to examine the performance of the model when extrapolated beyond its calibrated range. Results from the comparison between the MafCH model and experiments from these three compositions are shown in Fig. [6.](#page-13-0)

Of note, both Fanara et al. ([2015](#page-20-9)) and Schanofski et al. ([2019](#page-21-15)) determine fuid compositions using the mass-loss method, though neither study provided error estimates for the $X_{\text{H}_2\text{O}}^f$ values. In the mass-loss method, the experiment capsule is frst weighed, and then frozen in liquid nitrogen prior to and during puncture. The capsule is next allowed to warm to room temperature to release the $CO₂$ fluid and reweighed. Finally, the capsule is stored in a drying oven to release the $H₂O$ fluid and weighed again. There are a few sources of uncertainty involved in mass-loss fuid determinations that were mentioned in these studies, including balance error, incomplete fuid separation, and mixed-fuid bubbles bursting during oven heating. These sources of uncertainty are discussed in further detail in the supplementary material and Figs. S1, S2. Overall, larger uncertainties in $X_{\text{H}_2\text{O}}^f$ are expected for experiments that include small masses (<1 mg) of one or both fluids. Additionally, uncertainty in $X_{H_2O}^f$ propagates to greater uncertainty in fugacity at higher pressure. So, while we do not show error bars for fugacities in Fig. [6,](#page-13-0) we note that based on the calculations shown in the supplementary material, uncertainty in fuid composition can produce fugacity errors of hundreds of MPa, particularly at high fugacities.

The MafCH model shows strong agreement with the experimental data from the "trachybasalt" composition from Fanara et al. ([2015\)](#page-20-9) (Fig. [6a](#page-13-0), b). The vast majority of these experiments defne trends that align closely with both the $CO₂$ and H₂O models. The experiment with the highest $CO₂$ fugacity appears to notably deviate from the $CO₂$ model, but this discrepancy could perhaps be partly explained by errors in the fluid measurement $\left(X_{\mathrm{H}_2\mathrm{O}}^f\right)$) . This particular experiment contained ~ 10 mg of CO_2 in the fluid and only 1 mg of H₂O.

The MafCH model shows excellent agreement with the experimental data from the leucitite composition (Fig. [6](#page-13-0)c, d). The $CO₂$ model in particular is remarkably well suited to this experimental data. All but two experiments are within 500 ppm $CO₂$ of the model calculations, and most overlap with the model when analytical error is accounted for. The $H₂O$ data is generally offset to slightly higher $H₂O$ (average: 0.34 wt%) compared with the model, but many experiments, especially those with $<$ 5 wt% H₂O, do agree with the model within error.

The phonolite experiments illustrate the performance of the $CO₂$ model in MafiCH beyond its calibrated range as well as its limitations. Roughly one third of the experiments

for the more evolved phonolite composition show strong agreement with the $CO₂$ model, but the others diverge to lower $CO₂$ contents than predicted by the model (Fig. [6e](#page-13-0)). The experiments that follow the modeled solubilities all exhibit fluid compositions of $X_{\text{H}_2\text{O}}^f$ > 0.4. At drier compositions, however, the model and experiments deviate signifcantly (up to 1100 ppm diference), with the experiments showing lower $CO₂$ solubility than what is calculated by the model. Schanofski et al. ([2019](#page-21-15)) discuss this diference in $CO₂$ solubility at dry vs. wet conditions, and attribute it to the effect of H_2O on the polymerization of the melt. At high H_2O contents and $X_{H_2O}^f$, H_2O breaks up tetrahedra in the melt structure, and thus more $CO₂$ can be incorporated into the melt structure (e.g., Mysen [1976](#page-21-30)). These results suggest that the $CO₂$ model works well for relatively depolymerized melts (i.e., mafc magmas and hydrous intermediate magmas with $CO₂$ stored as $CO₃$), but does not accurately constrain solubility for polymerized melts beyond its calibrated range.

For H_2O , the phonolite experiments generally follow the MafCH model, with some variability (Fig. [6](#page-13-0)f). Note that some of the phonolite experiments were determined by Schanofski et al. ([2019](#page-21-15)) to have large errors in their fuid compositions as a result of mixed-fuid bubbles bursting during oven drying, and these experiments are marked with an x in Fig. [6e](#page-13-0), f. Excluding the experiments with large fuid composition errors, the average difference between the H_2O model and phonolite experiments is 0.34 wt%, identical to that of the leucitite experiments. In the phonolite experiments, however, the deviation from the model difers based on the amount of H_2O in the experiments. At low H_2O contents ($<$ 3 wt%), the model predicts slightly higher H₂O than the experiments, while at higher H_2O (> 5 wt%) the model predicts slightly lower H_2O . The experiments and H_2O model show strong agreement between 3 and 6 wt%.

Overall, these tests suggest that the MafCH model is accurate within its calibrated range, and in some cases (i.e., depolymerized melts) may apply beyond this compositional range. We recommend comparing the cation fractions of the composition of interest to the calibrated ranges shown in Fig. [5](#page-11-0) to determine whether the MafCH model will be useful for a specifc volcanic system.

Implications

Volcanic plumbing systems: saturation pressures from previously published solubility models

Melt inclusion volatile contents are commonly used to interpret the depth of melt inclusion formation and crystal residence and therefore magma storage and structure of the volcanic plumbing system (e.g., Lowenstern [1995\)](#page-21-7). Volatile

Fig. 6 Comparison between the model presented here (curves) and experiments (symbols) from Fanara et al. [\(2015](#page-20-9)) and Schanofski et al. ([2019\)](#page-21-15). Colors of symbols correspond to the total pressure of the experiment. Fugacities of the experiments were calculated using the equations of state for H_2O and CO_2 used in Allison et al. [\(2019](#page-20-3)). Panels in the left column show $CO₂$ data and panels in the right column show H_2O data. Top row shows the trachybasalt composition from Fanara et al. ([2015\)](#page-20-9); middle row shows the leucitite composition from Schanofski et al. ([2019\)](#page-21-15); bottom row shows the phonolite

composition from Schanofski et al. ([2019\)](#page-21-15). Error bars correspond to the values given in Fanara et al. [\(2015](#page-20-9)) and Schanofski et al. [\(2019](#page-21-15)). No error bars are shown for fugacity as these studies did not provide error estimates for fuid compositions, aside from noting specifc experiments of the Phonolite composition from Schanofski et al. ([2019\)](#page-21-15) with a large error in the determination of $X_{\text{H}_2\text{O}}^f$ (identified here by symbols containing an x). Phonolite experiments with $X_{\text{H}_2\text{O}}^f$ < 0.4 are shown with outlined symbols to indicate experiments with the most polymerized melt structures

solubility models are used to calculate the pressure at which the melt inclusion volatiles are saturated in the magma to provide minimum depth estimates. Diferent solubility models will yield diferent melt inclusion entrapment pressures (e.g., Fig. [1\)](#page-1-0), which will afect interpretation of the volcanic system.

To compare how diferent solubility models afect the interpretation of volcanic data, we determine saturation pressures at 1200 °C for hypothetical melt inclusion volatile compositions. We chose conditions for which the new MafCH model is particularly well calibrated to serve as a reference. In particular, the hypothetical melt inclusion volatile composition is relatively CO_2 -rich to take advantage of the 400–600 MPa experiments from Allison et al. [\(2019\)](#page-20-3) that form the core data set for model calibration. In the supplementary material, we show the results of this same test for two additional melt inclusion volatile compositions (Figs. S3, S4). We focus on only one volatile composition here, as the overall trends in calculated saturation pressures are largely the same for these three diferent melt inclusion volatile compositions.

We show saturation pressures calculated for a melt inclusion with 2.5 wt% H_2O and 4000 ppm CO_2 in Fig. [7.](#page-15-0) The saturation pressures are plotted for each of the 10 calibration compositions for the MafiCH $CO₂$ model according to the wt% total alkali content of the magma for ease of visualization. The major element compositions of these magmas are included in the supplementary material (Table S2). For models that require Fe speciation, we convert from total Fe assuming an oxidation state of $NNO+1$ using Kilinc et al. [\(1983\)](#page-21-16).

First, we discuss the results from the oldest and newest models being tested in comparison to the new MafCH model (Fig. [7a](#page-15-0), b): VolatileCalc (Newman and Lowenstern [2002](#page-21-8)) and MagmaSat (Ghiorso and Gualda [2015](#page-20-5)). VolatileCalc is unable to calculate saturation pressures for three compositions (basalt N72, basaltic andesite SFVF, and phonotephrite AH3) as they have > 49 wt% SiO₂. For the SiO₂ input for VolatileCalc calculations, we use the $SiO₂$ value that results from normalizing to 100% anhydrous after conversion of total Fe to FeO and $Fe₂O₃$. There is a significant misft between VolatileCalc and the new MafCH model for the Vesuvius (~280 MPa) and Stromboli (~ 190 MPa) compositions, and lower, but still notable misft for the leucitite $(-115 MPa)$ and Etna $(-90 MPa)$ compositions. The results from VolatileCalc are largely similar to the new MafCH model for the remaining three compositions (Sunset Crater, Erebus, and the basanite;<30 MPa diference). For the most volatile-rich melt inclusion composition (4.5 wt% H_2O) and 4000 ppm $CO₂$; see supplementary material Fig. S4), increasing divergence between VolatileCalc and the new MafCH model occurs, and noticeable misfts appear for all compositions. The VolatileCalc model is not intended for use at pressures above 500 MPa, and these results illustrate that it is not well calibrated at these high pressures as it calculates saturation pressures that are much higher than what are indicated by the latest experimental data. MagmaSat agrees very closely with the new MafCH model for these three hypothetical melt inclusion compositions for the magmas with > 5.5 wt% alkalis. There is some disagreement, however, between MagmaSat and MafCH for the compositions with lower total alkali contents, particularly the basalt (N72) and basaltic andesite (SFVF) magmas.

Next, we examine the two other comprehensive models (Fig. [7c](#page-15-0), d): Papale et al. ([2006\)](#page-21-9) and Duan ([2014\)](#page-20-4). The Papale et al. ([2006\)](#page-21-9) model calculates very similar saturation pressures for magmas across this entire compositional range, with only \sim 132 MPa difference between the lowest and highest saturation pressures (Fig. [7c](#page-15-0)). The range of saturation pressures predicted by MafCH is nearly 3×wider (371 MPa diference between the lowest and highest pressures) than the Papale et al. ([2006\)](#page-21-9) calculations. The Papale et al. [\(2006](#page-21-9)) model shows strong agreement with the new MafCH model for the Sunset Crater alkali basalt composition and moderate agreement (~50–60 MPa diference) for SFVF, Etna, Stromboli, and Erebus. For the remaining compositions, the Papale et al. [\(2006](#page-21-9)) model shows poor agreement with the MafCH model (>100 MPa diference), with particular misfts for the AH3 phonotephrite $($ \sim 285 MPa difference) and leucitite $(-205 \text{ MPa difference})$. The Duan (2014) (2014) model generally calculates higher saturation pressures for each composition compared with the new MafCH model, though it calculates lower saturation pressures for the Vesuvius composition. The Duan ([2014\)](#page-20-4) model agrees with the new MafCH model for two very diferent compositions: the Stromboli alkali basalt and Erebus phonotephrite. The Duan [\(2014](#page-20-4)) model also shows moderate agreement with the new MafCH model for the Vesuvius composition $(-55 \text{ MPa difference})$, but poor agreement (>100 MPa diference) for the remaining seven compositions. Another interesting note is that both the Duan ([2014\)](#page-20-4) and Papale et al. ([2006\)](#page-21-9) models calculate nearly identical saturation pressures for the Erebus and AH3 compositions, which have similarly high total alkali contents but signifcant compositional diferences in other elements. Experimental data and the new MafCH model show drastically different CO_2 solubilities for the Erebus and AH3 magmas.

Finally, we compare pressures calculated using the two models that are specific to mafic magmas (Fig. [7](#page-15-0)e, f): Iacono-Marziano et al. ([2012](#page-21-6)) and Shishkina et al. ([2014](#page-21-2)). The Shishkina et al. ([2014](#page-21-2)) model consistently calculates higher pressures than the new MafCH model, while the Iacono-Marziano et al. ([2012\)](#page-21-6) model consistently calculates lower pressures. There are noticeable

model (squares) is compared with two previously published models in each row: (top) VolatileCalc (Newman and Lowenstern [2002](#page-21-8)) and MagmaSat (Ghiorso and Gualda [2015\)](#page-20-5); (middle) Duan [\(2014](#page-20-4)) and Papale et al. [\(2006](#page-21-9)); (bottom) Shishkina et al. ([2014\)](#page-21-2) and Iacono-Marziano et al. ([2012\)](#page-21-6). Results are plotted according to total alkali content of the magma compositions

misfts between the Shishkina et al. ([2014](#page-21-2)) model and the new MafCH model, specifcally for the basaltic andesite $(SFVF; ~ 260 MPa$ difference), basalt $(N72; ~ 130 MPa$ diference), as well as the compositions with the highest alkali contents, AH3 (~ 190 MPa diference) and Erebus (~ 160 MPa diference). The Iacono-Marziano et al. ([2012\)](#page-21-6) model shows strong divergence from the new MafCH model for the Erebus (~ 180 MPa diference) composition and moderate disagreement for the basanite (-95 MPa) diference) and Sunset Crater (~ 75 MPa diference) compositions. For the remaining compositions, the pressures from Iacono-Marziano et al. [\(2012\)](#page-21-6) agree with the MafCH model within $<$ 50 MPa.

Overall, VolatileCalc (Newman and Lowenstern [2002](#page-21-8)), Duan ([2014\)](#page-20-4), and Shishkina (2014) tend to calculate higher saturation pressures than the new model, while the Iacono-Marziano et al. ([2012](#page-21-6)) model consistently yields lower saturation pressures. The Papale et al. ([2006\)](#page-21-9) model returns very similar saturation pressures for these 10 mafc compositions of variable alkali contents, suggesting that it is not well suited to distinguish solubility diferences in this compositional range. Saturation pressures in Fig. [7](#page-15-0) calculated using the Iacono-Marziano et al. ([2012](#page-21-6)) and MagmaSat (Ghiorso and Gualda [2015](#page-20-5)) models have the smallest average difference $({\sim}50$ MPa) from the MafiCH model for these 10 compositions. However, we note that we chose to focus on relatively hydrous volatile compositions for this test to avoid bias in saturation pressures as a result of variable isobar shapes at low $H₂O$ contents (see Fig. [1\)](#page-1-0). The Iacono-Marziano et al. ([2012\)](#page-21-6) and MagmaSat (Ghiorso and Gualda [2015](#page-20-5)) models in particular show a strong decrease in $CO₂$ solubility at low $H₂O$ contents, and would therefore show larger deviations from MafCH at relatively anhydrous compositions. The behavior of $CO₂$ solubility at low H_2O is poorly understood at present, so the different trends shown by models at H_2O -poor fluid compositions are relatively unconstrained.

The degree of consensus between models also varies based on the overall magma composition. Pressures calculated for the Sunset Crater alkali basalt show the best agreement for all models; in Fig. [7,](#page-15-0) the average difference between each model and the MafCH model is just ~ 55 MPa for Sunset Crater. The models show significant disagreement (> 100 MPa average difference from MafCH in Fig. [7\)](#page-15-0) for the highest silica composition (SFVF basaltic andesite), as well as the compositions at the extremes of total alkali contents in this range $\left($ < 3 wt $\%$ and >7 wt%). These significant disagreements may indicate that these compositional ranges are at or beyond the calibrated limits of the previous models. Some of these diferences are likely due to the fact that some models attribute most of the compositional dependence of $CO₂$ solubility in mafc magmas to total alkali contents rather than the full multicomponent magma composition. The Erebus magma, for example, is one of the compositions that show a wide range of saturation pressures predicted by the diferent models. Erebus has high total alkali contents, corresponding to high $CO₂$ solubility in some models, but it also has the lowest Ca cation fraction and highest Al cation fraction in our calibration dataset, resulting in lower $CO₂$ solubility in other models.

One fnal interesting observation from Fig. [7](#page-15-0) is the relative solubility diferences between the magmas. In the compositions assessed in Fig. [7,](#page-15-0) saturation pressures generally decrease (i.e., volatile solubility increases) with increasing total alkali content, with the exception of magmas with higher silica contents (i.e., the SFVF composition) and very high total alkali contents (> 6 wt%). With the exception of VolatileCalc (Newman and Lowenstern [2002](#page-21-8)) and the Papale et al. [\(2006\)](#page-21-9) model, the newer models generally replicate these same overall trends of volatile solubility with total alkali content. This may suggest that models have now identifed the major elemental impacts on volatile solubility in mafc magmas, even though the models do vary in their overall calibration. If that is the case, future work to refne the models should focus on compositions for which the recent models do not converge (i.e., basaltic andesites and magmas with high total alkali contents).

Relative infuence of compositional components on CO₂ solubility (what affects CO₂ solubility?)

Previous models specific to mafic magmas have correlated solubility relationships with compositional parameters that range from single elements to multicomponent calculations. For example, VolatileCalc (Newman and Lowenstern [2002\)](#page-21-8) uses the $SiO₂$ content (wt%) as a proxy for the compositional parameter *Π* from Dixon ([1997\)](#page-20-2). Iacono-Marziano et al. ([2012](#page-21-6)) and Shishkina et al. ([2014](#page-21-2)) use more complex compositional parameters (NBO/O and *Π**, respectively) to correlate with CO_2 solubility. In Fig. [8](#page-17-0) we compare the calculated $CO₂$ solubility from MafiCH at 500 MPa and 1200 °C for the 10 calibration compositions compared with these compositional parameters.

Figure [8a](#page-17-0) shows essentially no correlation between $CO₂$ solubility and $SiO₂$ content (wt%). This is unsurprising, because the $SiO₂$ parameterization incorporated into VolatileCalc (Newman and Lowenstern [2002](#page-21-8)) was based on suite of samples from a single submarine location and not intended for broad application. The NBO/O parameter used by the Iacono-Marziano et al. ([2012\)](#page-21-6) model also shows very little correlation with $CO₂$ solubility as determined by MafCH (Fig. [8](#page-17-0)b). In fact, three of these compositions have nearly identical values of NBO/O but very diferent CO_2 solubilities (~6000–13,000 ppm CO_2 at 500 MPa and 1200 °C). The *Π** parameter used by Shishkina et al. [\(2014](#page-21-2)) does appear to capture much of the variability in $CO₂$ solubility by these magmas, although the relationship between *Π*^{*} and CO₂ solubility is non-linear (Fig. [8](#page-17-0)c). Recent work by Mangan et al. ([2021](#page-21-31)) suggested that CO_2 solubility may

Fig. 8 Comparison of CO_2 solubility at 500 MPa and 1200 °C calculated by the MafCH model with compositional parameters from other works. $CO₂$ solubilities are calculated for the 10 calibration compositions in the CO₂ model of MafiCH. The parameters are: **a**

be related to the agpaitic index of a magma, defned as $(Ca^{+2} + Na^{+1} + K^{+1})/Al^{+3}$. The MafiCH model supports this conclusion, showing a strong positive correlation between $CO₂$ solubility and agpaitic index (Fig. [8d](#page-17-0)). The agpaitic index correlation helps to explain why two compositions with similar total alkali contents (i.e., Erebus and AH3) can have very different $CO₂$ solubilities.

Because the $CO₂$ model in MafiCH does provide accurate solubility relationships for a variety of mafic compositions (e.g., Fig. [6](#page-13-0)a and c), we make an assumption that it can be used to test how small changes in composition impact $CO₂$ solubility, especially when interpolating between calibrated compositions. While this is a signifcant assumption, this exercise may provide useful insights about the mechanism of $CO₂$ dissolution in mafic magmas and changes in volatile solubility during magma evolution or for closely associated magmas, as well as identify priorities for future experimental investigations.

To investigate the infuence of compositional components on $CO₂$ solubility, we determine the expected change SiO₂ content in wt% from VolatileCalc (Newman and Lowenstern [2002](#page-21-8)), **b** NBO/O from Iacono-Marziano et al. ([2012\)](#page-21-6), **c** *Π** from Shishkina et al. ([2014\)](#page-21-2), and **d** agpaitic index $(Ca^{+2} + Na^{+1} + K^1)/Al^{+3}$ as described in Mangan et al. [\(2021](#page-21-31))

in solubility when the abundance of one cation component is varied (Figs. [9](#page-18-0), [10\)](#page-19-0). We first calculate the CO_2 solubility at 500 MPa and 1200 °C for a specifc composition, represented by the asterisk. We then change just one cation component of this composition in 0.005 increments and renormalize all cations at each step. Then, using the MafCH model, we recalculate $\ln K_0$ and $\Delta V_r^{0,m}$ and determine the new $CO₂$ solubility as a result of this change in composition. Note that symbols in grey in Figs. [9](#page-18-0), [10](#page-19-0) indicate that the calculated cation fraction is beyond the calibrated range of the model.

Figure [9](#page-18-0) depicts the infuence of sodium, potassium, calcium, and silicon content on $CO₂$ solubility according to the MafCH model. We show the results of these tests for the Sunset Crater (Fig. [9](#page-18-0)a), Erebus (Fig. [9b](#page-18-0)), and Stromboli (Fig. [9c](#page-18-0)) magmas because they exhibit nearly identical $CO₂$ solubilities despite their variable chemical compositions. We also examine the Etna composition (Fig. [9](#page-18-0)d) as it is fairly similar in composition to the Sunset Crater magma yet has a higher $CO₂$ solubility. The remaining compositions used

Fig. 9 Predicted influence of Na⁺¹, K⁺¹, Ca⁺², and Si⁺⁴ on CO₂ solubility according to the MafiCH model. $CO₂$ solubility (dissolved CO₂ content) calculated by the model at 500 MPa and 1200 °C for the **a** Sunset Crater, **b** Erebus, **c** Stromboli, and **d** Etna compositions is shown by the asterisk symbol. Additional symbols show how calculated solubility (at 500 MPa and 1200 °C) changes as one compo-

to calibrate the $CO₂$ model display similar overall trends to those in Fig. [9](#page-18-0). According to this test, Si^{+4} , which is the sole compositional input (as $SiO₂$) in the VolatileCalc model (Newman and Lowenstern [2002\)](#page-21-8), has essentially no impact on $CO₂$ solubility in this compositional range. This is an interesting, but perhaps expected result as $SiO₂$ content was only used as a proxy for the compositional parameter Π from Dixon ([1997\)](#page-20-2) for a specific set of samples. This $SiO₂$ proxy was not intended to be broadly applied to a wide range of mafic magmas.

The effect of potassium on $CO₂$ solubility according to the MafiCH model is variable and non-linear. Its effect on $CO₂$ solubility is low in the Sunset Crater composition (Fig. [9a](#page-18-0)), slightly stronger for Stromboli (Fig. [9c](#page-18-0)) and Etna (Fig. [9](#page-18-0)d), and it has a very strong efect in the Erebus magma, nearly equal to the efect to calcium and sodium (Fig. [9](#page-18-0)b). However, the impact of potassium on $CO₂$ solubility appears to be much lower at low K^{+1} contents. For example, in the

nent is varied (single cation fraction in 5% intervals). At each step the modifed composition is re-normalized to determine new values of ln K_0 and $\Delta V_r^{0,m}$. Symbols in grey indicate that the calculated cation fraction is beyond the calibrated range of the model. Diagonal lines are drawn to aid in comparisons between panels

Stromboli composition (0.023 initial K^{+1} ; Fig. [9c](#page-18-0)), the addition of potassium has a positive effect on $CO₂$ solubility, but there is essentially no change in solubility if potassium is subtracted. In the Erebus magma (0.033 initial K^{+1} ; Fig. [9b](#page-18-0)), however, CO_2 solubility does show a notable decrease as potassium content is decreased.

Calcium and sodium exhibit the strongest positive efects on $CO₂$ solubility based on the results shown in Fig. [9](#page-18-0), but the effects vary across these four compositions. The magnitude of the solubility increase due to increased calcium or sodium is smaller for Sunset Crater (Fig. [9a](#page-18-0)) and Erebus (Fig. [9](#page-18-0)b) compared to Stromboli (Fig. [9c](#page-18-0)) and Etna (Fig. [9d](#page-18-0)). Furthermore, in the Sunset Crater and Erebus compositions, addition of calcium has a slightly stronger efect on $CO₂$ solubility than the addition of sodium, whereas for the Stromboli composition (Fig. [9](#page-18-0)c), addition of sodium has the larger effect. In the Etna composition (Fig. [9](#page-18-0)d), addition of

Fig. 10 Predicted influence of Ti^{+4} , Al^{+3} , Fe*, and Mg^{+2} on CO_2 solubility according to the MafiCH model. CO₂ solubility (dissolved $CO₂$ content) calculated by the model at 500 MPa and 1200 °C for the Stromboli composition is shown by the asterisk symbol. Additional symbols show how calculated solubility (at 500 MPa and 1200 °C) changes as one component is varied (single cation fraction in 5% intervals). At each step the modifed composition is re-normalized to determine new values of $\ln K_0$ and $\Delta V_r^{0,m}$. Symbols in grey indicate that the calculated cation fraction is beyond the calibrated range of the model. Diagonal lines are included for visual reference and easy comparison to Fig. [9](#page-18-0)

sodium has a nearly equal impact on $CO₂$ solubility as the addition of calcium.

We also examine the infuence of titanium, aluminum, iron, and magnesium content on $CO₂$ solubility according to the MafCH model in Fig. [10.](#page-19-0) Figure [10](#page-19-0) was constructed following the same method that was used for Fig. [9.](#page-18-0) For these elements, the overall trends are the same for all 10 magma compositions used to calibrate the $CO₂$ model, and so we focus only on the results for the Stromboli composition. Aluminum has a very strong negative effect on solubility, nearly as strong as the positive efect of calcium and sodium. This is likely because in order for Al^{+3} to form a tetrahedron with oxygen, it requires an additional cation, like K^{+1} or Na⁺¹ to charge balance the tetrahedron. So not only does aluminum serve to polymerize the melt by forming a tetrahedron, but it also prevents one of these alkali cations from bonding with carbonate, leading to a very strong effect on $CO₂$ solubility. The remaining elements in Fig. [10](#page-19-0) appear to have very little effect on $CO₂$ solubility in these compositions. Overall, this analysis (Fig. [9,](#page-18-0) [10\)](#page-19-0) illustrates the complexity of $CO₂$ solubility. The infuence of each individual component appears to depend upon the abundance of other components. Also, this result demonstrates that it is necessary to use the full multi-component melt composition to build well-calibrated solubility models.

Conclusions

We developed a general thermodynamic model for $CO₂$ solubility in mafc magmas across a wide range of total alkali contents. We combine this new thermodynamic model with an empirical model for H_2O solubility from Lesne et al. $(2011a)$ $(2011a)$ to yield a general model for H_2O –CO₂ solubility in mafc magmas called MafCH.

- 1. The $CO₂$ model was calibrated using recent experiments on six compositions from Allison et al. ([2019\)](#page-20-3) as well as four additional compositions from the literature. Using multiple linear regression analysis, we have derived two empirical compositional relationships (Eqs. [6–](#page-7-1)[7](#page-8-1)) that describe the thermodynamic parameters $\Delta V_r^{0,m}$ (partial molar volume change) and $\ln K_0$ (equilibrium constant at reference conditions).
- 2. The MafiCH model is calibrated for compositions with 44 to 53 wt% $SiO₂$ and 2 to 9 wt% total alkalis $(Na₂O + K₂O)$, at pressures between ~50 and 700 MPa. A comparison with experimental data from magmas both within and beyond this compositional space suggests that MafCH is very accurate within its calibrated range (i.e., mafic magmas with cation fractions within the ranges shown in Fig. [5\)](#page-11-0). In some cases, MafCH can be used beyond the calibrated compositional range, as long as the melt is a relatively depolymerized composition with $CO₂$ stored as $CO₃$.
- 3. One of the primary benefts of the MafCH model is that it accurately describes $CO₂$ solubility behavior in mafic magmas at a range of crustal pressures. The $CO₂$ model is particularly robust because it is based in thermodynamics, calibrated across a wide *P*–*X* range of mafc magmas, and employs the full multicomponent magma composition to determine $CO₂$ solubility relationships.
- 4. The new MafCH model yields melt inclusion saturation pressures that are typically lower than the pressures predicted by previously published volatile solubility models relevant to mafc magmas. The previously published models show the most divergence from MafCH in less constrained compositional regions such as in magmas with higher $SiO₂$ contents (i.e., basaltic andesites), as well as magmas with relatively high $(>7 \text{ wt\%})$ and low $(< 3 \text{ wt\%})$ total alkali contents. Many of the more recent models show similar trends in volatile solubility by magma composition, suggesting that models are beginning to agree on the elemental controls on volatile solubility.
- 5. Previously published volatile solubility models have developed compositional indices such as $SiO₂$, Π (or *Π**) and NBO/O to describe solubility within restricted compositional regions. $CO₂$ solubility determined

using the MafCH model does not directly correlate with any of these indices. However, the agpaitic index, $(Ca^{+2} + Na^{+1} + K^1)/Al^{+3}$, does generally scale with CO_2 solubility calculated by the MafCH model across a wide compositional range of mafc magmas. Additional analysis suggests that the infuence of individual compositional components will be required to further improve volatile solubility models.

- 6. Based on calculations using the MafiCH model, $Na⁺¹$ and Ca^{+2} appear to have the strongest positive effect on $CO₂$ solubility and $Al⁺³$ has a nearly equal negative effect. K^{+1} also has a strong positive effect. Other elements (e.g., Si^{+4} , Mg^{+2}) individually have little effect on $CO₂$ solubility in this compositional range.
- 7. The absolute solubility infuence of each element varies depending on the abundance of other elements. This assessment suggests that the full multi-component magma composition is necessary to constrain $CO₂$ solubility for mafic magmas. It also suggests that additional experiments are required to constrain compositional regions that extend beyond the calibrated range of the MafiCH model.

Supplementary Information The online version contains supplementary material available at <https://doi.org/10.1007/s00410-022-01903-y>.

Acknowledgements This work was supported by NSF grants EAR-1322078 and EAR-1642569 to ABC and KR. Thanks to Mattia de' Michieli Vitturi for discussions regarding model calculators and James Thompson for help with Python. We are grateful to Kayla Iacovino and an anonymous reviewer for thoughtful comments that improved this manuscript, as well as Mark Ghiorso for editorial handling.

Author contributions All the authors conceptualized the project, interpreted the results, and edited the paper. CMA calibrated and tested the model, generated the excel calculator and python scripts, performed all calculations for the previously published models, and wrote the original draft of the paper.

Funding This work was supported by NSF grants EAR-1322078 and EAR-1642569 to ABC and KR.

Availability of data and materials No new data were collected for this study.

Code availability An excel spreadsheet and two python scripts are available in the supplementary material to perform calculations with the MafiCH model.

Declarations

Conflict of interest Not applicable.

References

- Allison CM, Roggensack K, Clarke AB (2019) H_2O –CO₂ solubility in alkali-rich mafc magmas: new experiments at mid-crustal pressures. Contrib Mineral Petrol 174:58. [https://doi.org/10.1007/](https://doi.org/10.1007/s00410-019-1592-4) [s00410-019-1592-4](https://doi.org/10.1007/s00410-019-1592-4)
- Baker MB, Grove TL (1985) Kinetic controls on pyroxene nucleation and metastable liquid lines of descent in a basaltic andesite. Am Mineral 70:279-287
- Behrens H, Misiti V, Freda C, Vetere F, Botcharnikov RE, Scarlato P (2009) Solubility of H_2O and CO_2 in ultrapotassic melts at 1200 and 1250 degrees C and pressure from 50 to 500 MPa. Am Mineral 94:105–120.<https://doi.org/10.2138/am.2009.2796>
- Berndt J, Liebske C, Holtz F, Freise M, Nowak M, Ziegenbein D, Hurkuck W, Koepke J (2002) A combined rapid-quench and H_2 -membrane setup for internally heated pressure vessels: description and application for water solubility in basaltic melts. Am Mineral 87:1717–1726
- Blank JG, Brooker RA (1994) Experimental studies of carbon dioxide in silicate melts: solubility, speciation, and stable carbon isotope behavior. In: Carroll MR, Holloway JR (eds) Volatiles in magmas, vol 30. Mineralogical Society of America, Washington, pp 157–186
- Botcharnikov R, Freise M, Francois H, Behrens H (2005) Solubility of C-O-H mixtures in natural melts: new experimental data and application range of recent models. Annals of Geophys 48:633–646
- Brooker RA, Kohn SC, Holloway JR, McMillan PF (2001) Structural controls on the solubility of $CO₂$ in silicate melts part I: bulk solubility data. Chem Geol 174:225–239
- Cocheo PA (1994) The solubility of water in basanitic melts at low pressures, MS thesis. Arizona State University
- Di Matteo V, Mangiacapra A, Dingwell DB, Orsi G (2006) Water solubility and speciation in shoshonitic and latitic melt composition from Campi Flegrei Caldera (Italy). Chem Geol 229:113–124. <https://doi.org/10.1016/j.chemgeo.2006.01.015>

Dixon JE (1997) Degassing of alkalic basalts. Am Mineral 82:368–378

- Dixon JE, Stolper EM, Holloway JR (1995) An experimental study of water and carbon dioxide solubilities in mid ocean ridge basaltic liquids. Part I: calibration and solubility models. J Petrol 36(6):1607–1631
- Duan X (2014) A general model for predicting the solubility behavior of H_2O – CO_2 fluids in silicate melts over a wide range of pressure, temperature and compositions. Geochim Cosmochim Acta 125:582–609. <https://doi.org/10.1016/j.gca.2013.10.018>
- Duan Z, Zhang Z (2006) Equation of state of the H₂O, CO₂, and H₂O– $CO₂$ systems up to 10 GPa and 2573.15 K: molecular dynamics simulations with ab initio potential surface. Geochim Cosmochim Acta 70:2311–2324.<https://doi.org/10.1016/j.gca.2006.02.009>
- Eguchi J, Dasgupta R (2018) A $CO₂$ solubility model for silicate melts from fuid saturation to graphite or diamond saturation. Chem Geol 487:23–38. <https://doi.org/10.1016/j.chemgeo.2018.04.012>
- Fanara S, Botcharnikov RE, Palladino DM, Adams F, Buddensieck J, Mulch A, Behrens H (2015) Volatiles in magmas related to the Campanian Ignimbrite eruption: Experiments vs. natural fndings. Am Mineral 100(10):2284–2297. [https://doi.org/10.2138/](https://doi.org/10.2138/am-2015-5033) [am-2015-5033](https://doi.org/10.2138/am-2015-5033)
- Fine G, Stolper E (1986) Dissolved carbon dioxide in basaltic glasses: concentration and speciation. Earth Planet Sci Lett 76:263–278
- Ghiorso MS, Gualda GAR (2015) An H_2O –CO₂ mixed fluid saturation model compatible with rhyolite-MELTS. Contrib Mineral Petrol 169:53.<https://doi.org/10.1007/s00410-015-1141-8>
- Holloway JR (1977) Fugacity and activity of molecular species in supercritical fuids. In: Fraser DG (ed) Thermodynamics in geology. Reidel, Dordrect, pp 161–181
- Holloway JR (1981) Volatile interactions in magmas. In: Newton RC, Navrotsky A, Wood BJ (eds) Thermodynamics of minerals and melts. Springer-Verlag, New York, pp 273–293
- Holloway JR (1987) Igneous fluids. Rev Mineral Geochem 17(1):211–232
- Holloway JR, Blank JG (1994) Application of experimental results to C-O-H species in natural melts. In: Carroll MR, Holloway JR (eds) Volatiles in magmas, vol 30. Mineralogical Society of America, Washington, pp 187–230
- Iacono-Marziano G, Morizet Y, Le Trong E, Gaillard F (2012) New experimental data and semi-empirical parameterization of H_2O – CO₂ solubility in mafic melts. Geochim Cosmochim Acta 97:1-23. <https://doi.org/10.1016/j.gca.2012.08.035>
- Iacovino K, Moore G, Roggensack K, Oppenheimer C, Kyle P (2013) $H₂O-CO₂$ solubility in mafic alkaline magma: applications to volatile sources and degassing behavior at Erebus volcano, Antarctica. Contrib Mineral Petrol 166:845–860. [https://doi.org/10.](https://doi.org/10.1007/s00410-013-0877-2) [1007/s00410-013-0877-2](https://doi.org/10.1007/s00410-013-0877-2)
- Iacovino K, Oppenheimer C, Scaillet B, Kyle P (2016) Storage and evolution of mafc and intermediate alkaline magmas beneath Ross Island. Antarctica J Petrol 57(1):93–118. [https://doi.org/10.](https://doi.org/10.1093/petrology/egv083) [1093/petrology/egv083](https://doi.org/10.1093/petrology/egv083)
- Iacovino K, Matthews S, Wieser PE, Moore GM, Bégué F (2021) VESIcal Part I: an open-source thermodynamic model engine for mixed volatile (H_2O-CO_2) solubility in silicate melts. Earth Space Sci 8(11):e2020EA001584. [https://doi.org/10.1029/2020E](https://doi.org/10.1029/2020EA001584) [A001584](https://doi.org/10.1029/2020EA001584)
- Kilinc A, Carmichael ISE, Rivers ML, Sack RO (1983) The ferricferrous ratio of natural silicate liquids equilibrated in air. Contrib Mineral Petrol 83:136–140
- Lesne P, Scaillet B, Pichavant M, Iacono-Marziano G, Beny JM (2011a) The H_2O solubility of alkali basalts: an experimental study. Contrib Mineral Petrol 162(1):133–151. [https://doi.org/](https://doi.org/10.1007/s00410-010-0588-x) [10.1007/s00410-010-0588-x](https://doi.org/10.1007/s00410-010-0588-x)
- Lesne P, Scaillet B, Pichavant M, Beny JM (2011b) The carbon dioxide solubility in alkali basalts: an experimental study. Contrib Mineral Petrol 162(1):153–168. [https://doi.org/10.1007/](https://doi.org/10.1007/s00410-010-0585-0) [s00410-010-0585-0](https://doi.org/10.1007/s00410-010-0585-0)
- Lowenstern JB (1995) Applications of silicate-melt inclusions to the study of magmatic volatiles. In: Thompson JFH (ed) Magmas, fuids and ore deposition. Mineralogical Association of Canada, Short Course 23, Quebec, pp 71–99
- Mangan MT, Sisson TW, Hankins WB, Shimizu N, Vennemann T (2021) Constraints on deep, $CO₂$ -rich degassing at arc volcanoes from solubility experiments on hydrous basaltic andesite of Pavlof Volcano, Alaska Peninsula, at 300 to 1200 MPa. Am Miner. <https://doi.org/10.2138/am-2021-7531>
- Moore G, Vennemann T, Carmichael ISE (1995) Solubility of water in magmas to 2 kbar. Geology 23:1099–1102
- Moore G, Vennemann T, Carmichael ISE (1998) An empirical model for the solubility of H_2O in magmas to 3 kilobars. Am Mineral 83:36–42
- Mysen BO (1976) The role of volatiles in silicate melts: solubility of carbon dioxide and water in feldspar, pyroxene, and feldspathoid melts to 30 kb and 1625 °C. Am J Sci 276:969–996
- Newman S, Lowenstern JB (2002) VOLATILECALC: a silicate melt-H₂O-CO₂ solution model written in Visual Basic for excel. Comput Geosci 28(5):597–604. [https://doi.org/10.1016/S0098-](https://doi.org/10.1016/S0098-3004(01)00081-4) [3004\(01\)00081-4](https://doi.org/10.1016/S0098-3004(01)00081-4)
- Ohlhorst S, Behrens H, Holtz F (2001) Compositional dependence of molar absorptivities of near-infrared OH- and H_2O bands in rhyolitic to basaltic glasses. Chem Geol 174:5–20
- Papale P (1997) Thermodynamic modeling of the solubility of H_2O and CO₂ in silicate liquids. Contrib Mineral Petrol 126:237-251
- Papale P, Polacci M (1999) Role of carbon dioxide in the dynamics of magma ascent in explosive eruptions. Bull Volcanol 60:583–594
- Papale P, Moretti R, Barbato D (2006) The compositional dependence of the saturation surface of H_2O+CO_2 fluids in silicate melts. Chem Geol 229:78–95. [https://doi.org/10.1016/j.chemgeo.2006.](https://doi.org/10.1016/j.chemgeo.2006.01.013) [01.013](https://doi.org/10.1016/j.chemgeo.2006.01.013)
- Pichavant M, Di Carlo I, Le Gac Y, Rotolo SG, Scaillet B (2009) Experimental constraints on the deep magma feeding system at Stromboli volcano. Italy J Petrol 50(4):601–624. [https://doi.org/](https://doi.org/10.1093/petrology/egp014) [10.1093/petrology/egp014](https://doi.org/10.1093/petrology/egp014)
- Pichavant M, Scaillet B, Pommier A, Iacono-Marziano G, Cioni R (2014) Nature and evolution of primitive Vesuvius magmas: an experimental study. J Petrol 55(11):2281–2310. [https://doi.org/](https://doi.org/10.1093/petrology/egu057) [10.1093/petrology/egu057](https://doi.org/10.1093/petrology/egu057)
- Schanofski M, Fanara S, Schmidt BC (2019) $CO₂–H₂O$ solubility in K-rich phonolitic and leucititic melts. Contrib Mineral Petrol 174:52.<https://doi.org/10.1007/s00410-019-1581-7>
- Saxena SK, Fei Y (1987) High pressure and high temperature fuid fugacities. Geochim Cosmochim Acta 51:783–791
- Shishkina TA, Botcharnikov RE, Holtz F, Almeev RR, Portnyagin MV (2010) Solubility of H₂O- and CO₂-bearing fluids in tholeiitic basalts at pressures up to 500 MPa. Chem Geol 277:115–125. <https://doi.org/10.1016/j.chemgeo.2010.07.014>
- Shishkina TA, Botcharnikov RE, Holtz F, Almeev RR, Jazwa AM, Jakubiak AA (2014) Compositional and pressure efects on the solubility of H_2O and CO_2 in mafic melts. Chem Geol 388:112– 129.<https://doi.org/10.1016/j.chemgeo.2014.09.001>
- Stolper E, Holloway JR (1988) Experimental determination of the solubility of carbon dioxide in molten basalt at low pressure. Earth Planet Sci Lett 87:397–408
- Thibault Y, Holloway JR (1994) Solubility of $CO₂$ in a Ca-rich leucitite: effects of pressure, temperature, and oxygen fugacity. Contrib Mineral Petrol 116:216–224
- Vetere F, Botcharnikov RE, Holtz F, Behrens H, De Rosa R (2011) Solubility of H_2O and CO_2 in shoshonitic melts at 1250 °C and pressures from 50 to 400 MPa: implications for Campi Flegrei magmatic systems. J Volcanol Geotherm Res 202:251–261. <https://doi.org/10.1016/j.jvolgeores.2011.03.002>
- Vetere F, Holtz F, Behrens H, Botcharnikov RE, Fanara S (2014) The effect of alkalis and polymerization on the solubility of H_2O and CO₂ in alkali-rich silicate melts. Contrib Mineral Petrol 167:1014. <https://doi.org/10.1007/s00410-014-1014-6>
- Wieser PE, Iacovino K, Matthews S, Moore G, Allison CM (2022) A critical approach to volatile solubility modeling using the opensource engine VESIcal. Earth Space Sci. [https://doi.org/10.1029/](https://doi.org/10.1029/2021EA001932) [2021EA001932](https://doi.org/10.1029/2021EA001932)
- Witham F, Blundy J, Kohn SC, Lesne P, Dixon J, Churakov SV, Botcharnikov R (2012) SolEx: a model for mixed COHSCl-volatile solubilities and exsolved gas compositions in basalt. Comput Geosci 45:87–97. <https://doi.org/10.1016/j.cageo.2011.09.021>

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