

Chapter 6

Potential of Hydrogen Fermentative Pathways in Marine Thermophilic Bacteria: Dark Fermentation and Capnophilic Lactic Fermentation in *Thermotoga* and *Pseudothermotoga* Species



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1 Introduction

The steadily increasing use of renewable forms of energy is envisaged to mitigate climate risks, but effective reduction of the concentration of greenhouse gases entails carbon sequestration strategies and transition to fuels that are not carbon based. Hydrogen (H₂) is commonly considered a secure and environmentally safe alternative to traditional energy vectors based on fossil fuels. Utilization of hydrogen by combustion engine or fuel cell produces heat and electricity with pure water as only waste. Nevertheless, hydrogen production requires manufacturing by processes that are currently energy-consuming and polluting. The access to this hydrogen does not solve the environmental issue, and it is clear that only production of the energy vector from renewable sources can be sustainable in the long term.

Hydrogen gas is also the side product of metabolism of a few microorganisms through biological transformations that include photobiological water splitting and fermentation of biomass. The latter process, which comprises photo- and dark fermentation, is particularly interesting because it is entitled of high productivity and allows use of residual material such as agro-food waste. Hyperthermophilic and extremely thermophilic bacteria and archaea are promising candidates for the

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development of dark fermentation (DF)-based technologies because the rate and yield are higher than in mesophilic processes. In the last years, we reported that substitution of N_2 with CO_2 in the headspace of a standard culture of *Thermotoga neapolitana* DSMZ 4359 induces shift from DF to an unprecedented process that we named capnophilic lactic fermentation (CLF) after the mandatory presence of CO_2 and increase of lactic acid production [1, 2]. Differently from DF, CLF shows a so far unexplained deviation from the Thauer rule [3] with simultaneous synthesis in good yields of hydrogen and lactic acid [2, 4]. Very recently we noticed the acquisition of a novel phenotype and genotype of our lab strain of *T. neapolitana* that we have proposed as a new subspecies named *T. neapolitana* subsp. *capnolactica* with regard to the improved ability to produce lactic acid under capnophilic conditions [5].

T. neapolitana is a marine, organotroph eubacterium that ferments sugars to hydrogen under strictly anaerobic conditions. The microorganism belongs to the order *Thermotogales* that embraces a family of extremely thermophilic eubacteria that have been mostly isolated from marine geothermally heated environments across the globe, including shallow and deep-sea marine hydrothermal systems [6]. The order comprises the emended genus *Thermotoga* and the new genus *Pseudothermotoga* gen. nov. [7]. The aim of the present study is to give an overview of the previous research on *T. neapolitana* and to report unpublished results on the occurrence of CLF and DF in the other members of the *Thermotoga* and *Pseudothermotoga* genera maintained under standard (TnN_2) and capnophilic ($TnCO_2$) conditions.

2 Species and Culture Conditions

2.1 Taxonomy

Thermotogales (phylum *Thermotogae*, class *Thermotogae*) are anaerobic, Gram-negative, rod-shaped bacteria encapsulated by a unique “toga”-like outer membrane. These bacteria are strict organotrophs, fermenting preferentially simple and complex carbohydrates or complex organic matter. Genomic data from 17 members of the phylum support the division of the current genus *Thermotoga* in two evolutionary distinct taxonomic genera. On the basis of genome sequence data and genome-derived characteristics, Bhandari and Gupta [7] have proposed a reclassification of the genus *Thermotoga*. According to this work, the former genus *Thermotoga* should retain only the species *Thermotoga maritima*, *Thermotoga neapolitana*, *Thermotoga petrophila*, *Thermotoga naphthophila*, *Thermotoga* sp. EMP, *Thermotoga* sp. A7A, and *Thermotoga* sp. RQ2, while the other *Thermotoga* species (*Thermotoga lettingae*, *Thermotoga thermarum*, *Thermotoga elfii*, *Thermotoga subterranea*, and *Thermotoga hypogea*) are moved to a new genus, *Pseudothermotoga* gen. nov. [7]. According to molecular analysis [8], the recently reported *Thermotoga caldifontis* and *Thermotoga profunda* should be also included in the *Thermotoga* genus.

The genus *Thermotoga* embraces bacteria that have an optimal growth temperature in the range of 77–80 °C [7]. Together with members of the order *Aquificales*, these bacteria show the highest growth temperatures known so far. The genus *Pseudothermotoga* includes species that generally grow in the range of 65–70 °C. All members of the order produce hydrogen, but extent can change from one strain to another. The biogas is formed as final product and is released to protect the microorganisms [9].

2.2 Strain Origin

Thermotoga and *Pseudothermotoga* species have been isolated from geothermally heated environments across the globe, including continental solfataras springs of low salinity, shallow and deep-sea marine hydrothermal systems, and high-temperature marine and continental oil fields, and have been extensively studied for insights into the basis for life at elevated temperatures and for biotechnological opportunities (e.g., biohydrogen production, biocatalysis). Indeed the species *T. maritima* had been originally isolated from a geothermally heated, shallow marine sediment at Vulcano, Italy [10]. The second species of this genus, *T. neapolitana*, was obtained from a submarine hot spring at Lucrino near Naples, Italy [11, 12]. Members of the marine *T. maritima*-*T. neapolitana* group are widespread within high-temperature ecosystems, such as shallow submarine hydrothermal systems. The isolates from deep-subsurface petroleum reservoirs were *T. petrophila* and *T. naphthophila* isolated from the Kubiki oil reservoir production fluid in Niigata (Japan; [13]). *T. caldifontis* and *T. profunda* are the newest members of the family [8]. Both species were isolated from terrestrial hot springs in Japan. The optimum growth conditions for strain *T. profunda* were 60 °C at pH 7.4, and those for strain *T. caldifontis* were 70 °C at pH 7.4. Further *Pseudothermotoga* isolates from oil production wells were described as *P. elfii* [14], *Pseudothermotoga subterranea* (East Paris Basin; [15]), and *Pseudothermotoga hypogea* (Africa; [16]) and represent a third ecological group originating from subsurface ecosystems and adapted to levels of salinity intermediate between those of marine species and those of terrestrial species. *Pseudothermotoga thermarum* was isolated in 1989 from continental solfataric springs with low ionic strength in Lake Abbe, Djibouti [17]. Despite the terrestrial origin, the bacterium is able to grow at low levels of salinity. *Pseudothermotoga lettingae* was isolated from a sulfate-reducing bioreactor, where methanol was the only carbon source [18].

2.3 Culture Conditions

The following strains of *Thermotoga* and *Pseudothermotoga* genera used in this study *T. maritima* DSMZ 3109^T, *T. neapolitana* DSMZ 4359^T, *T. petrophila* DSMZ 13995^T, *T. naphthophila* DSMZ 13996^T, *T. caldifontis* DSMZ 23272^T, *T. profunda*

DSMZ 23275^T, *P. thermarum* DSMZ 5069^T, *P. elfii* DSMZ 9442^T, *P. subterranea* DSMZ 9912^T, *P. hypogea* DSMZ 11164^T, and *P. lettingae* DSMZ 14385^T were purchased from the Deutsche Sammlung von Mikroorganismen und Zellkulturen (Braunschweig, Germany). *T. neapolitana* subsp. *capnolactica* was originally bought as *T. neapolitana* DSMZ 4359^T and maintained in our laboratory under saturating concentrations of CO₂ for several years [5].

Except for *T. neapolitana* subsp. *capnolactica*, all the other strains were reactivated from lyophilized samples in *Tn* medium [19] supplemented with 28 mM (0.5% w/v) glucose and 0.4% (w/v) yeast extract/tryptone by using 120 mL sealed flasks with working volume of 30 mL, without agitation and with pH adjustment to optimal value for each bacterium by means of 1 M NaOH. Anaerobic cultures were grown at optimal temperature for each bacterium (60 °C for *T. profunda*; 70 °C for *T. caldifontis*, *P. subterranea*, *P. hypogea*, *P. lettingae*, *P. elfii*; 80 °C for *T. neapolitana*, *T. neapolitana* subsp. *capnolactica*, *T. maritima*, *T. naphthophila*, *T. petrophila*, and *P. thermarum*) under N₂ atmosphere. Fermentation test batches were inoculated (6% v/v) at room temperature with precultures grown overnight. Before each experiment, culture media were degasified by N₂ or CO₂ bubbling. Samples were regularly taken (1.5 mL every 24 h) from the cultures to monitor the main fermentation parameters including optical density at $\lambda = 540$ nm (O.D.), dry cell weight (mg mL⁻¹), glucose consumption, production of organic metabolites (acetic acid, lactic acid, alanine, valine, ethanol, 2,3-butanediol), hydrogen, and CO₂. After each sampling, hydrogen was removed by flushing into culture media pure nitrogen or carbon dioxide for 3 min, and pH was adjusted to optimal value for each bacterium by means of 1 M NaOH [1]. All the cultures were performed in triplicate.

3 Fermentative Hydrogen Production by *T. neapolitana*

Originally isolated from shallow submarine hot spring near Lucrino in the Bay of Naples in 1986 [11, 12], *T. neapolitana* is a Gram-negative bacterium that grows between 55 and 90 °C with an optimal growth temperature of 80 °C. An overview on *T. neapolitana* has been reported in [20]. The species is well-recognized producer of hydrogen from sugar fermentation. In the following paragraphs, we briefly summarize the production of hydrogen by the two main fermentation pathways, dark fermentation and capnophilic lactic fermentation, that are currently known to operate in this eubacterium and in its subspecies, *T. neapolitana* subsp. *capnolactica*.

3.1 Dark Fermentation (DF) by *T. neapolitana*

In analogy with the other members of the genus, *T. neapolitana* displays a wide metabolic ability to use a large variety of substrates, including sulfur compounds [14]. Conversion of glucose to pyruvate is only due to Embden-Meyerhof-Parnas

(EMP) glycolytic pathway, but it has been calculated that about 15% of hydrogen is due to fermentation of protein source [19]. According to the classical model of dark fermentation, glucose oxidation to acetate can theoretically produce 4 mol of hydrogen per mole of sugar [3]. As fermentative hydrogen production is a mean to dispose of electrons, there is a direct relationship between the biogas yield and the type of the organic products that are concurrently released during the process. As shown in Fig. 6.1, yield is optimized only when all glucose is converted to acetate, because there is no leak of electrons in other reactions. The entire pathway is thermodynamically driven by formation of ATP, but when hydrogen accumulates and consumption of NADH stops, pyruvate is diverted away from acetate production. In this case lactic acid or alanine is a common side product of the process [6]. According to the mechanism of Fig. 6.1, no hydrogen is produced when these metabolites are the only products of the fermentation.

Synthesis of lactate is under control of lactate dehydrogenase (LDH) and requires concomitant reoxidation of NADH to NAD⁺. Lactate levels reported during fermentation by *Thermotoga* species vary from trace amounts up to levels rivaling those of acetate [21–24]. On the other hand, the bacterium lacks the key genes necessary for further reduction of acetyl-CoA to ethanol and butyrate [25–27].

Evolution of hydrogen is an efficient way to dissipate excess reductant as a diffusible gas during microbial fermentation and photobiological processes. Synthesis of the gas by *T. neapolitana* is mostly due to the characteristics of the heterotrimeric [FeFe]-hydrogenase. Hydrogenases (H₂ase) constitute a family of metalloenzymes that reduce protons to hydrogen by low-potential electrons. These enzymes play a central role in energy metabolism of many bacteria and archaea but are also found in a few eukaryotes [28]. Hydrogenases are traditionally classified in

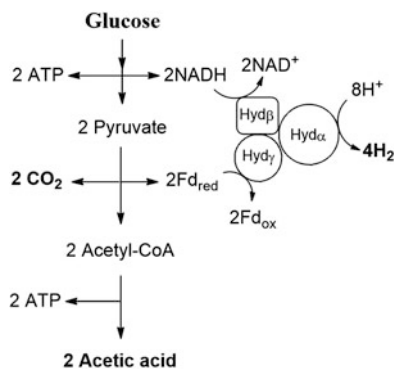


Fig. 6.1 Dark fermentation (DF) in *T. neapolitana*. The marine bacterium operates synthesis of hydrogen from sugar fermentation. Pyruvate is the key intermediate of the process and derives from Embden-Meyerhof-Parnas glycolytic pathway. Hydrogenase (Hyd) is represented by trimer composed of Hyd_α, Hyd_β, and Hyd_γ. The final organic product of dark fermentation is acetate even if other minor compounds are also released in the medium. The scheme illustrates the direct correlation between acetate synthesis and hydrogen production. The largest yield of hydrogen cannot exceed 4 mol/mol of glucose (Thauer limit) and can be achieved only when acetate is the product of the process (see main text). Fd_{red} = reduced ferredoxin; Fd_{ox} = oxidized ferredoxin. Protons and other side products and cofactors are omitted for simplicity

three groups according to the structure of the catalytic site: [FeFe]-hydrogenases, [NiFe]-hydrogenases, and [Fe]-hydrogenases [28–30]. Sequence analysis on the three proteins that form the hydrogenase of *T. maritima*, which has more than 90% homology with that of *T. neapolitana*, suggests a [FeFe]-heterotrimer. The α subunit (HydA) is a protein that contains the catalytic site, which is termed H cluster, composed of three 4Fe-4S and two 2Fe-2S clusters [23]. This is one of the most complex iron-containing structures characterized to date and requires the specific action of three highly conserved proteins to be assembled [31, 32]. Other three 4Fe-4S clusters and one 2Fe-2S cluster are also present in the β -subunit (HydB), whereas the hydrogenase γ -subunit (HydC) contains one 2Fe-2S cluster. According to the model suggested by Schut and Adams [23], HydA transfers electrons to H^+ from NADH through the β -subunit and from reduced ferredoxin through the γ -subunit. However, despite the detailed proposal of the active site, how the endergonic reaction of hydrogen production is accomplished under physiological conditions has been vague for a long time.

Reduction of H^+ is an energetically unfavorable reaction that is typically influenced by environmental conditions such as pH, cell growth rate, and hydrogen partial pressure. In 2008, a new mechanism of driving endergonic redox reactions was proposed for the synthesis of butyric acid from crotonyl-CoA in *Clostridium kluyveri* by simultaneous transfer of electrons from NADH ($E^{\circ} = -320$ mV) to ferredoxin ($E^{\circ} = -450$ mV) and crotonyl-CoA ($E^{\circ} = -10$ mV) [33]. The process is thermodynamically favored because the flux of electrons is “bifurcated” toward two acceptors with different redox potentials in order to conserve the total energy of the system [34]. Analogously, the hydrogenases of *T. maritima* and *T. neapolitana* are suggested to be electron-bifurcating enzymes that couple the endergonic reduction of H^+ to hydrogen by NADH with the exergonic reduction of H^+ to hydrogen by reduced ferredoxin [23]. The trimeric hydrogenase complex of these bacteria is not able to produce hydrogen with the oxidation of reduced Fd or of NADH when each was used as the sole electron donor. Only, the presence of both biological reductants promoted efficient hydrogen production with yield close to the Thauer limit. Because the hydrogenase of *T. neapolitana* uses both NADH and reduced ferredoxin as electron donors, hydrogen production may be influenced by factors that affect both reductants. Furthermore, the composite mechanism of this hydrogenase is consistent with the complexity of the trimeric structure, which is much greater than that of the typical Fd-dependent, single subunit [FeFe]-hydrogenase found in *Clostridium* spp.

3.2 *Capnophilic Lactic Fermentation (CLF) by T. neapolitana*

A continuous inflow of gases, mainly nitrogen (N_2), is the most commonly reported method for removing hydrogen from the reactor headspace and increasing productivity [35, 36]. Sparging pure cultures of *T. neapolitana* with CO_2 significantly

increases the rate of both glucose consumption and hydrogen production even if there is no improvement of the overall productivity and molar yield that remained substantially unchanged in comparison with standard N_2 conditions [1]. Paradoxically, CO_2 stimulated also synthesis of lactic acid. Feeding experiments with labeled precursors clearly proved that at least part of exogenous CO_2 was biologically coupled with acetyl-CoA to give lactic acid when the cultures were stripped by CO_2 gas or enriched in sodium bicarbonate. The process recycled both glycolysis-derived acetyl-CoA and exogenous acetate. In this latter case, the overall outcome was a conversion of equimolar concentration of acetate and CO_2 into lactic acid. The fermentative CO_2 -dependent synthesis of lactic acid and hydrogen was named capnophilic lactic fermentation (CLF), and as suggested in Fig. 6.2, it put forward the possibility to fully convert sugar to lactic acid (or other reduced derivatives of pyruvate) without affecting hydrogen synthesis by means of an additional consumption of reducing equivalents deriving from other cellular processes [2].

The transition from acetate production (dissimilation) to acetate utilization, also named acetate switch, is a common facet in the metabolism of many bacteria [37]. It is noteworthy that, according to acetyl-CoA synthetase (ACS) mechanism, acetate assimilation is an endergonic process that requires one mole of ATP and one mole of CoA per each mole of acetate that is imported and utilized in the bacterial cell. Assimilation of CO_2 in *T. neapolitana* is committed to synthesis of lactic acid and,

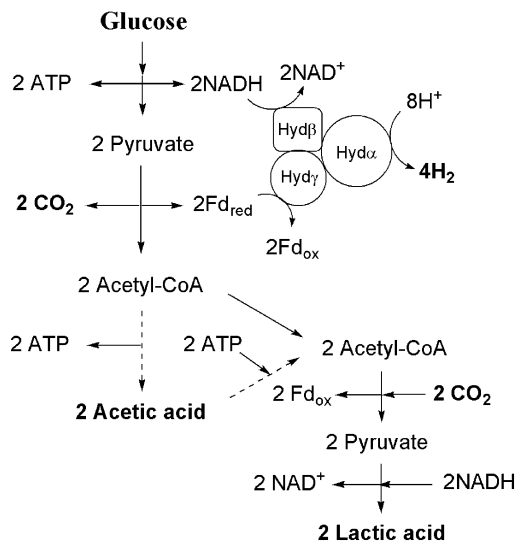


Fig. 6.2 Capnophilic lactic fermentation (CLF) in *T. neapolitana*. The process is an anaplerotic pathway that is activated by increase of the concentration of CO_2 in the reactor. As depicted in the scheme, acetyl-CoA deriving from sugar catabolism (see Fig. 6.1) undergoes to reductive carboxylation by reverse catalysis of pyruvate:ferredoxin oxidoreductase (PFOR). Newly generated pyruvate is then reduced to lactic acid by lactic dehydrogenase. The pathway is able also to use exogenous acetate. Hydrogen production is not affected by the capnophilic route, thus allowing simultaneous synthesis of lactic and hydrogen in deviation of the Thauer limit. Fd_{red} = reduced ferredoxin; Fd_{ox} = oxidized ferredoxin. Protons and other side products and cofactors are omitted for simplicity

like in acetogenic bacteria and methanogens [38, 39], is dependent on pyruvate:ferredoxin oxidoreductase (PFOR). The experiments established the presence of PFOR in strict occurrence with pyruvate synthase activity and production of lactic acid. Labelling of lactic acid during sugar fermentation unambiguously demonstrates that the catabolic and biosynthetic reactions can occur at the same time. However, pyruvate synthase levels were detectable for a longer time in cultures exposed to CO₂ thus suggesting that the two processes could be independently regulated by either glucose or CO₂. This is consistent with the apparent absence of cross talking between hydrogen production and capnophilic lactic fermentation under CO₂-enriched conditions [2].

In *Thermotogales* reductive carboxylation of acetyl-CoA (Ac-CoA) likely requires the pool of ferredoxin that is also involved in hydrogen production. The role of ferredoxin as efficient reductant in pyruvate synthesis has been demonstrated in vitro with *Clostridium thermoaceticum* [40] and suggested in vivo for methanogenic archaea, such as *Methanosarcina barkeri* [41]. It is noteworthy that the sequence of pyruvate oxido-reductase of this last organism has a good relation to those of *T. neapolitana* and *T. maritima* [2]. CLF is an example of biological sequestration of CO₂ by coupling with an exogenous substrate (acetate, glucose, etc.) and release of the end product (lactic acid) outside of the cell. Incorporation of radioactivity from ¹⁴C-glucose into cells proved that little of this carbon is used in primary metabolic pathways. Analogously, no carbon deriving from CO₂ or HCO₃⁻ is apparently fixed in the microbial biomass. This is not too surprising but makes a difference between CLF and mechanisms of fixation known in other anaerobes. In fact, unlike autotrophic [42, 43] and heterotrophic [44] pathways for CO₂ assimilation, the capnophilic metabolism of *T. neapolitana* implies complete excretion of CO₂ after “incorporation” in lactic acid and no synthesis of primary metabolites (e.g., proteins, sugars, or lipids). Recently, the first mathematical model of this process has been reported to describe the kinetics of the formation of lactate and hydrogen [4]. The model can effectively predict that about 90% of lactate was produced via the CLF pathway.

4 Anaerobic Sugar Fermentation in *Thermotoga* and *Pseudothermotoga* Genera

4.1 Bacterial Growth and Tolerance to CO₂

The lyophilized strains of *Thermotoga* and *Pseudothermotoga* genera were reactivated and grown on glucose in *Tn* medium enriched with yeast extract and tryptone [19]. Growth was measured as density at $\lambda = 540$ nm (O.D.) and also monitored as wet and dry cell weight. The choice to use the same medium for the

different species reflects our decision to make homogeneous the response. This condition is probably not optimal for every strain, and the resulting results do not indicate the best fermentation performance.

As reported in Fig. 6.3, the bacteria showed the common ability to growth on glucose under both N_2 (TnN_2 , standard DF) and CO_2 ($TnCO_2$, CLF) sparging. Stimulatory effect of CO_2 on the growth of obligate anaerobes is widely recognized [45] even if CO_2 is considered an inhibitor of biochemical processes, and, with this aim, the gas is used as a bactericide in food packaging and carbonated beverages.

Stripping with CO_2 significantly increases hydrogen yields in mixed cultures due to the removal of hydrogen [46]. A major complication with using CO_2 as stripping gas is the formation of bicarbonate accompanied by acidification of the medium and increased osmotic pressure. Acidification has been shown not to be necessarily the primary origin for growth inhibition by CO_2 since analogous reduction of the pH in N_2 atmospheres did not have the same inhibitory effect. However, higher solute concentrations can lead to growth inhibition and cell lysis. Bicarbonate and carbonate can also react with amino groups forming carbamates, which can affect the function of proteins. In addition, at low external pH, CO_2 can diffuse into the cell and lowers the intracellular pH by forming bicarbonate and thus reducing the growth rate. Finally, elevated partial CO_2 pressure might inhibit catabolism by reversing the biological decarboxylating reactions.

CO_2 atmosphere did not inhibit fermentation and growth of *Thermotoga* and *Pseudothermotoga* species despite previous studies report acidification of the medium and increase of the osmotic pressure [47]. This was not unexpected since other hyperthermophilic bacteria, e.g., *Pyrococcus furiosus*, can grow optimally in the presence of high salt concentrations for the ability to produce osmoprotectants, such as mannosylglycerate, di-myo-inositol phosphate, and glutamate [48].

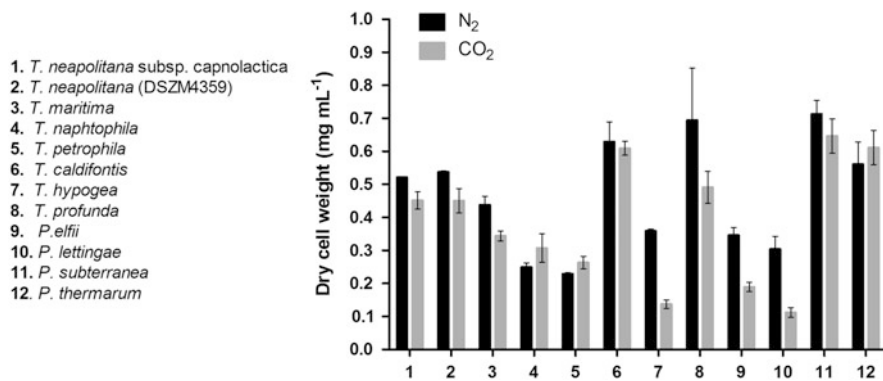


Fig. 6.3 Dry cell weight ($mg\ mL^{-1}$) comparisons in *Thermotoga* and *Pseudothermotoga* genera after glucose fermentation in *Tn* medium under N_2 or CO_2 atmosphere

4.2 Glucose Consumption and Hydrogen Yield Under N_2 and CO_2 Conditions

Response in *Thermotoga* and *Pseudothermotoga* species to CO_2 -enriched atmosphere was monitored by glucose consumption and production of hydrogen and organic metabolites (acetic acid, lactic acid, and alanine; valine, ethanol, and 2,3-butanediol) according to the methods described by Dipasquale et al. [1].

T. neapolitana subsp. *capnolactica*, *T. neapolitana* DSMZ 4359, *T. maritima*, *T. profunda*, *P. thermarum*, and *P. subterranea* showed the highest consumption rate of glucose and fermented almost completely the sugar under N_2 and CO_2 conditions (Table 6.1). Except for *T. maritima*, *P. hypogea*, and *P. lettingae*, use of CO_2 improved the efficiency of glucose consumption even if the effect was quantitatively different from one species to another. The most evident increase was recorded with *T. naphthophila*, *T. petrophila*, *T. caldifontis*, *T. profunda*, and *P. subterranea*, which are all species isolated from oil deposit or deep hot springs where presumably CO_2 concentration is higher than in other habitats [8, 13, 15]. All strains also produced hydrogen, but the molar yield (mol hydrogen/mol glucose) in these experimental conditions was significantly higher than 2 only with *T. neapolitana* subsp. *capnolactica*, *T. petrophila*, and *T. caldifontis* (Table 6.1).

Table 6.1 Glucose consumption and hydrogen yield (mean \pm standard deviation, $n = 3$) in *Thermotoga* and *Pseudothermotoga* genera after glucose fermentation in N_2 (TnN_2) or CO_2 ($TnCO_2$) atmosphere

Genus <i>Thermotoga</i>	Glucose consumption (mM)		Hydrogen yield (mol H_2 /mol consumed glucose)	
	TnN_2	$TnCO_2$	TnN_2	$TnCO_2$
<i>T. neapolitana</i> subsp. <i>capnolactica</i>	25.7 \pm 0.1	28.3 \pm 1.0	2.5 \pm 0.06	2.9 \pm 0.1
<i>T. neapolitana</i> DSMZ 4359	21.7 \pm 0.6	20.8 \pm 2.3	2.5 \pm 0.03	1.9 \pm 0.1
<i>T. maritima</i> DSMZ 3109	23.2 \pm 1.0	19.9 \pm 0.6	1.9 \pm 0.06	2.0 \pm 0.1
<i>T. naphthophila</i> DSMZ 13996	13.3 \pm 1.1	20.8 \pm 1.7	2.2 \pm 0.2	1.6 \pm 0.2
<i>T. petrophila</i> DSMZ 13995	9.2 \pm 1.3	14.2 \pm 0.6	3.0 \pm 0.4	1.9 \pm 0.1
<i>T. caldifontis</i> DSMZ 23272	10.9 \pm 1.1	15.2 \pm 0.9	2.6 \pm 0.1	1.8 \pm 0.03
<i>T. hypogea</i> DSMZ 11164	8.8 \pm 1.1	4.3 \pm 0.1	1.1 \pm 0.3	0.5 \pm 0.1
<i>T. profunda</i> DSMZ 23275	18.1 \pm 0.4	22.6 \pm 1.7	1.5 \pm 0.2	0.7 \pm 0.04
Genus <i>Pseudothermotoga</i>				
<i>P. elfii</i> DSMZ 9442	7.0 \pm 0.9	6.7 \pm 0.2	2.0 \pm 0.2	2.1 \pm 0.1
<i>P. lettingae</i> DSMZ 14385	9.3 \pm 0.5	8.1 \pm 0.7	1.2 \pm 0.1	1.3 \pm 0.3
<i>P. subterranea</i> DSMZ 9912	23.1 \pm 2.1	27.0 \pm 1.4	1.8 \pm 0.2	1.4 \pm 0.1
<i>P. thermarum</i> DSMZ 5069	Complete	Complete	1.8 \pm 0.02	1.5 \pm 0.1

Initial hexose concentration was 28 mM in 120 mL sealed flasks with working volume of 30 mL, incubated without agitation and with pH adjustment to optimal value for each bacterium by means of 1 M NaOH. Anaerobic cultures were grown at optimal temperature for each bacterium (60 °C for *T. profunda*; 70 °C for *T. caldifontis*, *P. subterranea*, *P. hypogea*, *P. lettingae*, *P. elfii*; 80 °C for *T. neapolitana*, *T. maritima*, *T. naphthophila*, *T. petrophila*, and *P. thermarum*)

Despite the increase of glucose consumption, almost all species lowered hydrogen production under $TnCO_2$ conditions, and only *T. maritima*, *P. elfii*, and *P. lettingae* showed substantially unvaried yield of the energy vector (Table 6.1). *T. neapolitana* subsp. *capnolactica* was the only species to increase H_2 yield moving from N_2 to CO_2 . In a few species, production of hydrogen did not reach 50% of the theoretical Thauer limit [3], but it is noteworthy that these experiments were not carried out under optimized culture conditions.

4.3 Organic Metabolite Production Under N_2 and CO_2 Conditions

1H -NMR analysis of the fermentation broths from TnN_2 and $TnCO_2$ experiments revealed that all the tested strains produced a mixture in which acetic acid, lactic acid, and alanine were the predominant and most recurring metabolites (Table 6.2). Despite our expectation on CLF metabolism, CO_2 atmosphere did not induce a generalized increase of lactic acid to the detriment of acetic acid. Only *P. subterranea* showed a significant change in the fermentation products, but this was mostly driven by synthesis of L-alanine. Production of this amino acid is a trait that *Thermotogales* share with members of the archaeal order Thermococcales. Therefore, it has been proposed that L-alanine production from sugar fermentation is a remnant of an ancestral metabolism that these microbes have inherited from their common ancestor [9]. The species *P. hypogea*, *P. elfii*, *P. lettingae*, and *P. subterranea* showed a significant increase of alanine production under CO_2 -enriched atmosphere (Table 6.2). This process was associated to reduction of hydrogen in *P. hypogea* as probably consequence of a shift of glucose fermentation from acetate to pyruvate and then alanine. The other three species maintained a constant level of hydrogen from N_2 to CO_2 , but we did not observe any reduction in acetate synthesis, thus suggesting that CLF does not operate in these bacteria. It is to note that the constant level of acetate in comparison with N_2 cultures suggests that synthesis of alanine is probably independent of DF. The investigation of the mechanism for the biosynthesis of alanine is behind the scope of this work, but the most plausible explanation is derivation of this amino acid from protein catabolism. Amino acids and peptides of the medium, such as the hydrolytes of yeast extract and tryptone, have been already shown to contribute to total hydrogen production and biomass formation in *T. neapolitana* [19, 49].

In addition to acetic acid, lactic acid, and alanine, *P. hypogea*, *P. elfii*, and *P. lettingae* produced valine, while the broth of the other strains contained also ethanol and 2,3-butanediol. *T. neapolitana* subsp. *capnolactica*, *T. neapolitana* DSMZ 4359, *T. profunda*, *P. subterranea*, and *P. thermarum* were the major producers of these products, whereas the highest valine level was found in *T. profunda*. However, increase of organic acid production under CO_2 conditions was found only in *T. naphthophila*, *T. caldifontis*, *P. elfii*, and *P. subterranea* (Table 6.3). A few species responded to CO_2 by reducing the fermentation process.

Table 6.2 Main organic metabolite productions (mean \pm standard deviation, $n = 3$) in *Thermotoga* and *Pseudothermotoga* genera after glucose fermentation in N_2 (TrN_2) or CO_2 ($TrCO_2$) atmosphere

Genus	Acetic acid (mM)		Lactic acid (mM)		Alanine (mM)	
	TrN_2	$TrCO_2$	TrN_2	$TrCO_2$	TrN_2	$TrCO_2$
Genus <i>Thermotoga</i>						
<i>T. neapolitana</i> subsp. <i>capnolactica</i>	27.3 \pm 0.8	22.1 \pm 0.9	8.6 \pm 0.2	11.3 \pm 0.1	2.5 \pm 0.2	3.0 \pm 0.3
<i>T. neapolitana</i> DSMZ 4359	30.2 \pm 0.4	20.8 \pm 0.1	2.2 \pm 0.02	1.2 \pm 0.06	1.9 \pm 0.3	2.4 \pm 0.3
<i>T. maritima</i> DSMZ 3109	25.5 \pm 0.5	18.3 \pm 0.3	5.3 \pm 0.8	1.6 \pm 0.2	2.4 \pm 0.06	2.3 \pm 0.3
<i>T. naphthophila</i> DSMZ 13996	15.7 \pm 0.1	19.2 \pm 0.1	1.4 \pm 0.06	5.0 \pm 0.02	0.8 \pm 0.1	1.8 \pm 0.05
<i>T. petrophila</i> DSMZ 13995	13.1 \pm 0.05	12.6 \pm 0.1	2.0 \pm 0.01	3.8 \pm 0.02	0	0.3 \pm 0.1
<i>T. caldifontis</i> DSMZ 23272	16.7 \pm 3.6	15.6 \pm 1.5	2.2 \pm 0.5	2.3 \pm 0.4	3.2 \pm 0.9	6.6 \pm 0.7
<i>T. hypogea</i> DSMZ 11164	6.4 \pm 0.1	3.1 \pm 0.2	0.1 \pm 0.004	0.1 \pm 0.004	2.9 \pm 0.1	3.4 \pm 0.3
<i>T. profunda</i> DSMZ 23275	15.9 \pm 0.4	5.6 \pm 0.2	5.7 \pm 0.1	2.3 \pm 0.04	1.4 \pm 0.06	2.6 \pm 0.3
Genus <i>Pseudothermotoga</i>						
<i>P. effii</i> DSMZ 9442	8.3 \pm 0.06	7.8 \pm 0.3	0.2 \pm 0.03	0.1 \pm 0.01	4.2 \pm 0.3	10.0 \pm 0.3
<i>P. lettingae</i> DSMZ 14385	5.1 \pm 0.05	4.4 \pm 0.1	0.2 \pm 0.003	0.05 \pm 0.01	2.7 \pm 0.05	3.7 \pm 0.2
<i>P. subterranea</i> DSMZ 9912	30.6 \pm 6.9	31.9 \pm 7.9	16.2 \pm 4.6	10.7 \pm 4.0	9.5 \pm 0.4	20.0 \pm 8.0
<i>P. thermanum</i> DSMZ 5069	30.0 \pm 2.2	24.8 \pm 0.7	6.5 \pm 0.2	5.6 \pm 0.6	1.1 \pm 0.07	2.2 \pm 0.2

Table 6.3 Total main organic metabolite productions (mean \pm standard deviation, $n = 3$) in *Thermotoga* and *Pseudothermotoga* genera after glucose fermentation in N_2 (TnN_2) or CO_2 ($TnCO_2$) atmosphere

Genus <i>Thermotoga</i>	Total acetic acid, lactic acid, and alanine productions (mM)	
	TnN_2	$TnCO_2$
<i>T. neapolitana</i> subsp. <i>capnolactica</i>	38.4 \pm 1.1	36.4 \pm 1.3
<i>T. neapolitana</i> DSMZ 4359	34.3 \pm 0.7	24.4 \pm 0.4
<i>T. maritima</i> DSMZ 3109	33.2 \pm 1.3	22.2 \pm 0.8
<i>T. naphthophila</i> DSMZ 13996	17.8 \pm 0.3	25.9 \pm 0.1
<i>T. petrophila</i> DSMZ 13995	19.0 \pm 0.2	16.7 \pm 0.2
<i>T. caldifontis</i> DSMZ 23272	22.1 \pm 5.1	24.4 \pm 2.7
<i>T. hypogea</i> DSMZ 11164	11.1 \pm 0.5	8.3 \pm 0.9
<i>T. profunda</i> DSMZ 23275	23.0 \pm 0.5	10.6 \pm 0.5
Genus <i>Pseudothermotoga</i>		
<i>P. elfii</i> DSMZ 9442	14.1 \pm 0.6	18.3 \pm 0.9
<i>P. lettingae</i> DSMZ 14385	8.0 \pm 0.1	8.2 \pm 0.3
<i>P. subterranea</i> DSMZ 9912	49.6 \pm 12.0	62.6 \pm 19.8
<i>P. thermarum</i> DSMZ 5069	37.7 \pm 2.5	32.6 \pm 1.5

Analysis of the single components made evident that in most species the acetic acid yields decreased under $TnCO_2$ condition in comparison with TnN_2 , but only in *T. neapolitana* subsp. *capnolactica*, *P. hypogea* and *T. naphthophila*, there was a positive effect on lactic acid. Oddly lactic acid production resulted to be lower under capnophilic conditions than TnN_2 in the cultures of *T. neapolitana* DSMZ 4359, *T. maritima*, *T. profunda*, *P. subterranea*, and *P. lettingae*. The ratio of lactic acid versus acetic acid (LA/AA) showed the highest values with *T. neapolitana* subsp. *capnolactica*, *T. naphthophila*, *T. petrophila*, *T. profunda*, and *T. hypogea* under capnophilic conditions (Fig. 6.4), whereas it remained unchanged or even slightly decreased in comparison with TnN_2 in the other strains.

Taking in consideration also glucose consumption and hydrogen yield, *T. neapolitana* subsp. *capnolactica*, *T. naphthophila* and, at a lesser extent, *T. petrophila* were the only species to give increase of LA/AA ratio with no or little detriment of hydrogen production. Apparently the original strain of *T. neapolitana* DSZM 4359 does not show the same performance. Our finding of *T. neapolitana* subsp. *capnolactica* is rather recent, but we cannot exclude that the mutation with the consequent increase of lactic acid production occurred earlier. Thus, in consideration of the present results, it is very likely that most of our previous reports [1, 4, 19, 50] were due to this new subspecies instead of the original DSZM 4359 strain.

According to the CLF model [1, 2], the key enzymatic step of the pathway is the reductive addition of CO_2 to acetyl-CoA catalyzed by an enzyme of the PFOR family. Sequence analysis of the four proteins that compose PFOR showed a very high identity in the three species of *Thermotoga* genus (Table 6.4). This was in agreement with the results in production of lactic acid in these species under CO_2 and indirectly supported the assumption about the role of this enzyme in the regulation of the CLF pathway.

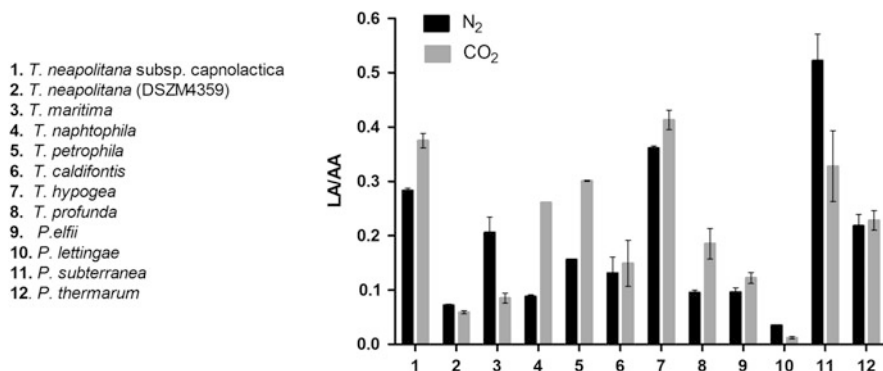


Fig. 6.4 Comparison between LA/AA ratio in *Thermotoga* and *Pseudothermotoga* genera after glucose fermentation in *Tn* medium under N₂ (*Tn*N₂) or CO₂ (*Tn*CO₂) conditions

Table 6.4 Identity (%) obtained by National Center for Biotechnology Information (NCBI)-BLAST between amino acidic sequences of *T. neapolitana* porA, porB, porC, and porD and those from *T. naphthophila* and *T. petrophila*

	Identity (%)	
	<i>T. naphthophila</i>	<i>T. petrophila</i>
<i>T. neapolitana</i>		
porA	97	97
porB	98	98
porC	96	93
porD	97	97

5 Challenges

Dark fermentation can achieve a maximum H₂ conversion of 33%, i.e., four molecules of H₂ per molecule of glucose. Based on thermodynamics, the process with mesophilic fermentation requires almost double the amount of feedstock compared to operation with thermophilic bacteria to produce the same amount of hydrogen. In general, only extreme thermophilic bacteria and archaea are able to use most of the reducing equivalents formed during glycolysis for the production of hydrogen, thus approaching the theoretical maximum of 4 mol H₂ per mol of hexose [3]. Recently, we reported that a combined process based on *T. neapolitana* under CLF conditions and *Rhodospseudomonas palustris* 42OL produces 9.4 ± 1.3 mol H₂ per mol of glucose [50], which is the highest value reported so far by combining dark and photofermentation.

In addition to the thermodynamic factor, other important aspects do favor the fermentation yields in thermophilic cultures [51]. In particular, due to higher hydrolysis activity, better pathogenic destruction, and less risk of biological contamination, extreme thermophilic fermentation seems also attractive for complex feedstock, such as lignocellulosic residues or agricultural and food residues. However, development of these processes at industrial level is so far hampered by inherent drawbacks, such inoculum production, low cell density, and tolerance.

Capnophilic lactic fermentation (CLF), as previously reported in *T. neapolitana* subsp. *capnolactica* and here described in *T. naphthophila* and, at a lesser extent, *T. petrophila*, may become the cornerstone for economically attractive biotechnological production of lactic acid from carbohydrate-rich feedstocks such as agro-food waste. However, this process needs optimization of upstream and downstream processes including the use and treatment of different substrates, the definition of the operational parameters, the reactor design, and the separation of the fermentation products. CLF process can be more economically sustainable if the reactors can handle with high organic loading rate (OLR) and with a short hydraulic retention time (HRT). These issues can be targeted either by using immobilized biomass or by applying other bioreactor configurations such as packed bed reactor (PBR) or fluidized bed reactor (FBR).

Hydrogen yield approaching the theoretical maximum value (i.e., Thauer limit) of 4 mol hydrogen/mol glucose can be achieved only if the flux electrons produced by glucose oxidation are directed to reduce protons (Fig. 6.1). Nevertheless, in practice, these reducing equivalents are also used for biosynthetic purposes and the formation of other fermentation products, i.e., lactate. Manipulation of the redox balance has been demonstrated to push the metabolism of mesophilic bacteria toward formation of organic acids. Evidence is that ferredoxin-NADH knob plays an important role for lactic production under CLF condition. Therefore, targeting the redox balance of *Thermotoga* and *Pseudothermotoga* species might constitute a promising metabolic strategy to improve the fermentation yields.

CLF pathway represents a first example of biological sequestration of CO₂ by coupling with an exogenous substrate (acetate, glucose, etc.) and release of the end product (lactic acid) outside of the cell. Since *T. neapolitana* does not convert CO₂ to the reduced organic compounds required for cell metabolism, the above mechanism is not related to the autotrophic fixation known in other anaerobes. The process appears to be unprecedented, but its regulation is largely unknown to date. However, the pathway offers the possibility to convert directly CO₂ into chemicals, which could become an economically feasible option after further improvement. Recently this approach has been explored for production and secretion of isobutyraldehyde and isobutanol directly from CO₂ by the genetically modified cyanobacterium *Synechococcus elongatus* [52]. The application of CLF and *Thermotoga* and *Pseudothermotoga* species in biotechnological processes will depend on the full elucidation of the molecular and biochemical characteristics of the process, as well as on selection and engineering of the productive species.

Finally, production of lactate independent of hydrogen suggests that CLF may trigger or be related to metabolic pathways other than glycolysis. One of the possibilities is the contribution of peptides and the effects of sparged CO₂ on peptide catabolism. Accurate redox and carbon balances are necessary to provide convincing data about the role of peptide in the lactate synthesis from acetate. Fermentation of *Thermotoga* and *Pseudothermotoga* strains is a challenging system in this regard, due to the dependence on peptides in the medium that makes it difficult to determine just how much acetate, hydrogen, or lactate is made as part of peptide versus glucose metabolism. New culture conditions must be designed to allow these measurements and to perform studies committed to estimate the energy and stoichiometry of the fully coupled reactions.

6 Conclusions

Thermotoga and *Pseudothermotoga* genera embrace a small but heterogeneous group of thermophilic and hyperthermophilic bacteria. To date the scientific and biotechnological attention for these microorganisms has been driven by the capability to produce hydrogen and, at lower extent, to the possibility to clean sites contaminated with petrochemicals and industrial wastes. The recent discovery of taxonomically related mesophilic members (*Mesotoga prima* and *Mesotoga infera*) [53, 54] and the finding of an apparently unprecedented pathway for synthesis of lactic acid from acetate and CO₂ clearly opened the use of these organisms in other biotechnological sectors. In particular, after further improvement, the fermentative transformation of agro-food residues combined with hydrogen production seems to be suitable to design a platform for the valorization of waste and CO₂, with recovery of both energy and value-added products. As outlined in this study, only a few members of the two genera show the capability to perform capnophilic lactic fermentation. However, all the species produce energy carriers and fuels, such as hydrogen and ethanol, and chemicals like acetic acid, butyric acid, and lactic acid, among others. In this context, these microorganisms appear as an attractive solution that will reduce those residues and increase the global efficiency of biomass-based production of energy and valuable chemicals, interlinked in a biorefinery concept.

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