

# Chapter 9

## Members of the Order Thermotogales: From Microbiology to Hydrogen Production

Martina Cappelletti

*Laboratory of General and Applied Microbiology, Department of Pharmacy  
and BioTechnology (FaBiT), University of Bologna, 40126 Bologna, Italy*

Davide Zannoni\*

*Department of Pharmacy and BioTechnology (FaBiT), University of Bologna,  
40126 Bologna, Italy*

and

Anne Postec, Bernard Ollivier

*Aix-Marseille Université, Université du Sud Toulon-Var, CNRS/INSU, IRD,  
MIO, UM 110, 13288 Marseille, Cedex 09, France*

|  |     |
|--|-----|
| Summary .....  | 197 |
| I. Introduction.....   | 198 |
| II. Habitat .....  | 198 |
| III. Metabolic Features .....                                    | 202 |
| A. Electron Donors .....   | 202 |
| B. Electron Acceptors .....                                      | 203 |
| C. End-Products of Metabolism .....                              | 204 |
| D. Oxygen Tolerance .....  | 205 |
| E. Hydrogen Sensitivity .....                                    | 206 |
| IV. Hydrogen Production by <i>Thermotogales</i> spp.....         | 206 |
| A. Thermodynamic Features .....                                  | 206 |
| B. The Hydrogenases of <i>Thermotoga</i> spp.....                | 209 |
| C. Hydrogen Production as a Function of Variable Substrate ..... | 212 |
| 1. Use of Simple Sugars and Polysaccharides.....                 | 213 |
| 2. Use of Carbon Sources from Various Waste-Residues .....       | 213 |
| D. H <sub>2</sub> Production Process and Culture Parameters..... | 216 |
| 1. Product Inhibition.....                                       | 216 |
| 2. pH Buffering System.....                                      | 217 |
| 3. Oxygen Exposure .....   | 217 |
| 4. Growth-Temperature and H <sub>2</sub> Production .....        | 218 |
| V. Future Perspectives .....                                     | 218 |
| Acknowledgements.....  | 219 |
| References .....   | 219 |

---

\*Author for correspondence, e-mail: [davide.zannoni@unibo.it](mailto:davide.zannoni@unibo.it)

## Summary

Members of the deep-branching order *Thermotogales* are widespread in various terrestrial, submarine and subterrestrial extreme environments. This bacterial order included both thermophilic and hyperthermophilic anaerobic microorganisms so far pertaining to ten genera. It is only recently (2011) that cultivation of a mesophilic member of this order belonging to a novel genus, *Mesotoga*, has been successful. All members, with the exception of *Mesotoga* spp., are recognized as high hydrogen producers having possible applications in biotechnology with a peculiar emphasis for members of the genus *Thermotoga* (e.g. *T. maritima* and *T. neapolitana*). The ecology, phylogeny and metabolism linked to hydrogen production of these bacteria, are reviewed.

## I. Introduction

Members of the order *Thermotogales* (Fig. 9.1) were represented as a deep-branching lineage within the phylogenetic tree (Huber et al. 1986; Reysenbach et al. 2001; Huber and Hannig 2006) thus suggesting that representatives of this order might have arisen early during the first steps of bacterial evolution. However the phylogenetic position of *Thermotogales*, as the nature (hyperthermophile or mesophile) of the ancestor of *Bacteria*, still remains a matter of debate (Brochier and Philippe 2002; Zhaxybayeva et al. 2009). Most of these Gram-negative anaerobic bacteria possess an outer sheath like structure called a “toga” ballooning over the ends of the cell (e.g. *Thermotoga* and *Thermosipho* spp.) (Huber et al. 1986; Antoine et al. 1997). Terminal protuberances on one end of the cells and single sphere containing several cells have also been observed in particular in *Fervidobacterium* spp. (Patel et al. 1985). *Thermotogales* range from thermophiles to hyperthermophiles having optimum temperature for growth above 80 °C with possible growth up to 90 °C (e.g. *Thermotoga maritima*, *T. neapolitana*, and *T. hypogea*). They are recognized as non-sporing rods occurring singly, in pairs or in chains with the absence of meso-

diaminopimelic acid in the peptidoglycan (Reysenbach et al. 2001; Huber and Hannig 2006). This order comprises ten genera: *Thermotoga*, *Thermosipho*, *Fervidobacterium*, *Geotoga*, *Petrotoga*, *Marinitoga*, *Thermococcoides* and the recently described genera *Kosmotoga*, *Oceanotoga* and *Defluviitoga* (Di Pippo et al. 2009; Jayasinghearachchi and Lal 2011; Ben Hania et al. 2012). Because of the almost identical 16S rRNA gene sequences of *K. olearia* and *Thermococcoides shengliensis*, and their many shared phenotypic features, *T. shengliensis* has been proposed to be reclassified within the genus *Kosmotoga* and named *K. shengliensis* (Feng et al. 2010; Nunoura et al. 2010). Recently, a mesophilic lineage (*Mesotoga*) within the *Thermotogales* has been evidenced by the detection of *Thermotogales* 16S rRNA gene sequences in many mesothermic environments (Nesbø et al. 2006, 2010). The mesophilic nature of such microorganisms has been established by their isolation and cultivation in 2011 (“*Mesotoga sulfurireducens*” strain PhosAc3, Ben Hania et al. 2011), in 2012 (*Mesotoga prima* strain MesG1.Ag.4.2, Nesbø et al. 2012) and in 2013 (*Mesotoga infera* strain VN100T, Ben Hania et al. 2013) with *Mesotoga prima* being the first described representative and type species of genus *Mesotoga* (Nesbø et al. 2012). All isolated *Mesotoga* species were confirmed to grow optimally at mesothermic conditions (40 °C for “*Mesotoga sulfurireducens*”, 45 °C for *M. infera* and 37 °C for *M. prima*) (Ben Hania et al. 2011, 2013; Nesbø et al. 2012) making them microorganisms of notable interest to understand bacterial evolution from mesophily to thermophily or *vice versa* (Nesbø et al. 2006; Ben Hania et al. 2011).

---

*Abbreviations:* CMC – Carboxy methyl cellulose; GAP deh – Glyceraldehyde-3-phosphate dehydrogenase; GghA – 1,4-β-D-glucan glucohydrolase; HEPES – 4-(2-hydroxyethyl)-1-piperazineethanesulfonic acid; MBS – Metabisulfite; NRO – NADH oxidoreductase; ORF – Open reading frames; RET – Reversed electron transport; ROS – Reactive oxygen species

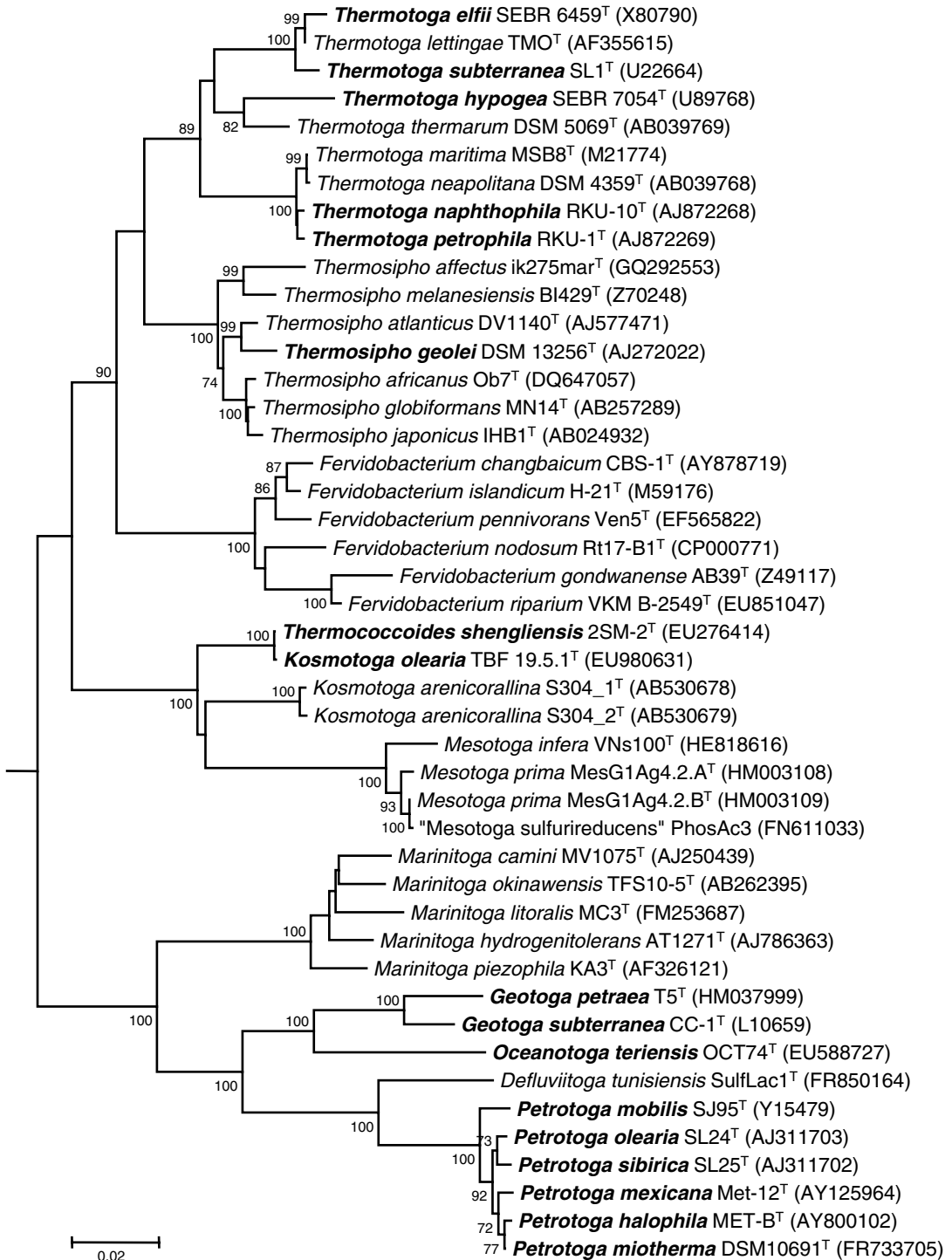


Fig. 9.1. Phylogenetic tree based on 16 rRNA gene sequences representing the position of oilfield microorganisms (bold characters) within the order *Thermotogales*. Neighbor joining method was used, calculation from 1,190 aligned pb, bootstrap from 1,000 replicates. *Aquifex aeolicus* (AJ309733) and *Bacillus subtilis* (K00637) were used as outgroup (not shown). Bar scale, 0.02 substitution per nucleotide.

## II. Habitat

Most of the thermophilic *Thermotogales* have been detected by molecular approaches and/or cultural approaches from geothermally heated environments (Table 9.1) (Huber and Hannig 2006). Most *Fervidobacterium* spp. have been isolated from low saline terrestrial hot springs (Patel et al. 1985; Huber et al. 1990; Andrews and Patel 1996; Friedrich and Antranikian 1996), which is also the case of *Thermotoga thermarum* (Windberger et al. 1989). Numerous slightly halophilic bacteria pertaining to the genera *Marinitoga* (Wery et al. 2001; Alain et al. 2002; Postec et al. 2005, 2010; Nunoura et al. 2007) and *Thermosipho* originated from marine ecosystems (e.g. deep-sea hydrothermal vents) (Huber et al. 1989; Antoine et al. 1997; Takai and Horikoshi 2000; Urios et al. 2004). Many thermophilic *Thermotogales* have been recovered from oilfield waters and facilities (Ollivier and Cayol 2005). They include *Thermotoga* spp. (*T. elfii*, *T. petrophila*, *T. hypogea*) (Magot et al. 2000; Ollivier and Cayol 2005), and *Kosmotoga olearia* (Di Pippo et al. 2009); species of both these genera were also isolated from submarine thermal vents (e.g. *T. neapolitana* and *K. arenicorallina*) (Windberger et al. 1989; Nunoura et al. 2010). Interestingly *Petrotoga*, *Geotoga*, and *Oceanotoga* spp. have representatives which originated only from oil reservoirs thus suggesting that such bacteria might be indigenous to these extreme environments and might possibly be relevant for enhancing oil recovery in the petroleum industry (Magot et al. 2000; Ollivier and Cayol 2005; Jayasinghearachchi and Lal 2011). However the indigenous character of *Thermotogales* to the oil field ecosystems should be considered with caution as their presence may result from anthropogenic activities after drilling operations or water injections during oil exploration (Magot et al. 2000). Besides geothermally heated sediments, only a few thermophilic *Thermotogales* have been isolated from anaerobic digesters. These include *Thermotoga lettingae* (Balk et al. 2002) and the recently described *Defluviitoga tunisiensis* (Ben Hania et al.

2012). *Thermotoga lettingae* was isolated from a thermophilic sulfate-reducing bioreactor operating at 65 °C with methanol as the sole substrate. *D. tunisiensis* was isolated from a mesothermic bioreactor (37 °C) treating lactoserum and phosphogypsum (Balk et al. 2002; Ben Hania et al. 2012). As mentioned above, there is now evidence for the presence of *Thermotogales* (*Mesotoga*) in mesothermic environments such as enrichment cultures degrading chlorinated compounds, temperate hydrocarbon-impacted sites, oil reservoirs, oil gas storage, anaerobic bioreactors treating solvent-containing pharmaceutical wastewater, and a gas-fed bioreactor treating sulfate- and zinc-rich wastewater (Ben Hania et al. 2011, 2013; Nesbø et al. 2006, 2012). In this respect, we may expect *Mesotoga* spp. to be of ecological relevance in the bioremediation of polluted sites (Ben Hania et al. 2011).

## III. Metabolic Features

### A. Electron Donors

Members of the *Thermotogales* are considered as heterotrophic fermentative microorganisms able to ferment sugars (Table 9.1) (Reysenbach et al. 2001; Huber and Hannig 2006). All thermophilic *Thermotogales* have been demonstrated to grow on complex organic substrates such as peptone and yeast extract, the latter being required to ferment sugars (Huber and Hannig 2006). Besides monosaccharides (e.g. glucose, fructose, xylose), di- and trisaccharides (e.g. sucrose, lactose, cellobiose, raffinose), *Thermotogales* can also ferment polysaccharides (Huber and Hannig 2006). Their use of cellulose has been reported, in particular for *Thermotoga maritima*, *T. neapolitana*, *Fervidobacterium islandicum*, and *Marinitoga camini* (Huber et al. 1986, 1990; Windberger et al. 1989; Wery et al. 2001; Huber and Hannig 2006). *Thermotoga maritima*, *T. neapolitana*, and *M. camini* were also reported to ferment glycogen (Huber et al. 1986; Windberger et al. 1989; Wery et al. 2001; Huber and Hannig 2006). The use of starch has been reported many times within the *Thermotogales* (e.g. *Thermotoga*, *Geotoga*,

Table 9.1. Characteristics of ten genera of Thermotogales order.

| Characteristic           | "Mesotoga"                         | <i>DeFluviitoga</i>     | <i>Oceanotoga</i> | <i>Kosmotoga</i>                         | <i>Marinitoga</i>  | <i>Geotoga</i>   | <i>Petrotoga</i>       | <i>Thermosiphonia</i>                | <i>Thermotoga</i>                                 | <i>Fervidobacterium</i> |
|--------------------------|------------------------------------|-------------------------|-------------------|--|--------------------|------------------|------------------------|--------------------------------------|---|-------------------------|
| Isolation source (s)     | Sediments, Mesothermic, Bioreactor | Mesothermic, Bioreactor | Oil reservoir     | Oil reservoir, Shallow hydrothermal vent | Hydrothermal vents | Oil reservoirs   | Oil reservoirs         | Hydrothermal vents and oil reservoir | Hydrothermal vents, oil reservoirs and bioreactor | Terrestrial hot springs |
| Temperature optimum (°C) | 37–40 °C                           | 55                      | 55–58             | 65                                       | 55–65              | 45–50            | 55–60                  | 65–75                                | 65–80   | 65–70                   |
| Oxygen tolerance (v/v)   | up to 2 %                          | up to 0.5 %             | nd                | Growth at 15 % O <sub>2</sub>            | No growth at 4 %   | Strict anaerobes | No growth with 0.2–1 % | No growth at 0.2–8 %                 | Do not grow aerobically                           | Strict anaerobes        |
| Electron acceptors       |                                    |                         |                   |  |                    |                  |                        |                                      |   |                         |
| Elemental sulfur         | +/-                                | +                       | +                 | -  | +                  | -                | +                      | +/-                                  | +/-   | +                       |
| Thiosulfate              | +/-                                | +                       | +                 | +  | +/-                | nd               | +/-                    | +/-                                  | +   | +/-                     |
| Nitrate                  | -                                  | nd                      | -                 | -  | -                  | nd               | -                      | -                                    | nd  | nd                      |
| Nitrite                  | -                                  | nd                      | nd                | -  | -                  | nd               | -                      | -                                    | nd  | nd                      |
| Sulfite                  | +/-                                | -                       | nd                | -  | -                  | nd               | +/-                    | -                                    | nd  | nd                      |
| Cystine                  | -                                  | nd                      | nd                | -  | +                  | nd               | -                      | +/-                                  | +/-   | nd                      |
| Sulfate                  | -                                  | -                       | -                 | + <sup>a</sup>                           | -                  | nd               | -                      | -                                    | -   | -                       |

(continued)

Table 9.1. (continued)

| Characteristic            | "Mesotoga"   | Defluviitoga                              | Oceanotoga  | Kosmotoga  | Marinitoga   | Geotoga  | Petrotoga  | Thermosiphona  | Thermotoga  | Fervido-<br>bacterium  |
|---------------------------|--|---|---|--|--|--|--|--|---|--|
| Substrate utilization     |  |   |   |  |  |  |  |  |   |  |
| Complex organic compounds | +  | +   | +   | +  | +/-  | +  | +  | +  | +   | +  |
| Carbohydrates             | +  | +   | +   | +  | +  | +  | +  | +  | +   | +  |
| Alcohols                  | nd   | nd  | nd  | nd   | nd   | nd   | nd   | nd   | +   | +  |
| Metabolic products        | Acetate, butyrate, isobutyrate, isovalerate, 2-methylbutyrate <sup>b</sup> | Acetate, H <sub>2</sub> , CO <sub>2</sub> | Acetate, H <sub>2</sub> , CO <sub>2</sub> , ethanol | Acetate, H <sub>2</sub> , CO <sub>2</sub> , lactate, isobutyrate, isovalerate <sup>b</sup> | Acetate, H <sub>2</sub> , CO <sub>2</sub> , butyrate, isovalerate <sup>b</sup> | Acetate, H <sub>2</sub> , CO <sub>2</sub> , ethanol <sup>b</sup> | Acetate, H <sub>2</sub> , CO <sub>2</sub> , ethanol <sup>b</sup> | Acetate, H <sub>2</sub> , CO <sub>2</sub> , L-alanine <sup>b</sup> | Acetate, H <sub>2</sub> , CO <sub>2</sub> , lactate, L-alanine <sup>b</sup> | Acetate, H <sub>2</sub> , CO <sub>2</sub> , L-alanine <sup>b</sup> |
| DNA G+C content (mol%)    | 45.3   | 33.6                                      | 26.8  | 42.5   | 28–29  | 29.5–29.9  | 31–39.8  | 29–33  | 39.2–50   | 33.7–40  |

Data were taken from Ben Hania et al. (2011, 2013); Nesbø et al. (2012) ("Mesotoga"); Ben Hania et al. (2012) (*Defluviitoga*); Jayasinghachari and Lal (2011) (*Oceanotoga*); Alain et al. (2002); Nunoura et al. (2007); Postec et al. (2005) and Wery et al. (2001) (*Marinitoga*); Davey et al. (1993) (*Geotoga*); L'Haridon et al. (2002); Lien et al. (1998) and Miranda-Tello et al. (2004, 2007) (*Petrotoga*); Antoine et al. (1997); Huber et al. (1989); L'Haridon et al. (2001); Takai and Horikoshi (2000) and Urios et al. (2004) (*Thermosiphona*); Balk et al. (2002); Fardeau et al. (1997); Huber et al. (1986); Jannasch et al. (1988); Jeanthon et al. (1995); Ravot et al. (1995); Takahata et al. (2001) and Windberger et al. (1989) (*Thermotoga*) and Andrews and Patel (1996); Friedrich and Antranikian (1996); Huber et al. (1990) and Patel et al. (1985) (*Fervidobacterium*)

nd No data available; – does not enhance growth; + enhanced growth; ± enhanced growth for some, but not all, species

<sup>a</sup>Slight growth enhancement, but no sulfide produced

<sup>b</sup>Metabolic products which are written in bold characters are produced by all species. For those which are not written in bold characters, they are produced depending on species

*Petrotoga*, *Thermosipho*, *Fervidobacterium*, *Marinitoga*, *Kosmotoga* spp.) (Huber and Hannig 2006). Xylanolytic activity has been detected in *T. maritima*, *T. hypogea*, and *Petrotoga* spp. (e.g. *P. mobilis* and *P. olearia*) (Huber et al. 1986; Davey et al. 1993; Fardeau et al. 1997; Lien et al. 1998). *Marinitoga camini* was shown to degrade chitin and *F. pennovorans* to degrade keratin (Friedrich and Antranikian 1996; Wery et al. 2001).

The alcohols possibly fermented by *Thermotogales* include mannitol (e.g. *T. naphthophila*), and glycerol (e.g. *T. lettingae*, *T. neapolitana* and *F. nodosum*) (Patel et al. 1985; Takahata et al. 2001; Van Ooteghem et al. 2004; Huber and Hannig 2006). Methanol was poorly fermented by *T. lettingae*, however, in the presence of thiosulfate or elemental sulfur as terminal electron acceptors, or methanoarchaea as hydrogenotrophic partners, methanol was more quickly used (12 days for the oxidative process instead of 30 days for the fermentative process) (Balk et al. 2002). Methanol utilization has also been demonstrated for *T. subterranea*, *T. elfii*, *T. maritima* and *T. neapolitana* by the same authors (Balk et al. 2002).

Regarding organic acids utilization, pyruvate served as energy source for some *Thermotoga* and *Petrotoga* spp. (Huber and Hannig 2006), and there is one report on formate utilization by *Thermotoga lettingae* (Balk et al. 2002). Besides formate, which was used only in the presence of thiosulfate as electron acceptor, *T. lettingae* was the first *Thermotogales* reported to ferment lactate (Balk et al. 2002). Thereafter, the use of lactate has been also evidenced in “*Mesotoga sulfurireducens*” and in *M. infera* where the presence of elemental sulfur as terminal electron acceptor was required thus suggesting that lactate was oxidized, but not fermented by this bacterium (Ben Hania et al. 2011, 2013). *T. lettingae* was also shown to oxidize acetate in the presence of thiosulfate or hydrogenotrophic methanoarchaea as terminal electron acceptors in agreement with results for previously described thermophilic or mesophilic acetate-degrading bacteria coupled to a methanogenic partner or an electron acceptor (Balk et al. 2002).

## B. Electron Acceptors

*Thermotogales* do not only use a wide range of organic substrates as energy sources but have also the ability to reduce sulfur-containing compounds (e.g. elemental sulfur, and thiosulfate, but not sulfate) into sulfide (Table 9.1) (Huber and Hannig 2006). Amongst *Thermotogales* genera, *Geotoga* is the only genus in which no thiosulfate-reducing species was reported (Davey et al. 1993). The ability of *Thermotogales* to reduce elemental sulfur in the presence of sugars was first reported for *T. maritima* and was found stimulatory for its growth (Huber et al. 1986). However, this reductive process was suggested to be a detoxifying process preventing H<sub>2</sub> accumulation rather than an energy-yielding electron sink reaction (Huber et al. 1986; Huber and Hannig 2006). A similar conclusion could have been drawn regarding thiosulfate reduction by *Thermotogales*. However growth experiments with *T. maritima* and *T. neapolitana* in the presence of thiosulfate suggested that thiosulfate reduction could be regarded as an energy-yielding reaction through an oxidative phosphorylation process from sugars (Ravot et al. 1995). Indeed, for both bacteria, despite important improvements of growth observed in the presence of thiosulfate, there was no significant change in the end-products of sugar metabolism (Ravot et al. 1996). Besides thiosulfate and elemental sulfur, Fe(III) was also used as electron acceptor by *T. maritima* and in its presence, hydrogen oxidation was demonstrated (Vargas et al. 1998). While one study indicated that *T. maritima* may gain energy by iron respiration (Vargas et al. 1998), other reports suggested Fe(III) as an additional electron sink together with thiosulfate and elemental sulfur to prevent the inhibitory effect of hydrogen on growth (Huber et al. 1986; Schröder et al. 1994; Huber and Stetter 2001). The ability of *T. maritima* to reduce Fe(III) raises questions on its possible involvement in reducing heavy metals and should merit further attention. In the presence of thiosulfate as terminal electron acceptor, *T. lettingae* was shown to oxidize

hydrogen (Balk et al. 2002). While the possible use of cystine as electron acceptor has been established for *Marinitoga*, *Thermotoga*, and *Thermosipho* species (Huber and Hannig 2006), only *T. lettingae* was reported to use anthraquinone -2,6-disulfonate as electron acceptor (Balk et al. 2002). Results obtained with *Thermotogales* regarding the possible use of sulfur compounds as electron acceptors, indicate they may play a crucial ecological role in mineralizing organic matter in hot ecosystems. This is particularly true for *Thermotogales* originating from shallow or deep sea hydrothermal vents (e.g. *Thermosipho* and *Marinitoga* spp.) where different oxidized forms of sulfur compounds, including elemental sulfur and thiosulfate, are not limiting.

### C. End-Products of Metabolism

The major end-products of sugar metabolism by thermophilic *Thermotogales* are acetate, hydrogen, and CO<sub>2</sub> (Table 9.1) (Reysenbach et al. 2001; Huber and Hannig 2006). Surprisingly, while the recent isolated mesophiles “*Mesotoga sulfurireducens*”, *M. prima* and *M. infera* were shown to produce mainly/only acetate from sugar utilization, there is no report on H<sub>2</sub> production by these microorganisms (Ben Hania et al. 2011, 2013; Nesbø et al. 2012). Moreover, in contrast to *M. prima* which was described as a fermentative bacterium (Nesbø et al. 2012), *M. infera* was shown to rather oxidize its substrates in the presence of elemental sulfur as terminal electron acceptor (Ben Hania et al. 2013). Further researches on the physiological traits of *Mesotoga* spp. will be therefore of interest to understand the overall metabolic capabilities within the *Thermotogales*. It was found, for example, that acetate was also produced during methanol fermentation by *Thermotoga lettingae* (Balk et al. 2002). Lactate production was detected in particular by *T. maritima* and was dependent on culture conditions (e.g. H<sub>2</sub> partial pressure) (Janssen and Morgan 1992; Schröder et al. 1994). It was also produced by *Marinitoga*

*camini* when growing on sugars (Wery et al. 2001). Ethanol has been measured at many occasions (e.g. *Geotoga*, *Petrotoga*, *Kosmotoga*, and *Oceanotoga* spp.) together with isovalerate, isobutyrate, and/or propionate (e.g. *M. camini*, *K. olearia*), but also alpha-aminobutyrate, hydroxyphenyl-acetate or phenylacetate (Huber and Hannig 2006) as end-products of sugar metabolism. Studies with *T. maritima* indicated that this bacterium used glucose *via* the Embden-Meyerhof glycolytic pathway and, to a lesser extent, *via* the Entner-Doudouhoff pathway (Schröder et al. 1994; Selig et al. 1997; Huber and Hannig 2006). However the importance of the use of both pathways in other *Thermotogales* when fermenting sugars is still poorly documented and deserves further investigation. Notably, it was demonstrated in *T. neapolitana* that glucose was taken up *via* an active transport system that was energized by an ion gradient generated by ATP derived from substrate-level phosphorylation (Galperin et al. 1996; Huber and Hannig 2006). It is established, that several *Thermotogales* have a high ratio of acetate produced *versus* sugar consumed, thus indicating that they are good candidates for H<sub>2</sub> production from the biomass approaching the theoretical maximum yield of 4 mol H<sub>2</sub> per mol glucose consumed (Schröder et al. 1994; Van Ooteghem et al. 2004; Eriksen et al. 2011). This is emphasized by the capacities of many species to use various carbohydrates including cellulose, hemicelluloses and starch together with proteinaceous compounds. Besides acetate, lactate and hydrogen, L-alanine was also found as a significant end-product of sugar fermentation by *Thermotoga elfii*, *Fervidobacterium islandicum*, *F. nodosum*, *F. gondwanense*, and *Thermosipho africanus* with up to 0.52 mol L-alanine produced per mol glucose consumed (*T. africanus*). In contrast, *T. maritima* and *T. neapolitana* were found to be poor L-alanine producers (Ravot et al. 1996). In the presence of thiosulfate, a decrease of the L-alanine/acetate ratio was observed for *F. islandicum*, *T. africanus*, *T. elfii*, *Thermotoga* SEBR 7054, and



*Thermotoga lettingae* (Ravot et al. 1996; Balk et al. 2002). For all these bacteria, the presence of thiosulfate caused a shift of metabolism with more acetate and less L-alanine being produced from sugars thus enabling them to obtain more ATP from substrate level phosphorylation via the formation of acetyl-CoA. It was hypothesized that similarly to the hyperthermophilic archaeon, *Pyrococcus furiosus*, L-alanine production from glucose fermentation resulted from alanine transferase activity coupled with glutamate dehydrogenase activity (Ravot et al. 1996). Therefore, because of a similar type of sugar metabolism by members of the *Thermococcales* (e.g. *Pyrococcus furiosus* and *Thermococcus profundus*), domain *Archaea*, placed as a deep-branching lineage within the phylogenetic tree, L-alanine production by *Thermotogales* has been interpreted as a remnant of an ancestral metabolism (Ravot et al. 1996). Interestingly, L-alanine was also produced when *T. lettingae* grew on methanol as energy source in the presence of thiosulfate or elemental sulfur and this was the first report of L-alanine formation from a C1 substrate. In contrast, in the presence of a methanogenic partner (e.g. *Methanothermobacter thermoautotrophicus*) methanol was completely oxidized to CO<sub>2</sub> (Balk et al. 2002). A complete oxidation of acetate was also observed when *T. lettingae* was cocultured with an hydrogenotrophic methanoarchaea, while L-alanine was produced from acetate in the presence of thiosulfate (Balk et al. 2002).

#### D. Oxygen Tolerance

Although *Thermotogales* are recognized as strict anaerobes, there are evidences that they may cope with limited amount of oxygen during their growth (Table 9.1). *T. maritima* may grow in the presence of 0.5 % of oxygen (Le Fourn et al. 2008), *T. neapolitana* was shown to grow under oxygen concentrations ranging from 1 to 6 % (Van Ooteghem et al. 2004) (see Sect. IV.A). *Kosmotoga olearia*, an oil-field isolate, was reported to grow in the presence of 15 % oxygen (Di Pippo et al. 2009).

This indicates that *Thermotogales* may use biochemical strategy(ies) to face oxidative stress as already reported for other strict anaerobes (e.g. sulfate-reducing bacteria) (Krekeler et al. 1998; Teske et al. 1998; Cypionka 2000; Dolla et al. 2006). *Thermotoga maritima* has been studied in recent years with regard to the strategy(ies) possibly used to deal with O<sub>2</sub> and reactive oxygen species (ROS) such as peroxides. Yang and Ma (2005) have purified and characterized a heterodimeric NADH oxidase catalyzing oxygen to hydrogen peroxide. They proposed this enzyme together with other hydrogen peroxide scavenging enzymes as acting in an oxygen-removing system. Le Fourn and collaborators (2008) using differential proteomics analyses identified a flavo-protein, homologous to the rubredoxin oxygen reductase (FprA) of *Desulfovibrio* sp. that was overproduced when *T. maritima* was cultivated under oxic conditions. They provided evidence that by reducing oxygen to water, this enzyme had a crucial role in protecting the bacterium against oxygen and suggested that NADH oxidase and rubredoxin oxygen reductase were involved in this process (Le Fourn et al. 2008). However, they outlined that the direct reduction of oxygen to water by FprA might be a preferred system as compared to the production of hydrogen peroxide, known to be highly toxic to cells. Later on, Le Fourn et al. (2011) showed that *T. maritima* cells could consume oxygen at a rate of 41.5 nmol min<sup>-1</sup> per mg of total protein and demonstrated that this bacterium reduced oxygen via a three-partner chain involving an NADH oxidoreductase (NRO), a rubredoxin (Rd) together with the rubredoxin oxidoreductase mentioned above (FprA), known as a flavo-diiron protein. They concluded that the genes coding for the three components O<sub>2</sub> reduction system were acquired by the *Thermococcales*, domain *Archaea*, through a single horizontal gene transfer event (Le Fourn et al. 2011). Because of the position of *Thermotogales* and *Thermococcales* within the phylogenetic tree, it has been suggested that such mechanism has been important for the first anaerobes to adjust to the presence of

traces of oxygen on the “primordial” Earth. Oxygen uptake has also been observed when *T. maritima* was grown in a 2.3-L bioreactor under controlled oxygen exposure (Lakhal et al. 2010). Transcriptomic analysis, indicated that when exposed to oxygen for a short time, *T. maritima* had to deal with oxygen but also with the peroxides produced. The oxygen reductase FprA appeared as primary consumer of oxygen, followed by alkyl hydroperoxide reductase and peroxiredoxin-encoding genes as main ROS-scavenging systems when higher concentrations of O<sub>2</sub> were reached (Lakhal et al. 2011). It is noteworthy that the expression of the gene *hyd* that encodes the single hydrogenase of *T. maritima* was drastically affected by the presence of oxygen (Lakhal et al. 2011). These data are in accordance with the known sensitivity of hydrogenases towards oxygen (Vincent et al. 2005). Regarding the anaerobic metabolism of *T. maritima*, batch cultures indicated that it significantly decreased the redox potential (E<sub>h</sub>) of the culture medium to about -480 mV (Lakhal et al. 2010) similarly to what was observed for the strict anaerobic methanarchaea (Fetzer and Conrad 1993). Finally, under oxidative conditions, Lakhal et al. (2010) observed that glucose consumption rate by *T. maritima* decreased with a concomitant shift in glucose metabolism towards lactate production.

From these results, we may conclude that despite the high sensitivity of *T. maritima* to oxygen, this bacterium adapted an adequate strategy to face exposures to this gas (see Sect. IV.B for more details). This may explain why this hyperthermophilic bacterium can survive and even grow in shallow hydrothermal vents where partially oxygenated conditions cannot be precluded.

#### E. Hydrogen Sensitivity

Hydrogen which accumulates during the fermentation processes of carbohydrates by *Thermotogales*, with the exception of *Mesotoga* spp. (see also § III.D) is known to inhibit the growth of most of them (Huber and Hannig 2006). No growth occurred when

cultures of *T. maritima* were pressurized with hydrogen-containing gas (H<sub>2</sub>/CO<sub>2</sub>=80:20; 300 kPa) (Huber et al. 1986). Similar observations were done with *Thermotoga thermarum* and *T. neapolitana* (Windberger et al. 1989), *Petrotoga miotherma*, *Geotoga petraea*, and *Thermosiphon melaniensis* (Davey et al. 1993; Antoine et al. 1997). However for all these microorganisms, growth inhibition could be overcome by gassing the headspace with N<sub>2</sub> or N<sub>2</sub>/CO<sub>2</sub> or by the addition of S<sup>0</sup> or thiosulfate (e.g. *Petrotoga mobilis*) which served as an electron acceptor in the culture medium; concomitantly H<sub>2</sub>S was formed. Depending on microorganisms (see comments above), the addition of elemental sulfur and/or thiosulfate may or may not have a stimulatory effect on growth. H<sub>2</sub> removal in the gas phase may also result from co-cultures of *Thermotogales* with thermophilic to hyperthermophilic methanarchaea (e.g. *Methanococcus*, *Methanopyrus* spp.) or other hydrogen oxidizing archaeons (e.g. *Archaeoglobus* or *Ferroglobus* spp.) (Huber and Hannig 2006). Some genera are hydrogen tolerant. *Geotoga subterranea* was not inhibited by the hydrogen concentration mentioned above (Davey et al. 1993). *Marinitoga camini* and *M. piezophila* reached maximum cell concentrations with 0 % H<sub>2</sub> while no growth occurred with 80 % H<sub>2</sub> (Wery et al. 2001; Alain et al. 2002), *M. hydrogenotolerans* can grow in the presence of 100 % H<sub>2</sub> in the gas phase (Postec et al. 2005) and this makes it the most hydrogen tolerant member of the *Thermotogales*. This confirms that *Thermotogales*, depending on species, have different H<sub>2</sub> sensitivities as reported earlier by Ravot et al. (1996).

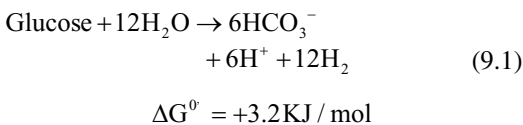
## IV. Hydrogen Production by *Thermotogales* spp.

### A. Thermodynamic Features

The organisms described in this chapter are mainly thermophilic or hyperthermophilic anaerobes with temperature optima above 65 °C. As stated in the preceding paragraphs,

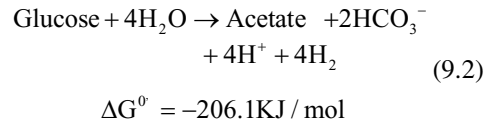
many of these, such as *Thermotoga maritima* and *T. neapolitana* are capable of performing fermentative hydrogen production from a wide variety of substrates. Indeed, thermophilic hydrogen production benefits from some general advantages of performing such a process at elevated temperatures thank to a lower viscosity, better mixing, less risk of contamination, higher reaction rates and no need for reactor cooling (Wiegel et al. 1985). As already stated in Chap. 1, to make hydrogen production economically sustainable, organisms are needed that can generate hydrogen or directly or indirectly from biomass. As cellulose and hemicellulose are the most abundant polysaccharides in nature, xylose and glucose are the predominant monomeric sugars available (Kapdan and Kargi 2006). Further, starch and sucrose can be abundantly present in plants as storage material. Interestingly, the bacterial species belonging to *Thermotoga* have the capacity to hydrolyze most of the substrates derived from biomass. For example, as also reported in Chap. 8, both *Caldicellulosiruptor* and *Thermotoga* spp. contain a variety of glycoside hydrolases and transferases stating their metabolic capacity (Vanfossen et al. 2008).

A few thermodynamic considerations clearly indicate that under standard conditions (reactants concentration equal to 1 M, at 25 °C and pH 7.0), glucose oxidation to CO<sub>2</sub> and H<sub>2</sub> has a positive Gibbs energy change (reaction 9.1). This means that H<sub>2</sub> production requires an input of extra energy.



As shown in Table 9.2, most of the available literature reports that under optimal growth conditions, the oxidation of one hexose molecule will result in the formation of a variable number of hydrogen molecules ( $>2 \leq 4$ ) in addition to acetate and CO<sub>2</sub>. The maximum amount of ATP is obtained through production of acetate but

this can only occur if all the reducing equivalents are disposed in the form of hydrogen molecules. Apparently, the *a priori* requirement to get a significant hydrogen production yield is to keep a low hydrogen partial pressure through the use of a hydrogen-consuming system (Schink and Stams 2006). Under this latter condition, as shown in reaction 9.2, glucose oxidation to acetate, CO<sub>2</sub> and H<sub>2</sub> has a significantly negative Gibbs energy change.



In most fermentative hydrogen producers, catabolism *via* the Embden-Meyerhof pathway generates reducing equivalents in the form of NADH at the level of the glyceraldehyde-3-phosphate dehydrogenase (GAP deh) and reduced ferredoxin by the pyruvate:ferredoxin oxidoreductase reaction. Under standard conditions, the mid-point potentials of NAD<sup>+</sup>/NADH and ferredoxin<sup>ox</sup>/ferredoxin<sup>red</sup> are -320 mV and -380 mV, respectively (Thauer et al. 1977). Recycling of these redox couples can be accomplished by various reactions such as, for example, the production of lactate though reduction of pyruvate by NADH; however, the feasibility of these reactions is *a priori* determined by the standard Gibbs free energy change ( $\Delta G^0$ ) of each specific conversion step. This latter consideration predicts that the production of H<sub>2</sub> by reduction of H<sup>+</sup> with NADH is a thermodynamically unfavorable process as expected by the low mid-point potential ( $E^0 = -414$  mV) of the H<sup>+</sup>/H<sub>2</sub> redox couple. Although the situation is more favorable in the case of ferredoxin ( $E^0 = -380$  mV) the formation of other products such as ethanol and lactate is thermodynamically more feasible. Thus, although the microbial reduction of protons to lead H<sub>2</sub> generation is a metabolic unexpected process, for certain thermophiles (see Table 9.1) the amount of hydrogen produced is close to

Table 9.2. H<sub>2</sub> production rates and H<sub>2</sub> yields from various sugars conversion by *Thermotoga* spp.

| Strain                | Carbon source | T° | Conc.     | Initial pH | Type of reactor  | H <sub>2</sub> production rate (mmol <sub>H<sub>2</sub></sub> /L/h) | H <sub>2</sub> yield (mol <sub>H<sub>2</sub></sub> /mol <sub>substrate</sub> ) | By-products      | References             |
|-----------------------|---------------|----|-----------|------------|------------------|---|--|------------------|------------------------|
| <i>T. maritima</i>    | Glucose       | 80 | 10–15 mM  | 6.5        | Batch            | 10.0  | 4.0  | Acetate          | Schröder et al. (1994) |
| <i>T. elfii</i>       | Glucose       | 65 | 10 g/L    | 7.5        | Controlled batch | 2.7   | 3.3  | Acetate          | Ván Niel et al. (2002) |
| <i>T. elfii</i>       | Glucose       | 65 | 7 g/L     | 7.5        | Batch            | –   | 3.3  | Acetate          | De Vrije et al. (2002) |
| <i>T. petrophila</i>  | Glucose       | 80 | 0.1 % w/v | 7.0        | Batch            | –   | 3.8  | Acetate, lactate | Takahata et al. (2001) |
| <i>T. naphrophila</i> | Glucose       | 80 | 0.1 % w/v | 7.0        | Batch            | –   | 4  | Acetate, lactate | Takahata et al. (2001) |
| <i>T. maritima</i>    | Glucose       | 80 | 7.5 g/L   | 6.5        | Batch            | 8.2   | 1.7  | –                | Nguyen et al. (2008a)  |
| <i>T. neapolitana</i> | Glucose       | 75 | 7.5 g/L   | 7.0        | Batch            | 8.7   | 1.8  | –                | Nguyen et al. (2008a)  |
| <i>T. neapolitana</i> | Glucose       | 77 | 7.0 g/L   | 7.5        | Batch            | –   | 3.2  | Acetate butyrate | Nguyen et al. (2010a)  |
| <i>T. neapolitana</i> | Glucose       | 75 | 5 g/L     | 7.5        | Controlled batch | 4.25  | 3.2  | Acetate, lactate | Ngo et al. (2011b)     |
| <i>T. neapolitana</i> | Glucose       | 85 | 2.5 g/L   | 7.5        | Batch            | 0.9   | 3.8  | Acetate, lactate | Munro et al. (2009)    |
| <i>T. neapolitana</i> | Glucose       | 80 | 5 g/L     | 8.0        | Batch            | –   | 2.4  | Acetate, lactate | Eriksen et al. (2008)  |
| <i>T. maritima</i>    | Arabinose     | 80 | 5 g/L     | 8.0        | Batch            | 0.6   | 3.2  | Acetate, lactate | Eriksen et al. (2011)  |
| <i>T. neapolitana</i> | Arabinose     | 80 | 5 g/L     | 8.0        | Batch            | 1.0   | 3.8  | Acetate, lactate | Eriksen et al. (2011)  |
| <i>T. maritima</i>    | Xylose        | 80 | 5 g/L     | 8.0        | Batch            | 0.4   | 2.7  | Acetate, lactate | Eriksen et al. (2011)  |
| <i>T. neapolitana</i> | Xylose        | 80 | 5 g/L     | 8.0        | Batch            | 1.5   | 3.4  | Acetate, lactate | Eriksen et al. (2011)  |
| <i>T. neapolitana</i> | Xylose        | 75 | 5 g/L     | 7.5        | Controlled batch | 3.9   | 2.8  | Acetate, lactate | Ngo et al. (2012)      |
| <i>T. neapolitana</i> | Xylose        | 75 | 5 g/L     | 7.5        | Controlled batch | 3.3   | 2.2  | Acetate, lactate | Ngo et al. (2011b)     |
| <i>T. neapolitana</i> | Sucrose       | 75 | 5 g/L     | 7.5        | Controlled batch | 1.9   | 5.0  | Acetate, lactate | Ngo et al. (2011b)     |
| <i>T. neapolitana</i> | Glycerol      | 75 | 5 g/L     | 7.5        | Batch            | –   | 1.0  | Acetate, lactate | Ngo and Sim (2011)     |
| <i>T. neapolitana</i> | Cellulose     | 80 | 0.5 % w/v | 7.5        | Batch            | –   | 2.2  | –                | Nguyen et al. (2008b)  |

four molecules per molecule of glucose oxidized, suggesting that in these microorganisms the thermodynamic constraints are somehow overcome as the growth conditions are quite far from the standard physiological values. Indeed, the actual Gibbs energy change as a function of both the substrates and products concentrations (see Eq. 9.3) predicts that even the reduction of H<sup>+</sup> by NADH becomes exergonic (−4.7 kJ/mol) if the partial H<sub>2</sub> concentration [P(H<sub>2</sub>)] is kept as low as 10<sup>−2</sup> kPa.

$$\Delta G = \Delta G^\circ + RT \ln\left(\frac{[C][D]}{[A][B]}\right) \quad (9.3)$$

Further, the thermodynamic of the process is affected by temperature at which the reaction takes place according to Eq. (9.4)

$$\Delta G^\circ = \Delta H - T\Delta S^\circ \quad (9.4)$$

which says that at temperatures higher than standard conditions (25 °C), the Gibbs free energy change for the overall reaction from glucose to acetate (Eq. 9.1) is more favorable. A second consideration that might explain why thermophiles show such unexpected H<sub>2</sub> yields, is based on the fact that as previously shown by Thauer et al. (1977) and Amend and Plyasunov (2001), the hydrogen partial pressure needed to make reaction (9.2) feasible varies from 0.022 kPa at 25 °C to 2.2 kPa at 100 °C. Thus, at room temperature, hydrogen must be rapidly removed to avoid the inhibition of reaction (9.2) while the presence of 10<sup>2</sup> higher hydrogen concentration is tolerated at 100 °C.

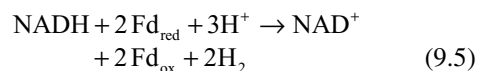
Another possible explanation for the hydrogen formation from redox couples having a mid-point potential higher than −414 mV (E<sup>0</sup> of H<sup>+</sup>/H<sub>2</sub>) might be the presence of a reversed electron transport (RET) mechanism linked to membrane bound NAD-dependent hydrogenases. Although this mechanism has never been described in thermophiles, its presence in the genus *Clostridium* (*Cl. tetanomorphum*), where a

sodium gradient is used to drive the reduction first of ferredoxin and then for hydrogen production (Boiangiu et al. 2005), does not exclude *a priori* that other fermenting bacteria support the uphill reduction of H<sup>+</sup> by NADH through the use of RET. Alternatively, it has clearly been shown by Schut and Adams (2009) that in cells of *Thermotoga maritima* (*T. maritima*) ferredoxin is a more suitable reducing agent for hydrogen production than NADH.

### B. The Hydrogenases of *Thermotoga* spp.

As overviewed in Chaps. 2, 3, 4, and 8, the enzymes responsible for hydrogen production (H<sub>2</sub>) combining hydrogen protons and reducing equivalents (2H<sup>+</sup>+2e<sup>−</sup>) are the hydrogenases (EC 1.12.99.6 and EC 1.12.7.2) also catalyzing the reversible oxidation of molecular hydrogen. In anaerobic thermophiles, two main types of hydrogenases, based on their metal content, are found: [Fe-Fe] and [Ni-Fe] hydrogenases. Further, hydrogenases can use different types of electron carriers, e.g. NAD, NADP, FAD and ferredoxin (Fd), which are reduced in the glycolytic pathway and in particular during the conversions of both glyceraldehyde-3-P to 3-P-glycerate and pyruvate to acetyl-CoA. In most fermentative hydrogen producers, reduced electron carriers generated in these steps (NADH and Fd<sub>red</sub>) need to be re-oxidized to keep the glycolytic pathway functioning and this disposal mechanism can be different among the different thermophilic hydrogen producers (Jenney and Adams 2008).

As many other bacterial species, *Thermotoga maritima* uses the Embden-Meyerhof pathways for glycolysis resulting in acetate, lactate, ethanol, CO<sub>2</sub> and H<sub>2</sub>. However, recycling of reducing equivalents is performed by a trimeric [Fe-Fe] hydrogenase which uses both NADH and Fd<sub>red</sub> in a 1:1 ratio to generate hydrogen (see Eq. 9.5).



This so-called “flavin-based bifurcating enzyme” is coupling the exergonic oxidation of  $\text{Fd}_{\text{red}}$  ( $E^{\circ}$  of  $\text{Fd}_{\text{ox}}/\text{Fe}_{\text{red}} = -453$  mV) to drive the unfavorable oxidation of NADH ( $E^{\circ}$  of  $\text{NAD}^+/\text{NADH} + \text{H}^+ = -320$  mV) to produce  $\text{H}_2$  ( $E^{\circ} = -420$  mV) (Schut and Adams 2009). As this mechanism is favored by low hydrogen pressures, in the case of higher  $\text{H}_2$  pressures, a switch from acetate to lactate production is seen (Huber et al. 1986). This however does not seem to affect the bifurcating mechanism of the hydrogenase, which presumably remains the same.

The anaerobically purified “bifurcating” hydrogenase of *T. maritima*, the enzyme being inactivated in the presence of even trace amounts of oxygen, is composed of three subunits – HydA (73 kDa), HydB (68 kDa) and HydC (18 kDa) – in a 1:1:1 ratio stoichiometry. The holoenzyme showed an apparent molecular mass of 500 kDa at pH 7.0 and one of 150 kDa at pH 10.0. The enzyme contained loosely bound FMN along with more than 30 Fe per heterotrimer in line with sequence analysis prediction (Buckel and Thauer 2012). Based on this latter approach, HydA subunit should harbor the active site interacting with hydrogen ( $\text{H}_2$ ). This prediction was confirmed by showing that HydA alone, after dissociation of the trimeric-complex with urea, can catalyze the reduction of viologen dyes with  $\text{H}_2$ . Besides the hydrogen interacting site, HydA contains  $3 \times [4\text{Fe-4S}]$  and  $2 \times [2\text{Fe-2S}]$  iron-sulfur clusters with a 43 % sequence similarity to the monomeric  $[\text{Fe-Fe}]$  hydrogenase of *Clostridium pasteurianum*. HydA of *T. maritima* differs however in having a C-terminal extension with a  $[2\text{Fe-2S}]$  binding site which is lacking in the monomeric enzyme from *C. pasteurianum*.

The HydB subunit shows a 70 % similarity to the gene product HndC of the  $\text{NADP}^+$ -reducing  $[\text{Fe-Fe}]$  hydrogenase from *Desulfovibrio fructosovorans* and 60 % similarity to NuoF of the NADH:ubiquinone oxidoreductase from *E. coli*. Within the sequence, there are two highly conserved stretches, one featuring  $\text{NAD}^+$  binding sites

and the other recalling orthodox FMN binding sites. The C-terminal part contains Cys motifs that could bind three  $[4\text{Fe-4S}]$  clusters. At its N-terminus HydB contains four Cys residues that are suggested to be involved in binding a  $[2\text{Fe-2S}]$  cluster (Verhagen et al. 1999).

The smaller subunit of this trimeric bifurcating hydrogenase, HydC, contains four Cys residues arranged in a motif which is highly similar (58 %) to motifs in *E. coli* Nuo and *D. fructosovorans* HndA, which are supposed to bind a  $[2\text{Fe-2S}]$  cluster.

The above reported information, gives a picture of the HydABC complex that is tentatively shown in Fig. 9.2 where a series of assumptions were made, namely: (a) the binding site for reduced ferredoxin ( $\text{Fd}_{\text{red}}$ ) at HydC; (b) the presence of a second FMN loosely bound to HydB; (c) the  $[\text{Fe-Fe}]$  center plus  $[4\text{Fe-4S}]$  cluster as part of the active site of the hydrogenase in subunit HydA.

It has been proposed that the three genes encoding HydABC in *T. maritima* are arranged in a cluster *hydCBA* that is most likely a transcription unit (Verhagen et al. 1999). Clustered genes for proteins with sequence similarity to HydABC product are also found in many other anaerobic bacteria such as for example *Clostridium ljungdahlii* (Kopke et al. 2010), *Acetobacterium woodii* (Poehlein et al. 2012), and *Moorella thermoacetica* (Pierce et al. 2008), although these gene products have not been characterized. Interestingly, the enzyme complex from the anaerobe *Thermoanaerobacter tengcongensis* is composed of four subunits rather than three. Most likely, this is due to the fact that in this latter species the HydA homolog lacks the C-terminal extension with the  $[2\text{Fe-2S}]$  cluster so that a fourth subunit, homologous to the C-terminal extension, is required (Soboh et al. 2004).

Another interesting observation recently done by Thauer et al. (2010) is that electron-bifurcating  $[\text{Fe-Fe}]$  hydrogenases are not found in the Archaea domain which appear to only contain  $[\text{Ni-Fe}]$ - and/or  $[\text{Fe}]$ -hydrogenases (Thauer et al. 2010).

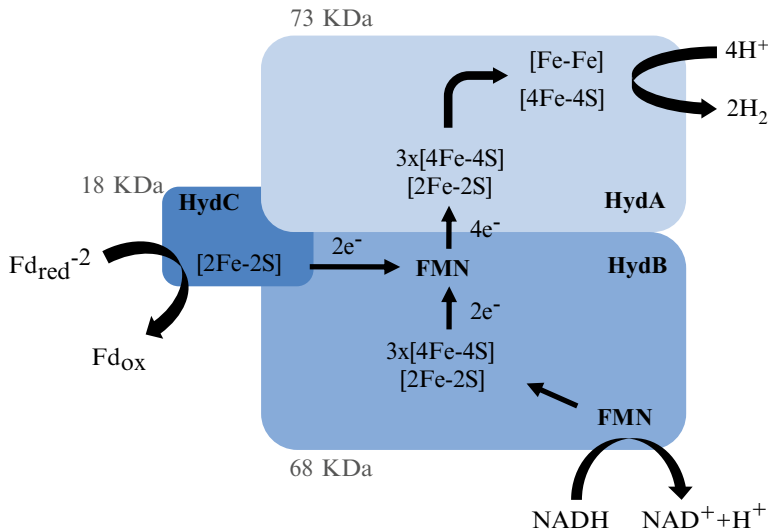
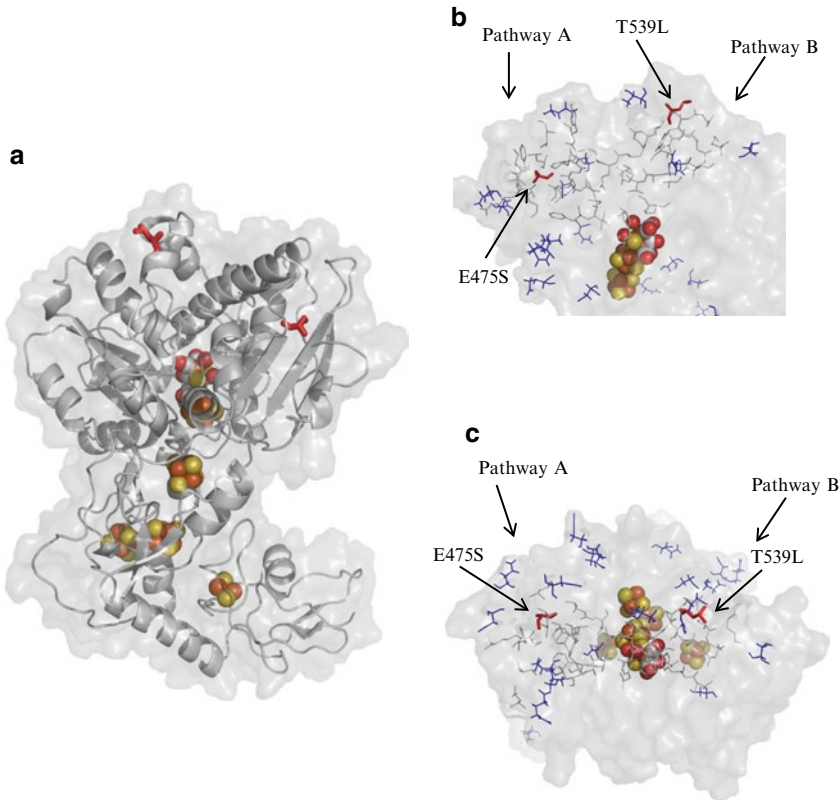


Fig. 9.2. Tentative representation of the structure and function of the HydABC complex from *Thermotoga maritima* (See text for details).

As mentioned in Sect. III.D, several strains of *Thermotogales*, such as *Petrogala miotherma*, *Thermosiphon africanus*, *Thermotoga elfii*, *Fervidobacterium pennavorans* and *Thermotoga neapolitana*, are able to tolerate microaerophilic growth conditions and efficiently produce H<sub>2</sub> as a by-product of their metabolism (Van Ooteghem et al. 2002). In particular, *T. neapolitana* showed the highest H<sub>2</sub> production (25–30 % v/v) in these conditions (Van Ooteghem et al. 2004). Through the use of a bioinformatics approach it has been shown that the operon structure of *T. neapolitana* is the same as *T. maritima* in both the ordering and spacing of the ORFs (open reading frames) (Tosatto et al. 2008). In details, a high sequence conservation is preserved from a minimum of 75 % to a maximum of 91 % for all gene products with a sequence identity attributed to the [Fe-Fe] hydrogenase subunits of 85–91 %. Notably, the HydA subunits of both species share a 91 % sequence identity, are of the same length, and can be aligned without gaps. At the DNA level, the two sequences share 82 % identity, for a total of 375 mutated nucleotides, comprising three fully mutated

codons corresponding to mutations R363E (GAA → AGG), E475S (GAG → TCC) and T539L (ACA → GTG). Taking into account the sequences of *T. petrophila* and *T. maritima* showing that R363 is not conserved between the two species (GAA → AAA), it has been concluded that only two residues, E475S and T539L of the *T. neapolitana* HydA subunit appear to be subjected to strong selection (Tosatto et al. 2008). Apparently, the functional differences between *T. neapolitana* and *T. maritima* reside in these latter subtle changes possibly involved in the conformation of the active site (H-cluster) near the surface of the protein. As suggested by Cohen et al. (2005) in the *C. pasteurianum* [FeFe] hydrogenase crystal structure, there might be two alternative gas diffusion pathways defining a hydrophobic channel toward the H-cluster active site. As suggested in Fig. 9.3, the possibility of a selective effect on gas accessibility based on the size of side-chains and charge distribution on the protein surface at the entrance of the hypothetical gas channels, B (Threonine 539) and A (Serine 475) has been discussed in detail by Tosatto et al. (2008).



**Fig. 9.3.** Structural model of *Thermotoga neapolitana* HydA protein. **Panel A.** Model is shown as cartoon beneath a semi-transparent surface. Iron–sulfur clusters are shown as *spheres*. **Panel B.** Close-up of upper half of model. Residues forming part of hydrophobic channel pathways *A* and *B* are shown as *blue lines*. Residues mutating between *T. neapolitana* and *Thermotoga maritima* HydA proteins are shown as *red lines*. Two mutated residues forming part of hydrophobic channel pathways *A* (E475S) and *B* (T539L), are in *red* and indicated by *arrows*. **Panel C.** Same model as in *panel B*, rotated by 90° around the x-axis to show a *top view* of the molecule, where hydrophobic channel entrances are located (Tosatto et al. 2008).

### C. Hydrogen Production as a Function of Variable Substrate

As reported above, *Thermotoga* spp. are able to grow on a wide array of simple sugars and polysaccharides, including starch,  $\beta$ -1,4 glucan (cellulose), and hemicellulose (xylan, laminarin and mannan) (Connors et al. 2006). This capacity is consistent with the production of a diverse set of proteins and enzymes that are devoted to the uptake and processing of carbohydrates (Vanfossen et al. 2008). The use of functional genomics-based approaches has provided important insights into the various mechanisms employed by these microor-

ganisms to assimilate and metabolize carbohydrates, and has helped to identify the specific genes and operons involved (Nguyen et al. 2001, 2004). *T. maritima* genome encodes for the largest number of glycoside hydroxylases of any sequenced thermophile (Chhabra et al. 2003). These enzymes specifically hydrolyze the glycosidic bond between two or more carbohydrates or between a carbohydrate and a non-carbohydrate moiety and function during the mobilization of complex carbohydrates for subsequent metabolism. *T. neapolitana* produces enzymes such as  $\alpha$ -galactosidase, a laminarinase, and two cellulases (endo-1,4- $\beta$ -glucanases) that



have orthologs in *T. maritima* (Zverlov et al. 1997; Bok et al. 1998; King et al. 1998), but this microorganism also produces several unique glycoside hydrolases. One example is a 1,4- $\beta$ -D-glucan glucohydrolase (GghA), which hydrolyzes cellotetraose, celotriose, cellobiose, and lactose (McCarthy et al. 2004). *T. petrophila* slightly differs from *T. maritima* and *T. neapolitana* with respect to the utilization of certain sugars, growing weakly on cellulose and, in the presence of a mixture of monosaccharides, utilizing glucose to a significantly lesser extent than the other two species (Takahata et al. 2001; Frock et al. 2012). Unlike *T. maritima* and *T. neapolitana*, *T. elfii* failed to grow on sucrose and carboxy methyl cellulose (CMC) (Van Niel et al. 2002). *T. maritima* was shown to have a preference for complex carbohydrates, as growth in the presence of monosaccharides was slower than growth in the presence of oligo/poly-saccharides (Chhabra et al. 2003).

### 1. Use of Simple Sugars and Polysaccharides

*Thermotoga* spp. produce hydrogen from a wide range of organic materials including complex carbohydrates and wastes/biomass rich in sugars. Simple sugars such as glucose and xylose are readily biodegradable and thus preferred as reference substrates for studying biochemical and physiological aspects of the hydrogen production by these bacteria. A wide variety exists among *Thermotogales* with respect to the utilization of sugars for growth and H<sub>2</sub> production that is consistent with the genetic diversity between the strains and the degree of optimization of the process for H<sub>2</sub> production (Frock et al. 2012). Table 9.2 summarizes the results of hydrogen production by *Thermotoga* spp. obtained with different types of simple and complex carbohydrates and different conditions of growth. Under optimal conditions, the oxidation of glucose and xylose will at best result in the formation of 4 mol of H<sub>2</sub> per mole of hexose and 3.33 mol<sup>-1</sup> mol of H<sub>2</sub> per mole of pentose, respectively. Maximum hydrogen

yields, both from hexoses or pentoses, are obtained with acetate as fermentation product. Lower yields are associated to the formation of more reduced end products compared to acetate, such as butyrate, propionate and alcohols (ethanol, butanol) and lactic acid. It would be therefore important to establish the actual bacterial metabolism resulting in acetate as end product (Kaushik and Debabrata 2004).

*T. neapolitana* converted effectively sucrose to H<sub>2</sub> with H<sub>2</sub> yield of 4.95 mol<sub>H<sub>2</sub></sub>/mol<sub>sucrose</sub> (Table 9.2) despite the poor fructose based metabolism reported for this strain (de Vrije et al. 2009, 2010). Woodward et al. (2002) reported the list of sugars that were used by *T. maritima* for H<sub>2</sub> production. This strain was shown to preferentially use glucose, fructose, and galactose, whereas mannose and lactose metabolisms mainly produced carbon dioxide (Woodward et al. 2002). *T. neapolitana* and *T. maritima* were able to use the glucose-based complex carbohydrates, starch and cellulose, for hydrogen fermentation, although H<sub>2</sub> yields obtained with raw cellulose (30 mL<sub>H<sub>2</sub></sub>/g<sub>cellulose</sub>) were significantly lower than with starch (180 mL<sub>H<sub>2</sub></sub>/g<sub>starch</sub>) (Nguyen et al. 2008a). The pretreatment of cellulose with chemical agents (e.g. ionic liquids) that could disrupt the hydrogen-bonding network of the polysaccharide significantly increased its degradability (Nguyen et al. 2008b).

### 2. Use of Carbon Sources from Varied Waste-Residues

Most studies on hydrogen production in *Thermotoga* have used glucose as carbon source although hydrogen production at a large scale should be based on cheap and renewable substrates, such as industrial/agricultural wastes and residues. These materials have often high contents of hexose and pentoses stored in carbohydrate polymers that are ideal conversion substrates for H<sub>2</sub> generation (Ntaikou et al. 2010). The major criteria that have to be met for the selection of substrates suitable for fermenta-

tive biohydrogen production are availability, cost, carbohydrate content, biodegradability and concentration of inhibitory compounds (Hawkes et al. 2002). As shown in Table 9.3, *T. neapolitana* was widely used in technical processes with variable feedstock sources owing to its many advantageous properties including tolerance of moderate oxygen amount (6–12 %) and resistance to high H<sub>2</sub> partial pressure (Van Ooteghem et al. 2002, 2004). This strain was shown to successfully produce H<sub>2</sub> from lignocellulosic materials such as rice straw, wheat straw and *Mischantus* (de Vrije et al. 2002, 2009; Nguyen et al. 2010b; Eriksen et al. 2011), algal biomasses (Nguyen et al. 2010c; Dipasquale et al. 2012) and food waste materials, such carrot pulp, cheese whey and molasses (Table 9.3) (de Vrije et al. 2010; Cappelletti et al. 2012). Many physical and chemical along with structural and compositional factors in complex feedstock sources often hinder the biological digestibility (Chang et al. 2001). Because of that reason, pre-treatment methods including wet oxidation under alkaline conditions, mechanical pre-treatment, mild and concentrated acid hydrolysis and solvent extractions were required for an efficient utilization of these feedstock sources promoting the accessibility of polysaccharides in the substrates for enzymatic hydrolysis (Ntaikou et al. 2010). Molasses and cheese whey were effectively converted into H<sub>2</sub> by both attached- and suspended-cells of *T. neapolitana* without any pre-treatment needed (Cappelletti et al. 2012). Besides high yields in terms of H<sub>2</sub> production, the *Thermotoga* ability of utilizing different sugars in complex mixtures is essential in making H<sub>2</sub> production from biomass successful. Simultaneous utilization of glucose and xylose has also been observed in *T. neapolitana* (de Vrije et al. 2009), while in this microorganism, catabolite repression of lactose has been demonstrated in the presence of glucose (Vargas and Noll 1996). A preference for glucose was also shown by *T. neapolitana* when a mixture of glucose and fructose was present in the medium although both sugars were consumed at the

same time (de Vrije et al. 2010). No mechanism of carbon catabolite repression has yet been defined for *T. maritima*.

In addition to carbohydrate-rich residues, *T. neapolitana* was also shown to produce H<sub>2</sub> by fermenting waste glycerol that is the main byproduct of the large-scale productions of bio-diesel (Ngo et al. 2011a; Ngo and Sim 2011). As compared with mesophilic *Enterobacter aerogenes* fermentation of glycerol, higher H<sub>2</sub> yield was obtained with *T. neapolitana* (2.7 mol<sub>H<sub>2</sub></sub> mol<sup>-1</sup><sub>glycerol</sub> instead of 0.9 mol<sub>H<sub>2</sub></sub> mol<sup>-1</sup><sub>glycerol</sub>) (Ito et al. 2005) (Table 9.3).

Non-sugar substrates, such as yeast extract and trypticase that are components of the typical *Thermotoga* growth media, were shown to contribute to 9–12 % of the total H<sub>2</sub> production (d'Ippolito et al. 2010; Cappelletti et al. 2012). These media components represent undefined sources of nitrogen and carbon for bacteria that were shown to increase cell biomass and H<sub>2</sub> production in *T. maritima* and *T. neapolitana* cultures growing on glucose, glycerol, cheese whey and molasses (Nguyen et al. 2008a; d'Ippolito et al. 2010; Ngo and Sim 2011; Cappelletti et al. 2012). van Niel et al. (2002) reported that growth of *T. elfii* was completely dependent on yeast extract, while in the absence of tryptone, lower H<sub>2</sub> yields were obtained. Alternative nitrogen sources such as soybean meal or canola meal alone supported growth but H<sub>2</sub> production rates were reduced (Drapcho et al. 2008).

Because of the complexity and richness of some industrial/agricultural wastes, the utilization of these complex feedstock sources for H<sub>2</sub> production by *Thermotoga* could allow the reduction of the process-associated cost by simplifying the culture medium. A growth medium composed only by NH<sub>4</sub>Cl, K<sub>2</sub>HPO<sub>4</sub>, NaCl, buffer and cysteine-HCl (see Sect. IV.D.b) led to an efficient H<sub>2</sub> production from molasses with *T. neapolitana* (Cappelletti et al. 2012). The omission of vitamin and trace elements solutions, some inorganic elements and nitrogen sources reduced the fermentation cost without a significant loss in H<sub>2</sub> production. Further cost

Table 9.3. H<sub>2</sub> production rates and H<sub>2</sub> yields from various industrial/agricultural wastes conversion by *Thermotoga* spp. described in the literature.

| Strain                | T° | Feedstock                     | Main carbon source                 | Additional treatment                               | H <sub>2</sub> production rate (mmol/L/h) | H <sub>2</sub> yield                                       | References                                |
|-----------------------|----|-------------------------------|------------------------------------|--|---|--|---|
| <i>T. elfii</i>       | 65 | <i>Miscanthus</i>             | Glucose, xylose                    | Mechanical and NaOH                                | –   | 1.1 mol <sub>H<sub>2</sub></sub> /mol <sub>sugar</sub>     | de Vrije et al. (2002)                    |
| <i>T. neapolitana</i> | 80 | <i>Miscanthus</i>             | Glucose, xylose, arabinose         | NaOH, Ca(OH) <sub>2</sub> and enzymatic hydrolysis | 13.1                                      | 3.2 mol <sub>H<sub>2</sub></sub> /mol <sub>hexose</sub>    | de Vrije et al. (2009)                    |
| <i>T. neapolitana</i> | 75 | Rice straw                    | Glucose, xylose                    | Combined treatment                                 | 4.7                                       | 2.7 mmol <sub>H<sub>2</sub></sub> /g <sub>straw</sub>      | Nguyen et al. (2010b)                     |
| <i>T. neapolitana</i> | 75 | Algal biomass                 | Starch, dextrans, oligosaccharides | Enzymatic hydrolysis                               | 227.3                                     | 2.5 mol <sub>H<sub>2</sub></sub> /mol <sub>glucose</sub>   | Nguyen et al. (2010c)                     |
| <i>T. neapolitana</i> | 80 | Carrot pulp                   | Glucose, fructose, sucrose         | Enzymatic hydrolysis                               | 12.5                                      | 2.7 mol <sub>H<sub>2</sub></sub> /mol <sub>hexose</sub>    | de Vrije et al. 2010                      |
| <i>T. neapolitana</i> | 75 | Biodiesel manufacturing waste | Glycerol                           | Removal of methanol/ ethanol and solids            | –   | 2.73 mol <sub>H<sub>2</sub></sub> /mol <sub>glycerol</sub> | Ngo et al. (2011a) and Ngo and Sim (2011) |
| <i>T. neapolitana</i> | 77 | Molasses                      | Sucrose, glucose, fructose         | –  | 1.2                                       | 2.95 mol <sub>H<sub>2</sub></sub> /mol <sub>hexose</sub>   | Cappelletti et al. (2012)                 |
| <i>T. neapolitana</i> | 77 | Cheese whey                   | Lactose, glucose, galactose        | –  | 0.9                                       | 2.5 mol <sub>H<sub>2</sub></sub> /mol <sub>hexose</sub>    | Cappelletti et al. (2012)                 |

reductions were achieved by replacing the lab-grade NaCl with non-refined sea salt and the cysteine-HCl with metabisulfite (see Sect. IV.D.b) (Cappelletti et al. 2012).

#### D. $H_2$ Production Process and Culture Parameters

Environmental parameters such as pH, hydrogen partial pressure, media components and temperature, are key factors as they influence the metabolism and therefore the fermentation end products. Thus, optimization of these processes and culture parameters is required to give enhanced  $H_2$  yields.

##### 1. Product Inhibition

Strategies for growth under  $H_2$  inhibition conditions have been developed in hypethermophiles including *T. maritima* and *T. neapolitana*.  $H_2$ -producing archaea and bacteria can use sulfur compounds such as elemental sulfur, polysulfides, and cystine as alternative electron acceptors (Adams 1990; Drapcho et al. 2008). The use of Fe(III) as electron acceptor was also observed in *T. maritima* when  $H_2$  levels became inhibitory (Vargas et al. 1998). Nevertheless, the metabolic pathways of hydrogen formation are sensitive to  $H_2$  concentrations and are subject to end-product inhibition. Therefore, the  $H_2$  partial pressure is an extremely important factor for hydrogen synthesis.  $H_2$  production is a means by which bacteria re-oxidise reduced ferredoxin and hydrogen-carrying coenzymes, and these reactions are less favourable as the  $H_2$  concentration in the liquid rises (Hawkes et al. 2002). Consequently,  $H_2$  production decreases and the metabolic pathways shift to production of more reduced substrates such as lactate, ethanol, acetone, butanol, or alanine (Levin et al. 2004). Several strategies have been developed to avoid the negative effect of  $H_2$  accumulation. These include vigorous mixing to avoid super-saturation (Lay 2000), utilization of  $H_2$  permeable membrane to remove dissolved  $H_2$  from mixed liquor (Liang et al. 2002) and sparging with inert nitrogen. The application

of the latter technique to *T. neapolitana* growing on either glucose or waste glycerol increased the  $H_2$  production by 50–80 % (Nguyen et al. 2010a; Ngo et al. 2011b). However, d'Ippolito et al. (2010) showed that sparging with nitrogen had a little influence on  $H_2$  yield at low ratio between the volumes of culture and headspace. Gas sparging became more important with the increase of the liquid fraction. They observed the highest  $H_2$  yield with a culture/headspace volume ratio of 1:3. An increased ratio between gas and liquid phase volumes was also associated to a decreased synthesis of lactic acid in cultures of *Thermotoga maritima* (Schröder et al. 1994).

In addition to culture/headspace volume ratio, the stirring regime and the substrate concentration were shown to influence  $H_2$  production most probably because of their correlation to the dissolved  $H_2$  concentration (Hawkes et al. 2002). A moderate agitation of the cultures (at 75 rpm) was shown to almost double the  $H_2$  production by *T. neapolitana* cultures in 20 h of growth on glucose (Van Ooteghem et al. 2002). Using the same type of culture and carbon source,  $H_2$  production rate was improved by increasing the stirring speed from 300 to 400 rpm. However, speeds of 500 and 600 rpm did negatively affect this fermentative process (Ngo et al. 2011b).

Considering the influence of the substrate concentration on the  $H_2$  production process, Nguyen et al. (2008a) reported that concentrations of glucose over 15 g/L had inhibitory effects on cell growth and  $H_2$  production in *T. neapolitana* and *T. maritima* strains batch cultures. The growth and  $H_2$  content showed the highest values at the initial glucose concentration of 7.5 g/L for both strains. In *T. neapolitana* cultures growing on xylose, the maximal values of biomass and cumulative  $H_2$  production were obtained at an initial substrate concentration of 5.0 g/L, while higher concentrations of xylose were not favorable for *T. neapolitana* growth and  $H_2$  formation (Ngo et al. 2012). However, at substrate concentration of 5.0 g/L, the converted  $H_2$  yield from xylose was lower than at the initial xylose concentration of 2 g/L

suggesting that the change in xylose concentration remarkably affected not only H<sub>2</sub> production itself but also the substrate utilisation (Ngo et al. 2012). The best performing initial concentration of waste glycerol (3.0 g/L) was less than half than the pure glycerol (7.0 g/L) despite they resulted in comparable H<sub>2</sub> productions (Ngo and Sim 2011). This indicates different potentials of the two types of glycerol sources to release a specific amount of H<sub>2</sub>.

## 2. pH Buffering System

A rapid decrease in pH is observed in cultures of *Thermotoga* spp. fermenting sugars to H<sub>2</sub> causing, in some cases, the process to stop before all the substrate is consumed (Eriksen et al. 2008). Experiments with pH adjustment showed that when cultures were neutralized with either increased initial buffer or injection of NaHCO<sub>3</sub> or NaOH, glucose was completely consumed and H<sub>2</sub>/acetic acid productions increased proportionally. Both the type of buffer and the initial pH have significant effect on H<sub>2</sub> production process. Organic and inorganic buffer systems have been tested in literature resulting in different H<sub>2</sub> productions depending on the growth conditions and buffers concentration in the culture medium. HEPES resulted to be the best performing buffer when compared to HPO<sub>4</sub>:H<sub>2</sub>PO<sub>4</sub>, Tris-HCl, Mops, Pipes buffers in experiments using *T. neapolitana* batch cultures growing on glucose (Cappelletti et al. 2012). Effective H<sub>2</sub> productions were also obtained with HEPES-buffered medium containing raw material feedstocks such as cheese whey, molasses and glycerol waste as carbon sources for *T. neapolitana* (Ngo et al. 2011a; Cappelletti et al. 2012). The good buffering properties of HEPES might be due to its pK (7.55) that is near the optimum for the growth of *T. neapolitana*. Itaconic acid was also successfully used to overcome pH-induced limitations of H<sub>2</sub>-producing *T. neapolitana* cultures growing glucose. The buffering capacity of this carbohydrate was tested after that it was found to be poorly metabolized by this strain (Van Ooteghem

et al. 2004). Its applicability for H<sub>2</sub> productions from industrial residues was demonstrated by Ngo and Sim (2011). The addition of itaconic acid into the culture medium of *T. neapolitana* growing on waste glycerol increased the process performance by almost 40 % (Ngo and Sim 2011).

In addition to the buffer, the initial pH value was shown to have a significant effect on growth and H<sub>2</sub> production of *Thermotoga* spp. Anna et al. (1991) indicated that the pH control is crucial to the H<sub>2</sub> formation pathway because of the effects of pH on the hydrogenase activity. The optimum initial pH for *T. neapolitana* suspended-cells ranged from 6.5 to 7.5 depending on both the substrate and the conditions of growth (Ngo et al. 2011b). Interestingly, an higher pH range (7.7–8.5) yielded the highest hydrogen production in experiments with glucose-grown *T. neapolitana* attached-cells on ceramic supports (Cappelletti et al. 2012). An initial pH of 7.0 provided the most promising results in terms of H<sub>2</sub> and acetic acid productions in *T. neapolitana* growing on xylose (Ngo et al. 2012). The optimum initial pH values for growth and hydrogen production from glucose were 6.5–7.0 for *T. maritima* and 6.5–7.5 for *T. neapolitana*, respectively. The best performing initial pH for H<sub>2</sub> production from glycerol by *T. neapolitana* was 7.0–7.5 (Ngo and Sim 2011). The application of initial pH above 8 resulted in a decrease of cumulative H<sub>2</sub> production as well as cell concentration suggesting the influence of pH over the metabolism pathway of the bacteria (Ngo and Sim 2011).

## 3. Oxygen Exposure

Hydrogen production by *Thermotoga* strains is a hyperthermophilic anaerobic process, thus, high temperatures (70–90 °C) and strictly anaerobic conditions must be initiated and maintained in the reactor vessel during production.

Some researchers have reported that low concentrations of oxygen are tolerated by both *T. neapolitana* (Tosatto et al. 2008) and *T. maritima* (Le Fourn et al. 2008) and an O<sub>2</sub>

insensitive hydrogenase have been described in *T. neapolitana* (Käslin et al. 1998). Van Ooteghem et al. (2002, 2004) reported that microaerobic metabolism increased the H<sub>2</sub> yield from *T. neapolitana* up to values higher than the theoretical 4 mol<sub>H<sub>2</sub></sub>/mol<sub>glucose</sub> possible from fermentative metabolism (Table 9.2); however, this result was not confirmed by other researchers who observed H<sub>2</sub> production after the injection of O<sub>2</sub>, but with rate and extent that were lower than those found in cultures without O<sub>2</sub> (Eriksen et al. 2008; Munro et al. 2009).

Prevention of O<sub>2</sub> exposure could be difficult on an industrial scale and requires expensive reducing agents (cysteine-HCl). Anaerobic conditions can be initiated, maintained, and monitored in the reactor vessels by (1) flushing media with nitrogen gas, (2) heating or boiling of the media to remove dissolved oxygen, (3) adding chemical agents such as sodium sulfite or cysteine-HCl to consume residual O<sub>2</sub> in the liquid, (4) adding resazurin to act as visible redox indicator, and (5) maintaining positive pressure in headspace to prevent air contamination (Drapcho et al. 2008). Cysteine-HCl at concentration of 0.5–1 g/L was commonly added to provide reducing conditions in media and consume residual oxygen (de Vrije et al. 2002; Van Ooteghem et al. 2002, 2004). The addition of a reducing agent to H<sub>2</sub> production resulted to be fundamental even when complex feedstock sources were supplemented to the culture medium. However, to reduce the cost of the process, the utilization of cheaper reducing agents was attempted. For example, the replacement of cysteine-HCl with metabisulfite (MBS) gave promising results in terms of both medium cost (90 % reduction) and H<sub>2</sub> yield in *T. neapolitana* cultures growing on molasses (Cappelletti et al. 2012). Conversely, in the cheese whey tests, the attempt to replace cysteine with MBS led to poor performances (Cappelletti et al. 2012).

#### 4. Growth-Temperature and H<sub>2</sub> Production

Optimum temperature of growth differs among *Thermotoga* species and has to be considered in the bioreactor operating pro-

cess to maximize H<sub>2</sub> production rates (Munro et al. 2009; Nguyen et al. 2008a). Optimum temperature of growth and H<sub>2</sub> production is 77 °C for *T. maritima*, 88 °C for *T. petrophila* and *T. naphthophila* and only 66 °C for *T. elfii* (Jannasch et al. 1988; Huber and Hannig 2006). Cultures of *T. neapolitana* grown at 77 and 85 °C exhibited the greatest rate and extent of H<sub>2</sub> production (Munro et al. 2009).

Advantages to using high temperatures for fermentation process include (1) to reduce the likelihood of contamination by H<sub>2</sub>-consuming organisms that lessens the need for sterilization of media and equipment, (2) to favour the catalytic activity of hydrogenase of evolving H<sub>2</sub> (Adams 1990) (3) to directly utilize industrial organic wastewaters that are often discharged at elevated temperatures; (4) to avoid cooling down processes usually required by mesophilic fermentations that in large scale generate excess heat (Drapcho et al. 2008).

## V. Future Perspectives

This Chapter summarizes our present knowledge on the microbiology, physiology, and biochemistry of the *Thermotogales* order with the aim to better define problems and challenges linked to H<sub>2</sub> production. In this respect, it is worth noting that important improvements have been recently made through optimization of both the bioprocess parameters and *Thermotoga* spp. to be used. Although the identification of suitable feed-stocks for fermentative hydrogen production was done, more research work to improve hydrogen production rates and yields, is required. The use, for example, of *Thermotoga* strains metabolically engineered and the development of a “two stage process” is likely to improve H<sub>2</sub> production. Indeed, this latter approach involves the fermentation of the selected substrate to both hydrogen and organic acids by *Thermotoga* spp. in the first stage and, in a second stage, either an additional energy extraction or the generation of highly-valuable products by exploiting the effluent of the first stage reactor. An alternative approach to improve H<sub>2</sub> production might also be achieved through a specific

bioreactor configuration ameliorating both biomass concentration and substrate conversion efficiency by employing biomass retention systems such as granules, flocs or biofilm-formation supports.

## Acknowledgements

The research leading to results obtained by D.Z. and M.C. on H<sub>2</sub>-production by *Thermotoga* spp. has received funding from the Italian Ministry of Agriculture, Food and Forestry (MIPAAF) under grant ‘Combined production of hydrogen and methane from agricultural and zootechnical wastes through biological processes (BIO-HYDRO)’.

## References

- Adams MWW (1990) The metabolism of hydrogen by extremely thermophilic, sulfur-dependent bacteria. *FEMS Microbiol Rev* 75:219–237
- Alain K, Marteinsson VT, Miroshnichenko ML, Bonch-Osmolovskaya EA, Prieur D, Birrien JL (2002) *Marinitoga piezophila* sp. nov., a rod-shaped, thermo-piezophilic bacterium isolated under high hydrostatic pressure from a deep-sea hydrothermal vent. *Int J Syst Evol Microbiol* 52:1331–1339
- Amend JP, Plyasunov AV (2001) Carbohydrates in thermophile metabolism: calculations of the standard molal thermodynamic properties of aqueous pentoses and hexoses at elevated temperatures and pressures. *Geochim Cosmochim Acta* 65:3901–3917
- Andrews KT, Patel BKC (1996) *Fervidobacterium gondwanense* sp. nov., a new thermophilic anaerobic bacterium isolated from non-volcanically heated geothermal waters of the Great Artesian Basin of Australia. *Int J Syst Bacteriol* 46:265–269
- Anna J, Shigetoshi A, Adams MWW (1991) The extremely thermophilic eubacterium, *Thermotoga maritima*, contains a novel iron-hydrogenase whose cellular activity is dependent upon tungsten. *J Biol Chem* 266:13834–13841
- Antoine E, Cilia V, Meunier J, Guezennec J, Lesongeur F, Barbier G (1997) *Thermosiphon melanesiensis* sp. nov., a new thermophilic anaerobic bacterium belonging to the order Thermotogales, isolated from deep-sea hydrothermal vents in the southwestern Pacific Ocean. *Int J Syst Bacteriol* 47:1118–1123
- Balk M, Weijma J, Stams AJ (2002) *Thermotoga lettin-gae* sp. nov., a novel thermophilic, methanol-degrading bacterium isolated from a thermophilic anaerobic reactor. *Int J Syst Evol Microbiol* 52:1361–1368
- Ben Hania W, Ghodbane R, Postec A, Brochier-Armanet C, Hamdi M, Fardeau M-L, Ollivier B (2011) Cultivation of the first mesophilic representative (“mesotoga”) within the order Thermotogales. *Syst Appl Microbiol* 34:581–585
- Ben Hania W, Ghodbane R, Postec A, Hamdi M, Ollivier B, Fardeau M-L (2012) *Defluvitoga tunisiensis* gen. nov., sp. nov., a thermophilic bacterium isolated from a mesothermic and anaerobic whey digester. *Int J Syst Evol Microbiol* 62:1377–1382
- Ben Hania W, Postec A, Aullo T, Ranchou-Peyruse A, Erauso G, Brochier-Armanet C, Hamdi M, Ollivier B, Saint-Laurent S, Margot M, Fardeau ML (2013) *Mesotoga infera* sp. nov., a novel mesophilic member of the order Thermotogales, isolated from an underground gas storage in France. *Int J Syst Evol Microbiol* 63:3003–3008. doi:1099/ijs.0.047993-0
- Boiangiu CD, Jayamani E, Brugel D, Hermann G, Kim J, Forzi L, Hedderich R, Vgenopoulou I, Pierik AJ, Steuber J, Buckel W (2005) Sodium ion pumps and hydrogen production in glutamate fermenting anaerobic bacteria. *J Mol Microbiol Biotechnol* 10:105–119
- Bok JD, Yernool DA, Eveleigh DE (1998) Purification, characterization, and molecular analysis of thermostable cellulases CelA and CelB from *Thermotoga neapolitana*. *Appl Environ Microbiol* 64:4774–4781
- Brochier C, Philippe H (2002) Phylogeny: a non-hyperthermophilic ancestor for Bacteria. *Nature* 417:244
- Buckel W, Thauer RK (2012) Energy conservation via electron bifurcating ferredoxin reduction and proton/Na<sup>+</sup> translocating ferredoxin oxidation. *Biochim Biophys Acta* 1827:94–113. doi:10.1016/j.bbabi.2012.07.002
- Cappelletti M, Bucchi G, Mendes JDS, Alberini A, Fedi S, Bertin L, Frascari D (2012) Biohydrogen production from glucose, molasses and cheese whey by suspended and attached cells of four hyperthermophilic *Thermotoga* strains. *J Chem Technol Biotechnol* 87:1291–1301
- Chang VS, Nagwani M, Kim CH, Holtzapple MT (2001) Oxidative lime pretreatment of high-lignin biomass. *Appl Biochem Biotechnol* 94:1–28
- Chhabra SR, Shockley KR, Connors SB, Scott KL, Wolfinger RD, Kelly RM (2003) Carbohydrate-induced differential gene expression patterns in the hyperthermophilic bacterium *Thermotoga maritima*. *J Biol Chem* 278:7540–7552
- Cohen J, Kim K, King P, Seibert M, Schulten K (2005) Finding gas diffusion pathways in proteins: application to O<sub>2</sub> and H<sub>2</sub> transport in Cpl [FeFe]-

- hydrogenase and the role of packing defects. *Structure* 13:1321–1329
- Connors SB, Mongodin EF, Johnson MR, Montero CI, Nelson KE, Kelly RM (2006) Microbial biochemistry, physiology, and biotechnology of hyperthermophilic *Thermotoga* species. *FEMS Microbiol Rev* 30:872–905
- Cypionka H (2000) Oxygen respiration by *Desulfovibrio* species. *Annu Rev Microbiol* 54:827–848
- d'Ippolito G, Dipasquale L, Vella FM, Romano I, Gambacorta A, Fontana A (2010) Hydrogen metabolism in the extreme thermophile *Thermotoga neapolitana*. *Int J Hydrog Energy* 35:2290–2295
- Davey ME, Wood WA, Key R, Nakamura K, Stahl D (1993) Isolation of three species of Geotoga and Petrotoga: two new genera, representing a new lineage in the bacterial line of descent distantly related to the 'Thermotogales'. *Syst Appl Microbiol* 16:191–200
- de Vrije T, De Haas GG, Tan GB, Keijsers ERP, Claassen PAM (2002) Pretreatment of *Miscanthus* for hydrogen production by *Thermotoga elfii*. *Int J Hydrog Energy* 27:1381–1390
- de Vrije T, Bakker RR, Budde MAW, Lai MH, Mars AE, Claassen PAM (2009) Efficient hydrogen production from the lignocellulosic energy crop *Miscanthus* by the extreme thermophilic bacteria *Caldicellulosiruptor saccharolyticus* and *Thermotoga neapolitana*. *Biotechnol Biofuels* 2:12
- de Vrije T, Budde MAW, Lips SJ, Bakker RR, Mars AE, Claassen PAM (2010) Hydrogen production from carrot pulp by the extreme thermophiles *Caldicellulosiruptor saccharolyticus* and *Thermotoga neapolitana*. *Int J Hydrog Energy* 35:13206–13213
- Di Pippo JL, Nesbo CL, Dahle H, Doolittle WF, Birkland N-K, Noll KM (2009) *Kosmotoga olearia* gen. nov., sp. nov., a thermophilic, anaerobic heterotroph isolated from an oil production fluid. *Int J Syst Evol Microbiol* 59:2991–3000
- Dipasquale L, d'Ippolito G, Gallo C, Vella FM, Gambacorta A, Picariello G, Fontana A (2012) Hydrogen production by the thermophilic eubacterium *Thermotoga neapolitana* from storage polysaccharides of the CO<sub>2</sub>-fixing diatom *Thalassiosira weissflogii*. *Int J Hydrog Energy* 37:12250–12257
- Dolla A, Fournier M, Dermoun Z (2006) Oxygen defense in sulfate-reducing bacteria. *J Biotechnol* 126:87–100
- Drapcho CM, Nhuan NP, Walker TH (eds) (2008) Hydrogen production by fermentation. In: *Biofuels engineering process technology*. McGraw-Hill, New York, pp 269–299
- Eriksen NT, Nielsen TM, Iversen N (2008) Hydrogen production in anaerobic and microaerobic *Thermotoga neapolitana*. *Biotechnol Lett* 30:103–109
- Eriksen NT, Leegaard Riis M, Kindby Holm N, Iversen N (2011) H<sub>2</sub> synthesis from pentoses and biomass in *Thermotoga* spp. *Biotechnol Lett* 33:293–300
- Fardeau M-L, Olliever B, Patel BKC, Magot M, Thomas P, Rimbault A, Rocchiccioli F, Garcia J-L (1997) *Thermotoga hypogea* sp. nov., a xylanolytic, thermophilic bacterium from an oil-producing well. *Int J Syst Bacteriol* 47:1013–1019
- Feng Y, Cheng L, Zhang X, Li X, Deng Y, Zhang H (2010) *Thermococcoides shengliensis* gen. nov., sp. nov., a new member of the order Thermotogales isolated from oil-production fluid. *Int J Syst Evol Microbiol* 60:932–937
- Fetzer S, Conrad R (1993) Effect of redox potential on methanogenesis by *Methanosarcina barkeri*. *Arch Microbiol* 160:108–113
- Friedrich AB, Antranikian G (1996) Keratin degradation by *Fervidobacterium pennavorans*, a novel thermophilic anaerobic species of the order Thermotogales. *Appl Environ Microbiol* 62:2875–2882
- Frock AD, Gray SR, Kelly RM (2012) Hyperthermophilic *Thermotoga* species differ with respect to specific carbohydrate transporters and glycoside hydrolases. *Appl Environ Microbiol* 78:1978–1986
- Galperin MY, Noll KM, Romano AH (1996) The glucose transport system of the hyperthermophilic anaerobic bacterium *Thermotoga neapolitana*. *Appl Environ Microbiol* 62:2915–2918
- Hawkes F, Dinsdale R, Hawkes D, Hussy I (2002) Sustainable fermentative hydrogen production: challenges for process optimisation. *Int J Hydrog Energy* 27:1339–1347
- Huber R, Hannig M (2006) Thermotogales. In: Dworkin M, Falkow S, Rosenberg E, Schleifer KH, Stackebrandt E (eds) *The prokaryotes*. Springer, New York, pp 899–922
- Huber R, Stetter KO (2001) Discovery of hyperthermophilic microorganisms. In: Adams MWW, Kelly RM (eds) *Methods in enzymology*. Academic, San Diego, pp 11–24
- Huber R, Langworthy TA, König H, Thomm M, Woese CR, Sleytr UB, Stetter KO (1986) *Thermotoga maritima* sp. nov. represents a new genus of unique extremely thermophilic eubacteria growing up to 90°C. *Arch Microbiol* 144:324–333
- Huber R, Woese CR, Langworthy TA, Fricke H, Stetter KO (1989) *Thermosiphon africanus* gen. nov., represents a new genus of thermophilic Eubacteria within the Thermotogales. *Syst Appl Microbiol* 12:32–37
- Huber R, Woese CR, Langworthy TA, Kristjansson JK, Stetter KO (1990) *Fervidobacterium islandicum* sp. nov., a new extremely thermophilic eubacterium belonging to the Thermotogales. *Arch Microbiol* 154:105–111



- Ito T, Nakashimada Y, Senba K, Matsui T, Nishio N (2005) Hydrogen and ethanol production from glycerol-containing wastes discharged after bio-diesel manufacturing process. *J Biosci Bioeng* 100:260–265
- Jannasch HW, Huber R, Belkin S, Stetter KO (1988) *Thermotoga neapolitana* sp. nov. of the extremely thermophilic, eubacterial genus *Thermotoga*. *Arch Microbiol* 150:103–104
- Janssen PH, Morgan HW (1992) Heterotrophic sulfur reduction by *Thermotoga* sp. strain FjSS3.B1. *FEMS Microbiol Lett* 96:213–217
- Jayasinghearachchi HS, Lal B (2011) *Oceanotoga teriensis* gen. nov., sp. nov., a thermophilic bacterium isolated from offshore oil-producing wells. *Int J Syst Evol Microbiol* 61:554–560
- Jeanthon C, Reysenbach AL, L'Haridon S, Gambacorta A, Pace NR, Glenat P, Prieur D (1995) *Thermotoga subterranea* sp. nov., a new thermophilic bacterium isolated from a continental oil reservoir. *Arch Microbiol* 164:91–97
- Jenney FE, Adams MWW (2008) Hydrogenases of the model hyperthermophiles. Incredible anaerobes: from physiology to genomics to fuels. *Ann N Y Acad Sci* 1125:252–266
- Kapdan IK, Kargi F (2006) Bio-hydrogen production from waste materials. *Enzyme Microb Technol* 38:569–582
- Käslin SA, Childers SE, Noll KM (1998) Membrane-associated redox activities in *Thermotoga neapolitana*. *Arch Microbiol* 170:297–303
- Kaushik N, Debabrata D (2004) Improvement of fermentative hydrogen production: various approaches. *Appl Microbiol Biotechnol* 65:520–529
- King MR, Yernool DA, Eveleigh DE, Chassy BM (1998) Thermostable alpha-galactosidase from *Thermotoga neapolitana*: cloning, sequencing and expression. *FEMS Microbiol Lett* 163:37–42
- Kopke M, Held C, Hujer S, Liesegang H, Wiezer A, Wollherr A, Ehrenreich A, Liebl W, Gottschalk G, Durre P (2010) *Clostridium ljungdahlii* represents a microbial production platform based on syngas. *Proc Natl Acad Sci U S A* 107:13087–13092
- Krekeler D, Teske A, Cypionka H (1998) Strategies of sulfate-reducing bacteria to escape oxygen stress in a cyanobacterial mat. *FEMS Microbiol Ecol* 25:89–96
- L'Haridon S, Miroshnichenko M, Hippe H, Fardeau M-L, Bonch-Osmolovskaya EA, Stackebrandt E, Jeanthon C (2001) *Thermosiphon geolei* sp. nov., a thermophilic bacterium isolated from a continental petroleum reservoir in Western Siberia. *Int J Syst Evol Microbiol* 51:1327–1334
- L'Haridon S, Miroshnichenko ML, Hippe H, Fardeau ML, Bonch-Osmolovskaya EA, Stackebrandt E, Jeanthon C (2002) *Petrotoga olearia* sp. nov. and *Petrotoga sibirica* sp. nov., two thermophilic bacteria isolated from a continental petroleum reservoir in Western Siberia. *Int J Syst Evol Microbiol* 52:1715–1722
- Lakhal R, Auria R, Davidson S, Ollivier B, Dolla A, Hamdi M, Combet-Blanc Y (2010) Effect of oxygen and redox potential on glucose fermentation in thermotoga maritima under controlled physico-chemical conditions. *Int J Microbiol* 2010:896510. doi:10.1155/2010/896510
- Lakhal R, Auria R, Davidson S, Ollivier B, Durand M-C, Dolla A, Hamdi M, Combet-Blanc Y (2011) Oxygen uptake rates in the hyperthermophilic anaerobe *Thermotoga maritima* grown in a bioreactor under controlled oxygen exposure: clues to its defence strategy against oxidative stress. *Arch Microbiol* 193:429–438
- Lay JJ (2000) Modeling and optimization of anaerobic digested sludge converting starch to hydrogen. *Biotechnol Bioeng* 68:269–278
- Le Fourn C, Fardeau M-L, Ollivier B, Lojou E, Dolla A (2008) The hyperthermophilic anaerobe *Thermotoga maritima* is able to cope with limited amount of oxygen: insights into its defence strategies. *Environ Microbiol* 10:1877–1887
- Le Fourn C, Brasseur G, Brochier-Armanet C, Pieuille L, Brioukhanov A, Ollivier B, Dolla A (2011) An oxygen reduction chain in the hyperthermophilic anaerobe *Thermotoga maritima* highlights horizontal gene transfer between Thermococcales and Thermotogales. *Environ Microbiol* 13:2132–2145
- Levin DB, Pitt L, Love M (2004) Biohydrogen production: prospects and limitations to practical application. *Int J Hydrog Energy* 29:173–185
- Liang TM, Cheng SS, Wu KL (2002) Behavioral study on hydrogen fermentation reactor installed with silicone rubber membrane. *Int J Hydrog Energy* 27:1157–1165
- Lien T, Madsen M, Rainey FA, Birkeland N-K (1998) *Petrotoga mobilis* sp. nov., from a North Sea oil-production well. *Int J Syst Bacteriol* 48:1007–1013
- Magot M, Ollivier B, Patel BK (2000) Microbiology of petroleum reservoirs. *Antonie Van Leeuwenhoek* 77:103–116
- McCarthy JK, Uzelac A, Davis DF, Eveleigh DE (2004) Improved catalytic efficiency and active site modification of 1,4-beta-D-glucan glucohydrolase A from *Thermotoga neapolitana* by directed evolution. *J Biol Chem* 279:11495–11502
- Miranda-Tello E, Fardeau M-L, Thomas P, Ramirez F, Casalot L, Cayol J-L, Garcia J-L, Ollivier B (2004) *Petrotoga mexicana* sp. nov., a novel thermophilic, anaerobic and xylanolytic bacterium isolated from an oil-producing well in the Gulf of Mexico. *Int J Syst Evol Microbiol* 54:169–174

- Miranda-Tello E, Fardeau M-L, Joulian C, Magot M, Thomas P, Tholozan JL, Ollivier B (2007) *Petrotoga halophila* sp. nov., a thermophilic, moderately halophilic, fermentative bacterium isolated from an offshore oil well in Congo. *Int J Syst Evol Microbiol* 57:40–44
- Munro SA, Zinder SH, Walker LP (2009) The fermentation stoichiometry of *Thermotoga neapolitana* and influence of temperature, oxygen, and pH on hydrogen production. *Biotechnol Prog* 25:1035–1042
- Nesbø CL, Dlutek M, Zhaxybayeva O, Doolittle WF (2006) Evidence for existence of “Mesotogas,” members of the order Thermotogales adapted to low-temperature environments. *Appl Environ Microbiol* 72:5061–5068
- Nesbø CL, Kumaraswamy R, Dlutek M, Doolittle WF, Foght J (2010) Searching for mesophilic Thermotogales bacteria: “Mesotogas” in the wild. *Appl Environ Microbiol* 76:4896–4900
- Nesbø C, Bradnan D, Adebayomi A, Dlutek M, Petrus A, Foght J, Doolittle W, Noll K (2012) *Mesotoga prima* gen. nov., sp. nov., the first described mesophilic species of the Thermotogales. *Extremophiles* 16:387–393
- Ngo TA, Sim SJ (2011) Dark fermentation of hydrogen from waste glycerol using hyperthermophilic eubacterium *Thermotoga neapolitana*. *Environ Prog Sustain Energy* 31:466–473
- Ngo TA, Kim MS, Sim SJ (2011a) High-yield biohydrogen production from biodiesel manufacturing waste by *Thermotoga neapolitana*. *Int J Hydrog Energy* 36:5836–5842
- Ngo TA, Kim MS, Sim SJ (2011b) Thermophilic hydrogen fermentation using *Thermotoga neapolitana* DSM 4359 by fed-batch culture. *Int J Hydrog Energy* 36:14014–14023
- Ngo TA, Nguyen TH, Bui HTV (2012) Thermophilic fermentative hydrogen production from xylose by *Thermotoga neapolitana* DSM 4359. *Renew Energy* 37:174–179
- Nguyen TN, Borges KM, Romano AH, Noll KM (2001) Differential gene expression in *Thermotoga neapolitana* in response to growth substrate. *FEMS Microbiol Lett* 195:79–83
- Nguyen TN, Ejaz AD, Brancieri MA, Mikula AM, Nelson KE, Gill SR, Noll KM (2004) Whole-genome expression profiling of *Thermotoga maritima* in response to growth on sugars in a chemostat. *J Bacteriol* 186:4824–4828
- Nguyen TAD, Kim JP, Kim MS, Oh YK, Sima SJ (2008a) Optimization of hydrogen production by hyperthermophilic eubacteria, *Thermotoga maritima* and *Thermotoga neapolitana* in batch fermentation. *Int J Hydrog Energy* 33:1483–1488
- Nguyen TAD, Kim JP, Kim MS, Oh YK, Sim SJ (2008b) Hydrogen production by the hyperthermophilic eubacterium, *Thermotoga neapolitana*, using cellulose pretreated by ionic liquid. *Int J Hydrog Energy* 33:5161–5168
- Nguyen TAD, Han SJ, Kim JP, Kim MS, Sim SJ (2010a) Hydrogen production of the hyperthermophilic eubacterium, *Thermotoga neapolitana* under N<sub>2</sub> sparging condition. *Bioresour Technol* 101:S38–S41
- Nguyen TAD, Kim KR, Kim MS, Sim SJ (2010b) Thermophilic hydrogen fermentation from Korean rice straw by *Thermotoga neapolitana*. *Int J Hydrog Energy* 35:13392–13398
- Nguyen TAD, Kim KR, Nguyen MT, Kim MS, Kim D, Sim SJ (2010c) Enhancement of fermentative hydrogen production from green algal biomass of *Thermotoga neapolitana* by various pretreatment methods. *Int J Hydrog Energy* 35:13035–13040
- Ntaikou I, Antonopoulou G, Lyberatos G (2010) Biohydrogen production from biomass and wastes via dark fermentation: a review. *Waste Biomass Valor* 1:21–39
- Nunoura T, Oida H, Miyazaki M, Suzuki Y, Takai K, Horikoshi K (2007) *Marinitoga okinawensis* sp. nov., a novel thermophilic and anaerobic heterotroph isolated from a deep-sea hydrothermal field, Southern Okinawa Trough. *Int J Syst Evol Microbiol* 57:467–471
- Nunoura T, Hirai M, Imachi H, Miyazaki M, Makita H, Hirayama H, Furushima Y, Yamamoto H, Takai K (2010) *Kosmotoga arenicorallina* sp. nov. a thermophilic and obligately anaerobic heterotroph isolated from a shallow hydrothermal system occurring within a coral reef, southern part of the Yaeyama Archipelago, Japan, reclassification of *Thermococcoides shengliensis* as *Kosmotoga shengliensis* comb. nov., and emended description of the genus *Kosmotoga*. *Arch Microbiol* 192:811–819
- Ollivier B, Cayol J-L (2005) The fermentative, iron-reducing, and nitrate-reducing microorganisms. In: Ollivier B, Magot M (eds) *Petroleum microbiology*. ASM Press, Washington, DC, pp 71–88
- Patel BKC, Morgan HW, Daniel RM (1985) *Fervidobacterium nodosum*; gen. nov. and spec. nov., a new chemoorganotrophic, caldoactive, anaerobic bacterium. *Arch Microbiol* 141:63–69
- Pierce E, Xie G, Barabote RD, Saunders E, Han CS, Detter JC, Richardson P, Brettin TS, Das A, Ljungdahl LG, Ragsdale SW (2008) The complete genome sequence of *Moorella thermoacetica* (f. *Clostridium thermoaceticum*). *Environ Microbiol* 10:2550–2573
- Poehlein A, Schmidt S, Kaster AK, Goenrich M, Vollmers J, Thurmer A, Bertsch J, Schuchmann K, Voigt B, Hecker M, Daniel R, Thauer RK, Gottschalk G, Muller V (2012) An ancient pathway combining carbon dioxide fixation with the generation and utilization of a

- sodium ion gradient for ATP synthesis. PLoS One 7:e33439. doi:10.1371/journal.pone.0033439
- Postec A, Le Breton C, Fardeau M-L, Lesongeur F, Pignet P, Querellou J, Ollivier B, Godfroy A (2005) *Marinitoga hydrogenitolerans* sp. nov., a novel member of the order Thermotogales isolated from a black smoker chimney on the Mid-Atlantic Ridge. Int J Syst Evol Microbiol 55:1217–1221
- Postec A, Ciobanu MC, Birrien J-L, Biennu N, Prieur D, Le Romancer M (2010) *Marinitoga litoralis* sp. nov., a thermophilic, heterotrophic bacterium isolated from a coastal thermal spring on Ile Saint-Paul, Southern Indian Ocean. Int J Syst Evol Microbiol 60:1778–1782
- Ravot G, Ollivier B, Magot M, Patel B, Crolet J, Fardeau M-L, Garcia J (1995) Thiosulfate reduction, an important physiological feature shared by members of the order Thermotogales. Appl Environ Microbiol 61:2053–2055
- Ravot G, Ollivier B, Fardeau M-L, Patel BKC, Andrews KT, Magot M, Garcia JL (1996) L-alanine production from glucose fermentation by hyperthermophilic members of the domains Bacteria and Archaea: a remnant of an ancestral metabolism? Appl Environ Microbiol 62:2657–2659
- Reysenbach A-L, Boone DR, Castenholz RW, Garrity GM (2001) Phylum BII. Thermotogae phy. nov. In: Boone DR, Castenholz RW (eds) Bergey's manual of systematic bacteriology. Springer, New York, pp 369–387
- Schink B, Stams A (2006) Syntrophism among prokaryotes. In: Schleifer K-H, Stackebrandt E (eds) The prokaryotes. Springer, New York, pp 322–337
- Schröder C, Selig M, Schönheit P (1994) Glucose fermentation to acetate, CO<sub>2</sub> and H<sub>2</sub> in the anaerobic hyperthermophilic eubacterium *Thermotoga maritima*: involvement of the Embden-Meyerhof pathway. Arch Microbiol 161:460–470
- Schut GJ, Adams MW (2009) The iron-hydrogenase of *Thermotoga maritima* utilizes ferredoxin and NADH synergistically: a new perspective on anaerobic hydrogen production. J Bacteriol 191:4451–4457
- Selig M, Xavier KB, Santos H, Schönheit P (1997) Comparative analysis of Embden-Meyerhof and Entner-Doudoroff glycolytic pathways in hyperthermophilic archaea and the bacterium *Thermotoga*. Arch Microbiol 167:217–232
- Soboh B, Linder D, Hedderich R (2004) A multisubunit membrane-bound [NiFe] hydrogenase and an NADH-dependent Fe-only hydrogenase in the fermenting bacterium *Thermoanaerobacter tengcongensis*. Microbiology 150:2451–2463
- Takahata Y, Nishijima M, Hoaki T, Maruyama T (2001) *Thermotoga petrophila* sp. nov. and *Thermotoga naphthophila* sp. nov., two hyperthermophilic bacteria from the Kubiki oil reservoir in Niigata, Japan. Int J Syst Evol Microbiol 51:1901–1909
- Takai K, Horikoshi K (2000) *Thermosipho japonicus* sp. nov., an extremely thermophilic bacterium isolated from a deep-sea hydrothermal vent in Japan. Extremophiles 4:9–17
- Teske A, Ramsing NB, Habicht K, Fukui M, Kuver J, Jorgensen BB, Cohen Y (1998) Sulfate-reducing bacteria and their activities in cyanobacterial mats of solar Lake (Sinai, Egypt). Appl Environ Microbiol 64:2943–2951
- Thauer RK, Jungermann K, Decker K (1977) Energy conservation in chemotrophic anaerobic bacteria. Microbiol Mol Biol Rev 41:100–180
- Thauer RK, Kaster AK, Goenrich M, Schick M, Hiromoto T, Shima S (2010) Hydrogenases from methanogenic archaea, nickel, a novel cofactor, and H<sub>2</sub> storage. Annu Rev Biochem 79:507–536
- Tosatto SCE, Toppo S, Carbonera D, Giacometti GM, Costantini P (2008) Comparative analysis of the [FeFe] hydrogenase from Thermotogales indicates the molecular bases of resistance to oxygen inactivation. Int J Hydrog Energy 33:570–578
- Urios L, Cuffe-Gauchard V, Pignet P, Postec A, Fardeau M-L, Ollivier B, Barbier G (2004) *Thermosipho atlanticus* sp. nov., a novel member of the Thermotogales isolated from a Mid-Atlantic Ridge hydrothermal vent. Int J Syst Evol Microbiol 54:1953–1957
- Van Niel EWJ, Budde MAW, de Haas GG, van der Wal FJ, Claassen PAM, Stams AJM (2002) Distinctive properties of high hydrogen producing extreme thermophiles, *Caldicellulosiruptor saccharolyticus* and *Thermotoga elfii*. Int J Hydrog Energy 27:1391–1398
- Van Ooteghem SA, Beer SK, Yue PC (2002) Hydrogen production by the thermophilic bacterium *Thermotoga neapolitana*. Appl Biochem Biotechnol 98–100:177–189
- Van Ooteghem SA, Jones A, van der Lelie D, Dong B, Mahajan D (2004) H<sub>2</sub> production and carbon utilization by *Thermotoga neapolitana* under anaerobic and microaerobic growth conditions. Biotechnol Lett 26:1223–1232
- Vanfossen AL, Lewis DL, Nichols JD, Kelly RM (2008) Polysaccharide degradation and synthesis by extremely thermophilic anaerobes. Ann N Y Acad Sci 1125:322–337
- Vargas M, Noll KM (1996) Catabolite repression in the hyperthermophilic bacterium *Thermotoga neapolitana* is independent of cAMP. Microbiology 142:139–144
- Vargas M, Kashefi K, Blunt-Harris EL, Lovley DR (1998) Microbiological evidence for Fe(III) reduction on early Earth. Nature 395:65–67

- Verhagen MF, O'Rourke T, Adams MW (1999) The hyperthermophilic bacterium *Thermotoga maritima* contains an unusually complex iron-hydrogenase: amino acid sequence analyses versus biochemical characterization. *Biochim Biophys Acta* 1412:212–229
- Vincent KA, Parkin A, Lenz O, Albracht SPJ, Fontecilla-Camps JC, Cammack R, Friedrich B, Armstrong FA (2005) Electrochemical definitions of O<sub>2</sub> sensitivity and oxidative inactivation in hydrogenases. *J Am Chem Soc* 127:18179–18189
- Wery N, Lesongeur F, Pignet P, Derennes V, Cambon-Bonavita M, Godfroy A, Barbier G (2001) *Marinitoga camini* gen. nov., sp. nov., a rod-shaped bacterium belonging to the order Thermotogales, isolated from a deep-sea hydrothermal vent. *Int J Syst Evol Microbiol* 51:495–504
- Wiegel J, Ljungdahl LG, Demain AL (1985) The importance of thermophilic bacteria in biotechnology. *Crit Rev Biotechnol* 3:39–108
- Windberger E, Huber R, Trincone A, Fricke H, Stetter KO (1989) *Thermotoga thermarum* sp. nov. and *Thermotoga neapolitana* occurring in African continental solfataric springs. *Arch Microbiol* 151:506–512
- Woodward J, Heyer NI, Getty JP, O'Neill HM, Pinkhassik E, Evans BR (2002) Efficient hydrogen production using enzymes of the pentose phosphate pathway. NREL/CP-610–32405. US Department of Energy, Washington, DC
- Yang X, Ma K (2005) Purification and characterization of an NADH oxidase from extremely thermophilic anaerobic bacterium *Thermotoga hypogea*. *Arch Microbiol* 183:331–337
- Zhaxybayeva O, Swithers KS, Lapierre P, Fournier GP, Bickhart DM, DeBoy RT, Nelson KE, Nesbø CL, Doolittle WF, Gogarten JP, Noll KM (2009) On the chimeric nature, thermophilic origin, and phylogenetic placement of the Thermotogales. *Proc Natl Acad Sci U S A* 106:5865–5870
- Zverlov VV, Volkov IY, Velikodvorskaya TV, Schwarz WH (1997) Highly thermostable endo-1,3-β-glucanase (chrysolaminaranase) LamA from *Thermotoga neapolitana*: nucleotide sequence of the gene and characterization of the recombinant gene product. *Microbiology* 143:1701–1708