BIOTECHNOLOGICAL PRODUCTS AND PROCESS ENGINEERING

## Efficient production of enantiomerically pure D-phenyllactate from phenylpyruvate by structure-guided design of an engineered D-lactate dehydrogenase

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Abstract 3-Phenyllactic acid (PLA) is an antimicrobial compound with broad-spectrum activity against bacteria and fungi that could be widely used in the food industry and livestock feeds. Notably, D-PLA exhibits higher antibacterial activity, which gains more attention than L-PLA. In this report, the Dlactate dehydrogenase DLDH744 from Sporolactobacillus inulinus CASD was engineered to increase the enzymatic activities toward phenylpyruvate by protein structure-guided modeling analysis. The phenylpyruvate molecule was first docked in the active center of DLDH744. The residues that might tightly pack around the benzene ring of phenylpyruvate were all selected for mutation. The single site mutant M307L showed the highest increased activity toward bulkier substrate phenylpyruvate than the wild type. By using the engineered Dlactate dehydrogenase M307L expressed in Escherichia coli strains, without coexpression of the cofactor regeneration system, 21.43 g/L D-PLA was produced from phenylpyruvate with a productivity of 1.58 g/L/h in the fed-batch biotransformation process, which ranked in the list as the highest production titer of D-PLA by D-lactate dehydrogenase. The

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enantiomeric excess value of produced D-PLA in the broth was higher than 99.7 %. Additionally, the structure-guided design of this enzyme will also provide referential information for further engineering other 2-hydroxyacid dehydrogenases, which are useful for a wide range of fine chemical synthesis.

**Keywords** Optical purity · D-Phenyllactate · Protein engineering · D-Lactate dehydrogenase

### Introduction

3-Phenyllactic acid (PLA) is a broad-spectrum antimicrobial compound, which has been shown to inhibit the growth of a wide range of species, including yeasts and gram-negative and gram-positive bacteria (Lavermicocca et al. 2000, 2003; Schwenninger et al. 2008; Dieuleveux et al. 1998a; Ohhira et al. 2004). PLA has a low molecular mass and is hydrophilic, for which it diffuses into food and feed more easily (Dieuleveux et al. 1998a). Therefore, PLA has interesting potential as an antimicrobial agent in the food industry. The ability of PLA to act as a fungicide provides new perspectives for the possibility of using this natural antimicrobial compound to control fungal contaminants and extend the shelf life of food- and/or feedstuffs. Between the two optical isomers, D-PLA shows the higher antibacterial activity than L-PLA (Dieuleveux et al. 1998a). Furthermore, PLA is a promising building block for bio-based materials, as PLA can be polymerized into the biopolymer poly-PLA (Fujita et al. 2013). Unlike polylactic acid, poly-PLA exhibits high ultravioletabsorbing properties due to the bulky aromatic side chain (Fujita et al. 2013).

Promising applications of PLA stimulated great endeavors in the development of synthesis strategies. PLA production has been reported in some studies with a variety of bacteria,



including Lactobacillus, Leuconostoc, Bacillus, Weissella, Pediococcus, Aspergillus, and Geotrichum (Dieuleveux et al. 1998b; Valerio et al. 2004; Mu et al. 2009, 2012; Ndagano et al. 2011; Zheng et al. 2011). In the catabolism of lactic acid bacteria, phenylpyruvic acid (PPA) is converted to PLA by the lactate dehydrogenase (LDH). Therefore, several literatures reported the transformation of PPA to PLA by high expression of the native or site-mutated LDHs in Escherichia coli strains to enhance the productivity. However, to date, the production titer is not satisfactory, probably due to the low activity toward bulkier substrates such as PPA since normally the native activity of LDH toward PPA was much lower than that for pyruvate (Zheng et al. 2013; Li et al. 2014; Yu et al. 2014). DLDH744 is a novel p-lactate dehydrogenase recently identified from Sporolactobacillus inulinus. The complete tertiary structure revealed that the active center of DLDH744 is larger than that of the other reported LDHs (Zhu et al. 2015a). The enzyme was also confirmed to have D-phenyllactate dehydrogenase activity. And it is notable that the  $K_{\rm m}$  values for pyruvate and PPA were determined to be  $3.4 \pm 0.02$  mM and 3.3 $\pm 0.08$  mM, respectively, which indicates that DLDH744 have the same affinity for PPA with pyruvate (Zhu et al. 2015b). All the above results demonstrate that DLDH744 may have advantage in facilitating the production of D-PLA.

In this study, the DLDH744 was first engineered to increase the enzymatic activities toward PPA by protein structure-guided modeling analysis. The transformation process was fully optimized, and the high titer and optical purity of D-PLA were achieved. Thus, this study suggested a promising alternative for the production of chiral D-PLA from PPA.

#### Materials and methods

#### Bacterial strains and plasmids

The gene of D-lactate dehydrogenase (DLDH744) from *S. inulinus* CASD was cloned from the genome (Yu et al. 2011). *E. coli* DH5 $\alpha$  (Tiangen, Beijing, China) was used for gene cloning, and *E. coli* JM109 (DE3) (Dingguo, Beijing, China) was used for protein expression. Plasmids pMD 19-T (Takara, Dalian, China) and pET-28a (Novagen) were used as cloning and expression vectors, respectively.

# Gene cloning, plasmid construction, protein expression, and purification

The cloning of DLDH744 gene and construction of recombinant plasmid pET-28a-DLDH744 were processed as described in our previous work (Zhu et al. 2015a). The recombinant plasmid was transformed into *E. coli* JM109 (DE3) for protein expression. The protein expression, purification, and desalination were performed as previous works (Zhu et al. 2015b). Protein concentration was determined by the Bradford method using bovine serum albumin as a standard (Bradford 1976).

### Enzyme assays

The enzyme activity was assayed at 30 °C in 400  $\mu$ l of 100 mM PBS (pH 5.5), 20 mM PPA or 10 mM pyruvate, 0.2 mM NADH, and the purified enzyme. The rate of NADH decrease was determined by measuring the absorbance change at 340 nm. One unit of enzyme activity was defined as the amount of enzyme that oxidates 1  $\mu$ mol NADH per minute. The specific enzyme activity was measured as units per milligram of protein (Wang et al. 2014).

#### Molecular docking and site-directed mutagenesis

The molecular docking was performed based on the X-ray crystal structure of DLDH744 from *S. inulinus* CASD (PDB number 4XKJ) by using software AutoDock (version 4.2.6) according to the reference (Morris et al. 1998). Site-directed mutagenesis was performed using pET-28a-DLDH744 as the template. The nucleotide sequences of primers used for mutagenesis are shown in Table 1. The mutant plasmids was constructed using high-fidelity Q5 DNA polymerase (New England Biolabs, Beijing, China) (Urban et al. 1997). The resultant plasmids were digested with the restriction enzyme DpnI (Takara, Dalian, China) at 37 °C for 2 h. *E. coli* JM109 (DE3) cells were transformed with these plasmids, and the resulting strains were termed as R9L, Q51A, Y101L, N268L, F298Y, and M307L, respectively.

Table 1 Primers used for site-directed mutagenesis of DLDH744

Primers	Sequences (5'-3')
R9L-F	CATTATGTTCAGCGTTC <u>TG</u> GATGATGAAGAGGCAG
R9L-R	CTGCCTCTTCATCATC <u>CA</u> GAACGCTGAACATAATG
Q51A-F	GACGGGATCGTGATT <u>GCA</u> CAGCGCAGCCACATC
Q51A-R	GATGTGGCTGCGCTG <u>TGC</u> AATCACGATCCCGTC
Y101L-F	CACCAATGTGCCGGCT <u>CTG</u> TCGCCGAACTCGGTTG
Y101L-R	CAACCGAGTTCGGCGA <u>CAG</u> AGCCGGCACATTGGTG
N268L-F	TGAGGAGCACTTCTTC <u>CTG</u> CAGGATCTGTGCGGCA
N268L-R	$TGCCGCACAGATCCTG\underline{CAG}GAAGAAGTGCTCCTCA$
F298Y-F	ACGCCGCATATTGGTTATTACACCAACAAAGCC
F298Y-R	GGCTTTGTTGGTGTA <u>AT</u> AACCAATATGCGGCGT
M307L-F	CAAAGCCGTGCAAAATCTGGTTGAGATCAGCCTG
M307L- R	CAGGCTGATCTCAACCA <u>G</u> ATTTTGCACGGCTTTG

The sites for mutation are all underlined

#### Effects of pH and glucose concentration on PLA yield

*E. coli* recombinant cells were cultured and induced as described above. The harvested induced cells were washed twice with 50 mM PBS (pH 7.0), then the cells were resuspended in 50 mM PBS containing 60 mM PPA at a final OD<sub>600</sub> of 60 and incubated at 30 °C for 2 h. The effects of pH on PLA production was determined by comparing the PLA yield in bioconversion process at various pH (5.5, 6.0, 6.5, 7.0, 7.5, 8.0, 8.5). To determine the initial glucose effect on bioconversion yield, PLA production was processed in an initial glucose concentration range of 0–12.5 g/L.

#### Biotransformation of PPA to PLA by E. coli whole cells

The fed-batch bioconversion was conducted with PPA substrate feeding to avoid substrate inhibition. The bioconversion was initiated in 50 mM PBS (pH 7.5) at an OD<sub>600</sub> of 80 containing 80 mM PPA and 5 g/L glucose at 30 °C; PPA was supplemented to maintain the initial concentration by one feeding. The fedbatch conversion was performed for 13.5 h. All experiments were performed in triplicate. The yield was calculated based on the produced PLA/added PPA (g/g, %).

#### Analytical methods

PLA and PPA were determined by using a high-performance liquid chromatography (HPLC) equipped with an Agilent Zorbax SB-C18 column  $(150 \times 4.6 \text{ mm}, 5 \mu \text{m})$  and a UV detector at 210 nm. The mobile phase was 1 mM H<sub>2</sub>SO<sub>4</sub> and acetonitrile with a ratio of 85:15 (*v*/*v*) at a flow rate of 0.7 ml/min at 30 °C. Glucose was measured with an SBA-40D glucose biosensor. D- or L-PLA was quantitatively measured by using HPLC with a chiral column (DAICEL CHIRALCEL OJ-RH) and a UV detector at 205 nm. The mobile phase was 0.1 % acetic acid and acetonitrile at a ratio of 90:10 (*v*/*v*), and the flow rate was 0.4 ml/min at 15 °C. The optical purity of PLA was defined as follows: D-PLA/(L-PLA+D-PLA)×100 %.

### Results

# Modeling of phenylpyruvate in the active center of DLDH744

For engineering the DLDH744 to further increase the activity, the substrate PPA molecule was first modeled in the active center of DLDH744 (Fig. 1). The orientation of PPA corresponds to the orientation of pyruvate in the structure of D-lactate dehydrogenase from *Aquifex aeolicus* (Antonyuk et al. 2009) and is sterically possible. In the structural model, the PPA carboxylate group binds



Fig. 1 Crystal structure of DLDH744 modeled with phenylpyruvate in the cofactor binding site.  $NAD^+$  is colored in *magenta* and shown in *sticks*. Phenylpyruvate is colored in *orange* and shown in *sticks*. Hydrogen bonds between residue and phenylpyruvate are shown in *dashed lines* 

the side chain of Thr77 and Tyr101 and the main-chain nitrogen atoms of Ala78. The substrate PPA molecule is oriented face-on and directly adjacent to the nicotinamide ring of the coenzyme; thus, hydride ion transfer can easily occur during catalysis. In a previous report, His295 polarize the carbonyl group of pyruvate, making it prone to receiving or donating a hydride ion. This residue also acts as an acid/base group by donating (or abstracting) a proton to the pyruvate carbonyl group or the lactate hydroxyl group. In the structural model, His295 also forms a hydrogen bond with the carbonyl group of PPA to ensure the enzyme reaction can proceed well. This is also the first report to model the PPA molecule in the LDH structure.



Fig. 2 Residues in the DLDH744 active center which are around the benzene ring of phenylpyruvate modeled in the protein structure.  $NAD^+$  is colored in *black* and shown in *sticks*. Phenylpyruvate is colored in *green* and shown in *sticks* 



Fig. 3 Relative enzymatic activities of wild type (WT) and mutants of DLDH744 for pyruvate and phenylpyruvate, respectively. The specific activity of wild type for pyruvate and PPA corresponding to the 100 % activity was  $4.91 \pm 0.172$  U/mg and  $2.59 \pm 0.087$  U/mg

# Exploration of the key sites for improving LDH activity toward phenylpyruvate

A ternary structural model showed that a cluster of residues (Arg9, Gln51, Tyr101, Asn268, and Met307) with large and long side chains are tightly packed around the benzene ring of the modeled PPA molecule and led to larger steric hindrance (Fig. 2). Mutation of these residues to those residues with short side chains could reduce the steric hindrance around the C-3 group of PPA molecules and thus increase the enzyme activity toward PPA. Additionally, the amino acid sequence of DLDH744 was also aligned with that of a PPA reductase. The corresponding amino acid residue with Arg9 in the PPA reductase is Leu, which has a shorter side chain (Fujii et al. 2011). In order to improve the catalytic activity of DLDH744 toward PPA, residues Arg9, Tyr101, Asn268, and Met307 around the C-3 group were all selected to be mutated to Leu to facilitate the activity contrast. Gln51 was mutated to Ala (corresponding residue of Tyr52 in D-LDH from Lactobacillus pentosus) since it has been reported that the Ala replacement could increase the enzymatic activity toward PPA (Ishikura et al. 2005). Furthermore, according to the structure, residue Phe298 was located near the PPA C-3 group (Fig. 2). In our previous report, the main-chain nitrogen atom of Phe298 forms a hydrogen bond with the carbonyl group of nicotinamide ring, so Phe298 is essential for the coenzyme binding in DLDH744 (Zhu et al. 2015a). Interestingly, it is a Tyr residue in the equivalent position of D-HicDH, which was supposed to favor the binding of aromatic substrate (Tokuda et al. 2003). Therefore, the residue Phe298 in DLDH744 was also chosen to be mutated to Tyr to cover all the possibility.

Based on the above structural model, amino acids around the benzene ring of the substrate were chosen to be mutated. R9L, Q51A, Y101L, N268L, F298Y, and M307L mutants were constructed, and their enzyme activities toward pyruvate and PPA were determined (Fig. 3). Q51A, Y101F, and M307L mutants showed higher enzyme activity than wild-type DLDH744 toward PPA, especially the M307L mutant, which increased the original activity toward pyruvate more than 1.5 times. However, R9L, N268L, and F298Y mutants were less active than the wild type. Notably, the enzyme activities of these mutants toward pyruvate were also all lower than those of the wild type.

The kinetic parameters of the M307L mutant for pyruvate and PPA were further determined using NADH as the cofactor (Table 2). After mutation, the  $K_{\rm m}$  value for PPA was reduced, whereas that for pyruvate was increased. The  $V_{\text{max}}$  with the M307L mutant using PPA as the substrate was increased to 7.15 U/mg. Moreover, the overall catalytic efficiency  $(k_{cat}/K_m)$ of the mutant was significantly increased. Then the production capacity of PLA by using M307L mutant was determined. Without optimization of the bioconversion conditions, E. coli JM109(DE3) harboring the wild-type enzyme DLDH744 could produce 1.11±0.022 g/L PLA while strain E. coli JM109(DE3) harboring M307L mutant could produce  $1.91 \pm 0.037$  g/L PLA under the same conditions. Since the native strain E. coli JM109(DE3) without introducing the enzyme DLDH744 only produced  $0.133 \pm 0.004$  g/L PLA, it should be concluded that M307L mutant increased the production titer of PLA from PPA. Thereafter, the mutant M307L was used in the subsequent experiments for transforming PPA to PLA.

#### **Optimization of bioconversion conditions**

Since *E. coli* strain is susceptible to acidic stress, the initial pH of the medium should be an important factor that affects PLA

Table 2 Kinetic constants of the wild type (WT) and mutants (M307L) of D-lactate dehydrogenase DLDH744

Enzyme	Substrate									
	Pyruvate				Phenylpyruvate					
	$K_{\rm m}({\rm mM})$	V <sub>max</sub> (U/mg)	$k_{\text{cat}}(\min^{-1})$	$k_{\text{cat}}/K_{\text{m}}(\text{mM}^{-1}\text{S}^{-1})$	$K_{\rm m}({\rm mM})$	V <sub>max</sub> (U/mg)	$k_{\rm cat}({\rm min}^{-1})$	$k_{\text{cat}}/K_{\text{m}}(\text{mM}^{-1}\text{S}^{-1})$		
WT M307L	$\begin{array}{c} 3.40 \pm 0.023 \\ 4.75 \pm 0.212 \end{array}$	$7.62 \pm 0.211 \\ 4.93 \pm 0.077$	$531.20 \pm 8.751 \\ 343.17 \pm 3.352$	$2.60 \pm 0.093$ 1. 20 ± 0.041	$\begin{array}{c} 3.32 \pm 0.080 \\ 1.27 \pm 0.035 \end{array}$	$\begin{array}{c} 4.26 \pm 0.105 \\ 7.15 \pm 0.057 \end{array}$	$\begin{array}{c} 296.47 \pm 0.081 \\ 497.60 \pm 5.790 \end{array}$	$\begin{array}{c} 1.49 \pm 0.076 \\ 6.53 \pm 0.092 \end{array}$		

production. Then the effects of pH on PLA production from PPA using resting cells of the recombinant *E. coli* strain with the mutant enzyme M307L were determined. PLA conversion yields at pH varying from 5.5 to 8.5 were examined. The high PLA yields were achieved in a broad range of pH from 7.0 to 8.5 while the highest PLA yield was obtained at pH 7.5 (Fig. 4).

Large-scale production of PLA from PPA using the enzymatic method requires large amounts of NADH and therefore has limited applications in the industry. In microbial conversion, NADH can be produced from low-cost cosubstrate glucose. Figure 5 shows the effect of glucose addition on wholecell bioconversion. Addition of glucose at a low concentration of 2.5 g/L significantly improved the PLA production. PLA production titer reached a maximum value of 56 mM with 5 g/ L glucose addition, and the yield was increased to 93.3 %.

# Production of PLA by the whole cells by fed-batch biotransformation

To improve the D-PLA production, fed-batch process by feeding PPA during conversion was conducted under the above optimal conditions. D-PLA was rapidly accumulated with the decrease of PPA during the first 2.5 h, and PPA feeding was performed subsequently. Before feeding the substrate, the D-PLA accumulation reached 12.05 g/L from total PPA of 12.97 g/L at a volumetric productivity rate of 4.82 g/L/h, and the conversion ratio of PPA to D-PLA was 92.91 % (Fig. 6). With the feeding of the substrate PPA during the fed-batch conversion, the D-PLA concentration was continuously increasing. The highest PLA production reached 21.43 g/L after 13.5 h, and the final conversion ratio of PPA to D-PLA was



Fig. 4 Effect of initial pH conditions on PLA production. The bioconversion was conducted in 50 mM PBS containing 60 mM PPA at a final  $OD_{600}$  of 60 at 30 °C for 2 h



Fig. 5 Effect of initial glucose concentration on PLA production. The bioconversion was conducted in 50 mM PBS (pH 7.5) containing 60 mM PPA at a final  $OD_{600}$  of 60 at 30 °C for 2 h

82.38 % (Fig. 6). We also tested the glucose addition with PPA feeding process, while there was no further positive effect on the production of PLA (data not shown). Considering substrate cost, only 5 g/L glucose was initially added. The volumetric productivity rate was 1.58 g/L/h, and the final optical purity of D-PLA reached a high value of 99.7 % (Fig. 7).

### Discussion

PLA is an important class of organic acids with versatile applications. It is an ideal antimicrobial compound with broadspectrum activity against both bacteria and fungi (Mu et al. 2012). Promising applications of PLA stimulated great endeavors in the development of its synthesis strategies. PLA has been reported to be produced by fermentation process.



**Fig. 6** Time course of fed-batch production of PLA by M307L mutant. Symbols:  $(\bullet)$ , PPA concentration;  $(\mathbf{\nabla})$ , PLA concentration;  $(\bullet)$ , PLA yield. Each point represents the mean standard deviation



**Fig. 7** The optical purity of produced D-PLA in fed-batch bioconversion process. **a** Sample was taken from the fed-batch biotransformation broth at 13.5 h. **b** Commercially available D-PLA standard. **c** commercially available L-PLA standard

However, the chemical and enantioselective purities of PLA produced by fermentation are usually at moderate level and difficult to be purified (Mu et al. 2009). Asymmetric bioreduction of PPA by using dehydrogenases is regarded as

one of the most promising solutions for the synthesis of PLA. especially optically pure PLA, due to its high efficiency, enantioselectivity, and easy operation (Zheng et al. 2013). Additionally, PPA is a feasible precursor for the large-scale production of PLA because it can be synthesized easily from hydantoin at a low cost. Many studies regarding engineering target enzymes have been reported while almost all the researches engineered the site of Tyr52 of D-LDH from L. pentosus. Tokuda et al. (2003) converted L. pentosus D-LDH into a D-hydroxyisocaproate dehydrogenase by replacing Tyr52 with a shorter Leu residue. Ishikura et al. (2005) enhanced the activity toward PPA of L. pentosus D-LDH through replacement of Tyr52 to Val and Ala. Zhu et al. (2015c) recently also replaced the Tyr52 residue of D-LDH from L. pentosus with small hydrophobic residues to enhance the PLA synthesis activity. Tyr52 and Phe299 of L. pentosus D-LDH were both selected for site-directed mutagenesis to abate the steric exclusion effect while only the Y52L mutant exhibited the best performance (Zheng et al. 2013). The above reports demonstrated the feasibility of improving D-LDH activity toward PPA by site-directed mutagenesis. Here, the Dlactate dehydrogenase DLDH744 from S. inulinus was selected as a starting target for improving the transformation capacity for PLA production, due to its high affinity for PPA which is different with all the previously reported LDHs. DLDH744 is much phylogenetically closer to D-hydroxyisocaproate dehydrogenase family, indicating DLDH744 might also have a larger space in the active center which might accept the larger substrates more efficiently (Zhu et al. 2015b).

 Table 3
 Comparative analysis of phenyllactate production reported in the literatures

Strains	Production process	Chirality	Genotype of D-LDH <sup>a</sup>	Production titer (g/L)	Glucose consumption (g/L)	Yield (%)	Reference
Lactobacillus sp. SK007	Biotransformation	Racemic PLA	_	1.13	10	56.7	Li et al. (2007)
Lactobacillus sp. SK007	Fed-batch fermentation	Racemic PLA	_	17.38	288.3	51.1	Mu et al. (2009)
Bacillus coagulans SDM	Biotransformation	Racemic PLA	_	37.3	126	70	Zheng et al. (2011)
Pediococcus pentosaceus	Fermentation	Racemic PLA	_	0.135	20	6.8	Yu et al. (2015)
Leuconostoc mesenteroides	Biotransformation	D-PLA	_	5.82	0	75.2	Li et al. (2014)
E. coli BL21(DE3)	Biotransformation	D-PLA	Y52V	15.6	10	77	Zhu et al. (2015c)
E. coli BL21(DE3)	Biotransformation	D-PLA	Y52L	8.23	(fdh) <sup>b</sup>	99	Zheng et al. (2013)
E. coli BL21(DE3)	Enzymatic production	D-PLA	Wild type	0.91	(fdh) <sup>b</sup>	36.7	Yu et al. (2014)
E. coli BL21(DE3)	Biotransformation	D-PLA	LaPPR <sup>c</sup>	91.3	150	91.3	Xu et al. (2015)
E. coli JM109(DE3)	Biotransformation	D-PLA	M307L	21.43	5	82.3	This study

<sup>a</sup> Applied only to the *E. coli* recombinant strains

<sup>b</sup> Coexpression of LDH with formate dehydrogenase for regeneration of NADH

<sup>c</sup> Wild-type of phenylpyruvate reductase (LaPPR, D-3-phosphoglycerate dehydrogenase subfamily) from Lactobacillus sp. strain CGMCC 9967

To fully identify the key sites which might be critical for improving the activity toward PPA, the PPA molecule was first docked in the active center of DLDH744. The residues that might tightly pack around the benzene ring of PPA from the structure-guided analysis were all selected for mutation. Replacement of Gln51, Tyr101, and Met307 residues with small residues obviously increased the enzyme activity toward PPA, which may be due to the further excessive space around the C-3 group of substrate after mutation and, therefore, reduced the steric hindrance of substrate. However, the enzyme activities of Q51A/Y101F, Q51A/M307L, and Y101F/M307L double mutants as well as Q51A/Y101L/M307L triple mutant were also examined, while no double or triple mutant gives better activity toward PPA than the wild type (data not shown). Some studies have reported that LDHs changed the catalytic domain from the open to the closed conformation when it is catalyzing (Razeto et al. 2002). It implied that tight coupling between substrate and the enzyme was essential to the enzyme activity. This could also explain that, with the increase of activities toward PPA, the LDH activities toward pyruvate were reduced after mutating to the small residues. After mutation, excessive space around the C-3 group of substrate reduced steric hindrance of PPA but also decreased the closeness between pyruvate and the enzyme. So, the catalytic efficiency for PPA was increased, while the catalytic efficiency for pyruvate was decreased accordingly.

Furthermore, D-LDH is an NADH-dependent reductase, and the cofactor NADH was required during the substrate reduction. Yu et al. (2014) reported that exogenous addition of NADH restored the PLA production. While for the production of optically pure D-PLA with a large scale, the application of enzyme method involving the use of a D-LDH is limited by the high cost of cofactor (NADH) regeneration. In the whole-cell bioconversion system, NADH regeneration could be obtained by simple addition of much cheaper glucose (Zheng et al. 2011), which is vital to the industrial application to minimize the costs. The effect of glucose on PLA production was investigated, and the results indicated that only addition of 5 g/L glucose could significantly increase the yield. Besides the advantage in the coenzyme utilization, the whole-cell biotransformation has some superiority in reducing the influence of microbiological contamination and high concentration of PLA. Hence, DLDH744 mutant M307L were transformed into E. coli JM109 (DE3) strain, and a production titer of D-PLA of 21.4 g/L was achieved without coexpression of the cofactor regeneration system, which ranked in the list as the highest production titer of D-PLA by engineered D-LDH (Table 3). A high titer (37.3 g/L) of racemic PLA (the main isomer is L-PLA) produced from PPA by the mutant of Bacillus coagulans, with a very high concentration of 126 g/L glucose consumption during the fermentation, limited the economic feasibility of this process (Zheng et al. 2011). During the preparation of this manuscript, Xu et al. (2015) reported a novel phenylpyruvate reductase (LaPPR,

D-3-phosphoglycerate dehydrogenase subfamily) from *Lactobacillus* sp. strain CGMCC 9967. By construction, the coexpression system with glucose dehydrogenase, as much as 100 g/L PPA, was asymmetrically reduced into D-PLA with a 91.3 % yield by addition of 1.5 equiv. glucose of PPA. The results suggest that LaPPR is also a promising biocatalyst for the synthesis of D-PLA. In our study, only 5 g/L glucose was required in the whole fed-batch process, which was the least consumption in comparison with other reports. This is probably due to predominant characteristic of DLDH744 that can use both NADH and NADPH as the coenzyme at equal efficiency (Zhu et al. 2015a).

In summary, the enzymatic activity of DLDH744 toward substrates with large aromatic group at C-3 was successfully improved by structured-guided mutation. Moreover, due to the high yield and high stereoselectivity of DLDH744 mutant M307L, the whole-cell catalysis system containing DLDH744 mutant was successfully applied to the direct synthesis of D-PLA. Thus, the process developed in this study could also be used as a promising alternative for the production of highly, optically pure  $\alpha$ -hydroxy carboxylic acid.

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#### Compliance with ethical standards

**Conflict of interest** The authors declare that they have no competing interests.

**Ethical statement** This article does not contain any studies with human participants or animals performed by any of the authors.

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