Chapter 3 Olefin Polymerization with Non-metallocene Catalysts (Early Transition Metals)

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Abstract In this chapter, recent developments of so called non-metallocene early transition metal (group 3–5) complexes as the catalyst precursors for olefin polymerization have been described. These catalysts display unique characterisitics especially for ethylene (co)polymerization, and high isospecificity ([*mmmm*] > 99.6 %) in propylene polymerization has been achieved in some catalyses. The ligand modification plays an essential key role not only for the catalytic activity, but also for control of tacticity and/or living nature in these catalyses.

3.1 Introduction

After a discovery of so called metallocene catalysts $[Cp_2ZrCl_2$ —methylaluminoxane (MAO) catalyst] by Kaminsky et al. [1, 2], many researchers focused on design and synthesis of bridged (*ansa*) metallocene (see Reviews for metallocenes [3–6]; *Frontiers in Metal-Catalysed Polymerization* (special issue) [7–10]) and half-titanocene complex (exemplified as constrained geometry catalyst, CGC) (see Reviews for linked half-titanocenes [11–13]) for efficient ethylene/ α -olefin copolymerization and isospecific polymerization of α -olefins. Nonbridged (unbridged) half-titanocene catalysts (see Reviews for nonbridged half-titanocenes [14–17]), described in Chap. 2, may also be considered as the related stream, although the basic concept in the catalyst design is somewhat different. In olefin polymerization using metallocene catalysts, it has been postulated that the cationic alkyl species, Cp_2Zr^+R , play an essential key role as the active species [3–6]. Therefore,

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researchers only focused on generating 14e species from the catalyst precursor. Later it has been well known exemplified as $[Me_2Si(C_5Me_4)(N'Bu)]TiCl_2$ (CGC) that 12e species also plays a role, suggesting many promising possibilities for designing efficient catalysts with various ligand. After a report concerning 1-hexene polymerization using a titanium complex containing bis(amide) ligand as the catalyst precursor by Dr. McConville [18, 19], described below, many researchers from both academic and industry invloved in the project for exploring a possibility with various early transition metals. Nowadays, tremendous number of reports have been known for this project, and some of them are very important from both academic and industrial point of view (see Reviews for post-metallocenes [20–24]; *Metal-catalysed Polymerisation (special issue)* [25]; Selected reviews for living polymerization [26–28]). In this chapter, efforts for designing molecular catalysts with early transition metals have been briefly reviewed.

3.2 Design, Synthesis of Molecular Catalyst with Early Transition Metals

3.2.1 Titanium, Zirconium, and Hafnium Complexes

As described above, titanium complex (1) containing bis(amide) ligand [18, 19] and zirconium complex with tridentate diamido ligand, [NON]ZrMe₂ (2) [29], for 1-hexene living polymerization introduced promising possibility for designing efficient catalyst, which does not contain cyclopentadienyl ligand (called non-metallocene catalyst), for olefin polymerization (Scheme 3.1). The catalytic activities by 1 in 1-hexene polymerization were suppressed upon addition of toluene, suggesting a possibility of coordination of toluene to the cationic catalytically-active species. Reaction of 1 with $B(C_6F_5)_3$ in *n*-pentane gave insoluble yellow-orange solids that was considered as a true catalyst for the living polymerization. The pentane suspensions slowly evolved CH_4 over several hours to give the pentane-soluble [ArN(CH₂)₃NAr]Ti[CH₂B(C₆F₅)₂](C₆F₅), which was structurally characterized and was inactive for the polymerization of α -olefins [30]. The resultant poly(1-hexene)s prepared by 1, 2 possessed atactic stereo-regularity.

Although the resultant polymer in the above reports afforded atactic poly (1-hexene), Eisen et al. presented synthesis of isotactic polypropylene by zirconium complexes containing tris(amidinate) ligand with chiral *N*-substituents, $[N(R^*)-C-N]_3ZrCl$ (3) [31]. In the propylene polymerization by 3—MAO catalyst in toluene, isotacticities for the resultant polymers were dependent upon the propylene pressure; the attempt under the atmospheric pressure of propylene was not successful. They speculated that one ancillary ligand was not acting as a spectator ligand, and MAO extracted one benzamidinate ligand from 3. This



Scheme 3.1 Pioneering examples for living 1-hexene polymerization [18, 19, 29]

displacement reaction would afford the proposed catalytically active species 3'. Isospecific propylene polymerization took place if zirconium complexes containing bis(amidinate) complexes (4), bearing achiral substituents R, at higher propylene pressures [32]. As shown in Table 3.1, the stereo-regularity in the resultant polypropylene was modulated by the pressure (from atactic to isotactic through elastomers). The different effects in the polymerization process such as the nature of solvent or cocatalyst, temperature, pressure, Al/M molar ratio (M = Ti, Zr), and the relationship between the symmetry of the complex and the polymer microstructure had been investigated [34]. The stereoregular errors were formed by the intramolecular epimerization of the growing chain at the last inserted unit. It was thus proposed that epimerization becomes faster than the stereoregular insertion of propylene at lower propylene pressure, leading to the formation of atactic polymer [34] (Scheme 3.2).

Isospecific living polymerization had been achieved by using C_2 symmetrical zirconium complex containing chelate bis(phenolate) ligand (**4b**, Scheme 3.3) [35]. Upon activation of **4b** with B(C₆F₅)₃, 1-hexene polymerization took place (rather efficiently), affording poly(1-hexene) with narrow molecular weight distribution (18 kg-polymer/mol-Zr·h, $M_w = 12000$, $M_w/M_n = 1.15$, >95% isotacticity). It was thus assumed that the high isotacticity would be due to a steric bulk of the ¹Bu group in **4b**, because the polymerization by **4a** under the same conditions afforded atactic poly(1-hexene) with higher activity (35 kg-polymer/mol-Zr·h, $M_w = 23000$, $M_w/M_n = 1.57$) [35]. The chloride analogue (**4c**) showed remarkable activity (5400 kg-polymer/mol-Zr·h), but the polymerization did not take place in a living manner, suggesting that the electronic factor on the phenyl group plays a role for exhibiting the high activity. In contrast, the titanium analogue of **4c** showed relatively high activity (200 kg-polymer/mol-Ti·h), affording ultra high molecular weight poly(1-hexene) with low PDI value as well as with relatively high isotacticity ($M_w = 5.50-19.0 \times 10^5$, $M_w/M_n = >1.2$, mm = 60 %) [36].

Titanium and zirconium complexes containing amine bis(phenolate) ligand (5) showed remarkable catalytic activity for α -olefin polymerization (Scheme 3.3)

| Solvent | Al/Zr ^b | Temp. /°C | Propylene /atm | Activity ^c | $M_{\rm n}^{\rm d}$ ×10 ⁻³ | $M_{\rm w}/M_{\rm n}^{\rm d}$ | mmmm ^e % | T ^f m ∕°C |
|------------|--------------------|--------------|-------------------|-----------------------|--|-------------------------------|-------------------------|-------------------------|
| Toluene | 250 | 25 | 9.2 | 110 ^g | 261 | 1.69 | 86 | 142 |
| | | | | | 36.0 | 2.35 | 11 | oil |
| CH_2Cl_2 | 250 | 25 | 9.2 | 220 | 10.7 | 2.49 | 90 | 146 |
| CH_2Cl_2 | 400 | 25 | 9.2 | 750 | 23.5 | 1.81 | 96 | 147 |
| CH_2Cl_2 | 1000 | 25 | 9.2 | 790 | 58.1 | 1.42 | 98 | 149 |
| CH_2Cl_2 | 250 | 0 | 5.1 | 50 | 10.2 | 1.85 | 86 | 138 |
| CH_2Cl_2 | 250 | 25 | 9.2 | 220 | 10.7 | 2.49 | 90 | 146 |
| CH_2Cl_2 | 250 | 50 | 17 | 2660 | 150 | 1.81 | 96 | 152 |
| Toluene | $B(C_6F_5)_3$ | 25 | 9.2 | 280 ^h | 26.0 | 1.96 | 98 | 154 |
| | | | | | 3.00 | 3.1 | 7 | oil |

Table 3.1 Propylene polymerization by $[Me_3SiNC(4-MeC_6H_4)NSiMe_3]_2ZrMe_2 (3'')^a$

^a Cited from Ref. [34]

^b MAO (solvent removed from a 20 % solution in toluene)

^c Activity in kg-PP/mol-Zr·h

^d GPC data 1,2,4-trichlorobenzene versus polystyrene standards

^e Estimated by ¹³ C NMR spectra

^f Melting Temperature

^g Mixture of isotactic (50 %) and atactic (50 %) fractions of polypropylene

h 70 % atactic and 30 % isotactic



Scheme 3.2 Isospecific propylene polymerization catalysts [31-34]

[36], and the reaction by the titanium analogue (R = t Bu, X = OMe) proceeded in a living manner, affording block copolymer consisting of poly(1-hexene) and poly(1-octene). An extra arm donor ligand plays an essential role to exhibit high catalytic activity, because the activity with the zirconium analogue (**6**) was extremely low [37]. This may be due to the fact that **6** folds pseudo-trigonal bipyramidal geometry whereas the complexes **5** fold distorted octahedral geometry around the metal center, which lead to the different bond angles between two benzyl (Bn) group (117.4° in **6** and 93.7° in **5**) [37]. More recently, Kol demonstrated that octahedral C_1 -symmetric titanium catalysts containing salalen ligand (**7**) are highly effective for isospecific propylene polymerization to afford polymers with extraordinary high isotacticity with high melting transition temperature ([*mmmm*] > 99.6 %, $T_m = 169.9$ °C) [43].

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Scheme 3.3 Group 4 metal complexes containing amine bis(phenolate) ligands [35-43]



Zirconium complexes bearing two salicylaldiminato-type ligands (8 in Scheme 3.4) exhibited remarkable catalytic activities for ethylene polymerization [44]. As shown in Table 3.2, the activity and the molecular weight of the polymer were dependent upon the substituent on the ligand. The activity was also affected by the centered metal [45], and increasing the steric bulk especially on both the phenoxy group in *ortho* position and the imino group strongly affected the catalytic activity. Molecular weights in the resultant PE were varied by the ligand modification [44]. The zirconium complex containing *N*-(3-cumyl-5-methyl-salicylidene) cyclohexylaminato ligand showed the highest activity for ethylene polymerization (4315000 kg-PE/mol-Zr·h) at 25 °C.

Importantly, ethylene polymerization by the fluorinated phenoxy-imine analogue (8') proceeded in a living manner [46], and the living polymerization of propylene afforded polypropylene with highly syndiotactic steroregularity [47, 48]. These living polymerizations took place even at room temperature, and synthesis of various block copolymers has been achieved in this catalysis [46–48]. The catalytic activity in the ethylene polymerization was high [46], whereas the activity for propylene polymerization was moderate but the polymerization

| • | | | | |
|---|-----------------|-----------------------|--------------------------|-------------------------------|
| $\frac{\text{Complex}}{\text{R}^1, \text{R}^2, \text{R}^3}$ | Amount /µmol | Activity ^b | $M_{ m v} 	imes 10^{-4}$ | $M_{\rm w}/M_{\rm n}^{\rm c}$ |
| H, ^t Bu, Ph | 0.02 | 550000 | 0.9 | 2.06 |
| Me, ^{<i>t</i>} Bu, Ph | 0.02 | 331000 | 0.7 | 2 |
| H, Me, Ph | 5 | 400 | 0.3 | 2.31 |
| H, ⁱ Pr, Ph | 5 | 900 | 0.6 | 2.48 |
| Me, adamantyl, Ph | 0.02 | 714000 | 1.2 | 2.69 |
| Me, cumyl, Ph | 0.01 | 2096000 | 1.8 | 7.2 |
| Me, cumyl, cyclohexyl | 0.005 | 4315000 | 1.5 | 1.88 |
| H, ^{t} Bu, 2-MeC ₆ H ₄ | 0.5 | 40000 | 32 | 2.13 |
| H, ^{<i>t</i>} Bu, $2 - {^{i}}PrC_{6}H_{4}$ | 0.5 | 58000 | 113 | 2.61 |
| H ^t Bu 2- ^t BuC ₆ H ₄ | 5 | 100 | >274 ^d | e |
| H, ^{<i>t</i>} Bu, 3,5- ^{<i>t</i>} Bu ₂ C ₆ H ₃ | 0.1 | 244000 | 2.6 | 1.79 |
| H, ^{t} Bu, 4- ^{t} BuC ₆ H ₄ | 0.1 | 271000 | 0.7 | 2.03 |
| H, ^{<i>t</i>} Bu, 2,6- ^{<i>i</i>} Pr ₂ C ₆ H ₃ | 5 | trace | | |
| Me, adamantyl, 2- ^{<i>i</i>} PrC ₆ H ₄ | 0.1 | 23000 | 153 | e |
| cumyl, cumyl, 2- ^{<i>i</i>} PrC ₆ H ₄ | 0.2 | 43000 | 220 | e |
| | | | | |

Table 3.2 Selected results for ethylene polymerization by Zr complex (8)—MAO catalyst systems $^{\rm a}$

^a Data cited from Ref. [44], Conditions: 25 °C, ethylene 1 atm, MAO (Al) 1.25 mmol, toluene 250 mL, 5 or 30 min

^b Activity in kg-PE/mol-Zr·h

^c Measured by GPC

^d Obtained from the polyethylene soluble in decalin under intrinsic viscosity measurement conditions

^e Polymer was hardly soluble in *o*-dichlorobenzene under GPC measurement conditions

proceeds in a highly syndiospecific manner although these Ti complexes possess C_2 symmetry [47, 48]. In ethylene polymerizations using titanium complexes with various fluorine containing phenoxy-imine chelate ligands, the complexes having a fluorine atom adjacent to the imine nitrogen showed the living nature at 50 °C, whereas the complexes possessing no fluorine adjacent to the imine nitrogen afforded polyethylenes having M_w/M_n values of ca. 2 with β -hydrogen transfer as the main termination pathway. In addition to the DFT calculation results, they assumed that the presence of a fluorine atom adjacent to the imine nitrogen is the requirement for the high-temperature living polymerization, because the fluorine of the active species for ethylene polymerization interacts with a β -hydrogen in the polymer chain, resulting in the prevention of β -hydrogen transfer [46].

Based on ¹³C NMR studies, they proposed that syndiotacticity in the propylene polymerization was governed by a chain-end control mechanism and that the polymerization is initiated exclusively via 1,2-insertion followed by 2,1-insertion as the principal mode of polymerization, and that the polypropylenes produced with the Ti complexes possess regio-block structures. Substitutions on the phenoxy-imine ligands affected both the catalytic activity and the stereo specificity, and the steric bulk of the substituent in *ortho* position of the phenoxy oxygen plays a decisive role in achieving high syndioselectivity for the chain-end controlled

| R in 8′ | Temp./ | TOF ^b | $M_{\rm n}^{\rm c} \times 10^{-3}$ | M _w / | $T_{\rm m}^{\rm d}/$ | rr ^e |
|-------------------|--------|------------------|------------------------------------|---------------------|----------------------|-----------------|
| | °C | | - | $M_{\rm n}^{\rm c}$ | °Ċ | |
| Н | 25 | 729 | 189 | 1.51 | nd ^f | |
| Me | 25 | 1635 | 260.2 | 1.22 | nd ^f | |
| ⁱ Pr | 25 | 739 | 153.7 | 1.16 | nd ^f | |
| ^t Bu | 0 | 68 | 23.6 | 1.05 | 136 | |
| ^t Bu | 25 | 87 | 28.5 | 1.11 | 137 | 87 |
| ^t Bu | 50 | 70 | 16.4 | 1.37 | 130 | |
| SiMe ₃ | 0 | 72 | 24.7 | 1.08 | 156 | 94 |
| SiMe ₃ | 25 | 139 | 47 | 1.08 | 152 | 93 |
| SiMe ₃ | 50 | 113 | 35.1 | 1.23 | 149 | 90 |
| SiEt ₃ | 0 | 42 | 11.9 | 1.08 | 152 | 93 |
| SiEt ₃ | 25 | 83 | 24.4 | 1.16 | 151 | |
| SiEt ₃ | 50 | 63 | 20.4 | 1.23 | 148 | |

Table 3.3 Selected results for propylene polymerization by 8'-MAO catalyst systems^a

 a Cited from Ref. [48], Conditions: complex 10 $\mu mol,$ MAO 2.5 mmol, propylene 1 atm, 5 h

^b Turnover frequency

^c Determined by GPC using polypropylene calibration

^d Melting temperature of produced PP determined by DSC

^e Estimated by ¹³C NMR spectra

f Not detected

polymerization (Table 3.3) [47, 48]. The Ti complex having SiMe₃ group in *ortho* position of the phenoxy ligand afforded highly syndiotactic, nearly monodisperse polypropylenes (94–90 % *rr*) with extremely high melting temperatures ($T_{\rm m} = 156-149$ °C). The polymerization behavior of the Ti complexes was explained by the proposed chain-end controlled, site-inversion mechanism for the formation of syndiotactic polypropylene by **8**'. Copolymerization of ethylene with α -olefin by **8**' also proceeded in a living manner in the presence of MAO, and various block copolymers were also thus prepared [49].

Synthesis of the related complexes such as titanium complexes containing two indole-imine ligands (9) [50], pyrrolide-imine ligand (10) were known [51], and living copolymerization of ethylene with norbornene took place if 10 was used as the catalyst precursor [52, 53].

Chain Shuttling Polymerization

Precise synthesis of microblock ethylene/1-octene copolymers which possesses two compositions (copolymers with low/high 1-octene contents) in a polymer chain was also achieved by adopting the polymerization process called "Chain Shuttling Polymerization" in the presence of two catalysts (with efficient/inefficient comonomer incorporations, different monomer reactivity, Scheme 3.5) and chain transfer reagent (Et₂Zn etc.) [54]. The resultant polymers (prepared by adding Et₂Zn during polymerization results in a block copolymer microstructure with intimately mixed interchain hard and soft segments) possess higher transparency than the polymers with two physical blend of high- and low-density polymers, and possessed higher melting temperature and low glass transition temperature (due to a



Scheme 3.5 Precise synthesis of microblock copolymers by "chain shuttling polymerization" [54]

block segment with low 1-octene content). These are recognized as a new technology for evolution of new polymers on the basis of precise olefin polymerization technique [54].

The isospecific α -olefin polymerization catalyst (11) was developed by DOW on the basis of 1600 catalyst screenings (required only for 3 weeks) by using "high throughput screening" (Symyx Technologies) technique: this demonstrated a new methodology for the catalyst development [55, 56]. Another key issue on this process is adopting rapid chain transfer reactions enabled by presence of Et₂Zn (rapid chain transfer by Et₂Zn [57–60]): rapid polymer exchange between 8″ and 11 through Zn afforded the polymers with multiblock (microblock) microstructure.

Ligand Modification from Ethylene Polymerization Catalyst to Trimerization Catalyst

It has been known in that ethylene polymerization catalyst was tuned to the ethylene trimerization by the ligand modification. $[(\eta^5-C_5H_5)CMe_2Ph]TiCl_3$ —MAO catalyst exhibited moderate catalytic activity with high selectivity for ethylene trimerization, whereas ethylene polymerization took place by $[(\eta^5-C_5H_5)CMe_3]$ -TiCl₃ [61]. Titanium trichloride complexes containing monoanionic tridentate ligands (**12,13**) exhibited moderate to high catalytic activities for ethylene polymerization (Scheme 3.6) [62, 64]: **12** showed better catalyst performance for ethylene copolymerization with 1-hexene and norbornene [62]. In contrast, complex **14** showed remarkable selectivity in ethylene trimerization in the presence of MAO, and second order dependence of activity on ethylene pressure (suggesting the metallacycle mechanism) was observed [65]. These would suggest that the



effective catalyst for the polymerization can be tuned to the effective catalyst for the trimerization by the ligand modification.

Ti–Al Hetero Bimetallic Complexes Containing Chelate Trianionic Donor Ligand Titanium complexes with tris(aryloxo)amine or bis(aryloxo)(alkoxo)amine ligand, Ti(OR')[(O-2,4-R₂C₆H₂-6-CH₂)₃N] or Ti(OR')[(O-2,4-R₂C₆H₂-6-CH₂)₂ (OCH₂CH₂)N] (R = Me, 'Bu; R' = ⁱPr, 'Bu), exhibited from moderate to high catalytic activity for ethylene polymerization especially at high temperature (100–120 °C), and the activities increased upon addition of small amount of AlMe₃ [66, 68]. The resultant polymers possessed unimodal molecular weight distributions, suggesting that the polymerization proceeded with a uniform catalyticallyactive species. The resultant heterobimetallic Ti–Al complexes (**15**, **16**) exhibited moderate catalytic activities upon heating under ethylene pressure even in the absence of any additional cocatalyst, strongly suggesting that cleavages of Ti–O bonds would generate the catalytically active cationic species in this catalysis (Scheme 3.7) [67, 68].

Isospecific/Syndiospecific Styrene Polymerization

Titanium complexes containing 1,4-dithiabutane-bridged derivatives (17) showed notable catalytic activities affording isotactic polystyrene with unimodal molecular weight distributions, whereas the 1,5-dithiapentane-bridged derivatives (18) showed low catalytic activities affording syndiotactic polystyrene (Scheme 3.8) [69]. The analogous zirconium, hafnium complexes of 17 also showed the low catalytic activity to afford isotactic polystyrene, suggesting that C_2 -symmetric ligand sphere should play a crucial role for this isospecific polymerization [69, 71].

As shown in Table 3.4, the substituents on the ligand affected the activity and stereoselectivity, and these facts were evidently related to the effect of these substituents on the stereorigidity of the catalyst precursors. Complexes bearing less bulky *ortho*-substituents R^1 in the aromatic ring (H, Me, ^{*i*}Pr) allowed rapid interconversion on the NMR time scale, while the complexes with bulky groups (^{*i*}Bu, CMe₂Ph) were stereorigid at temperatures up to 100 °C. Small *ortho*-



Scheme 3.7 Ti-Al Hetero bimetallic complexes that polymerize ethylene without cocatalyst [67, 68]



Scheme 3.8 Isospecific styrene polymerization by titanium complexes containing chelate bis(phenolate) ligands [69–71]

substituents thus led to configurational lability at room temperature and resulted in the loss of both activity and stereospecificity. Syndiospecific styrene polymerization with relatively low activity was observed by titanium complexes with 1,5dithiapentanediyl-linked bis(phenolato) ligands. Only the configurationally stable 1,4-dithiabutanediyl-linked phenolates with bulky *ortho*-substituents appeared to be capable of stabilizing a C_2 -symmetric, helical ligand sphere at the titanium center and thereby provided an active site for the isospecific styrene polymerization [71].

3.2.2 Vanadium Complexes

Classical Ziegler type vanadium catalysts (ex. VOCl₃, VCl₄, VCl₃–AlBr₃, AlCl₃– AlPh₃, Al^{*i*}Bu₃, SnPh₄) are known to display unique characteristics in olefin polymerization. In general, these catalyst systems afforded (i) high molecular

| Complex | Substituents: R ¹ , R ² | Activity ^b | $M_{\rm n}^{\rm c} \times 10^{-4}$ | $M_{\rm w}/M_{\rm n}^{\rm c}$ | $T_{\rm m}^{\rm d}/^{\circ}{\rm C}$ |
|------------------------|---|-----------------------|------------------------------------|-------------------------------|-------------------------------------|
| 17 ^e | H, H | 4 | 1.2 | 82 | |
| 17 ^f | H, Me | 7 | 193.5 | 1.57 | |
| | | 0.7 | 1.88 | | |
| 17 ^e | Me, Me | 4 | 1.2 | 50 | |
| 17 ^e | ⁱ Pr, ^t Bu | 5 | n.d. | n.d. | |
| $17^{\rm f}$ | ^t Bu, Me | 518 | 101.3 | 1.57 | 222 |
| $17^{\rm f}$ | ^t Bu, ^t Bu | 1543 | 265.4 | 2 | 223 |
| 17 ^f | ^t Bu, OMe | 3 | 91 | 1.66 | 222 |
| | | | 1 | 1.76 | |
| 17 ^e | CMe ₂ Ph, Me | 175 | 70 | 1.9 | 225 |
| 17 ^{f, g} | CMe ₂ Ph, CMe ₂ Ph | 682 | 31.4 | 2.36 | 223 |
| 18 ^f | ^t Bu, Me | 0.7 | 2.89 | 268 | |
| 18 ^f | ^t Bu, ^t Bu | 3 | n.d. | n.d. | 264 |

Table 3.4 Isospecific/syndiospecific styrene polymerization by titanium complexes containing chelate bis(phenolate) ligands^a

^a Cited from Ref [69], [styrene] = 3.5 mol/L (10 mL), toluene 15 ML

^b Activity in kg-PS/[mol-Ti][styrene mol/L][h]

^c Determined by GPC. n.d. = not determined

^d Determined by DSC thermograms

 e Conditions: Ti 10 µmol, [Al]/[Ti] = 500, 50 °C, 1 h

 $^{\rm f}$ Conditions: Ti 2.5 $\mu mol,~[Al]:[Ti]$ = 1500, 40 °C, 2 h

g Reaction time: 1 h

weight linear polyethylene with uniform molecular weight distribution [72–74], and (ii) high molecular weight amorphous polymers applied to syntheses of ethylene/propylene/diene copolymers (called EPDM, synthetic rubbers) [75–77], ethylene/cyclic olefin copolymers (COC). Moreover, (iii) the catalyst system [V(acac)₃ (acac = acetylacetonato)—Et₂AlCl] polymerizes propylene to give not only a syndiotactic "living" polymer with narrow molecular weight distribution ($M_w/M_n = 1.05-1.20$) [78–80], but also diblock copolymers of propylene and methyl methacrylate (MMA) [78–80]. On the basis of ESR and titration results, vanadium(III) species were postulated to play an important role as the catalytically active species [81–84], although it was estimated that fewer than 1 % of vanadium species were catalytically active in the mixture [83].

One of the main disadvantages of using this type of vanadium catalysts is the deactivation associated with the reduction to inactive vanadium(II) species. Although very high initial activities were observed by adopting these catalysts, the reduction causes very poor overall productivities. This problem could be overcome by reactivation of inactive vanadium(II) center to active vanadium(III) species by addition of re-oxidants such as hexachlorocyclopentadiene [85], ethyl trichloro-acetate [86], and the polymerization proceeded without significant decrease in the activity by continuous addition of an aluminum alkyl and the re-oxidants even at high temperature (>105 $^{\circ}$ C) [86].

As described above, the classical Ziegler type vanadium catalysts displayed unique characteristics as the olefin polymerization catalysts. Therefore, design and synthesis of new vanadium complex catalysts directed toward the controlled polymerization has been recognized as an attractive target [11–13, 29, 87–90]. Although examples for synthesis of vanadium complexes used as the catalyst precursors for olefin polymerization were known, however, known examples which exhibit the above described unique characteristics of using these transition metal complexes had been limited until recently [20–24, 86, 87–90].

3.2.2.1 Vanadium(III), (IV) Complexes

Vanadium(III), (IV) complexes have been focused on design of the efficient polymerization catalysts, because these were assumed to play an important role as the active species in olefin polymerization. Since only a trace of *actual* active species were present due to that these species would be unstable and be readily reduced by Al cocatalyst to afford the catalytically inactive vanadium(II) species, many researchers thus concentrate on stabilization of the oxidation state of the catalytically active species by an appropriate ligand modification [23, 86].

Dinuclear vanadium(III) chloride complex (19) containing bis(amido)amine ligand of type, (Me₃SiNCH₂CH₂)₂NSiMe₃, exhibited remarkable catalytic activity for ethylene polymerization in the presence of MAO, Me₂AlCl at 50 °C [activity: 237 kg-PE/mol-V·h (MAO), 660 kg-PE/mol-V·h (Me₂AlCl); ethylene 300 psig (20.4 atm), Al/V = 60 (molar ratio)] [91]. Resultant polyethylene prepared by 19-Me₂AlCl catalyst possessed high molecular weight with uniform molecular weight distribution $(M_w = 7.21 \times 10^5, M_w/M_n = 2.3)$. The catalyst system was short-lived, does not remain to be active for no more than 20-30 min, and this may be attributed to the reduction of the vanadium(III) center to an inactive divalent species. The reaction of 19 with AlMe₃, Me₂AlCl and MAO in *n*-hexane initially gave a red solution, which after a few days afforded another vanadium(II) complex identified as **19b** (Scheme 3.9). This result thus suggested that no ligand dissociation occurred in the present catalyst system but aggregation with the cocatalyst. The question of how the reduction of 19 afforded the inactive divalent species (19b) was thus considered. The reaction of 19 with AlCl₃ afforded disproportionated compounds, (tetravalent) 19c and (one divalent and two trivalent) 19d, clearly indicating that disproportionation was the basis of a reduction of the vanadium center. These results suggested a possibility of the reduction of 19 affording 19b and that the addition intermediate 19a, which is likely to be the catalytically-active species, has the intrinsic instability of a vanadium-carbon bond [91].

A mixed-valent vanadium complex containing dithiolate ligand (**20c**, Scheme 3.10) showed moderate catalytic activity for ethylene polymerization in the presence of both Et₂AlCl and MgCl₂ [activity 254 kg-PE/mol-V·h, ethylene 6 atm, 50 °C, 15 min.] [92], but the activity was lower than those by the aryloxo analogues (**20a**, 1990 kg-PE/mol-V·h; **20b**, 1020 kg-PE/mol-V·h), under the same conditions (in *n*-hexane) [92]. The ligand in **20c** transferred to Al alkyls upon treatment with



Scheme 3.9 Reaction of dinuclear vanadium(III) chloride complex containing bis(amido)amine ligand [91]

AlMe₃ affording vanadium(II) chloride and [AlMe{ μ_2 -O(CH₂CH₂S)}]₂ [93]. Use of thiobis(phenoxy) ligand improved the activity, and the complex **21** showed remarkable activities in the presence of cocatalyst [activity = 11708 kg-PE/mol-V·h (AlⁱBu₃), 8184 (Et₂AlCl), 4736 (MAO); ethylene 5 atm, Al/MgCl₂/V = 100/10/1 (AlⁱBu₃, Et₂AlCl) or 3000/10/1 (MAO)] [94]. The resultant polymers possessed unimodal molecular weight distributions ($M_w/M_n = 2.28-3.12$), suggesting that these polymerizations proceeded with uniform catalytically active species.

Vanadium(III) complexes containing two or three O,N-chelating aminophenolate ligand (22,23) exhibited activities for ethylene/propylene copolymerization in the presence of $Et_2AlCl \cdot EtAlCl_2$ [95]. The bis(phenoxy) complex (23) showed higher activity [159 kg-polymer/mol-V·h·bar, 8 bar of ethylene/propylene (ratio 1/2) in pentamethylheptane at 30 °C for 10 min.] than the tris(phenoxy) complex (22, 27 kg-polymer/mol-V·h·bar). Olefin polymerization using a series of vanadium complexes containing an amine bis(phenolate) ligand, $[(O-2,4-Me_2C_6H_2-6-CH_2)_2]$ $(Me_2NCH_2CH_2)N|^{2-}$ (exemplified as complex 24), with various oxidation states (II-V) were explored [96, 97]. Complex 24 showed notable activity in ethylene polymerization in the presence of EtAlCl₂, but showed negligible activity in the presence of MAO [96]. Copolymerizations of ethylene with 1-hexene, norbornene were attempted, but the activities decreased and the resultant polymers possessed a mixture of coplymers with different compositions estimated by their DSC thermograms [96]. Vanadium(III) complex containing bis(phenoxy)pyridine ligand (25) showed remarkable catalytic activity for propylene polymerization in the presence of MAO (activity 803 kg-PP/mol-V·h, propylene 5 atm in toluene at 0 °C for 30 min, Al/V = 3000), affording high molecular weight polymer with uniform molecular weight distribution ($M_w = 1.17 \times 10^6$, $M_w/M_n = 2.03$) [98]. The resultant polymer possessed large extent of regio irregular as generally seen in those prepared by vanadium catalysts.

Taking into account the above reports (vanadium complexes using chelate anionic and neutral donor ligands) [91–98], as described above, control, stabilization of the oxidation state, catalytically active species) by an appropriate ligand modification seems to be a key for the efficient catalyst with vanadium(III),



Scheme 3.10 Selected vanadium complexes for olefin polymerization [91-98]

although the *actual* active species including the activation/polymerization mechanism are still not clear at the present stage.

A series of vanadium(III) complexes containing β -enaminoketonato [99, 100], phenoxy-imine [101–104], imino-pyrrolide [105] ligands (exemplified in Scheme 3.11) were tested as olefin polymerization catalyst in the presence of Et₂AlCl and Cl₃CCO₂Et. The selected results are summarized in Table 3.5 [99, 100, 103, 105]. The observed activities by certain complexes were slightly/apparently higher than those by VCl₃(THF)₃, and the activities decreased at 70 °C probably due to the rapid deactivation even for short period (5 min) and in the presence of excess amount of re-oxidant (300 equivalent to V). On the basis of these data, it seems that **26b** $(R^1; R^2 = {}^tBu; CF_3)$ [99, 100], **26d** $(R^1; R^2 = Ph; CH_3)$ [99, 100], **27 h** [103] showed higher activities. The related phenoxy-imine analogues showed low activities under the same conditions [101–104]. Placement of neutral donor ligands (amine, pyridine) into the phenoxy-imine ligands in 27 was not effective; the observed activity by 27 h was relatively close to 26e. Although both the activities and the polymerization behavior were affected by the ligand substituents, the detailed explanation by electronic/steric factors seems difficult (factors such as ligand transfer to Al, reductions etc.). In contrast, the imino-pyrrolide analogues (28) showed remarkable activities [105], and the activities by 28 increased in the order (ethylene 1 atm, 50 °C for 5 min): 28c (R = $2,6^{-i}Pr_2C_6H_3$) > 28b, e (Ph, C_6F_5) > 28d



Scheme 3.11 Selected vanadium(III) complexes as catalyst precursors for olefin polymerization [99, 100, 103, 105]

| Complex | Temp. /°C | Activity /kg-PE/mol-V·h | $M_{ m w}^{ m b} 	imes 10^{-4}$ | $M_{\rm w}/M_{\rm n}^{\rm b}$ |
|-------------------------------------|-----------|-------------------------|---------------------------------|-------------------------------|
| VCl ₃ (THF) ₃ | 25 | 25800 | 22.7 | 2.8 |
| VCl ₃ (THF) ₃ | 50 | 23400 | 13.4 | 5.8 |
| VCl ₃ (THF) ₃ | 70 | 12600 | 9.9 | 21.9 |
| 26a | 50 | 27400 | 17.7 | 2.6 |
| 26b | 50 | 29000 | 18.6 | 3.0 |
| 26c | 50 | 21800 | 25.9 | 2.9 |
| 26d | 50 | 24000 | 17.3 | 2.9 |
| 26e | 50 | 18700 | 27.1 | 2.9 |
| 27a | 50 | 3840 | 4.0 | 2.4 |
| 27ь | 50 | 9600 | 3.5 | 3.0 |
| 27c | 50 | 15600 | 6.2 | 2.2 |
| 27d | 50 | 9120 | 4.8 | 2.5 |
| 27e | 50 | 7920 | 6.3 | 2.0 |
| 27f | 50 | 11300 | 4.6 | 2.5 |
| 27g | 50 | 9360 | 3.0 | 2.2 |
| 27h | 50 | 20600 | 2.4 | 2.0 |
| 28a | 50 | 28200 | 3.5 | 2.1 |
| 28b | 50 | 37800 | 4.3 | 2.2 |
| 28c | 25 | 39600 | 6.3 | 2.4 |
| 28c | 50 | 48600 | 2.5 | 1.7 |
| 28c | 70 | 34200 | 1.0 | 2.2 |
| 28d | 50 | 33000 | 4.4 | 2.4 |
| 28e | 50 | 39000 | 3.0 | 1.9 |
| | | | | |

Table 3.5 Ethylene polymerization by 26-28-Et₂AlCl-Cl₃CCO₂Et catalyst systems^a

^a Cited from Refs. [99, 100, 103, 105], Reaction conditions: vanadium 0.2 or 0.5 μ mol, Et₂AlCl and Cl₃CCO₂Et (ETA), Al/ETA/V = 4000/300/1 (molar ratio), ethylene 1 atm for 5 min ^b GPC data in 1,2,4-trichlorobenzene versus polystyrene standards

 $(4-CF_3C_6H_4) > 28a$ (cyclohexyl). The results thus suggest that both electronic and steric factors play an important role (probably for strong coordination).

Complex 27c showed high activity in the ethylene/norbornene copolymerization and the activity was close to that by 27h under the same conditions, although the activity by 27c was lower than that by 27h in the ethylene polymerization [103]. Complexes 28 showed moderate comonomer incorporation with higher activities in ethylene/10-undecen-1-ol copolymerizations, affording the copolymers with relatively low molecular weights ($M_n = 3.1-52.5 \times 10^3$) [105]: the M_n values decreased upon increasing the comonomer content [105].

Vanadium(III) complex containing neutral bis(imino)pyridine ligand (29a) exhibited remarkable catalytic activities for ethylene polymerization in the presence of MAO, affording the polymers with broad molecular weight distributions [activities 1420, 2240 kg-PE/mol-Vh, with Al/V = 600, 60 (molar ratio), respectively; ethylene 100 psig (6.8 atm), 50 °C, 15 or 30 min] (Scheme 3.12) [106]. The activities decreased at 140 °C, and the molecular weight distributions in the resultant polymers were dependent upon the Al/V molar ratios. The reaction with ethylene using the complexes (29d, e) containing mono substituted aromatic group on the imino ligand (in place of 2,6-diisopropylphenyl) afforded oligomeric mixtures and polyethylene (products by Schultz-Flory distribution) [107], (Dimerization of propylene (selectivity 80–95 %) [108]), and the reaction with propylene by **29f**, **g** afforded oligomers with relatively high C_6 selectivity (80-95 %, major products: methylpentenes) [107], (Dimerization of propylene (selectivity 80-95 %) [108]). These results suggested that the observed trend concerning the ligand effect was very similar to that observed in the ethylene polymerization/oligomerization using iron(II) complexes containing similar ligands [109–115]. The bis(carbene)pyridine complex (30) showed remarkable activities for ethylene polymerization, and the activity was affected by the Al cocatalyst employed [116]. The activity decreased in the order (ethylene 1 atm in toluene at r.t. for 30 min, Al/V = 500, molar ratio): 1446 kg-PE/mol-V·h (MMAO, methyl-isobutyl-aluminoxane) > 1280 (MAO) > 586 (dried MAO and $Al^{i}Bu_{3}$ > 278 (Et₂AlCl).⁵⁹

(Arylimido)vanadium(IV) dichloride complexes (**31**, Scheme 3.13) showed high activities for ethylene polymerization in the presence of Al cocatalyst [activity by **31b**: 59 kg-PE-mol-V·h (MAO, Al/V = 500), 120 kg-PE-mol-V·h (Et₂AlCl, Al/V = 10); ethylene 1 atm, 20 °C in toluene, 2 or 10 min], affording the polymers with uniform molecular weight distributions [117, 118]. The activities in ethylene/ propylene copolymerization using vanadium(IV) complexes containing two amide ligands (**32**) were affected by the Al cocatalyst employed, and the activity by **32a** decreased in the order: Et₂AlCl·EtAlCl₂ (860 kg-polymer/mol-V·h) > EtAlCl₂ (330) > Et₂AlCl (80) > AlEt₃ (24) [conditions: ethylene + propylene total 2 bar in hexane at 22 °C for 15 min, Al/V = 40 (molar ratio)] [119]. The isopropyl amide complex (**32a**) showed higher activity than the cyclohexyl analogue (**32b**) [119], and the resultant polymer possessed high molecular weight with uniform molecular weight distribution (**32a**—Et₂AlCl·EtAlCl₂ catalyst, $M_w = 2.29 \times 10^6$, $M_w/$ $M_n = 3.0$, ethylene 73 wt%). Vanadium(IV) complex with chelate bis(amide)



Scheme 3.12 Vanadium(III) complexes with neutral tridentate donor ligands [106–116]



Scheme 3.13 Selected vanadium(IV) complexes as catalyst precursors for olefin polymerization [117–123]

ligand (34) showed higher activity than the bis(amide) analogue (33) in ethylene polymerization [activities in the presence of Et₂AlCl·EtAlCl₂: 213 kg-PE/mol-V·h, 54 kg-PE/mol-V·h for 34, 33, respectively: ethylene 1 atm in toluene at 30 °C, Al/V = 50]. Although the activity in the ethylene polymerization by 36 is close to that by 32a (178 kg-PE/mol-V·h), 34 showed higher activity in ethylene/propylene copolymerization [120].

Vanadium(IV) complex with N,O-bidentate ligand (**35b**) showed higher activity than **35a**, probably owing to increasing the steric bulk, and the activity was highly affected by the Al cocatalyst employed [EtAlCl₂ \gg Et₂AlCl > MAO]. The resultant polymers possessed rather high molecular weights with moderate distributions

[121]. The salen-type tetradentate complexes (**36**, **37**) also showed from moderate to high activities for ethylene polymerization [122, 123], and the activities of **37** were higher than **36**: the activities were affected by the *ortho*- substituent in the phenoxo moiety, and by Al cocatalyst employed. However, the resultant polymer possessed broad molecular weight distributions ($M_w/M_n = 7.3-10.4$), suggesting generation of multiple catalytically active species [122, 123].

3.2.2.2 Vanadium(V) Complexes

As described above, VOCl₃ showed moderate activities for ethylene/propylene (co)polymerization in the presence of Al alkyls, however, one of the major concerns associated with use of vanadium(V) complexes as catalysts for Ziegler-Natta polymerizations is a facile reduction to yield lower-valent complexes. Use of arylimido analogues seemed to be promising, because a series of trichloride analogues, V(NAr)Cl₃, can be prepared in high yields by treating VOCl₃ with various isocyanates (ArNCO) [124–126], and these complexes showed moderate thermal stability, as demonstrated by synthesis of V(N-2,6-^{*i*}Pr₂C₆H₃)(CH₂Ph)₃ from the trichloride analogues by treating with PhCH₂MgCl in *n*-hexane [127]. The reported fact is noteworthy, because the most common problem encountered in attempts to synthesize vanadium(V) alkyls was the reduction of the metal center upon alkylation. Placement of appropriate alkyl substituent in the arylimido ligand is important for stabilization of the oxidation state upon the alkylation, and the approach is useful for synthesis various vanadium(V)-alkyls [128–131].

It turned out that the arylimido-aryloxo analogue (38) showed remarkable activities not only for ethylene polymerization [132–135], but also for ethylene/ norbornene copolymerization [136] especially in the presence of halogenated Al alkyls (Et₂AlCl, Me₂AlCl, EtAlCl₂ etc.) [134–136], affording high molecular weight polymers with uniform distributions. Selected results in the ethylene polymerization catalyzed by V(N-2,6-Me₂C₆H₃)Cl₂(O-2,6-Me₂C₆H₃) (38) are summarized in Table 3.6 [135]. The activity was highly dependent upon the Al cocatalyst employed, and the activities in toluene decreased in the order: ^{*i*}Bu₂AlCl $(52000 \text{ kg-PE/mol-V}\cdot\text{h}) > \text{EtAlCl}_2$ $(37400) > Me_2AlCl$ $(27500) > Et_2AlCl$ $(11700) > MAO (2930) \gg Et_2Al(OEt), Me_3Al, Et_3Al (trace or less).$ The activity did not decrease after 30 min, and was highly affected by the solvent employed; the activity of 584000 kg-PE/mol-V h (TOF 20800000 h⁻¹, 5780 s⁻¹) was attained in CH₂Cl₂ in the presence of EtAlCl₂. The resultant polymers prepared in toluene possessed ultra high molecular weights with unimodal molecular weight distributions (the $M_{\rm v}$ values in the resultant polymers prepared in the presence of ⁱBu₂AlCl, Me₂AlCl were 9.87–12.5 \times 10⁶, 8.98 \times 10⁶, respectively). The activity decreased upon addition of CCl₃CO₂Et, which is commonly used as the effective additives in the polymerization using vanadium(III) and/or vanadium(IV) complexes. The results clearly suggest that the active species were thus different from those prepared from vanadium(III), (IV) complexes. It was assumed that the observed difference in the catalytic activities in the presence of MAO and Et₂AlCl

| 38 / µmol | Al cocat. | Time / min | Activity ^b $\times 10^{-3}$ | $TOF^{c} \times 10^{-5}$ | $M_{\rm w}^{\rm d} \times 10^{-5}$ | $M_{ m w}/M_{ m n}^{ m d}$ | $M_{\nu}^{\rm e} \times 10^{-6}$ |
|-------------------|-----------------------------------|---------------|--|--------------------------|------------------------------------|----------------------------|----------------------------------|
| 1.0 | MAO | 10 | 2.93 | 1.04 | 28.7 | 1.64 | |
| 0.05 | Me ₂ AlCl | 10 | 27.5 | 9.8 | _ ^e | _ | 8.98 |
| 0.05 | Et ₂ AlCl | 10 | 11.7 | 4.15 | 36.5 | 1.42 | |
| 0.05 | Et ₂ AlCl | 30 | 11.4 | 4.06 | | | |
| 0.05 ^f | Et ₂ AlCl | 10 | 1.08 | 0.4 | | | |
| 0.05 | ⁱ Bu ₂ AlCl | 10 | 52.0 | 18.5 | _ ^e | - | 9.87 |
| 0.01 | ⁱ Bu ₂ AlCl | 10 | 64.8 | 23.1 | _ ^e | - | 12.5 |
| 0.05 | EtAlCl ₂ | 10 | 37.4 | 13.3 | 6.02 | 3.04 | |
| 1.0 | Et ₂ AlOEt | 10 | None | - | | | |
| 1.0 | Me ₃ Al | 10 | Trace | _ | | | |
| 1.0 | Et ₃ Al | 10 | Trace | _ | | | |
| 1.0 | ⁱ Bu ₃ Al | 10 | trace | - | | | |

Table 3.6 Ethylene polymerization catalyzed by $VCl_2(N-2,6-Me_2C_6H_3)(O-2,6-Me_2C_6H_3)$ (**38**)—Al cocatalyst systems: effect of Al cocatalyst^a

^a Data cited from Ref. 135, reaction conditions: toluene + cocatalyst solution = 30 mL, 0 °C (or 25 °C by MAO), ethylene 8 atm, Al cocatalyst 250 or 500 μ mol (or MAO 2.5 mmol)

^b Activity in kg-polymer/mol-V·h

^c TOF = (molar amount of ethylene consumed)/(mol-V·h)

^d GPC data in o-dichlorobenzene versus polystyrene standards

^e Molecular weight by viscosity due to that the resultant polymers were insoluble in *o*-dichlorobenzene for GPC measurement

^f Polymerization in the co-presence of CC₁₃CO₂Et (10.0 equiv to V)





Scheme 3.14 Proposed formation of two catalytically active species [23, 134, 135, 140]

cocatalyst would be due to the different catalytically active species, catalyst/ cocatalyst nuclearity effect [137, 138] generated in the two catalyst systems, as shown in Scheme 3.14 [23].



Scheme 3.15 Ethylene dimerization by (imido)vanadium(V) complexes containing (2-anili-domethyl)pyridine ligand [139, 140]

The (imido)vanadium(V) complexes containing (2-anilidomethyl)pyridine ligand, $V(NR)Cl_2[2-ArNCH_2(C_5H_4N)]$ [R = 1-adamantyl (Ad), cyclohexyl (Cy), phenyl (Ph)], exhibited remarkably high catalytic activities for ethylene dimerization in the presence of MAO, affording 1-butene exclusively (selectivity from 90.4 to > 99 %, Scheme 3.17) [139]. The phenylimido analogue (40) also afforded 1-butene under the same conditions, whereas the 2,6-dimethylphenylimido analogue (39) afforded polyethylene. The cyclohexylimido analogues also showed high activities to afford 1-butene exclusively. The adamantylimido analogues (41) showed the highest activities (TOF: 2730000 h^{-1}) for ethylene dimerization. These results thus clearly indicate that (i) the electronic nature of the imido ligand directly affects the activity, and (ii) the steric bulk of the imido substituents plays an essential key role toward the selectivity in this catalysis [139]. Moreover, 41—Et₂AlCl, Me₂AlCl afforded ultra high molecular weight polyethylene, suggesting a presence of proposed reaction scheme shown in Scheme 3.15 [140]. On the basis of reactions under various conditions, and ESR and NMR experiments, it was thus proposed that cationic vanadium(V)-alkyls play an important role in these catalysis [140].



Scheme 3.16 Known scandium catalysts for olefin polymerization [141–143]

3.2.3 Miscellaneous Early Transition Metal Complex Catalysts

3.2.3.1 Scandium Complexes

Examples for olefin polymerization using non-metallocene type scandium complex catalysts still have been limited but demonstrate promising possibilities: examples as catalyst precursors for conjugated diene polymerization (butadiene, isoprene) have also been reported. The complex containing β -diketiminato "nacnac" (42, Scheme 3.16) exhibited moderate to high catalytic activities for ethylene polymerization [1200 kg-PE/mol-Sc·h (MAO, Al/Sc = 20), 300 kg-PE/mol-Sc·h $\{B(C_6F_5)_3, ca. 1 \text{ equiv.}\}$: ethylene 300 psi, 50 °C, cyclohexane/toluene], affording high molecular weight polymers with uniform distributions ($M_{\rm w} = 8.51 - 18.7 \times$ 10^5 , $M_w/M_n = 1.7-2.48$ [141]. The reaction of 42 with 1.0 equiv. of B(C₆F₅)₃ afforded monocationic [(nacnac)ScMe]⁺[μ -Me-B(C₆F₅)₃]⁻, and the dicationic species $[(nacnac)Sc]^{2+}$ [μ -Me-B⁻(C₆F₅)₃]₂ by treating 42 with 2.0 equiv. of B(C₆F₅)₃ exhibited moderate catalytic activity for ethylene polymerization (1 atm at r.t.) [141]. In contrast, ethylene polymerization using the admidinate analogue, [ArNC(Ph)NAr]Sc(CH₂SiMe₃)₂(THF) (43) was low [activity 120 kg-PE/mol-Sc·h, ethylene 5 bar, {PhN(H)Me₂}(C₆F₅)₄, 30 °C 20 min], and the acitivity by the Y, Gd, Nd complexes showed higher catalytic activities $(1.0-1.5 \times 10^4 \text{ kg-PE/mol-M}\cdot\text{h})$ under the same conditions [142]. A dicationic scandium complexes containing a C_3 -chiral ligand, prepared from [^{*i*}Pr-trisox]Sc(CH₂SiMe₃)₃ (44) with 2.0 equiv. of $[Ph_3C][B(C_6F_5)_4]$, exhibited remarkable catalytic activities for 1-hexene polymerization $[2.03-36.2 \times 10^3 \text{ kg-polymer/mol-Sc} \cdot \text{h at } -30-21 \text{ °C}]$, and the activity increased at higher temperature. The resultant polymer prepared at -30 °C possessed highly isotactic structure (mmm = 90 %) with narrow molecular weight distribution ($M_w/M_n = 1.18$, $M_w = 7.50 \times 10^5$), suggesting a possibility of living polymerization [143]. In addition to promising results by half-metallocene type scandium complex in ethylene copolymerization (with styrene, cyclic olefins etc.) [144–147], these results suggest that the non-metallocene type scandium complexes



Scheme 3.17 Reported scandium dialkyl, trialkyl analogues [148–153]

would exhibit unique characteristics as the catalyst precursors for olefin polymerization.

Scandium complexes containing [6-amino-6-methyl-1,4-diazepine] ligand (45, Scheme 3.17) exhibited high activities for ethylene polymerization in the presence of [PhN(H)Me₂][B(C₆F₅)₄], affording polymer with unimodal molecular weight distribution [2660 kg-PE/mol-Sc·h, ethylene 5 bar, in toluene at 50 °C]: the activity increased at 70 °C (5800 kg-PE/mol-Sc·h) [148]. Although the dialkyl analogues containing monoanionic tridentate ligand, Sc(L)(CH₂SiMe₃)₂(THF) [L = 6-RN-1,4,6-trimethyl-1,4-diazepine] (R = Me, PhMe₂Si), exhibited negligible catalytic activities for ethylene polymerization in the presence of $[PhN(H)Me_2][B(C_6F_5)_4]$, the THF-free complex exhibited high activity under the same conditions [2920 kg-PE/mol-Sc·h, ethylene 5 bar, toluene, 50 °C, 10 min], affording high molecular weight polymer with uniform distribution ($M_{\rm w} = 1.2 \times$ 10^6 , $M_w/M_n = 1.9$ [149]. Removal of THF is thus found to be prerequisite for exhibiting remarkable activity. Ethylene polymerization using Sc complexes containing linked triazacyclononane(TACN)-amide ligands, [Me₂Si(Me₂TACN) (NR)]Sc(CH₂SiMe₃)₂ (**46**, R = ^{*t*}Bu, ^{*s*}Bu), were explored in the presence of borate cocatalysts [150]. These complexes exhibited high catalytic activities at 70 °C in the presence of $[Ph_3C][B(C_6F_5)_4]$ [activity = 2705 kg-PE/mol-Sc·h (R = ^tBu), 1810 kg-PE/mol-Sc·h ($R = {}^{s}Bu$): ethylene 5 bar, toluene, 10 min], affording

relatively high molecular weight polymers with uniform distributions. The activity in the presence of $[Ph_3C][B(C_6F_5)_4]$ was higher than that in the presence of $[PhN(H)Me_2][B(C_6F_5)_4]$, and the activity at 70 °C was higher than that conducted at 50 °C. The yttrium analogues exhibited further higher catalytic activities under the same conditions [150].

Trialkyl complexes containing four different neutral tridentate ligands (47, 48ac) were used as the catalyst precursors for polymerization of ethylene, 1-hexene in the presence of $[Ph_3C][B(C_6F_5)_4]$ in toluene (ethylene 6 bar, 33–36 °C, 10 min). Ring size of the tridentate ligand affected the activity for ethylene polymerization [activity = 60 kg-PE/mol-Sc·h (48b), 4380 kg-PE/mol-Sc·h (48c)], and replacement of NMe group with S (48a) was also effective (activity = 5160 kg-PE/mol-Sc \cdot h): the HC(Me₂pz)₃ analogue (47) also exhibited high catalytic activity (4980 kg-PE/mol-Sc·h). However, the resultant polymers possessed broad molecular weight distributions, although the 1-hexene polymerizations resulted in the polymers with uniform molecular weight distributions in most cases [151]. Taking into account these results, design of cationic Sc(III) alkyl complexes play an essential key role as the active species for olefin polymerization, and the ligand modifications which stabilize the oxidation state should be important for the efficient catalyst. Later, monoanionic bidentate or tridentate anilido-pyridine ligands (49, 50) were prepared and their catalyst performances for ethylene polymerizations were explored [152, 153].

3.2.3.2 Niobium and Tantalum Complexes

The Nb complexes 51 can be considered to contain either a neutral butadiene (C_4) ligand and a Nb(III) metal center or a dianionic butadienide (C_4^{2-}) ligand and a Nb(V) center (Scheme 3.18) [154]. The activity in ethylene polymerization by Cp*NbMe₂(butadiene) was 39 kg-PE/mol-Nb·h, affording high molecular weight polymer with narrow molecular weight distribution. PDI (M_w/M_p) values are very small (1.05) when these polymerizations were performed at low temperature $(-20 \ ^{\circ}C)$, suggesting the polymerization proceeds in a living manner. Halfmetallocene analogue, $Cp*Ta(=N^{t}Bu)Cl_{2}$, exhibited high catalytic activity for ethylene/1-octene copolymerization [40200 kg-polymer/mol-Ta-h: ethylene 500 psig (ca. 34 atm), 140 °C, 15 min] in the presence of Al imidazolide ([HNMe(C₁₈H₃₇)₂][(C₆F₅)₃AlNC₃H₃NAl(C₆F₅)₃]), affording the copolymer with uniform molecular weight distributions [155]. The activity was higher than that by the bis(amide) analogue (52, 6000 kg-polymer/mol-Ta·h) [155]. Niobium complexes containing tris(pyrazolyl)borate ligand (53) exhibited moderate catalytic activity for ethylene polymerization in the presence of $B(C_6F_5)_3$, and the activity was affected by the R substituent: the methyl analogue (R = Me) exhibited higher activity (130 kg-polymer/mol-Nb·h) than the H analogue. Treatment of the precatalyst with MAO does not result in any polymerization [156]. Bis(pyridyl-amido) niobium(V) (54) showed activity for ethylene polymerization upon addition of B(C_6F_5)₃, but the activity was low (4.4 kg-polymer/mol-Nb·h) and rapid



Scheme 3.18 Reported niobium and tantalum complexes for olefin polymerization [154–159]

decomposition of the catalytically active species was observed [157]. Analogous bis(pyridylamide) complexes (55, 56) showed very high activity, up to 23900 kg-PE/mol-Ta \cdot h (ethylene 5 bar, 80 °C), and rapid decrease in the activity was observed at low temperature [158].

More recently, four Ta complexes bearing tris(pyrazolyl)borate ligands (**57a–d**) were found to exhibit catalytic activities for ethylene polymerization. Activity in the presence of $Al^{i}Bu_{3}/[Ph_{3}C][B(C_{6}F_{5})_{4}]$ is higher than that in the presence of dried MAO; the sterically encumbered **57c**, **d** showed higher activities [activity: 77100 kg-PE/mol-Ta·h (**57c**) and 51300 kg-PE/mol-Ta·h (**57d**)], and some of the highest values reported to date for Ta-based catalysts [159].

3.3 Summary and Outlook

As described above, tremendous number of reports have been known for this project, and some of them are very important from both academic and industrial point of view [20–28]. It is clear that fine-tuning of the ligand plays a crucial role in this catalysis. Unfortunately, recent examples for chromium complex catalysts are not listed and these are also important on relevance of their ethylene trimerization catalysts [160]. Very successful examples such as highly isospecific polymerization of α -olefins, and living polymerization, so called chain shuttling polymerization have been demonstrated among recent advances in this research subject. These several promising findings that should be very important from both academic and industrial viewpoints have been demonstrated. These efforts will pave new promising possibilities for evolution of new *fine* polyolefins with unique properties by incorporation of new comonomers and/or by adopting new synthetic strategies. We highly expect more progress in this field in the near future.

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