

Microbial characterisation of polyhydroxyalkanoates storing populations selected under different operating conditions using a cell-sorting RT-PCR approach

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Abstract The identity of polyhydroxyalkanoates (PHA) storing bacteria selected under aerobic dynamic feeding conditions, using propionate as carbon source (reactor P), was determined by applying reverse transcriptase–polymerase chain reaction (RT-PCR) on micromanipulated cells and confirmed by fluorescence in situ hybridisation (FISH). Four genera, *Amaricoccus*, *Azoarcus*, *Thauera* and *Paracoccus* were detected, the latter only rarely present. All the biomass was involved in PHA storage as shown by Nile Blue staining. By quantitative FISH, their specific amount was determined in this and two other systems using acetate as the carbon substrate (sequencing batch reactor [SBR] A and A1). SBR A and reactor P had the same sludge retention time (SRT, 10 days), while reactor A1 was operated with the SRT of 1 day and the double organic loading rate (OLR). Systems fed with acetate (41.1 ± 2.2 and $49.4 \pm 1.4\%$ total *Bacteria*, for A and A1, respectively) became enriched in *Thauera* independently on the SRT and OLR, while it was only present in a minor amount when propionate was used as a substrate ($1.9 \pm 0.2\%$ total *Bacteria*). *Amaricoccus* was present in both reactors operated at 10 days SRT, favoured in the one fed with propionate ($61.4 \pm 1.9\%$ total bacteria), and almost completely removed at the SRT of 1 day. *Azoarcus* cells were found in all the analysed systems

(3.9 ± 0.3 , 23.3 ± 1.5 and 45.9 ± 1.5 for P, A and A1, respectively), while *Paracoccus* was scarcely present.

Keywords PHA production · Aerobic dynamic feeding · Mixed cultures · RT-PCR · FISH · Micromanipulation

Introduction

Awareness concerning the environment and the use of clean technologies is growing worldwide. As a consequence, research on biodegradability and use of renewable resources for industrial processes has been intensive in the last years. Polyhydroxyalkanoates (PHA) are biodegradable biopolymers that have been recognised as good candidates for synthetic polymers partial replacement. PHA are accumulated intracellularly by a wide variety of microorganisms, acting as carbon and energy sources. The industrial production of PHA is achieved using pure or genetically engineered cultures with a high storage capacity (up to 90% of cell dry weight; Marchessault 1996). The greatest drawback for their use as petrol-based polymers substitutes is the production cost, which can be four times higher than the chemical synthesis (Direction Générale des Ressources Naturelles et de l'Environnement du Ministère de la Région du Valoni 2002). PHA production processes based on mixed microbial cultures (MMC) are being investigated as a possible technology to decrease production costs, as no sterilisation is required and bacteria can adapt quite well to the complex substrate present in low-cost substrates. Although many processes using MMC have been proposed to reach this goal, the most promising one is based on the utilisation of periodic

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supply of carbon substrates: a short period of excess carbon (feast) followed by a long period of starvation (famine; Majone et al. 1996). This process is currently known as ‘feast and famine’ or aerobic dynamic feeding (ADF). These conditions favour the development of bacterial populations with a high and stable PHA storage capacity. Under ADF conditions, with carbon addition (acetate) by sequential pulses, Serafim et al. (2004) showed that the intracellular PHA content reached 65.4% cell dry weight. The polymer produced was a 3-hydroxybutyrate (3HB) homopolymer.

For the majority of applications, a co-polymer of 3HB and another monomer, such as 3-hydroxyvalerate (3HV), is preferred because it presents a lower crystallinity and melting temperatures, making the polymer more flexible and with improved mechanical properties. The use of different carbon substrates allows modulating the polymer composition according to the desired polymer-specific applications. As an example, propionate can act as the precursor for the three-carbon unit (propionyl-CoA) needed for the hydroxyvalerate synthesis. PHA co-polymers and terpolymers production using propionate and mixed cultures are reported in the literature (Beccari et al. 1998; Dionisi et al. 2004; Lemos et al. 2006).

One critical factor on the development of a competitive process for PHA production with MMC is the selection of organisms with high storage capacity. Therefore, it is mandatory to monitor the population dynamics and to assess for different groups of organisms, in terms of PHA storage and cell growth kinetics. In terms of microbial population dynamics, scarce information is available about the organisms responsible for PHA accumulation under ADF and how they evolve in time. Recently, molecular methods had been applied to identify PHA-accumulating organisms in an ADF reactor (Dionisi et al. 2005, 2006). These authors used denaturing gradient gel electrophoresis (DGGE) and performed a 16S rRNA (ribosomal ribonucleic acid) clone library to characterise the evolution of the microbial community with high storage capacity. From the 100 clones obtained, the most important organisms belonged to the *Betaproteobacteria* (*Thauera*, *Alcaligenes*, *Comamonas*, *Achromobacter*), but also several *Alphaproteobacteria* (*Xantobacter*, *Curtobacterium*) and *Gamma-proteobacteria* (*Kluyvera*, *Pseudomonas*, *Acinetobacter*) were present. The *Thauera* genus was assumed to be responsible for the PHA accumulation, although neither the abundance of this microorganism in the analysed sludge nor its involvement in PHA storage was confirmed in situ.

Fluorescence in situ hybridisation (FISH) has been recently employed for the characterisation of the microbial population in two reactors operated under ADF conditions, one adapted to acetate (reactor A) and the other to propionate (reactor P; Serafim et al. 2006). Three major morphotypes, Gram-negative *Zoogloea*-like bacilli (morphotype I) and two

similar tetrad-forming bacteria (morphotypes II and III), affiliated, respectively, to the *Betaproteobacteria* and the *Alphaproteobacteria*, were dominant in both reactors and were involved in PHA storage. The main responsible for PHA storage was affiliated to the genus *Azoarcus* belonging to *Betaproteobacteria*. These morphotypes were always present, but their relative abundance changed during the sequencing batch reactor (SBR) operation. However, variation in biomass composition did not affect the storage capacity and the type of polymer produced (Serafim et al. 2006). System A always produced an homopolymer P(3HB) from acetate and a terpolymer P(3HB-co-3HV-co-2M3HV) from propionate, while population P always produced a co-polymer P(3HB-co-3HV) from acetate and propionate. Differences in polymer composition suggested a diverse biomass composition in the two reactors, which was not evident by morphological observation. These results seem to indicate that reactor operational conditions as well as the kind of substrate used may have a great impact in population selection. The microbial population composition developed in these systems was likely different from that reported by Dionisi et al. (2004), in which P(3HV) was produced from propionate in a reactor operated with different conditions (cycle length, sludge age, organic loading rate).

In the present paper, the sorting/reverse transcriptase-polymerase chain reaction (RT-PCR) approach was utilised to reveal the main composition of the PHA-accumulating biomass present in the system fed with propionate (P). Using FISH, the relative abundance of the microorganisms identified by the sorting/RT-PCR approach was estimated for the biomass selected in reactors A and P. This comparison intended to determine the effect of carbon substrate on the biomass composition, as for both reactors, all the other operational conditions were the same. The influence of short sludge retention time (SRT) and double organic load rate (OLR), on the storage performance and biomass composition, was also investigated in the reactor fed with acetate (A1). Correlation between the specific abundance of the identified microbial populations in these systems and the reactor performance was established.

Materials and methods

Reactors operation

In this study, a SBR for the production of PHA, operating for 4 years and adapted to propionate as carbon source (reactor P), was investigated.

The reactor working volume was 1 L and the total SBR cycle length 12 h, consisting of 10.5 h of aerobiosis, 1 h of settling (mixing and air bubbling switched off) and 0.5 h withdrawing half of the volume of the supernatant, which was

replaced by the same volume of fresh medium during the first 15 min at the beginning of the cycle. The hydraulic retention time was 1 day. At the end of each cycle, before settling, a defined volume of mixed liquor was removed to keep the SRT at 10 days. Oxygen was supplied by an air compressor through a ceramic membrane disperser introduced inside the reactor at an airflow rate of 1.0 vvm (vol air/vol reactor min), maintaining dissolved oxygen concentration around 80% of the saturation value. The reactor was operated without pH control, but its value was monitored online (ranging between 8.0 and 9.2); the temperature was kept at 22°C and the stirring rate at 250 rpm. Timers controlled the air compressor, the medium feed, waste pumps and stirring.

A second reactor operated under the same conditions but using acetate as carbon source (A reactor) was also investigated. A third reactor (A1 reactor), using acetate as substrate, was operated under the same conditions of reactor A except that SRT was shorter (1 day) and organic loading rate was doubled (OLR, 120 C mmol L⁻¹ day⁻¹).

Culture medium

The standard mineral salts medium used in the SBR P was composed of (per litre of distilled water): 1.269 g CH₃CH₂COOH, 600 mg MgSO₄·7H₂O, 160 mg NH₄Cl, 100 mg EDTA ethylenediamine tetraacetic acid, 92 mg K₂HPO₄, 45 mg KH₂PO₄, 70 mg CaCl₂·2H₂O and 2 ml of trace elements solution. The trace solution consisted of (per litre of distilled water): 1,500 mg FeCl₃·6H₂O, 150 mg H₃BO₃, 150 mg CoCl₂·6H₂O, 120 mg MnCl₂·4H₂O, 120 mg ZnSO₄·7H₂O, 60 mg Na₂MoO₄·2H₂O, 30 mg CuSO₄·5H₂O and 30 mg of KI. Thiourea (10 mg/l) was added to inhibit nitrification. The pH of the salt solution was adjusted to 7.2 and then sterilised. The phosphorus solution was sterilised separately. After sterilisation, the two solutions were allowed to cool and were mixed together. The same mineral medium was used for SBR A and A1 with acetate, respectively, 40.796 and 81.592 g of CH₃COONa·3H₂O, as the only carbon source.

Analytical techniques

Cell dry weight was determined as volatile suspended solids according to Standard Methods (APHA 1995).

Acetate and propionate were analysed by high-performance liquid chromatography using a BioRad Aminex HPX-87H column, with 0.01 N sulphuric acid as eluent, an elution rate of 0.6 ml/min and an operating temperature of 50°C. A UV detector (Merck) set at 210 nm was used. Before injection, samples were filtered using a 0.2-µm membrane. PHA were determined by gas chromatography after acidic esterification according to Serafim et al. (2004) and Lemos et al. (2006). Ammonia was analysed using an ammonia gas-sensing

combination electrode ThermoOrion 9512. Exopolymeric substances (EPS) were analysed according to Frølund et al. (1996).

Morphological characterisation and FISH analysis of the biomass

SBR biomass samples were collected regularly, at the end of the feeding period, for microscopic observation and staining. An aliquot of each sample was fixed for later FISH analysis, as described by Amann (1995). The protocol described in Jenkins et al. (1993) was utilised for Gram, Neisser and India Ink stainings. Intracellular PHA granules were shown by Nile Blue staining (Ostle and Holt 1982).

FISH was performed following Amann (1995). According to Maszenan et al. (2000), a pre-enzymatic treatment was applied on sample before FISH to increase permeability of Gram-negative tetrad-forming organisms. The oligonucleotide probes utilised are reported in Table 1. An Olympus BX51 microscope was used for the observations of the biomass in phase contrast, bright field (after Gram, Neisser and Nile blue staining) and epifluorescence (after Nile blue staining and FISH). Images were collected and analysed with F-View Soft Image System video camera and AnalySIS software.

Quantification was carried out on the fixed biomass according to previously published methods (Bouchez et al. 2000; Crocetti et al. 2002), and results were visualised on a Zeiss LSM 510 Meta confocal laser-scanning microscope. Specific probes used were all CY3 labelled and used in combination with CY5-labelled EUBmix (EUB338+EUB338-II+EUB338-III). Image analysis of 40 randomly selected fields was performed using the free ImageJ software package (version 1.37b, Wayne Rasband, National Institute of Health, USA). The abundance of the diverse groups was expressed as percentage of all bacteria (as area occupied by probe-binding cells). The calculation was

Table 1 Specificities of the oligonucleotide probes utilised

Probe name	Specificity	Reference
EUB338	Most bacteria	Amann et al. 1990
EUB338-II	<i>Planctomycetales</i>	Daims et al. 1999
EUB338-III	<i>Verrucomicrobiales</i>	Daims et al. 1999
ALF968	<i>Alphaproteobacteria</i>	Neef 1997
BET42a	<i>Betaproteobacteria</i>	Manz et al. 1992
AMAR839	<i>Amaricoccus</i> spp.	Maszenan et al. 2000
AZA645	Most members of the <i>Azoarcus</i> cluster	Hess et al. 1997
THAU832	<i>Thauera</i> spp.	Loy et al. 2005
PAR651	genus <i>Paracoccus</i>	Neef et al. 1996

EUB338, EUB338 I and EUB338 II were applied as an equimolar mix (EUBmix).

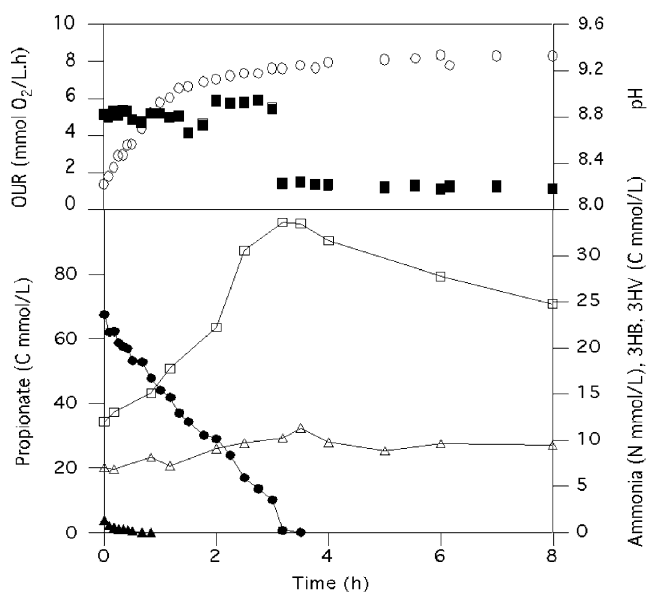


Fig. 1 Time profile of propionate (filled circles), 3HB (open triangles), 3HV (open squares), ammonia (filled triangles), pH (open circles) and OUR (filled squares) in reactor P under ADF conditions

performed from the images where the number of pixels with a positive signal from both the specific probe and the EUBmix probes was compared to the number of pixels with a positive signal from the EUBmix probe. The standard error of the mean was calculated as the standard deviation divided by the square root of the number of images.

Cell sorting–RT-PCR approach

The sorting–RT-PCR approach, described hereafter, was applied on ethanol fixed samples. For the specific amplification of the targeted bacteria 16S rRNA, a small cluster of cells with distinctive morphology was collected by micromanipulation from the mixed biomass spread on an agar plate. Small homogenous clusters composed mostly of a single morphotype with abundant 16S rRNA were necessary for the specific micromanipulation and the amplification. By microscopic observation and FISH analysis with the EUBmix probe, a suitable sample for the sorting/RT-PCR was selected. The cells collected were transferred from the micromanipulation hook directly in a PCR tube, containing 10 μ l of high purity distilled water, and then amplified by RT-PCR. RT-PCR was performed using the Invitrogen SuperscriptTM One RT-PCR kit (Invitrogen, Carlsbad, USA) with the universal primers U27f and U1492r.

Cloning and sequence analysis

Since the micromanipulation was carried out on clusters of bacteria selected solely on the basis of their morphology, it could not be guaranteed that all the collected cells belonged

to the same species. Amplified rDNAs (ribosomal deoxyribonucleic acids) pooled from the three reactions were purified by the QIAquick PCR purification kit (Quiagen) according to the manufacturer's instructions. Amplicons were then ligated into pcr[®]4-TOPO[®] vector (Invitrogen) and transformed into One Shot[®] TOP10 chemically competent *E. coli* cells according to the manufacturer's instructions. The obtained clones were partially sequenced with T3 forward primer, while the 16S rRNAs of clone 11 from morphotype I and clone 5 from morphotypes II–III were completely sequenced with T3 and T7 primers (MWG biotech). The compiled 16S rRNA sequences were manually aligned, and the organism identity was deduced by standard programs including BLASTN and BLAST2 for most likely identities. The sequences were deposited in GenBank (accession numbers are EF367341 for clone 11 and EF367342 for clone 5).

ProbeBase online tool (Loy et al. 2003) was utilised for the selection of probes matching the retrieved 16S rRNA sequences.

Results

Reactors performance

The microbial characterisation of the PHA-accumulating microorganisms was performed in three reactors, SBRs P, A and A1, operated under different conditions.

The SBR A and P have been simultaneously operated for several years under dynamic feeding conditions, with a SRT of 10 days and OLR of 60 C mmol L⁻¹ day⁻¹ (30 C

Table 2 Performance of reactors A, A1 and P under different operational conditions

SBR	P ^a	A ^b	A1
Carbon source	Propionate	Acetate	Acetate
SRT (days)	10	10	1
OLR (C mmol L ⁻¹ day ⁻¹)	60	60	120
PHA	P(3HB-co-3HV)	P(3HB)	P(3HV)
3HB:3HV	28:72	100:0	100:0
$-q_S$ (C mmol S/C mmol X h ⁻¹)	0.24	0.80	0.27
$-q_N$ (N mmol/C mmol X h ⁻¹)	0.034	0.032	0.055
$Y_{X/S}$ (C mmol X/C mmol S)	0.25	0.20	0.23
$q_{P(3HB-3HV)}$ (C mmol 3HA/C mmol X h ⁻¹)	0.008–0.031	0.47	0.11
$Y_{P(3HB-3HV)/S}$ (C mmol 3HA/C mmol S)	0.05–0.18	0.58	0.33

P 10 days SRT, fed with propionate, A 10 days SRT, fed with acetate, A1 1 day SRT, fed with acetate

^aData from Lemos et al. 2006

^bData from Serafim et al. 2004

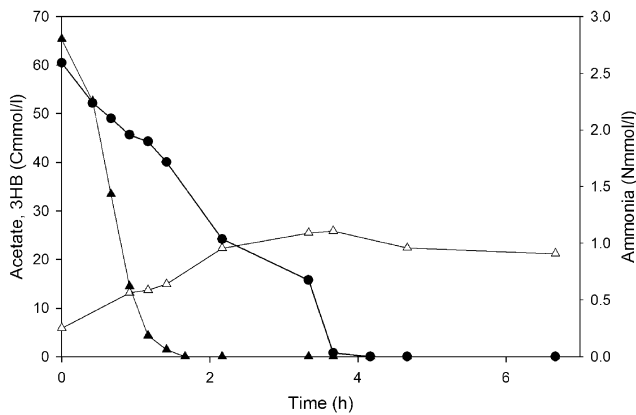


Fig. 2 Time profile of acetate (filled circles), P(3HB) (open triangles) and ammonia (filled triangles) in reactor A1 under ADF conditions

mmol/cycle) using, respectively, acetate and propionate as carbon source. Reactor A was fully described in Serafim et al. (2004). Figure 1 shows the profiles for carbon and nitrogen concentrations and for oxygen uptake rate during a batch experiment (one cycle) of the reactor P fed with propionate. The propionate consumption was linear with time, and the oxygen uptake rate was almost stable, dropping sharply after carbon depletion. P(3HB-co-3HV) was produced with a higher fraction of 3HV. Polymer production occurred simultaneously with cell growth, as shown by the ammonia consumption. When no external carbon source was available, the formed polymer was consumed for cellular maintenance. The kinetic and stoichiometric parameters calculated for these systems are reported in Table 2.

A new reactor for PHA production, SBR A1, was set with biomass of reactor A as inoculum. This reactor was operated for 101 days, fed with acetate, a SRT of 1 day and

a OLR of $120 \text{ C mmol L}^{-1} \text{ day}^{-1}$, while the C/N ratio was the same as in reactors A and P. Figure 2 presents the profiles of acetate, P(3HB) and ammonia during a feast and famine cycle of this system. This culture performed similarly to that of reactor A, where a homopolymer was produced. During the analysed operation period, the biomass from this system showed an average PHA cell content of 27.9% cell dry weight (maximum PHA storage capacity not optimised). Kinetic and stoichiometric parameters of this system were compared with the same data from reactors A and P (Table 2).

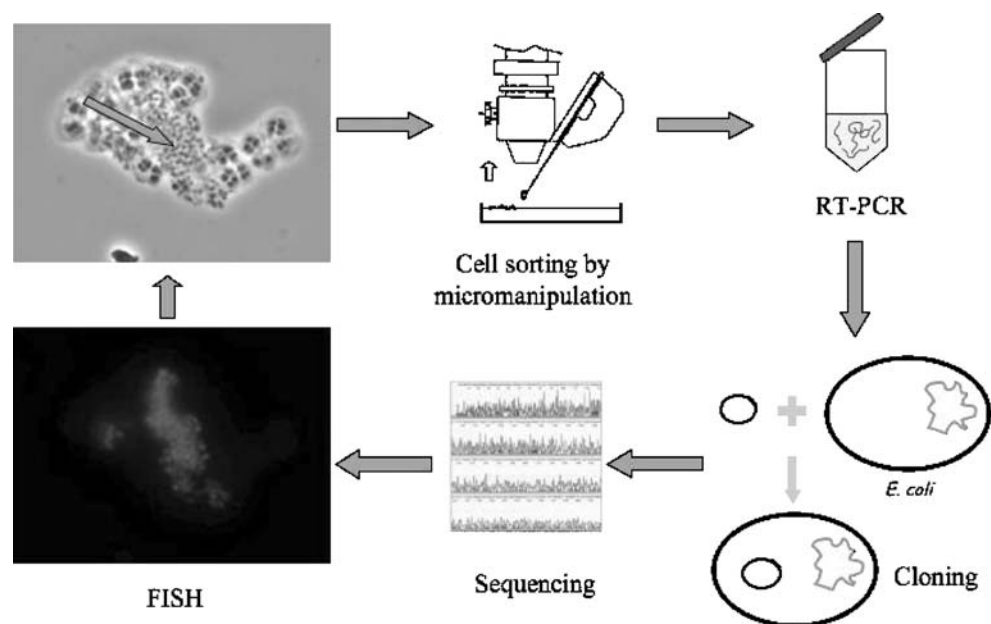
Sorting/RT-PCR approach

Cell sorting/RT-PCR was applied to determine the composition of the reactor P biomass at the genus level. By this method, bacteria with a distinctive morphology were selectively separated from the microbial community by micromanipulation and soon after the collected cells were utilised for successive 16S rRNA gene amplification by RT-PCR.

Because cell sorting is performed on clusters of bacteria selected on the basis of their morphology, the collected cells could belong to different bacterial species. Therefore, a small 16S rRNA gene clone library was constructed for each amplificate, and clones were sequenced to analyse all amplified 16S rDNAs. The obtained clones were sequenced, and the organism's identity was ascertained. The approach validation was obtained by FISH analysis through the application of specific oligonucleotide probes fully matching all the retrieved 16S rDNA sequences. A general scheme of the experimental procedure is given in Fig. 3.

The main morphotypes present in SBR P biomass (Fig. 4), their affiliation to *Proteobacteria* classes and their

Fig. 3 Sorting/reverse transcriptase-PCR strategy applied for the identification of PHA accumulation organisms. Morphologically distinguishable cell clusters were micromanipulated and transferred to a PCR tube containing high-purity water for successive 16S rRNA gene amplification by RT-PCR. The pool of amplified rDNAs were then ligated and transformed into chemically competent *E. coli* cells. The obtained 16S rRNA gene clones were sequenced, and the organism identities were ascertained. FISH was used to validate the approach: Oligonucleotide probes fully matching the retrieved 16S rRNA gene sequences were selected and applied on the original sample



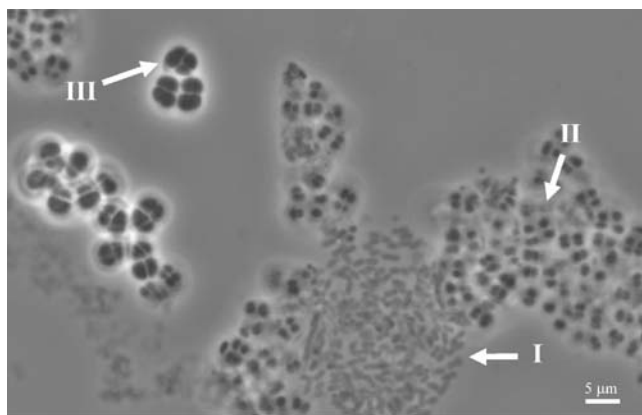


Fig. 4 Morphotypes composing reactors A, A1 and P biomass (I morphotype I *Betaproteobacteria*, bacilli ($1 \times 1.2\text{--}1.5 \mu\text{m}$), II morphotype II *Alphaproteobacteria*, coccobacilli ($1 \times 2 \mu\text{m}$) in pairs or loosely aggregated tetrads, III morphotype III *Alphaproteobacteria*, large cocci ($2 \times 2 \mu\text{m}$) in tightly packed tetrads)

role in PHA storage were previously described (Serafim et al. 2006). To identify the major component of this biomass, in the present study, one cluster of bacilli (Morphotype I) was collected by micromanipulation and directly utilised to 16S rRNA gene amplification by RT-PCR. The same procedure was applied to one cluster of tetrad-forming organisms, corresponding to morphotypes II and III that, being morphologically very similar, could not be differentiated at the microscopic magnification utilised for micromanipulation ($\times 350$). In both cases, amplicates were obtained from a single cluster.

Four 16S rRNA gene plasmid inserts, two from each micromanipulated bacterial aggregate, were sequenced. In Table 3, the closest relative of the obtained sequences are reported together with the available genus- and species-specific probes targeting these 16S rRNA.

16S rRNA gene sequences deriving from morphotype I cells (clones 11 and 2) belonged to the *Betaproteobacteria*, being almost identical to an uncultured bacterium affiliated to deeply branching clade in the *Azoarcus* (Juretschko et al. 2002). The 16S rDNA sequences obtained from morphotype II/III cells were, instead, affiliated to two different taxa in the order *Rhodobacterales* within the *Alphaproteobacteria*, one of them belonging to the *Amaricoccus* genus.

FISH analysis was performed on the biomass sample utilised for the sorting/RT-PCR approach, to ascertain the presence and the importance of the identified taxa. Probes available in literature for the genera *Azoarcus* (AZA645; Hess et al. 1997), *Amaricoccus* (AMAR839; Maszenan et al. 2000) and *Paracoccus* (PAR651; Neef et al. 1996), which have a full match with the retrieved 16S rRNA sequences, were used. Although no sequence belonging to the genus *Thauera* was obtained, their presence was also investigated with probe THAU832 (Loy et al. 2005). This microorganism was indicated as the most abundant and likely responsible for

the storage phenomena in a system operated under ADF conditions for PHA production (Dionisi et al. 2006).

Probes AZA645- and AMAR839-positive cells, respectively, morphotype I and II cells (Fig. 5), were present. *Azoarcus* cells were dominating, and the two species accounted for most of the biomass. The genus-specific probe THAU832 detected only a small portion of the reactor's bacterial population that could not be morphologically discriminated from *Azoarcus* cells. Probe PAR651 hybridised to thin bacilli ($0.5 \times 0.8 \mu\text{m}$), rarely present and usually disperse in flocs, while morphotype III cells, also present in a minor amount, were not recognised with the applied probes. The results did not allow the identification of this component of the biomass but confirmed that, although similar, the two morphotypes (II and III) belong to different taxons. The *Amaricoccus* cells could be differentiated from morphotype III also by the yellow autofluorescence of the cell wall when they were observed with a fluorescein filter (U-MWB2 Olympus).

Quantitative FISH analysis

The presence and abundance of the genera *Amaricoccus*, *Azoarcus*, *Thauera* and *Paracoccus* in the population selected in reactors P, A and A1 was determined by FISH.

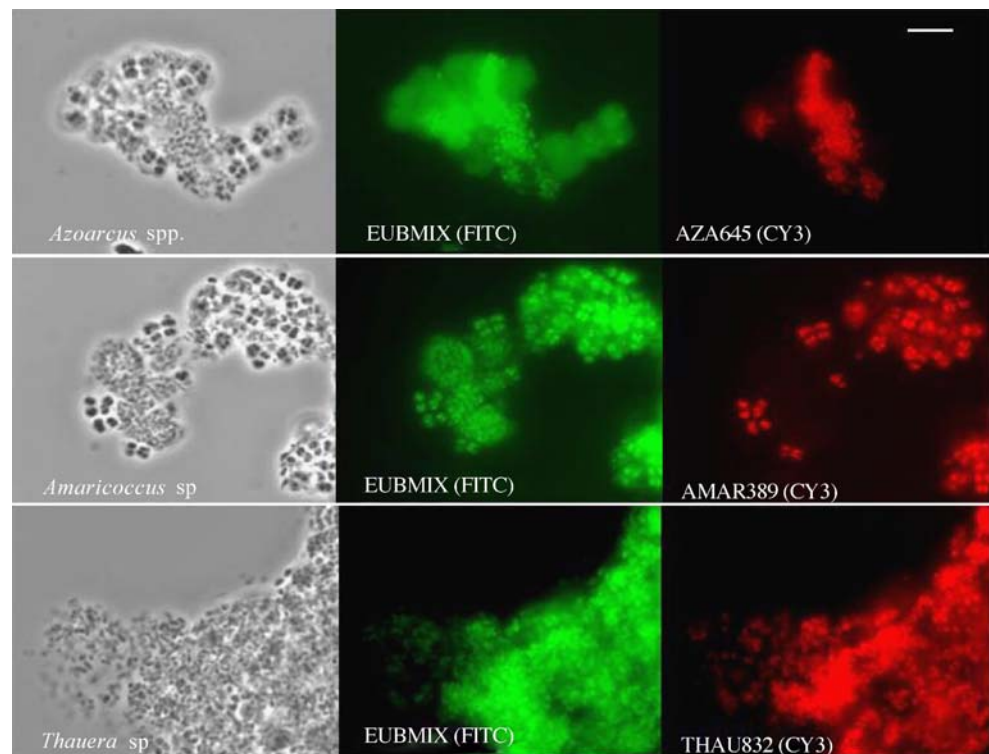
A sample from reactor P, different from the one used for the sorting RT-PCR approach, was analysed to determine the relative abundance of the microorganisms and to validate the previous identifications. The population of reactor A was also characterised. The effect of different carbon sources on microbial population dynamics was evaluated by comparing the composition of reactors A- and P-selected biomasses (Table 4).

FISH analysis confirmed that *Amaricoccus* spp. and *Azoarcus* spp. were still present in reactor P biomass after 2 years of operation. A major change in their relative abundance was observed in the present sample compared with that used for sorting/RT-PCR. *Amaricoccus* spp. was

Table 3 Affiliation of the retrieved sequences and matching FISH probes

Clone number	Closest phylogenetic relative (% 16S rDNA similarity)	FISH probe binding the sequences
2, 11	Uncultured <i>Azoarcus</i> sp. H30 from activated sludge (AF072924) (99%)	AZA645
18	<i>Amaricoccus kaplicensis</i> (AKU88041) (100%)	AMAR839
5	Uncultured sludge bacterium A41 (AF234761) (96%)	PAR651

Fig. 5 Phase contrast appearance and FISH detection of the dominant PHA accumulating organisms ($bar=10\ \mu m$)



in this case dominant (61.4%), and *Azoarcus* was present in minor amount (3.9%). In this reactor, only a few THAU832-positive cells were detected (1.9%). The biomass of reactor P was only partially identified (67.2% of the EUBmix-positive cells) with the genus-specific probes applied. This result was consistent with the abundant presence of morphotype III cells that hybridised only with the general probe for the *Alphaproteobacteria*.

Differently from what was observed in reactor P, almost all the biomass from reactor A was identified with the probes THAU832, AMAR839 and AZA645. All the three genera were present in a large amount: *Thauera* spp. cells composed approximately half of the biomass (41.1%), but also *Azoarcus* (23.3%) and *Amaricoccus* (28.8%) were quite abundant in the system. Morphotype III was not detected in reactor A, and

Table 4 Presence and abundance of *Azoarcus* spp., *Thauera* spp. and *Amaricoccus* spp. over EUBmix-positive signal in PHA-producing biomasses

	Reactor P (%)	Reactor A (%)	Reactor A1 (%)
AZA645	3.9±0.3	23.3±1.5	45.9±1.5
AMAR839	61.4±1.9	28.8±1.8	<1
THAU832	1.9±0.2	41.1±2.2	49.4±1.4
Total	67.2	93.2	95.3

Percentage of EUBmix-positive cells identified with the applied genus and species-specific probes as well as their standard deviation.

PAR651-positive cells belonging to the *Paracoccus* genus were only rarely observed in both reactors.

Nile blue staining for lipid detection was performed on these biomasses before feeding and just after the substrate depletion. All the biomass was involved in PHA storage, as shown by the increase of fluorescence from the beginning to the end of the feast phase. However, morphotype I cells always contained the higher amount of PHA (higher fluorescence intensity) and seemed to be the main responsible of the storage phenomena.

The microbial composition of reactor A1 was monitored by phase-contrast observation of the morphotypes present. This biomass appeared as large compact flocs composed of morphotype I cells, and rarely, tetrad-forming bacteria corresponding to morphotypes II/III were observed. No significant variations in the morphotypes were detected along the time of reactor operation. The presence and abundance of microorganisms belonging to the genera *Azoarcus*, *Thauera*, *Paracoccus* and *Amaricoccus* were investigated in this biomass by FISH analysis. *Thauera* and *Azoarcus* cells (morphotype I) constituted most of the microbial community being, respectively, 49.5 and 45.9% of EUBmix-positive cells. The genus *Paracoccus* was detected in low amount (data not shown). The main difference from reactor A was the almost complete disappearance of *Amaricoccus* genus (<1% EUBmix-positive cells) from this system. Nile blue staining also confirmed that, in this reactor, all the biomass was involved in PHA storage.

Discussion

The use of acetate or propionate as a carbon substrate and the application of diverse operating conditions (SRT and OLR) selected microbial populations with different composition and PHA storage performances.

In particular, the utilisation of different substrates led to the production of P(3HB) in SBR A and A1 and P(3HB-co-3HV) in SBR P. Acetate is the precursor of 3HB, while propionate, depending on the pathway, can originate monomers of 3HB and 3HV (Lemos et al. 2006). Biomass from reactor A presented substrate uptake rate (q_S , three times), PHA storage rate (q_P , 12 times) and polymers storage yield ($Y_{P/S}$, 2.5 times) higher than biomass from reactor P. The growth yield was slightly higher for sludge from reactor P ($Y_{X/S}$, 1.25 times) than for reactor A. The higher storage yield from acetate compared to that from propionate is partially explained by the fact that 3HB and 3HV synthesis from propionate requires decarboxylation, while 3HB synthesis from acetate does not. This was experimentally proven by feeding either acetate or propionate to the same enriched population (Lemos et al. 2006). Reactor A showed high PHA-specific productivities and PHA cell content. The latter (65.4% of cell dry weight) was obtained when acetate was supplied in three pulses of 60 C mmol/L each, being the highest value so far reported for mixed cultures (Serafim et al. 2004). In reactor P, the maximum PHA cell content obtained was lower, 41.2% of cell dry weight (unpublished results).

For the same substrate (acetate), changing the reactor SRT and organic loading rate resulted in different behaviour. In reactor A1, acetate and ammonia profiles along the feast and famine cycle were different from those observed for the SBR A (Serafim et al. 2004). In the former, ammonia was consumed at twice the rate observed in the reactor A. Despite the growth yield being slightly higher for A1 than for A, ammonia uptake rate (q_N) was faster. Operation of the reactor at SRT of 1 day selected faster-growing organisms than at SRT of 10 days. Specific acetate uptake and specific PHA storage rates were, respectively, three and four times lower with 1 day of SRT than with 10 days. The storage yield, for 1 day of SRT, was almost half of the value observed for 10 days. These results show that low values of SRT select biomass with a high specific growth rate but with low storage rate. Microscopic observation of biomass produced in SBR A1 appeared very slimy and resistant to India Ink diffusion, which are characteristics of EPS. Analytical determination of EPS showed a EPS yield on acetate of 0.07 C mmol glucose/C mmol S, which could explain the lower PHA polymer yield obtained in the biomass of reactor A1 compared with that of reactor A, where no EPS were detected. According to Cho et al. (2005), low values of SRT may favour EPS production by sludge.

The use of a short SRT (1 day against 10 days) and high OLR did not improve the biomass PHA storage capacity. Similar results were obtained by Beun et al. (2002), who estimated a decrease of the storage yield for SRT lower than 2 days.

The efficiency of the sorting/RT-PCR approach, previously applied for filamentous bacteria (Levantesi et al. 2006), was confirmed on these floc-former morphotypes. The most abundant of the targeted bacteria, morphotypes I and II, could be successfully identified analysing a restricted number of clones. Both *Thauera* and morphotype III cells, not retrieved with sorting/RT-PCR, were present in low number in the biomass.

The main microbial components of the analysed SBRs biocenosis were all previously found in activated sludge environment, and their storage capacities were reported. In particular, *Amaricoccus* spp. was detected in large number in wastewater treatment plants (WWTPs; Maszenan et al. 2000), and the high PHA storage capacity was confirmed (Falvo et al. 2001; Aulenta et al. 2003). The *Thauera/Azoarcus* group constituted 16% of the activated sludge biomass in a nitrifying–denitrifying industrial WWTP (Juretschko et al. 2002). The capacity of these bacteria to store PHA was reported in (Bergey's Manual 2005), and the presence of *Thauera* was already ascertained in a SBR for PHA production, although its involvement in lipid storage was not shown (Dionisi et al. 2006).

FISH analysis showed that bacteria belonging to the genera *Amaricoccus*, *Thauera* and *Azoarcus* were always present in reactors A and P. Clear differences in the abundance of these genera, which could be attributed to the kind of carbon source utilised, were, however, observed between the two reactors. As reported by Lemos et al. (2006), the different polymer composition produced as well as the kinetic and stoichiometric parameters calculated in these reactors, when the substrates supplied were shifted, could be explained on the basis of a diverse population composition of reactor A and P: propionate to population A and acetate to population P. Results indicated that the selection of *Thauera* spp. was favoured under ADF when acetate was present as a carbon source. While this genus was rarely observed in SBR P, it constituted almost half of the biomass in the two acetate reactors. *Thauera* was also enriched, in a SBR operated at a SRT of 1 day and under ADF conditions fed with acetate (Dionisi et al. 2005, 2006).

The use of propionate seemed, instead, to favour the development of *Amaricoccus* spp. Most of the species belonging to this genus are known to be able to use acetate and, a minor proportion, propionate as carbon source (Bergey's Manual 2005). *Amaricoccus kaplicensis* and *A. macauensis* are among the species able to use both substrates. As observed in the two samples of P reactor and as previously reported by Serafim et al. (2006), the bacterial composition of biomass was constant along the time of reactor operation, but the

relative abundance of each organisms varied. The dominance of the diverse genera in SBR A and P, in particular the selection between *Azoarcus* or *Amaricoccus*, seemed to be dependent not only on the substrate utilised but also on the reactor operational conditions. The major change in biomass composition was observed when the reactor SRT was reduced to 1 day and the OLR was duplicated. The latter conditions selected faster-growing organisms with lower storage capacity than those obtained at a SRT of 10 days. *Amaricoccus* was therefore washed out of SBR A1 (μ_{\max} of *A. kaplicensis* is 2.1–2.5 day⁻¹, Falvo et al. 2001).

A major challenge in the optimisation of the mixed culture PHA production process is the effective selection of cultures with high PHA storage capacity (high impact on PHA cell content) and growth rate (effect on the volumetric PHA production rate). In this work, the microbial population present in PHA accumulation processes was identified and correlated with the reactor-operating conditions. The application of microbiological and molecular techniques showed to be a useful tool to monitor the selection of target microorganisms. Cell sorting/RT-PCR was a valuable technique for the determination of the main species responsible for PHA production in the ADF SBRs used, and it can also be easily transferred for the analysis of any enrichment culture characterised by low biodiversity. Differently from other cell-sorting procedures (i.e. flow cytometry), it does not require sophisticated and expensive laboratory equipments and strongly limits the number of analysis to perform (i.e. low number of clones to screen).

The abundance of the different genera, *Amaricoccus*, *Thauera* and *Azoarcus*, where for some the presence was revealed by the cell sorting/RT-PCR approach, was indeed confirmed by quantitative FISH analysis. This is an important step forwards in the knowledge of this complex but most promising process.

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