

# MIXED CONVECTION OVER A HORIZONTAL PLATE WITH VECTORED MASS TRANSFER IN A TRANSVERSE MAGNETIC FIELD

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**Abstract.** An exact similarity solution is presented for developing mixed convection flows of electrically conducting fluids over a semi-infinite horizontal plate with vectored mass transfer at the wall which are subjected to an applied transverse magnetic field. This solution is given for the case of a wall temperature that is inversely proportional to the square root of the distance from the leading edge. By application of appropriate coordinate transformations, the governing momentum and energy boundary-layer equations are expressed as a set of coupled ordinary differential equations that depend on a magnetic parameter, the buoyancy parameter, and the Prandtl number. The shear stress, the total heat transfer, and the displacement thickness are calculated for different values of both buoyancy and magnetic parameters.

## 1. Introduction

The field of magnetohydrodynamic (MHD) heat transfer can be divided arbitrarily into two sections: one contains problems in which the heating is an incidental by product of the electromagnetic fields (as in such MHD devices as generators, pumps, etc.), and the second consists of problems in which the primary use of electromagnetic fields to control the heat transfer (as in the natural convection flows and aerodynamic heating). This study is devoted to the second class of problems, viz., the influence of magnetic field on combined or 'mixed' natural and forced convection heat transfer to electrically conducting fluids.

Extensive studies have been made on the combined forced and free convection MHD flows as by Georgantopoulos *et al.* (1979), Raptis *et al.* (1981), Mazumder *et al.* (1976), Tan and Wang (1968). The flow of an incompressible viscous fluid past an impulsively started, infinite, horizontal plate, in its own plane, was first studied by Stokes (1851). Recently, Georgantopoulos *et al.* (1979) studied the hydromagnetic free convection effects on the Stokes problem for an infinite vertical plate. Raptis *et al.* (1981) studied the effect of suction/injection on the hydromagnetic free convection flow of a viscous, incompressible, and electrically conducting fluid, past an infinite accelerated non-conducting, vertical plate with variable suction and heat flux. Mazumder *et al.* (1976) studied the flow of an electrically conducting liquid past an infinite porous plate in the presence of a uniform transverse magnetic field and in a rotating frame of reference, and deduced the flow and heat-transfer characteristics of the Ekman layer over the plate. Tan and Wang (1968) studied the steady state heat-transfer phenomena in an aligned flow past a semi-infinite flat plate in which the velocity and magnetic field vectors far

from the plate are parallel. They used a viscous, electrically conducting, incompressible fluid, as the working medium.

Earlier investigations (Schneider, 1979; Dey, 1982; Afzal and Hussain, 1984) on the OHD (ordinary hydrodynamic) mixed convection flow over a horizontal plate were confined to the nonmagnetic case. Schneider (1979) studied the effect of buoyancy forces and has shown the existence of similarity provided the wall temperature is prescribed as the inverse square root of the distance from the leading edge. Likewise, the work of Dey (1982), dealing with an extension of Schneider (1979) to mass transfer. The solutions (see Schneider, 1979; Dey, 1982) cover a limited range of buoyancy to forced convection parameter that do not include the strongly buoyant flows in aiding situations and nearly separating flows in opposing situations. Afzal and Hussain (1984) developed the solutions of Schneider (1979) to include the entire domain, beginning from purely free convection dominated to separated flows.

The aim of this work is to extend the previous works of Schneider (1979) and Dey (1982) to the MHD mixed convection flows over a horizontal plate. An exact similarity solution is presented for the case of both a wall temperature and the magnetic strength which are inversely proportional to the square root of the distance from the leading edge. Numerical results are obtained for the shear stress, the total heat transfer and the displacement thickness with vectored suction and injection for different values of the magnetic and buoyancy parameters. The velocity and temperature profiles are graphically represented and the previous results are discussed in the last section.

## 2. Formulation of the Problem

Consider a horizontal flat plate aligned parallel to an uniform free stream with velocity  $u_\infty$ , density  $\rho_\infty$ , and temperature  $T_\infty$ . The flow over the plate is considered to be plane, laminar, and steady. We use a Cartesian coordinate system  $x, y$  with the origin at the leading edge of the plate. The applied magnetic field is primarily in the  $y$ -direction and varies in strength as a function of  $x$ . No externally generated electrical field is imposed. Ohm's law is assumed and the magnetic Reynolds' number of the flow is taken to be small so that the flow induced distortion of the applied magnetic field can be neglected. Constant transport coefficients (including electrical conductivity) are assumed, the Boussinesq approximation is applied, and the boundary-layer approximation is assumed to hold. Under these conditions, the equations of continuity, momentum, and energy are

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \quad (1)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \frac{\partial^2 u}{\partial y^2} - \frac{\sigma B^2}{\rho} u, \quad (2)$$

$$\frac{1}{\rho} \frac{\partial p}{\partial y} = g\beta(T - T_\infty), \quad (3)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2}; \tag{4}$$

$u$  and  $v$  are the velocities in the horizontal and vertical directions.  $\rho$ ,  $\nu$ ,  $\beta$ ,  $\alpha$ , and  $\sigma$  are the density, kinematic viscosity, the thermal expansion coefficient, thermal diffusivity, and the electrical conductivity of the fluid.  $T$ ,  $p$ , and  $B$  are the temperature, pressure, and the applied magnetic field.

If we introduce the dimensionless variables in the form

$$\begin{aligned} X &= x/L, & Y &= \sqrt{\text{Re}} y/L, & U &= u/u_\infty, \\ V &= \sqrt{\text{Re}} v/u_\infty, & \theta &= \frac{T - T_\infty}{T^*}, & P &= (P - P_\infty)/\rho_\infty u_\infty^2, \end{aligned} \tag{5}$$

where  $\text{Re} = u_\infty L/\nu$  is the Reynolds number and the pressure is referred to  $p_\infty$ ,  $T^*$  represents a characteristic temperature difference between plate and free stream.

The boundary conditions in dimensionless forms as in the nonmagnetic case (cf. Schneider, 1979), for which the similarity solution is possible, are

$$\begin{aligned} U &= u_w, & V &= -2v_w X^{-1/2}, & \Theta &= X^{-1/2} \text{ on } Y = 0, & X > 0; \\ U &= 1, & \theta &= P = 0 \text{ as } Y \rightarrow \infty. \end{aligned} \tag{6}$$

Also for the similarity solution to be possible we choose the strength of the magnetic field in the form

$$B = B_0 X^{-1/2}. \tag{7}$$

The solution of these coupled nonlinear equations is facilitated by introducing a number of transformations. Introduce a stream function  $\psi$  such that  $U = \partial\psi/\partial Y$ ,  $V = -\partial\psi/\partial X$ . The following similarity transformation (originally used by Schneider (1979) in the non-magnetic case) reduces the problem to the solution of ordinary differential equations

$$\eta = YX^{-1/2}, \quad \psi = X^{1/2} f(\eta); \quad \theta = X^{-1/2} \phi(\eta). \tag{8}$$

These relations transform (1) through (8) into the following set of coupled ordinary differential equations

$$2f''' + ff'' + K\eta\phi - M\eta f' = 0; \tag{9}$$

$$\frac{2}{\text{Pr}} \phi'' + f\phi' + f'\phi = 0; \tag{10}$$

with the boundary conditions

$$\begin{aligned} f(0) &= f_w = \text{const. (given)}, & f'(0) &= f'_w = \text{const. (given)}, & \phi(0) &= 1, \\ f'(\infty) &= \phi(\infty) = 0; \end{aligned} \tag{11}$$

where primes denote differentiation with respect to the similar variable  $\eta$ ,  $Pr$  stands for the Prandtl number,  $Mn = \sigma B_0^2 L / \rho u_\infty = H^2 / Re$  is a magnetic parameter,  $H$  is the Hartmann number, and  $K$  is related to the Archimedes number  $Ar$  according to

$$K = Ar / \sqrt{Re}, \quad Ar = g L \beta_\infty T^* / u_\infty^2. \quad (12)$$

In technological applications, the total heat transfer  $Q_w$ , the wall shear stress  $f''(0)$  (in dimensionless form), and the displacement thickness  $\delta^*$  are often of great interest. In order to circumvent the difficulties linked to the singularity at the leading edge the total heat transfer  $Q_w$  is determined with the help of the heat flux equation in the form

$$Q_w = \rho_\infty C_p \int_0^\infty [(T - T_\infty)]_{x=l} dy. \quad (13)$$

where  $l$  is the length of the plate (not to be confused with the characteristic length  $L$ ) and  $c_p$  is the specific heat capacity at constant pressure. Introducing the dimensionless variables of Equation (5) and applying the similarity transformation (8), we obtain

$$St^* = \sqrt{Re} St = \int_0^\infty \phi f' d\eta, \quad (14)$$

where the Stanton number is

$$St = Q_w / \rho_\infty u_\infty C_p T^* L. \quad (15)$$

The displacement thickness  $\delta^*$  can be calculated from the relations

$$\begin{aligned} \delta^* &= \int_0^\infty \left(1 - \frac{u}{u_\infty}\right) dy = \sqrt{\frac{vx}{u_\infty}} \int_0^\infty [1 - f'(\eta)] d\eta \\ &= \sqrt{\frac{vx}{u_\infty}} \lim_{\eta \rightarrow \infty} [\eta - f(\eta)]. \end{aligned} \quad (16)$$

### 3. Numerical, Results, and Discussion

The system of ordinary differential equations (9) and (10) subject to the boundary conditions (11) has been solved numerically by means of the fourth-order Runge-Kutta method with a systematic estimates of  $f''(0)$  and  $\phi'(0)$  by the shooting technique. Numerical computations were carried out on a VME-2955 computer for  $Pr = 0.7$ ,  $f'_w = f_w = 0; \pm 0.1; \pm 0.2, 0 \leq k \leq 1$  and  $0 \leq Mn \leq 1$ . It is interesting to note that the wall heat transfer mode ( $\phi'(0) = -Pr f_w/2$ ) depends on  $f_w$ , which causes the boundary-layer fluid either to received heat from the wall ( $f_w > 0$ ) or to transfer heat to the wall ( $f_w < 0$ ). Also, the numerical values of  $\phi'(0)$  can be verified with the exact values and were found to be in good agreement.

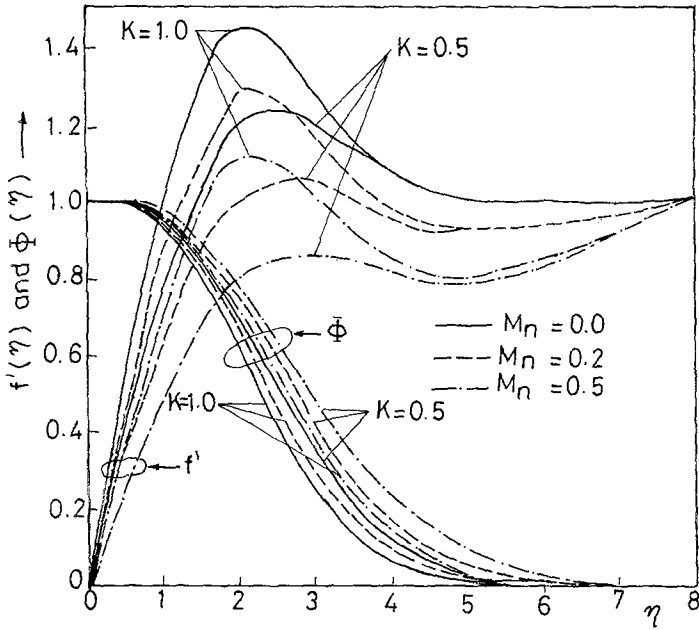


Fig. 1. Velocity and temperature profiles with no mass transfer ( $f_w = f'_w = 0$ ) for various values of buoyancy parameter  $K$  and magnetic parameter  $M_n$ .

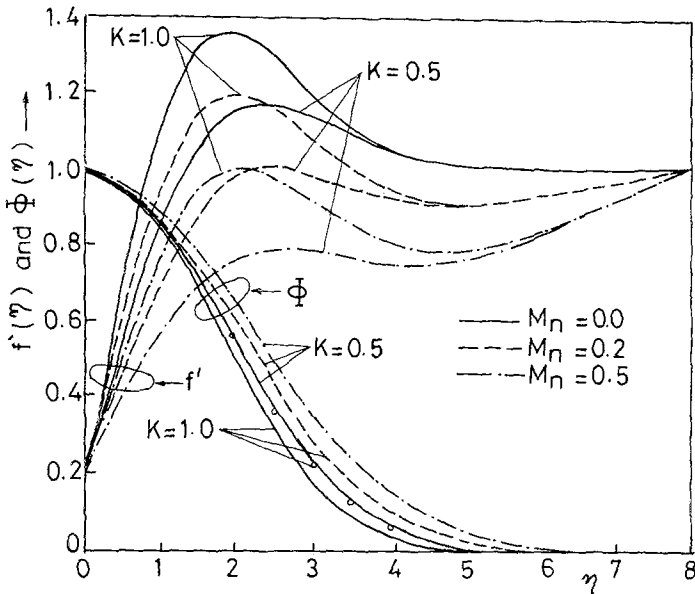


Fig. 2. Velocity and temperature profiles with vectored downstream suction ( $f'_w = f_w = 0.2$ ) for various values of buoyancy parameter  $K$  and magnetic parameter  $M_n$ .

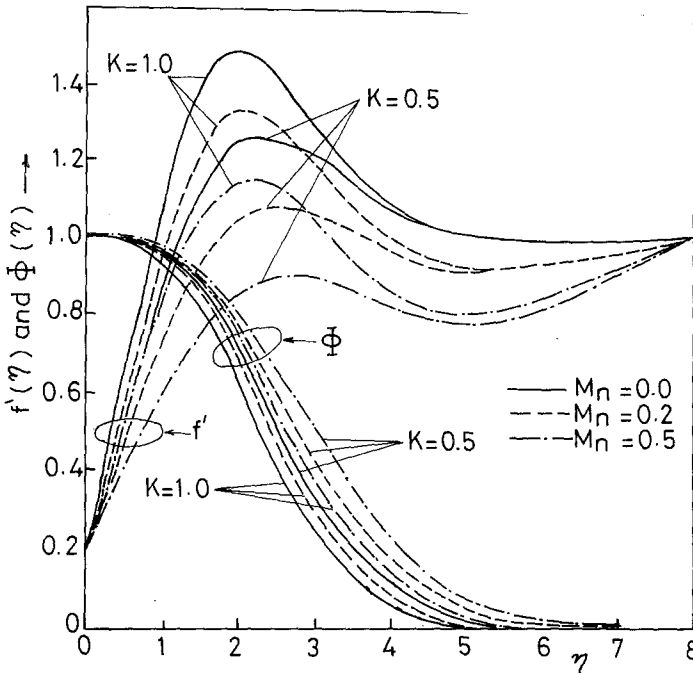


Fig. 3. Velocity and temperature profiles with vectored downstream injection ( $f'_w = 0.2$ ,  $f_w = -0.2$ ) for various values of buoyancy parameter  $K$  and magnetic parameter  $Mn$ .

Figures 1–3 illustrate the velocity and temperature profiles for different values of  $f'_w$ ,  $f_w$ ,  $k$ , and  $Mn$ , without mass transfer ( $f'_w = f_w = 0$ ), with downstream vectored suction ( $f'_w = f_w = 0.2$ ) and with downstream vectored injection ( $f'_w = 0.2$ ,  $f_w = -0.2$ ), respectively. It can be seen from Figures 1–3 that the velocity profile  $f'$  increases as the magnetic parameter  $Mn$  increases and it decreases as the buoyancy parameter increases. In the adverse case for the temperature profile  $\phi$ . It is interesting to note that for large values of  $K$  and small values of  $Mn$  there are obviously overshoots in the velocity profiles, i.e., the local velocities are larger than the free-stream velocity. From Figure 3, it can be seen that both cases of ( $K = 1.0$ ,  $Mn = 0.2$ ) and ( $K = 0.5$ ,  $Mn = 0.0$ ) coincide. The same thing happens for the two cases ( $K = 1.0$ ,  $Mn = 0.5$ ) and ( $K = 0.5$ ,  $Mn = 0.2$ ).

Numerical results for the wall shear stress values  $f''(0)$ , the Stanton number  $St$  and the displacement thickness  $\delta^*$ , which are not represented in Figures 4–6, are presented in Table I.

Figure 4 shows  $f''(0)$ , which is proportional to the wall shear stress, as a function of the buoyancy parameter  $K$  for different values of  $f'_w$ ,  $f_w$ , and  $Mn$ . Figure 4 and Table I show that the buoyancy force ( $K > 0$ ) enhances the wall shear values ( $f''(0)$ ) as in the case of mixed convection without mass transfer ( $f'_w = f_w = 0$ ). This is a consequence of there being a favorable pressure gradient above the plate due to buoyancy effects and the wall shear stress is larger than in the non-buoyant case (Schneider, 1979). On the

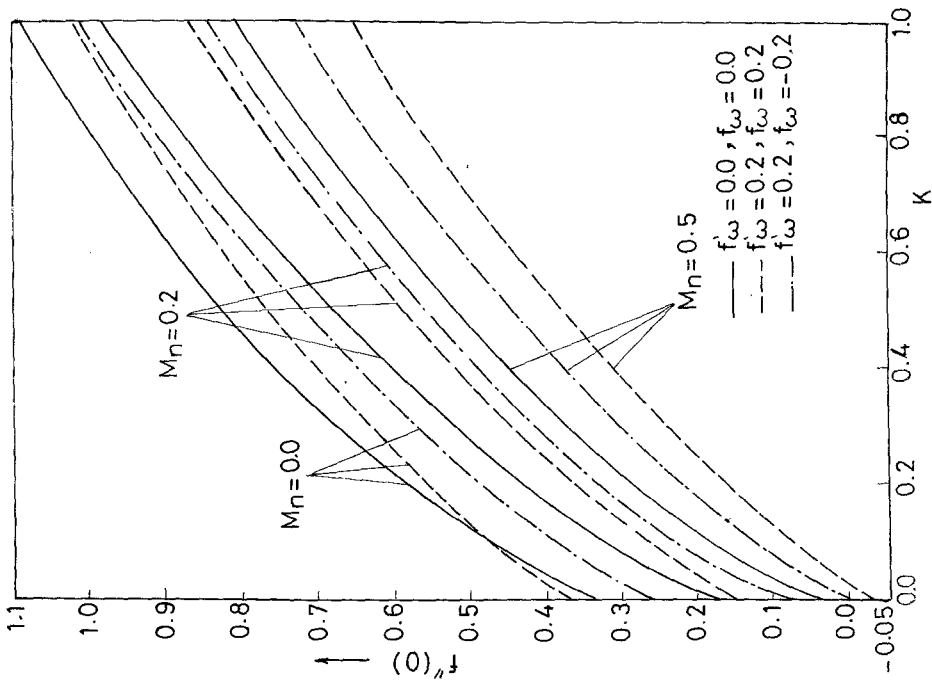


Fig. 4. Dimensionless wall shear values as a function of the buoyancy parameter  $K$  for various values of the magnetic parameter  $M_n$  and vectored mass transfer.

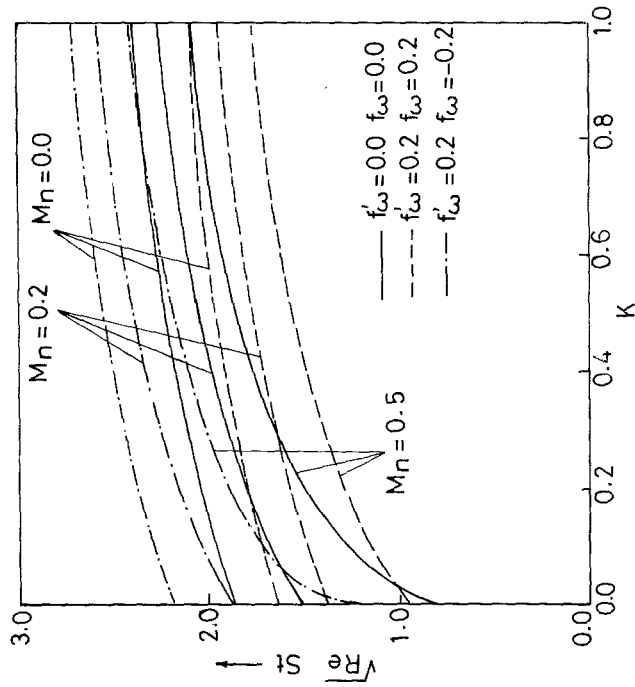


Fig. 5. Total heat transfer on the plate (Stanton number  $St$ ) as a function of the buoyancy parameter  $K$  with vectored mass transfer for different values of the magnetic parameter  $M_n$ .

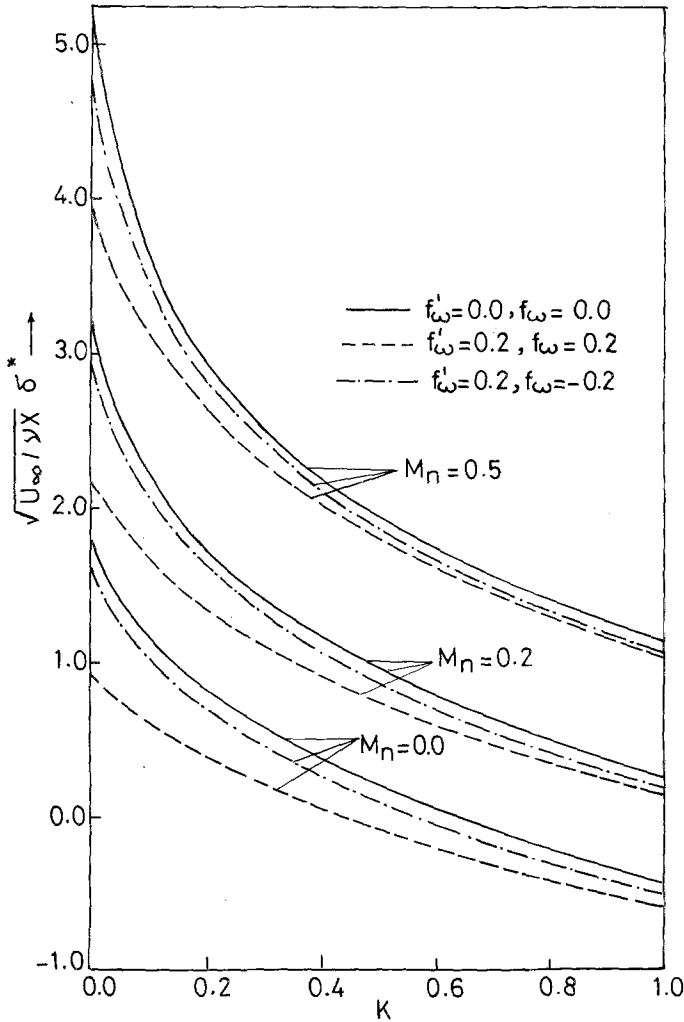


Fig. 6. Effect of buoyancy parameter  $K$  and magnetic parameter  $Mn$  on the displacement thickness  $\delta^*$  with vector mass transfer.

other hand the magnetic force ( $Mn > 0$ ) reduces the wall shear values. It is showed that the wall shear values are higher with downstream-vectored suction ( $f'_w = f_w = 0.2, 0.1$ ) than those with downstream-vectored injection ( $f'_w = 0.2, 0.1; f_w = -0.2, -0.1$ ). It is interesting to note that for  $Mn > 0$  and  $K > 0.15$  the wall shear values are higher with upstream-vectored injection ( $f'_w = f_w = -0.1, -0.2$ ) than those with downstream-vectored suction ( $f'_w = f_w = 0.1, 0.2$ ). Figure 4 and Table I show that, for  $Mn = 0.0$  and  $K < 0.15$ , the wall shear values are higher with downstream-vectored suction than those with upstream-vectored injection which agree with Dey (1982) and Inger and Swean (1975).



TABLE I  
Values of  $f''(0)$ ,  $\sqrt{\text{Re St}}$ , and  $\sqrt{u_{\infty}/\nu x} \delta^*$  for various values of  $f_w$ ,  $f_w$ ,  $K$  and  $Mn$

Mn	K	$f_w = -0.2, f_w = 0.2$			$f_w = -0.2, f_w = -0.2$			$f_w = 0.1, f_w = 0.1$			$f_w = 0.1, f_w = -0.1$		
		$f''(0)$	$\sqrt{\text{Re St}}$	$\sqrt{u_{\infty}/\nu x} \delta^*$	$f''(0)$	$\sqrt{\text{Re St}}$	$\sqrt{u_{\infty}/\nu x} \delta^*$	$f''(0)$	$\sqrt{\text{Re St}}$	$\sqrt{u_{\infty}/\nu x} \delta^*$	$f''(0)$	$\sqrt{\text{Re St}}$	$\sqrt{u_{\infty}/\nu x} \delta^*$
0.0	0.00, 403.860	1.533516	1.931613	3.313636	0.203548	2.276968	3.313636	0.359009	1.730155	1.271186	0.295946	2.009979	1.628746
	0.1	0.568434	1.664293	1.258008	0.443985	2.482772	1.722037	0.476977	1.828917	0.863426	0.429637	2.129595	1.082361
	0.2	0.687053	1.746067	0.877813	0.586339	2.542822	1.171328	0.573362	1.901010	0.580792	0.533406	2.209682	0.740253
	0.3	0.785976	1.809067	0.604573	0.688836	2.591706	0.816189	0.657669	1.959284	0.360919	0.622337	2.272375	0.485595
	0.4	0.783130	1.861411	0.388841	0.782425	2.634214	0.550235	0.733863	2.008834	0.179563	0.701884	2.324804	0.208816
	0.5	0.952201	1.906681	0.209471	0.866310	2.672155	0.336195	0.804180	2.052284	0.024410	0.774778	2.370300	0.108542
	1.0	1.278226	2.075552	-0.411750	1.206594	2.820647	-0.371787	1.101645	2.217219	-0.535393	1.080106	2.540558	-0.497227
0.2	0.0	0.223245	1.152036	3.643798	0.089036	0.807284	5.776979	0.164895	1.443437	2.632302	0.120852	1.686069	3.090895
	0.1	0.413987	1.449840	2.370657	0.334460	2.304958	2.751335	0.298523	1.608931	1.940048	0.270294	1.912394	2.148100
	0.2	0.536749	1.563237	1.835653	0.467885	2.400887	2.036523	0.400045	1.707884	1.538287	0.377504	2.022878	1.672252
	0.3	0.636529	1.641886	1.482970	0.573139	2.459177	1.608673	0.486539	1.782003	1.248590	0.467315	2.101748	1.344662
	0.4	0.723507	1.704363	1.216568	0.663820	2.506758	1.298936	0.563743	1.842504	1.019808	0.546836	2.164864	1.092136
	0.5	0.801988	1.757067	1.001111	0.745124	2.548375	1.054589	0.634437	1.894190	0.829722	0.619303	2.218229	0.885480
	1.0	1.123673	1.947111	0.284645	1.075661	2.708699	0.270780	0.930626	2.082960	0.173491	0.920963	2.410862	0.187408
0.5	0.0	0.139469	0.430354	5.424205	0.095395	0.224004	6.739623	0.006548	0.937206	4.488212	-0.008376	1.019296	4.978601
	0.1	0.292373	1.115872	3.770638	0.250225	1.897226	4.028332	0.132735	1.292779	3.360066	0.124378	1.580129	3.526218
	0.2	0.404233	1.311902	3.046758	0.368600	2.176445	3.106384	0.229378	1.446550	2.790962	0.224333	1.764698	2.872291
	0.3	0.496148	1.420656	2.602450	0.463345	2.273657	2.599463	0.311522	1.547019	2.410172	0.308355	1.873626	2.454494
	0.4	0.388881	1.499213	2.279599	0.545846	2.335818	2.245281	0.384837	1.623720	2.122204	0.382981	1.953649	2.145424
	0.5	0.649952	1.562408	2.024717	0.620434	2.385019	1.971206	0.452631	1.686786	1.889627	0.451192	2.018311	1.898991
1.0	0.0	0.154088	0.091935	6.419514	0.130020	0.052187	7.150473	-0.063455	0.450118	5.891081	-0.062097	0.482746	6.229893
	0.1	0.235569	0.610053	5.238526	0.208333	1.050049	5.522840	0.014249	0.845215	4.906370	0.016258	1.047087	5.049455
	0.2	0.316292	0.929485	4.444566	0.296085	1.705803	4.408148	0.087629	1.083264	4.252441	0.092266	1.370728	4.286495
	0.3	0.388881	1.105295	3.933290	0.372682	1.952216	4.807566	0.154209	1.231011	3.804772	0.160652	1.548375	3.793011
	0.4	0.454825	1.218810	3.567525	0.440921	2.072264	3.408251	0.215390	1.338215	3.470705	0.223068	1.664213	3.436524
	0.5	0.515867	1.302439	3.283268	0.503562	2.149077	3.109054	0.272466	1.415938	3.204985	0.281073	1.750089	3.158065
	1.0	0.777033	1.558902	2.394159	0.769657	2.364664	2.201229	0.519472	1.675028	2.349024	0.531022	2.014250	2.278995

Numerical results for the Stanton number  $St$  are shown in Figure 5. It is seen that as  $Mn$  increases the heat transfer rate decreases. On the other hand, as the buoyancy parameter increases the heat transfer rate increases. This happens because, for  $K > 0$ , the buoyancy accelerates the flow in the boundary layer.

The effect of the magnetic parameter  $Mn$  and the buoyancy parameter  $K$  on the displacement thickness  $\delta^*$  with  $f'_w = 0.2$  and  $f_w = \pm 0.2$  is shown in Figure 6. It is interesting to note that the displacement thickness is negative for relatively large  $K$ , but it is positive for all nonzero magnetic parameter  $Mn$ . This is a consequence of local velocities that are larger than the mean velocity, cf. Figures 1–3.

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