



# Short- and Long-Term Aluminum Filtration Trials with Carbon-Bonded Alumina Filters

Claudia Voigt, Jana Hubálková, Are Bergin, Robert Fritzsich, Shahid Akhtar, Ragnhild Aune, and Christos G. Aneziris

## Abstract

In the present study, carbon-bonded alumina filters, normally used for the filtration of steel melts, have been investigated as a potential filter material for the filtration of aluminum. Short- and long-term pilot-scale filtration trials were conducted, and the filter behavior during filtration of aluminum alloy was determined by the use of Porous Disk Filtration Apparatus (PoDFA) for the short-term trials (with the casting alloy AlSi7Mg) and Liquid Metal Cleanliness Analyzer (LiMCA) for the long-term trials with wrought alloy 6xxx aluminum. All applied filters were also investigated after the filtration trial by Scanning Electron Microscopy (SEM) analysis. Furthermore, sessile drop experiments with capillary

purification were performed to evaluate the wetting behavior as well as any reactions occurring between the filter material and the aluminum alloy being filtered.

## Keywords

Aluminum filtration • Ceramic foam filter • Ceramic

## Introduction

The application of ceramic foam filters is one of the state-of-the-art procedures for the removal of non-metallic inclusions (particles and films) from aluminum melt, which is important as the inclusions cause a reduction of the tensile strength and a sudden failure [1, 2]. Typically, silicon carbide (SiC) and alumina ( $\text{Al}_2\text{O}_3$ ) filters are used. Recently, Voigt et al. [3] considered carbon-bonded alumina filter ( $\text{Al}_2\text{O}_3\text{-C}$ ) as a new filter material for aluminum melts and obtained promising results regarding the filtration behavior.

Sessile drop measurements at 730 °C with capillary purification procedure showed a strong non-wetting behavior between aluminum and the  $\text{Al}_2\text{O}_3\text{-C}$  substrate and resulted in the roll-off of the aluminum droplet from the  $\text{Al}_2\text{O}_3\text{-C}$  substrate so that an interaction between the aluminum and  $\text{Al}_2\text{O}_3\text{-C}$  could not take place. Sessile drop measurements without capillary purification procedure, in contrast, require temperatures >950 °C for the removal of the oxide skin necessary for a reasonable measurement. However, the temperature of 950 °C (220 K higher than the temperature used for the filtration trials) entails further chemical reactions which cannot occur at lower temperatures during filtration [3].

Results from short-term filtration trials [3] show lower PoDFA values for  $\text{Al}_2\text{O}_3\text{-C}$  filters in comparison with  $\text{Al}_2\text{O}_3$  reference filters standing for a better filtration behavior of the  $\text{Al}_2\text{O}_3\text{-C}$  filter material.

In this study, a modified sessile drop test setup with a capillary purification was used to achieve a lasting interface

C. Voigt (✉) · J. Hubálková · C. G. Aneziris  
Technische Universität Bergakademie Freiberg, Institute of  
Ceramics, Refractories and Composite Materials, Agricolastr. 17,  
09599 Freiberg, Germany  
e-mail: [claudia.voigt@ikf.vw.tu-freiberg.de](mailto:claudia.voigt@ikf.vw.tu-freiberg.de)

J. Hubálková  
e-mail: [jana.hubalkova@ikf.vw.tu-freiberg.de](mailto:jana.hubalkova@ikf.vw.tu-freiberg.de)

C. G. Aneziris  
e-mail: [aneziris@ikf.vw.tu-freiberg.de](mailto:aneziris@ikf.vw.tu-freiberg.de)

A. Bergin  
Hydro Aluminium AS, Commercial Technology, Romsdalsvegen  
1, 6600 Sunndalsøra, Norway  
e-mail: [are.bergin@ntnu.no](mailto:are.bergin@ntnu.no)

R. Fritzsich · R. Aune  
Department of Materials Science and Engineering, Norwegian  
University of Science and Technology (NTNU), Trondheim,  
Norway  
e-mail: [robert.fritzsich@ntnu.no](mailto:robert.fritzsich@ntnu.no)

R. Aune  
e-mail: [ragnhild.aune@ntnu.no](mailto:ragnhild.aune@ntnu.no)

S. Akhtar  
Hydro Aluminium AS, Karmøy Primary Production, 4265 Håvik,  
Norway  
e-mail: [Shahid.Akhtar@hydro.com](mailto:Shahid.Akhtar@hydro.com)

between aluminum and  $\text{Al}_2\text{O}_3\text{-C}$  for the microstructural investigations by means of scanning electron microscopy (SEM) and energy dispersive X-ray spectroscopy (EDX). The aluminum filtration behavior of  $\text{Al}_2\text{O}_3\text{-C}$  filters was investigated with long-term filtration trials at a pilot filtration line whereby the filtration efficiency was measured by a liquid metal cleanliness analyzer (LiMCA).

## Materials and Methods

### Preparation of Ceramic Foam Filters and Substrates

For the preparation of alumina skeleton filters, the replica process using polyurethane foams was applied [4]. For the short-term filtration trials, skeleton filters in the form of square cuboids with dimensions of  $50 \times 50 \times 20 \text{ mm}^3$  and 20 ppi (pores per inch) were utilized. In the long-term filtration trials, skeleton filters in the form of a square frustum with a top base of  $178 \times 178 \text{ mm}^2$  (aluminum melt inlet), a bottom base of  $150 \times 150 \text{ mm}^2$  (aluminum melt outlet), a height of 48 mm, and 30 ppi were used.

The sintered alumina skeletons were coated with  $\text{Al}_2\text{O}_3\text{-C}$  slurry (see Table 1) using a combined dipping and centrifugation procedure (removal of excess slurry). After drying, the filters were coked at  $800 \text{ }^\circ\text{C}$  in a steel retort filled with pet coke to provide a reducing atmosphere for 20 h. For the preparation of reference filters, the alumina skeleton

foams were coated with an  $\text{Al}_2\text{O}_3$  slurry (see Table 2) in order to obtain similar macro pore sizes as for the  $\text{Al}_2\text{O}_3\text{-C}$  filters. The  $\text{Al}_2\text{O}_3$  reference filter was sintered at  $1600 \text{ }^\circ\text{C}$  in air atmosphere.

The substrates for the sessile drop test were slip cast to cylindrical samples with a diameter of 55 mm and a height of 5 mm with the help of a mold consisting of a plastic ring and a plaster bottom. The composition of the substrate slurries as well as their thermal treatment followed the same pattern as for the coated filters; see Tables 1 and 2 for more details.

### Sessile Drop Measurements

Sessile drop tests with aluminum are a challenging task due to the affinity of aluminum to oxygen and thus the formation of an oxide skin which alters the results of the contact angle measurements [6, 7]. Therefore, removal of the oxide skin is necessary, and can be achieved by a capillary purification method [7] or an improved sessile drop method [8]. In this study, a simple sessile drop setup with a dropping unit made of boron nitride (Henze Boron Nitride Products AG, Germany) was used [9]. The dropping unit consists of a hopper for the melting of aluminum and a steel plunger pulling the melted aluminum through a bottleneck to retain the oxide skin. The hopper filled with a cylindrical piece of Al99.7 (Rheinfelden, Germany) was placed on the substrate and positioned in the hot stage microscope. The kiln was heated

**Table 1** Composition of the  $\text{Al}_2\text{O}_3\text{-C}$  coating slurry based on [5] (\* based on sum of solids)

	$\text{Al}_2\text{O}_3\text{-C}$
$\text{Al}_2\text{O}_3$ Martoxid MR-70 (Martinswerk, Germany)/wt%	66.0
Coal pitch Carbores P (Rütgers, Germany)/wt%	20.0
Carbon black N991 (Lehmann & Voss & Co., Germany)/wt%	6.3
Graphite AF 96-97 (Graphit Kropfmühl, Germany)/wt%	7.7
Binder and Dispersant Ammonium ligninsulfonate* (Otto Dille, Germany)/wt%	1.5
Dispersant MelPers® 9360* (BASF, Germany)/wt%	0.3
Anti-foaming agent Contraspum K 1012* (Zschimmer & Schwarz, Germany)/wt%	0.1
Solid content/wt%	70
Coking temperature of the coating/ $^\circ\text{C}$	800

**Table 2** Composition of the  $\text{Al}_2\text{O}_3$  coating slurry (\* based on sum of solids)

	$\text{Al}_2\text{O}_3$
$\text{Al}_2\text{O}_3$ CT 9 FG (Almatis, Germany)/wt%	33.3
$\text{Al}_2\text{O}_3$ CT 3000 SG (Almatis, Germany)/wt%	33.3
$\text{Al}_2\text{O}_3$ T60/T64 45 $\mu\text{m}$ (Almatis, Germany)/wt%	33.3
Binder Optapix AC 170* (Zschimmer & Schwarz, Germany)/wt%	1.0
Dispersant Dolapix CE 64* (Zschimmer & Schwarz, Germany)/wt%	0.6
Solid content/wt%	85
Sintering temperature of the coating/ $^\circ\text{C}$	1600

with 10 K/min to a temperature of 730 °C with a holding time of 10 min. During thermal treatment, the kiln chamber was flushed with argon to minimize the oxygen level.

The substrate/Al couple was weighted after the cooling down and with the help of the mass of the ceramic substrate before the experiment, the droplet weight was calculated. The droplet weight was between 300 and 600 mg, which is significantly higher than typical droplet weights (<100 mg) for conventional sessile drop tests [3, 6]. Considering the measured contact angles, it has to be kept in mind that this setup produces droplets with a high weight which is necessary such that the dropping can take place. The higher droplet weight influences the contact angle due to the higher gravity of the droplet. Furthermore, the dropping temperature cannot be precisely adjusted due to the missing of a mechanical trigger leading to significant differences in the reached dropping temperatures and low temperatures (<700 °C). However, the primary goal for using this sessile drop setup was to enable the formation of the interface between Al<sub>2</sub>O<sub>3</sub>-C and aluminum, and not to measure the contact angle between Al<sub>2</sub>O<sub>3</sub>-C.

To reach an Al/Al<sub>2</sub>O<sub>3</sub>-C couple, a small deepening was introduced in the substrate by grinding to hinder the droplet to roll off.

After the sessile drop measurements, microsections of the substrate/Al couples were made to investigate the interface between the substrate material and solidified aluminum by means of the scanning electron microscope (SEM) Philips XL 30 (FEI, Eindhoven, Germany) equipped with an energy dispersive X-ray spectroscopy (EDX) device (Phoenix, USA).

### Short-Term Aluminum Filtration Trials

The short-term filtration trials were conducted at the metal foundry Georg Herrmann Metallgiesserei (Muldenhütten, Germany) with the aluminum alloy AlSi7Mg (EN AC-42100) from Rheinfelden Alloys (Rheinfelden, Germany) whereby the melt comprised 50% ingots and 50% scrap (recycled aluminum consisting of solidified feeders and runners) for the introduction of non-metallic inclusions to the melt. AlSi7Mg alloy was melted, skimmed, and cast into a sand mold consisting of a joint sprue, four horizontal runners with filter chambers, and vertical steel molds [3]. The used filters were cut out and embedded with epoxy resin, ground, polished, and analyzed with SEM/EDX. The aluminum in the steel mold was separated from the feeder and then analyzed regarding non-metallic inclusions with the help of a cold Porous Disk Filtration Apparatus analysis (PoDFA) performed by HOESCH Metallurgical Service (Niederzier, Germany).

### Long-Term Aluminum Filtration Trials

The long-term filtration trials were conducted in a pilot filtration line at Hydro Aluminium AS primary aluminum plant (Sunndal, Norway), which consists of a melting furnace, a launder system, a filter box, and a lifting pump. The line is equipped with two LiMCA II units (ABB Ltd., Canada), which allow the continuous monitoring of inclusion number and size in the front and behind the filter box. As the filter box is designed for 584 mm filters while only 178 mm Al<sub>2</sub>O<sub>3</sub>-C filters were producible for the filtration tests, a refractory adapter holding the four similar 178 mm filters was used. In order to avoid floating of the filters during the inverse priming procedure [10], all four filters were weighed down with a steel adapter. Before the inverse priming started, the filters were preheated using a hot air blower positioned below the filters.

For every trial, about 8 mT wrought aluminum alloy 6082 (main alloying elements of Si ~ 0.95%, Fe ~ 0.2%, Mn ~ 0.6%, and Mg ~ 0.65%) was transferred to the melting furnace and circulated in the loop with the help of the lifting pump. For the introduction of inclusions every 10 min, 4 kg of chips (made of compacted aluminum sawdust) were added behind the lifting pump. Altogether, two long-term filtration trials were conducted: one trial with a reference filter (labeled Al<sub>2</sub>O<sub>3</sub>) and one trial with carbon-bonded alumina filters labeled as Al<sub>2</sub>O<sub>3</sub>-C. The aluminum melt temperature at the priming procedure was 740 °C for both trials.

The employed filters were cut out and embedded in epoxy resin, ground, polished, and analyzed with SEM/EDX.

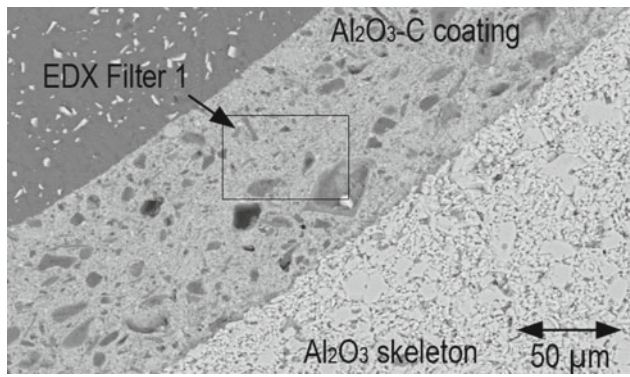
## Results

### Analysis of Ceramic Foam Filters

The filters and the substrates were prepared and examined whereby the structure of the Al<sub>2</sub>O<sub>3</sub>-C coating was examined by SEM, and the chemical composition was measured by EDX (which will be presented in “[Long-Term Aluminum Filtration Trials](#)”). A SEM micrograph of a virgin filter for the long-term filtration shows a heterogeneous microstructure of the Al<sub>2</sub>O<sub>3</sub>-C coating evoked by the different grain size distributions of the carbon raw materials (Fig. 1).

### Sessile Drop Measurements

The contact angles determined by means of the above-described setup possess discrepant results (Table 3) compared to the measurements at 730 and 950 °C performed by Voigt et al. [3]. The underlying causes for the differences



**Fig. 1** SEM micrograph (BSE mode) of a virgin  $\text{Al}_2\text{O}_3\text{-C}$  filter for long-term filtration trial

are manifold: The intended flat deepening on the part of the substrate, a relative high mass of the aluminum droplet as well as a low dropping temperature of  $<700\text{ }^\circ\text{C}$ . The contact angles measured using sessile drop measurement with capillary purification at  $730\text{ }^\circ\text{C}$  [3] are therefore more reliable.

After cooling to room temperature, preliminary tests revealed no adhesion between the aluminum droplet and the  $\text{Al}_2\text{O}_3\text{-C}$  substrate. To hinder a premature release of the solidified aluminum droplet from the substrate during handling and/or sample preparation, a small amount of superglue was used.

The SEM investigation of the interface showed no adhesion of the Al droplet to the substrate but a pronounced interface/reaction zone in the  $\text{Al}_2\text{O}_3\text{-C}$  substrate (dark area in the center left); see Fig. 2b, c. EDX analysis of two marked zones in Fig. 2b showed only slight differences in the chemical composition, particularly regarding silicon and carbon. Within the reaction zone (EDX 2), the silicon peak is higher than in the unreacted zone (EDX 1). Conversely, the carbon peak is lower in the reacted zone (EDX 2) in comparison with the unreacted zone (EDX 1). The origin of the detected silicon is unknown as pure aluminum (99.7%) was used for the sessile drop measurements. It should be mentioned that the carbon detection with EDX is afflicted with an error due to the low atomic number of carbon. But the

clear contrast in the SEM image taken in a backscattered electron mode (Fig. 2c) shows that there is a difference in the chemical composition of EDX 1 and EDX 2, although the difference in the height of the carbon peak is very small. The microstructural investigations by SEM revealed a similar amount and size of large pores ( $>5\text{ }\mu\text{m}$ ) (Fig. 3). Otherwise, a different quantity of small pores ( $<1\text{ }\mu\text{m}$ ) and hence a different polishing behavior due to the surface roughness were observed. This is approved by clear differences in surface morphology between the affected and unaffected zones in Fig. 2b.

### Short-Term Aluminum Filtration Trials

The short-term filtration trial took approximately 16 s and showed an equal filling of the aluminum [3]. The PoDFA index (given in the area of inclusions per kilogram analyzed aluminum) yields the sum of total detected inclusions. The lower PoDFA index indicates a smaller number of non-metallic inclusions in the aluminum sample and hence the better is the melt quality. The PoDFA analyses found  $\text{Al}_2\text{O}_3$  films, carbides, magnesium oxide, spinel, refractory material, iron and manganese oxides as well as grain refiners in the castings. The PoDFA index of  $0.106\text{ mm}^2/\text{kg}$  of the  $\text{Al}_2\text{O}_3\text{-C}$  filter sample was half of the PoDFA index of the  $\text{Al}_2\text{O}_3$  reference filter sample with  $0.246\text{ mm}^2/\text{kg}$ . This indicates an improved filtration when using the  $\text{Al}_2\text{O}_3\text{-C}$  filter.

The SEM images of the used filters of the short-term filtration trials show large inclusions consisting of mainly Al, Mg, Si, and O captured by the filters. The structure of the  $\text{Al}_2\text{O}_3\text{-C}$  coating is comparable to  $\text{Al}_2\text{O}_3\text{-C}$  coating of the unused filter; see Figs. 1 and 4.

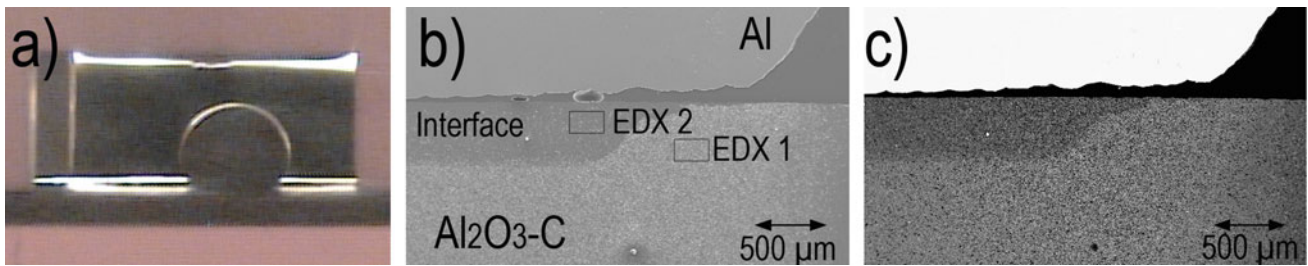
### Long-Term Aluminum Filtration Trials

The N20 values of the LiMCA measurements of the  $\text{Al}_2\text{O}_3$  and the  $\text{Al}_2\text{O}_3\text{-C}$  filter possessed a comparable behavior

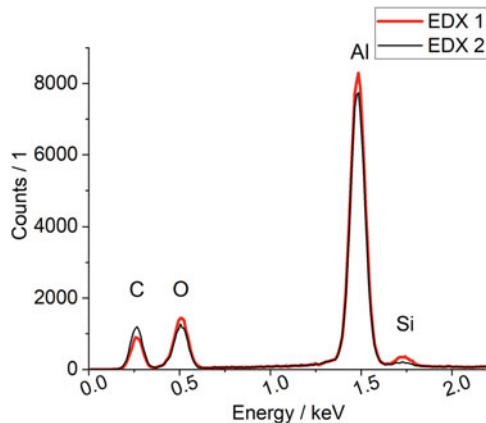
**Table 3** Contact angle and corresponding temperature of the sessile drop experiments

	$\text{Al}_2\text{O}_3$			$\text{Al}_2\text{O}_3\text{-C}$		
	Temperature / $^\circ\text{C}$	Left angle/ $^\circ$	Right angle/ $^\circ$	Temperature / $^\circ\text{C}$	Left angle/ $^\circ$	Right angle/ $^\circ$
Measurement 1	609	128	135	655	130	134
Measurement 2				661	130	135
<i>Contact angles measured for reference [3]</i>						
950 $^\circ\text{C}$ 150 min, vacuum [3]	950	100		950	92	
730 $^\circ\text{C}$ , 30 min, vacuum [3]	730	108		730	157	





**Fig. 2** Sessile drop experiment **a** photograph of the sessile drop setup after dropping, **b** SEM micrograph (SE mode) of  $\text{Al}_2\text{O}_3\text{-C}$ /aluminum couple, and **c** SEM micrograph (BSE mode)



**Fig. 3** EDX analyses of different areas of the substrate

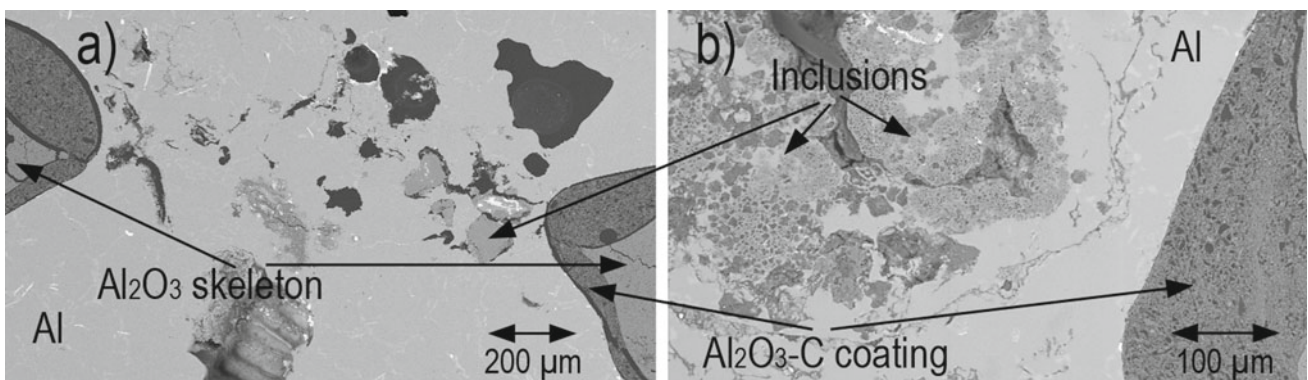
before and after the filter box. The N20 values before the filter box decreased at the beginning of the trial until they reached a relatively stable level. It should be noted that the stable area was shorter for the  $\text{Al}_2\text{O}_3\text{-C}$  trial due to an addition of 67 kg of extra chips for testing the filtration behavior with high inclusions load. The N20 level before the filter box increased with the addition of the chips, but an increase of the N20 level after the filter box is not observed.

The N20 values after the filter box showed a decrease at the beginning of the experiment which is a common

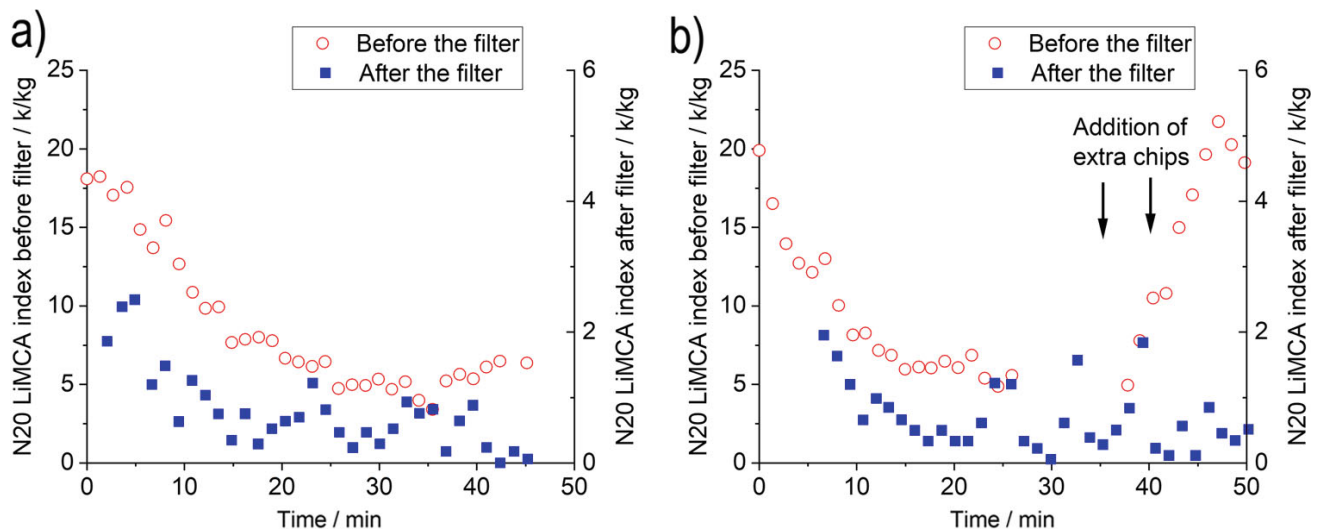
behavior observed at other filtration experiments [11, 12]. It is obvious that the N20 values after the filter box possessed a higher standard deviation than the N20 values in the front of the filter. The N20 levels before and after the filter box are comparable for the  $\text{Al}_2\text{O}_3$  and the  $\text{Al}_2\text{O}_3\text{-C}$  filtration trials. For the stable filtration areas, the filtration efficiency was calculated with  $91.2 \pm 6.7\%$  (for the  $\text{Al}_2\text{O}_3$  between 23.1 and 45 min) and  $88.8 \pm 12.3\%$  (for the  $\text{Al}_2\text{O}_3\text{-C}$  between 15 and 25.9 min). So, the filtration behavior of the two trials is comparable (Fig. 5).

An intensive SEM investigation of the used filters revealed a few typical inclusions captured in the filter. Nearly, no  $\text{Al}_2\text{O}_3$  films, carbides, magnesium oxide, spinel, and refractory material were found; see Fig. 6. Furthermore, a large number of iron-rich intermetallics were found due to the high iron content of the aluminum melt. The iron-rich intermetallic phases were often connected to the filter independent of the filter surface chemistry; see Fig. 6c. The affinity of iron-rich intermetallics to the filter surface would suggest that removal of iron with the help of filters could be effective.

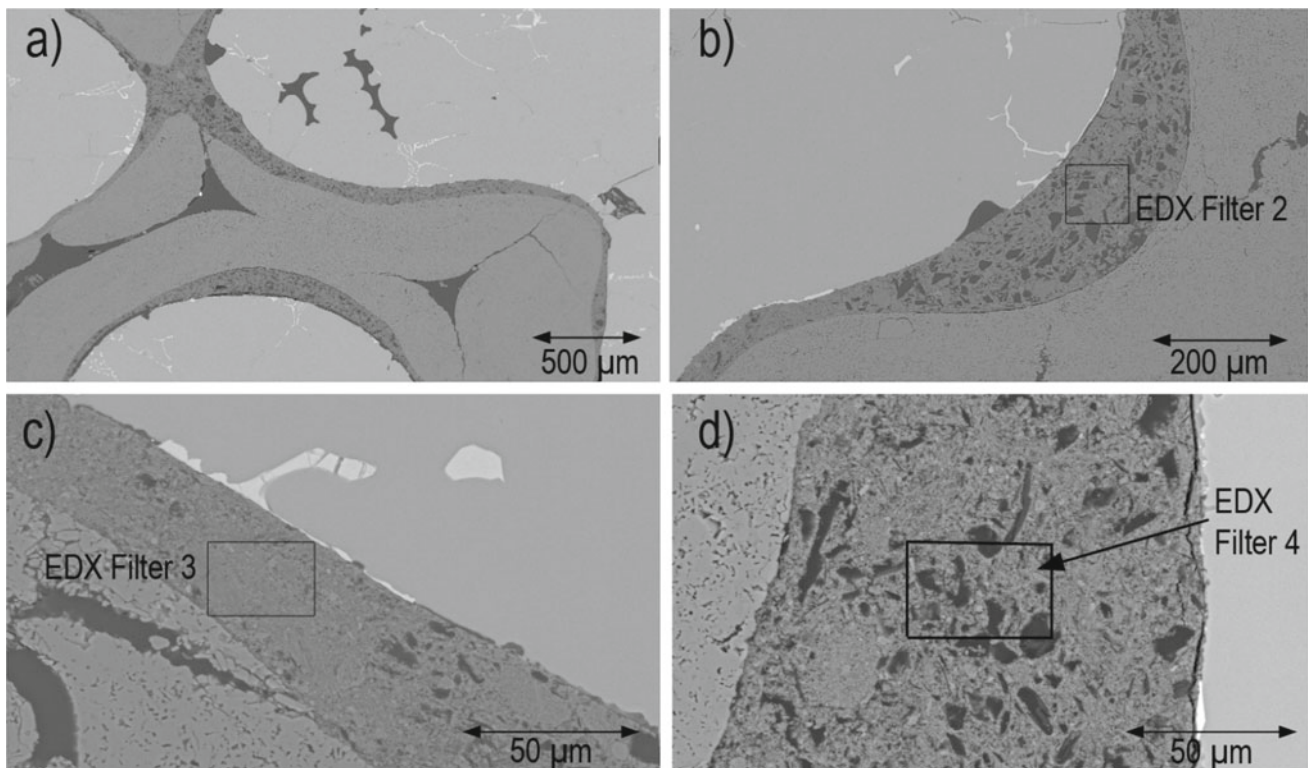
Thus, results from the SEM investigations indicate that the addition of the compacted aluminum sawdust chips does not seem to be a successful way of introducing a comparable level of typical inclusion to the melt because no typical inclusions were detected in the filters. Upon closer examination, it becomes evident that the  $\text{Al}_2\text{O}_3\text{-C}$  coating



**Fig. 4** SEM micrographs (BSE mode) of short filtration trial using  $\text{Al}_2\text{O}_3\text{-C}$  filters with different magnifications, **a** 80 $\times$ , **b** 200 $\times$



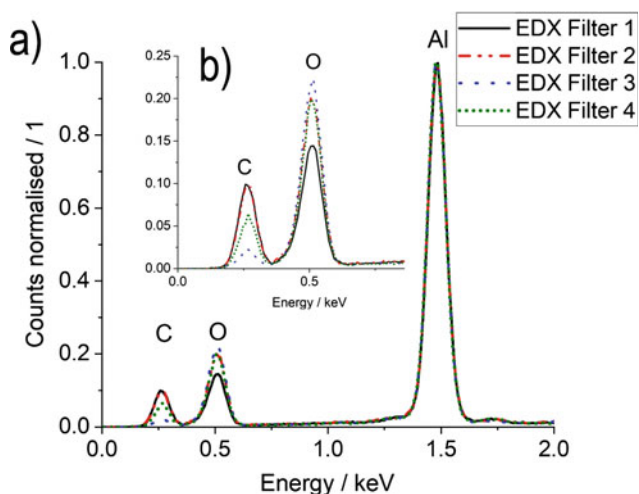
**Fig. 5** Long-term filtration trial **a**  $\text{Al}_2\text{O}_3$  reference and **b**  $\text{Al}_2\text{O}_3\text{-C}$



**Fig. 6** SEM micrographs (BSE mode) of  $\text{Al}_2\text{O}_3\text{-C}$  filter after long-term filtration trial with different magnifications; **a** 30 $\times$ , **b** 100 $\times$ , **c** 500 $\times$ , and **d** 500 $\times$

possessed different structures (Fig. 6) which are not comparable to the unused filter in Fig. 1. Figure 6c shows a very homogenous, dense, and compact coating, and nearly no pores or larger carbon structures are visible. In contrast, Fig. 6d shows  $\text{Al}_2\text{O}_3\text{-C}$  coating with large pores. The large structures of the unused filter (Fig. 1) are not empty—they are filled with carbon raw materials, for example, graphite.

No dependence on the location of the different structures in the filter was observed. Figure 6b shows both structures next to each other. It appears that only thinner areas of the coating have been affected by this phenomenon. EDX analysis showed that the denser the coating, the lower is the carbon peak (see Fig. 7). This observation implicates that in the denser structures, the carbon is partly disappeared and left



**Fig. 7** EDX analyses of different areas of the  $\text{Al}_2\text{O}_3\text{-C}$  coating, **a** overview, **b** only C and O peak; EDX filter 1 (Fig. 1), EDX filter 2 (Fig. 6b), EDX filter 3 (Fig. 6c), and EDX filter 4 (Fig. 6d)

behind pores (Fig. 6d) or a very dense structure made of mostly alumina particles (Fig. 6c). The latter is very surprising due to the high temperature needed to compact alumina grains ( $>1400\text{ }^\circ\text{C}$ ). The temperature during the filtration trials was not higher than  $750\text{ }^\circ\text{C}$ , i.e., significantly lower than the required compaction temperature. Further in-depth investigations towards the observations made in this study are necessary for more clarification (Fig. 7).

## Conclusion

In the present study, carbon-bonded alumina filters, normally used for the filtration of steel melts, have been investigated as a potential filter material for the filtration of aluminum. Short- and long-term pilot-scale filtration trials were conducted.

The sessile drop trials with a simple dropping unit generated  $\text{Al}_2\text{O}_3\text{-C/Al}$  couples which were examined by SEM and EDX. Despite a missing adhesion between aluminum droplet and  $\text{Al}_2\text{O}_3\text{-C}$  substrate, a reaction zone with a thickness of around  $500\text{ }\mu\text{m}$  next to the aluminum melt was observable.

The short-term trial showed a better filtration performance of the  $\text{Al}_2\text{O}_3\text{-C}$  filter compared to the  $\text{Al}_2\text{O}_3$  reference filter. In contrast, the long-term filtration trials did not reveal the beneficial filtration effect of carbon-bonded alumina filters regarding the LiMCA results.

The extensive SEM investigations of the used  $\text{Al}_2\text{O}_3$  and  $\text{Al}_2\text{O}_3\text{-C}$  filters did not detect a large amount of typical non-metallic inclusions in the solidified aluminum. Furthermore, the SEM analyses disclosed a partial transformation

of the  $\text{Al}_2\text{O}_3\text{-C}$  coating layer from a heterogeneous and porous layer into a dense and compact layer. EDX analyses revealed a correlation between the density and the carbon content of the  $\text{Al}_2\text{O}_3\text{-C}$  coating layer. The denser the layer, the lower was the carbon peak in the EDX analyses.

The missing improvement of the filtration behavior and the unstable structure of the  $\text{Al}_2\text{O}_3\text{-C}$  coating show that  $\text{Al}_2\text{O}_3\text{-C}$  (in its presented form) is not suitable for long-term filtration tasks. Further investigations towards the filtration behavior of  $\text{Al}_2\text{O}_3\text{-C}$  filters and the chemical and morphological alteration of  $\text{Al}_2\text{O}_3\text{-C}$  during filtration are necessary.

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