THEMATIC SECTION: ADDITIVE MANUFACTURING BENCHMARKS 2018



Accurate Prediction of Melt Pool Shapes in Laser Powder Bed Fusion by the Non-Linear Temperature Equation Including Phase Changes

Model validity: isotropic versus anisotropic conductivity to capture AM Benchmark Test AMB2018-02

Stefan Kollmannsberger¹ • Massimo Carraturo^{1,2} · Alessandro Reali² · Ferdinando Auricchio²

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Abstract

In this contribution, we validate a physical model based on a transient temperature equation (including latent heat), w.r.t. the experimental set AMB2018-02 provided within the additive manufacturing benchmark series, established at the National Institute of Standards and Technology, USA. We aim at predicting the following quantities of interest, width, depth, and length of the melt pool by numerical simulation, and report also on the obtainable numerical results of the cooling rate. We first assume the laser to possess a double-ellipsoidal shape and demonstrate that a well-calibrated, purely thermal model based on isotropic thermal conductivity is able to predict all the quantities of interest, up to a deviation of maximum 7.3% from the experimentally measured values. However, it is interesting to observe that if we directly introduce, whenever available, the measured laser profile in the model (instead of the double-ellipsoidal shape), the investigated model returns a deviation of 19.3% from the experimental values. This motivates a model update by introducing anisotropic conductivity, which is intended to be a simplistic model for heat material convection inside the melt pool. Such an anisotropic model enables the prediction of all quantities of interest mentioned above with a maximum deviation from the experimental values of 6.5%. We note that, although more predictive, the anisotropic model induces only a marginal increase in computational complexity.

Keywords Melt pool size · Validation · Model calibration · Laser powder bed fusion · Heat transfer analysis · SLM · Laser bed power fusion · Metal additive manufacturing

Introduction

The shape and thermal history of the melt pool are key ingredients to determine the physical properties of an artifact generated through a welding process. Therefore, the prediction of weld pool dynamics has been a subject of intensive research in the last decades in both the

Extended author information available on the last page of the article.

experimental and the numerical modeling communities of welding (e.g., recent reviews of this subject are provided in [8, 23]). Furthermore, it is fundamental to observe that process-structure-property relationships are also tightly interlinked and strongly determined by the characteristics of the weld pool in laser powder bed fusion (LPBF) additive manufacturing technologies [22]. Therefore, an accurate thermal analysis is a key ingredient in the numerical simulations and predictions of LPBF processes as well.

To this end, many physical models have been proposed to obtain accurate and reliable numerical approximations of melt pools. Although different in scale, the basic phenomena in LPBF are similar to those in arc welding processes (see [11, 15, 24] for an overview). Recent summaries more specific to LPBF processes are published in [18, 21, 22]. While particle-based models [12] as well as lattice Boltzmann-type approaches [14] exist, most common are

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Stefan Kollmannsberger stefan.kollmannsberger@tum.de

continuum models based on the conservation of mass, momentum, and energy [25]. Continuum approaches allow for modeling the transient evolution of primal variables (temperatures, pressures, and velocities), taking into account a large number of effects, such as the convection inside the melt pool, also including the one caused by a gradient in the surface tension (Marangoni effect as well as capillary effects), vaporization, momentum losses in mushy zones due to porous media effects, etc.

All these models may deliver very accurate results, but the more effects they include, the more computational power they require. Additionally, the abundance of models comes along with a wealth of parameters: these may be material viscosity, density, thermal conductivity and capacity, latent heat, etc., most of which show a non-negligible temperature dependence, such that their accurate, experimental determination may be both crucial and critical. Further, modeling parameters, such as emissivity or absorptivity or even the geometry of powder particles, may come into play and they can be introduced in the model as boundary or initial conditions. However, accurate measurements of many of the listed parameters are not publicly available. This is even true for the most basic parameters, such as heat capacity or thermal conductivity, that are not published for the temperatures involved in metal-based LPBF processes. All this drought of information results in the fact that even the evaluation of several parameters may itself often rely on models which, in turn, need to be calibrated against further observations.

The dilemma of choosing a correct model for the case of limited data is an important issue in statistics. As an example, George Box [3] stated, somewhat drastically in his wellknown aphorism, that all models are wrong and that, therefore, the most complicated model is not necessarily the best. Instead, it is recommended to follow the lines of William of Occam, in which an economical description of the observations is sought which "is as simple as possible, but not simpler."

Following this line of thought, the purpose of the present paper is to build and validate an economical model able to replicate the results obtained by the benchmark measurements of a single-line laser stroke on a bare metal plate of IN625 published in [1]. As stated in the chapter CHAL-AMB2018-02-MP of the previous reference, the quantities of interest are the width, depth, and length of the melt pool. Additionally, we also monitor the cooling rate as defined in CHAL-AMB2018-02-CR, even if this quantity is not of primary concern here. To this end, we employ a heat transfer model which considers the different phases of the material as homogeneous media. This model is designed to work for pure conduction, i.e., keyhole modes can neither be forecasted nor replicated. This approach is well established in the literature and has proven to be effective also in the thermal numerical analysis of large-scale LPBF processes [5, 7, 20]. Other successful attempts in this direction, however, with a focus on the scale of the melt pool, include the very recent publication of Zhang [26], which provides a summary of previous approaches but most importantly also incorporates anisotropic conductivities, as discussed in the paper at hand. The model proposed in [26] is more elaborate than ours as it also incorporates a spatially variable laser absorptivity and, in this sense, it is not minimal w.r.t. the dataset we face. Further, interesting efforts to construct a valid yet minimal model are published in [17] where the linking of thermal models to experiments is carried out via surrogate modeling based on multivariate Gaussian processes.

We begin by introducing the widely used physical model based on the transient heat equation including phase changes in "Governing Equations". We shortly remark on the verification of this model in "Model Verification", before we move to model validation in "Model Validation". The section on model validation is the main section and commences with reciting the main results of the bench mark cases obtained on two machines, a commercial machine (CBM) and the additive manufacturing metrology testbed (AMMT), both located at the National Institute of Standards and Technology, USA. In an effort to obtain a minimal set of modeling parameters, we evaluate the sensitivities of the quantities of interest to the modeling parameters given by the physical model. We then select only the most relevant modeling parameters and use them to calibrate the physical model toward a similar benchmark already published as case 7 in [9]. We then proceed with the evaluation of our model against the benchmark results on the CBM machine. We observe that the more accurate measurements of the laser profile on the AMMT render the model calibrated to the CBM machine using a doubleellipsoidal heat source less accurate in the AMMT case in which accurate measurements of the laser profile exist. This observation necessitates an update of the model. The model update is presented in "Anisotropic Conductivity Model" by incorporating anisotropic conductivity, which is thought to be a simple way to model the convection inside the melt pool. Finally, in "Summary and Conclusions", we conclude that, given accurate measurements of the profile of the laser, the anisotropic model provides an increase in accuracy over the tested parameter range as compared to the simpler, isotropic physical model.

Governing Equations

We use a non-linear heat transfer equation as a physical model to describe the evolution of temperature $T = T(t, \mathbf{x})$ as a function of space and time.

Given a spatial domain Ω and a time interval $\mathcal{T} = [0, t_{end})$, the heat transfer equation can be written as follows:

$$\rho c \frac{\partial T}{\partial t} + \rho L \frac{\partial f_{pc}}{\partial t} - \nabla \cdot (k \nabla T) = 0 \qquad \text{in} \quad \Omega \times \mathcal{T}.$$
(1)

Therein, ρ and *L* describe the density and the latent heat of the material, and $c = c(T, \mathbf{x})$ and $k = k(T, \mathbf{x})$ are the temperature-dependent heat capacity and thermal conductivity of the material, while $f_{pc} = f_{pc}(T)$ is the phase-change function describing the solid-to-liquid phase transition of the material. Therefore, besides the non-linear contribution of the heat capacity and thermal conductivity, the latent heat term of Eq. 1 introduces a further nonlinearity into the problem. Equation 1 is completed by the initial condition at time t = 0:

$$T(\mathbf{x},0) = T_0 \qquad \text{in} \quad \Omega, \tag{2}$$

as well as Neumann boundary conditions:

$$k\nabla T \cdot \mathbf{n} = q^r + q^l$$
 on $\Gamma_N \times \mathcal{T}$. (3)

Herein, T_0 is the initial temperature of the body, **n** is the unit normal vector, q^l is the heat flux input, and q^r is the radiation boundary condition defined as:

$$q^{r} = \sigma \epsilon \left(T^{2} + T_{e}^{2}\right) \left(T_{e}^{2} - T^{2}\right).$$
(4)

In Eq. 4, σ is the Stefan-Boltzmann constant, ϵ is the emissivity of the material, and T_e is the ambient temperature. In our model, convection boundary conditions are neglected. Further details, specifically the adopted finite element formulation, are provided in [4, 13].

Phase-Change Model

For isothermal phase changes, f_{pc} exhibits a jump at the melting temperature T_m , as the temperature changes the material state from solid to liquid. Since the phase change for metals is actually non-isothermal, we regularize this sudden jump between two temperatures T_s and T_l , with $T_s < T_l$. We can now define the phase change function f_{pc} , such as:

$$f_{pc}(T) = \frac{1}{2} \left[\left(S \frac{2}{T_l - T_s} \left(T - \frac{T_s + T_l}{2} \right) \right) + 1 \right].$$
(5)

The parameter S in Eq. 5 is initially estimated such that the bulk of the phase change occurs between T_s and T_l (see Fig. 1). Nevertheless, since no measurement data is available as to how exactly the phase change occurs, S also requires calibration.



Fig. 1 Phase-change function for different values of the parameter S

Heat Flux Model

In the sequel, we consider two variants of the heat flux input q^l . The first variant is the double-elliptical model of Goldak [10] described in Fig. 2. The front quadrant as is defined by:

$$q^{l} = \frac{2Q\eta f_{f}}{\pi ac_{f}} \exp\left(-2((z^{'} - z^{'}_{0})/c_{f}^{2} + (x - x_{0})/a^{2})\right), \quad (6)$$

while in the rear quadrant it takes the form:

$$q^{l} = \frac{2Q\eta f_{r}}{\pi a c_{r}} \exp\left(-2((z^{'} - z^{'}_{0})/c_{r}^{2} + (x - x_{0})/a^{2})\right).$$
 (7)

Herein, Q is the laser power and η is the absorptivity of the material. The geometrical parameters z'_0 and x_0 define the center of the laser beam on the upper surface at time t, while f_f and f_r are the fractions of heat deposited in the front and the rear quadrants, respectively, which have the side condition that $f_r + f_f = 2$ (see [10] for further details).



Fig. 2 Goldak model for the heat flux input. The model consists of a double-ellipse on which a Gaussian profile is defined

The second variant, the heat source q^l , is not a model. In fact, q^l is directly provided to Eq. 3 as given by corresponding measurements.

Model Verification

The computational model was verified against the series of analytical or semi-analytical solutions defined in [13], where a multi-level hp discretization was used. The computational model utilized in the paper at hand is slightly different, as it uses an IGA discretization wherein multilevel Bézier extraction is applied to construct an efficient discretization which is refined locally in the vicinity of the laser beam. This implementation was verified in [6] in two dimensions as well as in three dimensions using the same series of problems which were also used for the verification of the multi-level hp basis [13]. Since the focus of the present contribution is the validation of the model, we will not repeat these extensive verification studies. Instead, in the next section of this paper, we will use the capabilities of the proposed discretization to directly evaluate the validity of the physical model given in "Governing Equations".

Model Validation

As a preamble to this section, we want to highlight the fact that there are situations (e.g., the presence of highly complex phenomena, problem physics still unclear, model uncertainties and difficulties to ascertain its effectiveness, inability to measure all the model parameters) in which model validation must consist of two steps. In the first step (calibration step), the indeterminacy of the physical model is investigated and calibrated against a first set of experimental evidences; in the second step (validation step), the numerical results are compared against a different set of experimental evidences in order to define the range of validity and the robustness of the numerical model. The case under investigation is characterized by the inability to measure all the model parameters; in particular, we have limited information on the absorptivity, emissivity, thermal conductivity, and heat capacity of the material at high temperature, justifying the choice of the previously defined two-step model validation process.

In "Benchmark Cases", we will shortly describe and report the experimental benchmarks published in [1]. Following the previously described steps of the validation procedure, first, in "Isotropic Conductivity Model", we calibrate the isotropic model of "Governing Equations" using the double-ellipsoidal heat source introduced by Goldak [10] and then we validate the isotropic model using the two heat fluxes described in "Heat Flux Model". Table 1 CBM machine: parameter values

Parameter values	А	В	С
Laser power (W)	150	195	195
Laser speed (mm/s)	400	800	1200
Laser spot diameter $D4\sigma(\mu m)$	100	100	100

For the case in which an accurate measurement of the laser power distribution is given, we observe that the isotropic material assumption has a very limited range of validity. These findings serve as a motivation to extend the physical model by introducing anisotropic conductivities. This extended model is then presented in "Anisotropic Conductivity Model" where it will be demonstrated that it predicts weld pool shapes with an improved accuracy.

Benchmark Cases

All benchmark cases are thoroughly defined in the laser additive manufacturing benchmarks published in [1], including a detailed report on the measurements. The benchmarks are obtained through a traveling laser beam on a bare metal plate of nickel-based alloy IN625. The experimental quantities we will use to validate our model are width, length, and depth of the melt pool as defined in CHAL-AMB2018-02-MP of the above reference. We also report on the cooling rates defined in CHAL-AMB2018-02-CR, although they are not the primal focus in the paper at hand. The benchmarks cited above and reported in [1] were performed on two different machines: a commercial machine (CBM) and the additive manufacturing metrology testbed (AMMT), both located at the National Institute of Standards and Technology, USA. On each machine a set of ten measurements was carried out for three different cases (labeled A, B, and C), i.e., for varying laser power and speed. These cases are specified in Table 1 for the CBM machine and Table 2 for the AMMT machine. The averages of the experimental measurements for the CBM machine are reported in Table 3, while average measurements for the AMMT machine are reported in Table 4. In the first case, the cooling rate is defined as:

$$CR = \frac{1290\,[^{\circ}\mathrm{C}] - 1000\,[^{\circ}\mathrm{C}]}{\Delta d[mm]} \times v\left[\frac{mm}{sec}\right],$$

Table 2 AMMT machine: parameter values

Parameter values	А	В	С
Laser power (W)	137.9	179.2	179.2
Laser speed (mm/s)	400	800	1200
Laser spot diameter $D4\sigma(\mu m)$	170	170	170

 Case
 Length (μm) Cooling rate $(\frac{^{\circ}C}{sec})$

 A
 659 ± 21
 $6.20 \times 10^5 \pm 7.99 \times 10^4$

 B
 782 ± 21
 $9.35 \times 10^5 \pm 1.43 \times 10^5$

 C
 754 ± 46
 $1.28 \times 10^6 \pm 3.94 \times 10^5$

 Table 3
 CBM machine: experimental measurements according to [1], CHAL-AMB2018-02-MP

with v laser speed and Δd distance in the direction of the laser path, while in the second case as:

$$CR = \frac{1290\,[^{\circ}\text{C}] - 1190\,[^{\circ}\text{C}]}{\Delta d[mm]} \times v \left[\frac{mm}{sec}\right]$$

For the exact definition of v and Δd , as well as for further details on the experimental benchmarks, we refer to the original website which continues to be updated as further measurements become available [1].

Isotropic Conductivity Model

The calibration step of the isotropic model is carried out for case B on the CBM machine, as given in Table 1, which is exactly the same configuration as case 7 in [9]. The validation step is obtained by comparing the calibrated model to the cases A, B, and C of Table 3 and Table 4. For all the numerical simulations, the IN625 material parameters are taken from literature [2, 19] and are reported in Table 5, and Figs. 3 and 4. It is noteworthy that material and process parameters necessary to run the numerical simulation are not experimentally available for the effective temperatures occurring in LPBF processes. For example, the measurement of the thermal conductivity k in Fig. 3 is only available up to 871 °C, but the melting range for IN625 is 1290–1350 °C. Likewise, the melting temperature interval—the value of k—can only be extrapolated. It is important to note that this extrapolation itself represents a physical model which, in turn, needs to be calibrated. This circumstance is used in "Anisotropic Conductivity Model" to better describe the conductivity of the material and, consequently, improve the accuracy of the predicted melt pool geometry. Further coefficients, whose measurements are only available up to a certain temperature, are the

 Table 4
 AMMT machine: experimental measurements according to
 [1]
 CHAL-AMB2018-02-MP
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Case	Length (µm)	Width (μm)	Depth (µm)	Cooling rate $\left(\frac{^{\circ}C}{sec}\right)$
A	300	147.9	42.5	1.16×10^6
В	359	123.5	36	1.08×10^6
С	370	106	29.5	1.90×10^6

 Table 5
 Material and process constant parameters

Density	$8.44e - 6 (kg/mm^3)$
Latent heat	2.8e5 (J/kg)
Melting temperature interval	1290–1350 (°C)

absorptivity η and the emissivity ϵ . The latter is necessary to define the radiation boundary condition given in Eq. 3.

In the case of the CBM machine, the benchmark defines the laser spot radius as equal to $50\mu m$. We utilize this value for both parameters c_f and a of the double-elliptical model (see Fig. 2). However, our model also contains the radius ratio c_r/c_f as a model parameter as well as the power fraction f_f/f_r . Both these parameters are additional, potential candidates to calibrate the physical model.

Model Calibration Model calibration first requires identifying the sensitivities of the quantities of interest, i.e., length, width, depth, and cooling rate at the wake of the melt pool w.r.t. the modeling parameters η , ϵ , f_f/f_r and c_r/c_f given by the physical model presented in "Governing Equations". To this end, four studies were carried out, and for each study, a single parameter is varied while the others stay fixed. In the following, we only present the sensitivity studies w.r.t. the absorptivity η and the emissivity ϵ of the material, while the other results are provided in the additional material of the present article. Figure 5 presents the variation of the length, width, depth, and cooling rate w.r.t. the emissivity values. The study clearly suggests that there is practically no influence of the emissivity on the quantities of interest. At first sight, this result comes as a surprise because the model of the boundary conditions suggests an influence of fourth order in the temperature, something that for sure can not be



Fig. 3 Conductivity vs. temperature



Fig. 4 Heat capacity vs. temperature

neglected. Indeed, numerous authors explicitly include this boundary condition to obtain good results, see for example

[16] and the references cited therein. However, the investigation at hand considers the temperature directly under or in close vicinity to the laser and, therefore, the contribution of the radiation boundary condition is marginal. To illustrate this effect, we consider the flux caused by radiation at the melting temperature $T_m = 1290$ °C= 1563.15K, with an ambient temperature of $T_e = 20$ °C= 293.15K. The corresponding power loss is

$$5.67 \times 10^{-8} \times 0.47 \left(T_m^2 + T_e^2\right) \left(T_e^2 - T_m^2\right)$$
$$= 1.59 \times 10^5 \left[\frac{W}{m^2}\right] = 0.16 \left[\frac{W}{mm^2}\right], \quad (8)$$

which represents a negligible quantity compared to the peak power density of $q^l = 2.33 \times 10^4 [W/mm^2]$ in the center of the laser beam. Clearly, under these conditions, radiation itself may be neglected for studies of temperature fields in close proximity to the laser source. On the contrary, the absorptivity has a large influence (see Fig. 6), as do the



Fig. 5 CBM machine. Sensitivity studies w.r.t. the emissivity of the material ϵ



Fig. 6 CBM machine. Sensitivity studies w.r.t. the absorptivity of the material η

power fraction and the radius ratio ¹. An iterative calibration delivers the final choice of the parameters: $\varepsilon = 0.47$, $\eta = 0.38$, $f_f/f_r = 0.053$, and $c_r/c_f = 0.167$.

Numerical results for calibration Numerically computed temperature curves along the laser path are depicted in Fig. 7. The figure reports also the experimentally measured temperature, carried out using in situ thermography, as described in [9]. The different curves labeled 2 mm, 6 mm, and 12 mm indicate at which position the zero of the abscissa of the plot coincides with the laser path. A steady state is reached already after only 2 mm. We specifically note that the calibration was carried out to best capture the temperature range around the melting temperature. Larger even unphysical deviations are tolerated outside this

¹The latter two are not depicted due to limitations of space in this article



Fig. 7 Computation of the temperature profile calibrated to case 7 in [9]



Fig. 8 Computation of cross section (red line) calibrated to case 7 in [9]

region. This kind of calibration toward a process window is justifiable not only due to the fact that merely the region of interest needs to be captured with accuracy by the computations, but also because the camera itself delivers its most accurate measurements in that range. The plot also directly shows where the numerical model is not valid, namely directly inside the melt pool. Here, the temperature drastically overshoots to unrealistically high values. The very good agreement of the computation in the range of the melting zone is further confirmed in Fig. 8. This figure overlays the image of the cross section of the track taken by an ex situ measurement of a confocal laser scanning microscope (CLSM) with the calibrated computation. Both Figs. 7 and 8 demonstrate that it is possible to obtain an excellent agreement with the experiment using the simple physical model presented in "Governing Equations", if η , f_f/f_r , and c_r/c_f serve as model calibration parameters.

Model validation for the CBM machine The calibrated model delivers the results depicted in Table 6.

It can readily be concluded that the model is able to predict the length of the weld pool by up to at least 7.3% accuracy in the parameter range covered by cases A to C. The prediction of cooling rates is approximately less accurate by one order. In fact, the cooling rate is a derived variable (we directly compute only the temperature) and thus less accuracy is naturally expected; moreover, since

 Table 6
 CBM machine: obtained weld pool length l and cooling rates (CR)

Case	Meas. l(μm)	Num. l(µm)	Δ (%)	Meas. CR $\left(\frac{^{\circ}C}{sec}\right)$	Num. CR $\left(\frac{^{\circ}C}{sec}\right)$	Δ (%)
A	659	707	7.3	6.20×10^{5}	8.79×10^{5}	41.8
В	782	812	3.8	9.35×10^{5}	1.35×10^{6}	44.3
С	754	772	2.4	1.28×10^6	$2.09\!\times\!10^6$	63.3

Table 7	AMMT	machine:	computed	values
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Case	Length (µm)	Width (µm)	Depth (µm)	Cooling rate $\left(\frac{\circ C}{sec}\right)$
A	301	119	52	0.91×10^{6}
В	360	103	42	1.33×10^{6}
С	348	91	32	2.18×10^{6}

our model does neither include convection nor evaporation, the temperature predicted within the melt pool is likely inaccurate and this surely affects also the cooling rate results in the transfer region from solid to liquid.

It is interesting to note that the measured length in [9], i.e., the length toward which the model was calibrated was $813[\mu m]$, provided with a tolerance of $\pm 79[\mu m]$. However, measurements performed in [1] for exactly the same case (case B) were more accurate and are given as $782 \pm 21[\mu m]$ (see also Table 6). Thus, a recalibration of the model to case B will likely deliver more accurate predictions for the cases A and C. However, this was not carried out because even more accurate measurements are available for the AMMT machine which lead to the development of the extended physical model presented in "Anisotropic Conductivity Model".

Model validation for the AMMT machine Surprisingly, very different experimental results were obtained with the same scan parameters at the AMMT machine as compared to the CBM machine. Due to this reason, more thorough studies were carried out on the AMMT machine. These include measurements of the actual laser profile itself. These measurements, now published in [1], enable their direct application as the Neumann boundary condition q^{l} in Eq. 3. Thus, the physical model presented in "Governing Equations" is more tightly defined. This generates an interesting situation from the perspective of model validation because two (influential) calibration parameters, the power fraction f_f/f_r and the radius ratio c_r/c_f , are now fixed and, therefore, can not be used for calibration. Given that the emissivity ϵ has practically no influence, the absorptivity η is the only parameter left for

 Table 8
 AMMT machine: deviations from experimental values

Case	Length $\Delta(\%)$	Width $\Delta(\%)$	Depth $\Delta(\%)$	Cooling rate $\Delta(\%)$
A	0.47	19.3	18.6	21.6
В	0.11	16.4	15.8	23.1
С	5.9	14.2	10.1	14.7



Fig. 9 Scaling of the conductivity in direction i = x, y, z

a recalibration. For $\eta = 0.086$, we obtain the numerical results provided in Table 7. The corresponding deviations are provided in Table 8. While the deviations in the length are still at a maximum of approx. 6%, width and depth are only predicted to an accuracy of 20%. No further calibration is possible as there is only one parameter to calibrate but three values of interest to fit (excluding the cooling rate). This clearly shows the boundaries of validity of the model presented in "Governing Equations" and motivates the development of the model discussed in the next section.

Anisotropic Conductivity Model

Two possible modifications are readily imaginable: (a) a definition of an absorptivity field instead of a scalar value η and (b) the definition of an anisotropic conductivity. The former could be motivated by the fact that the melt pool surface will surely cause the absorption of the laser energy to be non-constant. However, to the authors' opinion, a good model should be as simple as possible, yet replicate the observed effects as accurately as possible. With this objective in mind, the definition of an anisotropic

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 Table 9
 Anisotropic conductivity model: computed values

Case	Length (µm)	Width (μm)	Depth (µm)	Cooling rate $\left(\frac{°C}{sec}\right)$
A	304	146.4	44.6	0.82×10^{6}
В	362	123.7	36.1	1.23×10^{6}
С	346	105.1	27.3	1.88×10^6

conductivity is a more attractive choice. The only change necessary is that the scalar value k in Eq. 1 changes to \mathbf{k} , a diagonal matrix with the entries $diag(k_x, k_y, k_z)$. Further, we set $\epsilon = 0$. The physical motivation for this model is that the (transient) diffusion equation given by Eq. 1 does by no means include the effects caused by convective heat transfer inside the weld pool. This flaw has already inspired other authors, e.g., [16], to use a strongly increased conductivity k inside the melt pool to model convective effects. We now extend this idea by choosing anisotropic values. For simplicity, we introduce the scaling factor ϑ_i where i = $\{x, y, z\}$ such that $\mathbf{k} = diag(k\vartheta_x, k\vartheta_y, k\vartheta_z)$. The values for ϑ_i deviate from 1 only after the last obtainable measurement (at $T = 871^{\circ}C$) of the conductivity as depicted in Fig. 9. After calibration to the AMMT machine B, we obtain the set $\vartheta_x = 1.0, \vartheta_y = 1.4, \vartheta_z = 0.9$. This delivers very well-matching weld pool geometries. While the effect of the scaling of k is marginal in a temperature plot along the length (because here $\vartheta_x = 1.0$), its effect in the cross section is quite pronounced (see Fig. 10 for a direct overlay of the melt pool geometry over the cross section). In the validation step, we keep the calibration parameters fixed, i.e., $\vartheta_x = 1.0$, $\vartheta_y = 1.4$, and $\vartheta_z = 0.9$, and we compute cases A and C of the AMMT machine. The computed values are provided in Table 9 and the corresponding deviations are provided in Table 10. We observe that for the anisotropic model the maximum deviation of length, width, and depth is 6.49% at worst, while, for the isotropic conductivity model, it was merely 19.3%. Even the forecast of the cooling rates has improved sightly.

Fig. 10 Melt pool cross-section micrograph image 50×DF (from https://phasedata.nist.gov/rest/ blob? id=5b102edd4407e700870ff13e)

over computed cross sections using isotropic (dashed red line) and anisotropic conductivity (dashed green line)



Case	Length $\Delta(\%)$	Width $\Delta(\%)$	Depth $\Delta(\%)$	Cooling rate $\Delta(\%)$
A	1.33	1.0	2.5	29.3
В	0.84	0.02	0.2	13.9
С	6.49	0.8	5.1	1.3

 Table 10
 Anisotropic conductivity model: deviations of computed values from experimental values

Summary and Conclusions

In this contribution, we used the standard heat diffusion model to predict the length, width, and depth of the melt pool in the laser additive manufacturing benchmarks CHAL-AMB2018-02-MP published in [1]. The physical model included a latent heat term as published, e.g., in [4], along with a radiation boundary condition. Within this model, we found the radiation boundary condition to have little to no influence upon the quantities of interest. This is due to the fact that in close proximity of the laser beam impact region, the power lost by radiation is much lower than the applied laser energy itself.

As a first approach, we assumed the laser source to possess the well-known double-elliptical shape as proposed for welding by Goldak [10]. We demonstrated that this model is well suited to predict the shape of the weld pool as it delivered a maximum deviation from the measurements of 7.3%. However, in case the shape of the laser source is given by a measurement, the standard, transient heat diffusion model only provides accuracies of 19.1% for the investigated benchmark cases. This renders it practically invalid.

We then extended the isotropic thermal model by introducing anisotropic conductivities. Their physical interpretation is to model anisotropic convection inside the melt pool. This slight extension enabled the model to deliver at worst 6.49% deviations in length, width, and depth of the melt pool. Therefore, we conclude that the introduction of an anisotropic conductivity is a simple yet effective way of improving the physical model based on the transient heat equation including phase changes, and remark that the added computational effort for this extension is marginal.

In the future, we aim at validating a numerical model including powder. Nevertheless, this task is not straightforward since measurements of melt pool shapes in the presence of a powder bed are extremely challenging. We want to finally stress the fact that the presented model is meant to provide, once thoroughly calibrated, a reliable model for multi-track and eventually multi-layer thermal simulations. However, it is not valid to predict the temperature distribution within the melt pool. **Funding Information** The first author received financial support from the German Research Foundation (DFG) under grant RA 624/27-2. This work was partially supported by Regione Lombardia through the project "TPro.SL - Tech Profiles for Smart Living" (No. 379384) within the Smart Living program, and through the project "MADE4LO - Metal ADditivE for LOmbardy" (No. 240963) within the POR FESR 2014-2020 program. Massimo Carraturo and Alessandro Reali have been partially supported by Fondazione Cariplo - Regione Lombardia through the project "Verso nuovi strumenti di simulazione super veloci ed accurati basati sull'analisi isogeometrica", within the program RST - rafforzamento.

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Affiliations

Stefan Kollmannsberger¹ . Massimo Carraturo^{1,2} · Alessandro Reali² · Ferdinando Auricchio²

Massimo Carraturo massimo.carraturo@tum.de; massimo.carraturo01@universitadipavia.it

Alessandro Reali alessandro.reali@unipv.it

Ferdinando Auricchio auricchio@unipv.it

- ¹ Technical University of Munich, Munich, Germany
- ² University of Pavia, Pavia, Italy