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# Backwash intensity and frequency impact the microbial community structure and function in a fixed-bed biofilm reactor

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Abstract Linkages among bioreactor operation and performance and microbial community structure were investigated for a fixed-bed biofilm system designed to remove perchlorate from drinking water. Perchlorate removal was monitored to evaluate reactor performance during and after the frequency and intensity of the backwash procedure were changed, while the microbial community structure was studied using clone libraries and quantitative PCR targeting the 16S rRNA gene.

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When backwash frequency was increased from once per month to once per day, perchlorate removal initially deteriorated and then recovered, and the relative abundance of perchlorate-reducing bacteria (PRB) initially increased and then decreased. This apparent discrepancy suggested that bacterial populations other than PRB played an indirect role in perchlorate removal, likely by consuming dissolved oxygen, a competing electron acceptor. When backwash intensity was increased, the reactor gradually lost its ability to remove perchlorate, and concurrently the relative abundance of PRB decreased. The results indicated that changes in reactor operation had a profound impact on reactor performance through altering the microbial community structure. Backwashing is an important yet poorly characterized procedure when operating fixed-bed biofilm reactors. Compared to backwash intensity, changes in backwash frequency exerted less disturbance on the microbial community in the current study. If this finding can be confirmed in future work, backwash frequency may serve as the primary parameter when optimizing backwash procedures.

Keywords Backwash frequency · Backwash intensity · Microbial community . Biofilm reactor. Perchlorate

#### Introduction

Biofilm reactor technology provides an important avenue for drinking water treatment and has demonstrated to be effective in removing a range of contaminants from source waters (Nerenberg and Rittmann [2004;](#page-11-0) Bouwer and Crowe [1988;](#page-10-0) Choi et al. [2008;](#page-11-0) Upadhyaya et al. [2010](#page-12-0); Ding and Yokota [2010\)](#page-11-0). A key component in further advancing the technology is to elucidate the linkages among reactor operation, reactor performance, and microbial community (Briones and Raskin

[2003;](#page-10-0) Curtis et al. [2003](#page-11-0)). In this study, a fixed-bed biofilm reactor designed to remove perchlorate from drinking water was studied to illustrate these relationships. Perchlorate is an endocrine disruptor with several adverse health effects (Greer et al. [2002](#page-11-0)) and has been detected in many drinking water sources (Urbansky [2002\)](#page-12-0). Therefore, perchlorate is on U.S. EPA's drinking water contaminant candidate list (US-EPA [2008\)](#page-12-0) and is regulated by a number of states in the U.S. at various levels ranging from 1 to 18 μg/L (CA-DHS [2005](#page-10-0); MA-DEP [2006;](#page-11-0) US-EPA [2005](#page-12-0)).

In recent years, fixed-bed biofilm reactors have been evaluated for the removal of perchlorate from drinking water (Miller and Logan [2000;](#page-11-0) Brown et al. [2003;](#page-10-0) Choi et al. [2007](#page-11-0); Li et al. [2010](#page-11-0)). During normal operation, the biofilm support medium in fixed-bed reactors remains stationary, as opposed to fluidized-bed reactors in which the support medium is fluidized. As water passes through the stationary bed in a downflow mode, particulates including microbial cell aggregates accumulate in void space and cause clogging. Clogging can be prevented by regular reactor backwashing, which is necessary for continued operation of these bioreactors (Hozalski and Bouwer [1998](#page-11-0)). Backwashing, the passing of a flow of water or a mixture of water and air in an upflow mode, removes particulate matter and resolves bioreactor clogging (Ahmad et al. [1998](#page-10-0)). Backwashing removes most loosely attached biofilms (i.e., cell aggregates in the pores of support media) and a fraction of tightly attached biofilms (Servais et al. [1991](#page-11-0)), depending on the backwash intensity. Backwashing with high intensity may cause too much biomass loss and impair reactor performance (Lahav et al. [2001\)](#page-11-0). Backwashing with low intensity may result in insufficient removal of accumulated biomass and quick pressure buildup during operation, and consequently, frequent backwashes will be needed. Backwash frequency is usually established by monitoring pressure buildup caused by clogging across the reactor. In general, backwash procedures are experimentally optimized for each individual facility, which creates challenges to systematically study this important procedure and explains why studies on backwashing have been scarce.

In an earlier study, the effects of backwash procedures on reactor performance were investigated using two fixed-bed biofilm reactors operated to remove perchlorate from water (Choi et al. [2007\)](#page-11-0). The two reactors had 3- and 1-mm diameter glass beads as support media, respectively, and were operated with various influent dissolved oxygen levels. Results showed that after the backwash frequency was increased from monthly to daily, reactor performance first decreased and then recovered when the backwashes were performed with low intensity. In contrast, daily strong backwashes caused a failure of perchlorate removal, particularly when influent DO level was high. The difference in performance responses to the various reactor operating conditions likely was rooted in the way microbial communities, especially perchlorate reducing

bacterial populations, responded to the changes in backwash procedure.

Perchlorate reducing bacteria (PRB) can utilize perchlorate as an electron acceptor and convert it to non-toxic chloride (Coates and Achenbach [2004](#page-11-0)). PRB described so far mainly belong to three genera Dechloromonas, Azospira, and Dechlorospirillum (Coates et al. [1999](#page-11-0); Waller et al. [2004](#page-12-0); Bardiya and Bae [2008;](#page-10-0) Zhang et al. [2005\)](#page-12-0). For most PRB, oxygen is the preferred electron acceptor over perchlorate (Coates and Achenbach [2004](#page-11-0)). Hence, to allow effective perchlorate removal in bioreactors, oxygen needs to be removed by PRB or other aerobic bacteria before biological perchlorate reduction can occur (Xu et al. [2003\)](#page-12-0). Therefore, simultaneous studies of PRB and other aerobic bacteria are crucial in studying engineered systems designed for perchlorate removal.

In this study, linkages among reactor operating conditions (backwash frequency and intensity), reactor performance or microbial community function (removal of dissolved oxygen and perchlorate), and microbial community structure (relative abundance of PRB and other aerobic bacteria) were investigated for a fixed-bed biofilm reactor designed to remove perchlorate from drinking water. The microbial community structure was first determined using clone library analyses targeting the 16S rRNA gene and then major bacterial populations were monitored using quantitative polymerase chain reaction (qPCR). Microbial community responses to various backwash parameters were reported, which provide insights in designing backwash strategies for fixed-bed biofilm systems.

#### Materials and methods

Fixed-bed biofilm reactor and reactor operation

The reactor configuration, influent composition, operating conditions, and backwash procedures were similar to the ones reported in an earlier study (Choi et al. [2007\)](#page-11-0). In brief, a bench-scale fixed-bed biofilm reactor with an inner diameter of 2.4 cm and a height of 24 cm was filled with 1-mm diameter glass beads, resulting in an empty bed volume of 63.4 mm<sup>3</sup>. The reactor was inoculated with biomass from a biologically active carbon filter previously operated to treat groundwater amended with 50 μg/L perchlorate using acetate as the electron donor (Lin [2004](#page-11-0)). Influent was pumped into the bottom of the reactor at a flow rate ( $Q_{\text{influent}}$ ) of 2.7 mL/min, resulting in an empty bed contact time of 23.4 min. A recirculation loop  $(Q_{recirculation} = 5 \times Q_{influent})$  was installed to the reactor to reduce the plug-flow characteristics of the reactor. The influent contained two electron acceptors, 3 mg/L DO and 50 μg/L perchlorate. A phosphate buffer solution with a final concentration of 0.5 mM maintained the pH inside the reactor at 7.5, and served as phosphorus source along with 0.01 mM NH4Cl as nitrogen source. Based on stoichiometric calculations

(Rittmann and McCarty [2001](#page-11-0)) with an assumed net yield value of 0.2 g  $\text{COD}_{\text{biomass}}/\text{g}$   $\text{COD}_{\text{acetate}}$ , 2 mg C/L of acetate was added to reactor influent to serve as the sole electron donor. These operating parameters were defined as the baseline operating condition for this system. In a "weak backwash", reactor content was stirred in 100-mL of previously collected reactor effluent in a 600-mL beaker with a 7.5-cm long magnetic stir bar at 75 revolutions per min (RPM) for 1 min, and then the supernatant was decanted. In a "strong backwash", the reactor content was stirred in 125 mL previously collected effluent at 150 RPM twice for 1 min each time, with supernatant decanting and new effluent replenishment between these periods. The reactor was backwashed about once a month before the daily weak backwash experiment started. Six days after the daily weak backwash experiment, the daily strong backwash experiment was conducted.

Influent and effluent DO concentrations were measured using WTW multi340 m with CellOx325 sensors in WTW D201 flow cells (WTW Inc., Weilheim, Germany) connected to the inlet and outlet of the reactor. All other chemical parameters were measured according to Standard Methods (American Public Health Association (APHA) [1992\)](#page-10-0). Perchlorate was measured using an ion chromatograph system (Dionex ICS-2000, Sunnyvale, CA) according to EPA Standard Method 314.1. An AS-16 analytical column and an AG-16 guard column were used, while the eluent was 65 mM KOH. The detection limits for DO and perchlorate were 0.01 mg/L and 1 μg/L, respectively.

## Data analyses on reactor performance

Mass balance calculations on chemical concentrations (i.e., DO and perchlorate) were performed for the biofilm reactor. The governing equation was

$$
V\frac{dC}{dt} = Q(C_{\text{in}} - C_{\text{out}}) - rV
$$

where C represents the concentration of either DO or perchlorate in the reactor,  $C_{\text{in}}$  and  $C_{\text{out}}$  are the influent and effluent concentrations,  $V$  is the volume of the reactor,  $Q$  is the flow rate, and  $r$  represents the DO or perchlorate removal rate inside the reactor due to microbial activities. For the calculations presented here, completely stirred tank reactor conditions were assumed and therefore:

 $C = C_{\text{out}}$ 

As a result, the governing equation was converted to:

$$
r = \frac{1}{T}(C_{\text{in}} - C_{\text{out}}) - \frac{dC_{\text{out}}}{dt}
$$

where  $T$  is the empty bed contact time of 23.4 min or 0.01625 day. The initial removal rate  $r$ , for both DO and perchlorate, after a backwash was calculated using the last

equation. The value of  $\frac{dC_{\text{out}}}{dt}$  was estimated by fitting measured  $C_{\text{out}}$  vs. t using a second-order polynomial trendline and calculating the derivative of the trendline at the time of backwash.  $C_{\text{in}}$  was 3 mg/L for DO or 50 µg/L for perchlorate. The  $C_{\text{out}}$  at the time immediately after backwash was obtained from the corresponding trendline equations.

#### eDNA and iDNA extractions and protein assay

For clone library construction, biomass samples were collected from the biofilm reactor on day 0 of the daily weak backwash experiment and day 5 of the strong backwash experiment. Total DNA was extracted from these two biomass samples using FastDNA SPIN Kit (Qbiogene Inc., Irvine, CA). For qPCR measurements, biomass samples were collected from backwash water at all 11 backwash events. The biomass remaining in the reactor after each backwash was not sampled because the size of the reactor was small and daily sampling over the course of the experiment would have significantly changed the amount of biofilm in the reactor. eDNA was separated from cellular materials and extracted by following a published protocol (Corinaldesi et al. [2005](#page-11-0)). iDNA was extracted from the eDNA-free cellular materials by following a published protocol (Griffiths et al. [2000\)](#page-11-0). All DNA extracts were quantified using a NanoDrop ND1000 (Thermo Scientific, Waltham, MA), and their qualities were evaluated using electrophoresis on a 1% agarose gel. Protein measurements were conducted using a protein assay kit (Bio-Rad, Hercules, CA).

#### Clone library

The bacterial 16S rRNA gene was amplified in triplicate PCR reactions on a Mastercycler (Eppendorf International, Hamburg, Germany) with the forward primer 8F (5′-AGA GTT TGA TCC TGG CTC AG-3′) and the reverse primer 1492R (5′-GG[C/T] TAC CTT GTT ACG ACT T-3′) (Dojka et al. [1998](#page-11-0); Richardson et al. [2002](#page-11-0)). The composition of the PCR solutions and the conditions of the PCR reactions were adopted from the literature (Dojka et al. [1998](#page-11-0)). The 30-cycle PCR reaction started with 12 min of denaturation at 94°C and ended with a final extension at 72°C for 12 min. Each cycle consisted of denaturation at 94°C for 1 min, annealing at 50°C for 45 s, and extension at 72°C for 2 min. Pooled PCR products from triplicates were purified using electrophoresis on a 1% agarose gel and extracted using a MinElute Gel Extraction Kit (QIAGEN Inc., Valencia, CA). Purified PCR products were cloned into pCR4-TOPO vectors (Invitrogen Inc., Carlsbad, CA), and transformed into chemically competent Escherichia coli. The transformed E. coli cells were plated on Luria–Bertani agar that contained 50 μg/mL kanamycin and were incubated at 37°C overnight.

<span id="page-3-0"></span>Colonies were randomly picked and used to inoculate three 96-well microplates. Two of the three microplates in glycerol stocks were sent to the Genomic Center at Washington University (St. Louis, MO) for sequencing.

#### Phylogenetic analyses

A total of 384 clones (four 96-well microplates) were sequenced using vector primers T3 and T7. Nucleotide sequences were analyzed and edited using BioEdit (Hall [1999](#page-11-0)). Closely related sequences (i.e., Dechloromonas-, Zoogloea-, and Curvibacter-like clones in both clone libraries) identified via the Ribosomal Database Project (RDP) (Cole et al. [2007\)](#page-11-0) were aligned using ClustalW (Chenna et al. [2003](#page-10-0)) for bacterial 16S rRNA genes. The differences between the corresponding genera in the two clone libraries were evaluated using the Library Comparison function on RDP. Sequences identified as chimeras using Mallard (Ashelford et al. [2006](#page-10-0)) were excluded from further analyses. The phylogenetic tree was based on a region of the 16S rRNA gene of ca. 600 bp starting at the 8F primer region and was created based on the evolutionary history inferred using the neighbor-joining method (Saitou and Nei [1987\)](#page-11-0) and the evolutionary distance computed using the Jukes–Cantor method (Jukes and Cantor [1969\)](#page-11-0) incorporated in the software program MEGA (Tamura et al. [2007](#page-11-0)). The percentages of replicate trees in which the associated taxa clustered together

in the bootstrap test (1,000 replicates) were shown next to the branches (Felsenstein [1985\)](#page-11-0). There were a total of 500 sites in the final dataset used to build the phylogenetic tree. Operational taxonomic units (OTUs) were defined as clones that shared 95% identity in the 16S rRNA gene (Fields et al. [2005\)](#page-11-0). OTUs, diversity statistics, and rarefaction curves were calculated using DOTUR (Schloss and Handelsman [2005](#page-11-0)). The similarities of the bacterial 16S rRNA gene clone libraries were evaluated using ∫-LIBSHUFF (Schloss et al. [2004\)](#page-11-0).

### qPCR primer design and reaction conditions

qPCR primer sets were designed based on representative sequences of the clones of interests (i.e., Dechloromonas, Zoogloea, and Curvibacter) using the Primer3 program (Rozen and Skaletsky [2000\)](#page-11-0) made available by Integrated DNA Technologies [\(www.idtdna.com\)](http://www.idtdna.com) and were synthesized by Invitrogen (Carlsbad, CA). The lengths of the amplicons using the three primer sets ranged from 106 to 155 bp. The specificities of the designed primer sets were manually verified using the Probe Match function of RDP (Cole et al. [2007\)](#page-11-0), while the coverage of the designed primer sets were evaluated against the clones of interest in relevant clone libraries using OligoReport [\(http://www.bioinformatics-toolkit.org/Cowslip/](http://www.bioinformatics-toolkit.org/Cowslip/index.html) [index.html](http://www.bioinformatics-toolkit.org/Cowslip/index.html)) (Table 1). The specificities of the designed primer sets were further characterized with various ranges of annealing temperatures using the gradient PCR function of a

Table 1 Sequence, coverage, specificity, and annealing temperature for each primer set designed in this study

Target $(16S \, rRNA \, gene)$		F/R Systematic name $a$ , $b$	Abbreviated name	Sequence $(5'$ to $3')$	Coverage in clone library $#1^c$	Coverage in clone library $#2^c$	Specificity <sup>d</sup>	Anneal-ing temp. $({}^{\circ}C)^{e}$
Dechloromonas	F	S-G-Dchm- $0991-a-S-24$	Dchm0991F	TTG ACA TGT CCA GAA GCC CGA AGA	23/26	7/7	12/29	58.5
	R	S-G-Dchm- $1146-a-A-24$	Dchm1146R	TGT CAC CGG CAG TCT CGT TAA AGT	21/26	6/7	68/196	
Zoogloea	F	$S-G-Zoog-$ $0487-a-S-24$	$Z$ oog $0487F$	ACC GTA AGA AGA AGC ACC GGC TAA	40/44	13/26	32/277	68.0
	R	$S-G-Zoog-$ $0627-a-A-24$	Zooq0627R	TGA TGC AGT CAC AAA CGC AGT TCC	35/44	20/26	23/24	
Curvibacter	F	S-G-Curvib- $1001-a-S-21$	Curvib1001F	CGG AAG TTA CCA GAG ATG GTT	21/21	73/77	71/110	64.0
	R	S-G-Curvib- $1107-a-A-21$		Curvib <sub>1107R</sub> CAA CTA ATG ACA AGG GTT GCG	20/21	74/77	203/7190	

<sup>a</sup> The primers were named according to standardized nomenclature (Alm et al. [1996\)](#page-10-0)

<sup>b</sup> The location of the primers were determined based on *Escherichia coli* numbering (Brosius et al. [1981\)](#page-10-0)

<sup>e</sup> Annealing temperatures were experimentally determined in this study (Fig. S1)

 $\rm^c$  Coverage="Number of target clones with perfect match to the corresponding primer"/"Number of target clones in the clone library". Clone library". #1 was built on the biomass collected on day 0 of daily weak backwash experiment, while clone library #2 on day 5 of daily strong backwash experiment

<sup>&</sup>lt;sup>d</sup> Specificity="Number of target sequences in database with perfect match to the corresponding primer"/"Number of sequences in public database with perfect match to the corresponding primer". The specificity results were obtained using the Probe Match function on RDP in May 2007 (Cole et al. [2007\)](#page-11-0). The non-target sequences with perfect match to the corresponding primer are not detected in the clone library results in this study. Therefore, little interference is expected for the qPCR results in this study

real-time PCR thermocycler Mastercycler realplex system (Eppendorf International, Hamburg, Germany) (Fig. S1). The selected annealing temperatures for the three designed primer sets (Table [1\)](#page-3-0) could differentiate the fluorescence signals between equal amounts of target and non-target templates (i.e.,  $10^6$  copies/ $\mu$ L) by at least 15  $C_{\text{threshold}}$  units (Fig. S1). The PCR amplicons from the characterization experiments using the primer set Dchm0991F/1146R were also tested by electrophoresis on a 1% agarose gel (Fig. S2). The gel image showed the correlation between fluorescence signals from qPCR and band intensity on an agarose gel. The specificity of the designed primer sets were further tested by monitoring the melting temperatures from the melting curves on target and non-target templates (Fig. S3). The qPCR primer set Bact1369F/1492R for quantifying total bacteria was adopted from Suzuki et al. ([2000](#page-11-0)).

All qPCR experiments were performed using a RealMasterMix SYBR Green Kit (Eppendorf International, Hamburg, Germany), which had a self-adjusting chelating mechanism to control  $Mg^{2+}$  concentrations. The reaction mixtures in a 25- $\mu$ L final volume contained 11.25 μL of 2.5× RealMasterMix SYBR Green solution (including 0.05 U/μL HotMaster Taq DNA polymerase, 10 mM magnesium acetate, 1.0 mM dNTPs, and 2.5× SYBR Green solution), 150 nM of forward and reverse primers, Sigma water (Sigma-Aldrich, St. Louis, MO), and target/non-target template of known concentrations or 10 ng of DNA template from environmental samples. All qPCR experiments included Sigma water as a non-template control to assure identification of false positives. As suggested in the manual of the RealMasterMix SYBR Green kit, amplification involved one cycle of 95°C for 10 min for initial denaturation and then 40 cycles of 95°C for 15 s followed by annealing at the temperatures reported in Table [1](#page-3-0) for 20 s and extension at 68°C for 30 s. Detection of SYBR Green fluorescence was set at the extension step of each cycle. Melting profiles were collected after 40 cycles of amplification to check the specificity of the amplification.

#### qPCR standard curves

Target and non-target templates were plasmid DNA extracted from clones obtained from the clone libraries constructed in the current study using QIAprep Miniprep Kit (QIAGEN Inc., Valencia, CA) and quantified using NanoDrop ND1000. The target templates contained the representative sequences based on which corresponding primer sets were designed, while the non-target templates contained sequences with the least number of mismatches with the designed primer sets in the relevant clone libraries (Table S1). Dilutions of purified E. coli plasmid DNA containing the 16S rRNA genes of Dechloromonas, Zoogloea, and Curvibacter were used as standards for qPCR in the quantification of specific populations. The plasmid DNA concentrations (copies/microliter) were calculated using the following equation

plasmid DNA concentration 
$$
\left[\frac{copy}{\mu L}\right]
$$
 = (plasmid DNA concentration  $\left[\frac{ng}{\mu L}\right] \times \frac{1}{(3956+1484)\times607.4+157.9} \left[\frac{nmol}{ng}\right]$   
  $\times \left(\frac{1 \text{ mol}}{10^9 \text{ mol}}\right) \times \left(\frac{6.023 \times 10^{23} \text{ copy}}{\text{mol}}\right)$ 

where 3,956 and 1,484 are the lengths of the pCR®4-TOPO vector (Invitrogen Corporation, Carlsbad, CA) and PCR insert, the constants of 607.4 and 157.9 were obtained for the calculation of the molecular weight of double stranded DNA ([www.ambion.com](http://www.ambion.com)).

The standard curve constructed from triplicate measurements for each qPCR primer set was linear between "C<sub>threshold</sub>" and "Log Target Concentration (copy # per microliter)" (Fig. S4). The  $R^2$  values ranged from 0.993 to 0.995 (Table S1). Among the four primer sets used, Bact1369F/1492R had the narrowest linear range: the  $C<sub>threshold</sub>$  values for the standards of  $10<sup>1</sup>$  and  $10<sup>2</sup>$  copies per microliter fell outside the linear range and thus were not included in the standard curve. The linear ranges in Fig. S4 covered all the measurements from unknown samples. The high y-intercept value for Bact1369F/1492R reported in Table S1 indicates a lower detection limit at a given cycle number (Ritalahti et al. [2006](#page-11-0)). The amplification efficiencies (*E*) were calculated using the equation,  $E = 10^{(-1/\text{slope})} - 1$ , where the slope is the slope of a standard curve. The amplification efficiencies for the four primer sets ranged from 0.627 (Bact1369F/1492R) to 0.990 (Zoog0487F/0627R, Table S1). To enumerate target copy numbers in environmental samples, standard curves were measured in triplicates on each 96-well microplates to avoid discrepancies across microplates.

#### Sequence submission

The sequences included in the phylogenetic tree have been submitted to the DDBJ/EMBL/GenBank databases under accession numbers FJ610473-FJ610667.

#### Results

## Extracellular DNA

Because extracellular DNA (eDNA) is deemed important for biofilm studies due to its high abundance in certain natural environments (Corinaldesi et al. [2005](#page-11-0); Steinberger et al. [2002\)](#page-11-0) and its sequence similarity to intracellular DNA (iDNA) in certain biofilms (Steinberger and Holden [2005](#page-11-0)), we investigated whether the presence of eDNA would affect the 16S rRNA gene sequence analyses and the quantification of total DNA extracted for the fixed-bed biofilm reactor. The mass ratios of eDNA to total DNA for the biomass samples, collected in two sets of backwash experiments (i.e., daily weak and daily strong backwash experiments, see below), are presented in Fig. 1. The average percentages were  $20.6\pm$ 4.6% ( $n=6$ ) and 24.8±13.7% ( $n=4$ , excluding the sample on day 1 of the daily strong backwash experiment) for the daily weak and daily strong backwash experiments, respectively. Statistical analyses showed no significant difference between the two sets ( $p=0.610$ ), indicating that the microbial community inside the biofilm reactor contained similar percentages of eDNA under different backwash intensities.

qPCR results showed that eDNA extracts from the biofilm reactor did not contain 16S rRNA gene sequences that were amplifiable by the four primer sets used in this study (data not shown). Among the four primer sets, three were designed in this study to target the three dominant bacterial genera in the reactor (Table [1\)](#page-3-0), and the other one was a published primer set targeting the bacterial domain (Suzuki et al. [2000\)](#page-11-0). The only exception was the eDNA extract from day 1 of the daily strong backwash experiment, which was amplified by all four primer sets (insert in Fig. 1). This eDNA extract likely was contaminated with iDNA, because qPCR results showed the relative abundances of the three targeted genera (i.e., Dechloromonas, Zoogloea, and Curvibacter) in this eDNA extract to be very similar to those in the corresponding iDNA extract. Since the eDNA samples did not contain sequences that were amplifiable with the four PCR primer sets, separate analyses of eDNA and iDNA were not pursued in subsequent experiments.

## Microbial community

To study the linkages among reactor operation, reactor performance, and microbial community structure, two sets of backwash experiments were conducted in sequence: a daily weak backwash experiment and a daily strong backwash experiment. Two 16S rRNA gene clone libraries were constructed to study the microbial community in the biofilm reactor: one for the biomass sample collected on day 0 of the daily weak backwash experiment, and one for the biomass sample collected on day 5 of the daily strong backwash experiment (Table [2](#page-6-0)). In both libraries, Betaproteobacteria was the most abundant class. In the first clone library, the two most abundant bacterial genera were Dechloromonas and Zoogloea. The most abundant genus in the second library was Curvibacter. Therefore, the relative abundances of these three genera were monitored using qPCR throughout the two backwash experiments. A phylogenetic tree was constructed for the clones that belonged to these three genera in the two clone libraries (Fig. [2\)](#page-7-0). Clones associated with Dechloromonas in both clone libraries clustered together and were closely related to Dechloromonas sp. HZ and Dechloromonas sp. JM. The clones associated with Zoogloea and Curvibacter in both libraries also clustered together.



Fig. 1 The ratios of eDNA to total DNA in biomass samples collected from the daily weak backwash (gray) and daily strong backwash experiments (dark). Due to contamination, the ratio for day 1 of the daily strong backwash experiment (hatched pattern) was not included

in the reported average percentages in the text. The insert shows the relative abundances of the three dominant genera in the iDNA and "eDNA" extracts of that particular sample, suggesting iDNA contamination in the eDNA extract

<span id="page-6-0"></span>Table 2 Relative abundances of bacterial populations in biomas samples collected on day 0 of th weak backwash experiment (total of 182 clones) and day 5 of the strong backwash experiment (total of 184 clones) determined using clone library sequence analyses (the criterion used in selecting taxa to be included in the table: taxa that contained more than one clone in at least one of the two libraries, with the exception of the genus Azospira

a Day 388 since the start of the reactor. Before the start of the daily weak backwash experiment, the reactor has been mainly operated using the baseline operating condition

b Taxa whose relative abundances were significantly different in the two clone libraries with values less than 0.01 according to the Library Comparison function on RDP  $c<sub>ND</sub>$  not detected



Genus level analyses revealed changes in the overall community structure before and after the two daily backwash experiments. In Fig. [3,](#page-8-0) the Chao1 and ACE indices increased from 60 and 75 to 81 and 92, respectively, indicating the microbial richness increased during the backwash experiments. The same trend was supported also by the rarefaction curves in Fig. [3](#page-8-0). In contrast, the Shannon–Weiner and Inverse Simpson's microbial diversity indices decreased from 2.77 and 11.51 to 2.40 and 4.73, respectively, due to the decrease in evenness. In addition, clone library results showed that the structures of the microbial communities before and after the backwash experiments were different (Table 2). This observation was statistically supported using ∫-LIBSHUFF (p<0.05).

#### Daily weak backwash experiment

Before the daily weak backwash experiment started, the fixedbed biofilm reactor had been operated using the baseline operating conditions for 388 days. The reactor was backwashed once every month and was able to consistently remove dissolved oxygen (DO) and perchlorate to below their respective detection limits of 0.01 mg/L and 1 μg/L (data not shown). The daily weak backwash initially caused disturbances in reactor performance, but a gradual recovery was observed (Fig. [4a, b\)](#page-8-0). Immediately after the weak backwash on day 1, effluent DO started at about 0.5 mg/L and then dropped to 0.04 mg/L at the end of the day. During the next 4 days, the effluent DO concentration immediately after each backwash decreased from about 0.5 mg/L on day 2 to about 0.05 mg/L on day 5. To better illustrate the improvement of reactor performance in lowering effluent DO concentration during the course of the experiment, the initial DO removal rate after each weak backwash was plotted in Fig. [4a](#page-8-0).

A similar trend was noted for the effluent perchlorate profiles (Fig. [4b](#page-8-0)). On day 1, the effluent perchlorate concentration immediately after the weak backwash was close to the influent perchlorate concentration (i.e., 50  $\mu$ g/L), and then decreased throughout the day. After each subsequent daily weak backwash, the effluent perchlorate concentration dropped faster than the day before. To better illustrate the improvement in perchlorate removal, the initial perchlorate removal rate after each weak backwash was calculated and plotted in Fig. [4b.](#page-8-0)

The amount of biomass removed was the highest for day 0 of the daily weak backwash experiment, because the reactor had been backwashed only once a month before this backwash experiment and had accumulated a large amount of biomass (Fig. [5a\)](#page-9-0). Assuming 55% of bacterial dry weight is made of protein and excluding the datum point from day 0 of the daily weak backwash experiment, protein assay results suggested the average amounts of biomass washed <span id="page-7-0"></span>Fig. 2 Phylogenetic tree of the 16S rRNA gene clones that were closely associated with the three major bacterial genera present in the biofilm reactor. "Day 0" and "Day 5" refer to day 0 of the daily weak backwash experiment and day 5 of the daily strong backwash experiment, respectively. The numbers in parentheses are the numbers of clones



out were 2.32 and 2.71 mg dry weight in weak and strong backwashes, respectively. With an assumed net yield of 0.2 g CODbiomass/g CODacetate, the dry weight of the biomass generated every day was calculated to be 2.66 mg, indicating that the daily biomass growth in the reactor approximately equaled the daily biomass loss through backwash.

Using qPCR, it was determined that the three most abundant bacterial populations responded differently to the daily weak backwashes. The relative abundance of Dechloromonas first decreased from 27.3% on day 0 to 2.5% on day 3, and then increased to 12.1% on day 5 (Fig. [5b](#page-9-0)). The relative abundance of Zoogloea first increased from 26.7% on day 0 to 36.1% on day 2, and then decreased to 15.6% on day 5. The relative abundance of Curvibacter increased from 19.8% on day 0 to 40.3% on day 5.

Daily strong backwash experiment

The bioreactor was not backwashed for 6 days after the daily weak backwash experiment. At the end of the 6 days, the reactor exhibited consistent and complete removal of DO and perchlorate (data not shown). Then, the reactor was subjected to strong backwashes for five consecutive days. The increase in backwash intensity dramatically affected reactor performance (Fig. [4c, d](#page-8-0)). Immediately after the strong backwash on day 1, the effluent DO concentration was 0.01 mg/L and remained low throughout the day. During the next few days, the effluent DO concentration immediately after each backwash increased as the experiment proceeded, except for day 4. Since the results of a replicate experiment with the same reactor (Fig. S5) also indicated a continuously increasing trend of effluent DO similar to that in Fig. [4c](#page-8-0), the effluent DO

<span id="page-8-0"></span>Fig. 3 Rarefaction curves indicating bacterial 16S rRNA gene richness within the two clone libraries. The dashed line represents 1:1, indicating infinite diversity. The table lists the bacterial 16S rRNA gene sequence diversity indices. OTUs were defined as groups of sequences sharing 95% 16S rRNA gene sequence identity. The estimates of phylotype richness were calculated according to the abundancebased coverage estimate (ACE) and the bias-corrected Chao1 estimator. The Shannon–Weiner diversity index and the Inverse Simpson's diversity index, which consider both richness and evenness, were also calculated



1. OTUs defined as 5% difference in 16S rRNA gene sequences.

<sup>2</sup>. Mean values with upper and lower 95% confidence intervals given in parentheses.

concentration on day 4 was not included when calculating the trendline for the initial DO removal rate after each strong backwash. This trendline demonstrated a deteriorating ability of the microbial community to lower DO.

A decreasing ability to remove perchlorate was also observed during the daily strong backwash experiment. The effluent perchlorate concentration immediately after each strong backwash was close to the influent perchlorate





Fig. 4 Effluent DO (top row) and perchlorate (bottom row) concentrations during the daily weak backwash experiment (left column) and the daily strong backwash experiment (right column). (Filled diamond) Effluent DO concentration; (empty diamond) initial DO removal rate; (filled circle) effluent perchlorate concentration; (empty circle) initial

perchlorate removal rate; the solid lines are second-order polynomial trendlines to help visualize the improvements of DO and perchlorate removal rates immediately after backwash events. The arrows point to the time when backwash events occurred

<span id="page-9-0"></span>concentration, 50 μg/L (Fig. [4d\)](#page-8-0). The reactor was able to achieve complete perchlorate removal at the end of day 1. Starting on day 2, the ability of the reactor to remove perchlorate deteriorated. On day 5, the effluent perchlorate concentration remained at a level close to the influent perchlorate concentration throughout the day. The trendline for the initial perchlorate removal rate after each strong backwash showed that the ability of the reactor to remove perchlorate had decreased.

Similar to the daily weak backwash experiment, the three major bacterial genera responded differently to the strong backwashes as determined using qPCR. The relative abundance of Dechloromonas decreased from 7.0% on day 1 to 0.5% on day 5 (Fig. 5d). The relative abundance of Zoogloea first increased from 9.0% to 14.3% during the first 2 days, and then decreased to 2.4% on day 5. The relative abundance of Curvibacter increased from 60.9% on day 1 to 97.5% on day 5.

## **Discussion**

Three qPCR primer sets, targeting strains that belong to the genera Dechloromonas, Zoogloea, and Curvibacter, were designed based on the sequences of the corresponding clones in two 16S rRNA gene clone libraries, instead of

using all sequences for the relevant genera available in pubic databases. Thus, the designed primers are not strictly genusspecific primers. Such design demands lower stringency on primer coverage and warrants higher specificity. Thus, it is not surprising that even the closest non-targets for some designed primers had more than seven mismatches (Table S1). The primer sets were characterized to obtain optimized annealing temperatures for qPCR experiments using known concentrations of plasmids that were obtained from the clone libraries and contained target or non-target sequences.

Dechloromonas spp. and Azospira spp. were the only known PRB detected in the reactor. The dominance of Dechloromonas in perchlorate reducing systems has been shown by other studies in which acetate (Zhang et al. [2005](#page-12-0)) or hydrogen (Nerenberg et al. [2008](#page-11-0)) was used as the sole electron donor. In the biofilm reactor studied by Zhang and coworkers, about 23% of the microbes on the surface of the biofilm were detected to be Dechloromonas strains. In the hydrogen-fed membrane biofilm reactors (MBfR) studied by Nerenberg and coworkers, the relative abundance of Dechloromonas comprised 49% of the bacterial community. The Dechloromonaslike clones recovered in this study clustered together and were found to be closely related to Dechloromonas sp. HZ and Dechloromonas sp. JM, both of which are PRB and can utilize



Fig. 5 Protein measurements (top row) and the relative abundances of the three major bacterial genera expressed as a fraction of the total bacterial population (bottom row) during the daily weak (left column) and strong (right column) backwash experiments

<span id="page-10-0"></span>acetate as an electron donor (Zhang et al. [2002](#page-12-0); Logan et al. [2001\)](#page-11-0). Other PRB species, such as Dechlorospirillum spp. and Azospirillum spp., which were isolated from various natural and engineered systems (Bardiya and Bae 2008; Waller et al. [2004\)](#page-12-0), were not detected in the current study.

The presence of Zoogloea spp. in the biofilm reactor is not surprising, as members of this genus have been characterized as slime formers in engineered systems (Rossellomora et al. [1995\)](#page-11-0). Zoogloea spp. are aerobic (Xie and Yokota [2006;](#page-12-0) Unz [1984\)](#page-12-0) and thus must have utilized DO as their electron acceptor in the current system. The genus Curvibacter has been described only relatively recently (Ding and Yokota [2004\)](#page-11-0), and knowledge about the ecological function of Curvibacter spp. is limited, except that they have been detected in freshwater (Ding and Yokota [2004;](#page-11-0) Ding and Yokota [2010](#page-11-0)), Antarctic coastal waters (Gentile et al. [2006\)](#page-11-0), and activated sludge (Thomsen et al. [2007](#page-12-0)).

Both reactor performance and PRB population abundance recovered from the disturbance imposed by the higher backwash frequency. Before the backwash frequency was increased from once a month to once a day, effluent perchlorate concentration was constantly below the detection limit. After the change, effluent perchlorate was high after each backwash event and then decreased for the rest of the day. Interestingly, across different days, perchlorate removal rate continuously improved (Fig. [4b\)](#page-8-0); however, the relative abundance of *Dech*loromonas spp. showed a down-and-up trend (Fig. [5b](#page-9-0)). The discrepancy in the trends of the relative abundance of PRB and perchlorate removal suggests that bacterial population(s) other than Dechloromonas spp. impacted perchlorate removal efficiency. Such bacterial population(s) likely affected perchlorate removal by consuming DO, the competing electron acceptor, in the bioreactor. When the bulk DO level dropped towards the end of the daily weak backwash experiment, the DO level in the biofilm must have decreased accordingly. The decreased DO level in the biofilm could have been responsible for the increase in the relative abundance of Dechloromonas during that time period. In contrast, neither the reactor performance nor the PRB population recovered from the increase in backwash intensity. Reactor performance in terms of perchlorate removal and the relative abundance of Dechloromonas spp. continuously dropped during the daily strong backwash experiment (Figs. [4d](#page-8-0) and [5](#page-9-0)). Although the amount of biomass within the reactor could not be monitored experimentally, it was expected to be relatively constant over the course of the study, as the daily biomass growth approximately equaled the biomass loss through daily backwash.

In conclusion, after a minor disturbance in reactor operation, i.e., an increase in backwash frequency, the major PRB population (Dechloromonas spp.) was able to recover, and reactor performance (perchlorate removal) recovered gradually. In comparison, after a major disturbance in reactor operation, i.e., an increase in backwash intensity, Dechloromonas spp.

failed to remain competitive in the microbial community, Curvibacter spp. became the dominant population, and consequently reactor performance deteriorated. To our knowledge, this is the first study designed to systematically investigate how two backwash parameters, frequency and intensity, affect the structure and function of microbial communities in biofilm reactors. Although different from those used in full-scale facilities, the backwash procedure used in this study allowed us to carefully control the two backwash parameters and to ensure high reproducibility between individual backwash events. The conclusions from this study, particularly the finding that increasing the backwash frequency disturbed the microbial community less compared to raising backwash intensity, are expected to be helpful to the development and optimization of backwash procedures at full-scale facilities.

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