Viscosity of undercooled melts

I. AVRAMOV

Institute of Physical Chemistry, Bulg. Acad., Sci., 1113 Sofia, Bulgaria

A number of models describe the temperature dependence of viscosity η of undercooled melts. According to the old-fashioned free volume approach, η depends on the ratio of the occupied volume to the free volume. Gibbs et al. [1,2] consider the molecular motion as a cooperative process involving a simultaneous rearrangement of a large number of particles. For that reason η should depend on the configurational entropy. Scherer [3] has shown that the free volume model is not able to describe properly the isostructural viscosity of oxide glasses. On the other hand, the Adam-Gibbs equation represents well the viscosity of some glasses but it fails for others. It is well known that despite the differences in the mechanism of molecular transport, all undercooled melts show a remarkable similarity in the temperature dependence of their shear viscosity. For that reason a generalized model was suggested [4] describing the kinetics of molecular motion in undercooled melts. In the present paper we discuss some aspects of the physical background and values of the parameters involved in the model. Moreover, the number of the parameters is reduced and their dependence on the composition is considered taking into account existing experimental data [5].

The most popular representation of the dependence of the jump frequency v on temperature T and activation energy E is formulated in terms of the active complex theory as:

$$v = v_0 \exp\left(-\frac{E}{RT}\right) \tag{1}$$

where $v_0 \approx 10^{(11\pm1)} \,\mathrm{s}^{-1}$ is the mean vibration frequency.

Every motion in undercooled melts is a cooperative process with a broad distribution of barrier heights, E. The disorder in amorphous media implies some probability distribution function, $W(E, \sigma)$, of the activation energy, E, for the jump of a building unit to a new position. The dispersity σ of $W(E, \sigma)$ reflects the degree of disorder in the system and is related to the entropy, S. The $\sigma(S)$ -dependence is described [4, 6] with sufficient accuracy through the dispersity σ_r at a given reference state at which the entropy is S_r .

$$\sigma = \sigma_{\rm r} \exp\left(\frac{2(S-S_{\rm r})}{ZR}\right) \tag{2}$$

Here R is the ideal gas constant and Z is the number of channels along which the building unit could escape from the given position. The entropy can be expressed through the heat capacity C_p . Adopting, as usual, $c_{\rm p} \approx \text{constant}$, it follows that

$$\sigma = \sigma_{\rm r} \left(\frac{T}{T_{\rm r}}\right)^{\alpha} \tag{3}$$

where

$$\alpha = \frac{2C_{\rm p}}{ZR} \tag{4}$$

The mean jump frequency is defined as

$$\langle v^{i} \rangle = \int_{0}^{\infty} W(E, \sigma) v(E) dE$$
 (5)

Fig. 1 shows schematically the dependence of $W(E, \sigma)$ (dashed line) and of v(E) (dotted line) on the activation energy E. Also given on the same figure is the product $P(E) = W(E, \sigma) v(E)$. It is clear that the maximum of P(E) and correspondingly the value of the integral, depends on the position and on the shape of the first peak of $W(E, \sigma)$ because at higher energies the value of the jump frequency ν (and correspondingly the value of P(E)) drops very quickly. This is the reason why we can neglect so many details of the motion. In this way the problem is simplified considerably and the unknown explicit form of $W(E, \sigma)$ can be replaced by a Poissonian distribution between 0 and E_{max} (Fig. 1). In [4] it was shown that for $\sigma > RT$ the solution of Equation 5 is given with sufficient accuracy as

$$\langle v \rangle = v_0 \exp\left(-\frac{E_{\max}}{\sigma}\right)$$
 (6)



Figure 1 The dependence of probability distribution function $W(E, \sigma)$ (----), of jump frequency v(E) (....) and of the product $P(E) = W(E, \sigma) v(E)$ (--) on the activation energy E. (--W approximation).

The combination of Equations 3 and 6 leads to

$$\langle v \rangle = v_0 \exp\left[-\frac{E_{\text{max}}}{\sigma_{\text{r}}} \left(\frac{T_{\text{r}}}{T}\right)^{\alpha}\right]$$
 (7)

In general the mean jump frequency and shear viscosity are reverse proportional $\langle v \rangle \eta = K$, where according to [4, 5] $K = 2.5 \times 10^9$ Pa for most glass-forming systems. So, the temperature dependence of viscosity is

$$\eta = \eta_0 \exp\left[\frac{E_{\max}}{\sigma_r} \left(\frac{T_r}{T}\right)^{\alpha}\right]$$
(8)

where the pre-exponential constant η_0 is the lower possible value of the viscosity of the melt at high temperatures.

$$\eta_0 = \frac{K}{\nu_0} = 10^{-A} \, \text{Pas} \tag{9}$$

with $A \approx 2 \pm 1$. From Equations 8 and 9 it follows that if we determine T_r as a temperature at which the viscosity η_r is a given constant than the E/σ_r value can be assumed a constant for all substances because the parameter A varies over narrow limits.

It is useful to choose for a reference state the temperature T_g at which the viscosity is $\eta_g = 10^{12.5}$ Pa s. In this case

$$B = \frac{E_{\text{max}}}{\sigma_{\text{g}}} = 2.3 \,(12.5 + A) \approx 33 \tag{10}$$

Thus glass transition occurs usually at a temperature at which the degree of disorder scales for all substances is such that $E_{\rm max}/\sigma_{\rm g} = 33$. The temperature dependence of η can be expressed through $\eta_{\rm g}$ as

 $\eta = \eta_{\rm g} \exp\left\{B\left[\left(\frac{T_{\rm g}}{T}\right)^{\alpha} - 1\right]\right\}$ (11)

or

$$\lg \eta \approx 12.5 + 14.5 \left[\left(\frac{T_{g}}{T} \right)^{\alpha} - 1 \right]$$
 (12)

There is an easy way to obtain the value of α from the experimental data. At a given temperature T the slope L(T) of the lg η against 1/T curve is

$$L(T) = \alpha (12.5 + A) \left(\frac{T_g}{T}\right)^{\alpha - 1} T_g$$

$$\approx 14.5 \alpha \left(\frac{T_g}{T}\right)^{\alpha - 1} T_g \quad (13)$$

It is readily seen [4] that the exponent, α , can be determined by comparing the slopes at two temperatures T_1 and T_2 :

$$\alpha = 1 + \frac{\ln \left[L(T_1) / L(T_2) \right]}{\ln \left[T_2 / T_1 \right]}$$
(14)

Once the value of exponent α is known the determination of A is trivial. The determination of α is possible even if experimental data are available in a narrow region around T_g only. The slope $L(T_g)$ is given with 7% accuracy as

$$L(T_{\rm g}) = \alpha (12.5 + A) T_{\rm g} \approx (14.5 \pm 1) \alpha T_{\rm g}$$
(15)

The temperature dependence of viscosity of more than 40 substances is described successfully in terms of Equation 15. The theoretical curves are always in excellent agreement with the experimental data [5], as illustrated in Fig. 2. According to Equation 11, in coordinates $\lg \eta$ against $(10^3/T)^{\alpha}$, the experimental data lay on straight lines having intercepts $A \approx -2$ and slopes equal to $33(T_g/10^3)^{\alpha}$. The agreement of this prediction with existing experimental data [5] is illustrated in Fig. 3.

We find that the value of α increases simultaneously with the molar concentration x of modifying oxides. For most silicates this is described by the equation:

$$\alpha = 1 + 6x \tag{16}$$

The dependence of α on composition is given in Fig. 4 for a number of substances.



Figure 2 Temperature dependence of viscosity of some silicate melts. The theoretical curves are shown as lines $(-\Delta - 40PbO - 60SiO_2; - - 60PbO - 40SiO_2; - - 30Li_2O - 70SiO_2)$.



Figure 3 The temperature dependence of viscosity of some typical glassforming melts. Note that in these coordinates the theory predicts straight lines (\Box 20Na₂O-80SiO₂; \diamond Na₂O-2SiO₂; \diamond 13.5Na₂O-86.5B₂O₃; \bigcirc Na₂O-2B₂O₃).



Figure 4 The dependence of exponent α on composition ($\triangle B_2O_3 + SiO_2$; \Box silicates; \blacksquare borates).

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