

## POISONING EFFECT OF CARBON MONOXIDE ON THE DESORPTION PROCESS OF HYDROGEN FROM PALLADIUM

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The desorption of  $H_2$  from clean and CO-poisoned Pd wires was studied by a temperature programmed desorption technique. Poisoning effect of CO on  $H_2$  desorption process can be accounted for in terms of blockage of the surface sites for the recombination of H atoms.

Десорбция  $H_2$  с чистой палладиевой проволоки и, отравленной CO, была исследована методом температурно-программированной десорбции. Отравляющий эффект CO на процесс десорбции  $H_2$  вызван, вероятно, блокированием поверхностных центров, на которых происходит рекомбинация атомов водорода.

It is well known that at low temperatures ( $< 100^\circ C$ ) the absorption rates of  $H_2$  by Pd are very sensitive to the presence of impurities on the surface /1/. These results suggest that the steps on the surface, e.g. dissociation of  $H_2$ , may be responsible for the absorption process. It is expected that a similar situation exists in the case of the desorption process of  $H_2$ . However, few data from this point of view have been reported up to the present /2, 3/. CO is one of the best known inhibitors for catalytic hydrogenation reactions. Conrad et al. /4/, studying the coadsorption of  $H_2$  and CO on Pd, have found that CO may displace preadsorbed  $H_2$  completely from the surface, whereas no displacement of adsorbed CO by  $H_2$  takes place. The purpose of this work was to clarify the effect of CO on the desorption process of  $H_2$  from the Pd-H system by a temperature programmed desorption technique (TPD).

## EXPERIMENTAL

Experiments were performed in an UHV system (base pressure  $10^{-9}$  Torr). A Pd wire ( $>99.9\%$  pure) 0.02 cm in diameter and 50 cm in length was used. The specimen was welded to metal leads in the reaction cell and connected to a bridge circuit. Cleaning and activation of the Pd surface were carried out by the following oxidation-reduction cycles: (1) first outgassed at  $800^\circ\text{C}$  in vacuum for several hours, (2) heated in  $\text{O}_2$  (1 Torr) at  $200^\circ\text{C}$  for 1 h, (3) pumped, then  $\text{H}_2$  (1 Torr) for 1 h at  $300^\circ\text{C}$ , and (4) pumped to  $10^{-9}$  Torr. It has been confirmed by different investigators that the electrical resistance in the  $\alpha$ -phase of Pd-H system is proportional to the H concentration /5, 6/. Therefore, the specimen was exposed to  $\text{H}_2$  (1 Torr) in a limited time at room temperature and then the amount of dissolved H was determined by measuring the resistance change (accuracy  $\pm 10^{-4} \Omega$ ). All the experiments were carried out using specimens in the range of  $\alpha$ -phase (atomic ratio, H/Pd = 0.0006–0.005). Following the absorption, the cell was rapidly cooled to  $-196^\circ\text{C}$  and pumped out and then TPD was commenced with a heating rate of  $0.2^\circ\text{C}/\text{sec}$ . The temperature of the specimen was measured by a thermocouple which was in contact with the specimen. The changes in the partial pressure due to desorbing gases were recorded with a B–A gauge and a mass filter simultaneously. Surface poisoning was made by exposure of the H containing specimens to CO at different pressures ( $10^{-3}$ – $10^{-4}$  Torr) at room temperature. The gases ( $\text{H}_2$ ,  $\text{O}_2$  and CO) of high purity were obtained from the Takachiho Co. and used without further purification.

## RESULTS AND DISCUSSION

*Desorption of  $\text{H}_2$  from clean surfaces.* Figure 1 shows typical TPD curves for the specimens with H/Pd = 0.0006–0.005. The desorption always commenced at the same temperature, about  $-180^\circ\text{C}$ . Only a single peak can be detected and the position of peak maximum shifts to lower temperatures with the increase of H content. This temperature shift and the symmetric shape of the spectra suggest that the desorption obeys second-order kinetics /7, 8/. Therefore, the data were analyzed in term of the equation

$$E_d/RT_m^2 = (n_0\nu/\beta) \exp(-E_d/RT_m),$$

where  $\nu$  is the preexponential factor,  $E_d$  the activation energy of desorption,  $n_0$  initial H concentration,  $\beta$  heating rate and  $T_m$  the temperature at which the desorp-

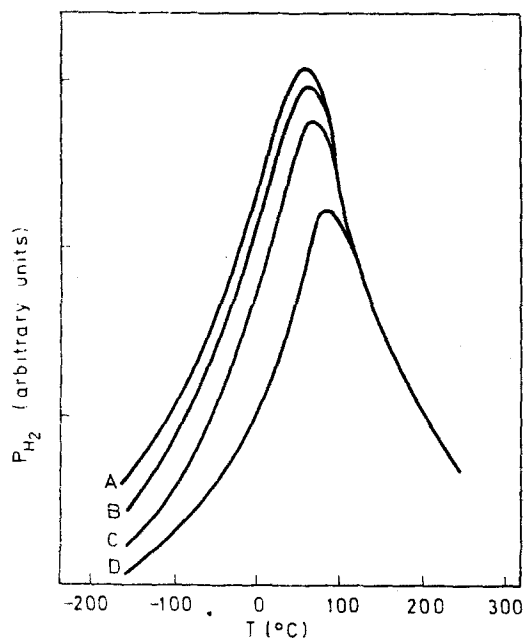


Fig. 1. TPD spectra of  $\text{H}_2$  from Pd with different H contents. H/Pd, (A) 0.005, (B) 0.004, (C) 0.0024, (D) 0.0006

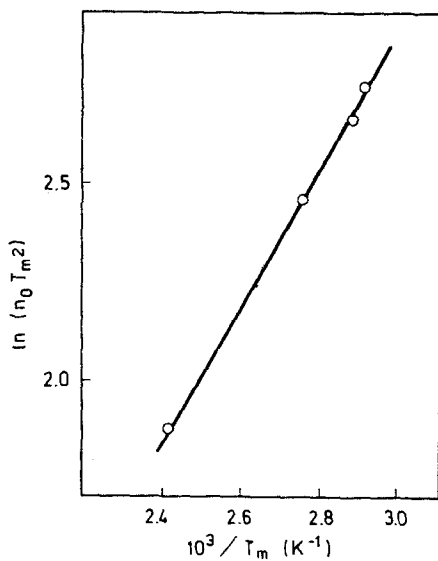


Fig. 2. Plot of  $\ln(n_0 \cdot T_m^2)$  vs.  $1/T_m$

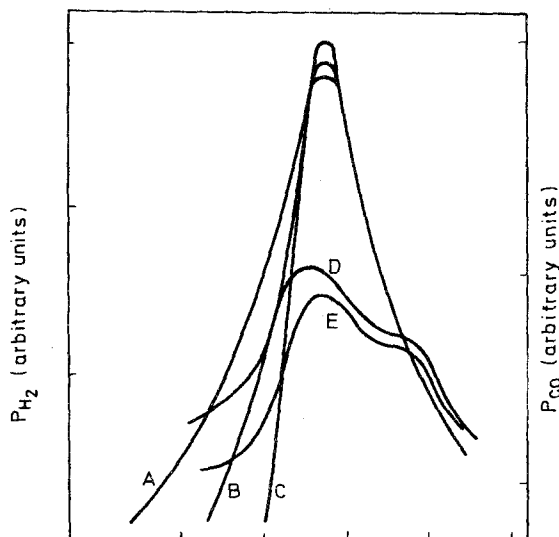


Fig. 3. Effect of CO poisoning on TPD spectra of  $H_2$  for the specimens with  $H/Pd = 0.0025$ . (A) without poisoning; dose pressure of CO, (B)  $3 \times 10^{-4}$  Torr, (C)  $1.5 \times 10^{-3}$  Torr. Curves (D) and (E) show the desorption of CO from specimens (B) and (C)

tion rate is maximum. Figure 2 shows that the desorption is well represented by second-order kinetics with an  $E_d$  of 15.5 kcal. An  $E_d$  value of 11.5 kcal was found by Auer and Grabke /6/, using thin foils of the  $\alpha$ -phase. It was suggested by them that this value is equal to the sum of the heat of dissolution of  $H_2$  (4.7 kcal) and the activation energy of absorption (6.8 kcal). Bucur et al. /9, 10/ also obtained a second-order rate law and  $E_d$  of 20.5 kcal on thin films under isothermal desorption conditions. These results suggest that the rate-controlling step of the desorption undoubtedly occurs at the surface. The discrepancy of  $E_d$  is difficult to explain but it may presumably result from the different type of specimens and the different methods of investigation used.

*Desorption of  $H_2$  from CO-poisoned surfaces.* Figure 3 shows TPD spectra obtained from CO-poisoned specimens ( $H/Pd = 0.0025$ ). It is seen that the initiation temperatures of  $H_2$  desorption ( $T_d$ ) are shifted to  $0^\circ C$  with increase of CO dose pressure, whereas  $T_m$  (about  $70^\circ C$ ) is almost unaffected. A relation between  $T_d$  and the dose pressure of CO is given in Fig. 4. In Fig. 3, CO desorption patterns are similar to those found by Stephan et al. /11/ and these peaks can be attributed to chemisorbed CO. It is clear that the rates of  $H_2$  desorption rapidly increase with removal of prechemisorbed CO, that is, the surface steps in the desorp-

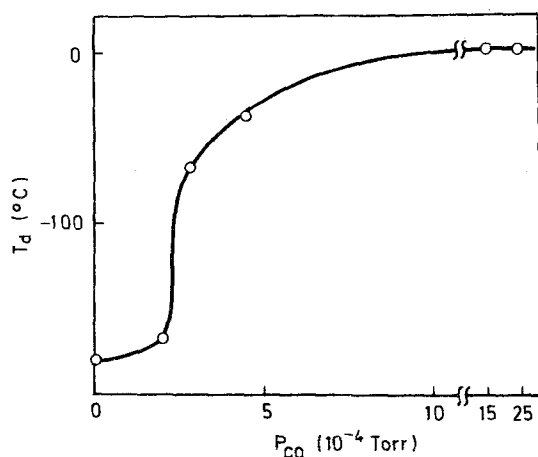


Fig. 4. Change in the initiation temperature ( $T_d$ ) of  $H_2$  desorption as a function of CO dose pressure

tion process are strongly inhibited by the presence of CO. During thermal desorption, only desorption of  $H_2$  and CO were observed and no reaction products were found. This fact is in agreement with the results of Conrad et al. /4/ observed in the case of mixed adsorbed layers on single crystal planes of Pd. Further, it was observed that  $T_m$  was independent of the amount of dissolved H in the range  $H/Pd = 0.0025-0.006$ . At present, we have no satisfactory explanation for the mechanism of  $H_2$  desorption from poisoned surfaces, but observations suggest that the interaction between H and CO at the surface must be weak and the chemisorbed CO merely blocks up the available sites for H recombination.

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