### ENVIRONMENTAL BIOTECHNOLOGY



# Nitrous oxide emissions from biofilm processes for wastewater treatment

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Received: 5 April 2018 / Revised: 13 August 2018 /Accepted: 15 August 2018 /Published online: 10 September 2018  $\circled{c}$  Springer-Verlag GmbH Germany, part of Springer Nature 2018

#### Abstract

This paper discusses the microbial basis and the latest research on nitrous oxide  $(N_2O)$  emissions from biofilms processes for wastewater treatment. Conditions that generally promote  $N_2O$  formation in biofilms include (1) low DO values, or spatial DO transitions from high to low within the biofilm; (2) DO fluctuations within biofilm due to varying bulk DO concentrations or varying substrate concentrations; (3) conditions with high reaction rates, which lead to greater formation of intermediates, e.g., hydroxylamine (NH<sub>2</sub>OH) and nitrite (NO<sub>2</sub><sup>-</sup>), that promote N<sub>2</sub>O formation; and (4) electron donor limitation for denitrification. Formation of  $N_2O$  directly results from the activities of ammoniaoxidizing bacteria (AOB), ammonia-oxidizing archaea (AOA), and heterotrophic denitrifying bacteria. More research is needed on the roles of AOA, comammox, and specialized denitrifying microorganisms. In nitrifying biofilms, higher bulk ammonia (NH<sub>3</sub>) concentrations, higher nitrite (NO<sub>2</sub><sup>-</sup>) concentrations, lower dissolved oxygen (DO), and greater biofilm thicknesses result in higher  $N_2O$  emissions. In denitrifying biofilms,  $N_2O$  accumulates at low levels as an intermediate and at higher levels at the oxic/anoxic transition regions of the biofilms and where COD becomes limiting. N<sub>2</sub>O formed in the outer regions can be consumed in the inner regions if COD penetrates sufficiently. In membraneaerated biofilms, where nitrification takes place in the inner, aerobic biofilm region, the exterior anoxic biofilm can serve as a N<sub>2</sub>O sink. Reactors that include variable aeration or air scouring, such as denitrifying filters, trickling filters, or rotating biological contactors (RBCs), can form peaks of  $N<sub>2</sub>O$  emissions during or following a scouring or aeration event.  $N_2O$  emissions from biofilm processes depend on the microbial composition, biofilm thickness, substrate concentrations and variability, and reactor type and operation. Given the complexity and difficulty in quantifying many of these factors, it may be difficult to accurately predict emissions for full-scale treatment plants. However, a better understanding of the mechanisms and the impacts of process configurations can help minimize  $N_2O$  emission from biofilm processes for wastewater treatment.

Keywords  $N_2O \cdot$  Biofilms  $\cdot$  Hydroxylamine  $\cdot$  MBBR  $\cdot$  MABR  $\cdot$  MBfR  $\cdot$  Granules

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# Introduction

Wastewater treatment processes can be a significant source of nitrous oxide  $(N_2O)$ , a powerful greenhouse gas  $(GHG)$ with a global warming potential around 300 times that of carbon dioxide  $(CO<sub>2</sub>)$  (Montzka et al. [2011](#page-12-0)). N<sub>2</sub>O is very stable and may persist in the atmosphere for over 120 years (Kampschreur et al. [2009](#page-11-0); Schreiber et al. [2012\)](#page-13-0). The U.S. Environmental Protection Agency (EPA) estimates that U.S. wastewater treatment plants emit around 5.2 Tg N<sub>2</sub>O year<sup>-1</sup> as  $CO<sub>2</sub>$  equivalents (Ritter & Chitikela [2014\)](#page-13-0), and these amounts are expected to increase with time (Law et al. [2012;](#page-12-0) Okabe et al. [2011](#page-12-0)).

Much past research has addressed  $N_2O$  emissions from suspended growth processes (Ahn et al. [2010](#page-10-0); Kampschreur et al. [2009](#page-11-0); Law et al. [2012](#page-12-0)). However, much less is known about emissions from biofilm processes, such as the moving bed biofilm reactor (MBBR), integrated fixed-film activated sludge (IFAS), biological aerated filter (BAF), granular sludge, and membrane-aerated biofilm reactors (MABRs) (Henze et al. [2008](#page-11-0); Martin and Nerenberg [2012](#page-12-0); Syron and Casey [2008\)](#page-13-0). Biofilm processes are becoming increasingly popular due to their higher volumetric treatment rates, reduced operational costs, minimal need for settling, and operational simplicity (Henze et al. [2008](#page-11-0); Khan et al. [2013;](#page-11-0) Nicolella et al. [2000;](#page-12-0) WEF [2010\)](#page-14-0).

While the microbial basis of  $N_2O$  formation, i.e., the microorganisms and metabolic pathways leading to its formation, are the same for suspended growth and biofilm systems, the observed behavior may be very different. This results from the microbial stratification, microbial interactions, substrate gradients, and substrate interactions unique to biofilms, as well as the biofilm reactor configuration (Henze et al. [2008](#page-11-0); Law et al. [2012;](#page-12-0) Vlaeminck et al. [2010](#page-14-0)). Thus, the "mechanisms" leading to  $N_2O$ emissions in biofilms may significantly differ from those of suspended growth systems.

Todt and Dorsch ([2016\)](#page-14-0) provided a comprehensive review of  $N_2O$  emissions from biofilm systems. They explored the biochemistry of  $N_2O$  production/consumption in relevant organisms, discussed current biofilm models, evaluated possible environmental factors affecting  $N_2O$ emissions, and tabulated emission factors for different processes. Massara et al. ([2017](#page-12-0)) briefly addressed biofilms as part of a comprehensive review of  $N_2O$  emissions from wastewater processes. This review provides an update, considering new information on the  $N<sub>2</sub>O$  emissions from microbial systems. It also discusses new types of microbial metabolism and different biofilm reactor configurations, and their impacts on  $N<sub>2</sub>O$  emissions.

### Biofilms vs. suspended growth systems

Biofilms are aggregates of microbial cells embedded in a network of self-produced extracellular polymeric substances (EPS) (Flemming et al. [2016;](#page-11-0) Stoodley et al. [2002](#page-13-0)). Biofilms are widespread in natural systems (Donlan [2002\)](#page-10-0) and increasingly used in engineered treatment processes, especially for those with low substrate concentrations and high flows (Henze et al. [2008;](#page-11-0) Nicolella et al. [2000](#page-12-0); WEF [2010](#page-14-0)). Unlike with suspended bacteria, diffusion and reaction in biofilms lead to substrate gradients. As a result, concentrations in the biofilm may differ significantly from those in the bulk liquid (Fig. 1). In addition, bacteria stratify into layers, where different types of metabolism may predominate at different depths within the biofilm.

The dynamics of growth, decay, and detachment influence the microbial community structure of biofilms (Elenter et al.  $2007$ ). Slow growing organisms may be "pushed out" of the biofilm by faster growing organisms (Lackner et al. [2008;](#page-11-0) Xavier et al. [2005\)](#page-14-0). Metabolic products may diffuse out of the biofilm or may be consumed by other populations. pH gradients may form due to proton-producing or consuming processes within the biofilm (Vroom et al. [1999\)](#page-14-0). The greater complexity of biofilms, compared to suspended growth processes, makes their behavior more difficult to predict.

# $N<sub>2</sub>O$  and nitrogen cycle

This section discusses basic microbial transformations that affect  $N_2O$  formation in wastewater treatment processes. These processes are relevant to both suspended growth and biofilm processes. The relationship between these transformations and N<sub>2</sub>O formation in biofilms is discussed in subsequent sections.

The nitrogen cycle includes a number of N species and both microbial and abiotic transformations, where N varies in redox state between − 3 and + 5. While most of the nitrogen

Fig. 1 Idealized schematics of a a floc and b a biofilm. The biofilm schematic shows the liquid diffusion layer (LDL), as well as profiles of a substrate and metabolic product. Note that real flocs are highly complex and heterogeneous in morphology, and biofilms may have rough or dendritic surfaces with internal pores



<span id="page-2-0"></span>cycle is well established, new biotic and abiotic transformation processes continue to be discovered (Daims et al. [2016](#page-10-0); Kuypers et al. [2018;](#page-11-0) Schreiber et al. [2012](#page-13-0); Stein and Klotz [2016\)](#page-13-0). Figure 2 schematically shows key N species and biological transformations. For wastewater treatment processes, the key transformations include nitrification and denitrification, where nitrate  $(NO<sub>3</sub><sup>-</sup>)$  is sequentially reduced to nitrogen gas  $(N_2)$ . Both processes can lead to  $N_2O$  formation.

#### $N<sub>2</sub>O$  from microorganisms related to nitrification

Nitrification is carried out by the sequential activity of ammonia-oxidizing bacteria (AOB) and archaea (AOA), and nitrite-oxidizing bacteria (NOB). AOB and AOA oxidize ammonia (NH<sub>3</sub>) to nitrite (NO<sub>2</sub><sup>-</sup>), with hydroxylamine (NH<sub>2</sub>OH) as an intermediate (Fig. [3](#page-3-0)) (Daims et al. [2016](#page-10-0); Guo et al. [2017\)](#page-11-0), while NOB oxidize  $NO_2^-$  to  $NO_3^-$ . AOB directly produce  $N_2O$  through two main pathways: nitrifier denitrification and  $NH<sub>2</sub>OH$  oxidation (Fig. [3](#page-3-0)). NOB, AOA, anammox, and comammox microorganisms may play an indirect role in  $N_2O$ formation by affecting the availability of  $NH_3$  and  $NO_2^-$ .

In the nitrifier denitrification pathway, AOB reduce  $NO_2^-$  to nitric oxide (NO) and  $N_2O$  (Chandran et al. [2011](#page-10-0); Kampschreur et al. [2007](#page-11-0); Kim et al. [2010;](#page-11-0) Tallec et al. [2006](#page-13-0)) (Fig. [3](#page-3-0)). The NH<sub>2</sub>OH oxidation pathway involves the oxidation of NH<sub>2</sub>OH to NO by hydroxylamine oxidoreductase (HAO) and subsequent reduction to  $N_2O$  catalyzed by the enzyme NO reductase (Chandran et al. [2011;](#page-10-0) Law et al. [2012;](#page-12-0) Stein [2011\)](#page-13-0) (Fig. [3\)](#page-3-0).



Fig. 2 Key processes in the N-cycle.  $N_2O$  is highlighted in gray (adapted from Daims et al. [2016](#page-10-0) and Schreiber et al. [2012](#page-13-0)). The dashed line for comammox shows not only the formation of  $NO_2^-$  as intermediate but also its oxidation to  $NO_3^-$  by the same organism. Abbreviations in figure: DNRA is dissimilatory nitrite reduction to ammonia; assimil. is assimilatory; dissimil. is dissimilatory. Note that denitrification can produce  $N<sub>2</sub>O$ , but it is also the only known process that can reduce it

Recent findings show that, in the canonical nitrifying bacteria N. europaea, two other routes for  $N_2O$  production exist under anaerobic conditions. One is the direct oxidation of  $NH<sub>2</sub>OH$  to  $N<sub>2</sub>O$  by cytochrome P460 (Caranto et al. [2016](#page-10-0)) and the nitrification intermediate NO (Caranto and Lancaster [2017\)](#page-10-0). Although not all AOB share the same route for  $N_2O$ production, these recent findings expand on previous knowledge where chemical reactions were thought to be mainly important at higher oxygen  $(O_2)$  levels (Liu et al. [2017a\)](#page-12-0).

 $N<sub>2</sub>O$  can also be produced biologically or abiotically by coupling NH<sub>2</sub>OH oxidation with the reduction of  $NO_2^-$ (Harper et al. [2015](#page-11-0); Terada et al. [2017](#page-14-0)), free nitrous acid  $(HNO<sub>2</sub>)$  (Soler-Jofra et al. [2016\)](#page-13-0), or NO (Spott et al. [2011\)](#page-13-0). These are termed N-nitrosation hybrid reactions, or simply "hybrid" reactions (Spott and Stange [2011](#page-13-0)). In addition, metals, such as copper (Harper et al. [2015\)](#page-11-0) and manganese (Heil et al.  $2015$ ), can catalyze abiotic N<sub>2</sub>O production from NH2OH via the hybrid reaction. Under some conditions, the hybrid reaction can become a predominant pathway for  $N_2O$ production in a partial nitrifying reactor (Soler-Jofra et al. [2018](#page-13-0); Terada et al.  $2017$ ). N<sub>2</sub>O production via the hybrid reaction is enhanced in the presence of AOB (Liu et al. [2017a;](#page-12-0) Terada et al. [2017](#page-14-0)).

Under aerobic conditions,  $N_2O$  is mainly formed via the NH2OH pathway, and rates are relatively low. When DO concentrations decrease, the nitrifier denitrification pathway becomes more important, leading to higher rates of  $N<sub>2</sub>O$  formation (Chen et al. [2018;](#page-10-0) Kampschreur et al. [2009](#page-11-0); Ma et al. [2017a](#page-12-0); Park et al. [2000;](#page-12-0) Tallec et al. [2008](#page-13-0)). However, under complete anoxic conditions  $N_2O$  emissions are again low due to the lack of DO for NH<sub>[3](#page-3-0)</sub> oxidation (Fig. 3). Spikes of  $N_2O$ production can occur at transitions from anoxic to aerobic, or aerobic to anoxic, conditions, due to an electron imbalance (Domingo-Felez et al. [2014](#page-10-0); Kampschreur et al. [2008;](#page-11-0) Sabba et al.  $2015$ ; Yu et al.  $2010$ ). Thus, N<sub>2</sub>O emissions can be significant in processes with anoxic/aerobic stages or intermittent aeration (Chandran et al. [2011\)](#page-10-0).

Unlike AOB, which have well-elucidated  $N_2O$  production pathways, the pathways for AOA are yet to be fully understood (Blum et al.  $2018b$ ). They perform NH<sub>3</sub> oxidation in a similar way to AOB (Kozlowski et al. [2016\)](#page-11-0); however, they lack the ability to produce  $N_2O$  enzymatically through side reactions of NH3 oxidation or nitrifier denitrification, as mediated by AOB (Spang et al. [2012;](#page-13-0) Tourna et al. [2011;](#page-14-0) Walker et al. [2010\)](#page-14-0). Stieglmeier et al. ([2014](#page-13-0)) showed that Nitrososphaera *viennensis*, a pure culture of AOA from soil, produces  $N_2O$ via a hybrid reaction. While AOA are found in WWTPs (Park et al. [2006;](#page-13-0) Sauder et al. [2012](#page-13-0); Zhang et al. [2009\)](#page-14-0), AOA are more common in marine environments (Santoro et al. [2011\)](#page-13-0) and soils (Gubry-Rangin et al. [2010;](#page-11-0) Li et al. [2018](#page-12-0); Nicol et al. [2008](#page-12-0); Zhang et al. [2012\)](#page-14-0).

Anammox bacteria convert NH<sub>3</sub> and NO<sub>2</sub><sup>-</sup> to N<sub>2</sub> under anoxic conditions (Kuypers et al. [2003](#page-11-0)). NO is a key <span id="page-3-0"></span>Fig. 3 Nitrogen transformations in AOB, NOB, and DNB. Abbreviations: AOB, ammoniaoxidizing bacteria; NOB, nitriteoxidizing bacteria; DNB, denitrifying bacteria, AMO, ammonia monooxygenase; HAO, hydroxylamine oxidoreductase (hydroxylamine dehydrogenase in Nitrospira); NXR, nitrite oxidoreductase; NirK, coppercontaining nitrite reductase; NirS, cytochrome cd1 type nitrite reductase; NOR, nitric oxide reductase; and NOS, nitrous oxide reductase. Purple arrows show intermediates potentially shared between nitrification and denitrification pathways. Abiotic reactions (gray) are further discussed in the text



intermediate in anammox metabolism (Kartal et al. [2011](#page-11-0)), and genomic evidence suggests that anammox species have the potential to produce  $N_2O$  via NO reduction (Kartal et al. [2007;](#page-11-0) Strous et al. [2006\)](#page-13-0). However, research suggests that  $N<sub>2</sub>O$  production under process-relevant conditions is negligi-ble (Blum et al. [2018a](#page-10-0)). Anammox may indirectly affect  $N_2O$ formation by heterotrophs and AOB by reducing the concentrations of  $NH_3$  and  $NO_2^-$ .

Comammox bacteria are a subset of the genus Nitrospira capable of complete ammonia oxidation (comammox) via oxidation of NH<sub>3</sub> to NO<sub>3</sub><sup> $-$ </sup> (Daims et al. [2015](#page-10-0); van Kessel et al. [2015\)](#page-14-0). Comammox are thought to have a competitive advantage over conventional ammonia oxidizers (e.g., AOA and AOB) under ammonia-limiting conditions (Costa et al. [2006;](#page-10-0) Daims et al. [2015](#page-10-0); Kits et al. [2017;](#page-11-0) van Kessel et al. [2015\)](#page-14-0). While little is known about comammox in wastewater biofilms, van Kessel et al. ([2015\)](#page-14-0) and Daims et al. [\(2015\)](#page-10-0) obtained comammox enrichments in the lab by operating their systems with low  $NH<sub>3</sub>$  concentrations. Thus, it is likely they play a role in wastewater biofilms under similar conditions.

Evidence suggests that comammox Nitrospira, as opposed to canonical *Nitrospira*, harbor genomic  $NH_3$  and  $NO_2^-$  oxidation machinery homologous to classical AOB and NOB, respectively (e.g., gene clusters encoding *amo*, hao, and nxr) (Daims et al. [2015;](#page-10-0) van Kessel et al. [2015\)](#page-14-0). However, very little is known about their capacity for  $N<sub>2</sub>O$  production. NH2OH appears to be an obligate intermediate of comammox metabolism, analogous to AOB catabolism, and it is likely that  $N_2O$  can be formed by comammox via the NH<sub>2</sub>OH pathway (Fig. 3). Comammox genomes recovered to date also

harbor capacity for  $NO_2^-$  reduction to NO (NirK), similar to non-comammox Nitrospira (Camejo et al. [2017;](#page-10-0) Lawson and Lucker [2018](#page-12-0)). Comammox clades A and B genomes reported to date lack a known NOR or proteins related to NOx metabolism (Palomo et al. [2018\)](#page-12-0), similarly to common Nitrospira taxa (Lawson and Lucker [2018](#page-12-0)) and therefore may be incapable of nitrifier denitrification. Thus, the presence of reactive nitrogen species produced by comammox biomass, e.g., NO or  $NH<sub>2</sub>OH$ , could to lead to abiotic reactions with the production of  $N_2O$  as a final product.

Comammox may be detrimental to PN/A systems, where  $NO_2^-$  production is needed. However, they may also reduce  $N_2O$  emissions by minimizing  $NO_2^-$  accumulation. The presence of comammox in wastewater treatment processes, both in suspended growth and biofilm processes, and the metabolic versatility of Nitrospira species including the two comammox Nitrospira clades is currently an active area of research. Future research should also address the selecting factors for partitioning between comammox and canonical Nitrospira and clarify the potential role for comammox in  $N_2O$  emissions.

### N<sub>2</sub>O from microorganisms related to denitrification

Denitrification is the sequential reduction of  $NO_3$ <sup>-</sup> and  $NO_2$ <sup>-</sup> to NO,  $N_2O$ , and finally  $N_2$  (Ni and Yuan [2015](#page-12-0)). It involves four enzymes: the nitrate reductase (NAR), nitrite reductase (NIR), nitric oxide reductase (NOR), and nitrous oxide reductase (NOS). A schematic of the denitrification metabolism is shown in Fig. 3.

The formation of  $N<sub>2</sub>O$  in wastewater denitrification processes is often due to selective inhibition of the NOS enzyme (Guo et al. [2017\)](#page-11-0). This can be caused by its greater sensitivity to DO (Firestone et al. [1979](#page-11-0); Tallec et al. [2008](#page-13-0)), pH (Firestone et al. [1979;](#page-11-0) Hanaki et al. [1992](#page-11-0)),  $NO<sub>2</sub><sup>-</sup>$  (Alinsafi et al. [2008\)](#page-10-0), carbon source type and concentration (Tallec et al. [2006](#page-13-0)), carbon limitation (Alinsafi et al. [2008;](#page-10-0) Tallec et al. [2006](#page-13-0)), and hydrogen sulfide  $(H<sub>2</sub>S)$  (Schonharting et al. [1998\)](#page-13-0).

While denitrifying bacteria produce  $N_2O$  during denitrification, they also can reduce  $N_2O$  to  $N_2$  (Read-Daily et al.  $2016$ ). Externally supplied N<sub>2</sub>O can be reduced concurrently with  $NO_3^-$  and  $NO_2^-$  (Conthe et al. [2018a](#page-10-0); Pan et al. [2013a,](#page-12-0) [2015;](#page-12-0) Read-Daily et al. [2016](#page-13-0)).

While many denitrifying bacteria have a complete reduction pathway and can reduce  $NO_3^-$  and  $NO_2^-$  all the way to  $N_2$ , less is known about bacteria that can grow with  $N_2O$  but not with  $NO_3^-$  or  $NO_2^-$ . Newly classified clade IItype  $nosZ$  N<sub>2</sub>O reducing bacteria were recently discovered (Jones et al. [2013](#page-11-0); Sanford et al. [2012\)](#page-13-0). These have since been detected in a granular sludge reactor (Lawson et al. [2017\)](#page-12-0), a MABR (Kinh et al. [2017b\)](#page-11-0) and a biofiltration system (Yoon et al. [2017](#page-14-0)). Some isolates harboring clade II type nosZ have higher affinity for  $N_2O$  reduction than those harboring clade I type  $nosZ$  (Suenaga et al. [2018](#page-13-0); Yoon et al. [2016\)](#page-14-0), whereas a contradictory finding was reported (Conthe et al. [2018](#page-10-0)a), requiring more in-depth analysis concerning bacteria as an  $N_2O$  sink at a low  $N_2O$ concentration. Some clade II-type nosZ bacteria appear to lack genes encoding for NIR and/or NOR, suggesting their potential as an  $N_2O$  sink but not an  $N_2O$  source (Graf et al. [2014](#page-11-0)). As reviewed elsewhere, these non-denitrifying  $N<sub>2</sub>O$ -reducing bacteria in wastewater engineering are yet to be explored in detail (Hallin et al. [2018\)](#page-11-0). The ecophysiology of non-denitrifying  $N<sub>2</sub>O$  reducers in a biofilm system warrants further research.

There are a wide range of denitrifying microorganisms and some with special behavior with respect to  $N_2O$  formation and reduction. Some can fully reduce  $NO_3^-$  and  $NO<sub>2</sub><sup>-</sup>$  to  $NH<sub>3</sub>$  in an ecologically important process called dissimilatory nitrate or nitrite reduction to ammonium (DNRA) (Stein and Klotz [2016\)](#page-13-0) (Fig. [2\)](#page-2-0). In this process,  $NO_3^-$  or  $NO_2^-$  is reduced to  $NH_3$ , with  $N_2O$  produced at the  $NO_2^ NO_2^ NO_2^-$  reduction stage as a by-product (Fig. 2) (Kelso et al. [1997](#page-11-0); Rutting et al. [2011](#page-13-0); Streminska et al. [2012](#page-13-0)). Unlike denitrification, this process conserves N in the ecosystem (Rutting et al. [2011](#page-13-0); Tiedje et al. [1982\)](#page-14-0). Many DNRA microorganisms can produce  $N_2O$  as a by-product (Stevens and Laughlin [1998;](#page-13-0) Stevens et al. [1998\)](#page-13-0). Some of these microorganisms employ DNRA as a detoxification mechanism in order to avoid high concentration of  $NO_2$ <sup>-</sup> (Kaspar [1982\)](#page-11-0). However, the actual contribution of DNRA to  $N_2O$  formation in these species remains uncertain (Butterbach-Bahl et al. [2013\)](#page-10-0).

Behavior regarding  $N<sub>2</sub>O$  emissions may also vary based on the type of electron donor. For example, elemental-sulfur (S°)oxidizing denitrifiers (Di Capua et al. [2015](#page-10-0); Liu et al. [2017b\)](#page-12-0), methane  $(CH_4)$ -oxidizing denitrifiers (He et al. [2018](#page-11-0)), phosphate-accumulating (PAO) denitrifiers (Gao et al. [2017;](#page-11-0) Wang et al.  $2011$ ,  $2014$ ; Zhou et al.  $2012$ ),  $H_2$ -oxidizing denitrifiers (Li et al. [2017\)](#page-12-0), and bacteria growing with an electrode as an electron donor (Jiang et al. [2018](#page-11-0)) display different behaviors with respect to  $N_2O$  emissions. Methane-oxidizing denitrifiers appear to reduce  $NO_2^-$  to  $N_2$  without forming  $N_2O$ as an intermediate and therefore are thought to minimize  $N_2O$ emissions (He et al. [2018\)](#page-11-0). While the details on each of these donors are beyond the scope of this review, the kinetics for each donor can have important impacts on  $N<sub>2</sub>O$  formation and consumption.

## Types of biofilm reactors and impacts on  $N_2O$ emissions

This section describes different types of biofilm reactors and their special characteristics as relate to  $N_2O$  emissions. Based on the analysis in the previous section, and also following Todt & Dorsch [\(2016](#page-14-0)) and Massara et al. ([2017](#page-12-0)), conditions that promote  $N_2O$  emission include (1) low DO values, or DO spatially transitioning from high to low within the biofilm, as this leads to nitrifier denitrification or incomplete heterotrophic denitrification; (2) conditions where the DO fluctuates temporally from high to low values, (3) conditions with high reaction rates, which lead to greater formation of intermediates (e.g., NH<sub>2</sub>OH, NO<sub>2</sub><sup>-</sup>) that promote N<sub>2</sub>O formation; and (4) limiting electron donor for denitrification.

The above factors may have different impacts for different types of biofilm reactors. There is a wide range of biofilm reactors, and they can be classified based on the arrangement of their solid, liquid, and gas phases, whether the carriers are fixed or moving, their carrier specific surface area (area of carrier per unit volume of reactor), their mixing regime (completely mixed or plug flow), and the mechanisms of transfer of gases and electron donor or acceptor substrates. Typical biofilm reactor configurations are shown schematically in Fig. [4](#page-5-0).

Trickling filters (Fig. [4](#page-5-0)a) are commonly used for COD removal and nitrification. The media is non-submerged and is kept aerobic by convective air currents within the bed. While considered aerobic, anoxic niches can form in the deeper biofilm (Dalsgaard and Revsbech [1992\)](#page-10-0). The variations in DO and donor concentration in the biofilm between passes of the wastewater distributor arm can lead to  $N<sub>2</sub>O$ emissions. When used for nitrification,  $N_2O$  is likely to form within the bed, with some stripped by the air currents and present in the effluent (Melse and Mosquera [2014\)](#page-12-0). There is little experimental data on  $N_2O$  emissions from trickling

<span id="page-5-0"></span>Fig. 4 Types of biofilm reactors. a Unsubmerged filter (e.g., trickling filter or biofilter), b upflow fixedbed reactor (e.g., biologically active filter (BAF), c downflow fixed-bed reactor (e.g., BAF), d rotating biological contactor (RBC), e suspended or airlift biofilm reactor, f fluidized-bed biofilm reactor (FBBR or granular sludge), g moving-bed biofilm reactor (MBBR), integrated fixed film activated sludge (IFAS), and h membrane-supported biofilm reactor (e.g., MBfR or MABR). Note:  $i =$  influent;  $e =$  effluent;  $r =$ recycle;  $w =$  wasting flow;  $g =$  gas flow (typically air) in or out. Black dots in panels e, f, and g are biofilm carriers. Adapted from (Morgenroth [2008\)](#page-12-0) and (WEF [2010](#page-14-0))



filters, possibly due to the difficulty in capturing the off-gases, and further research is needed in this area.

Biofilters (Fig. 4a) are similar to trickling filters, but used to treat gaseous contaminants such as odorous compounds in air or volatile organic compounds (VOCs). Air is passed through a non-submerged packed bed with biofilms growing on the media, and the contaminants partition into the liquid phase coating the biofilm. Yoon et al.  $(2017)$  proposed using a biofilter supplied to remove  $N_2O$  in off gases from an activated sludge aeration basin. Raw wastewater was used as the electron donor. In lab tests, 99.9% of  $N_2O$  was removed when supplied at 100 ppmV in  $N_2$ , i.e., without any  $O_2$ . However, removals decreased significantly when supplied in air. Biofilters are likely an expensive approach to mitigating N2O emissions, as they require covering aeration basin to collect off gases, treating large volumes of gas, and adding an additional process and complexity to the treatment train.

Packed bed reactors (Fig. 4b, c) are fully submerged fixed bed biofilm reactors. They can be operated in upflow or downflow mode and either aerated (e.g., for nitrification) or unaerated with electron donor addition (denitrifying filters). Upflow packed bed reactors, such as nitrifying or denitrifying filters, typically operate in plug flow fashion. Thus, the filters experience high substrate concentrations at the influent end and low concentrations at the effluent end. The concentration gradients (e.g., high  $NH<sub>3</sub>$  at influent, low DO at effluent) can impact  $N_2O$  formation processes. When used for denitrification, air pulses are periodically performed at the bottom of the filter to release  $N_2$  bubbles accumulating in the reactor. These pulses can strip  $N_2O$  formed at the beginning of the bed, when normally it would be reduced to  $N<sub>2</sub>$  further within the bed (Bollon et al. [2016\)](#page-10-0). Whenever air is added to a denitrifying filter, there is potential for  $N_2O$  formation at some location within the biofilm due to the greater sensitivity of  $N_2OR$  to  $O_2$  inhibition.  $N<sub>2</sub>O$  may also accumulate due to insufficient electron donor supply. For nitrifying and denitrifying packed bed reactors, backwashing is carried out regularly to remove excess biomass. Thinner biofilms may not allow full treatment, leading  $N_2O$  breakthrough from the reactor. For denitrifying biofilms, breakthrough can also be caused by donor limitation. Bollon et al. ([2016](#page-10-0)) found that a full-scale denitrifying filter with a C/N of 3 or higher had up to 93% N2O reduction. However, during a carbon supply failure, removals lowered 26%. Similar results were found by Capodici et al. [\(2018](#page-10-0)) and Zhang et al. [\(2016\)](#page-14-0). In the latter study, the authors found that a decrease of the C/N from 3 to 0.65 led to an increase of the genes encoding for NOR that would enhance the transformation of NO to  $N_2O$  and lead to increased  $N_2O$  emissions. Zhang et al. [\(2017\)](#page-14-0) studied the behavior of lab-scale denitrification filters and found a complex interaction of the denitrification with anammox and DNRA. Gene abundance together with accumulation of  $NO_2^-$  at temperatures between 5 and 15  $\degree$ C were found to be important factors for N<sub>2</sub>O accumulation. Further research is required to investigate the impact of influent  $NO_2^-$  and possible adaptation of bacteria to variable influent loadings of both  $NO_2^-$  and  $NO_3^-$  in denitrifying filters.

RBCs (Fig. [4d](#page-5-0)) use rotating wheels of media partially submerged in wastewater. When the wheels are outside the water, the biofilm can experience  $O_2$  concentrations in the biofilm exterior, while the DO concentrations can drop significantly when immersed in the wastewater (Pynaert et al. [2002\)](#page-13-0). This cycling of high and low DO concentrations, as well variations in donor concentration when the biofilm is submerged vs. when it is out of the wastewater, can potentially lead to higher  $N_2O$  emissions. There does not appear to be any published findings of  $N_2O$  emissions from RBCs. Note that RBCs are often covered to prevent from UV toxicity and to protect from low temperatures in winter. In these cases, it may be possible to pump air from the enclosures through an anoxic zone or into a biofilter, such as that described above, to reduce  $N_2O$  to  $N_2$ .

Airlift, MBBRs, and IFAS (Fig. [4e](#page-5-0), g) use carriers that "float" in the water and therefore have little relative velocity between the carrier and the water. They can be operated under aerobic or anoxic conditions. In continuous systems, the biofilm carriers are kept in a single zone, experiencing consistent bulk environments. This can avoid the high  $N<sub>2</sub>O$  emissions in suspended growth systems transitioning from anoxic to aero-bic zones (Chandran et al. [2011](#page-10-0)). Recent research on  $N_2O$ emissions from MBBRs are consistent with the factors described at the beginning of this section, depending on the application (Mannina et al. [2017,](#page-12-0) [2018a,](#page-12-0) [b;](#page-12-0) Wei et al. [2017](#page-14-0)).

Fluidized bed reactors (Fig. [4](#page-5-0)f) behave similarly to a BAF, but use much finer media. This provides a high specific surface area and allows the particles to become suspended in the upward wastewater flow. These reactors also experience a somewhat higher degree of mixing, compared to packed bed reactors, but still have some plug flow behavior. Excess biofilm is continuously removed by abrasion, and biofilms typically are thinner than in BAFs. The behavior with respect to  $N<sub>2</sub>O$  emissions should be similar to the BAFs. Note that aerobic granular sludge can behave similarly to a fluidized bed reactor. However, granular sludge is typically operated in sequencing batch mode (Castro-Barros et al. [2015](#page-10-0)). Recent research on  $N<sub>2</sub>O$  emission from granular sludge also confirms the above mechanisms (Jia et al. [2018](#page-11-0); Lu et al. [2018;](#page-12-0) Peng et al. [2017](#page-13-0); Reino et al. [2017](#page-13-0)).

Counter-diffusional biofilms are those where one substrate diffuses from the bulk liquid, while the other penetrates the biofilm from the attachment surface. The counter-diffusion of substrates leads to a range of different behaviors with respect to conventional, co-diffusional biofilms (Nerenberg [2016](#page-12-0)). Examples of counter-diffusional biofilms include MABRs, where the membranes are used to supply air or  $O_2$ ; membrane-biofilm reactors (MBfRs) where membranes supply  $H_2$  or CH<sub>4</sub> (Liu et al. [2017b](#page-12-0)); sulfur-based biofilms, where solid  $S<sup>o</sup>$  particles support a biofilm (Wang et al. [2016a](#page-14-0)); and even bioelectrochemical biofilms (Jiang et al. [2018\)](#page-11-0). MABR behavior is discussed in more detail in the next section.

# Mechanisms of N<sub>2</sub>O formation in biofilm processes for wastewaster treatment

Because of their special layered structure and organization, biofilms allow unique niche formation with specific metabolic functions. In addition, intermediates formed in one biofilm location can diffuse to another with different environments, leading to transformations that would not normally occur in a suspended growth system (Dalsgaard et al. [1995](#page-10-0); de Beer et al. [1997;](#page-10-0) Nielsen et al. [1990;](#page-12-0) Sabba et al. [2017b;](#page-13-0) Schreiber et al. [2009\)](#page-13-0). This section discusses basic behavior of biofilms for some key processes, including nitrification, denitrification, combined nitrification and denitrification, and partial nitrification/anammox. The behavior is common for most biofilm reactors except for MABRs, which are described separately. The figures in this section are intended to illustrate typical behavior. They are only schematics, not meant to reflect an actual operating condition.

#### Nitrifying biofilms

Nitrifying biofilms form when  $NH<sub>3</sub>$  is the dominant or sole electron donor. While AOB and NOB are primary population members in nitrifying biofilms, heterotrophic bacteria typically co-exist (Kindaichi et al. [2004](#page-11-0)), growing on the decay products from nitrifying microorganisms (Gieseke et al. [2005;](#page-11-0) Okabe et al.  $2005$ ). However, N<sub>2</sub>O production in nitrifying biofilms is likely dominated by AOB, with a minor contribution from heterotrophic bacteria. In this section, we focus on the mechanisms of  $N<sub>2</sub>O$  from the nitrifying population. In the subsequent section, we discuss the impact of heterotrophs on nitrifying biofilms, especially when organic carbon is present in the bulk.

Typical substrate profiles in nitrifying biofilms and zones of  $N<sub>2</sub>O$  formation and emission are shown schematically in Fig. [5.](#page-7-0) In conventional, co-diffusional biofilms, the outer biofilm is aerobic and has the highest  $NH<sub>3</sub>$  concentrations. As a result, the  $NH<sub>3</sub>$  oxidation rates are high, leading to high  $NH<sub>2</sub>OH$  concentrations. In addition, the nitrifier denitrification pathway is inhibited by the high DO in this zone. Thus, the  $NH<sub>2</sub>OH$  oxidation pathway is likely to dominate, and  $N<sub>2</sub>O$  formation rates are likely to be relatively low. Nitrifier denitrification may become significant in the aerobic/anoxic transition zone (Mao et al. [2008;](#page-12-0) Schreiber et al. [2008,](#page-13-0) [2009](#page-13-0)). In the anoxic zone,  $N<sub>2</sub>O$  formation rates are low. This is because  $NH<sub>3</sub>$  oxidation, which is the source of electrons for nitrifier denitrification, requires  $O_2$ . However, Sabba et al. ([2015](#page-13-0)) proposed that NH<sub>2</sub>OH formed in the aerobic biofilm exterior would diffuse to the interior anoxic zones. AOB in this zone could utilize  $NH<sub>2</sub>OH$  as a rich electron source, enabling the nitrifier denitrification pathway and resulting in a spike of  $N<sub>2</sub>O$ . Further research is needed to confirm this mechanism <span id="page-7-0"></span>Fig. 5  $N_2O$  formation in nitrifying biofilms. a Codiffusional and b counterdiffusional. Solid black arrow indicates  $N<sub>2</sub>O$  loss towards either bulk or membrane lumen.  $NO_2$ <sup>-</sup> and NO are not shown for clarity



experimentally. In Fig. 5, the  $N_2O$  concentration profile slopes towards the outer biofilm, indicating diffusive mass transfer towards the bulk. If diffused aeration is used, the  $N<sub>2</sub>O$  is readily stripped from the liquid phase (Law et al. [2012](#page-12-0); Rassamee et al. [2011;](#page-13-0) Wu et al. [2014](#page-14-0)).

MABRs are a novel biofilm process for wastewater treatment, where  $O_2$  is supplied from the membrane and NH<sub>3</sub> from the bulk (Martin and Nerenberg [2012](#page-12-0); Syron and Casey [2008\)](#page-13-0) (Fig. 5). Because of the unique penetration of  $NH_3$  and  $O_2$ from opposite sides of the biofilm, they are called, as mentioned above, counter-diffusional biofilms (Nerenberg [2016\)](#page-12-0). N2O can also occur in MABRs systems. In MABs, the highest nitrification rates usually occur in the biofilm interior, not at the outer edge. Thus,  $N_2O$  formation via the  $NH<sub>2</sub>OH$  pathway is likely to occur in the deep biofilm. In addition, the aerobic/ anoxic transition occurs in the biofilm interior, and the bulk is anoxic. Thus, while  $N_2O$  can be stripped from suspended growth systems by bulk aeration (Law et al. [2012;](#page-12-0) Rassamee et al. [2011;](#page-13-0) Wu et al. [2014](#page-14-0)), N<sub>2</sub>O in MABRs can be consumed by denitrifying bacteria in the outer biofilm or bulk liquid. Conversely, some  $N_2O$  may be stripped from MABR biofilms by air flowing through the membrane lumen, if operated with open end membranes (Kinh et al. [2017a](#page-11-0)). Stripping from the lumen is indicated in Fig. 5b by the slope of the  $N_2O$  concentration profile towards the membrane in its proximity.

NOB can contribute indirectly to  $N_2O$  emissions by scavenging DO and favoring the formation of a steeper gradient for transitioning from oxic to anoxic conditions (Sabba et al. [2015](#page-13-0), [2017a](#page-13-0)). They also can play a key role in reducing the  $NO_2^-$  concentration, which reduces the rates of nitrifier denitrification (Schreiber et al. [2009](#page-13-0)). Anammox bacteria can play a similar role in decreasing N2O emissions (Pellicer-Nacher et al. [2010\)](#page-13-0). As mentioned previously, NOB do not play a direct role for NO and  $N_2O$ emissions, but may affect emission by modifying the  $NO_2^$ concentrations (Wang et al. [2016b](#page-14-0)).

#### Denitrifying biofilms

Denitrifying biofilms are those where  $NO<sub>3</sub><sup>-</sup>$  is the primary electron acceptor. We also consider biofilms with an aerobic exterior and denitrifying interior, but neglect any nitrification in the aerobic zone. In denitrifying biofilms,  $N_2O$  is an obligate intermediate. It is typically present at higher concentrations in the outer biofilm region, where  $NO_3^-$  and  $NO_2^-$  reduction activity is higher, but can diffuse and be consumed in deeper regions where  $NO_3^-$  and  $NO_2^-$  concentrations are lower (Fig. [6a](#page-8-0)). Thus, biofilms can have regions that can serve as an  $N_2O$  sink, mitigating  $N_2O$  emissions (Dalsgaard and Revsbech [1992](#page-10-0); Nielsen et al. [1990\)](#page-12-0).

In the presence of high DO, denitrification is usually inhibited and therefore little  $N_2O$  is formed (Conte et al. [2018](#page-10-0)b) (Fig. [6b](#page-8-0)). However, biofilms typically have DO gradients, and denitrification and  $N_2O$  formation may occur deeper in the biofilm (Dalsgaard and Revsbech [1992](#page-10-0); Nielsen et al. [1990\)](#page-12-0). In the transition zone from oxic to anoxic, higher amounts of  $N_2$ O will be formed due to the higher sensitivity of NOS to  $O_2$ inhibition (Bonin et al. [1992;](#page-10-0) Lu and Chandran [2010;](#page-12-0) Morley et al. [2008](#page-12-0); Otte et al. [1996\)](#page-12-0). When this transition zone is near the outer biofilms, more  $N_2O$  may be exported to the bulk liquid. When the transition occurs deeper in the biofilm, i.e., at higher bulk DO concentrations, and when electron donor is sufficient,  $N<sub>2</sub>O$  is more likely to be reduced in the deeper biofilm and less emissions will occur (Dalsgaard and Revsbech [1992\)](#page-10-0).

If  $N_2O$  is formed in the outer biofilm and if sufficient electron donor is available in the deeper zones of the biofilm, denitrifying biofilms can serve as an  $N_2O$  sink (Eldyasti et al. [2014;](#page-11-0) Sabba et al. [2017b](#page-13-0)). However, if sulfate reduction occurs in the deeper biofilm where  $NO<sub>3</sub><sup>-</sup>$  has been depleted,  $H_2S$  may accumulate and inhibit N<sub>2</sub>O reduction (Pan et al. [2013b\)](#page-12-0). Electron donor limitation in the denitrifying zone also may result in greater  $N<sub>2</sub>O$  formation (Dalsgaard and Revsbech [1992;](#page-10-0) Nielsen et al. [1990](#page-12-0); Todt and Dorsch [2015\)](#page-14-0) (Fig. [6c](#page-8-0)).

<span id="page-8-0"></span>Fig. 6  $N<sub>2</sub>O$  formation in denitrifying biofilms. a Excess e<sup>−</sup> donor, **b** excess  $e^-$  donor with  $O_2$ , and c limiting e<sup>−</sup> donor. Solid black arrow indicates  $N<sub>2</sub>O$  loss towards bulk and dashed black arrow indicates reduction within the biofilm depth.  $NO_2^-$  and NO are not shown for clarity



### Combined nitrifying/denitrifying biofilms

Biofilms exposed to both organic carbon and  $NH_3$  usually have an outer layer dominated by fast-growing heterotrophic bacteria (Henze et al. [2008\)](#page-11-0). In the presence of non-limiting organic substrates,  $O_2$  is usually consumed by heterotrophic activity with little formation nitrifying biomass. However, in presence of low or transient organic carbon concentrations, nitrifying organisms can develop in the biofilm. These biofilms are here referred as "combined nitrifying/denitrifying biofilms."

In combined nitrifying/denitrifying biofilms, the mechanisms of  $N_2O$  formation can be quite complex. Both co- and counter-diffusional combined nitrifying/denitrifying biofilms are characterized by the presence of complex communities, where  $N<sub>2</sub>O$  not only is formed by both nitrifiers and denitrifiers but also reduced by denitrifiers (Matsumoto et al. [2007](#page-12-0); Nerenberg [2016](#page-12-0)). Various intermediates play roles in both pathways, as indicated in Fig. [2](#page-2-0). For example,  $NO_2^-$  and NO, two crucial components of both nitrifier denitrification and  $NH<sub>2</sub>OH$  oxidation pathways, also play a role as intermediates in the denitrification pathway (Todt and Dorsch [2015\)](#page-14-0).

Thickness is also a crucial component for both co- and counter-diffusional biofilm, if adequate thickness and COD concentrations are present, then  $N_2O$  reduction can occur (Eldyasti et al. [2014;](#page-11-0) He et al. [2017\)](#page-11-0).

Co-diffusional combined nitrifying/denitrifying biofilms receive both electron donor and acceptor from the bulk (Fig. 7a). In this type of biofilm, heterotroph are typically more abundant in the outer biofilm, due to their faster growth rates and the greater availability of COD. This zone is typically aerobic, so little or no denitrification or  $N<sub>2</sub>O$  reduction occurs. Nitrifiers are typically located in the aerobic zone below the heterotrophs. If enough COD is present, then  $N_2O$ reduction can occur in the deeper biofilm (Fig. 7a) (Chae et al. [2012;](#page-10-0) Eldyasti et al. [2014;](#page-11-0) He et al. [2017\)](#page-11-0). When the bulk is aerated in co-diffusional combined nitrifying/ denitrifying biofilms, there is greater  $N_2O$  mass transfer towards the bulk rather than towards the anoxic zone where it can be reduced. This translates in higher  $N<sub>2</sub>O$  emissions.

In counter-diffusional combined nitrifying/denitrifying biofilms, DO penetrates the biofilm from the attachment surface. In this case, and assuming the bulk liquid is anoxic, the

Fig. 7  $N<sub>2</sub>O$  formation in combined nitrifying/denitrifying biofilms. a Co-diffusional and b counter-diffusional. Solid black arrow indicates  $N_2O$  loss towards either bulk or membrane lumen; dashed black arrow indicates reduction within the biofilm depth.  $NO_2^-$  and NO are not shown for clarity



nitrifiers would only be active near the membrane surface (Kinh et al.  $2017a$ ). In addition, N<sub>2</sub>O formed by the nitrifiers could potentially be reduced by the heterotrophs in outer, anoxic region of the biofilm, where the COD concentrations are highest (Cole et al. [2004](#page-10-0); Kinh et al. [2017b;](#page-11-0) LaPara et al. [2006\)](#page-12-0). As seen for nitrifying biofilms (Fig. [5b](#page-7-0)), there could also be  $N_2O$ stripping by the membrane, as indicated from a negative slope of the  $N_2O$  profile towards the membrane (Fig. [7](#page-8-0)b). The lack of bulk aeration reduces  $N<sub>2</sub>O$  mass transfer to the bulk. Note that MABR membranes can also strip  $CO<sub>2</sub>$  from the biofilm, leading to pH shifts that can impact the microbial community and potentially impact  $N_2O$  emissions (Ma et al. [2017b\)](#page-12-0).

Based on the above, the type of biofilm (co- vs. counterdiffusional) also can affect the microbial community structure and therefore the  $N_2O$  emissions. For each bulk substrate condition and detachment regime, there may be a different microbial community structure, which in turn can affect the formation/reduction and emissions of  $N_2O$ . Therefore, the behavior of these biofilms is complex and hard to predict (Martin and Nerenberg [2012;](#page-12-0) Nerenberg [2016\)](#page-12-0).

#### Partial nitritation/anammox biofilms

In combined partial nitritation/anammox (PN/A) reactors,  $NH_3$  is partially oxidized to  $NO_2^-$  by AOB. The remainder of the NH<sub>3</sub> is then oxidized to N<sub>2</sub> gas via NO<sub>2</sub><sup> $-$ </sup> reduction by anammox bacteria. NOB are undesirable in PN/A reactors, and diverse strategies are employed to outselect these organisms. PN/A reactors typically also harbor a diverse flanking community, many of which are capable of heterotrophic denitrification (Lawson et al. [2017](#page-12-0)).

A distinguishing feature of PN/A systems is the presence of multiple biological sinks for  $NO_2^-$ . Biofilm-based PN/A systems are further distinguished by strong spatial segregation of AOB (in oxic layers) and anammox and denitrifiers (in anoxic, usually deep, layers) (Hubaux et al. [2015;](#page-11-0) Laureni et al. [2016;](#page-12-0) Okabe et al. [2011\)](#page-12-0). Crossfeeding within the biofilm and capacity of certain denitrifiers to act as internal  $N_2O$  sinks likely differentiates  $N_2O$  emissions in biofilms from suspended growth PN/A processes.

The potential of PN/A systems to act as significant  $N_2O$ sources, particularly from biofilm or hybrid PN/A reactors, is poorly understood. Results suggest that emissions depend strongly on bulk  $O_2$  concentration (Harris et al. [2015\)](#page-11-0),  $\overline{NO_2}^{-}$ concentration (Van Hulle et al.  $2012$ ), NH<sub>3</sub> oxidation activity (Blum et al. [2018a;](#page-10-0) Domingo-Felez et al. [2014](#page-10-0)), nitrogen loading (Yang et al. [2016\)](#page-14-0), aeration regime (intermittent vs. continuous aeration) (Blum et al. [2018a;](#page-10-0) Domingo-Felez et al. [2014](#page-10-0); Kampschreur et al. [2008](#page-11-0); Ma [2018](#page-12-0)), presence of organic matter (Jia et al. [2018](#page-11-0)), and biofilm thickness (Vlaeminck et al. [2010\)](#page-14-0).

Intermittent aeration mirrors conditions recently shown to promote N<sub>2</sub>O generation (Chandran et al. [2011;](#page-10-0) Kampschreur et al. [2008](#page-11-0), [2009;](#page-11-0) Yu et al. [2010](#page-14-0)), but has also been suggested

that appropriate intermittent aeration can facilitate control or minimization of  $N_2O$  emissions from PN/A processes (Castro-Barros et al. [2015;](#page-10-0) Domingo-Felez et al. [2014;](#page-10-0) Su et al. [2017\)](#page-13-0).

While sources of  $N_2O$  in PN/A systems are still not well understood, multiple studies have indicated it may derive predominantly from AOB. Ali et al. [\(2016\)](#page-10-0) provided evidence based that nitrifier denitrification and  $NH<sub>2</sub>OH$  pathways were equally important to  $N<sub>2</sub>O$  formation in the oxic surface region of granules from a PN/A reactor. However,  $\sim 30\%$  of N<sub>2</sub>O emissions in this system could be attributed to the anammox dominated anoxic interior of granules due to either heterotrophic denitrification or a yet unidentified pathway. Harris et al. [\(2015\)](#page-11-0) showed that  $N_2O$  site preference data from a suspended growth PN/A reactor was inconsistent with current understanding of  $N_2O$  production pathways and further suggested that  $N<sub>2</sub>O$  emissions in this system could be due in part to an unknown inorganic or anammox-associated  $N<sub>2</sub>O$  production pathway. In general, biofilm-based PN/A processes appear to emit less  $N<sub>2</sub>O$  than suspended nitrifying processes (Gilmore et al. [2013](#page-11-0)). Further research is needed to better identify sources of  $N<sub>2</sub>O$  in biofilm-based and hybrid biofilm suspended growth PN/A systems and to quantitatively evaluate how spatial structuring, biofilm thickness, and aggregate architecture influence  $N<sub>2</sub>O$  emissions in these emerging low energy N removal systems.

### Conclusions

 $N<sub>2</sub>O$  formation is promoted when there are (1) low DO values, or DO spatially transitioning from high to low within the biofilm; (2) conditions where the DO fluctuates temporally from high to low values; (3) conditions with high reaction rates, which lead to greater formation of intermediates (e.g.,  $NH<sub>2</sub>OH$  and  $NO<sub>2</sub><sup>-</sup>$ ) that promote  $N<sub>2</sub>O$  formation; and (4) limiting electron donor for denitrification. The microbial basis of  $N<sub>2</sub>O$  formation in biofilms and suspended growth systems are similar, yet  $N_2O$  emissions in biofilm systems depend greatly on microbial stratification, the formation of substrate gradients, the exchange of intermediates within the biofilm, and the type of biofilm reactor. This can lead to different patterns and quantities of  $N_2O$  emission for the same bulk environment and make it more difficult to predict  $N_2O$  emissions. Codiffusional and membrane-aerated biofilms may have substantially different behavior, due to the unique microbial and stratifications and substrate profiles. In order to predict  $N_2O$  emissions from biofilm processes and develop strategies to minimize them, it is important to understand the microbiological and biochemical basis for  $N<sub>2</sub>O$  formation, the factors affecting  $N<sub>2</sub>O$  formation in biofilms, as well as the impacts of reactor configurations and operating modes. Future research should address the pathways and kinetics of  $N_2O$  emissions from AOA, comammox bacteria, methane-oxidizing denitrifying

<span id="page-10-0"></span>bacteria, and others. It also is important to explore their abundance in biofilms. Given the complexity of biofilms and biofilm processes, empirical assessments of  $N<sub>2</sub>O$  emissions from the broad range of biofilm reactors type and operating conditions is needed, and application-specific recommendations to minimize emissions should be developed.

Funding information This study was funded by the Water Environment Research Foundation (grant U2R10), the USA National Science Foundation (grant CBET0954918), the Japanese Society for the Promotion of Science (grant 17H01893), and the Danish Council for Independent (Project N2OMan, File No. 1335-00100B). F.S. and R.N. were partially supported by NSF project CBET0954918 and WERF project U2R10. A.T. was partially funded by Grant-in-Aid for Scientific Research (17H01893)—Japan Society for the Promotion of Science and BFSM was funded by the DFF project N2OMan.

### Compliance with ethical standards

Conflict of interest F. Sabba declares he has no conflict of interest.

- A. Terada declares he has no conflict of interest.
- G. Wells declares he has no conflict of interest.
- B. F. Smets declares he has no conflict of interest.
- R. Nerenberg declares he has no conflict of interest.

Ethical approval This article does not contain any studies with human participants or animals performed by any of the authors.

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