

CRUDE OILS OF THE GEORGIAN SSR

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A study has been made of Georgian SSR (Gruziya) crude oil, consisting of a mixture of crudes from the Samgori, Norio, Mirzani, Supsa, and Chaladidi fields. Georgian crude is low sulfur, medium resin, and medium wax. The characteristics of this crude are as follows:

Density ρ_4^{20}	0.8528
Molecular weight	204
Kinematic viscosity, cSt	
at 20°C	8.44
at 50°C	3.65
Solid point, °C	
without thermal treatment	-4
with thermal treatment	0
Flash point, closed cup, °C	18
Content, %	
sulfur	0.17
nitrogen	0.11
silica gel resins	3.50
asphaltenes	1.37
wax	4.20
Carbon residue, %	2.33
Ash content, %	0.013
Acid no., mg KOH/g oil	0.25
Content of fractions, wt. %	
below 200°C	26.3
below 350°C	61.0
below 500°C	86.8

It will be seen from the data of Table 1 that the hydrocarbon group composition of the fractions of Georgian crude distilling below 200°C is characterized by a predominance of paraffinic hydrocarbons (87-56%) over naphthenes (13-42%) and aromatics (0-14%).

A study of the 28-150°C cut by gas-liquid chromatography showed that, out of the total quantity of paraffins in this cut (8.59% calculated on crude), the branched-chain paraffins account for 5.22% and n-paraffins for 3.37%. The branched-chain paraffins consist mainly of hydrocarbons with a single methyl group, such as 2-methylheptane (0.53%), 2-methylhexane (0.48%), and 3-methylhexane (0.40%). Of the straight-chain paraffins, the largest percentages are those of n-octane (1.10%) and n-heptane (0.95%).

The content of naphthenic hydrocarbons in the cut is 6.01% (calculated on crude), with more cyclohexane derivatives (3.28%) than cyclopentanes (2.73%). The individual cyclopentane derivative present in largest amount is methylcyclopentane (0.38%), the cyclohexane derivative methylcyclohexane (1.25%).

The naphtha cuts are good feedstocks for catalytic reforming, since the content of naphthenic hydrocarbons in these cuts ranges from 27.4 to 41.5%, calculated on the cut. These cuts are essentially sulfur-free.

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TABLE 1. Hydrocarbon Group Composition of 28-200°C Cuts

	Cut points, °C					
	28-62°C	62-95°C	95-122°C	122-150°C	150-200°C	28-200°C
Yield on crude, %	0,8	3,3	4,7	6,6	10,7	26,1
Density ρ_4^{20}	0,6618	0,7063	0,7341	0,7558	0,7872	0,7590
Refractive index n_D^{20}	1,3707	1,3921	1,4087	1,4210	1,4377	1,4232
Content of hydrocarbons, %						
aromatics	0	3	5	9	14	9
naphthenes	13	32	42	28	30	32
paraffins	87	65	53	63	56	59
normal structure	45	29	25	22	20	23
iso structure	42	36	28	41	36	36

A kerosene cut was obtained in amount of 29.3% (calculated on crude), characterized by low contents of total sulfur (0.01%) and mercaptan sulfur (0.0003%) and rather high thermal stability.

The kerosene distillates are characterized by poor burning qualities (the 150-320°C cut has a smoke point below 20 mm); these distillates can be used as diesel fuel components.

The diesel fuel distillates are distinguished by high cetane numbers; these materials meet the GOST specification requirements for summer-grade diesel fuel.

The residue boiling above 350°C was treated by adsorptive separation and subsequent dewaxing of the mixture of paraffinic-naphthenic and Group I aromatic hydrocarbons, obtaining a lube base stock in yield of 16.7% (on crude) with a viscosity on the order of 48.08 cSt at 50°C and 9.03 cSt at 100°C, a V.I. of 86, and a solid point of -26°C.

In accordance with GOST 11954-66, the Georgian crude cannot be recommended for asphalt production.

INFLUENCE OF FEEDSTOCK DISTILLATION RANGE ON HYDROCARBON CONVERSION AND CHANGES IN LUMINOMETER NUMBER UPON DEAROMATIZATION OF DISTILLATES FROM NIZHNEVARTOVSK CRUDE OIL

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Today, the use of effective hydrogenation catalysts makes it possible to dearomatize sulfur-containing kerosine distillates at relatively low pressures, on the order of 50 kg/cm² [1-3]. The process of catalytic hydrogenation is of considerable interest in producing fuels for gas-turbine engines from crude oils with high contents of aromatic hydrocarbons. Nizhnevartovsk crude oil is a promising material for the production of gas-turbine fuels, but it is impossible to obtain fuel with less than 20% aromatic hydrocarbons from this crude by the use of conventional hydrotreating processes.

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