

Chapter 5

Composite Membranes Based on Heteropolyacids and Their Applications in Fuel Cells

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Abstract Heteropolyacids (HPAs) are a class of inorganic materials that have been widely used as additives to enhance the performance of fuel cell membranes, recently. This chapter covers the use of HPAs in the preparation of proton exchange membranes (PEM) for polymer electrolyte membrane fuel cells (PEMFCs). The fundamental aspects of HPAs and their corresponding salts in addition to various structural configurations such as Keggin, Wells–Dawson, and Lacunar are discussed. The use of HPAs for preparation of membranes for high-temperature PEMFC and direct methanol fuel cell (DMFC) based on the immobilization on various substrates including perfluorinated sulfonic acids (PFSA)s, aromatic hydrocarbons, poly(vinyl alcohol) (PVA), and polybenzimidazole (PBI) are reviewed. The research challenges that need to be addressed to bring the new composite membranes to practical application are also discussed.

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List of abbreviations

CS-HEC	Chitosan-hydroxy ethyl cellulose
CsPW	Cs hydrogen salts of phosphotungstic acid
HPA	Heteropolyacid
LbL	Layer by layer
mGO	Graphene oxide modified with 3-aminopropyl-triethoxysilane
MMT	K10 montmorillonite
MO	Metal oxide
MOR	Methanol oxidation reaction
ORR	Oxygen reduction reaction
PBI	Polybenzimidazole
PDDA	Poly(diallyl dimethyl ammonium chloride)
PEFC	Polymer electrolyte fuel cell
PEMFC	Polymer electrolyte fuel cell
PFSA	Perfluorosulfonic acid
PMA	Molybdophosphoric acid or phosphomolybdic acid, $H_3PMo_{12}O_{40}$
POM	Polyoxometalate
Ppy	Polypyrrole
PVA	Poly(vinyl alcohol)
PWA	Phosphotungstic acid, $H_3PW_{12}O_{40}$
QDPSU	Quaternary diazabicyclo-octane polysulfone
rGO	Reduced graphene oxide
SiMA	Silicomolybdic acid, $H_4SiMo_{12}O_{40}$
SiWA	Silicotungstic acid $H_4SiW_{12}O_{40}$
SPAEK	Sulfonated poly(aryl ether ketone)
SPBN	Sulfonated polynorbornene
SPEEK	Sulfonated poly(ether ether ketone)s
SPS	Sulfonated polystyrene
ZrP	Zirconium phosphate

1 Introduction

The interest in developing highly stable and cost-effective new proton exchange membranes for polymer electrolyte fuel cells (PEMFCs) has been ever growing to promote the commercialization for this type of fuel cell [1–12]. This is to overcome the limitation of perfluorosulfonic acid (PFSA) membranes, which rely on water in proton conduction that prevent the operation of PEMFCs above 80 °C [13–15]. Higher fuel cell operation is desired to enhance reaction kinetics of electrochemical

reactions, increase CO tolerance of electrodes and reduce or eliminate water management system [16–18].

Various approaches have been used to develop alternative membranes including modification of commercially available PFSA membranes, chemical synthesis of sulfonate hydrocarbon membranes, and formation of composite membranes [19]. Particularly, composite ionic membranes composed of organic–inorganic components have received great attention in the past decade because of their ability to be operated under wide ranges of temperatures including much higher ones than membranes made of the pure polymers [20]. Moreover, the incorporation of inorganic fillers provides a number of advantages ranging from improvement in the mechanical properties and water management of the membrane to inhibition of the fuel crossover by increasing the tortuosity of transport pathways. These composite membranes can be formed by: (1) introducing nanosized hygroscopic inorganic fillers such as SiO_2 , ZrO_2 , and TiO_2 , (2) doping of basic substrates with nonvolatile proton conducting solvents such as phosphoric acid, N-heterocycles, heteropolyacids (HPAs), and ionic liquids, and (3) incorporation of solid proton conductors such as phosphate salts of zirconium (ZrP) and HPAs. Various synthesis routes can be used to introduce one phase into the other one. A review on various methods of introducing each phase in organic/inorganic composite membrane is available [21].

Among composite membranes, those doped with or containing solid proton conductors such as HPAs are promising candidates for PEMFC [22, 23, 21]. This is because HPAs display the highest proton conductivity among inorganic solids near ambient temperatures. They also have distinct discrete ionic structures including heteropoly anions and counter cations (e.g., H^+ , H_3O^+ , and H_5O_2^+) and therefore exhibit high-proton mobility. Moreover, the presence of bounded water molecule in HPAs makes them interesting for the development of moderate temperature PEMFC since proton conduction is independent of external humidification [2, 23].

The objective of this chapter is to review the progress of developments in regard to composite ionic membranes based on HPAs. A special attention is given to the types and structures of HPAs and their use in synthesis of nanocomposite polymeric materials with ion conducting functional groups for various types of PEMFC applications. The challenges remaining for further research to achieve important breakthroughs are also discussed.

2 Heteropolyacids Types and Structures

Polyoxometalates (POMs) are group of chemicals that have attracted an increasing attention due to the diversity and selectivity of their properties making them suitable for wide number of applications [24]. HPAs are complex proton acids incorporating polyoxometalate anions (heteropolyanions) having metal-oxygen octahedral as basic structural units [25, 26]. Keggin and Wells–Dawson are two important

categories of the HPAs. In 1933, Keggin used X-ray diffraction technique to determinate the $\text{H}_3[\text{PW}_{12}\text{O}_{40}]\cdot 5\text{H}_2\text{O}$ structure and provided a clear description of the bonds between the WO_6 octahedra of the molecule [27]. The Wells–Dawson structure was theoretically described by Wells in 1945 and experimentally confirmed in 1953 [28].

HPAs are subsets of metal oxides distinguished by central heteroatoms, which are surrounded by a number of metal-oxygen octahedra. There are strong bonds between the atoms supporting the polyhedra structures and connect them with the heteroatoms. The metal in HPAs is usually tungsten or molybdenum and less usually vanadium or uranium. The heteropoly anions having metal-oxygen octahedral as the basic structural units make up the primary structure of the HPA as shown in the Keggin anion (Fig. 1).

The Keggin HPAs, which is the most studied, represented by the formula $\text{X}^{x+}\text{M}_{12}\text{O}_{40}^{x-8}$, contain 12 addenda atoms and one heteroatom, where X is the heteroatom (central atom, commonly P^{5+} , Si^{4+} , or B^{3+}), x is its oxidation state, and M is the addenda atom (metal ion, commonly W and Mo). It is composed of a central tetrahedron (XO_4), which is surrounded by 12 edge- and corner-sharing metal oxide octahedra (MO_6). The octahedra are arranged in four M_3O_{13} groups, and each group has three octahedra sharing edges. They are linked through strong oxygen bonds, which also connect the central tetrahedron [29]. A typical FTIR-ATR spectrum of Keggin-type phosphotungstic acid (PWA) showing four different W-O bonds and characteristic bands at 1080 (P-O_a), 983 (W=O_d), 893 ($\text{W-O}_b\text{-W}$), and 797 ($\text{W-O}_c\text{-W}$) cm^{-1} is shown in Fig. 2.

Due to the complexity, other polyoxometalates including Wells–Dawson heteropolyanions $\text{X}_2^{x+}\text{M}_{18}\text{O}_{62}^{2x-16}$, Keggin and Dawson lacunary anions,

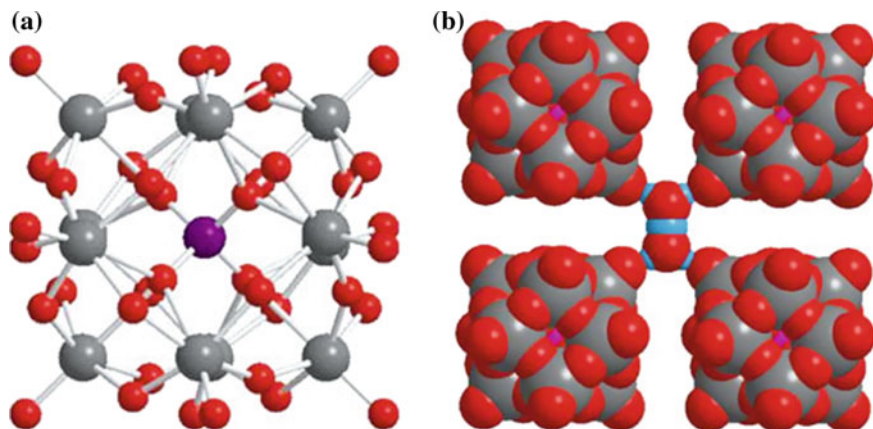


Fig. 1 HPA structures: **a** ball and stick model of the silicotungstic Keggin anion ($\text{SiW}_{12}\text{O}_{40-4}$) and **b** space filling model of the secondary crystalline structure of Keggin HPA with base-centered cubic arranged cavities containing H_5O_2^+ cations (red O, gray W, blue H, purple P, or Si)

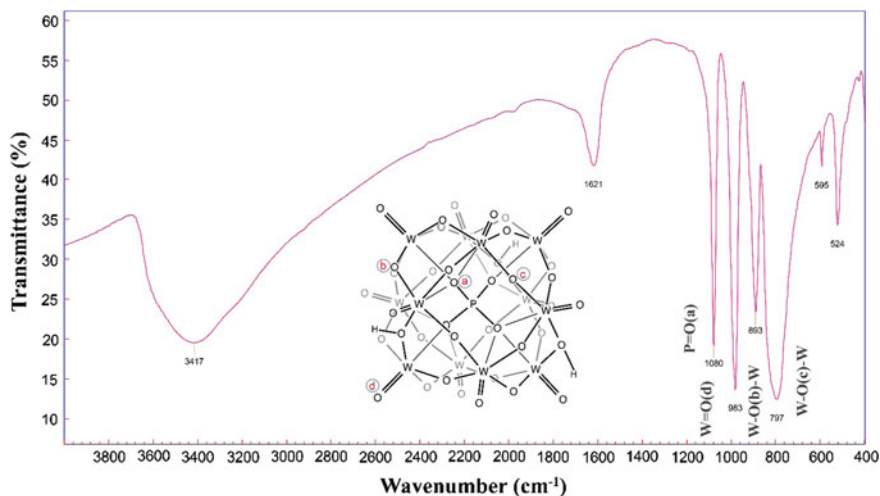


Fig. 2 FTIR-ATR spectrum of Keggin-type PWA showing four characteristic bands

$\text{XM}_{11}\text{O}_{39}^{x-12}$ and $\text{X}_2\text{M}_{17}\text{O}_{61}^{2x-20}$, and transition metal complexes have not been fully examined.

In addition to metals, HPAs are interestingly having multiple active sites in their structure including protons and oxygens. Functionally, protons act as Brønsted acids to promote acid-catalyzed process including proton transports. Besides, some oxygen atoms on the surface of HPA (especially oxygens located on the lacunary sites of lacunary POM anions with a high negative charge) are basic enough to react with protons and hydronium ions (protonate) and can practically behave as active sites in base-catalyzed reactions. On the other hand, the metals of HPAs are active sites in all oxidative reactions. The details of various catalytic activities of HPAs were reviewed [30–32].

Although Dawson HPAs were used in various applications including proton transport materials [33], majority of the patents and investigations are based on the applications of the Keggin-type HPAs and their salts. This primarily includes $\text{H}_3\text{PMo}_{12}\text{O}_{40}$ (PMA), $\text{H}_3\text{PW}_{12}\text{O}_{40}$ (PWA), $\text{H}_4\text{SiMo}_{12}\text{O}_{40}$ (SiMA), and $\text{H}_4\text{SiW}_{12}\text{O}_{40}$ (SiWA). Solid HPAs commonly form ionic crystals composing of anions (which is heteropolyanions), cationic counterions (H^+ , H_3O^+ , H_5O_2^+ , etc.), and hydration water. The HPAs are noticeably crystallizing with a large number of water molecules as in PWA and PMA, both of which have 29 water molecules compared to 30 for SiWA [34, 35]. The status of water is important for assessing HPA role as a proton transfer material. Some HPAs loss water very easily even at room temperature where as others can retain water tightly even at high temperature.

In HPA crystals, the Keggin anions are quite mobile. Due to structural flexibility and mobility of HPAs, not only water but also a diversity of polar molecules can enter and leave HPA crystals that is important when using HPAs in fuel cell applications. It should be noted that proton conductivity of solids is generally

related to their acid-based catalytic activities [36]. HPAs display strong acidity, good solubility in polar solvents such as water, lower alcohols, ketones, ethers and esters, in addition to good thermal stability and reversible redox behavior. One of the most important properties of HPAs is the ability to be chemically adjusted or tuned by simple modification of their structures. The acidity of the HPAs is dependent upon the total charge of the anion and the heteroatom in their structure [37–39]. The strong acidity level means fast proton mobility, which results in a high catalytic activity [29]. The acidity strength of crystalline HPAs decreases in the series $PW > SiW \geq PMo > SiMo$, which is identical to that in solutions [40].

Due to their versatile properties, HPAs have been used in an extensive range of applications, including chemical analysis, biochemistry, ion selective membranes, sensors, and electrochemical energy devices [41, 42]. Particularly, HPAs have been useful constituent of polymer electrolyte fuel cells (PEFCs) and their corresponding fuel cells using liquid fuels such as methanol or ethanol. Intensive work has been reported on membranes incorporating HPAs for fuel cells, specifically, saturated HPAs and unsaturated (defective) or lacunary HPAs were evaluated for fuel cell applications [43]. Figure 3 compares the structure of saturated HPA of $[SiW_{12}O_{40}]^{4-}$ in a hydrated form of $H_4[SiW_{12}O_{40}]22H_2O$, which is also known as 12-HSiW and one of the corresponding lacunary structures $[SiW_{11}O_{39}]^{8-}$ in a hydrated form of $H_8[SiW_{11}O_{39}]26H_2O$ known as 11-HSiW. As shown, the number of acidic hydrogens and water molecules is higher in lacunary HPAs. Interestingly, lacunary HPAs can be simply prepared by hydrolysis of the parent HPAs with a base under controlled conditions of temperature and ionic strength. Removal of one, two, or three metal oxide (MO) units from the parent HPAs results in a mono-, di-, or tri-lacunary POMs. A general reaction scheme for the preparation of various lacunary HPAs is shown Fig. 4.

Lacunary HPAs could be further modified by bonding with functional silanes that can subsequently crosslinked or polymerized to achieve more stable HPAs.

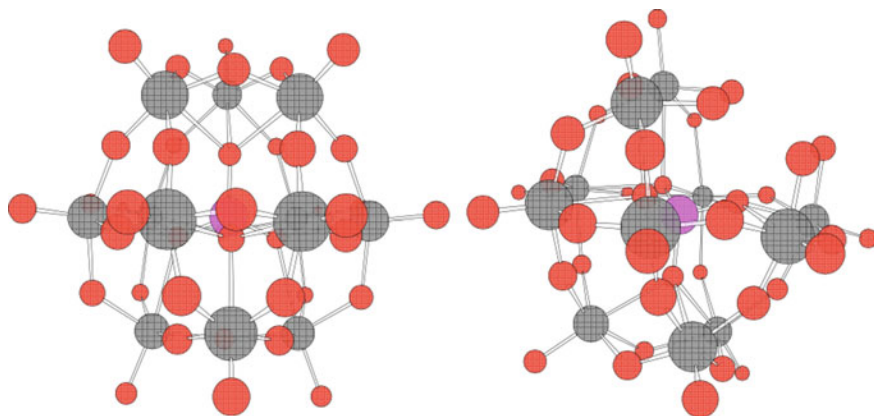
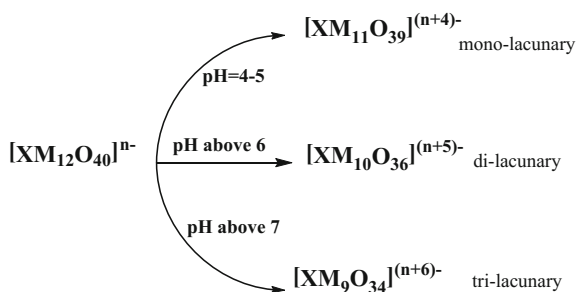


Fig. 3 Comparison of HPA and corresponding mono-lacunary structures

Fig. 4 General pathways for preparation of various lacunary HPAs



Such HPAs offer high ionic conductivities prompting their use in fuel cells. For example, indium-substituted HPAs with Keggin $H_4[In(H_2O)PW_{11}O_{39}]11H_2O$ and $H_5[In(H_2O)SiW_{11}O_{39}]8H_2O$, structures were reported to be solid high-proton conductors with a conductivity of $2.60 \times 10^{-4} \text{ S cm}^{-1}$ and $5.25 \times 10^{-4} \text{ S cm}^{-1}$ (at 18°C and 80% relative humidity), respectively. The conductivity of these materials also increased with the rise of the temperature [44].

The conductivity performance of HPAs varies widely depending upon the type of the HPAs' structure. Particularly, the change in the constitutional elements of polyanion can lead to the difference in the degree of hydration and proton mobility [45]. Typically, $H_5[SiW_{11}VO_{40}]15H_2O$ shows an excellent conductivity of $7.93 \times 10^{-3} \text{ S cm}^{-1}$ at 15°C and 50% RH [38]. In addition, the size of the HPAs influences considerably their performances specially when they are incorporated in the composite membranes [46].

Generally, HPAs have high thermal stability, in the order of $PW > SiW > PMo > SiMo$ (Keggin types) that decompose at 465, 445, 375, and 350°C , respectively. On the other hand, the influence of the heteroatom on the thermal stability is negligible [47]. The redox activity of HPAs promotes their application as redox bi-functional catalysts. With increasing electronegativity of the addenda atom, the reduction potential of the HPA decreases, while increases as the electronegativity of the counter cations or the heteroatoms increases, but it decreases as the electronegativity of the addenda atom increases [28]. The oxidation potential decreases in the Keggin structures as $PMo > SiMo \gg PW > SiW$.

HPAs have been used in an extensive range of applications, including chemical analysis, biochemistry, ion selective membranes, sensors, and electrochemical energy devices [41, 42]. Most generally, they are used as inorganic catalysts. Depending on their composition, HPAs can be effective catalysts for both acid catalysis and redox catalysis [47]. One of the important specific characteristics of the HPAs is that they can be tuned by adding different elements to their structures, allowing for the design of HPAs for special reactions. The high selectivity, thermal stability as well as hydrolytic stability, long lifetimes in solution, high oxidation potential, and noncorrosive nature of many HPAs make them economically and environmentally attractive as a natural 'green catalysts' [48]. In addition, the list of proteins or enzymes that can interact with HPA is long which supports the use of HPAs in a number of biochemical and biomedical applications [49]. Moreover, due

to antiviral and antitumor activity of HPAs, these find use in biomedicine applications [50, 51].

The appealing applications of HPAs as dopants and fillers in ionic composite membranes are indicated by the large number of patents and publications appeared recently [2, 52, 53, 37, 54, 55, 56]. This was motivated by their high ionic conductivity, thermal stability, very strong Brønsted acidity approaching the superacid region (more acidic than sulfuric acid and Nafion), and their capability to undergo redox processes under the mild conditions. Such membranes also found uses in ion selective electrodes, gas detection apparatuses, solid-state electrochromic devices, and solid or liquid electrolytes in electrolytic cells [57, 58, 59, 31, 32]. A great deal of work has been focused on the self-immobilization of POMs especially the Keggin type into the polymers matrices such as polypyrrole, polythiophene, and polyaniline to increase the performance of hybrid membranes.

3 HPAs and Proton Transport in Fuel Cells

Due to the dissociated protons combined with the anions having good mobility, HPAs are excellent proton conductors and promising solid electrolytes. The interest in HPAs began after reporting remarkably high conductivities of $2 \times 10^{-1} \text{ S cm}^{-1}$ at 25 °C, and low activation energies of 15.5 and 13.7 kJ/mol for crystals of $\text{H}_3[\text{Mo}_{12}\text{PO}_{40}]29\text{H}_2\text{O}$ and $\text{H}_3[\text{W}_{12}\text{PO}_{40}]29\text{H}_2\text{O}$ [60], respectively. However, upon application for fuel cell, keeping the samples in their fully hydrated form without decomposition is difficult since HPAs dissolve in the water that formed in a fuel cell during the operation [61]. Highly concentrated aqueous solution of HPA was reported for the use as a fuel cell electrolyte, which resulted in a comparable performance with PEMFC [62, 63]. Although stable cell performance for HPA electrolyte was reported for 300 h, however, the high crossover results in voltage loss of fuel cell.

HPAs with high stability in water have been obtained upon immobilization on clay [64], aluminum phosphate [53], and silica supports [65]. It was reported that the addition of aluminum phosphate in SPEEK/PWA remarkably increased water retention and effectively reduced leaching of PWA from the composite membrane [53]. On the other hand, the proton conductivity of mesoporous silica is as low as 10^{-6} – $10^{-4} \text{ S cm}^{-1}$. However, its remarkable structural order, large surface area and pore volumes, availability and simple functionalization make it an ideal porous framework for HPA based proton conductors [47, 66, 67].

Typically, an inorganic glass composite membrane containing a mixture of PWA and PMAPWA/PMA– P_2O_5 – SiO_2 resulted in very highly conductivity values of 1.014 S cm^{-1} at 30 °C and 85% RH [68] and $1.01 \times 10^{-1} \text{ S cm}^{-1}$ at 85 °C under 85% RH for a mesoporous-structured PWA– P_2O_5 – SiO_2 glass [69]. The fuel cell performance of these inorganic materials was 35–42 mW cm^{-2} in H_2/O_2 at 30% RH and 30 °C [68, 69]. However, they cannot be used as electrolytes in fuel cells in

their powdered form. Therefore, composite membranes with a polymer binder have been developed for fuel cell application.

Several approaches to incorporate HPA into fuel cell membranes include fabricating unsupported HPA pellets [61], doping polymer electrolytes [70], and sol-gel methods [71]. Among these, HPAs have been mainly used as dopants in composite proton exchange membranes. It was suggested that specific interactions between HPAs and polymers could have a significant influence on the fuel cell performance at elevated temperatures and thus they have received considerable attention [71]. More details of various preparation methods can be found elsewhere [72–75]. Five different procedures were commonly used to produce such composite membranes as schematized in Fig. 5. They include mixing of HPA with a polymer in a solution form followed by casting [76, 77] or impregnation of HPA in a porous substrate [78, 70]. HPAs were supported on various substrates including silica. When preparing the membrane from a polymer solution, the incorporation of HPAs supported on silica within a polymeric membrane can be achieved by two different ways: (i) pre-formation of HPA–silica particles followed by direct mixing with a polymer solution [65, 79] and (ii) in situ preparation of the inorganic phase within the matrix during film formation, e.g., via the sol-gel process of an alkoxide precursor in the presence of PWA [80–82]. Particle size and distribution heterogeneity are two main concerns when using the first method. However, the sol-gel method is normally lead to better distribution, more stability and possible control for the size

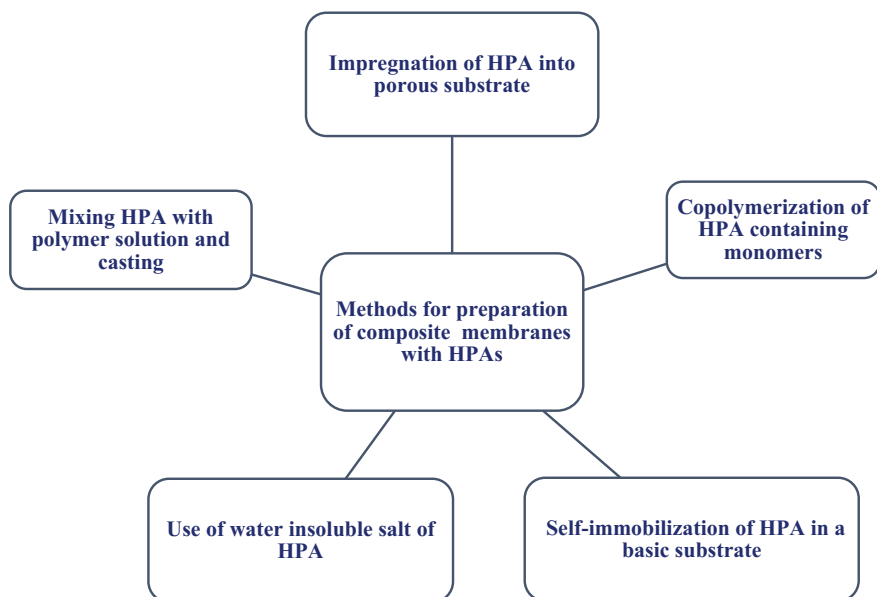


Fig. 5 Various methods for preparation of composite proton exchange membranes containing HPAs

of the particles by variation of the preparation parameters such as pH, temperature, and concentration of starting components [83, 84].

HPA supported on the polymers and porous fillers are likely subjected to leaching out of HPA during the fuel cell operation, despite the improvement took place in other properties including proton conductivities [85]. Such limitation is due to low loading level, loose interaction with solid organic substrate and possible agglomeration leading to the formation of large particles or clusters in the polymer substrate during the casting process [86, 87]. To overcome this problem, a third effective method involving copolymerization of HPA containing monomers or covalent bonding of HPA to a polymer backbone was proposed [87, 88, 89, 43]. The covalent bonding of dopant to the polymer backbone minimizes leaching and enhances the immobilization level of HPAs. Nevertheless, this synthetic procedure is costly and, therefore, the application of this method was limited to few examples [52].

The fourth method involves a self-immobilization of HPAs onto basic polymer backbones typically in a fiber form [2, 52] or adding another filler with high specific surface area such as reduced graphene oxide (rGO) [54] or rGO covalently modified with 3-aminopropyl-triethoxysilane (mGO) [90]. For example, amounts of up to 50 wt% of PWA could be simply immobilized onto nylon nanofibers by self-immobilization. The fifth proposed method for solving the leaching problem of HPAs was to use water-insoluble salt of HPAs such as $\text{Cs}_x\text{H}_{3-x}\text{PW}_{12}\text{O}_{40}$ [91]. In this regard, HPA salts such as CsH_2PO_4 have been intensively investigated because of their desirable high operating temperature (230–260 °C) [92, 93] and high-protonic conductivity ($\sigma = 2.2 \times 10^{-2} \text{ S cm}^{-1}$ at 240 °C) [94]. Such advantages explain the reason for applying the compositions of CsH_2PO_4 with oxyanions [95], cations [96], and inorganic/organic scaffolds [97, 98] for improving proton conductivity, mechanical properties, and thermal stability at high temperatures in addition to reducing methanol permeability.

4 HPAs in PEM Fuel Cell

HPAs have been used extensively in the PEMFC as additive to the catalyst layer and membrane. As additive to the catalyst layer, HPAs have been used in both cathode and anode mainly to address the CO-poisoning by enhancing the tolerance. Particularly, it was reported that the addition of PMA and corresponding vanadium substituted analogs into Pt results in a remarkable performance improvements when the fuel cell was fed with reformed hydrogen containing 100 ppm CO [99]. It was concluded that PMA acts as an oxidizing agent for the reaction between CO and water in the presence of Pt, Pd, and Au [100, 22]. Besides, the addition of HPAs in the electrode is likely to improve the catalytic activity towards oxygen reduction reaction (ORR) and methanol oxidation reaction (MOR) [101, 55, 102]. However, HPA applications in the catalyst layers of electrodes are beyond the scope of this chapter and more details can be found elsewhere [22].

PFSAs are the choice materials for the membranes for PEMFC applications. However, these membranes are not gas tight enough especially at temperature above 80 °C [20, 5, 103]. Several low cost alternatives such as poly(vinyl alcohol) (PVA), sulfonated poly(ether ether ketone)s (SPEEK), and sulfonated polystyrene (SPS) have been evaluated for PEMFC applications. These membranes exhibited good chemical stability and low fuel crossover. However, their proton conductivity is significantly lower than PFSAs. Typically, the proton conductivity of PVA and SPEEK are in the ranges of 10^{-14} – 10^{-10} S cm⁻¹ [22, 104] and 10^{-4} – 10^{-3} S cm⁻¹ [83], respectively. HPAs have been introduced to various low cost PFSA alternatives to enhance the proton conductivity. This led to an increase in the conductivity up to the range of 10^{-3} – 10^{-1} S cm⁻¹ [83, 105, 106]. Interestingly, such improvement in the conductivity was accompanied by an increase in the thermal stability of membranes.

5 HPAs in High-Temperature and Low-Humidity PEMFC

The main limitation of PFSA family of membranes is their dependence on level of hydration to achieve high conductivity, and this poses a problem when operating at temperatures higher than 80 °C as the proton conductivity of the membranes decreased significantly. The variation of hydration level undermines the permeability of H₂ and O₂ due to the involvement of the formed hydrated ionic clusters in the gas permeation mechanism [107, 108]. On the other hand, the retention and management of water within these types of membranes is challenging, costly and in most cases affect the PEMFC performance. Therefore, there is a strong demand for the PEMs to work at lower relative humidity and/or under anhydrous conditions. However, acceleration of electrochemical reactions and simplification of water management system of fuel cells under lower humidity and/or anhydrous conditions is challenged by dramatic losses of proton conductivity of PFSA membranes [109, 110, 5]. Typically, Nafion 112 losses an order of magnitude of its proton conductivity at around 60% RH, which increases two orders of magnitude with the reduction of RH to 25%.

Various materials and designing strategies were proposed to prepare alternative proton conductors for high-temperature fuel cell operation under dry conditions. The use of other media of proton conduction or less-volatile liquids such as phosphoric and phosphonic acids [1, 111] and amine heterocycles [112] have been widely considered. However, in most cases, the proton conductivity is not comparable to PFSAs and there is a risk of liquid electrolytes leaching. On the other hand, addition of an inorganic material with hydrophilic properties such as HPAs was proposed to maintain high water content levels at elevated temperatures or under dry conditions. There is a linear relationship between water content of the membrane and its conductivity at lower RH%.

A lot of work has been reported on incorporation of different HPAs in PFSA membranes [76, 113, 114] and other hydrocarbon membranes [83, 115, 105, 106, 116, 117] for PEMFCs application. It was shown that the activation energy for proton transport (E_a) decreased significantly for PFSA membranes upon increasing the amount of HPAs under lower RH% [118]. For example, the addition of 5 wt% of PWA lowered E_a by 40% at 60% RH compared to pristine membrane. Initial investigation on various HPAs such as PWA, SiWA, PMA, and SiMA indicated that the additives containing molybdenum were less stable in the membrane environment than those containing tungsten [76]. Upon operating in fuel cell for a few hours, the amount of molybdenum-based additive present in the cathode catalyst layer increased. It was suggested that molybdates migrated into the catalyst layers, where they had a detrimental effect on the performance by undergoing parasitic redox reactions on the surfaces of carbon and platinum, resulting in an increase in the activation overpotential. Table 1 summarizes some of the efforts to introduce HPAs to membranes used in the PEMFC.

Initial studies reported the limiting changes in the stability of HPA in hydrated conditions and the strong influence of humidity on the proton conductivities and diffusional problems of the membranes. The high water solubility of HPAs triggers leaching problem and consequently high drop in a performance. Two different approaches of using alternative heteropolysalts instead of their acid and supported HPAs were widely used to avoid the leaching problem in high-temperature PEMs. More stable HPA containing membranes were achieved using heteropolysalts as fillers in membranes for PEMFCs. In this regard, larger cations such as Cs^+ , NH_4^+ , Rb^+ , and Tl^+ [133] as well as organic cations such as 4,4'- and 2,2'-bipyridines [134] were combined with HPAs to produce heteropoly salts. Precipitation from aqueous solutions was normally used to achieve such partially substituted heteropolysalts [135, 136]. On the other hand, it was shown that a solid-state reaction involving mechano-chemical treatments using a high-energy ball mill is more efficient to prepare heteropolysalts and normally lead to more conductive heteropolysalts [137, 138], and subsequent composite membranes [115]. Additional investigation revealed that the reduction in the particle size facilitates the conductivity due to enhancement in the surface to volume ratio, which permits more efficient proton hopping and increase in conductivity [23]. For example, reducing a filler size from 1–2 mm to 30–50 nm resulted in 35% enhancement in proton conductivity [139].

In the second approach, HPAs or their corresponding salts were supported on different materials including SiO_2 [86, 121, 84, 122, 77, 140, 123], ZrO_2 [84, 120, 77], WO_2 [77], and TiO_2 [84, 77] followed by immobilization in polymeric membranes [86]. PWA was found to be the only heteropolyacid that has been found suitable for these hybrid membranes, and it was concluded that SiO_2 is the best supporting material since there is a strong interaction between the $\text{H}_3\text{PW}_{12}\text{O}_{40}$, Nafion[®], and the SiO_2 molecules [121]. The proton conductivity and the fuel cell performance at 100% RH of the composite membrane close to those of pristine membranes. However, the merits of HPA became evident upon increasing the temperature or reducing the RH%. Improved performance under dry conditions was

Table 1 Properties of some HPA containing membranes for proton exchange membrane fuel cell application

Polymer substrate	HPA (loading level)	Thickness	Proton conductivity ($S\text{ cm}^{-1}$)	Condition	Fuel cell performance ^a (mA cm^{-2})	Refs.
Nafion [®]	NaPWA	175	2.3×10^{-2}	100 °C, 100% RH	136	[119]
	NaPWA	165	1.5×10^{-2}		140	
	NaPMA	160	1.3×10^{-2}		145	
	PWA (25 wt%)	–	6×10^{-2}	80 °C, 75% RH	–	[76]
Nafion [®]	SiWA (25 wt%)	–	1.5×10^{-2}	120 °C, 35% RH	–	
		–	8.5×10^{-2}	80 °C, 75% RH	–	
	PMA (25 wt%)	–	1.0×10^{-2}	120 °C, 35% RH	–	
		–	–	–	–	
	SiMA (25 wt%)	–	8×10^{-2}	80 °C, 75% RH	–	
		–	1.0×10^{-2}	120 °C, 35% RH	–	
Chitosan	PWA-ZrO ₂ (30 wt%)	50–75	6×10^{-3}	120 °C, 25% RH	–	[120]
	PWA-SiO ₂	70 ± 5	1.19×10^{-3}	90 °C, 40% RH	82	[121]
	PWA-SiO ₂ (10 wt%)	120	0.01	Conductivity: 100 °C, 40% RH Fuel cell: 110 °C, 100% RH	540	[122]
Chitosan	PWA/ SiO ₂ (14.3 wt%)	120	2.67×10^{-2}	110 °C, 70% RH	540	[77]
	PWA/meso-SiO ₂	–	0.07	120 °C, 25 RH%	510	[123]
	PWA/mGO (1 wt%)	40	0.0092	80 °C, 20% RH	841	[90]
	CsPWA (2 wt%)	30	0.028	25 °C	410	[124]
Chitosan	CsPWA (2 wt%)	30	0.018	25 °C, low RH ($T_{\text{gas}} = 25\text{ °C}$)	350	[125]
		3	0.014	25 °C, low RH ($T_{\text{gas}} = 25\text{ °C}$)	550	[56]

(continued)

Table 1 (continued)

Polymer substrate	HPA (loading level)	Thickness	Proton conductivity (S cm ⁻¹)	Condition	Fuel cell performance ^a (mA cm ⁻²)	Refs.
SPEEK	CsPWA (20 wt%)	84	2.06×10^{-3}	80 °C, 80 RH%	245	[115]
	CsSiWA (20 wt%)	75	2.25×10^{-3}		247	
	CsPWA/SiO ₂ (2 wt%)	30–40	6.2×10^{-3}	100 °C, 90% RH		[83]
	H ₄ PW ₁₁ VO ₄₀ ·8H ₂ O (70 wt%)	31	10 ⁻²	30 °C, 100% RH	–	[116]
H ₄ PW ₁₁ VO ₄₀ ·8H ₂ O/rGO (70 wt%/2 wt%)	134	6.43×10^{-2}	65 °C, 65% RH	–	–	[54]
PWA (10 wt%)/aluminum phosphate (3 wt%)	52	6.8×10^{-4}	30 °C, 100% RH	–	–	[53]
SPSU	SiO ₂ (2 wt%)/PMA 20 wt%	50	Same to Nafion 112	30–80 °C, 100% RH	–	[126]
PVA	H ₅ [SiW ₁₁ VO ₄₀]15H ₂ O (70 wt%)	33	10 ⁻⁴	30 °C, 100% RH	–	[116]
	PMA (33.3 wt%)		0.0101	–	–	[127]
PBI	PWA (30 wt%)/H ₃ PO ₄	–	0.036	140 °C, 20% RH	–	[128]
	SiWA (30 wt%)/H ₃ PO ₄	–	0.046	200 °C, 5% RH	–	[128]
	SiWA-SiO ₂ (30 wt%)/H ₃ PO ₄	50–80	0.206	150 °C	–	[129]
	C _{82.5} H _{60.5} PM _{0.12} O ₄₀	30	0.00004	150 °C, 0% RH	–	[130]
	C _{82.5} H _{60.5} PM _{0.12} O ₄₀ /H ₃ PO ₄	30	0.04	Conductivity: 8.4% RH, 180 °C Fuel cell: 150 °C, 0% RH	800	
	C ₈ POMo (30 wt%)/H ₃ PO ₄	50 ± 3	0.12	150 °C, 0% RH	630	[131]
	C ₈ POW (30 wt%)/H ₃ PO ₄		0.1		590	
	C ₈ SiOMo (30 wt%)/H ₃ PO ₄		0.051		480	
	C ₈ SiOW (30 wt%)/H ₃ PO ₄		0.057		510	

(continued)

Table 1 (continued)

Polymer substrate	HPA (loading level)	Thickness	Proton conductivity (S cm ⁻¹)	Condition	Fuel cell performance ^a (mA cm ⁻²)	Refs.
	CsPWA/H ₃ PO ₄		1.91 × 10 ⁻²	160 °C, 0% RH	84	[98]
	CsSiWA/H ₃ PO ₄		1.71 × 10 ⁻²		–	
PTFE porous	CsPOMo/QDPSU ^b /H ₃ PO ₄	30	0.04	150 °C, 0% RH	240	[132]
Nylon ^c	HPA (51 wt%)	67	0.08	Conductivity: 80 °C, 80% RH Fuel cell: 60 °C, 40% RH	930	[2]

^aMaximum power density (otherwise stated)^bQuaternary diazabicyclo-octane polysulfone^cSandwiched between two Nafion layers

also achieved for membranes containing $\text{Cs}_x\text{H}_{3-x}\text{PWO}_{40}$ immobilized on TiO_2 [141] and CeO_2 [142]. Nevertheless, immobilization of HPA salts and their stability on the inorganic supports were much better than pure HPAs [141]. Table 1 illustrates some of the results on HPA salts loading level and properties of the obtained composite membranes.

Commercially available polybenzimidazole (PBI) has been the most extensively studied and used for the PEMFC under high-temperature. Particularly, PBI membranes impregnated with phosphoric acid have been studied as polymer electrolytes in PEMFCs for two decades and were reasonably successful with excellent thermo-chemical stability and good conductivity [143, 144]. Several organic modifiers including ZrP [7] and PWA [145] have been incorporated into PBI to improve the performance of the PBI/ H_3PO_4 membrane.

PWA and SiWA [128, 146], PMA [147], PWA/ SiO_2 [148], and SiWA/ SiO_2 [145] were initially used to fabricate PBI composite membranes. Initial results indicated that the conductivities of the composite membranes containing 20 and 30 wt% of PWA at 140 °C and that of SiWA at 200 °C were lower than that of pristine PBI membranes under the same conditions [128]. It was reported that the SiO_2 support provided a stable structure and membranes were thermally stable up to 400 °C. The conductivity values of $1.5 \times 10^{-3} \text{ S cm}^{-1}$ at 150 °C for PWA/ SiO_2 /PBI and $2.23 \times 10^{-3} \text{ S cm}^{-1}$ at 160 °C for SiWA/ SiO_2 /PBI were reported. In a separate study, 37.5 wt% of SiWA- SiO_2 /mPBI showed excellent proton conductivity of $1.32 \times 10^{-3} \text{ S cm}^{-1}$ at room temperature [149]. Despite the good conductivity values of the composite membranes, there are few reports on fuel cell performance. Membranes composed of PWA/PBI or SiWA/PBI doped with phosphoric acid showed high conductivity compared to neat PBI membranes in high-temperature PEMFC [150]. At 150 °C, the conductivity of the 40% SiWA/PBI composite membrane was 0.1774 S cm^{-1} . In a single cell test, for example, 40 wt% SiWA/PBI exhibits only around 10–15 mV loss in cell potential due to IR drop which is around 75 mV at 500 mA cm^{-2} for PBI. The best fuel cell performance was achieved with a 40 wt% SiWA/PBI composite membrane at 120 °C. However, at higher temperatures, contrary to the PBI membrane, the performance of the SiWA/PBI composite membrane declined in fuel cell. It has been suggested that the PWA/PBI composite membranes were suitable for the temperature limit of 120 °C.

CsHPA was used extensively for PEMFC due to its insolubility in water. Typically, PBI/ $\text{Cs}_{2.5}\text{H}_{0.5}\text{PMo}_{12}\text{O}_{40}/\text{H}_3\text{PO}_4$ composite membrane exhibited conductivity as high as $0.15 \times 10^{-2} \text{ S cm}^{-1}$ and in a fuel cell gave a high power density of 0.7 W cm^2 (at atmospheric pressure and 150 °C with H_2/O_2) [130]. Higher proton conductivities of $1.91 \times 10^{-2} \text{ S cm}^{-1}$ and $1.71 \times 10^{-2} \text{ S cm}^{-1}$ were achieved at 160 °C under anhydrous conditions for mechano chemically synthesized CsHPA composites of PBI-50 $\text{H}_3\text{PW}_{12}\text{O}_{40}$ -50CsHSO₄ with 87 wt% phosphoric acid doping level and PBI-50 $\text{H}_4\text{SiW}_{12}\text{O}_{40}$ -50CsHSO₄ with 82 wt% doping level, respectively [98]. Nevertheless, these composite membranes show better conductivity with comparable single cell results, despite the lower phosphoric acid doping level compared to PBI.

Comparative conductivity, stability and fuel cell performance of PBI composite membranes with four different cesium salts of CsPOMo, CsPOW, CsSiOMo, and CsSiOW were evaluated [131]. The composite membranes loaded with H_3PO_4 showed higher conductivities than that of the phosphoric acid loaded PBI membrane. The conductivity increased with an increase in the percentage of inorganic component in the composite up to 30%. CsPOMo/PBI/ H_3PO_4 exhibited a conductivity of 0.12 S cm^{-1} under anhydrous conditions at 150°C . The membrane having P form of the CsHPA demonstrated higher conductivity than those containing Si atom, although the mechanical strength was inferior. The performance of the fuel cell with these composite membranes was better than that with a phosphoric acid-doped PBI membrane under the same conditions. The CsPOMo gave the best power density of around 0.6 W cm^2 with oxygen at atmospheric pressure and 150°C .

6 HPAs in DMFC

DMFCs is an alternative cell to the hydrogen PEMFC, which avoids the limitations associated with the use of H_2 as a fuel. In order to be competitive, the DMFC must be reasonably cheap and capable of delivering high power densities. However, the performance of DMFCs is limited by the catalyst and membranes. The slow kinetics of the anode reaction and poisoning of the platinum catalyst together with the high methanol crossover are among main concerns. Typically, PFSA membranes showed exceptional proton conductivity upon employing in DMFCs but excess methanol permeability causes fuel loss, which lowers energy efficiency and fuel cell performance. The use of diluted methanol fuel (<4 molar of methanol), which supposed to minimize excessive fuel permeability is likely to reduce the energy density of fuel cell significantly [151]. Particularly, these drawbacks reduce the energy density to as low as 2000 Wh kg^{-1} and yield low operating voltage compared to PEMFC [152]. The ultimate solution to high methanol crossover, which is a key barrier for the development of DMFC, is the utilization of membranes with low methanol permeability that have potential for operation at higher temperatures. Introducing nanoparticles into polymers substrates is an effective tool to suppress methanol crossover, but is often accompanied by the partial loss of proton conductivity because protons and methanol are transported through the same pathway. HPAs having very strong Brønsted acidity approaching to the level of the superacids (more acidic than 100% sulfuric acid and Nafion) and fast reversible redox transformations are interesting candidates for preparation of composite membranes for DMFC [153]. HPAs have been immobilized in various proton conducting membranes to improve methanol barrier property and/or proton conductivity [154, 155]. DMFC performance based on the PWA—meso-silica nanocomposite membrane and low Pt catalyst loading (1 mg cm^2)—was found close to the advanced DMFCs ($100\text{--}200 \text{ mW cm}^2$) [156].

Majority of reported studies of HPAs based composite membranes were dedicated to PFSA based membranes including Nafion. Generally, various HPAs were

used as dopants that are usually sonicated with liquid Nafion in a high boiling point solvent before casting. Typically, stable molybdophosphoric acid (PMA)-impregnated membranes were reported to be prepared either by exposing cast membranes to solvent vapor at room temperature for 24 h and annealing at 150 °C [157] or by imbedding in polymer films using mixed solvents [158]. The obtained membranes showed noticeable enhancement in the conductivity [157] and improvement in the methanol rejection [158] compared to commercial Nafion.

Operation at high temperatures significantly enhances the kinetics of methanol oxidation. It was reported that the addition of inorganic hygroscopic materials to Nafion extends the operating temperature range of DMFC [159, 160, 140]. Nafion–silica composite membranes doped with phosphotungstic and silicotungstic acids were investigated at 145 °C and improvements in the electrochemical characteristics at high current densities were reported [140]. For instance, a maximum power density of 400 mW cm⁻² was obtained at 145 °C in the presence of oxygen feed, whereas the maximum power density in the presence of air feed was around 250 mW cm⁻² [140]. In another study, the power densities of 33 mW cm⁻² at 80 °C, 39 mW cm⁻² at 160 °C, and 44 mW cm⁻² at 200 °C were reported [160]. Such improved performance was correlated to the strong interaction of inorganic fillers with water at high temperature. Table 2 illustrates additional examples of HPAs

Table 2 PWA loading level, thickness, conductivities, and methanol permeability of various DMFC membranes

Sample	Thickness (μm)	Proton conductivity (S cm ⁻¹)	MeOH permeability (×10 ⁻⁸ cm ² s ⁻¹)	DMFC performance ^a (mW cm ⁻²)	Refs.
SPBN ^b	–	6.1 × 10 ⁻² at 100% RH, 30 °C	93.9	63 at 80 °C, (1 M methanol)	[161]
SPEEK/PWA	–	1.7 × 10 ⁻² at 100% RH, 100 °C	–	–	[162]
SPEEK/MMT ^c -SiWA (30 wt%)	–	43.8 × 10 ⁻² at 100% RH, 30 °C	35.0	–	[64]
Nylon ^d (51.12)	95	3.59	16.3	127.1 at 60 °C, (5 M methanol)	[52]
40%-smpCTS/PWA (52.4)	–	29 at 80 °C	0.47	16 at 80 °C, (2 M methanol)	[10]
PPy-layered SPEES/PWA	–	6.0 at 25 °C	21	–	[163]
PES/PVP-PWA	–	78 at 80 °C	165	132 (2 M methanol)	[11]
Nafion/PPO/PMA	100 ± 5	3.41 × 10 ⁻² at room temperature	44.1	Higher OCV than Nafion	[158]
Nafion-silica/PWA	80	–	–	250 at 145 °C	[140]
Nafion-silica/ PWA	–	0.024	25	70 at 80 °C	[164]
N212/PDDA-PWA ^e	51	–	–	–	[165]

(continued)

Table 2 (continued)

Sample	Thickness (μm)	Proton conductivity (S cm ⁻¹)	MeOH permeability (×10 ⁻⁸ cm ² s ⁻¹)	DMFC performance ^a (mW cm ⁻²)	Refs.
SPAEEK-COOH/polycation chitosan (CTS)-PWA	50	0.24 at 80 °C	100	–	[166]
Pore-filled PVDF with PWA	–	0.098 at 80 °C	90	–	[167]
Pore-filled PVDF with Si-PWA	60	1.01 × 10 ⁻² at 60 °C	–	21.6 at 25 °C	[168]
PVA-ZrP-CsSiWA	180	13 at 100 °C, 50% RH	200	2.1	[169]
PVA immobilized Si-PWA	80	0.0105 × 10 ⁻² at 50 °C	16	29.6 at 35 °C	[170]
PVA/PAA-CsPMA	250 ± 20	3.7	11	36 at 25 °C	[171]
PVA/PAA-CsPWA	250 ± 20	3	6.7	30 at 25 °C	[171]
PVA/PAA-CsSiWA	250 ± 20	1.8	1.38	39 at 25 °C	[171]
CsPW-Nafion	50	0.05	15.4	30.6 at 25 °C, (2 M methanol)	[172]
CsPW-Chitosan	–	75 at 80 °C	156	–	[173]
CsPW-SPEEK	80–100	1.3 × 10 ⁻¹ at 80 °C 100% RH	47	–	[174]
PWA-MC/Imidazole		31.6 at 80 °C, room temperature	166	–	[154]
PVA-ZrP-SiWA	250	1 × 10 ⁻² at 60 °C, 60% RH	60	–	[175]
PVA-PWA-SiO ₂	–	0.004–0.017	1–10	–	[176]
PVA/PMA	–	2.05	154	–	[177]
PEG/SiO ₂ -PWA	150–400	5.04 × 10 ⁻³	121	–	[178]

^aMaximum power density (otherwise stated)^bSulfonated polynorbornene membranes^cK10 montmorillonite^dSandwiched between two Nafion layers^eFour bilayers of poly(diallyl dimethyl ammonium chloride) and PWA

composite membranes for DMFC applications at high temperature as well as normal operation temperature.

PWA in SPEEKs and poly(1,4-phenylene ether ether sulfone) stabilized by surface modification with polypyrrole (Ppy) using an in situ polymerization method showed a reduction in the methanol crossover without significant leaching in PWA [163, 179]. In addition, the water uptake, swelling ratio, and the tensile strength of the surface-coated membranes were improved with the increase in the thickness of Ppy layer. In a similar approach, PWA was microcapsulated into imidazole and incorporated into SPEEK membrane matrix prior to evaluation in DMFC and revealed improved DMFC performance [154].

Pore-filling of polymer substrates with HPAs was also reported to achieve an improved performance of DMFC [168, 167]. Typically, pores of PVDF substrates filled by sulfonated poly(aryl ether ketone sulfone) membranes blended with phosphotungstic acid resulted in a membrane with comparable conductivity and lower methanol permeability than Nafion [167]. The layer-by-layer (LbL) self-assembly is another method to introduce a thin multilayer film on a substrate by sequential electrostatic adsorption between the negatively and positively charged polyelectrolytes. A 50% reduction in the methanol permeability was reported for most of the LbL membranes. Typically, bilayers of chitosan and PWA onto sulfonated poly (aryl ether ketone) (SPAEEK) substrate resulted in a membrane with high-proton conductivity values up to 0.24 S cm^{-1} at $80 \text{ }^\circ\text{C}$ and extremely low water swelling ratio and methanol permeability [166].

Inorganic PEM such as PWA immobilized into mesoporous silica matrix such as MCM-41 (Si-PWA) was assembled and used in DMFC [180, 181]. The PWA/MCM-41 electrolyte has a high-proton conductivity of $4.5 \times 10^{-2} \text{ S cm}^{-1}$ at $150 \text{ }^\circ\text{C}$ with an activation energy of ca. 8 kJ mol^{-1} . Single fuel cell tests showed a peak power density of 95 mW cm^{-2} at $100 \text{ }^\circ\text{C}$ and 100% RH with H_2/O_2 system and 90 mW cm^{-2} in methanol/ O_2 at $150 \text{ }^\circ\text{C}$ and an extremely low RH of 0.67%. This sub-micron to nano-sized Si-PWA immobilized onto PVA crosslinked glutaraldehyde [170] and porous PVDF [168] were also reported. Lower methanol permeability than Nafion and a maximum power density of around 44 mW cm^{-2} were obtained at $60 \text{ }^\circ\text{C}$.

An interesting class of materials for suppressing methanol permeability is the polymers containing basic groups including amine, amide, imine, and imidazole [182–184]. One of the key membranes of interest in DMFC is PBI based materials such as commercialized Celtec-V membrane, which is a blend of PBI and poly (vinylphosphonic acid) [185]. Although some encouraging results were reported [186], the conductivity was low and needed to be improved. PWA was self-immobilized on various substrates with basic groups to reduce methanol permeability [52, 10]. Since the HPA is immobilized, the leaching risk is minimized and the conductivity could be simply tuned by controlling the level of PWA. Upon using micro-pores chitosan as a substrate, comparable performance and excellent methanol-blocking performance of 60% lower than that of Nafion 212 membrane was achieved [10].

Recently, it was reported that self-immobilization of high level of PWA on electrospun nylon nanofibrous results in a highly selective methanol barrier with undetectable leaching of PWA [52]. Upon assembling in a sandwiched proton conducting membranes (Fig. 6) with Nafion outer layers, superior methanol barrier properties (viz. $P = 3.59 \times 10^{-8} \text{ cm}^2 \text{ s}^{-1}$) and selectivity mounting to more than 20 times higher than Nafion 115 coupled with proton conductivities reaching $58.6 \times 10^{-3} \text{ mS cm}^{-1}$ at $30 \text{ }^\circ\text{C}$ were achieved. When tested in DMFC single cell, the performance of hybrid membrane was far better than Nafion 115 especially at higher methanol concentrations. For example, at 2 M methanol feed, the composite membrane had an improvement in power peak by 49.6% over Nafion 115. An increase in the power peak by 113.3% was obtained with 5 M methanol feed and

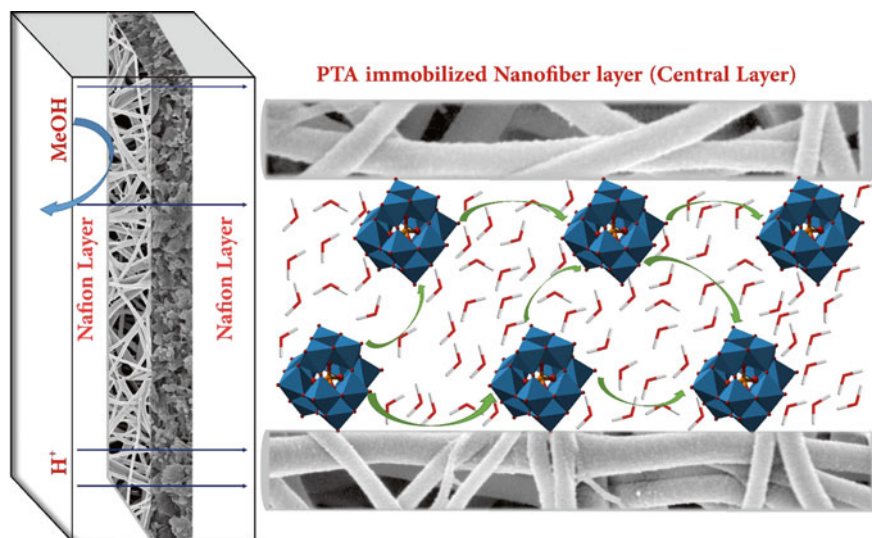


Fig. 6 Three-layered membranes composed of self-immobilized PWA on electrospun nylon and two outer Nafion layers [52]

the maximum power density of 127.1 mW cm^{-2} that was observed for 3L membrane compared to 59.6 mW cm^{-2} for Nafion 115. In addition, the OCV, which is directly related to the methanol crossover, was improved to 693 and 675 mV giving about 41 and 78 mV higher than that of Nafion 115 in 2 and 5 M methanol, respectively. Self-immobilization of PWA on PES/PVP-PWA also resulted in comparable performance of 132 mW cm^{-2} to that of Nafion 212 at $80 \text{ }^\circ\text{C}$ [187, 11].

Cesium phosphotungstate salt enhances the proton conductivity and reduces methanol permeability of various host substrates including SPEEK [174] chitosan-hydroxy ethyl cellulose (CS-HEC) [188], chitosan [173], PVA [169] and PVA/PAA [171], etc. Cesium phosphotungstate salt has excellent conductive capability and increased stability in aqueous media. PVA/PAA membranes with various Cs salt of heteropolyacids were assembled for DMFC [171]. The blend of PVA and PAA was crosslinked with glutaraldehyde, and the Cs salts of different HPAs, including PMA, PWA, and silicotungstic acid (SiWA), were incorporated into the polymer network to form PVA/PAA–CsPMA, PVA/PAA–CsPWA, and PVA/PAA–CsSiWA. A dense network formation was achieved through crosslinking with glutaraldehyde, which led to an order of magnitude decrease in the methanol permeability compared to Nafion 115 membrane. The hybrid membrane containing CsSiWA exhibited a very low methanol permeability of $1.4 \times 10^{-8} \text{ cm}^2 \text{ s}^{-1}$) compared to other membranes. Better performance was achieved when sulfosuccinic acid used as a crosslinker possibly due to the presence of sulfonic acid in the structure of crosslinker [189]. Ultralow methanol permeability resulted to a power density of 150 mW cm^{-2} at a current density of 500 mA cm^{-2} .

To avoid any heterogeneity in the membrane preparation and consequent decline in both proton conductivity and mechanical properties of composite membranes, which may cause by the relatively large particle sizes, an in situ synthesis of proton-conductive nanoparticles within a polymer matrix was reported [172]. Particularly, nanoparticles of Cs hydrogen salts of phosphotungstic acid (CsPW) synthesized in situ in Nafion (CsPW–Nafion) resulted in a 101.3% increase of maximum power density relative to pristine Nafion in DMFC [172].

7 Concluding Remarks and Future Perspectives

Various types of HPAs in a pure or modified forms and as an additive have been incorporated in composite membranes in various types of PEMFC. In composite proton exchange membranes, HPAs and their corresponding salts have been immobilized into various inert and ionomeric substrates to reduce fuel crossover and enhance the proton transport and fuel cell performance especially at high temperatures and in dry conditions. In addition, HPAs were evaluated in DMFC to suppress methanol crossover. Among various types of HPAs, phosphotungstic acid and corresponding cesium salts have been used widely due to their long-term stability in fuel cell.

Effective immobilization of HPAs onto polymeric substrates is still challenging due to the highly solubility of such fillers in water. Using of corresponding salts of HPAs, covalent attachments to the polymer backbones and immobilization on the porous silica or fibrous structured amid-type backbones have been proposed to overcome the HPAs leaching during PEMFC or DMFC operation. Although some preliminarily reports indicate a stable immobilization of HPAs in the composite membranes, the long-term stability under dynamic fuel cell conditions has been not provided in many cases. Particularly, the PEMFC performance under higher temperature and low relative humidity is lacking and this aspect is needed to be investigated comprehensively.

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