Chapter 58 Synthesis of Poly (β-L-malic Acid) by the Optimization of Inorganic Nitrogen Complexing with Growth Factors Using *Aureobasidium pullulans* CGMCC3337

Changsheng Qiao, Yumin Song, Zhida Zheng, Xujia Fan and Shiyun Yu

Abstract Poly (β -L-malic acid) (PMLA) can be used as a prodrug or used for drug delivery system, and it has attracted industrial interest. In previous studies, we could obtain 38 g/L PMLA with 10 g/L yeast extract as a nitrogen source, but the complex broth component made it difficult to the downstream process. To decrease the pressure in the extraction process, we used inorganic nitrogen resources and growth factors to replace yeast extract. Response surface methodology (RSM) was applied to optimize the fermentation medium formulation to improve the production of poly (β -L-malic acid) (PMLA) with *Aureobasidium pullulans CGMCC3337*. It was confirmed that ammonium nitrate 2.06 g/L, adenine 0.02 g/L, cytosine 0.012 g/L aspartate (Asp) 0.42 g/L, histidine(His) 0.6 g/L, leucine(Leu) 0.4 g/L, and threonine(Thr) 0.28 g/L could replace the yeast extract in PMLA production. The model developed based on RSM successfully predicted PMLA productivity ($R^2 = 0.9697$). With the optimum medium established, 37.62 g/L PMLA was accumulated in the fermentation broth, and the impurities in the fermentation broth was reduced apparently.

Keywords *Aureobasidium pullulans* • Poly (β-malic acid) • Inorganic nitrogen • Growth factors • Response surface methodology (RSM)

58.1 Introduction

PMLA is a well-known biodegradable, bioabsorbable, and water-soluble polymer having pendant carboxylic groups, which allow further conjugation of functional groups or molecules, including drugs via chemical modification. These advantages

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make it important to investigate high purity and high-yield production of PMLA. For example, it is reported that a PMLA-based drug delivery system and biodegradable nanoparticles could be used for tumor targeting [1, 2]. So PMLA can be used as a prodrug or for drug delivery systems, which has attracted a great deal of interest in industries [3–5]. PMLA can be obtained by chemical synthesis or microbial fermentation. Recently, biosynthesis has been extensively investigated. Leathers [6] did significant work on PMLA production by strains of *Aureobasidium pullulans*. 9–11 g/L PMLA could be gained by adding yeast extract and peptone to the medium. Under optimized conditions, using sodium nitrate as the nitrogen source, 9.8 g/L PMLA was produced after nine days of fermentation in the stirredtank reactors with an overall yield of 0.11 g PMLA/g glucose [7]. In preliminary studies, we had successfully accumulated 38.9 g/L β -PMLA with the addition of 10 g/L yeast extract, which was bad for the downstream process of β -PMLA production. The application of PMLA was vastly restricted in medicine and other industries.

Therefore, the objective of the present investigations is to optimize the cultural medium formulation with the addition of inorganic nitrogen source and amino acids, to acquire the highest possible production of PMLA, to reduce impurities in the fermentation broth, to easily investigate the metabolic flux analysis and metabonomics analysis, and to provide a kind of cheap medium components for PMLA production by the strain *A. pullulans* CGMCC3337.

58.2 Materials and Methods

58.2.1 Microorganism

Aureobasidium pullulans CGMCC3337 was isolated in the Key Laboratory of Industrial Microbiology, Ministry of Education, Tianjin University of Science and Technology, and stored in China General Microbiological Culture Collection Center.

58.2.2 Medium and Culture Method

The compositions of the inoculum medium were as follows (g/L): glucose 80.28, yeast extract 3, $(NH_4)_2SO_4$ 3.06, succinic acid 2, K_2CO_3 0.4, KH_2PO_4 0.1, CaCO_3 27.7, ZnSO_4·7H_2O 5 × 10⁻³, MgSO_4·7H_2O 0.1. The medium was autoclaved for 20 min at 121 °C after the pH of the medium was adjusted to 4.5.

For the inoculums preparation, cells cultivated on potato-glucose agar inoculated to 50 ml seed medium in 500 ml baffle flasks and incubated at 25 °C, 200 rpm for 2 days on a rotary shaker. Fermentation was carried out in 500 ml baffled flasks, and

each flask contains 50 ml sterile fermentation medium, which was inoculated with 5 ml of the prepared inoculum. Then the flasks were incubated for 7 days on a rotary incubator at 25 °C, 200 rpm.

58.2.3 Preliminary Experiments

We had developed a semisynthetic medium using yeast extract as the nitrogen source. To replace the yeast extract, we study the effect of nitrogen on PMLA production. Various inorganic salts were tested individually. Fifteen amino acids and a number of growth factors as trace elements were also evaluated for their suitability for the PMLA production. Carbon source and metal irons were kept at the initial levels. Since optimizing amino acids and growth factors involved in many parameters, only one parameter varied in the optimization process.

58.2.4 Experimental Design

Plackett–Burman design (PBD) was used to identify those variables that significantly influenced PMLA production. Then, experiments were performed along the steepest ascent path until the response showed no further increase. Based on the results of our preliminary experiments, the major factors were optimized by response surface methodology (RSM) design (Design-Expert 6).

58.2.5 Determination of Poly Malic Acid Yield

The PMLA content was determined by an HPLC method on a column of Prevail C^{18} after the PMLA was hydrolyzed to L-malic and was expressed as g/L [8].

58.3 Results and Discussion

58.3.1 Effects of Inorganic Nitrogen Sources to the Synthesis of PMLA

In order to replace yeast extract, inorganic nitrogen sources (NH₄Cl, NaNO₃, NH₄NO₃, Urea, NH₄HSO₄, (NH₄)₂CO₃, and (NH₄)₂SO₄) were individually evaluated for their performances in PMLA production by the strain *A. pullulans* CGMCC3337 (Table 58.1). To provide the optimal C/N, the addition of inorganic nitrogen source was consistent with nitrogen content in the yeast extract.

Table 58.1 Effect of inorg.	anic nitrogen	sources on PN	ALA production					
Nitrogen source (g/L)	NH4CI	NaNO ₃	$\rm NH_4 NO_3$	Urea	NH4HSO ₄	$(NH_4)_2CO_3$	$(NH_4)_2SO_4$	Yeast extract
Concentration	2.75	4.37	2.06	1.54	5.92	2.67	3.38	5.92
Biomass	10.3	0.28	19.86	16.29	0.24	10.87	0.31	38.80
PMLA	4.5	0.18	17.92	5.63	0.43	2.37	0.57	20.67

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Among the various inorganic nitrogen sources tested, NH_4NO_3 exhibited a prominent effect on the production ability of 19.86 g/L and maximum biomass is 17.92 g/L, followed by urea 16.29 g/L, 5.63 g/L, NH_4Cl 10.3 g/L, 4.5 g/L, $(NH_4)_2CO_3$ 10.87 g/L, 2.3 g/L, respectively. NH_4HSO_4 , $(NH_4)_2SO_4$, and $NaNO_3$ exhibited no effect on the growth ability (data not shown). The yield and biomass of inorganic nitrogen were obviously lower than those of yeast extract. This might be a result of growth factors existence in yeast extract. Therefore, the effects of growth factors on synthesis of PMLA were investigated subsequently.

58.3.2 Effects of Growth Factors on PMLA Production

In the investigation process, adding relevant growth factors according to the content in the yeast extract, while the other nutrient contents were as follows: sugar 65, KH_2PO_4 0.15, $MgSO_4 \cdot 7H_2O$ 0.4, $CaCO_3$ 12 g/L. The concentration of PMLA increased 18.98, 7.22, 11.61, and 11.01 % compared to the original value of 19.8 g/L, with the addition of Asp (0.28), His (0.4), Leu (0.6), and Thr (0.38 g/L), as shown in Fig. 58.1a. When the fermentation medium added Ala, Glu, Ile, Met, Phe, and Ser, it had little effect on PMLA production. However, negative effects on PMLA production had been observed with Arg, Gly, Lys, Tyr, and Val. The effects of purines (Adenine, Guanine) and pyrimidines (Cytosine, Thymine) were investigated for the synthesis of PMLA. The results were shown in Fig. 58.1b. When various vitamins were added to the basic medium, the production of PMLA had no difference (data not shown). The addition of trace of growth factors almost had no effects on the



Fig. 58.1 Effects of growth factors on PMLA (g/L) production. **a** 15 kinds of amino acids (g/L); **b** purines (Adenine, Guanine) and pyrimidines (Cytosine, Thymine) (g/L)

vels for	No.	Variables	Coefficient	F-value	P-value
tt-Burman experiment	X_1	sugar	-0.9	3.48	0.0993
	X_2	KH ₂ PO ₄	0.68	1.99	0.1961
	X_3	MgSO ₄ ·7H ₂ O	-1.25	6.66	0.0326*
	X_4	NH ₄ NO ₃	-0.97	4.03	0.0796
	X_5	CaCO ₃	0.86	3.18	0.1124
	X_6	Adenine	-1.9	15.46	0.0043*
	<i>X</i> ₇	Cytosine	-0.3	0.39	0.5503
	X_8	Asp	2.35	23.69	0.0012*
	X_9	His	0.46	0.91	0.3686
	<i>X</i> ₁₀	Leu	-0.63	1.7	0.2289
	X ₁₁	Thr	-1.01	4.36	0.0703

Table 58.2 Variables and test lev Placke

* Statistically significant at 95 % of probability level

biomass, respectively (data not shown). Finally, adding all the valuable factors to medium, we gained 29.8 g/L PMLA and 18.98 g/L biomass. All the results we investigated are helpful to the biomass accumulation. In order to further improve the production, RSM was used to optimize the addition of components in the medium (Table 58.2).

58.3.3 Screening of Significant Nutrients Using PBD

Twenty independent experiments were conducted according to the experimental design shown in Table 58.3. On the basis of the calculated coefficients, F-values and P-values (Table 58.2) X_3 , X_6 , X_8 were found to be the most significant variables affecting PMLA and chosen for further optimization in the next path of steepest ascent and BBD.

58.3.4 Method of Steepest Ascent

The method of steepest ascent was based on the zero level of the PBD and moved sequentially along the direction in which X_3 , X_6 decreased and X_8 increased. The experimental design and results were shown in Table 58.4. The highest response was 34.76 with X₃ 15, X₆ 1.2, X₈ 0.42 g/L.

Run	<i>X</i> ₁	X ₂	<i>X</i> ₃	<i>X</i> ₄	<i>X</i> ₅	<i>X</i> ₆	X ₇	X ₈	X9	X ₁₀	<i>X</i> ₁₁	PMLA (g/L)
1	80	0.2	0.3	2.02	14	0.03	0.01	0.42	0.36	0.62	0.24	29.51
2	50	0.2	0.5	2.02	10	0.03	0.01	0.42	0.44	0.58	0.32	27.91
3	80	0.1	0.5	2.1	10	0.02	0.01	0.42	0.44	0.62	0.24	26.8
4	80	0.2	0.3	2.1	14	0.02	0.01	0.42	0.44	0.62	0.32	32.57
5	50	0.2	0.5	2.02	14	0.03	0.01	0.34	0.44	0.62	0.32	25.01
6	50	0.1	0.5	2.1	10	0.03	0.01	0.34	0.36	0.62	0.32	18.72
7	50	0.1	0.3	2.1	14	0.02	0.01	0.42	0.36	0.58	0.32	31.79
8	50	0.1	0.3	2.02	14	0.03	0.01	0.42	0.44	0.58	0.24	32.6
9	80	0.1	0.3	2.02	10	0.03	0.01	0.34	0.44	0.62	0.24	22.26
0	50	0.2	0.3	2.02	10	0.02	0.01	0.42	0.36	0.62	0.32	31.01
11	80	0.1	0.5	2.02	10	0.02	0.01	0.42	0.44	0.58	0.32	28.48
12	50	0.2	0.3	2.1	10	0.02	0.01	0.34	0.44	0.62	0.24	29.79
13	80	0.1	0.5	2.02	14	0.02	0.01	0.34	0.36	0.62	0.32	22.35
14	80	0.2	0.3	2.1	10	0.03	0.01	0.34	0.36	0.58	0.32	18.53
15	80	0.2	0.5	2.02	14	0.02	0.01	0.34	0.36	0.58	0.24	29.81
16	80	0.2	0.5	2.1	10	0.03	0.01	0.42	0.36	0.58	0.24	27.14
17	50	0.2	0.5	2.1	14	0.02	0.01	0.34	0.44	0.58	0.24	25.63
18	50	0.1	0.5	2.1	14	0.03	0.01	0.42	0.36	0.62	0.24	25.79
19	80	0.1	0.3	2.1	14	0.03	0.01	0.34	0.44	0.58	0.32	23.65
20	50	0.1	0.3	2.02	10	0.02	0.01	0.34	0.36	0.58	0.24	30.85

Table 58.3 Plackett-Burman design of variables (in coded levels) with PMLA yield as response

Table 58.4 Experimental design of steepest ascent and corresponding response

Step change value	MgSO ₄ ·7H ₂ O (g/L)	Adenine (g/L)	Asp (g/L)	PMLA (g/L)
0	0.4	0.025	0.38	29.76
$0 + 1\Delta$	0.35	0.023	0.4	32.08
$0 + 2\Delta$	0.3	0.021	0.42	34.76
$0 + 3\Delta$	0.25	0.019	0.44	28.48
$0 + 4\Delta$	0.2	0.017	0.46	30.59
$0 + 5\Delta$	0.15	0.015	0.48	31.57

58.3.5 Further Optimization of the Nutrients Using BBD

The design matrix of tested variables and the experimental results were represented in Table 58.5. The statistical analysis results were shown in Table 58.5, and the regression model was given as:

$$Y = 37.61 + 0.52X_3 + 0.034X_6 + 0.26X_8 - 0.33X_3X_6 + 0.87X_3X_8 + 1.51X_6X_8 - 1.87X_3^2 - 2.82X_6^2 - 3.48X_8^2$$

Run	Coded	level		PMLA(g/L)		
	X ₃	<i>X</i> ₆	<i>X</i> ₈	Experimental value	Predicted value	
1	0.25	0.019	0.42	31.69	32.04	
2	0.35	0.019	0.42	34	33.74	
3	0.25	0.023	0.42	32.5	32.76	
4	0.35	0.023	0.42	33.5	33.15	
5	0.25	0.02	0.4	33.18	32.35	
6	0.35	0.02	0.4	31.87	31.65	
7	0.25	0.02	0.44	30.92	31.14	
8	0.35	0.02	0.44	33.09	33.92	
9	0.3	0.019	0.4	32.05	32.53	
10	0.3	0.023	0.4	29.01	29.58	
11	0.3	0.019	0.44	30.6	30.03	
12	0.3	0.023	0.44	33.6	33.12	
13	0.3	0.02	0.42	37.03	37.61	
14	0.3	0.02	0.42	37.98	37.61	
15	0.3	0.02	0.42	37.94	37.61	
16	0.3	0.02	0.42	37.12	37.61	
17	0.3	0.02	0.42	37.98	37.61	

Table 58.5 BBD matrix for optimization of PMLA

where Y is the predicted β -PMLA yield, X_3 is MgSO₄·7H₂O, X_6 is Adenine, and X_8 is initial Asp. The quadratic regression model was evaluated by ANOVA. As shown in Table 58.6, the model F-value was 24.89, and the value of "Prob > F" was 0.0002, suggesting that the model was highly significant. The "Lack of Fit F-value" of 4.10 implied the lack of fit that was not significant relative to the pure error. There was a 10.32 % chance that a "Lack of Fit F-value" of this large could occur due to the noise. The model was found to be adequate for prediction within the range of variables employed. The determination of coefficient (R^2) was 0.9697.

Table 58.6 Analysis of variance (ANOVA) for the experiment results of the	e BBD
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Source	Sum of squares	Degrees of freedom	Mean square	F-value	P-value
Model	125.08	9	13.9	24.89	0.0002*
Residual	3.91	7	0.56		
Lack of fit	2.95	3	0.98	4.1	0.1032
Pure error	0.96	4	0.24		
Cor total	128.99	16			

 $R^2 = 0.9697, R^2_{Adj} = 0.9308$ * Statistically significant at 95 % of probability level



Fig. 58.2 Three-dimensional response surface plots for PMLA (g/L) production by *A. pullulans* CGMCC3337 showing variable interactions of: **a** MgSO4·7H2O (g/L) and Adenine (g/L); **b** MgSO4·7H2O (g/L) and Asp (g/L); **c** Adenine (g/L) and Asp (g/L)

The high R^2 values in this study indicated that the model equation could adequately predict the responses. The values of the adjusted determination coefficients (adjusted R^2) 0.9308 also indicated high significance for the model.

Three-dimensional response surface Fig. 58.2a, b, c represented regression equations to depict the relationships among the variables and to confirm these results. PMLA fermentation by *A. pullulans* was carried out under the optimum medium, which was improved by the RSM optimization approach. The mean value of the PMLA yield was 37.62 ± 0.21 g/L in triplicate tests, which was in agreement with the predicted value. The value also was closed to that of yeast extract (38 g/L). Yeast extract could be replaced by the complex of NH₄NO₃ complexing with growth factors to produce PMLA.

58.4 Conclusion

The present studies demonstrated that a synthetic fermentation medium would be optimized with poly (β -L-malic acid) fermentation. When the yeast extract was totally replaced by inorganic ammonium nitrate, the PMLA production was significantly increase with the addition of adenine (0.02 g/L), cytosine (0.012), Asp (0.42), His (0.6), Leu (0.4) and Thr (0.28 g/L) by response surface methodology. Finally, 37.62 ± 0.21 g/L PMLA was gained, which was closed to the value of yeast extract (10 g/L) addition. In this way, the impurities in fermentation broth were reduced apparently and the difficulty in the downstream process of PMLA production was reduced significantly. Meanwhile, PMLA produced under the condition ultimately reduced the cost of medium components. And the unclear flux of metabolic of PMLA would be much easier to be investigated in the further studies.

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