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## **A Novel Cu(II) Ion‑Imprinted Alginate–Chitosan Complex Adsorbent for Selective Separation of Cu(II) from Aqueous Solution**

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## **Abstract**

A novel Cu(II) ion-imprinted complex adsorbent [Cu(II)-IIP] from alginate and chitosan was prepared by a three-step process of beading–combining–crosslinking with  $Cu^{2+}$  as the template ion. The Cu(II)-IIP showed higher capacity and selectivity for Cu(II) than the non-imprinted polymer. The theoretical maximum adsorption capacity of Cu(II)-IIP reached 83.33 mg/g, and the separation factor  $(\alpha)$  for Cu(II) versus  $Zn(II)$  was 2.28. The adsorption of  $Cu^{2+}$  onto the Cu(II)-IIP was perfectly described by the Langmuir isotherm model. The adsorption kinetics agreed with the pseudofrst-order model in the frst 8 h and more ftted pseudo-second-order model after then. Weber–Morris model confrmed that the adsorption rate would be controlled dominantly by the intraparticle difusion and the inner surface binding. Moreover, the Cu(II)-IIP complex adsorbent exhibited good regeneration, and the adsorption capacity was stable within the frst three adsorption–desorption cycles without signifcant reduction.

**Keywords** Chitosan · Alginate · Complex · Ion imprinting ·  $Cu(II)$  ion · Adsorption

## **Introduction**

Heavy metal ions in the aqueous environment remains a major issue because of their high toxicity, persistence and susceptible carcinogenic effect [[1–](#page-14-0)[4\]](#page-14-1). Selective recognition of metal ions is a real challenge for a wide range of applications in the analytical feld including extraction, detection and quantifcation. For that purpose, ion-imprinted polymers (IIPs) have been increasingly developed during the past decades [[5,](#page-14-2) [6\]](#page-14-3). Similar to molecularly imprinted polymers (MIPs), IIPs are a class of well-tailored functional materials, in which specifc cavities that match the target ion

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(namely the template ion) in shape, size and functional groups are distributed, rendering high binding affinity and specificity to the target ion  $[7, 8]$  $[7, 8]$  $[7, 8]$  $[7, 8]$  $[7, 8]$ . The crosslinking of linear chain polymers carrying metal-binding groups is a well-developed technique used to prepare IIPs [\[9](#page-15-1), [10](#page-15-2)]. This approach is simpler than polymerization and can avoid the use of an initiator. Moreover, the IIPs possess good chemical stability [\[11](#page-15-3)].

The development of metal ion imprinting technology is of signifcance for the environment, materials, life science and other felds. Nishide [\[12](#page-15-4)] prepared a metal ion-imprinted polymer for the frst time in 1976 and opened a precedent for the study of metal ion imprinting. Su et al.  $[13, 14]$  $[13, 14]$  $[13, 14]$  $[13, 14]$  prepared Ni $(II)$  ion-imprinted polymers by using surface ion imprinting technique with mycelia and chitosan as raw materials and epichlorohydrin as crosslinking agent. The adsorption capacity for  $Ni<sup>2+</sup>$  reached 82.5 mg/g in a suitable condition. An and Gao  $[15, 16]$  $[15, 16]$  $[15, 16]$  $[15, 16]$  grafted polyethylenimine to the surface of silica gel particles and prepared metal ion [Cr(III), Cu(II)]-imprinted polymer IIP-PEI/SiO<sub>2</sub> with epichlorohydrin as crosslinking agent. The adsorption capacity of IIP-PEI/SiO<sub>2</sub> enhanced nearly two times compared to  $PEI/SiO<sub>2</sub>$ , and the selectivity for the template ion was excellent. Araki et al. [[17\]](#page-15-9) applied a surface imprinting technique to prepare a Zn(II) ion-imprinted polymeric membrane, which showed higher adsorption affinity and permeation selectivity towards  $\text{Zn}^{2+}$  than the non-imprinted counterpart.

Natural polymer materials (cellulose, chitin and sodium alginate, etc.) have been widely used in the separation of heavy metals in the water environment. In recent years, natural polymer materials were tried to be combined with the ion imprinting technology to prepare the adsorbent materials with low cost, biodegradability and specifc adsorption for metal ions. Cellulose is a natural polymer with rich sources, non-toxicity and wide application. Lin [[18\]](#page-15-10) grafted acrylic acid onto cellulose and prepared Pb(II) ion-imprinted polymer microspheres by inverse suspension polymerization. The imprinted microspheres showed a high adsorption amount (412 mg/g) and excellent selectivity for  $Pb^{2+}$ .

In this paper, sodium alginate and chitosan, two kinds of natural polymer materials, are employed as matrix to explore a novel complex adsorbent for  $Cu(II)$  ions by using ion imprinting technology, where the electrostatic interaction between the carboxyl groups of sodium alginate and the protonated amino groups of chitosan is fully used to prepare the alginate–chitosan (ALG–CTS) complex adsorbent and improve the adsorption performance comparing with chemical modifcation. Furthermore, the adsorbent has a regular shape and good dispersibility which is better for recycling and reuse. This study is of great signifcance to the treatment of heavy metal pollution in water environment.

#### **Experimental**

#### **Materials**

Sodium alginate (SA) was obtained from Pharmaceutical Group Shanghai Chemical Reagent Company (China). Chitosan (CTS) and

2-[(5-bromo-2-pyridinyl)-azo]-5-diethylamino-phenol were purchased from Sinopharm Chemical Reagent Co., Ltd. (China). Anhydrous calcium chloride and acetic acid were obtained from Shanghai Reagent Plant (China). CuCl<sub>2</sub>·2H<sub>2</sub>O was purchased from Shantou Guanghua Chemical Factory (China). Glutaraldehyde was obtained from Tianjin Fuchen Chemical Reagent Factory (China).  $ZnSO<sub>4</sub>·7H<sub>2</sub>O$ was purchased from Guangdong Guanghua Chemical Factory Co., Ltd. (China). All other reagents were of analytical grade and were used without further purifcation. All solutions were prepared with deionized water.

#### **Preparation of Cu(II)‑IIP Complex Adsorbent**

The spherical Cu(II)-IIP complex adsorbent based on SA and CTS was prepared by a three-step process of beading–combining–crosslinking.

Beading: 0.6 g SA was dissolved in 59.4 g of deionized water to obtain 1% of SA solution. Then, the SA solution was dropped by syringe into 60 mL of mixed solution (1.5% CaCl<sub>2</sub> and 0.5% CuCl<sub>2</sub>) to form alginate (ALG) gel beads. The gel beads were washed with deionized water to remove Cl− on the surface after static incubation for 1 h.

Combining: 0.4 g of CTS and 75 mg of Cu(II) were dissolved in 39.6 g of  $1\%$ acetic acid solution to obtain 1% of CTS solution. The washed ALG gel beads were then transferred to the CTS solution for 24 h of combination. The ALG–CTS complex gel beads were thus obtained and washed with deionized water to remove the unreacted CTS on the surface.

Crosslinking: the ALG–CTS complex gel beads were transferred to 4.17% (*w*/*w*) of glutaraldehyde solution to crosslink at 25  $\degree$ C for 12 h. The residual glutaraldehyde on the crosslinked complex gel beads was washed away with deionized water at  $60 °C$ .

Finally, the crosslinked complex gel beads were treated with 1 mol/L HCl to completely elute the template  $Cu(II)$  ions. After that, the samples were dried at 50 °C under vacuum for 12 h. The obtained product was the  $Cu(II)$  ion-imprinted ALG–CTS complex adsorbent and was labelled as Cu(II)-IIP.

For comparison, the non-ion-imprinted ALG–CTS complex adsorbent (NIP) was also prepared under the same conditions as above but without adding template  $Cu(II)$  ions.

#### **Characterization**

The morphology of the Cu(II)-IIP before drying was observed by ZSA302 zoom stereomicroscope (Chongqing Optical Instrument Co., Ltd., China). The Cu(II)-IIP was freeze-dried and observed by HIROX SH-4000M desktop scanning electron microscope (Questar China Limited, USA). The infrared spectra were recorded by Spectrum-2000 FTIR (Perkin-Elmer, USA) with a solid KBr tablet method. The adsorption capacity of the adsorbent was detected by Cary 50 UV spectrophotometer (Varian, USA) at room temperature.

#### **Batch adsorption**

A total of 0.01 g of adsorbent was mixed with 50 mL of  $Cu^{2+}$  solutions with different initial concentrations and pH values in a conical fask. The pH value was adjusted by 0.1 mol/L HCl or 0.1 mol/L NaOH. The batch experiments were carried out in a shaking air bath at 25  $\degree$ C for 24 h. The adsorbent was separated by filtration, and the concentration of  $Cu^{2+}$  in solution was analysed using an UV spectrophotometer. The amount of Cu(II) bound on Cu(II)-IIP and NIP was calculated according to the following equation:

$$
q_e = \frac{(C_0 - C_e)V}{m} \tag{1}
$$

where  $q_e$  is the equilibrium adsorption capacity (mg/g);  $C_0$  and  $C_e$  are the initial and equilibrium concentrations of  $Cu^{2+}$  in the adsorption solution ( $\mu$ g/mL), respectively; *V* is the volume of the adsorption solution (mL); and *m* is the mass of adsorbent (g).

#### **Selectivity of Adsorption**

The selective adsorption test of Cu(II)-IIP towards  $Cu^{2+}$  was implemented with  $Zn^{2+}$  as the competitor. A total of 0.01 g of Cu(II)-IIP was added into 50 mL of solution with 60 mg/L of Cu(II) or  $Zn(II)$  at pH 5.73. The residual concentration of ions in the solution was measured at intervals by a UV spectrophotometer until the adsorption reached equilibrium. Imprinting factor  $(\beta)$  and separation factor  $(\alpha)$  were used to evaluate the selectivity of Cu(II)-IIP and were calculated as follows.

$$
K_d = \frac{C_p}{C_s} \tag{2}
$$

$$
\beta = \frac{K_{dIP}}{K_{dNP}}\tag{3}
$$

$$
\alpha = \frac{K_{dCu}}{K_{dZn}}\tag{4}
$$

where  $K_d$  is the static partition coefficient (mL/g);  $C_p$  is the equilibrium concentration of metal ions on the adsorbent ( $\mu$ g/g);  $C_s$  is the equilibrium concentration of metal ions in the solution ( $\mu$ g/mL);  $K_{dIP}$  and  $K_{dNP}$  are the static partition coefficients of Cu(II) for Cu(II)-IIP and NIP, respectively; and  $K_{dCu}$  and  $K_{dZn}$  are the static partition coefficients of Cu(II) and Zn(II), respectively.  $\beta$  reflects the difference of Cu(II)-IIP and NIP in template ion recognition. The greater  $\beta$  indicates the better

imprinting effect.  $\alpha$  reflects the selectivity of adsorbent for template ion. If  $\alpha > 1$ , it indicates a certain selectivity, and the greater  $\alpha$  means the better selectivity.

#### **Regeneration**

The regeneration of an adsorbent decides the economic success of the adsorption process. Desorption experiments of Cu(II)-adsorbed Cu(II)-IIP were performed at ambient temperature for 80 min using 1 mol/L hydrochloric acid solution as the stripping agent. After that, Cu(II)-IIP was separated and washed with distilled water and then dried in a vacuum oven at 50  $^{\circ}$ C. The adsorption–desorption cycle was repeated fve times to assess the reusability of the Cu(II)-IIP complex adsorbent.

## **Results and Discussion**

## **Imprinting Process of Cu(II)‑IIP**

In the preparation of  $Cu(II)$ -IIP complex adsorbent, two kinds of natural polymer materials, SA and CTS, were adopted as the functional matrix. The imprinting process is suggested schematically in Fig. [1.](#page-4-0) The carboxylate ions of SA possibly formed ionic complexes with  $Cu^{2+}$  while the hydroxyls of SA could form coordinate bonds to  $Cu^{2+}$ . Thanks to these two kinds of chemical bonds, many stable structures like eggbox were formed in SA. This was the frst type of imprinting site of Cu(II)-IIP, and the whole structure was negatively charged. Meanwhile, coordination bonds could be easily formed between the aminos of chitosan and  $Cu^{2+}$ . This was the second type of imprinting site of Cu(II)-IIP, and the whole structure of acidifed CTS was positively charged. An ionic complex could be established between



<span id="page-4-0"></span>**Fig. 1** Schematic preparation of Cu(II)-IIP complex adsorbent



<span id="page-5-0"></span>**Fig. 2** FTIR spectra: **a** CTS, **b** Cu(II)-IIP and **c** SA

<span id="page-5-1"></span>**Table 1** Characteristic peaks of FTIR spectra

$SA$ (cm <sup>-1</sup> )	$CTS$ (cm <sup>-1</sup> )	$Cu(II)-IIP$ (cm <sup>-1</sup> )			
3490: $v(0-H)$	3440: $v(0-H)$	3504: $v$ (O-H)			
	[including $v(N-H)$ ]	[including $v$ (N-H)]			
	2875: $v$ (C-H)	2832: $v$ (C-H)			
1615: $v_{\text{as}}$ (COO <sup>-</sup> )	1656: $v$ (C=O) (amide I)	1736: $v(C=0)$			
1421: $v$ (COO <sup>-</sup> )	1590: δ (N-H)				
	[including 1550 amide II: $v$ (C–N) + $\delta$ (N–H)]				
1031: $v_{\text{ss}}$ (C-O-C)	1158: $v_{\text{ac}}$ (C-O-C) + v (C-N)	1036: $v_{\text{as}}$ (C-O-C)			
	1088: $v_{\text{ss}}$ (skeleton)				

the eggbox-like structures and the acidifed CTS via ionic interaction, although the strength of the eggbox-like structures was actually deficient due to the water dis-sociation [\[19](#page-15-11)]. Therefore, the ionic interaction of COO<sup>−</sup> and NH<sub>3</sub><sup>+</sup> played an important role in the preparation of Cu(II)-IIP. After the template  $Cu^{2+}$  was removed by elution, the Cu(II)-IIP could rebind  $Cu^{2+}$  selectively. The imprinting sites with the proper size and oriented groups exactly for  $Cu^{2+}$  in  $Cu(II)$ -IIP would contribute to a high adsorption efficiency and selectivity for  $Cu^{2+}$  due to metal–ligand chemistry [\[20](#page-15-12)].

#### **FTIR Spectra**

The spectra of SA, CTS and Cu(II)-IIP are shown in Fig. [2](#page-5-0), and the typical peaks of the chemical bonds in the three samples are presented in Table [1](#page-5-1) [\[21](#page-15-13)].

As shown in Fig. [2](#page-5-0) and Table [1,](#page-5-1) the typical peaks at 1656 and 1590 cm−1 attributing to the amide in CTS disappeared after imprinting. Similarly, the peaks at 1615 and 1421 cm−1 attributing to the antisymmetric and symmetric stretching vibration of −COO− in SA also disappeared after imprinting. However, a new peak at 1736 cm−1 was observed in the Cu(II)-IIP. The results of FTIR revealed that a reaction occurred between the  $-NH_2$  in CTS and  $-COO^-$  in SA during the imprinting process.



<span id="page-6-0"></span>**Fig. 3** Surface structures of Cu(II)-IIP and NIP. **a** Stereomicroscopic light image of wet Cu(II)-IIP beads, **b** stereomicroscopic backlight image of wet Cu(II)-IIP beads, **c** SEM of freeze-dried NIP beads ( $\times$ 100), **d** SEM of freeze-dried Cu(II)-IIP beads (×100), **e** SEM of freeze-dried Cu(II)-IIP beads after adsorption of  $Cu^{2+}$  ( $\times$ 100) and **f** energy spectrum of freeze-dried Cu(II)-IIP beads after adsorption of Cu<sup>2+</sup>

#### **SEM Analysis**

Figure [3a](#page-6-0), b is the stereomicroscopic images of the wet  $Cu(II)$ -IIP beads under light and backlight conditions, respectively. As shown in the pictures, the  $Cu(II)$ -IIP beads were in the state of hydrogel with a certain content of moisture and smooth surface. The particle size was uniform and the average size was about 1.78 mm.

The SEM of freeze-dried NIP and Cu(II)-IIP beads is shown in Fig. [3](#page-6-0)c, d. A lot of folds were observed on the surfaces of the two kinds of beads due to the dehydration of the gel beads. However, the degree of surface folds on Cu(II)-IIP was smaller than that on NIP. It was attributed to the structure change in the presence of  $Cu^{2+}$ during imprinting, which resulted in a slower rate of water loss.

The SEM of Cu(II)-IIP complex beads after adsorption of  $Cu^{2+}$  is shown in Fig. [3](#page-6-0)e. The more surface folds were observed and they arranged closely, indicating that the presence of  $Cu^{2+}$  had influence on the surface morphology of  $Cu(II)$ -IIP complex adsorbent, also confirming that  $Cu^{2+}$  could change the three-dimensional network structure of the complex gel beads and then afected the water loss process. Figure [3](#page-6-0)f is the corresponding electron difraction energy spectrum diagram of Fig. [3](#page-6-0)e. A strong peak of element Cu showed that the  $Cu(II)$ -IIP has a strong adsorption ability for  $Cu(II)$ . At the same time, the peak of element N was also observed, which meant that CTS was successfully combined with ALG to form composite. And the composite was stable enough to endure elution to produce Cu(II)-IIP.

#### **Adsorption Experiments**

#### **Infuence of pH Value**

The pH value of solution is one of the most important parameters governing the uptake of metal ions on adsorbents [\[22](#page-15-14)]. The effect of pH value on  $Cu^{2+}$  adsorption by



<span id="page-7-0"></span>**Fig. 4** Effect of pH value on  $Cu^{2+}$  adsorption capacity

Cu(II)-IIP was investigated at diferent pH values ranging from 2.61 to 5.73, and the results are shown in Fig. [4](#page-7-0).

As shown in Fig. [4,](#page-7-0) the adsorption of  $Cu^{2+}$  on  $Cu(II)$ -IIP was pH-dependent, and the adsorption capacity increased as the solution pH value increased from 2.61 to 5.73. When the pH value was below 4.07, the adsorption capacities of Cu(II)-IIP was very low, which was mainly due to the protonation of the −NH<sub>2</sub> group moieties and their diminishing ability to chelate  $Cu^{2+}$  [[23](#page-15-15)]. The adsorption of  $Cu^{2+}$  on Cu(II)-IIP was higher when the pH value was over 4.73. The possible reason was that the  $NH_3^+$ groups were deprotonated and their chelating ability was recovered. When the pH value of solution was increased to 6.0,  $Cu(II)$  was deposited as  $Cu(OH)_{2}$ . Thus, the pH value of solution should be adjusted to  $pH$  5.73 to obtain the optimal adsorption efficiency.

#### **Adsorption Isotherm**

Figure [5](#page-8-0) shows the adsorption isotherm of Cu(II)-IIP towards Cu<sup>2+</sup> at pH 5.73. It could be observed that the equilibrium adsorption capacity  $(q_e)$  increased sharply in the low initial concentration of  $Cu^{2+}$  and then increased slowly until saturation.

In order to describe the  $Cu(II)$  distribution between the liquid and adsorbent phases and the maximum adsorption capacity of  $Cu(II)$ -IIP, Langmuir and Freundlich isotherm models were used to ft the adsorption process as follows.

$$
\frac{C_e}{q_e} = \frac{1}{bq_{\text{max}}} + \frac{C_e}{q_{\text{max}}}
$$
(5)

$$
\ln q_e = \ln k_f + \frac{1}{n} \ln C_e \tag{6}
$$



<span id="page-8-0"></span>**Fig. 5** Adsorption isotherm of  $Cu^{2+}$  on  $Cu(II)$ -IIP



<span id="page-9-0"></span>**Fig. 6** Fitting results of adsorption isotherm of  $Cu^{2+}$  on Cu(II)-IIP. **a** Langmuir model and **b** Freundlich model

<span id="page-9-1"></span>

where  $q_e$  is the equilibrium adsorption capacity (mg/g);  $C_e$  is the equilibrium concentration of Cu<sup>2+</sup> (μg/mL);  $q_{\text{max}}$  is the maximum adsorption capacity (mg/g); *b* is the Langmuir constant that represents the affinity between solute and adsorbent; and  $k_f$  and *n* are Freundlich constants related to the adsorption capacity and the adsorption intensity, respectively.

The ftting results of Langmuir and Freundlich isotherms for the adsorption of  $Cu^{2+}$  on Cu(II)-IIP are shown in Fig. [6](#page-9-0) and Table [2.](#page-9-1) According to the value of correlation coefficient  $(R^2)$ , the Langmuir model  $(R^2 = 0.993)$  was more suitable than the Freundlich model ( $R^2$ =0.878) for describing the adsorption process. The maximum adsorption capacity obtained from Langmuir model was 83.33 mg/g, which indicated that the Cu(II)-IIP had a strong affinity for  $Cu^{2+}$ .

#### **Adsorption Kinetics**

Figure [7](#page-10-0) shows the time dependence of the adsorption amounts of  $Cu^{2+}$  on  $Cu(II)$ -IIP with 60 ug/ml of the initial  $Cu^{2+}$  concentration and contact time from 0 to 25 h at pH 5.73. It could be seen from Fig. [7](#page-10-0) that the adsorption amounts increased rapidly during the first  $12$  h and then leveled off as equilibrium was reached. The high adsorption rate at the beginning was attributed to the sufficient adsorption sites on Cu(II)-IIP with strong chelation and good affinity towards  $Cu^{2+}$  [\[23](#page-15-15)].

Adsorption kinetics is usually used to confrm the rate controlling step of adsorption. To reveal the mechanism of adsorption, the adsorption kinetics for  $Cu^{2+}$  onto the Cu(II)-IIP were investigated by three kinetics models, namely Lagergren pseudofrst-order model, pseudo-second-order model and Weber–Morris model. The linear forms of the three models are expressed as follows:



<span id="page-10-0"></span>**Fig. 7** Variation of adsorption amount of  $Cu^{2+}$  with contact time

$$
\ln(q_e - q_t) = \ln q_e - k_1 t \tag{7}
$$

$$
\frac{t}{q_t} = \left(\frac{1}{k_2 q_e^2}\right) + \frac{t}{q_e} \tag{8}
$$

$$
q_t = k_{\text{dif}}t^{0.5} \tag{9}
$$

where  $q_e$  and  $q_t$  are the adsorption capacity (mg/g) at equilibrium and at time  $t$  (h), respectively;  $k_1$ ,  $k_2$ ,  $k_{\text{dif}}$  are the adsorption rate constants. The adsorption kinetic con-stants and correlation coefficients are summarized in Table [3.](#page-10-1)

According to the data presented in Fig. [8](#page-11-0) and Table [3,](#page-10-1) the kinetic curve ftted the pseudo-frst-order model in the frst 8 h, and the pseudo-second-order mechanism was predominant after 8 h. This meant that the  $Cu^{2+}$  diffusion onto and in the Cu(II)-IIP could be the rate controlling step at frst. Then, the adsorption was dominated by the intraparticle difusion and the inner surface binding. The inner surface binding was associated with the chemisorption of  $Cu^{2+}$  onto the two types of imprinting sites in the  $Cu(II)$ -IIP as illustrated in Fig. [1.](#page-4-0)

Weber–Morris model was usually used to estimate whether the intraparticle difusion was the rate controlling step of adsorption. According to the Weber–Morris model,

	Adsorbent Pseudo-first-order			Pseudo-second-order			Weber-Morris model	
		$k_1$ (1/h) $q_{e,m}$ (mg/g) $R^2$		$k_2$ (g/mg h) $q_{e,m}$ (mg/g) $R^2$			$k_{\text{dif}}$ (mg/g h <sup>1/2</sup> ) $R^2$	
$Cu(II)$ -IIP $0.159$		73.6	0.984	0.003	82.5	0.949 23.52		0.981

<span id="page-10-1"></span>**Table 3** Fitting results of adsorption kinetics models



<span id="page-11-0"></span>**Fig. 8** Pseudo-first-order model (filled square) for  $Cu^{2+}$  adsorption before 8 h and pseudo-second-order model (filled circle) for  $Cu^{2+}$  adsorption after 8 h



<span id="page-11-1"></span>**Fig. 9** Fitting plot of intraparticle diffusion model for  $Cu^{2+}$  adsorption

the fitting plot of  $q_t$  versus time  $t^{0.5}$  is shown in Fig. [9](#page-11-1) and the regression parameters are listed in Table [3](#page-10-1). It showed that the  $Cu^{2+}$  adsorption onto the  $Cu(II)$ -IIP was not always linear and could be divided into two stages, which demonstrated that there are not only one rate limiting step during the  $Cu^{2+}$  adsorption.

From the above discussion, an explanation about the kinetic process of adsorption of  $Cu^{2+}$  onto  $Cu(II)$ -IIP was suggested. At the beginning, the adsorption was fast owing to the diffusion of  $Cu^{2+}$  from the solution to the external surface of Cu(II)-IIP. Then, the Cu<sup>2+</sup> gradually passed through the apertures in Cu(II)-IIP at a lower speed, and they were subsequently bound to the imprinting sites through the



<span id="page-12-0"></span>**Fig. 10** Variation of adsorption amount of metal ions with contact time

Metal ion	$Cu(II)$ -IIP			<b>NIP</b>			
	$q \text{ (mg/g)}$	$K_d$ (mL/g)	$\alpha$	$q \text{ (mg/g)}$	$K_d$ (mL/g)	$\alpha$	
$Cu2+$	71.15	31.09	2.28	50.92	20.44	1.72	1.52
$Zn^{2+}$	36.03	13.65	$\overline{\phantom{0}}$	31.82	11.87	-	

<span id="page-12-1"></span>**Table 4** Selective adsorption of Cu(II)-IIP for  $Cu^{2+}$  versus  $Zn^{2+}$ 

electrostatic attraction and metal–ligand interaction. The intraparticle difusion and the inner surface binding were the main rate controlling steps. Finally, the adsorption equilibrium occurred when the imprinting sites were all occupied and the intraparticle difusion reached steady state.

#### **Selectivity of Cu(II)‑IIP**

 $Zn(II)$  ion was chosen as the competitor ion due to the fact that  $Zn^{2+}$  has the same charge and similar size to  $Cu^{2+}$ . As shown in Fig. [10](#page-12-0), the adsorption amount of Cu(II)-IIP did not stop increasing with contact time until 12 h for Cu(II) but 5 h for  $Zn(II)$  when the equilibrium reached. The equilibrium adsorption capacity of  $Cu^{2+}$ was clearly higher than that of  $Zn^{2+}$ . It implied that Cu(II)-IIP exhibited a much stronger affinity to  $Cu^{2+}$  than that to  $Zn^{2+}$ .

Static distribution coefficients, separation factor ( $\alpha$ ) and imprinting factor ( $\beta$ ) are calculated and summarized in Table [4](#page-12-1). From Table [4,](#page-12-1) the separation factor of  $Cu(II)$ -IIP for  $Cu(II)$  versus  $Zn(II)$  reached 2.28 and the imprinting factor reached 1.52 compared with NIP. It confrmed that the Cu(II)-IIP had a certain selective recognition for  $Cu(II)$ . As in Fig. [1](#page-4-0), the imprinted sites with specific recognition groups in a predetermined orientation for  $Cu^{2+}$  were formed in the Cu(II)-IIP.  $Cu^{2+}$  could be rebound to the imprinting sites while  $\text{Zn}^{2+}$  could not match the imprinting sites well



<span id="page-13-0"></span>**Fig. 11** Efect of the time of reuse on adsorption capacity

<span id="page-13-1"></span>**Table 5** The adsorption for Cu(II) of some absorbents reported in the literature

Adsorbents	$q_{\text{max}}$ (mg/g)	Equilibrium time (h)	Optimum pH	References
$Cu(II)$ -MICA	46.25	6.0	5.5	$\lceil 24 \rceil$
$Cu(II)$ -MIIP	24.20	0.17	5.0	[25]
$Cu(II)$ -IIP	76.00	0.17	5.0	[26]
$Cu(II)$ -MICA	71.36	4.0	5.5	[27]
CTS-ECH-TPP	166.94	20.0	6.0	[28]
$Cu-ALG-CTS$	70.54	13.0		[29]
$Cu(II)$ -IIP	83.33	8.0	5.7	This work

in shape, size, and functional groups. Therefore, the Cu(II)-IIP showed the specifc selectivity and higher adsorption capacity for  $Cu^{2+}$ .

## **Regeneration and Reuse of Cu(II)‑IIP**

The stability and reusability of  $Cu(II)$ -IIP were investigated by means of adsorption–desorption cycle, and the results are illustrated in Fig. [11](#page-13-0). It was found that the adsorption capacity of Cu(II)-IIP for  $Cu^{2+}$  was stable in the first three cycles without significant reduction. This referred that the  $Cu(II)$ -IIP could be regenerated effectively and reused to lower the cost.

## **Adsorption Performance**

Our work and some other reported absorbents for adsorption of  $Cu(II)$  are listed in Table [5](#page-13-1). The prepared Cu(II)-IIP has high binding capacity for  $Cu(II)$  and possesses potential application in the removal of Cu(II) from wastewater.

## **Conclusions**

A novel Cu(II) ion-imprinted complex adsorbent (Cu(II)-IIP) from alginate and chitosan was successfully prepared by a three-step process of beading–combining–crosslinking. FTIR suggested that the ionic interaction occurred between the amino of chitosan and the carboxyl of alginate during imprinting. SEM indicated that the morphology of the  $Cu(II)$ -IIP was affected by the imprinting process. The adsorption and selectivity of Cu(II)-IIP for Cu<sup>2+</sup> were investigated in detail. It was found that the adsorption amount of  $Cu^{2+}$  varied obviously with pH value, initial  $Cu^{2+}$  concentration and contact time. The suitable pH value for favourable  $Cu<sup>2+</sup>$  adsorption was 5.73. The adsorption isotherm well fitted Langmuir model, which indicated that the monolayer coverage of  $Cu^{2+}$  was formed at the surface of  $Cu(II)$ -IIP and the theoretical maximum adsorption capacity was 88.33 mg/g. The adsorption of Cu(II)-IIP for Cu<sup>2+</sup> performed rapidly at first and then slowed down until reaching equilibrium. Pseudo-frst-order model, pseudo-second-order model and Weber–Morris model were used to ft the adsorption behaviour, which suggested that the adsorption rate would be controlled dominantly by the intraparticle difusion and the inner surface binding. Competitive adsorption test showed that the Cu(II)-IIP had the specifc selectivity and higher adsorption capacity for Cu <sup>2+</sup> versus  $\text{Zn}^{2+}$  with a separation factor of 2.28 due to the Cu<sup>2+</sup> imprinting sites. The regeneration experiments demonstrated that the Cu(II)-IIP could be repeatedly used without signifcant loss in adsorption capacity. These conclusions suggested that the Cu(II)-IIP could be used as a feasible adsorbent for selective removal of Cu(II) from water.

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