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TRAPPING ADSORPTION OF CARBON MONOXIDE LOCATED BETWEEN CARBON DIOXIDE ADSORBED ON MAGNESIUM OXIDE

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Carbon monoxide adsorbed on MgO is strongly trapped by the adsorbed carbon dioxide, increasing the heat of adsorption from 85.4 to 184.1 kJ/mol. The trapped CO is thought to be captured by two or three adsorbed  $CO_2$  and becomes less active to react with oxygen.

Моноокись углерода, адсорбированная на MgO, сильно связана адсорбированной двуокисью углерода, что приводит к увеличению теплоты адсорбции с 85,4 до 184,1 кДж/моль. Полагают, что одна молекула СО захватывается двумя или тремя адсорбированными молекулами СО<sub>2</sub> и тем самым становится менее активной к реакции с кислородом.

The interaction between CO species adsorbed on MgO has been studied in detail by Zecchina et al. [1], who illustrate the formation of CO clusters and carbonate like species. In the present study, our further interest is focused on the interaction of CO with  $\rm CO_2$  coadsorbed on MgO at 290-320 °C. An anomalously coinfluenced adsorption behavior of CO and  $\rm CO_2$  has been studied by the transient response method [2,3] and the temperature programmed desorption technique in a flow system.

The sample used in this study was prepared from Wako Pure Chemicals, guaranteed reagent. MgO (20-30 mesh, BET surface area is 27.5  $m^2/g$ ) was packed into a Pyrex glass tubular flow reactor and pretreated in a He stream at 300 °C for 20 h prior to use.

Figure 1 shows the transient desorption behavior of CO

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Fig. 1. Desorption of adsorbed CO retained on the surface into the  $\rm CO_2-He$  stream

affected by the adsorption of  $CO_2$ . In Run 1, the catalyst is exposed to a mixture of CO (10%) -  $CO_2$  (5%) - He (A-gas stream) for 30 min at 300 °C to perform the co-adsorption of CO and  $CO_2$ , and then the gas mixture is separately switched over to three different gas streams (Run 2), a pure He (gas-B<sub>1</sub>), a  $CO_2$ (0.4%) - He (gas-B<sub>2</sub>) and a  $CO_2$  (2.3%) - He (gas-B<sub>3</sub>) streams. In Run 2, the desorption response of CO is sensitively affected by the concentration of  $CO_2$  coexisting.

The graphical integration of the three response curves in Run 2 of Fig. 1 shows the amount of desorbed CO, which is decreased with increasing concentration of  $CO_2$  in the gas phase. One may recognize the critical concentration of  $CO_2$  for completely trapping CO to be  $P_{CO_2}^C$  = 0.023 atm. When the gas mixture at the critical  $CO_2$  (designated as  $P_{CO_2}^C$ , is successively switched over to the pure He stream, an appreciable amount of CO is desorbed as shown in Run 3. The desorbed amount  $q_{CO}^{II}$  = =  $2.5 \times 10^{-6}$  mol/g) is in good agreement with that  $(q_{CO}^{I} = 2.65 \times 10^{-6} \text{ mol/g})$  obtained in the pure He stream (gas-B<sub>1</sub>) at Run 2. These results clearly show that the CO trapped on the surface in the CO<sub>2</sub>-He mixture is desorbed with the desorption of CO<sub>2</sub> in He.

The amount of CO<sub>2</sub> desorbed in Run 3 of Fig. 1 is estimated to be  $q_{CO_2} = 6.3 \times 10^{-6}$  mol/g from graphical integration: the ratio of  $q_{CO_2}$  to  $q_{CO}^{II}$  is therefore about 2.5. This means that 2.5 adsorbed CO<sub>2</sub> is necessary to trap one adsorbed CO.  $P_{CO_2}^C$ corresponds to the critical concentration of CO<sub>2</sub> to completely trap the adsorbed CO on the surface, and it depends on the concentration of gaseous CO. Figure 2 illustrates the amounts of CO desorbed in Run 2 of Fig. 1 as functions of  $P_{CO_2}$  in Run 2 and  $P_{CO_2}$  in Run 1.  $P_{CO_2}^C$  equals  $7 \times 10^{-3}$  atm at  $P_{CO} = 0.05$  atm and  $2.3 \times 10^{-2}$  atm at  $P_{CO} = 0.10$  atm. A large number of calculations



Fig. 2. Plots of  $q_{CO}$  as a function of  $P_{CO_2}$  in Run 2 of Fig.1

for the amounts of adsorbed CO and CO<sub>2</sub> obtained at  $P_{CO_2}^C$  falls between two and three adsorbed CO<sub>2</sub> species to trap one adsorbed CO species.

The adsorption isotherm of CO obtained from the transient response method in the He stream, in which there is no trapping

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effect by  $CO_2$ , obeys the Langmuir equation and the heat of adsorption is estimated to be 85.4 kJ/mol. The temperature programmed desorption spectra of CO, on the other hand, are obtained in the  $CO_2$  coexisting stream, and the peak analysis of the spectra obtained by changing the rate of temperature increase estimates the activation energy of desorption to be 184 kJ/mol. This much higher energy compared to the adsorption heat in He should result from the strong trapping effect of  $CO_2$  on the adsorbed CO.

On the contrary, the desorption behavior of  $CO_2$  is not affected by the CO coexisting in the stream with no appreciable change in its adsorption heat and in its adsorbed amount. In addition, the separate transient experiments clearly demonstrate that no CO adsorbs on the surface fully occupied by the adsorbed  $CO_2$ . From these results, one may exactly recognize that  $CO_2$  is competitively adsorbed on the same active sites stronger than CO, and CO is strongly trapped by  $CO_2$  adsorbed on the neighboring sites. For the detailed mechanism for the trapping effect of  $CO_2$ , although it is difficult to clear in this study, one may propose a possible explanation: the base sites which are  $O^{2^-}$  with lower coordinative unsaturation may be considered as the active sites [4], and the CO will be trapped on the vacant  $O^{2^-}$  located between two or three neighboring  $CO_2$ .

For the reactivity of the trapped CO, it has been confirmed that the CO has no activity to react with oxygen, whereas, if freed from the trapping effect of  $CO_2$ , it can easily react with adsorbed oxygen to produce  $CO_2$ . Further study of the detailed structure of the trapped CO is under way using the FT-IR technique and will be reported later.

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