

Chapter 1

Resource Recovery and Recycling from Waste Metal Dust (I): Waste Iron Dust and Waste Aluminum Dust



Daniel Ogochukwu Okanigbe 

1.1 Waste Metal Dusts

Extractive metallurgy uses smelting to create a metal from its ore [1]. Heat and a chemical reduction agent are used in smelting to break down the ore, removing other components as gases or slag and only leaving the metal behind [2, 3] while purifying an impure metal is the purpose of refining in the field of metallurgy [4–6]. In contrast to smelting, which results in a chemical change to the raw material, refining typically results in a purer finished product that is typically chemically same to the original [7].

However, in order to convert metal ores like copper glance [8, 9], pisolitic ironstone [10], bauxite [11], and galena [12] into pure copper, iron, aluminum, and lead, respectively, these two metallurgical processes need to reach extremely high temperatures. As a result, throughout the smelting process, it is crucial to know these metals' melting points, for instance, copper melts at 1085 °C [13, 14], iron melts at 1536 °C [15, 16], aluminum melts at 660 °C [17], lead melts at 328 °C [18] and so on. Many other metals and metal compounds also melt or volatilize at these temperatures; for instance, lead has a melting point of 328 °C [18], and mercury, cadmium, zinc, and arsenic all have boiling points of 357 °C [19], 765 °C [20], 906 °C [21], and 613 °C [22], respectively.

Wastes are produced during the metal smelting and refining processes, including dusts among others [23]. Metals including copper, iron, aluminum, lead, zinc, nickel, cadmium, chromium, mercury, selenium, arsenic, cobalt, etc., are frequently found in these wastes.

D. O. Okanigbe (✉)

Department of Chemical, Metallurgical and Materials Engineering, Faculty of Engineering and the Built Environment, Tshwane University of Technology, Pretoria, South Africa

Pantheon Virtual Engineering Solutions, Nigel, South Africa

e-mail: okanigbedo@tut.ac.za; okanigbeogochukwu@gmail.com

To create metal alloys, these elements may be present in the ores utilized or they may be introduced as mixed metals to the melting [24].

In this chapter, the dusts created during metal smelting and refining are referred to as waste metal dust (WMD) because they frequently contain considerable amounts of valuable metal oxides. Due to the high metal concentrations, WMD created in the smelting furnace is categorized as both a lucrative by-product and a dangerous pollution [25]. In order to manage this type of metallurgical waste, this has inspired various researchers in the past and even now to study further acceptable ways on resource recovery and recycling from WMD.

Because of this, this chapter provides a summary of resource recovery and recycling from WMD, concentrating on the generation of WMD, their description, their recirculation or disposal, as well as modern methods for resource recovery and recycling from WMD.

1.2 Types of Waste Metal Dusts

1.2.1 Waste Iron Dust

1.2.1.1 Generation

For the most part, low-carbon stainless steels are refined using the argon oxygen decarburization (AOD) and vacuum oxygen decarburization (VOD) procedures. During the refining process, waste iron dust (WID) [26, 27] is generated. It has a significant amount of precious metal oxides of Fe, Cr, and Ni, and its production rises together with that of stainless steel [28, 29].

Several reports have been shared on its treatment, because of these valuable metals, WID often contains [30–34]. WID is metal and slag mixes that primarily found their way into the equipment used for collecting. Additionally, some WID was released from the flue gas pipelines as a result of the ferociously violent stirring of molten steel during the operations for producing stainless steel.

1.2.1.2 Description of WID

Particle Size Distribution of WID

WID is very fine material, according to all reported analyses [30, 31, 35]. Particles with a diameter of less than 5 μm made up roughly 70–90% (by weight) of the dusts, and even more of them had a diameter of less than 1 μm . In WID, there are still a few sizable solid agglomerates that make about 10–30% of the total weight and may have had a diameter of more than 150 μm .

Chemical Composition of Typical WID

According to Sofilić et al. [29], the chemical species in WID depend on the quality of the steel scrap treated, the type of steel being produced, technological and operating circumstances, and the degree of dust returned into the process.

According to this assertion, Table 1.1 illustrates the several chemical species that make up the predominant composition of these WID. Since iron ore is

Table 1.1 Chemical Species in WID from Various Processing Facilities across the World

Species	Content						
	WID 1	WID 2	WID 3	WID 4	WID 5	WID 6	WID 7
CaO	14.00	6.59	9.02	9.14	12.90	9.14	2.31
SiO ₂	5.60	5.76	5.14	5.45	4.81	5.45	6.42
Al ₂ O ₃	0.70	0.74	0.64	0.66	0.40	0.66	6.67
MgO	2.60	4.25	3.63	3.48	5.44	3.48	2.35
Cr ₂ O ₃ /CrO	14.30 ^[Cr₂O₃]	—	16.30 ^[Cr₂O₃]	15.10 ^[Cr₂O₃]	14.60 ^[Cr₂O₃]	13.51 ^[CrO]	9.09 ^[Cr₂O₃]
MnO/MnO ₂	3.30 ^[MnO]	5.88 ^[MnO]	4.41 ^[MnO₂]	4.67 ^[MnO₂]	5.08 ^[MnO]	4.67 ^[MnO₂]	2.64 ^[MnO]
Fe ₂ O ₃	45.20	39.56	51.30	48.00	43.40	56.00	≈ 46.28
CuO	—	—	—	—	—	—	0.43
WO ₃	—	—	—	—	—	—	0.91
BiO	—	—	—	—	—	—	≈ 0.07
SnO ₂	—	—	—	—	—	—	≈ 0.05
TiO ₂	—	0.16	0.08	0.12	0.08	—	≈ 0.07
NiO	4.30	—	6.25	6.70	2.79	6.70	2.42
ZnO	5.80	—	0.96	0.93	4.49	0.93	7.41
Na ₂ O	4.20	1.01	0.60	0.53	0.60	—	—
K ₂ O	—	0.48	0.72	1.47	0.97	—	—
P ₂ O ₃	—	0.04	0.30	0.62	0.04	—	—
V ₂ O ₅	—	—	—	—	0.09	—	0.13
PbO	—	—	0.29	0.16	0.39	0.16	0.45
CdO	—	—	0.01	0.01	—	—	≈ 0.01
MoO ₃	—	—	—	—	1.35	—	—
CoO	—	—	—	—	—	—	≈ 0.04
ZrO ₂	—	—	—	—	—	—	0.02
Nb ₂ O ₅	—	—	—	—	—	—	≈ 0.07
SO ₃	—	—	—	—	0.47	—	—
F	—	—	—	—	—	—	—
Cl	—	—	—	—	0.86	—	—
S	—	—	—	—	—	—	0.13
LOI	—	3.67	—	—	0.21	—	—
Others	—	31.86	—	—	1.45	—	9.75

Key: WID 1 = Kim and Sohn [26] (wt%); WID 2 = Laforest and Duchesne [32] (mass fraction, %); WID 3 = Tang et al. [33] (mass fraction, %, bag house); WID 4 = Tang et al. [33] (mass fraction, %, stockpile); WID 5 = Ma and Garbers-Craig [34] (mass fraction, %); WID 6 = Peng et al. (2007) (mass fraction, %, stockpile); WID 7 = Takano [36] (wt%); LOI = loss on ignition

involved, Fe_2O_3 had the highest percentage in each WID (39.56–56.00%), as one might anticipate. Then comes CaO (2.31–14.00%), ZnO (0.93–7.41%), NiO (2.42–6.70%), SiO_2 (4.81–6.42%), MnO/MnO_2 (2.64–5.88%), MgO (2.35–5.44%), and $\text{Cr}_2\text{O}_3/\text{CrO}$ (9.09–16.30%). The variety of these WID's contents and compositions places a great emphasis on the need for categorization of these WID [29]. Information like this demonstrates even more how the WID from the various sources listed in Table 1.1 differs in terms of harmful chemical species like Cr_2O_3 . This has influenced how waste management strategies have been adopted [34].

Mineralogy of WID

Some researches [26, 29, 32] looked at the phase structures of the WID. Complex oxides, which frequently take the form of phases like $\text{ZnS}_2\text{O}_4\text{Na}_2\text{S}_2\text{O}_4\text{nH}_2\text{O}$ [29] and $\text{Fe}_2(\text{SO}_4)_3\text{H}_2\text{SO}_4\text{2H}_2\text{O}$, are abundant in the WID and predominate there. Sulfides (FeS , Fe_9S_8 , Ni_7S_6 [29], and silicate SiO_2 , 2FeOSiO_2 [29]) are also present, though. Before disposal, a suitable process path has always been designed for the recovery of the valuable metals, depending on the composition of these compounds and associations.

Morphology of WID

Several researches have investigated the micro-shape of the WID constituents [29, 32, 37]. Individual particles were typically spherical [30, 37, 38] and frequently seen in aggregate forms; angular particles were uncommon [29, 39].

1.2.1.3 Stabilization/Solidification for Recirculation or Disposal of WID

WID must first be converted into briquettes using a suitable reducing agent, such as carbon, in order to be recirculated [26, 40, 41]. But because they require more binder, such as bentonite or cement, and increase the volume of slag, impurities like CaO , SiO_2 , Al_2O_3 , MgO , and ZnO in the recirculated WID might reduce the furnace's efficiency and use unnecessary electricity [26, 40, 42].

Recirculation to the furnace is also not an option due to the presence of harmful heavy metals, some of which are partially soluble, such as the fatal hexavalent chromium (Cr^{6+}) [26].

Should these harmful heavy metals in WID be stabilized or consolidated for ultimate disposal to class one landfill sites, like the large but expensive Vlakfontein investment in South Africa (SA) (Fig. 1.1)? Where this WID are disposed of, potential liability issues may still exist.



Fig. 1.1 Shows the enormous Vlakfontein investment in SA, which was built to address the problem of hazardous wastes. (Source: google image)

1.2.1.4 Resource Recovery and Recycling from WID

The Recovery of Metals from WID

For both economic and environmental reasons, many regions have been processing these WID during the past 20 years in order to extract the valuable metal components, such as nickel, chromium, molybdenum, and iron.

The Use of Hydrometallurgical Techniques

Four processes make up the majority of the hydrometallurgical process: roasting, leaching, purification, and electrowinning. It is a common technique for obtaining non-ferrous metals including zinc, lead, copper, and so forth. According to several commercial methods, hydrometallurgical techniques have been employed to recover Zn from WID using alkaline leaching [43–46].

The Use of Pyrometallurgical Techniques

WID mixes from several researchers have been used in laboratory size reduction smelting studies [36]. Approximately 90% of the total iron, 95% of the chromium, and practically 100% of the nickel in the WID, according to the results, may be recovered by combining molten metals at the right temperature with additives and reductants.

The Use of Physical Separation Techniques

Smaller, more polluted particles are often removed using physical separation methods. Centrifugation, sedimentation, gravity separation, magnetic separation, and other techniques are among them. According to reports, certain commercial

processes have recovered Ni and Cr from stainless-steel wastes using magnetic separation or gravity separation techniques, but the majority of research has remained in the lab [47]. When separating minerals with radically differing densities, gravity separation is an efficient technique. The recovery of ferromagnetic metals from non-ferrous metals and other non-magnetic wastes is frequently accomplished using magnetic separation.

Conversion of WSD into Value-Added Product

Ordoez and Colorado [48] used WID in their research as a complementing material in the additive manufacturing (AM) of kaolinite-based clays as an example of attempts toward the conversion of WID into value-added product. The direct ink writing method was the AM technique used. Since the residues can be immobilized and the water can be less contaminated, adding WID to the clay is good for the environment. The current study demonstrates the potential for employing WID in 3D printed components as well as an admixture with clay ceramics after sintering.

1.2.2 Waste Aluminum Dust

1.2.2.1 Generation

One of the materials that can be recycled the most easily is aluminum [49, 50]. In fact, according to one estimate, 75% of the aluminum that has ever been produced is still in use [51]. This is due to the existence of industrial procedures for the conversion of primary aluminum and scrap into secondary or second fusion aluminum, which generates a number of by-products.

Even so, enormous amounts are wasted as dusts (such as waste aluminum dust), slags, etc. [52], salt slag (more than 500 kg/MT Al), aluminum slag (less than 10,000 MT/year), and furnace filter fines (more than 35 kg/MT Al [53], herein referred to as waste aluminum dust), are the waste products produced in the secondary aluminum melting step (WAD).

1.2.2.2 Description of WAD

Particle Size Distribution of WAD

The particle size of the WAD examined in the study by Nifuku et al. [54] was primarily greater than 105 μm for samples 1 and 2 and primarily in the range of 8–20 μm for sample 3. According to Liu et al. [55], the WAD employed in their

investigation had a larger size dispersion and a mean particle size of about 80 μm . The samples examined, according to Galindo et al. [52], had a significant percentage of fine particles. According to Wang et al. [50], the particle distributions for the WAD under study are 1.34 μm , 3 μm , and 6.59 μm , respectively.

Chemical Composition of Typical WAD

The claim of WAD containing significant amounts of value metals is supported by Table 1.2, which lists the many chemical species that make up the bulk of these WAD's composition. Al_2O_3 has the largest percentage in each WAD (21.56–82.28%), as one might expect given that aluminum ore is included [52, 55]. SiO_2 (range: 0.38–6.30%), MgO (range: 2.37–4.31%), CaO (range: 1.00–2.80%), and Fe_2O_3 (range: 0.64–1.40%) follow.

The amount of salts employed in the melting process in order to achieve a higher aluminum recovery, according to the researchers, is what caused the high sodium concentration, Na_2O (range: 4.7–21.69%).

Table 1.2 Chemical Compositions of WAD Used in Different Study

Composition	Content (wt. %)		
	WAD 1	WAD 2	WAD 3
Al_2O_3	82.28	75.00	21.56
SiO_2	5.74	6.30	0.38
Na_2O	4.71	2.20	21.69
MgO	4.31	4.00	2.37
CaO	1.00	2.80	1.37
Fe_2O_3	0.72	1.40	0.64
K_2O	0.41	0.70	5.88
TiO_2	0.27	2.80	0.37
CuO	0.25	–	–
MnO_2/MnO	0.13 ^[MnO₂]	–	0.05 ^[MnO]
ZnO	0.08	–	–
V_2O_5	0.05	–	–
Cr_2O_3	0.04	–	–
NiO	0.02	–	–
P_2O_5	–	–	0.03
S	–	–	2.69
F	–	–	2.89
Cl	–	1.20	24.42
LOI	–	–	21.82
Others	–	3.30	–

Key: WAD 1 = Liu et al. [55]; WAD 2 = Galindo et al. [52]; WAD 3 = Eliche-Quesada et al. [56]

Mineralogy of WAD

Aluminum metal and aluminum oxide were found to be the primary crystal phases in the investigation by Liu et al. [55] using an XRD diffractogram of WAD. Aluminum nitride, aluminum magnesium oxide, and silicon are additional crystal phases.

Morphology of WAD

According to the morphology of the WAD particles utilized in the investigation by Liu et al. [55], they had an irregular form and a rough surface. While many small rod-like particles congregate on the surface of larger particles, some particles have a plate-like shape. On the other hand, the WAD employed in the study by Wang, Xu, and Wang [50] shows that the particles are roughly spherical and the surface is not rough.

1.2.2.3 Recirculation of WAD

A type of WMD having explosive potential [57–59], WAD produced during the production of aluminum goods is categorized as a hazardous waste in many nations [55, 60].

1.2.2.4 Resource Recovery and Recycling from WAD

Conversion of WAD into Value-Added Product As an illustration of efforts to convert WAD into a value-added product, refractory mullite was prepared using WAD from the fine polishing process used in the manufacture of aluminum parts (also known as aluminum buffing dust) [61]. Ball milling was used to combine Ranong kaolin with WAD in a ratio of 100:0 to 40:60. By dry pressing, the batch mixtures were shaped. The temperature used to fire the green specimens ranged from 1100 to 1400 °C.

In the work by Liu et al. [55], WAD was utilized to create autoclaved aerated concrete by acting as a foaming agent, while Eliche-Quesada et al. [56] produced geopolymer foams using the WAD from the secondary aluminum industry's dust filter as a foaming agent. The source of alumina and the foaming agent in this study was WAD. By using a commercial sodium silicate solution and a sodium hydroxide aqueous solution, precursors were chemically activated. The authors claim that the synthetic geopolymer foam materials are equivalent to traditional building products including gypsum boards, foamed concrete, and insulating materials in terms of

their qualities. They suggested using these synthetic geopolymer foams as materials for gas filtration or catalyst support in other applications.

1.3 Conclusions

The comparative particle size distribution, chemical composition and morphology results of WID and WAD, provide a better analysis of the possibility of their recirculation or disposal after their stabilization/solidification. Hence, the following deductions were reached:

1. All particle size distribution results show that WID was very fine, with particle size smaller than 5 μm in diameter.
2. The chemical composition of WID produced by steel producers around the world is often identical, with Fe_2O_3 having the highest content (39.56–56.00%), as followed by $\text{Cr}_2\text{O}_3/\text{CrO}$ (9.09–16.30%), then CaO (2.31–14.00%), ZnO (0.93–7.41%), NiO (2.42–6.70%), SiO_2 (4.81–6.42%), MnO/MnO_2 (2.64–5.88%), MgO (2.35–5.44%).
3. The metals in WID were mainly present in the form of complex oxide, and also as silicates.
4. On some occasions, the particle size of WAD ranged between 80 and 105 μm , whereas WAD's PSD was reported between 1.34 and 20 μm size fractions.
5. Al_2O_3 makes up the greatest percentage of each WAD (21.56–82.28%), followed by SiO_2 (0.38–6.30%), MgO (2.37–4.31%), CaO (1.00–2.80%), and Fe_2O_3 (0.64–1.40%).
6. Aluminum metal and aluminum oxide were found to be the primary crystal phases in WAD. Aluminum nitride, aluminum magnesium oxide, and silicon are additional crystal phases reportedly present in WAD.
7. The WAD particle shapes range from small rod-like particles with a roughly spherical shape to smooth surfaces.

All of these findings indicate that the WMDs mentioned contain significant amounts of precious metals and other components in addition to hazardous metals. Direct stabilization/solidification techniques for disposal or recirculation were not the most effective ways to manage WMD, though, due to the scarcity of mineral resources. Therefore, resource recovery and recycling from these WMDs is a sustainable strategy from both an economic and environmental standpoint.

Acknowledgments The author will want to appreciate the Council for scientific and industrial research, Pretoria, South Africa and Tshwane University of Technology, Pretoria, South Africa, for the financial support. The author additionally acknowledges the facilities provided by Gravity concentrator Africa (PTY), Randburg, South Africa; Vaal University of Technology, Vanderbijlpark, South Africa; and University of Pretoria, Pretoria, South Africa.

References

1. F. Habashi, *Principles of Extractive Metallurgy: Pyrometallurgy* (Routledge, Abingdon, 2017)
2. L. Lu, J. Pan, D. Zhu, Quality requirements of iron ore for iron production, in *Iron Ore*, (Woodhead Publishing, Oxford, 2015), pp. 475–504
3. L. Brückner, J. Frank, T. Elwert, Industrial recycling of lithium-ion batteries—A critical review of metallurgical process routes. *Metals* **10**(8), 1107 (2020)
4. J. Li, B. Ban, Y. Li, X. Bai, T. Zhang, J. Chen, Removal of impurities from metallurgical grade silicon during Ga-Si solvent refining. *Silicon* **9**(1), 77–83 (2017)
5. S. Esfahani, M. Barati, Purification of metallurgical silicon using iron as an impurity getter part I: Growth and separation of Si. *Met. Mater. Int.* **17**(5), 823–829 (2011)
6. F. Huang, Q. Lu, M. Wu, L. Zhao, Purification of metallurgical-grade silicon by Sn-Si solvent refining with different tin content. *Silicon*, **14**, 1–11 (2022)
7. M. Cavallini, Thermodynamics applied to iron smelting techniques. *Appl. Phys. A* **113**(4), 1049–1053 (2013)
8. K. Murari, R. Siddique, K.K. Jain, Use of waste copper slag, a sustainable material. *J. Mater. Cycles Waste Manag.* **17**(1), 13–26 (2015)
9. G.A. Flores, C. Risopatron, J. Pease, Processing of complex materials in the copper industry: Challenges and opportunities ahead. *JOM* **72**(10), 3447–3461 (2020)
10. E.E. Okafor, *Early Iron Smelting in Nsukka-Nigeria: Information from Slags and Residues* (Doctoral dissertation, University of Sheffield, 1992)
11. C.R. Borra, B. Blanpain, Y. Pontikes, K. Binnemans, T. Van Gerven, Recovery of rare earths and major metals from bauxite residue (red mud) by alkali roasting, smelting, and leaching. *J. Sustain. Metall.* **3**(2), 393–404 (2017)
12. M. Shamsuddin, H.Y. Sohn, Constitutive topics in physical chemistry of high-temperature nonferrous metallurgy—A review: Part I. Sulfide roasting and smelting. *JOM* **71**(9), 3253–3265 (2019)
13. X.H. Chen, X. Tang, Z.D. Wang, X.D. Hui, M. Li, Y.W. Wang, Manufacturing process and microstructure of copper-coated aluminum wires. *Int. J. Miner. Metall. Mater.* **22**(2), 190–196 (2015)
14. J.P. Tavener, Development of a standard platinum resistance thermometer for use up to the copper point. *Int. J. Thermophys.* **36**(8), 2027–2035 (2015)
15. S.A. Oglezneva, V.Y. Bulanov, Y.V. Kontsevoi, I.E. Ignat'ev, Production of nickel and iron nanopowders by hydrogen reduction from salts. *Russ. Metall. (Met.)* **2012**(7), 654–658 (2012)
16. K.T. Jacob, C.B. Alcock, The oxygen potential of the systems Fe+ FeCr₂O₄+ Cr₂O₃ and Fe+ FeV₂O₄+ V₂O₃ in the temperature range 750–1600 C. *Metall. Trans. B* **6**(2), 215–221 (1975)
17. S. Hasani, M. Panjepour, M. Shamanian, The oxidation mechanism of pure aluminum powder particles. *Oxid. Met.* **78**(3), 179–195 (2012)
18. V.P. Itkin, C.B. Alcock, The Ca-Pb (calcium-lead) system. *J. Phase Equilib.* **13**(2), 162–169 (1992)
19. C. Guminski, The melting and boiling points of mercury (I-Ig). *J. Chem. Thermodyn.* **4**, 603 (1972)
20. Z. Han, Z. Guo, Y. Zhang, X. Xiao, Z. Xu, Y. Sun, Pyrolysis characteristics of biomass impregnated with cadmium, copper and lead: Influence and distribution. *Waste Biomass Valoriz.* **9**(7), 1223–1230 (2018)
21. C. Wang, B. Lei, P. Jiang, X. Xu, G. Mi, Numerical and experimental investigation of vacuum-assisted laser welding for DP590 galvanized steel lap joint without prescribed gap. *Int. J. Adv. Manuf. Technol.* **94**(9), 4177–4185 (2018)
22. P. Kumar, A. Kumar, R. Kumar, Phytoremediation and Nanoremediation, in *New Frontiers of Nanomaterials in Environmental Science*, (Springer, Singapore, 2021), pp. 281–297
23. R.H. Hanewald, W.A. Munson, D.L. Schweyer, Processing EAF dusts and other nickel-chromium waste materials pyrometallurgically at INMETCO. *Min. Metall. Explor.* **9**(4), 169–173 (1992)

24. J. Banhart, Manufacturing routes for metallic foams. *JOM* **52**(12), 22–27 (2000)
25. Z. Wang, Z. Cui, L. Liu, Q. Ma, X. Xu, Toxicological and biochemical responses of the earthworm *Eisenia fetida* exposed to contaminated soil: Effects of arsenic species. *Chemosphere* **154**, 161–170 (2016)
26. G. Kim, I. Sohn, Selective metal cation concentration during the solidification of stainless steel EAF dust and slag mixtures from high temperatures for increased Cr recovery. *J. Hazard. Mater.* **359**, 174–185 (2018)
27. I.F. Kurunov, The direct production of iron and alternatives to the blast furnace in iron metallurgy for the 21st century. *Metallurgist* **54**(5), 335–342 (2010)
28. J. Rieger, J. Schenk, Residual processing in the European steel industry: A technological overview. *J. Sustain. Metall.* **5**(3), 295–309 (2019)
29. T. Sofilić, A. Rastovčan-Mioč, Š. Cerjan-Stefanović, V. Novosel-Radović, M. Jenko, Characterization of steel mill electric-arc furnace dust. *J. Hazard. Mater.* **109**(1–3), 59–70 (2004)
30. C.L. Li, M.S. Tsai, Mechanism of spinel ferrite dust formation in electric arc furnace steelmaking. *ISIJ Int.* **33**(2), 284–290 (1993)
31. P.J. Nolasco-Sobrinho, D.C.R. Espinosa, J.A.S. Tenório, Characterisation of dusts and sludges generated during stainless steel production in Brazilian industries. *Ironmak. Steelmak.* **30**(1), 11–17 (2003)
32. G. Laforest, J. Duchesne, Characterization and leachability of electric arc furnace dust made from remelting of stainless steel. *J. Hazard. Mater.* **135**(1–3), 156–164 (2006)
33. M.T. Tang, J. Peng, B. Peng, D. Yu, C.B. Tang, Thermal solidification of stainless steelmaking dust. *Trans. Nonferrous Metals Soc. China* **18**(1), 202–206 (2008)
34. G. Ma, A.M. Garbers-Craig, Stabilisation of Cr (VI) in stainless steel plant dust through sintering using silica-rich clay. *J. Hazard. Mater.* **169**(1–3), 210–216 (2009)
35. L. Wu, N.J. Themelis, The flash reduction of electric arc furnace dusts. *JOM* **44**(1), 35–39 (1992)
36. C. Takano, F.L. Cavallante, D.M. dos Santos, M.B. Mourão, Recovery of Cr, Ni and Fe from dust generated in stainless steelmaking. *Miner. Process. Extr. Metall.* **114**(4), 201–206 (2005)
37. Z. Huaiwei, H. Xin, An overview for the utilization of wastes from stainless steel industries. *Resour. Conserv. Recycl.* **55**(8), 745–754 (2011)
38. F. Škvára, F. Kaštánek, I. Pavelková, O. Šolcová, Y. Maléterová, P. Schneider, Solidification of waste steel foundry dust with Portland cement. *J. Hazard. Mater.* **89**(1), 67–81 (2002)
39. P. Rocabois, E. Lectard, J.C. Huber, F. Patisson, Thermodynamic assessment of the oxide phase in the Fe–Zn–O system-application to dust formation in electric arc furnace. In *Proceedings of the 10th International IUPAC Conference on High Temperature Materials Chemistry*, Julich, Germany, 10–14 April 2000; pp. 1–12.
40. H. Zhang, J. Dong, H. Xiong, Z. Wang, Y. Lu, Investigation on cooperative desulfurization efficiency for bearing carbon stainless steel dust briquettes chromium and nickel recovery process. *J. Alloys Compd.* **699**, 408–414 (2017)
41. S. Ri, M. Chu, Separation of metal nugget from self-reduced product of coal composite stainless steel dust briquette. *ISIJ Int.* **55**(8), 1565–1572 (2015)
42. S.S. Jung, G.B. Kim, I. Sohn, Understanding the solidification of stainless steel slag and dust mixtures. *J. Am. Ceram. Soc.* **100**(8), 3771–3783 (2017)
43. A.J.B. Dutra, P.R.P. Paiva, L.M. Tavares, Alkaline leaching of zinc from electric arc furnace steel dust. *Miner. Eng.* **19**(5), 478–485 (2006)
44. B. Lindblom, C. Samuelsson, G. Ye, Fine-particle characterization—An important recycling tool. *JOM* **54**(12), 35–38 (2002)
45. N. Menad, J.N. Ayala, F. Garcia-Carcedo, E. Ruiz-Ayúcar, A. Hernandez, Study of the presence of fluorine in the recycled fractions during carbothermal treatment of EAF dust. *Waste Manag.* **23**(6), 483–491 (2003)
46. S. Kelebek, S. Yörük, B. Davis, Characterization of basic oxygen furnace dust and zinc removal by acid leaching. *Miner. Eng.* **17**(2), 285–291 (2004)
47. J. Geldenhuis, A.W. Home, in *85th Steelmaking Conference Proceedings*, Iron and Steel Society, Nashville TN, 661–668 (2002).

48. E. Ordoñez, H.A. Colorado, Additive manufacturing via the direct ink writing technique of kaolinite-based clay with electric arc furnace steel dust (EAF dust), in *Energy Technology 2020: Recycling, Carbon Dioxide Management, and Other Technologies*, (Springer, Cham, 2020), pp. 307–315
49. M.F. Gándara, Aluminium: The metal of choice. *Mater. Tehnol.* **47**(3), 261–265 (2013)
50. B. Wang, K. Xu, Y. Wang, Using sodium D-gluconate to suppress hydrogen production in wet aluminium waste dust collection systems. *J. Hazard. Mater.* **397**, 122780 (2020)
51. M. Bertram, S. Ramkumar, H. Rechberger, G. Rombach, C. Bayliss, K.J. Martchek, D.B. Müller, G. Liu, A regionally-linked, dynamic material flow modelling tool for rolled, extruded and cast aluminium products. *Resour. Conserv. Recycl.* **125**, 48–69 (2017)
52. R. Galindo, I. Padilla, O. Rodríguez, R. Sánchez-Hernández, S. López-Andrés, A. López-Delgado, Characterization of solid wastes from aluminum tertiary sector: The current state of spanish industry. *J. Miner. Mater. Charact. Eng.* **3**(2), 55–64 (2015)
53. C. Directive, 96/61/EC of 24 September 1996 concerning integrated pollution prevention and control. *Off. J. L* **257**(10), 10 (1996)
54. M. Nifuku, S. Koyanaka, H. Ohya, C. Barre, M. Hatori, S. Fujiwara, S. Horiguchi, I. Sochet, Ignitability characteristics of aluminium and magnesium dusts that are generated during the shredding of post-consumer wastes. *J. Loss Prev. Process Ind.* **20**(4–6), 322–329 (2007)
55. Y. Liu, B.S. Leong, Z.T. Hu, E.H. Yang, Autoclaved aerated concrete incorporating waste aluminum dust as foaming agent. *Constr. Build. Mater.* **148**, 140–147 (2017)
56. D. Eliche-Quesada, S. Ruiz-Molina, L. Pérez-Villarejo, E. Castro, P.J. Sánchez-Soto, Dust filter of secondary aluminium industry as raw material of geopolymer foams. *J. Build. Eng.* **32**, 101656 (2020)
57. L. Marmo, D. Cavallero, M.L. Debernardi, Aluminium dust explosion risk analysis in metal workings. *J. Loss Prev. Process Ind.* **17**(6), 449–465 (2004)
58. R. Malviya, R. Chaudhary, Factors affecting hazardous waste solidification/stabilization: A review. *J. Hazard. Mater.* **137**(1), 267–276 (2006)
59. R.B. Moussa, C. Proust, M. Guessasma, K. Saleh, J. Fortin, Physical mechanisms involved into the flame propagation process through aluminum dust-air clouds: A review. *J. Loss Prev. Process Ind.* **45**, 9–28 (2017)
60. E. David, J. Kopac, Aluminum recovery as a product with high added value using aluminum hazardous waste. *J. Hazard. Mater.* **261**, 316–324 (2013)
61. N. Kongkajun, B. Cherdhirunkorn, W. Borwornkiatkaew, P. Chakartnarodom, Utilization of aluminium buffing dust as a raw material for the production of mullite. *J. Met. Mater. Miner.* **29**(3), 71–75 (2019)