

A Model Predictive Approach to Dynamic Control Law Design in Discrete-Time Uncertain Systems

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Abstract

A model predictive control (*MPC*) scheme is mainly developed in discrete-time uncertain systems. The control law contains a dynamic property in the proposed *MPC*. Hence, the *MPC* with a dynamic control policy is simply known as model predictive dynamic control (*MPDC*). To this end, a suitable matrix transformation is suggested to convert the *MPDC* problem into another optimization issue. Then, a systematic procedure based on linear matrix inequality (*LMI*) is addressed to the *MDPC* design. Hence, the *MPDC* synthesis is translated into an *LMI* minimization problem, which handles both constraints on the control inputs and plant outputs. The optimization problem can be numerically solved at each sample time through the well-known *LMI* solver. Then, the parameters of the dynamic controller would be automatically updated at each sample time. The method is applied in a discrete-time example to verify the effectiveness of the presented approach versus similar results.

Keywords MPC · LMI · Dynamic control law · Discrete-time uncertain systems

1 Introduction

Nowadays, model predictive control (*MPC*) has drawn the attention of many researchers and engineers [1, 20]. The *MPC* problem is initially investigated in a linear discrete-time system [3]. Some closed-form results have been addressed in simplified discrete-time systems [3]. These techniques have been used in industrial applications successfully [32, 36]. The commercial versions of the *MPC* include dynamic matrix control (*DMC*), predictive functional control (*PFC*), generalized predictive control (*GPC*), and the other *MPC* methods [5, 23, 27].

In the *MPC* methods, the plant behavior is anticipated at each sample time knowing the nominal model. Then, some control sequences are generated while a given

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cost function is minimized. The first input signal is applied to the plant and the others are discarded. Such a process is repeated at each sample time [24, 25]. In the mentioned scheme, a suitable control sequence is numerically computed at the sample time by some matrix calculations [3]. The *MPC* concept can also be used in various applications as well as chaotic systems synchronization [17] and constrained guidance system [29].

In the last decade, the linear matrix inequality (LMI) has been an efficient and powerful tool due to the huge progressive development in the matrix calculus. Hence, analysis tools and synthesis techniques based on the *LMI* have some advantages over the other ones [2, 28].

Most times, the stability checking and also control system design can be translated into an *LMI* feasibility or a minimization problem [10, 28]. A static gain is expressed as an *LMI* feasibility problem in the state feedback control design [28]. Such a static gain may be deliberately determined at each sample time [30]. In the mentioned *MPC*, some controller parameters like the gains are updated at each sample time rather than computing the whole control sequences.

An *LMI*-based *MPC* scheme is firstly addressed in discrete-time systems [16, 37]. In this method, both the prediction and control horizons tend to the infinity for obtaining an *LMI* representation. Thus, the *MPC* design is actually translated into a selection of some suitable static gains that are updated at each sample time. Then, a similar control problem has been formulated in linear systems subjected to actuator nonlinearity [33, 38], nonlinear systems [21, 22], constrained systems [7, 18], uncertain systems [8], networked control systems [31, 32, 42], parameter-varying systems [19], event-triggered systems [41] and time-delayed systems [11, 40]. Initially, the *MPC* is inherently suggested in control systems with a discrete-time representation, but the *MPC* formulation could also be extended into continuous-time systems [4, 9, 26].

A typical dynamic control system has various additional degrees of freedom rather than a static control policy. As a result, it is expected that the transient response is effectively compensated by the dynamic controller in comparison with the static control law. The static control design is restricted to a suitable gains selection in the state or output feedback structure. But, the problem formulation is increasingly complicated in the dynamic control design as well. Additionally, an extra cost should be paid due to the computational load. Therefore, a reasonable trade-off between the closed-loop performance and required computation time may be necessarily taken into account in the real-time systems. The raised issues are substantially reduced utilizing fast numerical optimization techniques. Consequently, the transient performance is progressively improved via predictive dynamic control. The existing *MPCs* are usually realized with a static control law. In this study, the *MPC*, in which the control law contains some state variables, is referred to as the model predictive dynamic control (*MPDC*).

Over the last decade, various *MPDC* methods have been developed in discretetime control systems. An *MPC* scheme has been designed in discrete-time systems through dynamic output feedback [6]. A discrete-time integral sliding-model predictive control addresses the dynamic lateral motion of autonomous driving vehicles [15]. By applying event-triggered dynamic output feedback, *MPC* is planned in uncertain fuzzy systems [35]. Then, by a predictive event-triggered strategy, a dynamic surface control is investigated in strict-feedback systems in the presence of network-induced delays [39]. The aforementioned control method may not be immediately applicable to a typical uncertain system.

Although the design of static control systems may follow the standard ways, synthesizing the dynamic control systems will have some major complexities. Hence, MPDC will be interested in uncertain dynamical systems. Lately, an MPDC has been derived in continuous-time uncertain systems [12]. In this method, a minimization problem subjected to some LMIs is solved at predefined sample times. Then, the parameters of the dynamic control are updated in realtime operation. The results of the continuous-time MPDC cannot be directly applied to the discrete-time systems due to the induced discretization error. Accordingly, it may destabilize and/or destroy the transient response of the closed-loop system. This point motivates the author to reformulate the MPDC problem for synthesizing an effective discrete-time control system in the presence of unstructured uncertainties. A matrix transformation is suggested to perform such a control goal. The presented MPDC can be expressed based on some LMI terms. Thus, the main contribution is concentrated on a robust MPDC formulation and synthesis in uncertain discrete-time systems. Hence, an LMI-based control technique is proposed to the MPDC design in uncertain control systems. The dynamic controller parameters can be automatically updated in real-time applications.

To tune the controller parameters, at each sample time, an *LMI* solver as well as *YALMIP*, *SEDUMI*, *SDPT3*, *MOSEK*, *LMILab* and so on may be used to handle the optimization problem numerically. Therefore, the stability and/or performance characteristic of the closed-loop system can be considerably improved via the *MPDC* when compared to the existing *MPC*.

The rest of the paper is organized as follows: In Sect. 2, some mathematical preliminaries and definitions are briefly addressed. The discrete-time *MPDC* problem is formulated in Sect. 3, and then, the main contribution is presented in Sect. 4. In Sect. 5, the results are used in a numerical simulation. Finally, some concluding remarks are presented in the last section.

2 Definitions and Mathematical Preliminaries

Hereafter, I_n is a $n \times n$ identity matrix and the operator $\|.\|$ is a two-norm of the given matrix. The Euclidean spaces \mathbb{R}, \mathbb{R}^n and $\mathbb{R}^{m \times n}$ are some well-known vector spaces. Thus, the set \mathbb{R} describes all real numbers, \mathbb{R}^n is the set of all real vectors that contain n elements, and $\mathbb{R}^{m \times n}$ is the set of all $m \times n$ real matrices. A symmetric matrix $\Theta \in \mathbb{R}^{n \times n}$ is positive definite if the condition $\vartheta^T \Theta \vartheta > 0$ satisfies for every non-zero $\vartheta \in \mathbb{R}^n$. Additionally, the matrix Θ is negative definite if $-\Theta$ is a positive definite matrix. The following mathematical lemmas are borrowed from the literature to make this study self-contained:

Lemma 1 For any symmetric matrices $Q \in \mathbb{R}^{s \times s}$, $R \in \mathbb{R}^{t \times t}$ and rectangular matrix $S \in \mathbb{R}^{s \times t}$, the following inequalities are equivalent:

1. R > 0 and $Q - SR^{-1}S^{T} > 0$ 2. Q > 0 and $R - S^{T}Q^{-1}S > 0$ 3. $\begin{bmatrix} Q & S \\ S^{T} & R \end{bmatrix} > 0$

Lemma 1 can be explicitly obtained by the Schur's matrix decomposition. Hence, it is referred to as the Schur's complement lemma [28].

Lemma 2 (Barbalat's lemma [14]) Let $\varphi(.) : R^+ \to R^+$ be a uniformly continuous Lebesgue measureable function on $[0, +\infty)$. If $\lim_{t\to+\infty} \int_0^t \varphi(\tau) d\tau$ exists, then $\lim_{t\to+\infty} \varphi(t) = 0$. In a similar way, if $\lim_{k\to+\infty} \sum_{i=0}^k \varphi(i)$ exists, then $\lim_{k\to+\infty} \varphi(k) = 0$.

These lemmas will be very useful in the proof of the main theorems.

3 Problem Setup

Consider a discrete-time plant described by the following difference equation:

$$\begin{cases} x_p(k+1) = A_p x_p(k) + B_p u(k) + f_p (x_p(k)) \\ y(k) = C_p x_p(k) \end{cases}$$
(1)

where $x_p(k) \in \mathbb{R}^{n_p}$ is the state vector, $y(k) \in \mathbb{R}^q$ is the output vector and $u(k) \in \mathbb{R}^p$ is the control input of the plant (1). The plant (1) can be imagined as an *LTI* system that is subjected to a nonlinear term $f_p(.)$. The control effort u(k) is inherently unknown and generated by the control law. In other words, the signal u(k) is not known in advance. It is numerically calculated via the proposed optimization problem. Furthermore, the uncertain system (1) may be stable or unstable in the open-loop structure. The following assumptions are considered to formulate the *MPDC* problem:

Assumption 1 Assume that the time-independent plant (1) is stabilizable. Thus, there exists a constrained control sequence u(k), $||u(k) - \overline{u}|| \le u_{\max}$ and $\overline{u} = \lim_{\substack{k \to +\infty \\ k \to +\infty}} u(k)$, such that the plant states $x_p(k)$ converge to its equilibrium point \overline{x} (i.e. $\lim_{\substack{k \to +\infty \\ k \to +\infty}} x_p(k) = \overline{x}$). Additionally, it is assumed that the states of the uncertain plant (1) are measurable for the control purpose.

Assumption 2 The nonlinear function $f_p(.)$ may be unknown, but it is zero at zero (i.e. $f_p(0) = 0$). The following inequality also holds:

$$\|f_p(\alpha) - f_p(\beta)\| \le L_p \|\alpha - \beta\|, \forall \alpha, \beta \in \mathbb{R}^{n_p}$$
(2)

The inequality (2) is known as the Lipschitz condition. The constant L_p is the maximum slope of the nonlinear term $f_p(.)$. The vector $f_p(.)$ can be fully unknown for the designer. Hence, the nonlinear function $f_n(.)$ is treated as an uncertain term. The exact value of the nonlinear term $f_n(.)$ is not necessary to be known for the proposed method. Although the uncertain system (1) is partially unknown, the control parameters are determined with only some certain values of the plant (1)as well as A_p , B_p , C_p and L_p .

The following dynamic control system may be used to regulate the plant (1):

$$\begin{cases} x_c(k+1) = A_c x_c(k) + B_c e(k) \\ u(k) = C_c x_c(k) + D_c e(k) \end{cases}$$
(3)

where $x_c(k) \in \mathbb{R}^{n_c}$ is the state vector of the control system (3) and also the term e(k) = r(k) - y(k) denotes the error signal. Thus, the set point r(k) is explicitly appeared in the error term e(k). Then, in order to regulate the plant output y(k), the controller (3) is designed such that the error signal is modified in a suitable way.

Assumption 3 For the sake of simplicity, the reference r(k) = r is assumed to be constant. Furthermore, the number of the controller states is equal to the number of plant state (i.e. $n_c = n_p = n$).

Let define the variable $x(k) \stackrel{\text{def}}{=} \left[x_p^T(k) x_c^T(k) \right]^T$. Then, the closed-loop system that contains the uncertain plant and controller can be written as:

$$\begin{cases} x(k+1) = Ax(k) + Br + f_N(x(k))\\ y(k) = Cx(k) \end{cases}$$

$$\tag{4}$$

where

$$A = \begin{bmatrix} A_p - B_p D_c C_p & B_p C_c \\ -B_c C_p & A_c \end{bmatrix}, B = \begin{bmatrix} B_p D_c \\ B_c \end{bmatrix}, C = \begin{bmatrix} C_p & 0 \end{bmatrix}, f_N(x(k)) = \begin{bmatrix} f_p(x_p(k)) \\ 0 \end{bmatrix}$$

The system matrix A can be decomposed as follows:

$$A = \begin{bmatrix} A_p & 0 \\ 0 & 0 \end{bmatrix} + \begin{bmatrix} 0 & B_p \\ I_n & 0 \end{bmatrix} \begin{bmatrix} A_c & B_c \\ C_c & D_c \end{bmatrix} \begin{bmatrix} 0 & I_n \\ -C_p & 0 \end{bmatrix}$$
(5)

Besides, the reference signal is a constant one, when the closed-loop system (4) is stable, the equilibrium point is found as:

$$\begin{cases} \bar{x} = A \bar{x} + Br + f(\bar{x}) \\ r = C \bar{x} \end{cases}$$
(6)

where $\lim_{k \to +\infty} x(k) = \lim_{k \to +\infty} x(k+1) = \bar{x}$. Let define a deviated variable like $\xi(k) \stackrel{\text{def}}{=} \left[\xi_p^T(k) \xi_c^T(k) \right]^T = x(k) - \bar{x}$. Then, the closed-loop plant model can be written as the following autonomous system:

$$\xi(k+1) = A\xi(k) + f(\xi(k)) \tag{7}$$

where the nonlinear term is defined as $f(\xi(k)) \stackrel{\text{def}}{=} f_N(x(k)) - f_N(\bar{x})$. Thus, the proposed control tries to handle the autonomous system (7).

To design the control system parameters, an infinite horizon cost function may be selected at sample time k as follows:

$$J(k) = \sum_{i=0}^{+\infty} \left(\left(\hat{x}_p(k+i|k) - \bar{x}_p \right)^T Q \left(\hat{x}_p(k+i|k) - \bar{x}_p \right) + \left(\hat{u}(k+i|k) - \bar{u} \right)^T R \left(\hat{u}(k+i|k) - \bar{u} \right) \right)$$
(8)

where $u = \lim_{k \to +\infty} u(k)$ and the weights $Q \in \mathbb{R}^{n \times n} \ge 0$ and $R \in \mathbb{R}^{p \times p} > 0$ are symmetric matrices.

In the cost function (8), the term $\hat{x}_p(k+i|k)$ is the predicted value of the plant states at time instant k + i with $\hat{x}_p(k|k) = x_p(k)$. The first computed control effort $\hat{u}(k+i|k)$ is applied to the plant (1) while the other input signals are discarded. The objective function (8) will enforce that the plant state and control input are converged to their steady-state values (i.e. \bar{x}_p and \bar{u}). Hence, the summation arguments will tend to zero.

The control signal u(k) is designed such that the cost function (8) is minimized in the *MPDC* problem. In Eq. (8), the prediction horizon tends to infinity. Hence, by using the Barbalat lemma, if the objective function (8) is bounded, then the plant states $x_p(k)$ are converged to a predefined value x_p (i.e. $\lim_{k \to +\infty} x_p(k) = \bar{x}_p$). Therefore, it implies $\lim_{k \to +\infty} e(k) = 0$ when considering Eq. (6). Although the objective function (8) explicitly depends on the plant states $x_p(k)$, the tracking error e(k) is implicitly considered in the control problem. In the control system (3), we have:

$$u(k) = C_{c}x_{c}(k) + D_{c}(r - C_{p}x_{p}(k))$$
(9)

Then, the cost function (8) may be rewritten as:

$$J(k) = \sum_{i=0}^{+\infty} \widehat{\xi}^T(k+i|k) \Phi \widehat{\xi}(k+i|k)$$
(10)

where

$$\Phi = \begin{bmatrix} Q + C_p^T D_c^T R D_c C_p & -C_p^T D_c^T R C_c \\ -C_c^T R D_c C_p & C_c^T R C_c \end{bmatrix}$$
(11)

The weight matrix Φ can be decomposed as follows:

$$\Phi = \begin{bmatrix} Q & 0 \\ 0 & 0 \end{bmatrix} + \begin{bmatrix} C_p^T D_r^T \\ -C_c^T \end{bmatrix} R \begin{bmatrix} D_c C_p & -C_c \end{bmatrix}$$
(12)

The *MPDC* design is subsequently presented in discrete-time systems.

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4 Main Results

An *LMI*-based approach is developed to find the parameters of a dynamic control system (3). Hence, the controller parameters can be obtained via the solution of an *LMI* minimization problem with a systematic procedure.

Theorem 1 Suppose that the assumptions 1–3 are held and $A \in \mathbb{R}^{2n}$ and $\Phi \in \mathbb{R}^{2n}$ are two known matrices. At time instant k, if there exists a symmetric positive definite matrix $P \in \mathbb{R}^{2n}$ and a positive constant γ such that the following minimization problem is feasible:

Min γ

subject to

^

$$A^{T}PA + L_{p}\left(PA + A^{T}P\right) + \left(L_{p}^{2} - 1\right)P + \Phi \le 0$$

$$\tag{13}$$

$$\xi^T(k)P\xi(k) \le \gamma \tag{14}$$

then, the closed-loop system (4) is asymptotically stabilized with the control law (3), and also, the minimized value γ is an upper bound for the cost function (8).

Proof Consider a quadratic Lyapunov function like $V(k) = \hat{\xi}^T(k)P\hat{\xi}(k)$ and its difference as $\Delta V(k) = V(k+1) - V(k)$. Let pre-multiply the inequality (13) by the vector $\hat{\xi}^T(k+i|k)$ and post-multiply it by the vector $\hat{\xi}(k+i|k)$. Then,

$$\hat{\xi}^{T}(k+i|k) \Big(A^{T}PA + L_{p} \big(PA + A^{T}P \big) + L_{p}^{2}P \Big) \hat{\xi}(k+i|k) \le \hat{\xi}^{T}(k+i|k)(P-\Phi)\hat{\xi}(k+i|k)$$
(15)

The following inequalities can be found by applying the inequality (2):

$$\begin{cases} f^{T}\left(\widehat{\xi}(k+i|k)\right)Pf\left(\widehat{\xi}(k+i|k)\right) \leq L_{p}^{2}\widehat{\xi}^{T}(k+i|k)P\widehat{\xi}(k+i|k)\\ \widehat{\xi}^{T}(k+i|k)A^{T}Pf\left(\widehat{\xi}(k+i|k)\right) \leq L_{p}\widehat{\xi}^{T}(k+i|k)A^{T}P\widehat{\xi}(k+i|k)\\ f^{T}\left(\widehat{\xi}(k+i|k)\right)PA\widehat{\xi}(k+i|k) \leq L_{p}\widehat{\xi}^{T}(k+i|k)PA\widehat{\xi}(k+i|k) \end{cases}$$
(16)

Using the condition (16), an upper bound of the following inequality can be obtained:

$$\begin{aligned} \left(A\hat{\xi}(k+i|k) + f\left(\hat{\xi}(k+i|k)\right)\right)^T P\left(A\hat{\xi}(k+i|k) + f\left(\hat{\xi}(k+i|k)\right)\right) \\ &\leq \hat{\xi}^T(k+i|k) \left(A^T P A + L_p \left(P A + A^T P\right) + L_p^2 P\right) \hat{\xi}(k+i|k) \\ &\leq \hat{\xi}^T(k+i|k) (P - \Phi) \hat{\xi}(k+i|k) \end{aligned}$$
(17)

Therefore, inequality (17) can be found as:

$$\left(A\hat{\xi}(k+i|k) + f\left(\hat{\xi}(k+i|k)\right) \right)^T P\left(A\hat{\xi}(k+i|k) + f\left(\hat{\xi}(k+i|k)\right) \right) - \hat{\xi}^T(k+i|k) P\hat{\xi}(k+i|k) + \hat{\xi}^T(k+i|k) \Phi\hat{\xi}(k+i|k) \le 0$$
 (18)

Then, by using Eq. (7), the inequality (18) can be written as follows:

$$\hat{\xi}^{T}(k+i+1|k)P\hat{\xi}(k+i+1|k) - \hat{\xi}^{T}(k+i|k)P\hat{\xi}(k+i|k) + \hat{\xi}^{T}(k+i|k)\Phi\hat{\xi}(k+i|k) \le 0$$
(19)

Therefore, the inequality (13) implies that the following condition holds at any time instant *k*:

$$\Delta V(k+i|k) = V(k+i+1|k) - V(k+i|k) \le -\hat{\xi}^T(k+i|k)\Phi\hat{\xi}(k+i|k)$$
(20)

Then, at time instant k, by taking summation from both sides of the inequality (20) from i = 0 to infinity, we have:

$$\lim_{i \to +\infty} V(k+i+1|k) - V(k|k) \le -J(k)$$
(21)

The Barbalat's lemma implies $\lim V(k + i + 1|k) = 0$. Then,

$$J(k) \le \xi^T(k) P\xi(k) \tag{22}$$

The cost function J(k) has an upper bound like γ by considering the condition (22) at time instant k. The minimum γ could be obtained by a suitable selection of the matrix P.

In Theorem 1, two matrices A and Φ are explicitly dependent on the controller parameters (A_c, B_c, C_c, D_c) . The matrices A and Φ are not completely known. Thus, the control design problem may have some complexities. But, an innovative matrix transformation is suggested to translate the *MPDC* problem into an *LMI* optimization one. Hence, the controller parameters are directly computed at each sample time in the next theorem.

Theorem 2 Suppose that the assumptions 1–3 are held simultaneously. At time instant k, if there exists two symmetric positive definite matrices $X, Y, U, V \in \mathbb{R}^{n \times n}$ and some compatible matrices $K \in \mathbb{R}^{n \times n}, L \in \mathbb{R}^{n \times p}, M \in \mathbb{R}^{q \times n}, N \in \mathbb{R}^{q \times p}$ and a positive constant γ such that following minimization problem is feasible:

$$\begin{array}{l}
\text{Min } \gamma \\
\text{subject to} \\
\left[\begin{array}{c} Y & I_n \\
I_n & X \end{array}\right] > 0
\end{array}$$
(23)

$$\begin{bmatrix} Y & * & * \\ I_n & X & * \\ M & -NC_p & u_{max}^2 I_p \end{bmatrix} \ge 0$$
(24)

$$\begin{bmatrix} Y & V & \xi_p(k) \\ * & Y & \xi_c(k) \\ * & * & 1 \end{bmatrix} \ge 0$$
(25)

where the star symbol * denotes the matrix symmetry and also the matrices \mathcal{M}_{11} , \mathcal{M}_{12} , \mathcal{M}_{13} , \mathcal{M}_{14} , \mathcal{M}_{22} and \mathcal{M}_{24} are defined as follows:

$$\begin{pmatrix}
\mathcal{M}_{11} \stackrel{\text{def}}{=} \left(1 - L_p^2\right)Y - L_p\left(A_pY + B_pM + YA_p^T + M^TB_p^T\right) \\
\mathcal{M}_{12} \stackrel{\text{def}}{=} \left(1 - L_p^2\right)I_n - L_p\left(A_p - B_pNC_p + A_p^T - C_p^TN^TB_p^T\right) \\
\mathcal{M}_{13} \stackrel{\text{def}}{=} A_pY + B_pM \\
\mathcal{M}_{14} \stackrel{\text{def}}{=} A_p - B_pNC_p \\
\mathcal{M}_{22} \stackrel{\text{def}}{=} \left(1 - L_p^2\right)X - L_p\left(XA_p - LC_p + A_p^TX - C_p^TL^T\right) \\
\mathcal{M}_{24} \stackrel{\text{def}}{=} XA_p - LC_p
\end{cases}$$
(27)

Then, by means of the dynamic control law (3) with the following parameters:

$$A_{c} = U^{-1} \left(K - XA_{p}Y + LC_{p}Y - XB_{p}M - XB_{p}NC_{p}Y \right) V^{-1}$$
(28)

$$B_c = U^{-1}(L - XB_pN) \tag{29}$$

$$C_c = (M + NC_P Y)V^{-1}$$
(30)

$$D_c = N \tag{31}$$

where

$$\begin{cases} U = X (I_n - X^{-1} Y^{-1})^{\frac{1}{2}} \\ V = - (I_n - X^{-1} Y^{-1})^{\frac{1}{2}} Y \end{cases}$$
(32)

The uncertain plant (1) is asymptotically stabilized while the minimized value γ is an upper bound for the cost function (8).

Proof The matrix *P* is a symmetric positive definite one. Let partition *P* as follows:

$$P = \gamma \begin{bmatrix} X & U \\ U & X \end{bmatrix}$$
(33)

The Schur's complement lemma implies that the matrices X must be positive definite. The inverse of the matrix P is also symmetric positive definite. It can be written as:

$$P^{-1} = \gamma^{-1} \begin{bmatrix} Y & V \\ V & Y \end{bmatrix}$$
(34)

where

$$\begin{cases} XY + UV = I_n \\ XV + UY = 0 \\ XY = YX \\ UY = YU \end{cases}$$
(35)

The Schur's complement lemma implies that Y must be positive definite matrices. It is not hard to show that the matrices U and V in term of X and Y can be computed as:

$$\begin{cases} U = X (I_n - X^{-1}Y^{-1})^{\frac{1}{2}} \\ V = -(I_n - X^{-1}Y^{-1})^{\frac{1}{2}}Y \end{cases}$$
(36)

Consider another invertible symmetric matrix Ψ as follows:

$$\Psi = \begin{bmatrix} Y & V \\ V & 0 \end{bmatrix}$$
(37)

The matrix Ψ can be decomposed as:

$$\Psi = \begin{bmatrix} I_n & 0\\ 0 & V \end{bmatrix} \begin{bmatrix} Y & I_n\\ I_n & 0 \end{bmatrix} \begin{bmatrix} I_n & 0\\ 0 & V \end{bmatrix}$$
(38)

Let define two matrices Λ and Ω as follows:

$$\Lambda \stackrel{\text{\tiny def}}{=} \begin{bmatrix} I_n & 0\\ 0 & V \end{bmatrix}, \Omega \stackrel{\text{\tiny def}}{=} \begin{bmatrix} Y & I_n\\ I_n & 0 \end{bmatrix}$$
(39)

The inverse of the matrix Ψ may be computed as:

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$$\Psi^{-1} = \begin{bmatrix} 0 & V^{-1} \\ V^{-1} & -V^{-1}YV^{-1} \end{bmatrix} = \begin{bmatrix} I_n & 0 \\ 0 & V^{-1} \end{bmatrix} \begin{bmatrix} 0 & I_n \\ I_n & -Y \end{bmatrix} \begin{bmatrix} I_n & 0 \\ 0 & V^{-1} \end{bmatrix}$$
(40)

Besides the matrix *P* is symmetric positive definite, the matrix $\Psi P \Psi$ is also symmetric and positive definite. Then, the condition (23) may be obtained as follows:

$$\Psi P \Psi = \gamma \begin{bmatrix} Y & V \\ V & VXV \end{bmatrix} = \gamma \begin{bmatrix} I_n & 0 \\ 0 & V \end{bmatrix} \begin{bmatrix} Y & I_n \\ I_n & X \end{bmatrix} \begin{bmatrix} I_n & 0 \\ 0 & V \end{bmatrix} > 0$$
(41)

Therefore,

$$A^{T}PA + L_{p}(PA + A^{T}P) + (L_{p}^{2} - 1)P + \Phi \le 0$$
(42)

Let pre- and post-multiply both sides of the inequality (42) by the matrix Ψ . Then

$$\Psi A^T P A \Psi + L_p \Psi P A \Psi + L_p \Psi A^T P \Psi + (L_p^2 - 1) \Psi P \Psi + \Psi \Phi \Psi \le 0$$
(43)

The inequality (43) may be compactly rewritten as follows:

$$\left(1 - L_p^2\right)\Psi P\Psi - L_p\Psi PA\Psi - L_p\Psi A^T P\Psi - (\Psi PA\Psi)^T (\Psi P\Psi)^{-1}\Psi PA\Psi - \Psi \Phi\Psi \ge 0$$
(44)

The controller parameters (A_c, B_c, C_c, D_c) in terms of the matrices (K, L, M, N) can be found as:

$$\begin{bmatrix} A_c & B_c \\ C_c & D_c \end{bmatrix} = \begin{bmatrix} U & XB_p \\ 0 & I_p \end{bmatrix}^{-1} \begin{bmatrix} K - XA_pY & L \\ M & N \end{bmatrix} \begin{bmatrix} V & 0 \\ -C_pY & I_q \end{bmatrix}^{-1}$$
(45)

The controller parameters could be simplified as follows:

$$\begin{cases}
A_{c} = U^{-1} \left(K - XA_{p}Y + LC_{p}Y - XB_{p}M - XB_{p}NC_{p}Y \right) V^{-1} \\
B_{c} = U^{-1} \left(L - XB_{p}N \right) \\
C_{c} = \left(M + NC_{p}Y \right) V^{-1} \\
D_{c} = N
\end{cases}$$
(46)

It is evident that the matrices (K, L, M, N) in terms of the controller parameters (A_c, B_c, C_c, D_c) are expressed as:

$$\begin{bmatrix} K & L \\ M & N \end{bmatrix} = \begin{bmatrix} U & XB_p \\ 0 & I_p \end{bmatrix} \begin{bmatrix} A_c & B_c \\ C_c & D_c \end{bmatrix} \begin{bmatrix} V & 0 \\ -C_p Y & I_q \end{bmatrix} + \begin{bmatrix} XA_p Y & 0 \\ 0 & 0 \end{bmatrix}$$
(47)

In inequality (43), the term $\Psi \Phi \Psi$ is computed as follows:

$$\Psi\Phi\Psi = \begin{bmatrix} Y & V \\ -M & NC_p V \end{bmatrix}^T \begin{bmatrix} Q & 0 \\ 0 & R \end{bmatrix} \begin{bmatrix} Y & V \\ -M & NC_p V \end{bmatrix}$$
(48)

Then,

$$\Psi\Phi\Psi = \begin{bmatrix} I_n & 0\\ 0 & V \end{bmatrix} \begin{bmatrix} Y & I_n\\ -M & NC_p \end{bmatrix}^T \begin{bmatrix} Q & 0\\ 0 & R \end{bmatrix} \begin{bmatrix} Y & I_n\\ -M & NC_p \end{bmatrix} \begin{bmatrix} I_n & 0\\ 0 & V \end{bmatrix}$$
(49)

and also the term $\Psi PA\Psi$ can be obtained as:

$$\Psi PA\Psi = \gamma \begin{bmatrix} A_p Y + B_p M & A_p V - B_p N C_p V \\ V K & V X A_p V - V L C_p V \end{bmatrix}$$
(50)

It can be decomposed as follows:

$$\Psi PA\Psi = \gamma \begin{bmatrix} I_n & 0\\ 0 & V \end{bmatrix} \begin{bmatrix} A_p Y + B_p M & A_p - B_p N C_p\\ K & X A_p - L C_p \end{bmatrix} \begin{bmatrix} I_n & 0\\ 0 & V \end{bmatrix}$$
(51)

Let pre- and post-multiply both sides of the inequality (44) by the matrix Λ^{-1} . Then

$$\begin{pmatrix} 1 - L_p^2 \end{pmatrix} \begin{bmatrix} Y & I_n \\ I_n & X \end{bmatrix} - L_p \begin{bmatrix} A_p Y + B_p M & A_p - B_p N C_p \\ K & X A_p - L C_p \end{bmatrix}$$
$$- L_p \begin{bmatrix} A_p Y + B_p M & A_p - B_p N C_p \\ K & X A_p - L C_p \end{bmatrix}^T - \gamma^{-1} \begin{bmatrix} Y & I_n \\ -M & N C_p \end{bmatrix}^T \begin{bmatrix} Q & 0 \\ 0 & R \end{bmatrix} \begin{bmatrix} Y & I_n \\ -M & N C_p \end{bmatrix}$$
$$- \begin{bmatrix} A_p Y + B_p M & A_p - B_p N C_p \\ K & X A_p - L C_p \end{bmatrix}^T \begin{bmatrix} Y & I_n \\ I_n & X \end{bmatrix}^{-1} \begin{bmatrix} A_p Y + B_p M & A_p - B_p N C_p \\ K & X A_p - L C_p \end{bmatrix}$$
(52)

Therefore, the condition (26) is obtained by applying the Schur's complement lemma. At each sample time k, the Lyapunov stability theorem can lead to the following condition:

$$J(k) < \xi^T(k) P \xi(k) \le \gamma \tag{53}$$

It can be modified as:

$$\xi^{T}(k) \begin{bmatrix} Y & V \\ V & Y \end{bmatrix}^{-1} \xi(k) \le 1$$
(54)

Then, the inequality (25) is found by applying the Schur's lemma. The control effort u(k) is written as:

$$v(k) = u(k) - \overline{u} = \left[-D_c C_p \ C_C \right] \xi(k)$$
(55)

The two-norm of the deviated control signal v(k) is computed as:

$$\|v(k)\|^{2} = \xi^{T}(k) \left[-D_{c}C_{p} \ C_{C} \right]^{T} \left[-D_{c}C_{p} \ C_{C} \right] \xi(k)$$
(56)

Equation (56) can be written as follows:

$$\|v(k)\|^{2} = \xi^{T}(k) \left[-NC_{p} \left(M + NC_{P}Y \right) V^{-1} \right]^{T} \left[-NC_{p} \left(M + NC_{P}Y \right) V^{-1} \right] \xi(k)$$
(57)

The following matrix decomposition is used to find an upper bound:

$$\left[-NC_{p} \left(M+NC_{p}Y\right)V^{-1}\right] = \left[M - NC_{p}\right] \left[\begin{matrix} 0 & V^{-1} \\ I_{n} & -YV^{-1} \end{matrix}\right]$$
(58)

The condition (57) can be rewritten as:

$$\|v(k)\|^{2} = \xi^{T}(k) \begin{bmatrix} 0 & V^{-1} \\ I_{n} & -YV^{-1} \end{bmatrix}^{T} \begin{bmatrix} M & -NC_{p} \end{bmatrix}^{T} \begin{bmatrix} M & -NC_{p} \end{bmatrix} \begin{bmatrix} 0 & V^{-1} \\ I_{n} & -YV^{-1} \end{bmatrix} \xi(k)$$
(59)

It is easy to check that the following decomposition is valid:

$$\begin{bmatrix} Y & I_n \\ I_n & X \end{bmatrix} = \begin{bmatrix} Y & V \\ I_n & 0 \end{bmatrix} \begin{bmatrix} Y & V \\ V & Y \end{bmatrix}^{-1} \begin{bmatrix} Y & I_n \\ V & 0 \end{bmatrix}$$
(60)

Using the Schur's lemma, one may have:

$$\begin{bmatrix} M & -NC_p \end{bmatrix}^T \begin{bmatrix} M & -NC_p \end{bmatrix} \le u_{\max}^2 \begin{bmatrix} Y & I_n \\ I_n & X \end{bmatrix} = u_{\max}^2 \begin{bmatrix} Y & V \\ I_n & 0 \end{bmatrix} \begin{bmatrix} Y & V \\ V & Y \end{bmatrix}^{-1} \begin{bmatrix} Y & I_n \\ V & 0 \end{bmatrix}$$
(61)

Let pre- and post-multiply the inequality (61) by the following matrices, respectively:

$$\begin{bmatrix} Y & V \\ I_n & 0 \end{bmatrix}^{-1} = \begin{bmatrix} 0 & I_n \\ V^{-1} & -V^{-1}Y \end{bmatrix} \text{ and } \begin{bmatrix} Y & I_n \\ V & 0 \end{bmatrix}^{-1} = \begin{bmatrix} 0 & V^{-1} \\ I_n & -YV^{-1} \end{bmatrix}$$
(62)

The inequality (61) could be simplified as follows:

$$\left[-NC_{p}\left(M+NC_{P}Y\right)V^{-1}\right]^{T}\left[-NC_{p}\left(M+NC_{P}Y\right)V^{-1}\right] \leq u_{\max}^{2}\left[\begin{array}{c}Y & V\\ V & Y\end{array}\right]^{-1} (63)$$

Then, the control sequence ||v(k)|| may be an upper-bounded using the condition (57).

$$\|v(k)\|^{2} \le u_{\max}^{2} \xi^{T}(k) \begin{bmatrix} Y & V \\ V & Y \end{bmatrix}^{-1} \xi(k) \le u_{\max}^{2}$$
(64)

It completes the proof.

Remark 1 The inequality (26) is used while both matrices Q and R are invertible. Sometimes, the matrix Q may not be invertible. Hence, the symmetric matrices Q and R could be decomposed by means of the Cholesky factorization technique as follows [34]:

$$\begin{cases} Q = Q_{ch}^T \times Q_{ch} \\ R = R_{ch}^T \times R_{ch} \end{cases}$$
(65)

where the terms Q_{ch} and R_{ch} are some unique triangular matrices. Then, the condition (26) could be interchanged with the following *LMI*:

$$\begin{vmatrix} \mathcal{M}_{11} & \mathcal{M}_{12} & \mathcal{M}_{13} & \mathcal{M}_{14} & YQ_{ch} & -M^T R_{ch} \\ * & \mathcal{M}_{22} & K & \mathcal{M}_{24} & Q_{ch} & C_p^T N^T R_{ch} \\ * & * & Y & I_n & 0 & 0 \\ * & * & * & X & 0 & 0 \\ * & * & * & * & \gamma I_n & 0 \\ * & * & * & * & * & \gamma I_n \end{vmatrix} \ge 0$$

$$(66)$$

The other matrix factorization techniques like diagonalization procedure may be also used to tackle such difficulty. The matrices Q and R are decomposed via the diagonalization method as follows [34]:

$$\begin{cases} Q = Q^{\frac{1}{2}} \times Q^{\frac{1}{2}} \\ R = R^{\frac{1}{2}} \times R^{\frac{1}{2}} \end{cases}$$
(67)

where the terms $Q^{\frac{1}{2}}$ and $R^{\frac{1}{2}}$ are the square root of the matrices Q and R, respectively. Then, the *LMI* condition (26) is interchanged with the following *LMI*:

Remark 2 The plant output y(k) norm may admit an upper bound like y_{max} (i.e. $||y(k) - r|| < y_{max}$). Such inequality can be written as follows:

$$\begin{bmatrix} I & C_p \xi_p(k) \\ * & y_{\max}^2 \end{bmatrix} > 0$$
(69)

In Theorem 2, the inequality (69) can be added to the *LMI* sets (23)–(26) to guarantee that the output constraint is satisfied.

Remark 3 The *MPDC* may outperform the other *MPCs* in terms of the performance cost. But, its computational demand to solve the *MPDC* optimization problem seems harder than the other *MPC*. In the discrete-time control implementation, there is enough time to compute the controller parameters by solving the *LMI* minimization problem. The optimization issue is typically solved in less than 0.1 s in the proposed method. Hence, such a problem can be handled in practical applications.

Remark 4 The minimization of the quadratic performance index (8) subject to some plant constraints is the main objective of the *MPDC* approach. Thus, the

optimization of the objective function (8) is only taken into account in the *MPDC* design rather than in the other control requirements. Therefore, various practical issues, as well as the actuator life cycle problem (control input rate), can also be considered in the cost function to achieve a more efficient control scheme.

Remark 5 The optimization problem of Theorem 2 may be solved at each sample time. The results of Theorem 2 can also be used to design a robust optimal control in the uncertain system (1). Hence, the cost function can be written as follows:

$$J = \sum_{k=0}^{+\infty} \left(\left(x_p(k) - \bar{x}_p \right)^T Q \left(x_p(k) - \bar{x}_p \right) + \left(u(k) - \bar{u} \right)^T R \left(u(k) - \bar{u} \right) \right)$$
(70)

The proposed optimization problem is solved in an off-line way when the initial conditions of the uncertain plant (1) are known. Therefore, an off-line dynamic control system may be obtained in an uncertain system (1).

Remark 6 In Assumption 1, it is supposed that the states of the uncertain system (1) have to be measurable to the control designer. But, some parts of the states may not be available in real-time implementations. In this case, an extra (full or reduced order) observer block can be incorporated to estimate the non-measured states of the uncertain system (1). Nevertheless, an additional error is induced regarding the transient response of the estimator dynamic. Consequently, in the case of the non-measured states, the raised issue could be handled if the output feedback *MPDC* is derived for the uncertain system (1).

5 Simulation Results

Consider the following discrete-time system [13]:

$$\begin{cases} x_p(k+1) = \begin{bmatrix} 0.9 & 0.8 & 0.1 \\ -0.1 & 0.7 & 0.2 \\ -0.2 & -0.4 & -0.2 \end{bmatrix} x_p(k) + \begin{bmatrix} 0 \\ 0 \\ 1 \end{bmatrix} u(k) + \frac{1}{2 + x_3^2(k)} \begin{bmatrix} 0 \\ x_1(k) \\ x_2(k) \end{bmatrix}$$
(71)
$$y_p(k) = \begin{bmatrix} 1 & 0 & 0 \end{bmatrix} x_p(k)$$

The initial conditions of the plant (71) and the controller states are chosen as $x_p(0) = \begin{bmatrix} 1 & 2 & 1 \end{bmatrix}^T$ and $x_c(0) = \begin{bmatrix} 0 & 0 & 0 \end{bmatrix}^T$, respectively. Recently, two *LMI*-based *MPC* algorithms have been suggested to regulate the uncertain plant (1). They include the discrete-time *MPC* [13] and the continuous-time *MPDC* [12]. In order to implement the continuous-time *MPDC*, a continuous-time form of the nonlinear system (1) may be approximated via the Euler backward method as follows:

$$\dot{x}_p = A_p^c x_p + f_p^c \left(x_p \right) + B_p^c u \tag{72}$$

| Performance index | Proposed control | Discrete-time MPC | Continuous-time MPDC |
|-------------------|------------------|-------------------|----------------------|
| J_0 | 60.1201 | 69.2362 | 80.1314 |

Table 1 The comparison of the performance indexes



Fig. 1 The applied control signal u(k)

where $A_p^c = \frac{1}{T}(A_p - I_n)$, $B_p^c = \frac{1}{T}B_p$, $f_p^c(.) = \frac{1}{T}f_p(.)$ and *T* denote the sample time. The discrete-time *MPC* is applied as $u(k) = F(k)x_p(k)$. The gain F(k) is updated at sample time with the solution of a minimization problem.

Hence, the simulation results are compared to the mentioned *MPC* methods with the same Q and R weights. The weight matrices are selected as $Q = I_3$ and R = 1. Then, it is assumed that the control input affects the performance index the same as the plant states. The weights Q and R are some invertible matrices. Hence, no factorization is necessary.

The results of Theorem 2 is applied to the *MPDC* design while the constraint on the control input sets as $|u(k)| \le 0.5$. In the numerical simulation, the reference signal is assumed to be zero and the sample time is selected as 1 s. The control and prediction horizons tend to infinity. The optimization problem is numerically solved via the *LMILab*. Then, the *MPCs* parameters are updated at each sample time. The following quadratic cost function is considered as the performance index:

$$J_0 = \sum_{k=0}^{+\infty} x_p(k)^T Q x_p(k) + u(k)^T R u(k)$$
(73)

The performance criterion can be evaluated by applying Theorem 2. The comparative results are shown in Table 1. Thus, the controllers are designed while the cost function J_0 is minimized as well.



Fig. 2 The first state of the plant $x_1(k)$



Fig. 3 The second state of the plant $x_2(k)$

The generated control signal u(k) is plotted in Fig. 1. The states of the example are also illustrated in Figs. 2, 3 and 4. The cost value upper bound γ at each sample time is depicted in Fig. 5. It is seen that the state deviations of the uncertain plant (71) are considerably small via the suggested predictive control compared to the other control techniques. The simulation results are demonstrated in Figs. 1–5 and Table 1 by using the proposed and existing *MPCs*.



Fig. 4 The third state of the plant $x_3(k)$



Fig. 5 The upper bound of the cost function γ

As a consequence, the outcomes verify the performance improvement of the closed-loop system compared to the other predictive control methods. Therefore, the control goals are accomplished by the presented *MPDC* in the discrete-time systems by considering the system uncertainty and the given control constraint.

6 Conclusion

The *MPDC* design is investigated in the discrete-time uncertain systems. A quadratic objective function is selected as the control design requirement. Then, a matrix transformation is used to express the results in terms of some *LMI*'s. It is shown that the *MPDC* synthesis can be translated into another *LMI* minimization problem by using the matrix transformation. The dynamic controller parameters are updated at each sample time via the solution of the optimization problem. The procedure is applied to a discrete-time example to demonstrate the effectiveness of the proposed approach versus the existing results. The efficiency of the suggested *MPDC* is numerically shown in terms of the control and transient performances.

References

- 1. F. Allgöwer, A. Zheng, Nonlinear Model Predictive Control (Springer, Basel, 2012)
- S. Boyd, L. El Ghaoui, E. Feron, V. Balakrishnan, *Linear Matrix Inequalities in System and Control Theory* (SIAM, Pennsylvania, 1994)
- 3. E.F. Camacho, C.B. Alba, *Model predictive control*, 2nd edn. (Springer Science & Business Media, London, 2013)
- M. Cannon, B. Kouvaritakis, Infinite horizon predictive control of constrained continuous-time linear systems. Automatica 36(7), 943–955 (2000)
- P. Chalupa, J. Novák, P. Januška, State space MPC using state observers. Int. J. Circuits Syst. Signal Process. 8, 9–14 (2014)
- Q.-X. Chen, L. Yu, Robust model predictive control for uncertain discrete time-delay systems via dynamic output feedback. Kongzhi Lilun Yu Yinyong/Control Theory Appl. 23(3), 401–406 (2007)
- F.A. Cuzzola, J.C. Geromel, M. Morari, An improved approach for constrained robust model predictive control. Automatica 38(7), 1183–1189 (2002)
- D.M. De la Pena, D.R. Ramírez, E.F. Camacho, T. Alamo, Explicit solution of min-max MPC with additive uncertainties and quadratic criterion. Syst. Control Lett. 55(4), 266–274 (2006)
- B. De Schutter, T.J. van den Boom, MPC for continuous piecewise-affine systems. Syst. Control Lett. 52(3–4), 179–192 (2004)
- M. Elloumi, M. Ghamgui, D. Mehdi, F. Tadeo, M. Chaabane, Stabilization of 2D Singular Systems: A Strict LMI Approach. Circuits Syst. Signal Process. 38(7), 3041–3057 (2019)
- 11. R.M. Esfanjani, S. Nikravesh, Stabilizing model predictive control for constrained nonlinear distributed delay systems. ISA Trans. **50**(2), 201–206 (2011)
- 12. V. Ghaffari, A robust control system scheme based on model predictive controller (MPC) for continuous-time systems. Optim. Control Appl. Methods **38**(6), 1032–1041 (2017)
- 13. V. Ghaffari, S.V. Naghavi, A. Safavi, Robust model predictive control of a class of uncertain nonlinear systems with application to typical CSTR problems. J. Process Control **23**(4), 493–499 (2013)
- 14. H. Khalil, Nonlinear Systems, 3rd edn. (Upper Saddle River, New Jersey, 2002)
- D.J. Kim, C.M. Kang, S.-H. Lee, C.C. Chung, Discrete-time integral sliding model predictive control for dynamic lateral motion of autonomous driving vehicles. in *Annual American Control Conference (ACC) 2018*, pp. 4757–4763
- 16. M.V. Kothare, V. Balakrishnan, M. Morari, Robust constrained model predictive control using linear matrix inequalities. Automatica **32**(10), 1361–1379 (1996)
- 17. Z. Longge, L. Xiangjie, The synchronization between two discrete-time chaotic systems using active robust model predictive control. Nonlinear Dyn. **74**(4), 905–910 (2013)
- 18. L. Lu, Y. Zou, Y. Niu, Event-driven robust output feedback control for constrained linear systems via model predictive control method. Circuits Syst. Signal Process. **36**(2), 543–558 (2017)
- 19. Y. Lu, Y. Arkun, Quasi-min-max MPC algorithms for LPV systems. Automatica 36(4), 527–540 (2000)

- M. Morari, J.H. Lee, Model predictive control: past, present and future. Comput. Chem. Eng. 23(4), 667–682 (1999)
- G. Pannocchia, J.B. Rawlings, S.J. Wright, Conditions under which suboptimal nonlinear MPC is inherently robust. Syst. Control Lett. 60(9), 747–755 (2011)
- 22. N. Poursafar, H.D. Taghirad, M. Haeri, Model predictive control of non-linear discrete time systems: a linear matrix inequality approach. IET Control Theory Appl. 4(10), 1922–1932 (2010)
- S.J. Qin, T.A. Badgwell, A survey of industrial model predictive control technology. Control Eng. Pract. 11(7), 733–764 (2003)
- 24. J.B. Rawlings, Tutorial overview of model predictive control. IEEE Control Syst. 20(3), 38–52 (2000)
- 25. M. Razi, M. Haeri, Efficient algorithms for online tracking of set points in robust model predictive control. Int. J. Syst. Sci. **48**(8), 1635–1645 (2017)
- M. Reble, F. Allgöwer, Unconstrained model predictive control and suboptimality estimates for nonlinear continuous-time systems. Automatica 48(8), 1812–1817 (2012)
- 27. J. Richalet, Industrial applications of model based predictive control. Automatica **29**(5), 1251–1274 (1993)
- 28. C. Scherer, S. Weiland, *Linear matrix inequalities in control* (Dutch Institute for Systems and Control, Delft, 2000)
- S. Shamaghdari, S. Nikravesh, M. Haeri, Integrated guidance and control of elastic flight vehicle based on robust MPC. Int. J. Robust Nonlinear Control 25(15), 2608–2630 (2015)
- T. Shi, R. Lu, Q. Lv, Robust static output feedback infinite horizon RMPC for linear uncertain systems. J. Franklin Inst. 353(4), 891–902 (2016)
- T. Shi, P. Shi, S. Wang, Robust sampled-data model predictive control for networked systems with time-varying delay. Int. J. Robust Nonlinear Control 29(6), 1758–1768 (2019)
- Y. Song, Z. Wang, D. Ding, G. Wei, Robust model predictive control under redundant channel transmission with applications in networked DC motor systems. Int. J. Robust Nonlinear Control 26(18), 3937–3957 (2016)
- Y. Song, G. Wei, S. Liu, Distributed output feedback MPC with randomly occurring actuator saturation and packet loss. Int. J. Robust Nonlinear Control 26(14), 3036–3057 (2016)
- 34. G. Strang, Introduction to Linear Algebra, 4th edn. (Wellesley-Cambridge Press, Wellesley, 2009)
- X. Tang, L. Deng, Model predictive control for uncertain discrete-time TS fuzzy systems via eventtriggered dynamic output feedback scheme. in Annual International Conference on CYBER Technology in Automation, Control, and Intelligent Systems 2018, pp. 1427–1432
- A. Ulbig, S. Olaru, D. Dumur, P. Boucher, Explicit nonlinear predictive control for a magnetic levitation system. Asian J. Control 12(3), 434–442 (2010)
- Z. Wan, M.V. Kothare, An efficient off-line formulation of robust model predictive control using linear matrix inequalities. Automatica 39(5), 837–846 (2003)
- J. Wang, Y. Song, S. Zhang, S. Liu, A.M. Dobaie, Robust model predictive control for linear discrete-time system with saturated inputs and randomly occurring uncertainties. Asian J. Control 20(1), 425–436 (2018)
- R. Wu, D. Fan, H.H.-C. Iu, T. Fernando, Dynamic surface control for discrete-time strict-feedback systems with network-induced delays using predictive event-triggered strategy. Int. J. Syst. Sci. 50(2), 337–350 (2019)
- J. Zhang, H. Yang, M. Li, Q. Wang, Robust model predictive control for uncertain positive timedelay systems. Int. J. Control Autom. Syst. 17(2), 307–318 (2019)
- 41. K. Zhu, Y. Song, D. Ding, G. Wei, H. Liu, Robust MPC under event-triggered mechanism and Round-Robin protocol: an average dwell-time approach. Inf. Sci. **457**, 126–140 (2018)
- 42. Y. Zou, Q. Wang, T. Jia, Y. Niu, Multirate event-triggered MPC for NCSs with transmission delays. Circuits Syst. Signal Process. **35**(12), 4249–4270 (2016)